

A comprehensive constitutive law for waxy crude oil: A thixotropic yield stress fluid

Christopher J. Dimitriou,^{a,b} and Gareth H. McKinley^{*a}

Received Xth XXXXXXXXXXXX 20XX, Accepted Xth XXXXXXXXXXXX 20XX

First published on the web Xth XXXXXXXXXXXX 200X

DOI: 10.1039/b000000x

Guided by a series of discriminating rheometric tests, we develop a new constitutive model that can quantitatively predict the key rheological features of waxy crude oils. We first develop a series of model crude oils, which are characterized by a complex thixotropic and yielding behavior that strongly depends on the shear history of the sample. We then outline the development of an appropriate preparation protocol for carrying out rheological measurements, to ensure consistent and reproducible initial conditions. We use RheoPIV measurements of the local kinematics within the fluid under imposed deformations in order to validate the selection of a particular protocol. Velocimetric measurements are also used to document the presence of material instabilities within the model crude oil under conditions of imposed steady shearing. These instabilities are a result of the underlying non-monotonic steady flow curve of the material. Three distinct deformation histories are then used to probe the material's constitutive response. These deformations are steady shear, transient response to startup of steady shear with different aging times, and large amplitude oscillatory shear (LAOS). The material response to these three different flows is used to motivate the development of an appropriate constitutive model. This model (termed the IKH model) is based on a framework adopted from plasticity theory and implements an additive strain decomposition into characteristic reversible (elastic) and irreversible (plastic) contributions, coupled with the physical processes of isotropic and kinematic hardening. Comparisons of experimental to simulated response for all three flows show good quantitative agreement, validating the chosen approach for developing constitutive models for this class of materials.

1 Introduction

The term “yield stress fluid” is used to describe soft rheologically-complex materials that behave like a solid at low levels of imposed stress, yet flow when subjected to stresses that exceed a critical value^{1,2}. These types of materials are ubiquitous in nature and in industrial applications, so predicting their rheology with a constitutive model is an important challenge. The term yield stress fluid is a rather broad classification for materials which exhibit this general behavior of transitioning from solid to liquid, and these materials can exhibit additional complexities in their rheological behavior. Møller et al.³ proposed using thixotropy as a distinguishing behavior that separates “ideal” yield stress fluids from “non-ideal” yield stress fluids. Thixotropy describes the ability of a material to exhibit a continuous and reversible time-dependent change (usually a decrease) in viscosity at a particular constant imposed shear rate.^{4–6} These time-dependent changes in viscosity are due to a gradual change in the microstructure of the material resulting from the application of shear;

this mechanism is commonly referred to as shear rejuvenation. Thixotropic materials also exhibit aging, which describes the ability of the material to reacquire its initial structure under the absence of shear (hence the reversibility of the initial time-dependent change). The aging phenomenon is commonly the result of thermally activated Brownian motion causing a sufficient rearrangement of the material's microconstituents. When this rearrangement occurs, the attractive forces between these microconstituents can cause a reformation of the sample spanning network in the material structure^{5,6}.

The classification used by Møller et al. is a simplified view of yield stress fluids. For example, Divoux et al.^{7,8} showed that even Carbopol, widely considered to be an “ideal” yield stress fluid³, can exhibit some non-idealities (e.g. shear banding) that are associated with thixotropic yield stress fluids. Given the ubiquity of thixotropic behavior in yield stress fluids, it is important to have an appropriate constitutive framework for modeling the rheology of these fluids. The development of such a framework is a critical issue which remains to be addressed⁶. There is a significant body of literature which has strived towards this goal^{9–19}. Many of the models in the literature adopt a scalar structure parameter (frequently, but not always, denoted as λ) to describe some appropriate measure of the internal material structure. This material structure

^a Department of Mechanical Engineering, Massachusetts Institute of Technology, Cambridge, MA 02139; E-mail: gareth@mit.edu

^b Current address: Nike Inc. Polymers R&D, 13630 SW Terman Rd., Beaverton, OR 97005

can build up or break down over time due to the application of shear, and the evolution equation for the structure parameter therefore typically contains an aging term, and a shear rejuvenation term. The structure parameter is then related to macroscopic rheological parameters in the fluid, such as the yield stress, shear viscosity, or elastic modulus.

Other models in the literature take a different approach by modeling the underlying microstructural physics in these materials. Rather than prescribing a constitutive behavior based on rheological measurements of the material, the constitutive relations are formally derived by considering interactions between the material's microstructural elements. Some of the more prominent examples of such models include the Soft Glassy Rheology (SGR) model^{13,20}, the Shear Transformation Zone (STZ) model^{14,21} and the Kinetic Elastoplastic (KEP) model^{18,22}. As a testament to the capability of these models, several important experimental observations are predicted including shear banding/nonlocal effects^{23,24}, power law dependency of LVE moduli on frequency and stress overshoots¹³. Together with their generality and the added intuition developed from the microstructural approach, these models are quite appealing. However considerable mathematical manipulation is often required in order to express them in terms of macroscopic variables such as stress or strain, and they have not been as extensively fit to experimental data. On the other hand, models such as those of Quemada¹⁵, Mujumdar et al.¹⁷ as well as many others, are explicitly written in terms of stress and strain. This form facilitates the fitting and use of such models in engineering applications.

The particular subclass of thixotropic yield stress fluids studied here are model waxy crude oils. Wax is a commonly encountered component of crude oils that can be present as a solid precipitate at low temperatures. These solid precipitates have adverse effects on the rheology of the crude oil during production scenarios^{25,26}, so engineers and scientists must be aware of the thixotropic nature of waxy crude oils^{4,27}. Detailed studies of the rheology of these fluids emphasized the importance of sample preparation protocol (or *beneficiation*²⁸) in order to ensure repeatable rheological data^{29–31}. However, one of the issues presented when measuring the rheology on these fluids is the variability in sample composition across different crudes (asphaltene content, wax content³²). For these reasons, we utilize a *model* waxy crude oil in the present study, the composition of which can be tightly controlled by formulating the fluid in the laboratory.

The thixotropic behavior of these fluids also makes reproducible rheological data difficult to obtain. Comprehensive, quantitative comparisons with model predictions are therefore scarce. Many of the models employed in the literature are simplified inelastic models, e.g. the frequently used Houska model^{9,33} does not account for material elasticity, and the Pedersen model^{28,34} assumes a generalized Newtonian

fluid with temperature dependency. A more complete and experimentally-substantiated constitutive law would be useful for developing *flow assurance* strategies³⁵. The goal of flow assurance is to ensure continuous flow of production fluids (crude oils) under adverse scenarios, such as the presence of precipitates or non-Newtonian behavior²⁶. As an illustration, we note that the pressure drop ΔP required to restart a gelled pipeline typically scales with the material yield stress σ_y . In the simplest case, a force balance on a gelled plug of wax gives $\Delta P \pi R^2 \sim \sigma_y \pi D L$, where D is the diameter of the pipe and L is the length. Designing a pipeline network with a fixed pumping capacity ΔP therefore requires a priori knowledge of how the yield stress σ_y varies in the gelled crude oil (especially when aging processes and shear history cause large variations of σ_y with time). This necessitates a constitutive law that can be both fit to rheological data, and has predictive capabilities.

A more comprehensive approach to the rheology of elastoviscoplastic materials, both in terms of experiments and modeling, is therefore required. Coussot et al.¹⁰ and Mujumdar et al.¹⁷ propose several different rheological experiments, among them startup of steady shear and large amplitude oscillatory shear (LAOS) as methods to validate and discriminate between constitutive models. There have also been many recent experimental studies which have combined bulk rheological measurements with velocimetry. These are important experimental efforts, because thixotropic yield stress fluids often exhibit shear banding and other types of heterogeneities in simple viscometric flows. This behavior is commonplace and is observed in a number of specific materials, including suspensions of star polymers³⁶, Laponite gels^{37,38}, emulsions²⁴, Carbopol micro gels⁷ and other colloidal gels³⁹. Shear banding or inhomogeneous flow can significantly affect interpretation of experimental data, so the use of velocimetric techniques has become an important part of the experimentalist's toolbox.

Hence, combined with a detailed preparation protocol for our model fluid (which is validated using direct measurements of flow kinematics), we will use a suite of well-defined viscometric flows to evaluate a constitutive model. The model we develop will be verified across a wide range of data. Once the model parameters are fixed, the constitutive equations are solved for an additional independent test protocol in order to explore the predictive capabilities of the model. This gives further experimental validation to future numerical studies which would utilize the model to predict pipeline restart.^{40,41}

We endeavor to expand the approaches for describing thixotropic materials by introducing ideas from plasticity that have not been widely used in prior studies of such phenomena. The term “yield stress fluid” generally describes a yielding material with rate-dependent plastic flow above a critical stress. This behavior is generic, and is even exhibited by metals at elevated temperatures^{42,43}. The strengthening/softening

processes that characterize thixotropy are similar to hardening mechanisms that are used in plasticity, which also utilize an internal microstructural variable of the form of the scalar parameter λ ⁴². These similarities suggest that there are underlying links between the models employed to describe thixotropic yield stress fluids, and the models used in plasticity⁴⁴. Early work hinted at the utility of employing concepts from plasticity to model yield stress fluids⁴⁵, but only recently have these mechanisms been used to successfully predict the behavior of a (non-thixotropic) yield stress fluid⁴⁶. In the present contribution, we show for the first time how a constitutive model can quantitatively predict the rheology of waxy crude oil (a specific thixotropic yield stress fluid) across a comprehensive set of experimental data. The set of experimental data includes steady and transient tests, as well as linear and nonlinear rheological measurements.

This is accomplished by utilizing detailed experiments on a model crude oil to motivate the development of the model. In the development of this model, we take an approach which allows us to rapidly express our model in terms of macroscopic variables (stress and strain), which are the variables that are of interest to the practicing engineer or scientist who deals with flow of a real crude oil. While this approach will not give as detailed an account of the microstructural yielding and thixotropic mechanisms as other approaches^{13,14,18}, we will still take care to provide a general discussion of the microstructural interpretation of these plasticity mechanisms. We will also illustrate the links between this model, and other models that have been employed to predict thixotropic behavior. The constitutive framework can describe the material response to a number of different rheometric test protocols, and also has a general 3D continuum mechanics formulation. It will therefore ultimately be useful for numerical simulations of complex flows of waxy crude oils that can then be used to guide flow assurance strategies.

2 Experimental

2.1 Model Fluids & Rheometry

The class of thixotropic yield stress fluids used here has been characterized in detail in a previous study⁴⁷. They are created by combining a heavy mineral oil (Sigma Aldrich 330760) with a paraffin wax (Sigma Aldrich 327212). The components are combined together at a high temperature ($\geq 60^\circ\text{C}$) and stirred continuously to fully dissolve the wax in the oil. The model fluid behaves as a Newtonian liquid in this state, and can be loaded into the rheometer and cooled in-situ.

Two different rheometers are used to probe the response of this fluid to imposed deformations. A controlled strain rheometer (ARES LS, TA Inst.) is used for large amplitude oscillatory shear (LAOStrain) measurements. The ARES

rheometer is equipped with a lower Peltier plate for temperature control of the sample. The upper fixture is a cone with a diameter of 50 mm and an angle of 2° . The upper and lower surfaces are also roughened (root mean squared roughness $R_q \simeq 30 \mu\text{m}$) in order to suppress wall slip.

A stress controlled rheometer (AR-G2, TA Inst.) is also used. This rheometer is utilized in two different configurations. The first of these is the standard configuration, which incorporates a lower Peltier plate for temperature control, and an upper cone (diameter 60 mm and angle of 2°). This configuration also utilizes roughened upper and lower surfaces, with $R_q \simeq 30 \mu\text{m}$. The second configuration is a custom-designed Rheo-PIV configuration, which allows *in-situ* measurements of the flow field within the fluid to be extracted. This apparatus is described in detail in Sec. 2.2.

In Fig. 1, we illustrate one of the characteristic thermorheological features of these model waxy crude oils - the wax appearance temperature, T_{wa} . Fig. 1 presents measurements of the viscosity of the heavy oil, and a 5% and 10% wax in oil mixture over a range of temperatures (obtained using the standard AR-G2 configuration). In Fig. 1, a shear rate of $\dot{\gamma} = 50 \text{ s}^{-1}$ is imposed on the fluid, while lowering the temperature at a rate of $1^\circ\text{C}/\text{min}$ from 55°C to 25°C . As seen in Fig. 1, the mineral oil exhibits an Arrhenius-like exponential dependence of viscosity on temperature. Both the 10% and 5% wax in oil systems exhibit a similar Arrhenius-like variation of viscosity on temperature for large values of T . However, they rapidly diverge from this dependency at a temperature known as the wax appearance temperature, T_{wa} . This temperature corresponds to the point at which wax crystals first begin to precipitate in a sufficient amount to affect the viscosity of the fluid. The morphology of these crystals is typically sheet-like or needle like^{30,48}, and the high aspect ratio of the crystallites results in mechanical percolation and formation of a gel at low concentrations of precipitated wax.⁴⁹

2.2 Rheo-PIV configuration

A Rheo-PIV apparatus was used to obtain in-situ measurements of the velocity/displacement field within the model fluids as they are sheared in the rheometer. This Rheo-PIV apparatus is based on a previous design^{47,50}, and a schematic diagram is shown in Fig. 2 (a). A laser light sheet (10mW, 635nm wavelength), created by a plano-concave lens, is directed vertically downward into the sample at a location r_l . Displacements of illuminated tracer particles are then tracked to extract the deformation field of suspended particles across the gap between the upper plate and lower cone (with angle ϕ). The fluid is seeded with reflective TiO_2 particles of average size $3 \mu\text{m}$, at a volume fraction of 2×10^{-5} (this volume fraction is low enough not to affect the rheology of the fluid being studied). Cross correlation PIV software (Digi-

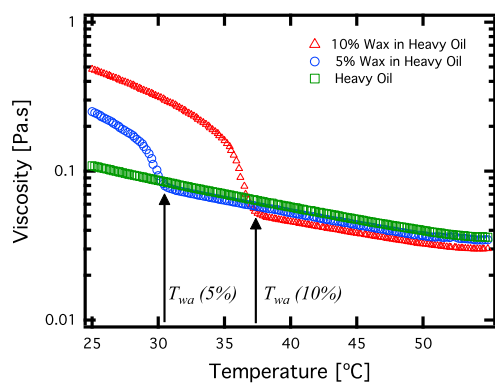


Fig. 1 Temperature sweep of viscosity for 3 different model fluids, at an imposed shear rate of $\dot{\gamma} = 50 \text{ s}^{-1}$. Temperature is ramped at a rate of $1^\circ\text{C}/\text{min}$.

flow, Dalziel Research Partners, Cambridge UK) was used to process sequences of images and obtain the 2-dimensional velocity field within the fluid from a sequence of particle displacements. The 2-dimensional field is averaged along the direction of flow, providing a velocity profile of the form $v(y)$. In this case, y is the position between the lower cone and upper plate, with $y = 0$ at the lower cone, and $y = H \equiv r_l \tan \phi$ at the upper plate. This configuration differs from the standard configuration of the AR-G2 by using a lower cone and an upper plate. A stepped lower Peltier plate (TA Instruments part #531052.901) is utilized that allows for interchangeable lower geometries to be used. All measurements made using the Rheo-PIV configuration use either a 4° or 2° lower machined aluminum cone. The cone is black anodized in order to suppress reflection of the laser sheet from this surface. The upper and lower geometries are smoother than the geometries used in the standard configuration ($R_q \sim 0.1 \mu\text{m}$) - a polished upper geometry is necessary to provide a clear optical path for the reflected light from the tracer particles.

The RheoPIV fixture shown in Fig. 2 has one important alteration from previous versions - the upper rotating plate, which is made from a transparent acrylic disc of diameter 50 mm, has a polished 45° bevel machined into the upper corner. This allows the laser-illuminated plane in the sample to be imaged through the flat beveled surface, rather than through the curved fluid meniscus at the edge of the geometry. The fluid meniscus may change in shape over the course of an experiment due to sample shrinkage (which waxy crude oils are known to exhibit⁵¹), or edge instabilities⁵². The flat beveled edge avoids local image distortion which arises from refraction of light across the irregularly shaped air-fluid meniscus. The index of refraction of the acrylic and model oils ($n = 1.49$ and $n = 1.47$ respectively) is very close. This refractive index matching, combined with the bevel, avoids optical aberrations and systematic errors that could arise from the lens/camera

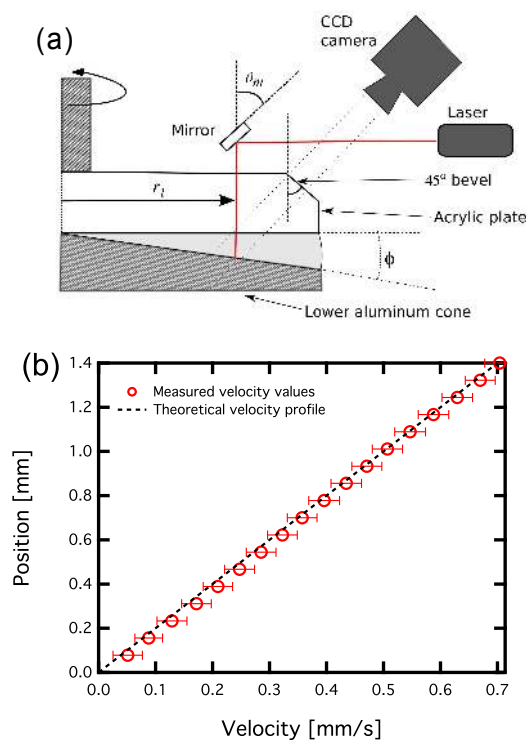


Fig. 2 (a) Schematic diagram of the RheoPIV configuration mounted on the AR-G2. (b) Calibration velocity profile for a Newtonian mineral oil under an applied shear rate of $\dot{\gamma} = 0.5 \text{ s}^{-1}$.

axis not being positioned orthogonally to an interface between two media with different values of refractive index $n_1 \neq n_2$.

The apparatus shown in Fig. 2 (a) allows for the location of the laser light sheet r_l and the angle of the reflective mirror θ_m to be adjusted and optimized. For the experiments presented in this work, the value of r_l was kept constant at 20 mm, while θ_m was held constant at 45° (creating a vertical laser light sheet). It is possible to decrease θ_m so that the plane of illuminated particles is orthogonal to the camera's imaging axis. However, this was not necessary because the camera/lens assembly had a high enough focal depth ($> 2 \text{ mm}$), and all of the illuminated particles across the gap were sufficiently in focus. The laser light sheet is also very thin (approximately $50 \mu\text{m}$), resulting in radial variations in particle location having a negligible effect on the velocity profile. A velocity calibration profile of a heavy mineral oil undergoing steady shear of $\dot{\gamma} = 0.5 \text{ s}^{-1}$ in a 50 mm diameter, $\phi = 4^\circ$ cone-plate geometry is shown in Fig. 2 (b). The profile is averaged from 100 frames of video taken over a course of 3 seconds. It shows excellent agreement with the linear, theoretical profile predicted for a Newtonian fluid with no wall slip at either fixture surface.

