

**A COMPREHENSIVE OVERVIEW ON THE MICRO- AND NANO-TECHNOLOGICAL ADVANCES FOR ENHANCING THE CHEMICAL STABILITY AND BIOAVAILABILITY OF CAROTENOIDS**

Journal:	<i>Critical Reviews in Food Science and Nutrition</i>
Manuscript ID:	BFSN-2014-1351.R1
Manuscript Type:	Review
Date Submitted by the Author:	n/a
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Keywords:	bioactive compounds, controlled release, storage stability, functional food, bioaccessibility, structural design

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3 1 A COMPREHENSIVE OVERVIEW ON THE MICRO- AND NANO-TECHNOLOGICAL  
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5 2 ENCAPSULATION ADVANCES FOR ENHANCING THE CHEMICAL STABILITY  
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7 3 AND BIOAVAILABILITY OF CAROTENOIDS  
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38 16 Running title: Encapsulation of carotenoids  
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## ABSTRACT

Carotenoids are lipophilic secondary plant compounds, and their consumption within fruits and vegetables has been positively correlated with a decreased risk of developing several chronic diseases. However, their bioavailability is often compromised due to incomplete release from the food matrix, poor solubility and potential degradation during digestion. In addition, carotenoids in food products are prone to oxidative degradation, not only lowering the nutritional value of the product but also triggering other quality deteriorative changes such as formation of lipid pro-oxidants (free radicals), development of discolorations or off-flavor defects. Encapsulation refers to a physicochemical process aiming to entrap an active substance in structurally engineered micro- or nano-systems in order to develop an effective thermodynamical and physical barrier against deteriorative environmental conditions, such as water vapor, oxygen, light, enzymes or pH. In this context, encapsulation of carotenoids has shown to be a very effective strategy to improve their chemical stability under common processing conditions including storage. In addition, encapsulation may also enhance bioavailability (via influencing bioaccessibility and absorption) of lipophilic bioactives, via modulating their release kinetics from the carrier system, solubility and interfacial properties. In the present paper, it is aimed to present the state of the art of carotenoid microencapsulation in order to enhance storability and bioavailability alike.

Keywords: Bioactive compounds; bioaccessibility; controlled release; storage stability; functional food; structural design

## 46 INTRODUCTION

47 Carotenoids are natural organic pigments comprising eight isoprene units joined to a skeleton  
48 of 40 carbon atoms. Carotenoids can be generally classified into *oxygen containing*, i.e.  
49 xanthophylls (e.g. lutein, cryptoxanthin, astaxanthin) and *hydrocarbon* carotenoids, i.e.  
50 carotenes (e.g.  $\alpha$ -,  $\beta$ - carotene, lycopene, phytoene). Carotenoids are synthesized by all plants  
51 and many microorganisms (bacteria and fungi), but not by animals including humans. On  
52 many occasions, carotenoids are responsible for the red, yellow and orange color of fruit,  
53 vegetables, flowers etc. (Britton, 1996).

54 The presence of a conjugated, delocalized  $\pi$ -electron