2.2.1 Spatially averaged vs. local stresses and shear rates

Throughout this work, we carefully distinguish between spatially averaged measurements of stress and shear rate, and the local values of the stress and shear rate within the fluid. The model waxy crude oils here are known to exhibit wall slip and other shear localization phenomena⁴⁷. When these phenomena are present in cone-plate geometries, the stress and shear rate may no longer be uniform across the radial extent of the geometry^{53,54}. We will therefore define a spatially averaged stress $\hat{\sigma}$ and shear rate $\hat{\gamma}$ as follows:

$$\hat{\sigma} \equiv \frac{3\mathcal{T}}{2\pi R^3}, \quad (1)$$

$$\hat{\gamma} \equiv \frac{\Omega}{\phi}, \quad (2)$$

where \mathcal{T} is the torque that the rheometer imposes on the sample, Ω is the angular rotation rate of the geometry, R is the radial size of the geometry, and ϕ is the cone angle. We also define an average strain accumulated as $\hat{\gamma} \equiv \int_{t_1}^{t_2} \frac{\Omega(t)}{\phi} dt$. Under homogenous shearing with no wall slip, these average quantities reduce to the local true stress σ , the local true shear rate $\dot{\gamma}$ and the local true strain γ . Due to the presence of wall slip and other shear localization events in the fluids, we will reserve the symbols σ and $\dot{\gamma}$ to refer to the stress and shear rate under homogenous deformations only.

2.3 Preparation methods of the model fluid - Slurry vs. Strong Gel

In order to carry out reproducible bulk rheological measurements on waxy crude oil, an appropriate sample preparation protocol must be selected. Waxy crude oils are extremely sensitive to variations in their thermal and shear history as they are cooled to below their wax appearance temperature⁵⁵. Here we justify the selection of one particular preparation protocol which minimizes the impacts of wall slip and material instabilities. This provides reproducible rheometric data, which can subsequently be used for the development of a constitutive model.

We envision two distinct flow assurance scenarios under which waxy crude oils are transported through pipelines. For the first scenario, consider a length of pipeline containing waxy crude at a temperature $T > T_{wa}$, under quiescent (zero flow-rate) conditions. If the temperature of this fluid slowly and uniformly drops to below T_{wa} , then a gel network forms in the material due to the presence of solid wax precipitates. The cooling of this fluid occurs under no flow conditions with zero shear rate. The crystallite aggregates therefore grow to large sizes and the percolated gel structure formed in the crude oil will be stiff (high viscosity and modulus). Restarting the flow in the pipeline after cooling will therefore require large applied pressure drops, with the possibility that the fluid undergoes an adhesive failure (or wall slip) at the pipe wall⁵¹.

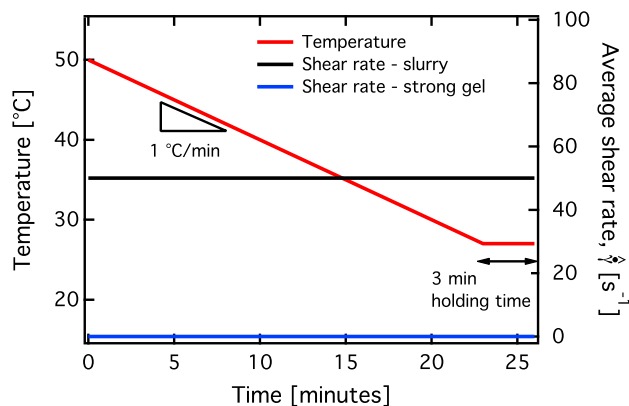


Fig. 3 Protocol used to prepare the model waxy crude oil to its “slurry” state (black curve) and the “strong gel” state (blue curve). The rate of cooling is the same in both cases, however the slurry is formed under the application of a high shear rate (50 s^{-1}).

The second scenario involves cooling the waxy crude oil under non-quiescent (flowing) conditions. For these conditions, the gel structure formed in the oil will be softer (lower modulus and viscosity), due to the disruptive effect of shearing the aggregates of wax crystals as they form. Smaller pressure drops will be required in order to maintain the flow of the fluid through the pipeline, and wall slip will be less likely.

We refer to the state of the crude oil in the first scenario as a “strong gel” and the state of the material in the second scenario as a “slurry”. The strong gel and slurry states of the oil are reproduced in a laboratory scale setup by cooling the model wax-oil mixture from a single phase mixture at $T > T_{wa}$ in the rheometer either quiescently (under zero imposed shear rate) or under a high shear rate ($\hat{\gamma} = 50 \text{ s}^{-1}$). In previous work⁴⁷ we focused on the behavior of the wax-oil system in its strong gel state, which is dominated by wall slip and other interfacial failure processes. Here, we restrict our focus to the rheology of the material in its slurry state. In the slurry state bulk rheological behavior is easier to interpret, due to the absence of these failure processes.

Fig. 4 illustrates the critical differences between the response of a 5% wax-oil mixture in the two different states to a step in the shear rate to $\hat{\gamma} = 1.2 \text{ s}^{-1}$. The response of the model fluid in the slurry state is shown in Fig. 4 (a). The model fluid is brought to this state by cooling the sample from 55°C to 27°C at a cooling rate of $1^\circ\text{C}/\text{min}$, under an applied shear rate of $\hat{\gamma} = 50 \text{ s}^{-1}$. Once the fluid reaches the final temperature of 27°C , the shear rate of $\hat{\gamma} = 50 \text{ s}^{-1}$ is held for an additional 3 minutes, so that any thermal transients in the system die out. After these 3 minutes, the shear rate is immediately reduced to $\hat{\gamma} = 1.2 \text{ s}^{-1}$. This sequence of steps is administered using the AR-G2 in its RheoPIV configuration with a 2° lower cone (discussed in Sec. 2.2). Both the spatially averaged values of

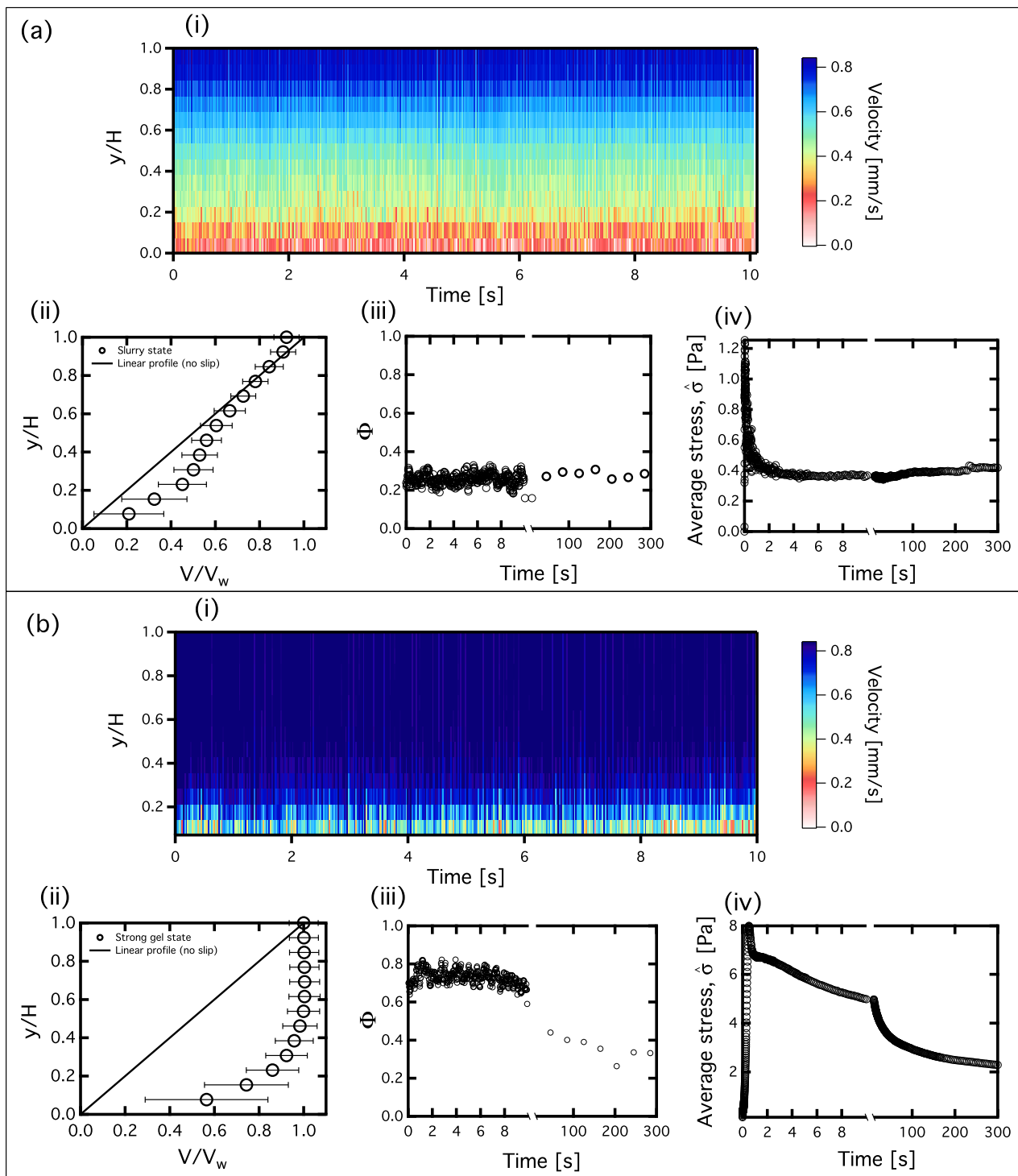


Fig. 4 Illustrating the difference between the wax-oil system in its “slurry state” (a) and in its “strong gel” state (b). For each of the states, a step in (spatially averaged) shear rate to $\dot{\gamma} = 1.2 \text{ s}^{-1}$ is imposed at $t = 0$, and $\hat{\sigma}$ is measured over the course of 300 seconds (iv). In (i), we show spatiotemporal diagrams of the velocity field within the fluid for the first 10 seconds. Plots of the parameter Φ for the entire 5 minutes are given in (iii), while in (ii) we give the average velocity field within the fluid over the 300 seconds. Error bars are equivalent to 2 standard deviations of the velocity measurement at each height.

$\hat{\sigma}$ and $\hat{\gamma}$, and the local flow field within the sample are measured.

The response of the model fluid in its strong gel state is shown in part (b) of Fig. 4. The fluid reaches this state by undergoing the same protocol for the slurry state, however for the cooling step and the subsequent 3 minute holding time, the shear rate is held at $\hat{\gamma} = 0 \text{ s}^{-1}$. This results in an essentially unperturbed gel network before the startup of steady shear of $\hat{\gamma} = 1.2 \text{ s}^{-1}$ is imposed.

The RheoPIV configuration enables measurements of the average stress $\hat{\sigma}$ in the fluid, as well as measurements of the local velocity field during the 300 second application of the shear rate $\hat{\gamma} = 1.2 \text{ s}^{-1}$. In the slurry state, the spatially average stress $\hat{\sigma}$ shows a constant measured value of 0.4 Pa. The strong gel state shows an initial peak in the stress, followed by a slow decay in the measured value of $\hat{\sigma}$, occurring over the course of several minutes. The velocity field within the fluid in the two states (illustrated through the use of spatiotemporal diagrams for the first 10 seconds, as well as the average velocity profiles shown in (ii)) is markedly different for the two cases. For the strong gel state, larger stresses are needed to break the gel structure in the bulk of the fluid. The stiff material therefore flows through the mechanism of wall slip at the lower surface, and remains adhered to the upper surface. The velocity profile in this state is plug-like, in contrast to what is seen for the material in the slurry state. In the slurry state, a velocity profile closer to linear is observed, with a non-zero shear rate in the bulk

We quantify the long term evolution of the velocity profiles in these two states by utilizing a non-dimensional metric Φ , defined in a previous study⁴⁷. This dimensionless scalar measures deviations from homogenous linear shear and varies from 0, for a perfectly linear velocity profile with $v(y) = \hat{\gamma}y$, to 1, for a plug-like profile with velocity $v(y) = V_p$. Φ is evaluated using the following equation:

$$\Phi = \frac{1}{\hat{\gamma}H^2/4} \int_0^H \left| [v(y) - \hat{\gamma}y] - \left[\int_0^H v(y)dy - \hat{\gamma}H/2 \right] \right| dy. \quad (3)$$

A single value of Φ can be determined for each frame of video, so measured values of Φ corresponding to each frame of video are plotted for the first 10 seconds of the experiment. Subsequently, values of Φ which have been averaged over 10 seconds of video are plotted at 30 second intervals (and the time axis on the figure is expanded in this region). The material in the slurry state shows constant values of $\Phi \leq 0.25$ over the entire 300 second duration of the test. Measurements of $\Phi = 0$ are difficult to obtain for wax-oil fluids below T_{wa} , due to some residual wall slip, and due to the turbidity of the fluid. This turbidity introduces errors in the velocity measurements that always positively contribute towards Φ . However this behavior can still be compared to the behavior of the material in

the strong gel state. In the strong gel state, $\Phi \simeq 0.7$ initially, then subsequently decreases. This process has been observed and documented previously in these fluids⁴⁷ and is the result of erosion³⁷ whereby the wax crystal structure breaks down into smaller aggregates and the gel weakens.

The measurements of $\hat{\sigma}$ and Φ in Fig. 4 show that the strong gel response to an imposed shear rate is dominated by localized failure events at the wall. This is followed by long transients in the evolution of the heterogenous microstructure. These circumstances are different from the uniform distribution of stress and shear rate typically assumed for a fluid being deformed in a cone and plate rheometer. In order to avoid the impact that these complicated yielding scenarios have on interpreting bulk rheological data, we choose to utilize the slurry preparation protocol for all experiments that follow. As is seen in Fig. 4 (a), the 5% wax-oil system in its slurry state exhibits significantly less wall slip. It also does not exhibit a prolonged decay in the stress signal due to fluctuating stick-slip events and erosion of the microstructure. Some deviations of the velocity profile from the linear form for values of $y/H < 0.4$ are observed - these are due to the turbidity of the material decreasing the precision of the velocity measurements deeper into the fluid (and consequently the error bars are much larger for these values of $y/H < 0.4$). Bulk rheological data for material prepared in this slurry state is more congruent with a continuum mechanics constitutive modeling framework (especially when roughened surfaces are used to eliminate residual wall slip).

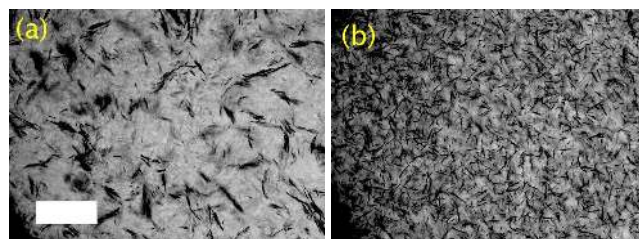


Fig. 5 Bright field microscopy images of the 5% wax-oil system in (a) the slurry state and (b) the strong gel state. The white scale bar is 200 μm , both images are taken at 25°C under quiescent conditions (and at the same magnification).

Fig. 5 graphically illustrates the difference between the “strong gel” and “slurry” states. The figure contains two bright-field microscopy images of the wax crystal microstructure for a 5% wax-oil mixture at 25°C in its slurry state (a), and in the strong gel state (b). The wax crystals appear as dark particles in a light background. These crystals are discotic, but appear needle-like when viewed edge-on in the two-dimensional plane. The wax network formed in the slurry state is looser with more vacant (light gray) regions where no precipitates are present. The strong gel state consists of fewer va-

cant regions with a more closely packed network of wax precipitates. The wax crystals in the strong gel are non-Brownian in character, and form a sample-spanning jammed structure. However in the slurry the discrete crystals (with typical sizes 10-50 μm) can be aligned by the shearing flow. This results in strong shear thinning in the apparent viscosity observed in the steady-state flow curve (see Fig. 6 below).

3 Experimental Results and Discussion

3.1 Rheology of Wax-Oil system in slurry state

We propose three different rheometric tests as canonical flows to probe the material response of the wax-oil mixture, and provide a set of data for fitting to a constitutive model. In what follows, we describe these three different test protocols, and discuss implications of the experimental results for constitutive modeling.

3.2 Steady state flowcurve.

For thixotropic systems, steady state flow curves (that is, plots of viscosity vs. shear rate, or shear stress vs. shear rate) are difficult to obtain⁵. The measured viscosity will depend on the duration of the experiment, due to the thixotropic transients exhibited by the material. However, flowcurves are commonly used in fitting of constitutive models to thixotropic yielding materials.^{31,56} Souza Mendes and Thompson⁵⁷ argue that the steady state flowcurve describes the equilibrium locus of the dynamic thixotropic system. For constitutive models which incorporate an evolving internal structural parameter (commonly denoted generically as $\lambda(t)$ ⁵), this implies that the steady state flowcurve can be fit to the constitutive model predictions for the special case when $\dot{\lambda} = 0$. This significantly simplifies the fitting procedure.

In Fig. 6 we plot the measured flowcurves for the heavy mineral oil, and the 5% and 10% wax-oil systems in their slurry state ($T = 27^\circ\text{C}$). These measured flowcurves are obtained by using the AR-G2 in its standard configuration. The measurements are carried out by shearing at a given globally averaged rate $\dot{\gamma}$, and are determined to have reached a steady state by using a “steady state sensing” option on the rheometer. Using this option we measure the temporally averaged torque \mathcal{T} over successive 30 second periods, and determine that the measurement has reached a steady state when three successive sampling periods are within 5% of the same value. Each measurement point usually requires 5 minutes to reach a steady state, and the measurement of the entire flow curve requires 2-3 hours.

Several key features can be identified from the flowcurves shown in Fig. 6. First, both the 5% and 10% model fluids exhibit Newtonian-like behavior at high shear rates, with the

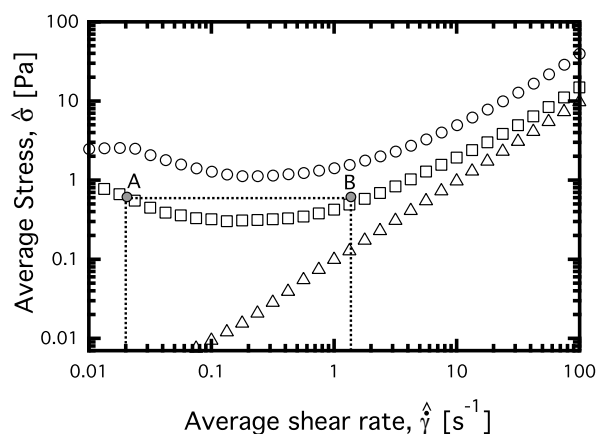


Fig. 6 Measured flow-curves of the various systems used in this study using the standard configuration of the AR-G2 rheometer. (Δ) Heavy mineral oil, (\circ) 10% wax in oil, and (\square) 5% wax in oil. Points A and B correspond to the shear rates imposed in Fig. 7.

average stress $\hat{\sigma}$ being linearly proportional to average shear rate $\dot{\gamma}$. Second, the 10% system has a larger steady state viscosity than the 5% system, due to the higher volume fraction of solid precipitates. Third, the flowcurves of the model crude oils exhibit a non-monotonicity, i.e. there is a region at lower applied shear rates ($\dot{\gamma} \leq 0.1 \text{ s}^{-1}$) where the average stress decreases as the shear rate is increased.

Non-monotonic flowcurves (NMFC's) point towards the presence of a material instability.⁵⁸⁻⁶¹ Some shear banding fluids, for example wormlike micellar solutions, exhibit an *underlying* non-monotonic flowcurve.⁶² This non-monotonic flowcurve cannot be measured, because at imposed shear rates in the decreasing region of the flowcurve, the material bifurcates into two⁶³ or more⁶⁴ coexisting regions with different local shear rates. We refer to this as a “standard shear banding scenario”⁶¹.

There are several examples in the literature of *measured* NMFC's. Dijkstra et al.⁶⁵ measured NMFC's in granular media in a number of different geometries, while Michel et al.⁶⁶ measured non-monotonic flowcurves in microemulsions of oil in water which form transient networks. In the latter, the authors observe “wavy deformations of the sample surface” and “progressive cavitation-like proliferation of bubbles in the bulk”. These manifestations are indicative of an unstable flow within the material, even though the imposed deformation is steady. This differs from the standard shear banding scenario envisioned for wormlike micellar solutions, in which a steady (banded) velocity field is established in the material. The underlying non-monotonic constitutive curve is then manifested as a stress plateau with an approximately constant value of the average stress $\hat{\sigma}$ ⁶¹.

For our model crude oil, the data shown in Fig. 6 indicates

that a NMFC of $\hat{\sigma}$ vs. $\hat{\gamma}$ is measurable. We therefore emphasize that the results shown in Fig. 6 correspond to temporally converged values of average stress $\hat{\sigma}$ in the material at an imposed global shear rate $\hat{\gamma}$. However, as pointed out by Michel et al.⁶⁶, substantial temporal and spatial fluctuations in microstructure and local stress must persist.

3.2.1 Rheo-PIV in the non-monotonic region of the flowcurve. The AR-G2 in its Rheo-PIV configuration was used to provide experimental evidence for a material instability associated with the NMFC. The 5% wax-oil system in its slurry state at a temperature of $T = 27^\circ\text{C}$ was utilized for this (higher wax content systems are too turbid to provide discriminating velocimetric data). The particular protocol that is used is as follows: first; preshearing the material at $\hat{\gamma} = 50 \text{ s}^{-1}$ for 5 minutes. Then, a sequence of three steps in shear rate is imposed. The first step is to $\hat{\gamma} = 0.02 \text{ s}^{-1}$ (at a time denoted as $t = 0 \text{ s}$), followed by a step to $\hat{\gamma} = 1.2 \text{ s}^{-1}$ at $t = 1432 \text{ s}$, and finally a step back to $\hat{\gamma} = 0.02 \text{ s}^{-1}$ at $t = 3232 \text{ s}$. The measured stress and velocity profiles for this test are shown in Fig. 7.

From Fig. 7 (a) it is apparent that the rheometer imposes an apparent shear rate in the two cases which differs by a factor of 60, however the steady state value of the average stress $\hat{\sigma}$ is roughly equal (within $\pm 12\%$) for both values of $\hat{\gamma}$. This is indicative of the extreme shear thinning exhibited by the model waxy crude oil, and is consistent with the non-monotonicity in the measured flowcurve of Fig. 6. Transient responses are also exhibited in the response of the material to the steps in shear rate. At $t = 1432 \text{ s}$, when the shear rate is stepped to $\hat{\gamma} = 1.2 \text{ s}^{-1}$, an instantaneous increase in the stress occurs, followed by a subsequent decrease with the stress reaching a minimum at approximately $t = 1452 \text{ s}$. Then, there is a gradual increase (from $t = 1452 - 2800 \text{ s}$) in the stress towards a steady value of $\hat{\sigma} = 0.71 \pm 0.01 \text{ Pa}$. At $t = 3232 \text{ s}$, when the shear rate is suddenly dropped back to $\hat{\gamma} = 0.02 \text{ s}^{-1}$, the stress instantaneously decreases, followed by a subsequent increase in the stress reaching a maximum (and steady value) at $t = 3280 \text{ s}$.

These long transient responses are consistent with a thixotropic material undergoing cycles of structuring and de-structuring⁶⁷. In particular, from $t = 1432 \text{ s}$ to $t = 1452 \text{ s}$, the material evolves from a structured state (due to the low value of the shear rate imposed for $t \leq 1432 \text{ s}$) to a de-structured state. The high shear rate after the jump results in a sudden increase in the stress, which subsequently breaks the wax structure. The structure breaks down completely and the stress reaches a minimum at $t = 1452 \text{ s}$. From $t = 3232 \text{ s}$ to $t = 3280 \text{ s}$ when the shear rate is decreased, the material starts from a de-structured state due to the high value of the shear rate imposed previously. A smaller stress is required to drive the flow, but this stress progressively increases due to a build up in the structure at the lower imposed shear rates. From $t = 1452 \text{ s}$ to $t = 2800 \text{ s}$ we also observe the additional effect of a long-time

structuring which results in an increase in the measured or apparent viscosity within the fluid $\hat{\eta}(t) \equiv \hat{\sigma}(t)/\hat{\gamma}$. This presence of multiple timescales for restructuring of the fluid is to be expected. Fig. 5 (a) indicates that for the material in the slurry state, there is a distribution of characteristic sizes of the wax precipitates and aggregates. The characteristic rotary diffusion time for rearrangement of the discotic microstructure is a strong function of the size of these crystals and aggregates⁵. The evolution of the bulk fluid rheology should therefore reflect this distribution of timescales.

The measurements of $\hat{\sigma}$ in Fig. 7 (a) provide clear evidence that the model waxy crude oil is highly thixotropic. The larger temporal fluctuations in the average stress $\hat{\sigma}(t)$ at lower shear rates is also notable. However, Fig. 7 (a) provides no indication whether the flow field within the material is heterogenous or shear-banded. Rheo-PIV evidence supporting a material instability is given in Figs. 7 (b) and (c). In these two sub-figures we contrast the measured velocity field within the fluid as two different values of $\hat{\gamma}$ are imposed. At the lower imposed shear rate of $\hat{\gamma} = 0.02 \text{ s}^{-1}$, we observe stochastic fluctuations in the average shear rate across the gap, in the slip velocity at the upper plate, and in the general form of the velocity profile. From $t = 0 - 100 \text{ s}$, the velocity profile indicates a region of higher shear rate near the center of the gap. This is reminiscent of the 3-banded velocity profiles which have been observed in wormlike micellar solutions under imposed steady shear in cone-plate geometries.^{50,64,68} However, this structure in the velocity profile is ephemeral. The velocity profiles at later times (e.g. $t = 1150 \text{ s}$ and $t = 1300 \text{ s}$ plotted in Fig. 7 (b) (ii)) show a more uniform shear rate across the gap with larger slip velocities at the upper and lower plates. The velocity profile plotted for $t = 1300 \text{ s}$ is nearly plug-like ($\Phi = 0.73$) with scaled slip velocities of $(1 - v(y)/V_w) = 0.48$ at the upper surface and $(v(y)/V_w) = 0.28$ at the lower surface.

We quantify these fluctuations by considering a Reynolds decomposition of the velocity field $v(y, t)$ such that:

$$v(y, t) = \bar{v}(y) + v'(y, t), \quad (4)$$

where $\bar{v}(y)$ is the average part of the velocity defined as follows:

$$\bar{v}(y) \equiv \frac{1}{t_2 - t_1} \int_{t_1}^{t_2} v(y, t) dt \quad (5)$$

and $v'(y, t)$ is the fluctuating part of the velocity. We define a temporally and spatially averaged dimensionless shear rate measured across the gap as follows:

$$\langle \hat{\gamma} \rangle \equiv \frac{1}{\hat{\gamma} H (t_2 - t_1)} \int_{t_1}^{t_2} \int_0^H \frac{dv(y, t)}{dy} dy dt = \frac{\bar{v}(H) - \bar{v}(0)}{V_w}, \quad (6)$$

where $\bar{v}(H)$ and $\bar{v}(0)$ are the temporally-averaged velocities of the upper and lower walls. To quantify the effect that the

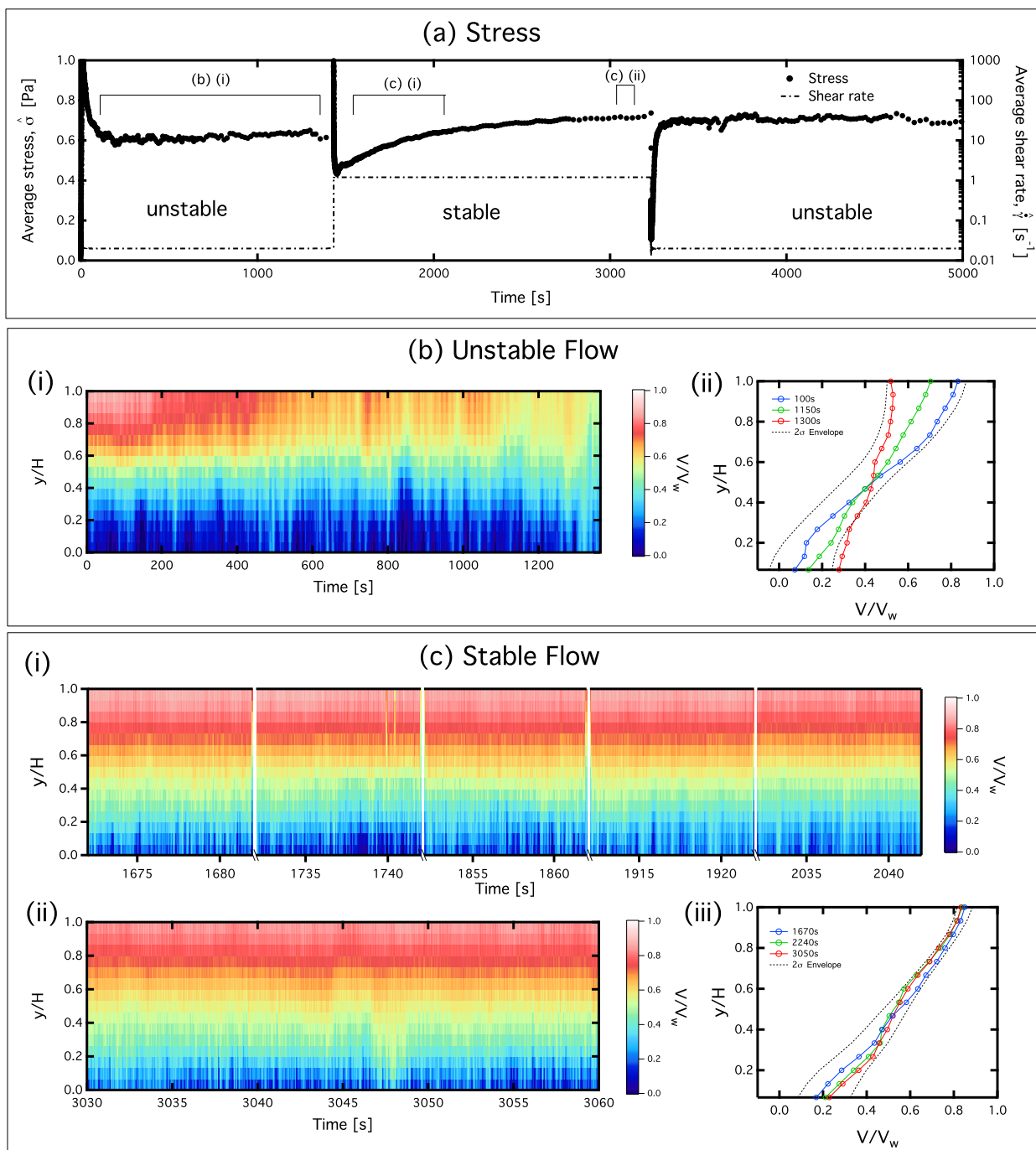


Fig. 7 Switching between the stable ($\hat{\gamma} = 1.2 \text{ s}^{-1}$) and unstable ($\hat{\gamma} = 0.02 \text{ s}^{-1}$) regions of the flowcurve in Fig. 6 (5% wax-oil mixture). The steady (averaged) measured stress values are the same for the two different shear rates, however in the unstable region (b), substantially enhanced fluctuations are observed in the velocity profile, as indicated by the 2σ (standard deviation) envelope of the profiles. Within the stable region, velocity profiles are sampled at several 10 second intervals (c) (i), and then for a longer 30 second interval (c) (ii) beginning at $t = 3030 \text{ s}$. Fluctuations in the instantaneous shear rate across the gap are more than a factor of two lower in this stable region. Measurements are carried out using the RheoPIV configuration of the AR-G2 (smooth cone-plate geometry)

fluctuating part of the velocity $v'(y)$ has on the shear rate, we define a standard deviation of the shear rate as follows:

$$\Sigma_{\dot{\gamma}} \equiv \sqrt{\frac{1}{t_2 - t_1} \int_{t_1}^{t_2} \left(\langle \dot{\gamma} \rangle - \frac{v(H) - v(0)}{V_w} \right)^2 dt} \quad (7)$$

$$= \sqrt{\frac{1}{t_2 - t_1} \int_{t_1}^{t_2} \left(\frac{v'(H) - v'(0)}{V_w} \right)^2 dt}. \quad (8)$$

For the velocity data in Fig. 7 (b), the average shear rate measured across the gap is $\langle \dot{\gamma} \rangle \pm 2\Sigma_{\dot{\gamma}}$, where the \pm represents the 95% confidence bound in this average over time, and is indicative of the extent of the fluctuations in the local shear rate $\dot{\gamma}$ over time. For Fig. 7 (b), we compute $\langle \dot{\gamma} \rangle = 0.59$ and $\Sigma_{\dot{\gamma}} = 0.13$.

In Fig. 7 (c), we show measured profiles for the case when $\hat{\gamma} = 1.2 \text{ s}^{-1}$. At this higher shear rate, images are acquired at a higher frame rate due to the increased velocity of the tracer particles. Due to limited digital storage space, sampling of the velocity field is limited to several smaller intervals in time. The velocity field is therefore sampled for 5 different 10 second intervals from $t = 1670 \text{ s}$ to $t = 2040 \text{ s}$, which coincides with the region of increasing measured stress. The velocity is also sampled for 30 seconds at $t = 3030 \text{ s}$, where the spatially averaged stress $\hat{\sigma}$ has approached and remains at a constant value. In these regions, the average shear rate across the gap fluctuates considerably less, with $\langle \dot{\gamma} \rangle = 0.66$ and $\Sigma_{\dot{\gamma}} = 0.068$. The 95% confidence bounds for the velocity profiles have been reduced by a factor of 2 compared to the lower shear rate. The velocity field also appears linear for all times, with some wall slip still occurring at both the upper ($(1 - \bar{v}(H)/V_w) = 0.14$) and lower ($(\bar{v}(0)/V_w) = 0.21$) surfaces. The fluctuations in shear rate and slip velocity that are observed in Fig. 7 (b) are therefore markedly reduced when compared to Fig. 7 (b).

Fig. 7 (b) (ii) and (c) (ii) also include envelopes which represent the magnitude of the fluctuations in the velocity $v'(y)$. These envelopes are defined as $\bar{v}(y) \pm 2\Sigma_v(y)$, where $\Sigma_v(y)$ is the standard deviation of the velocity as a function of position across the gap, and is defined as follows:

$$\Sigma_v(y) \equiv \sqrt{\frac{1}{t_2 - t_1} \int_{t_1}^{t_2} (v'(y))^2 dt}. \quad (9)$$

We find that $\Sigma_v(y)|_{\hat{\gamma}=1.2} < \Sigma_v(y)|_{\hat{\gamma}=0.02}$ for all values of y , indicating that there are more fluctuations in the velocity when the applied shear rate is $\hat{\gamma} = 0.02 \text{ s}^{-1}$. The difference in the magnitude of these fluctuations is highest near the upper surface ($y = H$), where fluctuations are 4.8 times larger for the case when $\hat{\gamma} = 0.02 \text{ s}^{-1}$. Incidentally, at $y = H$ the velocity measurements are most accurate due to diminished effects of sample turbidity. The RheoPIV data and associated statistical

analysis presented in Fig 7 provides strong evidence of spatiotemporal fluctuations in the velocity field associated with a material instability in the wax-oil mixture. This unstable flow is most pronounced at low shear rates (which lie in the decreasing region of the NMFC).

3.2.2 Stress overshoots - Startup of steady shear.

The second rheometric test that we utilize to characterize thixotropy is the measurement of overshoots in the average stress $\hat{\sigma}$ under startup of steady shear. These tests probe the effect of the ‘‘aging time’’ that elapses between sample preparation, and imposing the step in shear rate. The initial sample preparation is typically carried out by shearing (or rejuvenating) the material at a high and constant deformation rate (well within the stable region of the flowcurves shown in Fig. 6) for an extended period of time. Then, during the period of aging, the sample is left unperturbed in the rheometer so that the material microstructure starts to build up. When the step in shear rate is subsequently imposed, the gelled and structured material will go through a yielding transition which depends on the initial structure, which in turn depends on the aging time. These tests have been used previously to quantify the effect that internal microstructure has on the rheology of a thixotropic system, and to quantify the characteristic time scales which may be associated with the formation of this structure⁶⁹.

The tests presented here are carried out on the 10% model waxy crude oil prepared to its slurry state at a temperature of 27°C. The AR-G2 in its standard configuration is used, which utilizes roughened cone-plate surfaces to eliminate wall slip. We adopt the nomenclature of Fielding et al.⁷⁰ and denote the aging/waiting time as t_w . After the sample is prepared, an initial waiting time of $t_w = 2 \text{ s}$ is applied, and then a step in shear rate to $\hat{\gamma} = 2 \text{ s}^{-1}$ is imposed for 10 minutes. Following this step, the material is left unperturbed for a waiting time $t_w = 5 \text{ s}$, and an applied steady shear rate of $\hat{\gamma} = 2 \text{ s}^{-1}$ is imposed for 10 minutes. In total, seven startup tests of steady shear are imposed successively, with the waiting time between these steps being incremented in a logarithmic fashion up to a maximum value of $t_w = 200 \text{ s}$. For each value of t_w , measurements of the stress $\hat{\sigma}$ are obtained for the 10 minute step in shear rate. For consistency, the measurements of stress and strain rate in this section will be indicated as averages ($\hat{\sigma}$ and $\hat{\dot{\gamma}}$). However, the average strain rate $\hat{\dot{\gamma}}$ here is high enough, and wall slip is suppressed by the roughened geometry, so deviations of the average values from the local shear rate $\dot{\gamma}$ and local stress σ will be small.

In Fig. 8 we plot the measured response of the average stress $\hat{\sigma}$ as a function of the imposed strain $\hat{\gamma}$, for seven different values of t_w . An overshoot is seen at applied deformations of approximately $\hat{\gamma} = \hat{\dot{\gamma}}\Delta t \simeq 0.3$ dimensionless strain units. The magnitude of this overshoot increases with t_w , however it ap-

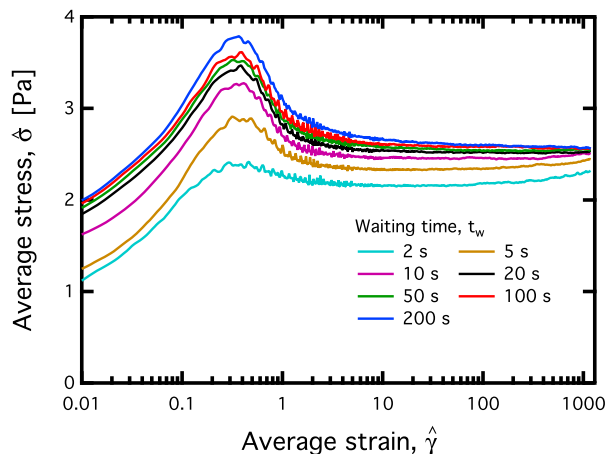


Fig. 8 Stress overshoots for different waiting times t_w in the 10% model waxy crude oil system. Fluid is prepared to its slurry state at 27° C. The applied shear rate is $\dot{\gamma} = 2 \text{ s}^{-1}$.

appears to saturate for $t_w \geq 20 \text{ s}$. The overshoot is clearly the result of structuring within the fluid that occurs over the course of the aging time t_w . There is also a gradual monotonic increase in the long time steady state value of $\hat{\sigma}$ which occurs over much longer time scales, and over multiple steps in the shear rate. This slower increase in $\hat{\sigma}$ is a manifestation of the same slow aging process that is observed in Fig. 7 (a) - even at a (stable) applied shear rate of 1.2 s^{-1} it takes a long time (on the order of tens of minutes) for the value of $\hat{\sigma}(t)$ (and hence $\hat{\eta}(t)$) to stabilize. This slow structuring occurs on time constants that are much larger than the waiting time of $t_w = 20 \text{ s}$ which is approximately required for the peak stress to saturate. This is additional experimental evidence of a distribution of processes and time scales associated with the internal material structuring.

Our constitutive model will primarily focus on predicting the transient yield peak in the stress $\hat{\sigma}(t)$ at intermediate strains $\hat{\gamma} \simeq 0.3$. This is frequently of greater relevance to flow assurance than the very long time response of the material stress. These initial yield peaks observed in Fig. 8 would be responsible for relatively large additional pressure drops being required to restart a pipeline where flow has ceased for a short period of time. Several other constitutive models have had success in predicting these types of overshoots (e.g. see the SGR model¹³, or the thixo-elastic Maxwell model¹⁵, among any others). In the present work, we develop a model capable of predicting these overshoots by incorporating mechanisms from plasticity theory. The model will quantitatively predict these stress overshoots, as well as several other key experimental observations. Although lacking the more detailed microstructural physics interpretation of some other models^{13,14,18}, the model introduced here will be

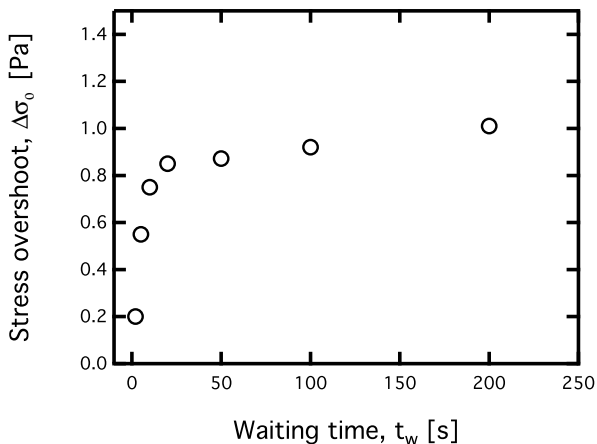


Fig. 9 Thixotropic evolution in the stress overshoot $\Delta\sigma_0$ as a function of waiting time t_w extracted from the startup experiments presented in Fig. 8.

written in terms of a set of evolution equations in macroscopic variables, rather than in integral form. This differential form is more suitable for implementation in common Eulerian flow solvers. Furthermore, the mechanisms utilized in this model are rooted in a robust continuum mechanics framework, so the model can also be generalized to tensorial form in a straightforward manner (see the table in the supplemental information).

To quantify the magnitude of the yield peak, which will in turn assist in the fitting of the constitutive model, we define our stress overshoot $\Delta\sigma_0$ as the difference between the peak stress during each test and the measured stress 10 seconds (i.e. 20 strain units) after the step in shear rate is imposed. At this level of imposed strain it is clear that the initial transients associated with the thixotropic yield peak have died out. The measured value of $\Delta\sigma_0$ is plotted as a function of t_w in Fig. 9. In this figure, the magnitude of the yield peak saturates with $\Delta\sigma_0$ approaching a value close to 1 Pa, or approximately 40 % of the final flow stress. Some further increases at longer times (between 100-200 s) are also evident, and these smaller increases are evidence of the same long time restructuring behavior that was discussed in Sec. 3.2.1.

3.2.3 Large Amplitude Oscillatory Shear. The third rheometric test utilized here to probe the time-varying nonlinear constitutive response of the material is large amplitude oscillatory shear (LAOS). LAOS is generally carried out by imposing an oscillatory deformation on the material of the following form:

$$\gamma(t) = \gamma_0 \sin \omega t . \quad (10)$$

For the measurements presented here an oscillatory *aver-*

age strain will be imposed on the material, $\hat{\gamma} = \gamma_0 \sin \omega t$. Even though we suppress wall slip, we will utilize the averaged quantities $\hat{\sigma}$, $\hat{\gamma}$ and $\hat{\dot{\gamma}}$ to represent the measured rheological data. This is to account for the possibility of small fluctuations in the local variables σ , γ and $\dot{\gamma}$.

Two independent test parameters can be modified in LAOS; the oscillation frequency ω and the strain amplitude γ_0 . When the strain amplitude is small enough, the stress in the material $\sigma(t)$ is linear in strain and can be decomposed into in phase and out of phase components as follows:

$$\sigma(t) = \gamma_0 \{ G'(\omega) \sin \omega t + G''(\omega) \cos \omega t \}, \quad (11)$$

where the storage and loss moduli G' and G'' are both functions of the frequency ω . When strains are large, most materials exhibit a nonlinear response with a periodic stress that can be expressed in terms of a Fourier series as follows:

$$\sigma(t; \gamma_0, \omega) = \sum_{n \text{ odd}} \gamma_0 \{ G'_n(\omega, \gamma_0) \sin n\omega t + G''_n(\omega, \gamma_0) \cos n\omega t \}, \quad (12)$$

where $G'_n(\omega, \gamma_0)$ and $G''_n(\omega, \gamma_0)$ are higher harmonic moduli that now depend on both the frequency of oscillation and the strain amplitude. This approach, using Fourier transform rheology,⁷¹ is the basis for many techniques which analyze the response of a material to LAOS deformations⁷². We do not analyze our LAOS data using the Fourier transform representation, because this decomposition can only be applied to periodic stress waveforms. Because of the thixotropic nature of the model crude oil, the material response to a sinusoidal shearing deformation will contain prolonged stress transients due to the aging and shear rejuvenation of the fluid that can occur over multiple periods of oscillation. Our goal is to quantify these transients and then develop a constitutive model that predicts them. Any measures based on Fourier transform rheology cannot be applied to these transients. Instead, an instantaneous approach such as that introduced by Rogers⁷³ would be required.

The LAOS strain measurements presented here will be used primarily as a fitting tool in order to guide the development of a suitable elasto-viscoplastic model, and then to compare the model response to the response of the real fluid. One benefit of using LAOS tests to fit constitutive models is that several key aspects of the rheological behavior of the fluid are revealed under LAOS forcing. At low values of γ_0 , the linear viscoelastic behavior of the fluid is probed. Larger values of γ_0 can then probe the plastic yielding transition of the test material. It is also possible to observe transients in the LAOS response which result from the thixotropic behavior of these fluids. These transients are represented clearly in the Lissajous curves as decays towards a periodic attractor. Hence, if a constitutive model can predict the response of a material to LAOS,

then it is likely to predict other time- and strain-varying responses that occur over a wide range of deformations.

Several researchers have used cyclic stress-strain loading curves, or Lissajous-Bowditch curves, as signatures that are used to fit material responses to a constitutive model.^{17,46,74} We represent the response of our model crude oil to LAOS through the use of these Lissajous-Bowditch curves (with strain as the abscissa and stress as the ordinate). A series of these curves can be plotted for a number of different strain amplitudes γ_0 and frequencies ω . We carry out a series of LAOS tests on the 10% model crude oil fluid in its slurry state at a temperature of 27°C. These measurements are done on the ARES rheometer, with a roughened cone-plate geometry configuration. A series of measurements at progressively larger strain amplitudes γ_0 and at a single fixed frequency of $\omega = 1$ rad/s is shown in Fig. 10. Between each measurement, a waiting time of $t_w = 100$ s is applied so that the structure associated with the transient yield peaks shown in Fig. 8 has enough time to build up. For each measurement at a given strain amplitude, four complete oscillation periods are applied.

In Fig. 10 (b) we represent the Lissajous curves as 3D trajectories with the measured stress $\hat{\sigma}$ plotted against the sinusoidally varying strain $\hat{\gamma}$, and the strain rate $\hat{\dot{\gamma}}$ which varies in quadrature. We are primarily interested in the stress-strain projection of these 3D curves, as shown in Fig. 10 (a), because this reveals the elastoviscoplastic character of the material response. The curves in Fig. 10 (a) and (b) are only shown for their stable limit cycle or “alternance state”⁷⁵. This alternance state is reached after multiple cycles of oscillation. In Fig. 10 (c), we illustrate the transients which occur before reaching the alternance state by plotting these Lissajous curves on independent (rescaled) axes for each strain amplitude γ_0 . The magnitude of the maximum stress σ_m and strain at each strain amplitude is shown by each figure. In Fig. 10 (c), overshoots and prolonged transients are clearly evident in the response of the material.

From Fig. 10 (c) we can see that at low values of γ_0 the material response is that of a linear viscoelastic solid, with $G' > G''$. This can be distinguished from the elliptical shape of the loading curve, which implies a linear response. As γ_0 is progressively increased, the maximum stress σ_m also increases. However σ_m then saturates at moderate strain amplitudes, a behavior typically associated with a yield-like response. For moderate strain amplitudes between 5% and 50% the characteristic shape of the cyclic loading curves changes and indicates yielding. At these values of γ_0 the material undergoes a sequence of processes which involve elastic loading, followed by saturation of the stress and subsequent viscoplastic flow, before elastically unloading when the direction of straining is reversed. This sequence of events occurs within each cycle (i.e. it occurs on an intra-cycle basis), and is responsible for the transition from elliptical to rhomboidal

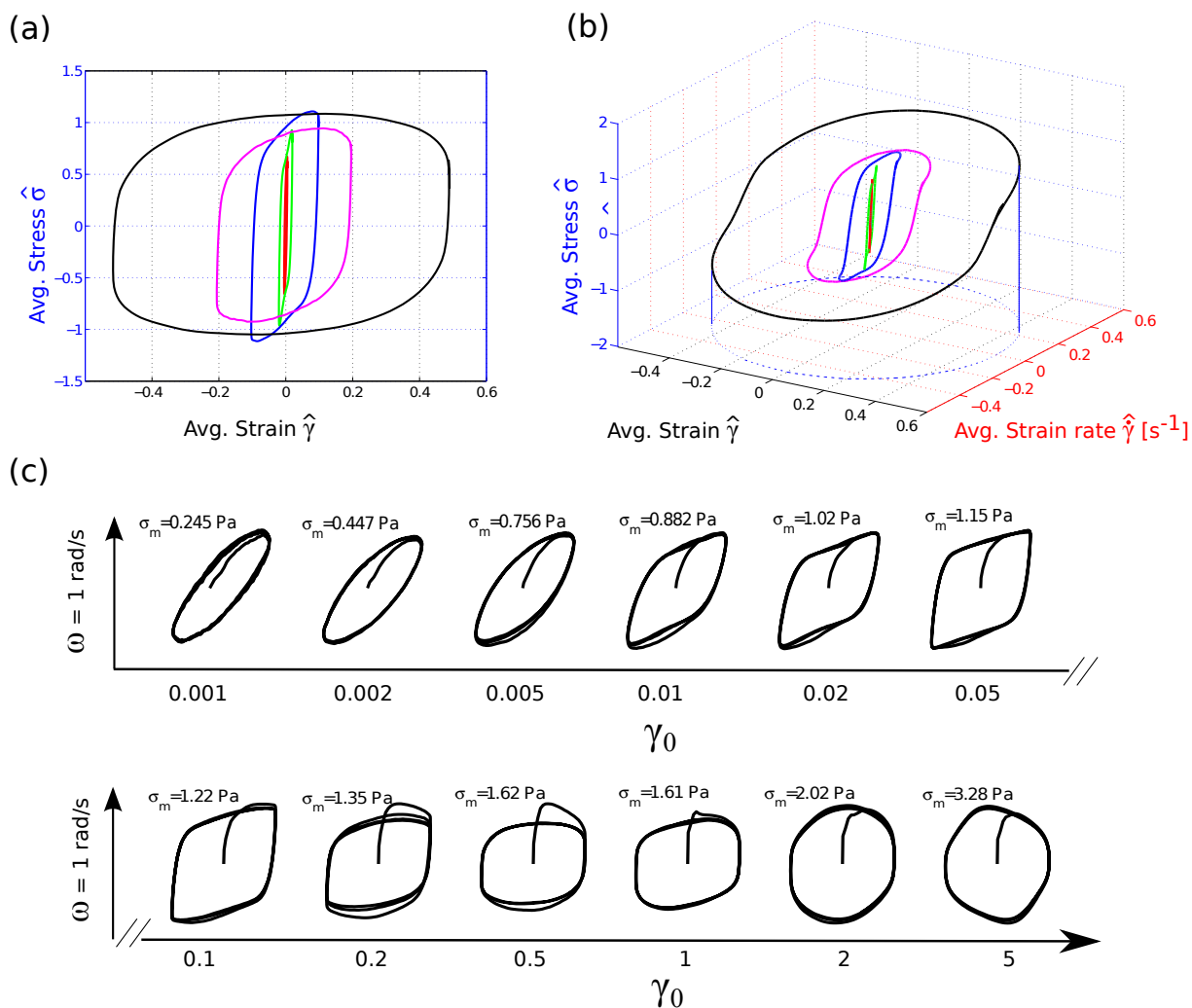


Fig. 10 Lissajous figures showing LAOS tests on the 10% model crude oil in its slurry state at 27°C. The tests are carried out at a frequency of $\omega = 1$ rad/s, with increasing strain amplitude γ_0 . Waiting time between successive tests is held constant at $t_w = 100$ s. The full 3D trajectory of the periodic alternance state is shown in (b), with the 2D stress-strain projection in (a). In (c) the evolution in the shape of the cyclic loading curves and the transients associated with the startup of oscillatory shear flow are shown for a large range of increasing γ_0 .

shaped loading curves^{76,77}.

There is additional valuable information contained in the material's inter-cycle response, i.e. in the prolonged transients exhibited, especially for intermediate strain amplitudes of $20\% \leq \gamma_0 \leq 100\%$. These transients are manifested in the form of an initial stress overshoot which occurs as the material is first strained. This stress overshoot is evidence of the same transient yield peak that was documented in Sec. 3.2.2 for the startup of steady experiments. Several cycles are required (spanning a time period on the order of 10 seconds) for the stress to settle into its steady alternance state.

Several key features of Fig. 10 can be used to guide the development of our constitutive model (the detailed formulation of which will be given in Sec. 4). First, there is no observable inter-cycle change in the linear viscoelastic behavior between each cycle of loading. This implies that G' and G'' remain constant with time for the material. If both G' and G'' are to be non-constant functions of some microstructure parameter λ , which in turn depends on t_w , then deformations in the linear regime cannot cause a change in the microstructural parameter λ . This will be accounted for by specifying a *plastic strain* as being responsible for changing the structure parameter λ , and this plastic strain is only allowed to accumulate when the material yields at larger stresses and strains. Thus, a central component of our modeling approach will be to additively decompose the total strain into plastic and viscoelastic contributions, with plastic strain only accumulating when the shear stress in the sample exceeds some critical value. As a mechanical analog representation, this model can be visualized as a viscoelastic element in series with a nonlinear plastic yielding element. The yielding element will then utilize two important concepts from plasticity theory – isotropic hardening and kinematic hardening – in order to capture both the nonlinear intra-cycle behavior of the material, as well as the transient inter-cycle behavior (i.e. stress overshoots) which is exhibited under LAOS.

4 Constitutive Model

4.1 Formulation of the Isotropic-Kinematic Hardening Model (IKH Model)

In this section we outline the development of a constitutive model that quantitatively predicts the salient features of the model crude oil's rheological response. As noted above, a central component of our approach is to additively decompose the total shear strain in our material into linear viscoelastic (γ^{ve}) and plastic (γ^p) components, such that

$$\gamma = \gamma^{ve} + \gamma^p . \quad (13)$$

Irreversible plastic strain accumulates in the material when the applied stress is above a certain critical value, so for low

stresses $\gamma = \gamma^{ve}$ and the response of the material is linear and viscoelastic. This decomposition differs slightly from classical descriptions of viscoplasticity, where strain is additively decomposed into plastic and purely elastic components. Here we rename our elastic strain a viscoelastic strain in order to account for some linear viscoelastic effects that are present in our material below the yielding point. This linear viscoelastic response can be specified further by decomposing the viscoelastic strain γ^{ve} into elastic and viscous components, such that $\gamma^{ve} = \gamma^v + \gamma^e$. This would correspond to specifying a Maxwell-like linear viscoelastic behavior below the yield stress, with $\gamma^e = \sigma/G$ and $\dot{\gamma}^v = \sigma/\eta$. Alternatively, a Kelvin-Voigt viscoelastic behavior can be specified. In fact any LVE-type behavior can be specified within this general constitutive framework, depending on the characteristics of the soft gel and the desired fidelity of the model prediction. We show three canonical forms in Fig. 11 in the form of corresponding mechanical analog elements. Because the flows of interest are nonlinear, we will predominantly focus on prescribing the correct behavior of the nonlinear yielding element that is characterized by the plastic strain γ^p . As a result, we will not discuss fitting of linear viscoelastic behavior in detail. Interested readers can consult any of the classical textbooks on linear viscoelasticity^{78–80} and replace the simple linear viscoelastic elements shown in Fig. 11 with the elements of their choice (and this will not significantly affect the large strain nonlinear behavior).

For most of the calculations below, the simplest canonical form of LVE behavior is considered, i.e. a linear Maxwell-like behavior as shown in Fig. 11 (a) with elastic modulus G and damping η . Incidentally, this MIKH form of the model is compatible with the classical description of yielding materials with $\gamma = \gamma^e + \gamma^p$, since the plastic strain can be redefined to include the linear damping element with viscosity η . In addition to this, two assumptions are made about the nature of the linear viscoelastic behavior. First, we observed in Sec. 3.2.3 that under small amplitude oscillatory shear, G' and G'' remain constant in time - i.e. imposed deformations in the linear regime do not affect material structure. Therefore, only the plastic accumulated strain γ^p can drive a thixotropic restructuring of the fluid. The second, stronger assumption is based on measurements of G' and G'' as a function of t_w . These measurements show that both G' and G'' are in fact at most *weak* functions of waiting time t_w , with G' only varying by 20% and G'' varying by even less as t_w is changed (see supplementary information). For this data, the LVE parameters G and η are therefore assumed to be constant, and do not vary significantly with changes in material structure. This assumption has been discussed by Quemada¹⁵, and is utilized here to reduce the number of constitutive parameters associated with this model. However, the IKH model will still quantitatively capture the three nonlinear flows discussed in Sec. 3.

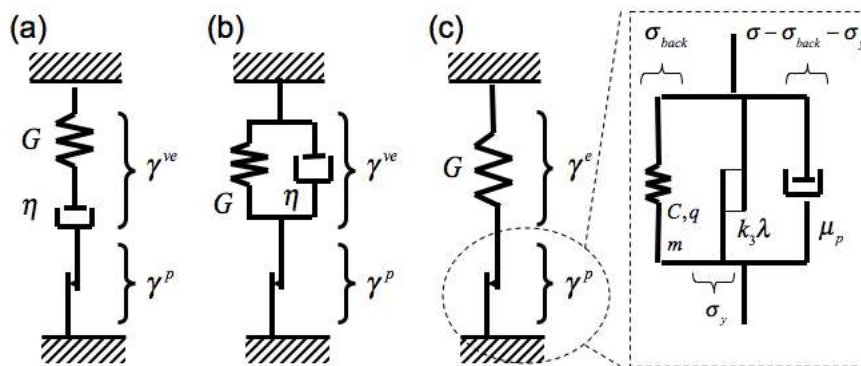


Fig. 11 Three possible forms of the general IKH model. (a) Maxwell IKH model (MIKH) (b) Kelvin IKH model (KIKH) and (c) Elastic IKH model (EIKH). Decomposition of individual contributions to the total stress in the nonlinear element is shown on the far right.

4.1.1 Specifying the plastic strain γ^p . Having discussed the linear viscoelastic behavior, the form of the plastic shear strain γ^p must now be specified. A common first order assumption^{4,6,81} is to prescribe a Bingham-like behavior, in which plastic flow only occurs above a critical stress σ_y :

$$\dot{\gamma}^p = \begin{cases} 0 & \text{if } |\sigma| < \sigma_y \\ n^p \left(\frac{|\sigma| - \sigma_y}{\mu_p} \right) & \text{if } |\sigma| \geq \sigma_y \end{cases}, \quad (14)$$

where $n^p = \sigma/|\sigma|$ is the direction of the applied stress - this is the codirectionality hypothesis⁴², which ensures that plastic deformations always occur in the same direction as the applied stress. The parameter μ_p is the plastic viscosity.

The simple Bingham equation given in Eq. 14 captures some of the basic features of the flowcurve in Fig. 6, however it lacks the ability to predict the transient behavior and nonlinear stress overshoots that were documented in Sec. 3. To predict these transients, the flow rule in Eq. 14 must be modified to account for the constitutive processes of kinematic hardening and isotropic hardening/softening⁴². We have used the concept of kinematic hardening in previous work to model the response of simple (non-thixotropic) yield stress fluids⁴⁶, Kinematic hardening accounts for a movement of the center of the yield surface in stress space. Isotropic hardening, on the other hand, accounts for an expansion or contraction of the yield surface, and is frequently used to model the strengthening of polycrystalline metals under imposed deformations⁴³.

These hardening mechanisms are abundantly used in the plasticity literature, and full three-dimensional versions of models with combined isotropic and kinematic hardening have been developed^{82,83} that are both frame invariant and thermodynamically consistent. For simplicity, we only describe here a one-dimensional version of the model. To capture these two additional microstructural mechanisms, the Bingham equation

given in Eq. 14 is modified as follows:

$$\dot{\gamma}^p = \begin{cases} 0 & \text{if } |\sigma_{\text{eff}}| < \sigma_y(\lambda) \\ n^p \left(\frac{|\sigma_{\text{eff}}| - \sigma_y(\lambda)}{\mu_p} \right) & \text{if } |\sigma_{\text{eff}}| \geq \sigma_y(\lambda) \end{cases}, \quad (15)$$

where the total stress σ has been replaced by the effective stress, σ_{eff} , which is defined as follows:

$$\sigma_{\text{eff}} = \sigma - \sigma_{\text{back}}. \quad (16)$$

Here σ_{back} is the back stress in the material, which effectively tracks the location of the center of the yield surface. The yield surface refers to a surface defined in the three-dimensional “stress space” formed by the principal stress axes. Many different definitions of yield surfaces exist, e.g. von Mises, Tresca. However, we deal with a one-dimensional form of the IKH model, so our stress space consists of a single axis (σ), and our yield surface is thus defined by three points. The first is the back stress, σ_{back} , which is the center of the yield surface, and the other two are the yield limits in the positive and negative directions of stress, $\sigma_{\text{back}} + \sigma_y(\lambda)$ and $\sigma_{\text{back}} - \sigma_y(\lambda)$, respectively. In this model, plastic flow only occurs when the applied stress σ lies outside of the yield surface defined by these three points. The presence of both the back stress and yield stress in the material can be more thoroughly illustrated in Fig. 11 by decomposing the stress σ acting on the nonlinear yielding element into individual stress branches.

In addition to the presence of the back stress in Eqn. 15, the yield stress σ_y is now a function of a single internal structure parameter λ . Furthermore, the direction of plastic strain n^p is now codirectional with the effective stress, so that:

$$n^p = \frac{\sigma_{\text{eff}}}{|\sigma_{\text{eff}}|}. \quad (17)$$

With the formulation in Eqn. 15-17, the center of the yield surface can change through the variation of the back stress σ_{back}

with the imposed plastic strain (*kinematic hardening*) and the yield surface itself can contract/expand through the variation of σ_y with microstructure (*isotropic hardening*). The incorporation of two yield parameters (center of yield surface σ_{back} and size of yield surface σ_y) bears some similarity to the Houska model used by Sestak et al.⁸⁴ and Cawkwell and Charles⁹, in which the yield stress is decomposed into two components (a constant term and a varying component). This model is commonly used to predict the rheology of crude oils, however as an inelastic model, it cannot capture the full behavior of waxy crude oils, especially in large amplitude oscillatory flows.

The variation of the back stress σ_{back} and the yield stress σ_y for a given deformation must be specified. The back stress is related to an internal structural variable A which was utilized in previous work to model ideal (non-thixotropic) yield stress fluids⁴⁶:

$$\sigma_{\text{back}} = CA . \quad (18)$$

The linear relationship between σ_{back} and A results from taking the derivative with respect to A of a quadratic form of a defect energy in the material that accumulates with the plastic strain γ^p ^{46,83,85}. This is analogous to an additional elastic free energy for the defects, so C can be thought of as the back stress modulus, and has units of stress⁸⁵. The internal variable A can be physically interpreted as a dimensionless strain-like variable, or a back strain. The defect energy accumulates because of a rearrangement of the material microstructure, which in our case consists of the interlocking wax crystal network. For three-dimensional versions of constitutive models that include kinematic hardening, the variable A necessarily takes on a tensorial form.⁸³

The back strain A follows an evolution equation that is a more general form of the Armstrong-Frederick equation⁸⁶ discussed by Jiang and Kurath⁸⁷ that can be used to capture the Bauschinger effect⁸⁸,

$$\dot{A} = \dot{\gamma}^p - f(A)|\dot{\gamma}^p| . \quad (19)$$

The Bauschinger effect essentially refers to a decrease in the yield strength of a material upon reversal of the direction of stress⁴². In the above equation, when $f(A) = qA$ (with q a dimensionless material constant) the classical Armstrong-Frederick equation is recovered, which is typically used to describe cyclic loading in metals, but was more recently used to describe the LAOS behavior of soft Carbopol microgels.⁴⁶ To more accurately capture the intra-cycle behavior under LAOS model waxy crude oil over a wide range of imposed strain amplitudes γ_0 , a power law function of $f(A)$ is specified:

$$f(A) = (q|A|)^m \text{sign}(A) , \quad (20)$$

where both m and q are material constants. In the fitting which will follow in Sec. 4.2, Eq. 19 is always evaluated with an initial condition of $A = 0$. This is the approach taken in previous

work - it presupposes that the material is initially in a “virgin state”⁸² with no directional preference for yielding (i.e. a back stress of zero). It also follows from the assumption that the deformation is beginning from a state where the stress and shear rate in the material is zero. Under such conditions, the back stress and back strain typically relax back to their zero values.

When the plastic strain rate $\dot{\gamma}^p$ is zero, the back strain A will initially increase in the direction of the plastic strain γ^p . This results in an increase in the back stress, or a “hardening” of the material in the direction of flow. However, the back strain A eventually saturates due to the second term in Eq. 19. The saturation value of A is $\pm 1/q$, with the back stress therefore saturating at $\pm C/q$ (with the sign depending on the direction of the plastic straining $\dot{\gamma}^p$). The value C/q therefore corresponds to the center of the yield surface under steady flowing conditions ($\dot{\gamma}^p \neq 0$) and for the case of a material with $\sigma_y = 0$, then C/q would also correspond to the steady state yield stress of the material as the flow curve is ramped to zero.

Finally, the variation of the additional contribution to the yield stress $\sigma_y(\lambda)$ is specified. Here we select the simplest linear relationship between the yield stress σ_y and the dimensionless microstructural variable λ

$$\sigma_y = k_3 \lambda , \quad (21)$$

where the parameter k_3 is a material constant with units of stress, and λ is an additional evolving internal variable that characterizes the material microstructure.

A differential equation which determines how λ evolves over time is then specified. The following canonical form, which is frequently encountered in thixotropic material models, will be used here^{5,17,89}

$$\frac{d\lambda}{dt} = k_1 (1 - \lambda) - k_2 \lambda |\dot{\gamma}^p| . \quad (22)$$

The change in λ is therefore determined by the competition between a microstructural build up term (first term in Eq. 22) and a breakdown term (second term of Eq. 22). The buildup term is assumed to be the result of Brownian motion or other internal aging processes causing a rearrangement in the local wax microstructure which increases the stiffness of the gel. The breakdown term results from the irreversible plastic shearing of this microstructure. The two new material constants in Eq. 22 are the rate constant k_1 (with units s^{-1}) and the coefficient k_2 which is dimensionless. The constant k_1 sets the scale for the waiting time $t_w \sim 1/k_1$ required for a build up of the wax microstructure, while the constant k_2 determines the rate at which the wax microstructure breaks down for a given shear rate. An important distinction of the evolution equation proposed in Eq. 22 compared to other proposed models is that only the *plastic* strain rate, and not the total strain rate, is responsible for destroying the material structure. This reflects

the fact that only large and irreversible strains should cause a significant change in the material microstructure. Furthermore, small strains which result in primarily elastic behavior should not perturb the material microstructure, and should not have an effect on the microstructural parameter λ or on the back strain A . This distinction is frequently made in the plasticity literature⁴², but is less common in thixotropic rheological models.

The evolution equation for λ , also requires specifying an initial condition. The initial value of λ will depend on how long the material has been aging at rest for (λ can build up under the absence of any type of deformation). Typically an initial condition of $\lambda = 0$ is used when a deformation begins immediately after a long history of preshearing at a high shear rate. If a deformation begins immediately after a long aging time, then an initial condition of $\lambda = 1$ is used.

Eq. 22 allows for both isotropic hardening *and* softening. The isotropic hardening only results from a build up in structure in the material which occurs even when the shear rate is zero. This contrasts to some of the hardening equations that are used in the plasticity literature, where shear can cause an increase in the yield stress of the material^{82,85}. For our model crude oil, shear only results in a nonzero softening term (i.e. the second term in Eq. 22) which causes the yield stress $\sigma_y(\lambda)$ to decrease.

4.1.1.1 Physical interpretation of the internal parameters

In most thixotropic models, a single variable λ is frequently used to characterize the material structure⁵. The model introduced here bears more similarities to the approach taken in plasticity⁸², due to the introduction of two variables, λ and A . Here we discuss the significance of these two variables with respect to the material microstructure.

Mujumdar et al.¹⁷ argued that the scalar parameter λ quantifies the ratio of the number of links in a transient network at a particular level of structure, to the number of links in the network when it is fully structured. For the wax microstructure, we envision λ as being representative of the total number of links per unit volume between the wax particles that form aggregates. Assuming that the force required to break such links is always the same, then the yield stress σ_y can be approximated as a linear function of λ . Because the variable λ quantifies the number of links, it will necessarily be a positive scalar parameter, even in a 3-dimensional version of the model. Furthermore, this scalar parameter can only be used to quantify an isotropic resistance to deformations (i.e. a resistance which is the same in all directions of loading).

However, an additional parameter is necessarily required to characterize anisotropy in the local material microstructure and the resulting non-isotropic resistance, i.e. a stiffening of the material along the direction of imposed deformation. Non-isotropic resistance to deformation is most important when

considering oscillatory loading, where the direction of deformation changes (e.g. LAOS), or more complex 3-dimensional deformations. Capturing this non-isotropic resistance is the purpose of the back strain A and the resulting back stress σ_{back} , which are allowed to take on both negative and positive values for the one-dimensional case of this model (unlike λ and σ_y which are always positive scalar quantities). Furthermore, a fully three-dimensional version of this model would generalize A to a tensor valued quantity (\mathbf{A}), and the back stress σ_{back} to a tensor valued quantity (\mathbf{T}_{back})⁴⁶. Thus, in contrast to the scalar variable λ which only measures the total number of links between wax particles, this tensor valued internal variable \mathbf{A} additionally characterizes the orientation of the wax microstructure. This aspect of the microstructure will be affected by the orientation of the wax sheets observed in Fig. 5 (a property which cannot be described by a simple scalar), which will in turn play a role in determining how these particles resist deformation along a certain direction. The inclusion of both of these internal variables therefore provides a more complete picture of the material microstructure.

4.1.2 Summary of the IKH model equations. Here we summarize the constitutive model in a concise form, and provide a list of the material constants required for fitting. The decomposition of shear strain into linear viscoelastic strain and nonlinear plastic strain is as follows:

$$\gamma = \gamma^{ve} + \gamma^p \quad (23)$$

The linear viscoelastic strain is specified through the introduction of an appropriate LVE constitutive element (Maxwell, Kelvin-Voigt, or simple elastic solid as shown in Fig. 11), while the rate of change of the plastic strain is given by the following:

$$\dot{\gamma}^p = \begin{cases} 0 & \text{if } |\sigma - CA| < k_3 \lambda \\ \frac{\sigma - CA}{|\sigma - CA|} \left(\frac{|\sigma - CA| - k_3 \lambda}{\mu_p} \right) & \text{if } |\sigma - CA| \geq k_3 \lambda \end{cases}, \quad (24)$$

where A and λ are the internal variables that vary through the following differential equations:

$$\dot{A} = \dot{\gamma}^p - (q|A|)^m \text{sign}(A)|\dot{\gamma}^p| \quad (25)$$

$$\dot{\lambda} = k_1(1 - \lambda) - k_2 \lambda |\dot{\gamma}^p|. \quad (26)$$

With the Maxwell model specified as the LVE behavior shown in Fig. 11 (a), this model has 9 fitting parameters, which are: $G, \eta, \mu_p, k_1, k_2, k_3, C, q, m$. This is one additional parameter compared to the Houska model, which is commonly used to describe the rheology of crude oils.²⁷

For the reader interested in more general tensorial forms of this model, the additive strain decomposition for the case of the EIKH model shown in Fig. 11 (c) can be generalized to

a multiplicative Kroner Decomposition⁹⁰ of the deformation gradient \mathbf{F} such that

$$\mathbf{F} = \mathbf{F}^e \mathbf{F}^p, \quad (27)$$

where \mathbf{F}^e is the elastic part of the deformation gradient, and \mathbf{F}^p is the plastic part of the deformation gradient. Anand et al.⁸², Henann and Anand⁸³ and Ames et al.⁸⁵ all give examples of frame invariant forms of constitutive models with both isotropic and kinematic hardening (although their evolution equations for the internal variables differ).

4.2 Quantitative predictions

The IKH model can be used to predict the model crude oil rheological response in the three canonical flows given in Sec. 3. We use data sets for the 10% model waxy crude system in its slurry state at a temperature of 27°C. First the steady state flow curve given in Fig. 6 is considered. Under steady flowing conditions, the IKH model reduces to the limiting case where $\dot{\lambda} = 0$ and $\dot{A} = 0$. The relationship between the magnitude of the plastic flow rate $|\dot{\gamma}^p|$ and the magnitude of the stress $|\sigma|$ in Eq. 15 simplifies to the following:

$$|\sigma| = \mu_p |\dot{\gamma}^p| + \frac{C}{q} + \underbrace{\frac{k_3 k_1}{k_1 + k_2 |\dot{\gamma}^p|}}_{k_3 \lambda_s}. \quad (28)$$

In the case where the KIKH or EIKH variants of the model are used, $\dot{\gamma}^p$ is the only contribution towards the strain rate. Eqn 28 therefore gives a functional form of the IKH model which can be fitted to steady state flowcurves such as that in Fig. 6. In Fig. 12 we show such a fit, and it correctly predicts the important features of the flowcurve. It predicts a Newtonian limit at high shear rates, as well as locally nonmonotonic decreasing region of the flowcurve at the intermediate shear rates. As the shear rate approaches zero, the EIKH and KIKH variants predict a constant stress $|\sigma| = C/q + k_3$. The MIKH variant however will predict a high viscosity Newtonian region at lower shear rates with $\sigma \simeq \eta \dot{\gamma}$ (which our model crude oil does not appear to exhibit). These types of high viscosity, Newtonian regions at very low imposed shear rates often appear for thixotropic yield stress fluids¹, but are difficult to measure precisely. Tuning the LVE element in the IKH model allows for flexibility in the model in capturing this type of behavior.

The values of the model parameters used in Fig. 12 are $C/q = 0.85$ Pa, $\mu_p = 0.42$ Pa.s, $k_3 = 1.5$ Pa, $k_1/k_2 = 0.033$ s⁻¹ and $\eta = 500$ Pa.s. The fitting to the steady state flowcurve only depends on the ratios k_1/k_2 and C/q , and not the specific values of the individual constants. The fitting also does not depend on the modulus G or the softening exponent m (or the viscosity η in the case of the MIKH and KIKH variants). It is

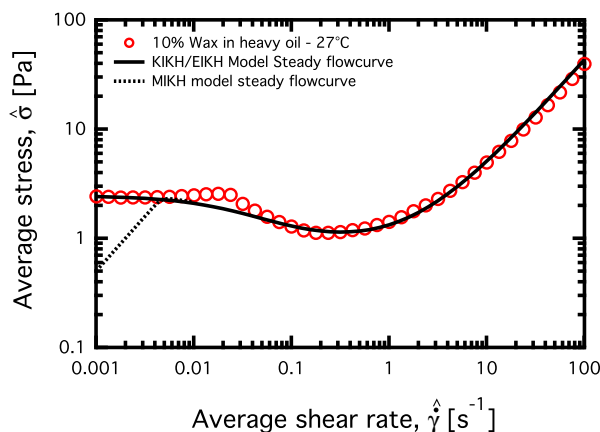


Fig. 12 Fitting of the IKH model to the flowcurve of Fig. 6. Values of model constants are $C/q = 0.85$ Pa, $\mu_p = 0.42$ Pa.s, $k_3 = 1.5$ Pa, $k_1/k_2 = 0.033$ s⁻¹ and $\eta = 500$ Pa.s

therefore necessary to fit the model to additional deformation histories in order to determine the values of these parameters.

Although the simple equation given in Eq. 28 predicts a non-monotonic dependency of stress σ on shear rate $\dot{\gamma}$, it does so assuming the case of homogenous shear, i.e. a spatially and temporally uniform shear rate within the material. Such a nonmonotonic response can also lead to shear banding⁹¹. In Sec. 3.2.1 we indicated experimentally that for shear rates where we observe a decrease in the average stress $\hat{\sigma}$ as the average shear rate $\hat{\gamma}$ is increased, unstable flow occurs within the material and the local shear rate is not homogenous across the gap. Therefore, Eqn. 28 should only be viewed as a first order approximation of what the local stress is within the material as a function of the globally applied shear rate. A more complete prediction for the stress in Fig. 12 would account for these heterogeneities and material instabilities in the flow. In Sec. 4.3 we briefly discuss possible avenues for predicting this complex flow behavior using the IKH model.

The stress overshoots that were measured in Sec. 3.2.2 can also be quantitatively predicted by the IKH model using the same values of the model parameters used in Fig. 12. Values of $G = 250$ Pa, $k_1 = 0.1$ s⁻¹, $C = 70$ Pa and $m = 0.25$ are specified (and the Maxwell variant of the model illustrated in Fig. 11 is used). Initial conditions for the internal variables are $A(t = 0) = 0$ and $\lambda(t = 0) = \lambda(t_w)$. Fig. 13 (a) shows that the IKH model does indeed capture the key features of the response of the 10% wax oil system to startup of steady shear. Stress overshoots are predicted, and these increase as a function of waiting time t_w due to the magnitude of the microstructure parameter λ increasing during the waiting time as a result of rheological aging. The value of the stress overshoot also saturates beyond waiting times of $t_w \sim 1/k_1 = 10$ s, in accordance with our experimental observations.

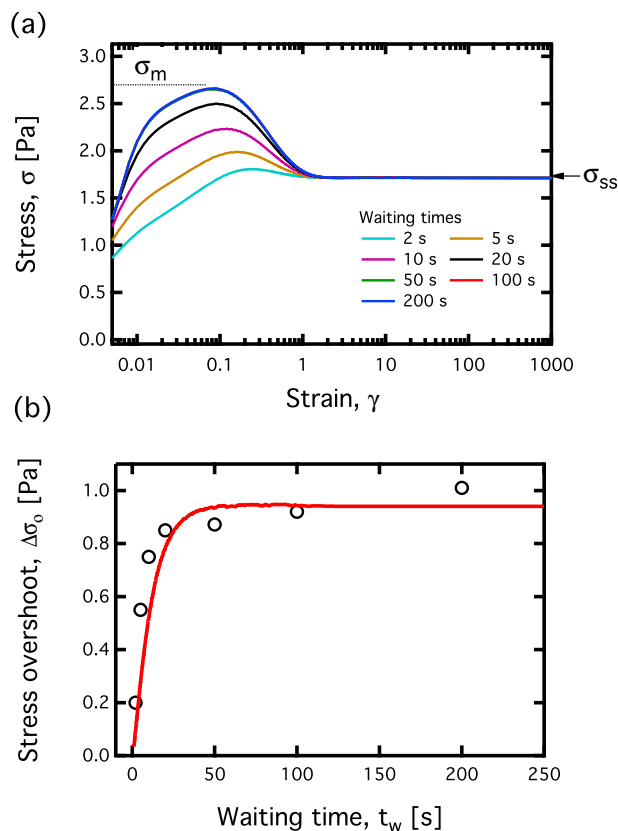


Fig. 13 Prediction of stress overshoots under startup of steady shear for the IKH model. In (a), the imposed shear rate is $\dot{\gamma} = 2 \text{ s}^{-1}$. In (b), we plot the predicted stress overshoot (red line) from the IKH model simulated in (a) vs the experimental data from Fig. 9 (circles). The model parameters are the same for (a) and (b), and are as follows: $C/q = 0.85 \text{ Pa}$, $\mu_p = 0.42 \text{ Pa}\cdot\text{s}$, $k_3 = 1.5 \text{ Pa}$, $k_1/k_2 = 0.033 \text{ s}^{-1}$, $G = 250 \text{ Pa}$, $\eta = 500 \text{ Pa}\cdot\text{s}$, $k_1 = 0.1 \text{ s}^{-1}$, $C = 70 \text{ Pa}$, $m = 0.25$.

Fig. 13 (b) gives a quantitative comparison between the predicted value of the stress overshoot $\Delta\sigma_0 \equiv \sigma_m - \sigma_{ss}$ with its measured value. At a shear rate of 2 s^{-1} , which is far from the unyielded state, the steady state stress is approximately $\sigma_{ss} \simeq C/q + \mu_p \dot{\gamma}$. The maximum in the stress scales as $\sigma_m \sim (C/q + k_3 + \mu_p \dot{\gamma})$, so the stress overshoot will scale as $\Delta\sigma_0 \sim k_3$. The IKH model correctly predicts the overshoot saturating at approximately 1 Pa, and it predicts the critical waiting time $t_w \sim 1/k_1$ required for this overshoot to saturate.

One aspect of the material response that the IKH model does not predict is the long term increase in the steady measured stress $\hat{\sigma}(t)$ which is observed in Fig. 8. This slow transient aging in $\hat{\sigma}(t)$ can be attributed to the presence of additional longer time scales for restructuring in the wax. The IKH model can be readily modified to account for this behavior by introducing a third internal variable, and making the high

shear rate plastic viscosity μ_p a function of this variable (similar dependencies are also adopted for some isotropic hardening models⁸³). An evolution equation for this third variable that is similar to Eq. 22 could be specified. However the associated parameters determining time scales (e.g. the aging rate k_1) would have to be modified in order to reflect this slow restructuring. This would result in the introduction of several new material parameters, making the model significantly more complex. For the sake of simplicity and compactness, we choose to focus on predicting the relative stress overshoot $\Delta\sigma_0$ (which is more important for flow assurance restart procedures), and therefore avoid introducing a third internal variable. The introduction of a third internal variable also requires a subtle distinction in the microstructural interpretation for the λ variable used here. This can be justified by considering rearrangement of the individual wax crystals vs. rearrangement of flocs of crystals. Due to the difference in size, the flocs rearrange much slower than the individual crystals, and have different impacts on the fluid rheology (e.g. the slow floc rearrangement will impact long term changes in steady state viscosity whereas the local rapid rotary diffusion of the wax crystals will affect initial yielding transients).

We also assess the predictive capabilities of the IKH model with respect to the measured LAOS response of the waxy crude oil presented in Fig. 10. For the LAOS response, the values of the model parameters used for the fits in Figs. 13 and 12 are kept constant, other than k_3 and C/q which are both set to 0.7 Pa (while keeping C constant at 70 Pa). With a value of $k_3 = 1.5 \text{ Pa}$, the general features under LAOS are still captured (see supplemental information), however a lower value of k_3 more accurately predicts the absolute value of σ_m under LAOS. In Fig. 14 (a), the fit of the MIKH variant to the LAOS response is shown for the 10% wax oil system in its slurry state at 27° C . The simulated LAOS response of the IKH model always uses the initial conditions of $A = 0$ and $\lambda = 1$. For visual clarity Fig. 14 only illustrates the limit cycle, or alternance state of these LAOS tests.

There is good agreement between the experimental data and the IKH model for the limit cycles observed under LAOS. Both material and model exhibit a transition from linear viscoelastic behavior (corresponding to elliptical Lissajous curves) to nonlinear behavior at strain amplitudes of approximately $\gamma_0 = 0.2\%$. This very small linear range of strains implies that at moderate strain amplitudes (1% - 10%), the IKH response is dominated by the behavior of the nonlinear yielding element with strain γ^p .

In Fig. 14 (b) we compare the values of the maximum stress σ_m determined from the experimental data and from the IKH model. The maximum stress σ_m is defined as the maximum stress over all cycles of oscillation, so it includes the initial transients (overshoots) that are not included in the alternance plots of Fig. 14 (a) (but are shown below in Fig. 15). Fig. 14

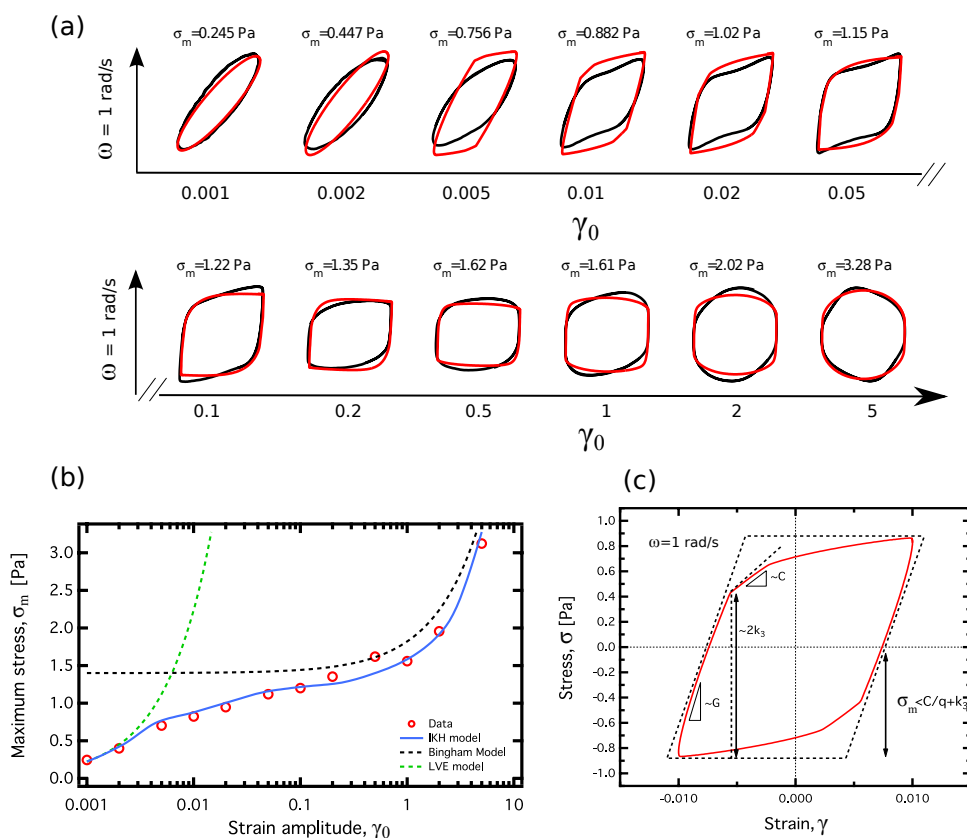


Fig. 14 Modeling of the alternance state in (a) of LAOS tests shown in Fig. 10 ($\omega = 1$ rad/s). Model parameters are $C/q = 0.7$ Pa, $\mu_p = 0.42$ Pa.s, $k_3 = 0.7$ Pa, $k_1/k_2 = 0.033$ s $^{-1}$, $G = 250$ Pa, $\eta = 500$ Pa.s, $k_1 = 0.1$ s $^{-1}$, $C = 70$ Pa, $m = 0.25$. The red line is the IKH model, the black line shows data for a 10% model crude oil. In (b) the prediction of the maximum stress σ_m from the IKH model is compared to the experimentally measured values of σ_m . The predictions of a Maxwell LVE model (green dashed line) and a Bingham model (black dotted line) are also shown. Fig. 14 (c) illustrates the key features of the rhomboidal Lissajous curve for the IKH model, when $\gamma_0 = 1\%$.

(b) includes the predicted values of σ_m for a Maxwell LVE element (with $\eta = 500$ Pa.s and $G = 250$ Pa), and a Bingham model (with $\mu_p = 0.42$ Pa.s and $\sigma_y = 1.4$ Pa). The MIKH model reduces to the LVE model for small strains, and to the Bingham model for large strains, while also maintaining the ability to predict the behavior at intermediate strains.

Fig. 14 (c) decomposes the “sequence of physical processes”⁷⁷ that the IKH model undergoes as the stress and strain vary under LAOS at moderate strain amplitudes. Starting from the lower left point of the curve, the material undergoes an initial (primarily) elastic loading, characterized by a slope/modulus of $G = 250$ Pa. When the stress has increased by a value of $2k_3$, the material yields in the forward direction. As soon as yielding starts, there is an onset of kinematic hardening (relative to a perfect yield plateau), leading to an increase in the stress with $\frac{d\sigma}{d\gamma} \simeq C$ initially. The recovery term in the evolution equation for A (Eq. 19) causes this initial slope to decrease as the imposed deformation continues to increase. A rhomboidal shape in the curve arises, and this is indicative of the presence of the Bauschinger effect⁴². For low shear rates (i.e. $\mu_p\omega\gamma_0 \ll (k_3 + C/q)$), the maximum stress σ_m never exceeds the value of $k_3 + C/q$, corresponding to the limiting value of static yield stress in Fig. 12 at low shear rates. For larger strain amplitudes (and hence larger shear rates), the plastic viscosity contribution to the stress $\mu_p\dot{\gamma}$ becomes more prominent, resulting in Lissajous curves with a diminished rhomboidal shape and increasing convexity.

The IKH model is also capable of predicting the initial transient response of the material as it undergoes large amplitude deformations. Before each test is carried out at a given amplitude γ_0 , a waiting time $t_w = 100$ s is applied, resulting in the material being fully structured before the oscillatory deformation is imposed. For this reason, the IKH simulation begins with the initial condition $\lambda = 1$, and over the course of several oscillations λ will decrease as a result of a nonzero plastic strain rate $\dot{\gamma}^p$, resulting in a decrease in the size of the Lissajous orbits.

Fig. 15 shows two representative transient Lissajous curves of the material undergoing an initial three cycles of deformation at two different amplitudes, $\gamma_0 = 0.1\%$ and $\gamma_0 = 20\%$. For the small amplitude case in Fig. 15 (a), the material requires one half of a cycle of oscillation before the behavior settles into a steady state. Furthermore, no overshoots are observed in the stress when the oscillatory deformation is initialized. This behavior is consistent with a standard linear viscoelastic response, where no thixotropy is present. The IKH model predicts this behavior, validating our argument that only the plastic contribution to the strain γ^p should appear in the evolution equation of λ in Eqn. 22. Thixotropic effects only become apparent at larger strain amplitudes when $\dot{\gamma}^p$ is no longer zero. These thixotropic effects are apparent in the LAOS measurements at a higher strain amplitude in Fig. 15 (b). An initial

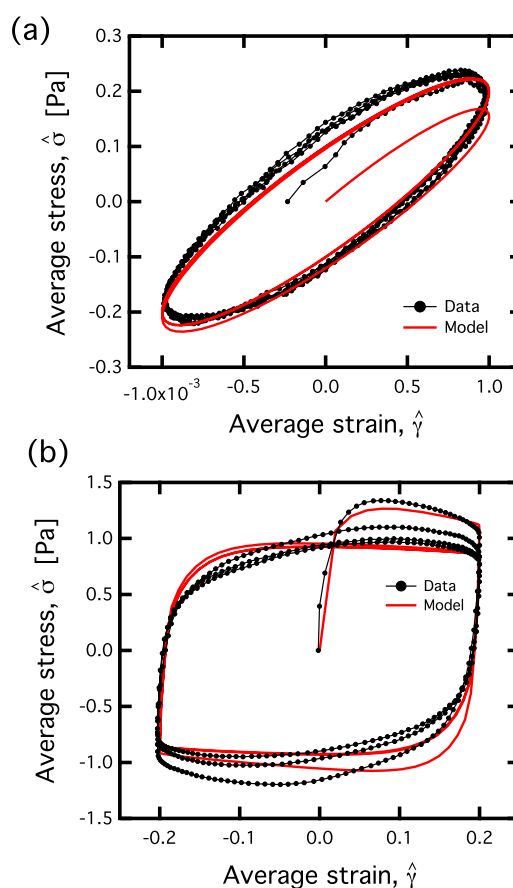


Fig. 15 Transient LAOS data for the IKH model (red line) and the 10% crude oil (points) at two strain amplitudes; (a) $\gamma_0 = 0.1\%$ and (b) $\gamma_0 = 20\%$. Frequency is $\omega = 1$ rad/s in both cases. The same model coefficients as in Fig. 14 are used.

stress overshoot is observed, and multiple cycles of oscillation are required for the material to settle into an alternance state. The IKH model quantitatively predicts the magnitude of this overshoot, and also predicts the slow contraction of the Lissajous orbits towards the ultimate limit cycle. At a given frequency, the ratio of parameters $k_2/k_1 = 30$ s controls the rate of the contraction; as k_2/k_1 increases the orbits will contract more rapidly.

The LAOS tests in Fig. 14 only show the dependency of the material response on the imposed strain amplitude γ_0 . The oscillation frequency ω was also varied at a moderate strain amplitude ($\gamma_0 = 2\%$) to further illustrate the nature of the material’s response in the nonlinear regime of deformations. The specific strain amplitude of 2% was chosen because it lies in the intermediate regime of Fig. 14 (b) between linear viscoelastic (LVE) behavior and Bingham-plastic behavior. In each of these limiting regimes, the effect of varying ω is well understood. In the LVE regime, varying ω enables the appro-

appropriate viscoelastic mechanical model for the material properties below yield to be probed. In the Bingham-plastic regime, the dependency on ω is dominated by the plastic viscosity μ_p , since the instantaneous shear rates are high leading to increasing circular trajectories (as shown in Fig. 14 (a)).

However, in the intermediate regime where strains are between 1%-20%, the material exhibits a rate-independent behavior. Fig. 16 (a) illustrates this by showing the cyclic Lissajous curves of the first 3 cycles of oscillation for the material undergoing LAOS at 4 frequencies spanning an order of magnitude ($\omega = 0.5$ rad/s to $\omega = 5$ rad/s). At this moderate strain amplitude, the material response is clearly nonlinear, with a small amount of thixotropic contraction occurring in the orbits over multiple cycles. However, there is little dependency of the material response on the frequency ω . This is indicative of a deformation rate-independent response at moderate strain amplitudes. The predicted model response shown in Fig. 16 (b) captures this type of behavior. This is because of the rate-independent nature of the kinematic hardening behavior prescribed in Eq. 19. This equation can be rewritten in terms of increments in A and γ^p as follows:

$$dA = d\gamma^p - f(A)|d\gamma^p|. \quad (29)$$

The back strain A therefore evolves independently of the rate of plastic strain γ^p . For the strain amplitude shown in Fig. 16, $\sigma_m \simeq 1$ Pa, so $\gamma^{ve} \sim (\sigma_m/G + \sigma_m/(\eta\omega)) \simeq 0.006$ when $\omega = 1$ rad/s. A large proportion of the total imposed strain, $\gamma_0 = 0.02$, is therefore taken up by the plastic strain $\gamma^p = \gamma - \gamma^{ve}$. As a result, the behavior at this strain amplitude is primarily rate independent. The other internal variable, λ , evolves in a rate-dependent fashion set by the ratio k_2/k_1 , but on a time scale longer than the period of a single orbit $2\pi/\omega$. Hence, the overall response of the material at this range of frequencies is characterized by rate-independent kinematic hardening - a behavior which is most appropriately described by equations of the Armstrong-Frederick type⁸⁶ used in Eq. 29.

The IKH model predicts all of the important features of the material response to the three canonical rheological flows outlined in Sec. 3. To end this subsection, we will discuss one additional flow, and compare it to the predicted response of the IKH model.

In Fig. 6, the particular experimental protocol that was used to measure the flowcurve of the material controlled the applied global (or spatially averaged) deformation rate $\hat{\gamma}$ on the material. An alternative way to control the flow in the material would be to ramp the applied average stress $\hat{\sigma}$ on the material at a very slow rate, and measure the corresponding average shear rate at subsequent points in time. This ‘‘stress ramp’’ test was conducted with the 10% wax-oil system in its slurry state at 27°C using the AR-G2 in its standard configuration. The material is initially brought to its fully structured state by applying a wait time of $t_w = 300$ s, and then a stress ramp

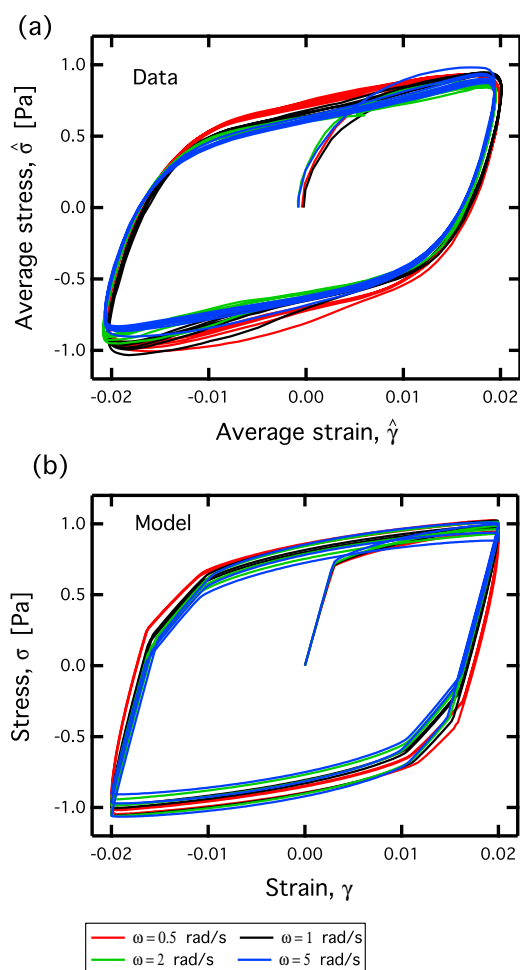


Fig. 16 Frequency dependent behavior under LAOS at moderate strain amplitudes ($\gamma_0 = 2\%$) for both the 10% model crude oil (a) and the IKH model (b). The IKH model model coefficients are the same as in Figs. 14 and 15.

from 0.1 Pa to 5 Pa is imposed over the course of 2 hours (this results in a constant value of $d\hat{\sigma}/dt = 0.00136$ Pa/s). Once the stress reaches the maximum value of 5 Pa, the ramp is immediately reversed and brought down to 0.1 Pa at a rate of $d\hat{\sigma}/dt = -0.00136$ Pa. The average shear rate within the fluid (as measured by the rate of rotation of the conical fixture) is sampled at regular intervals over the course of the increasing and decreasing ramps in stress.

In Fig. 17, we show the experimental results of this stress test, as well as the predicted response of the IKH model to such a stress ramp using the same model parameters that were determined from Fig. 12 and 13. For comparison with the average shear rate measurements, the flowcurve obtained in Fig. 6 is also included on this figure. The non-monotonicity

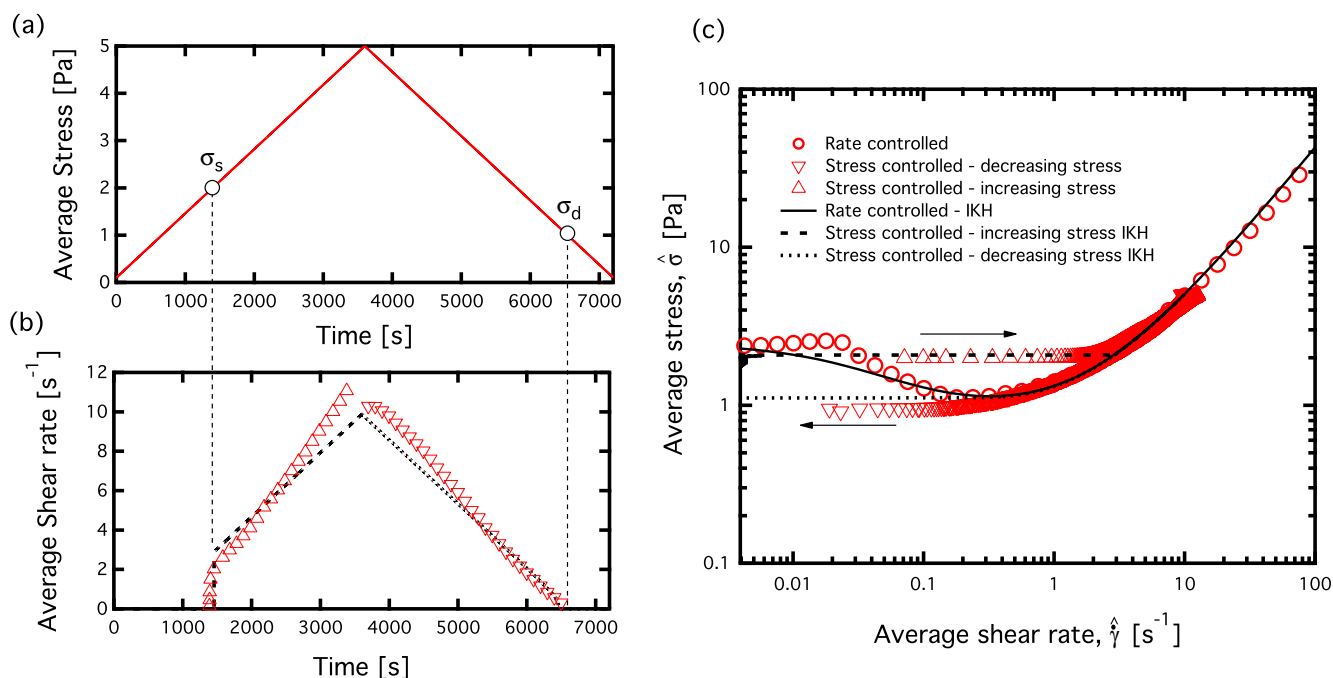


Fig. 17 Rheological measurements for an imposed stress ramp shown in (a), and measured (points) and simulated (lines) shear rates in (b). The different static and dynamic yield stresses are also annotated. The resulting flowcurves of the model crude oil (red data points) and the IKH model (solid and dashed lines) are given in (c). The data is for the same model system at the same temperature shown in Figs. 12 - 16, with the same model parameters as in Fig. 12 and 13.

in the IKH model results in hysteresis being captured in the stress ramp experiments. Specifically, a larger imposed stress (asymptotic value of $\sigma_s \simeq 2$ Pa) is required to start the flow from the structured state, and as the stress is decreased, the same shear rates can be sustained at lower values of the applied stress (asymptotic value of $\sigma_d \simeq 1.1$ Pa). This essentially corresponds to different measurements for the static and dynamic yield stress within the material⁹², and the nonzero value of the microstructural parameter λ is responsible for this difference. While σ approaches the limit of $C/q + k_3 = 2.35$ Pa in the limit $\dot{\gamma} \rightarrow 0$ for the rate-controlled experiment, the asymptotic values of σ determined from the stress ramp experiments are both different from this value. The difference between the static and dynamic yield stress is responsible for the “avalanche effect” that is frequently observed in thixotropic yield stress fluids⁹³ - the supplementary information shows how the IKH model can predict this avalanche effect.

The microstructural physics captured by the IKH model is thus extremely versatile and is able to capture the complex rheology of a structured and aging material such as an elastoviscoplastic crude oil. It can capture the salient features of the response exhibited by the fluid to a number of different steady and time-varying rheological flows. The numerical values of the model parameters were consistent among these different

flows, so the measurements in Fig. 17 constitute a true test of the predictive nature of the model.

4.3 Further Discussion

To conclude our discussion of the IKH model, we expand on a few important points related to the current form of the model. We will also comment on how this model is related to other constitutive models that are commonly encountered in the literature.

4.3.1 Fitting procedure We outline a general fitting procedure used to determine values of the model parameters in the IKH model. This procedure can be summarized as follows: We first fit the parameters μ_p , k_3 and the ratios C/q and k_1/k_2 to the steady state flowcurve in Fig. 6. Next frequency sweeps at low strains below the yield point can be used to fit the linear viscoelastic behavior. If the material is Maxwell-like, then G , η and the corresponding viscoelastic relaxation time η/G can be determined. Subsequently, LAOS can be used to determine appropriate values of the back stress modulus C , and the constants q and m which control the shape of the Lissajous curves. The rate constants k_1 and k_2 which control the rate of thixotropic contraction towards a final periodic alternance state can also be determined from the LAOS

measurements. Finally, stress overshoot measurements can be used to verify that the value of the aging parameter $1/k_1$ agrees with the critical waiting time t_w required for the saturation of the yield overshoot or yield peak. However, the fitting of the parameters to the steady state flowcurve of Fig. 6 may proceed differently for different classes of thixotropic yield stress fluids. Specifically, the nature of the unstable flow that was observed in Sec. 3.2.1 may differ among different classes of soft solids and gel-like materials. For example, an alternative shear banding scenario may be observed where the non-monotonic region of the flowcurve is inaccessible to time-averaged measurement.

4.3.2 Accounting for shear heterogeneities The steady state flowcurve of the IKH model show in Fig. 12 represents a homogenous shear flow, however, at the lowest globally applied shear rates, PIV measurements indicate that the flow of the model crude oil is not homogenous. The nonmonotonicity of the IKH model means that it can predict these types of shear heterogeneities. One way to account for these would be to initially specify a spatially heterogenous value of $\lambda(y, t = 0)$, and then allow for the material elements to evolve under application of a constant global shear rate. The IKH model predicts transient shear banding under such a scenario - regions with initially high values of λ will not deform, but regions with low values of λ will exhibit high shear rates. This shear banding would be extremely sensitive to initial spatial variations of $\lambda(y)$. A heterogenous distribution of the λ parameter is a reasonable assumption, given the observations in this work, as well as previous observations that have shown thixotropic yield stress fluids exhibiting an “erosion” behavior that is often spatially heterogenous³⁸

Shear banding is also predicted by the IKH model under deformations in geometries with sufficiently large stress gradients. We illustrate this in Fig. 18 by simulating startup of shearing flow for the IKH model in a Taylor-Couette cell under a steady applied torque \mathcal{T} . For the simulations in Fig. 18, the inner radius of the cell is set to $R_{in} = 23.7$ mm and the outer radius is $R_{out} = 25$ mm, corresponding to a typical experimental cup and bob. The dimensionless radial position is defined as $\rho \equiv (r - R_{in}) / (R_{out} - R_{in})$, and thus varies from 0 to 1. The torque is set so as to impose a stress which varies (in a $1/r^2$ fashion) from $\sigma = 2.05$ Pa at $\rho = 0$ to $\sigma = 1.85$ Pa at $\rho = 1$. The IKH simulation presented in Fig. 18 assumes that the fluid is initially in a fully structured state with spatially uniform values of $\lambda = 1$ and back strain $A = 0$. The model parameters used were $G = 250$ Pa, $\eta = 500$ Pa.s, $\mu_p = 0.42$ Pa.s, $k_1 = 0.1$ s⁻¹, $k_2 = 3$, $k_3 = 1.5$ Pa, $C = 70$ Pa, $q = 82$ and $m = 0.25$ (these are consistent with the parameter values for the real model waxy crude oil). The data in Fig. 18 is plotted against dimensionless time t/t_c , where $t_c = k_2 / (k_1 q)$. The timescale t_c arises from equating the natural timescales

for the kinematic hardening and isotropic softening/hardening processes.

At time $t/t_c = 0$, the step increase in the torque is imposed and the material starts to deform away from its fully structured state (corresponding to $\lambda = 1$). There is initially a nonzero shear rate across the gap, which decreases up until $t/t_c = 1$. During this initial deformation stage, the material deforms elastically, begins to yield, and then kinematically hardens, resulting in an increase in A and a strengthening of the material in the flow direction. Consequently, the shear rate across the gap decreases during this time period.

For $t/t_c > 1$, the fluid begins to shear band. For the region of the fluid located closest to the inner wall, i.e. for values of $\rho < 0.4$, the isotropic softening process (accounted for by the term $-k_2|\dot{\gamma}|^p|\lambda$ in the evolution equation for λ) begins to dominate over the kinematic hardening process. The value of λ decreases in this region, and a high shear rate band forms in the material closest to the inner wall. For times $t/t_c \gg 1$ the material near the inner wall has fully yielded, and at $\rho = 0$ the velocity reaches its maximum value, $v = v_m = 1.52$ mm/s. The material closer to the outer wall experiences lower shear rates and continues to harden and age, until it exhibits a negligibly small shear rate at long times. These steady shear banded profiles (with one strongly sheared band and one stationary, unsheared band) have been observed in numerous thixotropic yield stress fluids; for example they are carefully documented in the work by Martin and Hu⁹⁴.

4.3.3 Genealogy of Constitutive Models.

The general IKH framework we have described in this work can be simplified to several other constitutive models under various limits. It can be reduced to the Bingham generalized Newtonian fluid model by setting $k_3 = 0$, and then taking the limit of $G \rightarrow \infty$ and $C \rightarrow \infty$, while keeping the ratio C/q constant and equal to the yield stress σ_y . This results in the back stress σ_{back} immediately responding to a given stress level σ_y , by either saturating at $\pm\sigma$ if $|\sigma| < \sigma_y$ or saturating at $\pm\sigma_y$ if $|\sigma| > \sigma_y$. An alternative way to reduce the IKH model to a Bingham model would be to set the back stress to zero $\sigma_{back} = 0$ and set λ to a constant.

The IKH model can also be readily simplified to the kinematic hardening model used by Dimitriou et al.⁴⁶ to describe non-thixotropic yield stress fluids. This is accomplished by setting $k_3 = 0$. While the KH model was shown in that work to predict the correct LAOS behavior for a “simple yield stress fluid”⁹¹, it is not able to predict stress overshoots or prolonged transients under multiple cycles of large amplitude deformation.

The limit of the inelastic Houska model studied by Cawkwell and Charles⁹ and others^{33,41} can be realized by taking the limit of $C \rightarrow \infty$ while keeping the ratio C/q constant and equal to their “fixed” component of the yield stress. The dependence

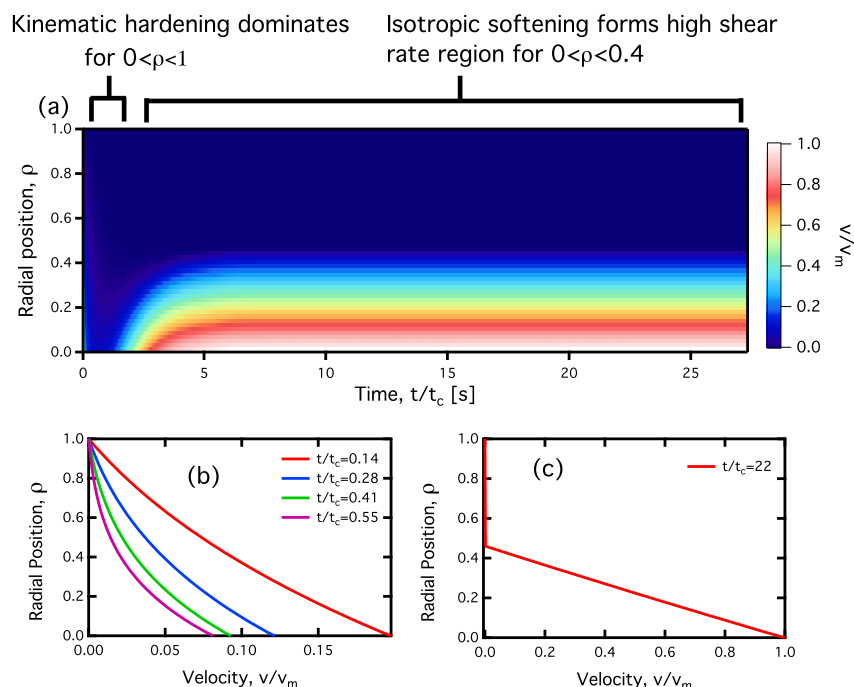


Fig. 18 Shear banding predicted by the IKH model in a Taylor-Couette concentric cylinder geometry. A steady imposed torque \mathcal{T} is applied, resulting in a steady imposed, heterogeneous stress in the material. The material is allowed to evolve from its initial configuration of being fully structured, i.e. $\lambda = 1$. In (a), a space-time profile of the velocity field is shown. In (b) and (c) several velocity profiles are given for different instants in time. Velocity is plotted in a non-dimensional form using the maximum velocity for long times at near the inner wall, $v_m = 1.52$ mm/s.

of σ_y on λ however remains with an evolution equation for λ resulting in the second component of the yield stress not varying. The Houska model also does not account for any elastic behavior below yield, corresponding to the limit $G \rightarrow \infty$.

Finally, the IKH model can be reduced to the “toy” λ -model employed by Coussot et al.⁹⁵. This limit can be achieved by setting both yield parameters σ_y and σ_{back} equal to zero, taking the limit of $G \rightarrow \infty$, and making the viscosity μ_p a function of λ . Coussot employs a different evolution equation for λ , which results in λ growing unbounded in time when the shear rate is zero.

The IKH model is more broadly related to the Mujumdar¹⁷ and Souza Mendes¹⁹ models. These models exhibit key differences from the IKH model. The Mujumdar model does not explicitly decompose strain into elastic and plastic components - as a result the authors necessarily introduce a critical strain γ_c into the model which is used to determine whether or not the structure of the material is breaking. The Mujumdar model does utilize the same form of the evolution equation for λ that is employed here.

The Souza Mendes family of models^{19,57,96} use a different form for the evolution equation of λ , specifically the stress σ enters this equation and is assumed to be the driving force

for disrupting the material microstructure. Souza Mendes and Thompson take this approach in order to avoid disruption of the material microstructure in any elastic, reversible regime of deformation⁵⁷. The use of $\dot{\gamma}^p$ in our evolution equation in λ achieves this same goal. Souza Mendes also writes the linear viscoelastic moduli G and η as functions of λ , resulting in additional material parameters that must be determined by regression to data¹⁹. This may be required for a more complete form of the IKH model, however for simplicity and compactness these dependencies are neglected in the IKH model.

5 Conclusions

The primary goal of this work has been to develop a suitable elasto-viscoplastic constitutive model that can predict the rheology of a thixotropic yield stress fluid. The fluid studied here is a waxy crude oil that is relatively easy to formulate and prepare in a repeatable manner, but still captures the rheological complexity of a real crude oil.

To develop this model, Rheo-PIV measurements were first used to distinguish between the material behavior under different sample preparation protocols. We distinguished between the material in a “slurry” state vs. a “strong gel” state. In the

former, the material exhibits a weaker gel network and is less likely to flow through the mechanism of interfacial wall slip. In the latter, the material can undergo irreversible breakdown of an initially strong gel network. Furthermore, the material in its “strong gel” state is more likely to exhibit localized fracture and failure at the fluid/solid interface.

Second, we outlined three canonical flow scenarios to probe the rheology of the model fluid in its slurry state. These are measurements of the steady (spatially averaged) flowcurve of the material ($\hat{\sigma}$ vs. $\hat{\gamma}$), startup of steady shear flow following different waiting times t_w , and large amplitude oscillatory shear strain (LAOStrain). Furthermore, we used Rheo-PIV measurements to elucidate the nature of flow instabilities that occur in the material at low shear rates. These coincide with a non-monotonic region in the material’s flowcurve. The material instabilities consist of spatially and temporally fluctuating values of local shear rate and shear stress within the material, with a constant globally applied shear rate $\hat{\gamma}$ and average shear stress $\hat{\sigma}$.

Third, we developed an elastoviscoplastic constitutive model (referred to for simplicity as the IKH model) which quantitatively captures the material response to these three flow scenarios. The key features of this model are the additive decomposition of strain into two components (γ^e and γ^p) and the use of the isotropic and kinematic hardening mechanisms adapted from plasticity theory. An added benefit of this approach is that the model is extendable to a frame invariant, 3-dimensional tensorial form that can be utilized in simulations of more complex flow scenarios. The IKH model was fitted to the 10% wax in oil model system in its “slurry state” at 27°C, under these isothermal conditions it was capable of capturing the rheological aging behavior exhibited by the fluid, and the subsequent effects of this aging process on the material response to deformations. Values of the model parameters were generally consistent across the three different rheological flows. The IKH model was also shown to be capable of predicting transient shear banding behavior under deformations in geometries with sufficiently large gradients in the stress.

There are several avenues for a continuation of this work on the IKH model - some of which we have already highlighted. These include accounting for additional slower restructuring timescales which affect the high shear rate plastic viscosity. In the present study we have taken this viscosity to be a constant, μ_p . The IKH model could also be improved by introducing nonlocal terms into the constitutive model, to better describe the nature of the flow instabilities that are observed at low globally-applied shear rates^{18,97}. Other than the results presented in Sec. 4.3, all of the predictions of the IKH model were obtained by assuming homogenous flow. The work by Moorcroft et al.^{98,99} suggested that instances of inhomogeneous flow may be more ubiquitous than previously thought

(in particular where stress overshoots are present). Thus, understanding how the IKH framework might be able to predict these instabilities in more detail would be a worthwhile endeavor. Finally, the model could be modified to capture the continuous, temperature-dependent transition that the material exhibits as it is cooled from above T_{wa} (where it behaves as a Newtonian liquid) to below T_{wa} where it begins to exhibit thixotropic, elastoviscoplastic behavior. The ultimate goal of such work would be to develop a temperature-dependent IKH model, which can then be implemented into simulations of non-isothermal flow in pipelines for flow assurance applications. This would substantially build on the temperature-dependent models that are available today, which typically assume a generalized Newtonian fluid and do not account for elastic or yielding behavior^{28,34}. Practical applications for such a model would be widespread, and would greatly assist in optimizing operating conditions for pipelines that transport waxy crude oil.

6 Acknowledgments

The authors would like to L. Anand and K. Kamrin for fruitful discussions on developing the constitutive model framework employed in this paper. They would also like to acknowledge the help of R. Venkatesan, as well as Chevron Energy Technology Company for funding this research.

References

- 1 H. A. Barnes, *Journal of Non-Newtonian Fluid Mechanics*, 1999, **81**, 133–178.
- 2 D. Bonn and M. M. Denn, *Science*, 2009, **324**, 1401–1402.
- 3 P. Møller, A. Fall, V. Chikkadi, D. Derks and D. Bonn, *Phil. Trans. R. Soc. A*, 2009, **367**, 5139–5155.
- 4 J. Mewis, *Journal of Non-Newtonian Fluid Mechanics*, 1979, **6**, 1–20.
- 5 H. A. Barnes, *Journal of Non-Newtonian Fluid Mechanics*, 1997, **70**, 1–33.
- 6 J. Mewis and N. J. Wagner, *Advances in Colloid and Interface Science*, 2009, **147–148**, 214–227.
- 7 T. Divoux, D. Tamarii, C. Barentin and S. Manneville, *Physical Review Letters*, 2010, **104**, 208301.
- 8 T. Divoux, C. Barentin and S. Manneville, *Soft Matter*, 2011, **7**, 9335–9349.
- 9 M. G. Cawkwell and M. E. Charles, *Journal of Pipelines*, 1987, **7**, 41–52.
- 10 P. Coussot, A. I. Leonov and J. M. Piau, *Journal of Non-Newtonian Fluid Mechanics*, 1993, **46**, 179–217.
- 11 D. De Kee and C. F. Chan Man Fong, *Polymer Engineering & Science*, 1994, **34**, 438–445.
- 12 E. Toorman, *Rheologica Acta*, 1997, **36**, 56–65.
- 13 P. Sollich, F. Lequeux, P. Hébraud and M. E. Cates, *Physical Review Letters*, 1997, **78**, 2020–2023.
- 14 M. L. Falk and J. S. Langer, *Phys. Rev. E*, 1998, **57**, 7192–7205.
- 15 D. Quemada, *The European Physical Journal of Applied Physics*, 1999, **5**, 191–207.
- 16 F. Yziquel, P. Carreau, M. Moan and P. Tanguy, *Journal of Non-Newtonian Fluid Mechanics*, 1999, **86**, 133–155.

- 17 A. Mujumdar, A. N. Beris and A. B. Metzner, *Journal of Non-Newtonian Fluid Mechanics*, 2002, **102**, 157–178.
- 18 L. Bocquet, A. Colin and A. Ajdari, *Physical Review Letters*, 2009, **103**, 036001–.
- 19 P. R. de Souza Mendes, *Soft Matter*, 2011, **7**, 2471–2483.
- 20 P. Sollich, *Phys. Rev. E*, 1998, **58**, 738–759.
- 21 J. S. Langer and L. Pechenik, *Phys. Rev. E*, 2003, **68**, 061507.
- 22 V. Mansard, A. Colin, P. Chauduri and L. Bocquet, *Soft Matter*, 2011, **7**, 5524–5527.
- 23 J. Goyon, A. Colin, G. Ovarlez, A. Ajdari and L. Bocquet, *Nature*, 2008, **454**, 84–87.
- 24 J. Goyon, A. Colin and L. Bocquet, *Soft Matter*, 2010, **6**, 2668–2678.
- 25 H. Petter Rønningsen, *Journal of Petroleum Science and Engineering*, 1992, **7**, 177–213.
- 26 A. Hammami and J. Ratulowski, *Asphaltenes, Heavy Oils, and Petroleomics*, 2007, pp. 617–660.
- 27 M. Cawkwell and M. Charles, *Journal of Pipelines*, 1989, **7**, 251–256.
- 28 K. S. Pedersen and H. P. Rønningsen, *Energy & Fuels*, 2000, **14**, 43–51.
- 29 L. T. Wardhaugh and D. V. Boger, *Journal of Rheology*, 1991, **35**, 301–308.
- 30 R. Venkatesan, N. Nagarajan, K. Paso, Y. Yi, A. Sastry and H. Fogler, *Chemical Engineering Science*, 2005, **60**, 3587–3598.
- 31 R. F. G. Visintin, R. Lapasin, E. Vignati, P. D'Antona and T. P. Lockhart, *Langmuir*, 2005, **21**, 6240–6249.
- 32 J. G. Speight, *The Chemistry and Technology of Petroleum*, CRC Press, 4th edn, 2007.
- 33 K. Paso, T. Kompalla, H. J. Oschmann and J. Sjöblom, *Journal of Dispersion Science and Technology*, 2009, **30**, 472–480.
- 34 E. Ghanaei and D. Mowla, *Energy & Fuels*, 2010, **24**, 1762–1770.
- 35 W. C. Chin, *Offshore*, 2000, **60**, 92.
- 36 S. A. Rogers, D. Vlassopoulos and P. T. Callaghan, *Phys. Rev. Lett.*, 2008, **100**, 128304.
- 37 T. Gibaud, C. Barentin and S. Manneville, *Physical Review Letters*, 2008, **101**, 258302.
- 38 T. Gibaud, C. Barentin, N. Taberlet and S. Manneville, *Soft Matter*, 2009, **5**, 3026–3037.
- 39 P. C. F. Møller, S. Rodts, M. A. J. Michels and D. Bonn, *Phys. Rev. E*, 2008, **77**, 041507.
- 40 A. Wachs, G. Vinay and I. Frigaard, *Journal of Non-Newtonian Fluid Mechanics*, 2009, **159**, 81–94.
- 41 C. Chang, O. Nguyen and H. Rønningsen, *Journal of Non-Newtonian Fluid Mechanics*, 1999, **87**, 127–154.
- 42 M. Gurtin, E. Fried and L. Anand, *The Mechanics and Thermodynamics of Continua*, Cambridge, 2010.
- 43 J. Lemaitre and J.-L. Chaboche, *Mechanics of Solid Materials*, Cambridge, 1990.
- 44 M. Rubin and A. Yarin, *Journal of Non-Newtonian Fluid Mechanics*, 1993, **50**, 79–88.
- 45 D. Doraiswamy, A. N. Mujumdar, I. Tsao, A. N. Beris, S. C. Danforth and A. B. Metzner, *Journal of Rheology*, 1991, **35**, 647–685.
- 46 C. J. Dimitriou, R. H. Ewoldt and G. H. McKinley, *Journal of Rheology*, 2013, **57**, 1–44.
- 47 C. J. Dimitriou, G. H. McKinley and R. Venkatesan, *Energy & Fuels*, 2011, **25**, 3040–3052.
- 48 M. Kanè, M. Djabourov, J.-L. Volle, J.-P. Lechaire and G. Frebourg, *Fuel*, 2002, **82**, 127–135.
- 49 A. Aiyejina, D. P. Chakrabarti, A. Pilgrim and M. Sastry, *International Journal of Multiphase Flow*, 2011, **37**, 671–694.
- 50 C. J. Dimitriou, L. Casanellas, T. Ober and G. McKinley, *Rheologica Acta*, 2012, **51**, 395–411.
- 51 H. S. Lee, P. Singh, W. H. Thomason and H. S. Fogler, *Energy and Fuels*, 2008, **22**, 480–487.
- 52 M. Keentok and S. Xue, *Rheologica Acta*, 1999, **38**, 321–348.
- 53 J. M. Piau, *Journal of Non-Newtonian Fluid Mechanics*, 2007, **144**, 1–29.
- 54 W. B. Russel and M. C. Grant, *Colloids and Surfaces A: Physicochemical and Engineering Aspects*, 2000, **161**, 271–282.
- 55 L. T. Wardhaugh and D. V. Boger, *AIChE Journal*, 1991, **37**, 871–885.
- 56 P. Coussot, L. Tocquer, C. Lanos and G. Ovarlez, *Journal of Non-Newtonian Fluid Mechanics*, 2009, **158**, 85–90.
- 57 P. R. de Souza Mendes and R. L. Thompson, *Journal of Non-Newtonian Fluid Mechanics*, 2012, **187–188**, 8–15.
- 58 R. G. Larson, *Rheologica Acta*, 1992, **31**, 213–263.
- 59 F. Pignon, A. Magnin and J.-M. Piau, *Journal of Rheology*, 1996, **40**, 573–587.
- 60 J. D. Goddard, *Annual Review of Fluid Mechanics*, 2003, **35**, 113–133.
- 61 P. Olmsted, *Rheologica Acta*, 2008, **47**, 283–300.
- 62 J.-F. Berret, *Langmuir*, 1997, **13**, 2227–2234.
- 63 J.-B. Salmon, A. Colin, S. Manneville and F. Molino, *Phys. Rev. Lett.*, 2003, **90**, 228303.
- 64 M. M. Britton and P. T. Callaghan, *Physical Review Letters*, 1997, **78**, 4930–4933.
- 65 J. A. Dijksman, G. H. Wortel, L. T. H. van Dellen, O. Dauchot and M. van Hecke, *Phys. Rev. Lett.*, 2011, **107**, 108303.
- 66 E. Michel, J. Appell, F. Molino, J. Kieffer and G. Porte, *Journal of Rheology*, 2001, **45**, 1465–1477.
- 67 K. Dullaert and J. Mewis, *Journal of Rheology*, 2005, **49**, 1–18.
- 68 P. Callaghan, *Rheologica Acta*, 2008, **47**, 243–255.
- 69 S. A. Rogers, P. T. Callaghan, G. Petekidis and D. Vlassopoulos, *Journal of Rheology*, 2010, **54**, 133–158.
- 70 S. M. Fielding, P. Sollich and M. E. Cates, *Journal of Rheology*, 2000, **44**, 323–369.
- 71 J. S. Dodge and I. M. Krieger, *Transactions of the Society of Rheology*, 1971, **15**, 589–601.
- 72 K. Hyun, M. Wilhelm, C. O. Klein, K. S. Cho, J. G. Nam, K. H. Ahn, S. J. Lee, R. H. Ewoldt and G. H. McKinley, *Progress in Polymer Science*, 2011, **36**, 1697–1753.
- 73 S. A. Rogers, *Journal of Rheology*, 2012, **56**, 1129–1151.
- 74 T. S.-K. Ng, G. H. McKinley and R. H. Ewoldt, *Journal of Rheology*, 2011, **55**, 627–654.
- 75 A. Giacomini, R. Bird, L. Johnson and A. Mix, *Journal of Non-Newtonian Fluid Mechanics*, 2011, **166**, 1081–1099.
- 76 R. H. Ewoldt, P. Winter, J. Maxey and G. H. McKinley, *Rheologica Acta*, 2010, **49**, 191–212.
- 77 S. A. Rogers, B. M. Erwin, D. Vlassopoulos and M. Cloitre, *Journal of Rheology*, 2011, **55**, 435–458.
- 78 M. Reiner, *Advanced Rheology*, H. K. Lewis, 1971.
- 79 J. D. Ferry, *Viscoelastic Properties of Polymers*, John Wiley and Sons, 3rd edn, 1980.
- 80 R. B. Bird, R. C. Armstrong and O. Hassager, *Dynamics of Polymeric Liquids Vol. 1*, John Wiley and Sons, 2nd edn, 1987.
- 81 A. Slibar and P. R. Paslay, in *Intern Symp on Second Order Effects in Elasticity, Plasticity and Fluid Dynamics*, ed. M. Reiner and D. Abir, Pergamon Press, 1964, pp. 1–314.
- 82 L. Anand, N. M. Ames, V. Srivastava and S. A. Chester, *International Journal of Plasticity*, 2008, **25**, 1474–1494.
- 83 D. L. Henann and L. Anand, *International Journal of Plasticity*, 2009, **25**, 1833–1878.
- 84 J. Sestak, M. E. Charles, M. G. Cawkwell and M. Houska, *Journal of Pipelines*, 1987, **6**, 15–24.
- 85 N. M. Ames, V. Srivastava, S. A. Chester and L. Anand, *International Journal of Plasticity*, 2009, **25**, 1495–1539.
- 86 P. J. Armstrong and C. O. Frederick, *Materials at High Temperatures*, 1966, **24**, 1–26.
- 87 Y. Jiang and P. Kurath, *International Journal of Plasticity*, 1996, **12**, 387

- 88 J. Bauschinger, *Mitteilung aus dem Mechanisch-technischen Laboratorium der Königlichen polytechnischen Hochschule in München*, 1886, **13**, 1–115.
- 89 F. Moore, *Transactions of the British Ceramic Society*, 1959, **58**, 470–494.
- 90 E. Kroner, *Archive for Rational Mechanics and Analysis*, 1960, **4**, 273–334.
- 91 G. Ovarlez, S. Cohen-Addad, K. Krishan, J. Goyon and P. Coussot, *Journal of Non-Newtonian Fluid Mechanics*, 2013, **193**, 68–79.
- 92 D. C.-H. Cheng, *Rheologica Acta*, 1986, **25**, 542–554.
- 93 P. Coussot, Q. D. Nguyen, H. T. Huynh and D. Bonn, *Physical Review Letters*, 2002, **88**, 128302.
- 94 J. D. Martin and Y. Thomas Hu, *Soft Matter*, 2012, **8**, 6940–6949.
- 95 P. Coussot, Q. D. Nguyen, H. T. Huynh and D. Bonn, *Journal of Rheology*, 2002, **46**, 573–589.
- 96 P. R. de Souza Mendes and R. L. Thompson, *Rheologica Acta*, 2013, **52**, 673–694.
- 97 D. L. Henann and K. Kamrin, *Proceedings of the National Academy of Sciences*, 2013, **110**, 6730–6735.
- 98 R. L. Moorcroft and S. M. Fielding, *Phys. Rev. Lett.*, 2013, **110**, 086001.
- 99 R. L. Moorcroft and S. M. Fielding, *Journal of Rheology*, 2014, **58**, 103–147.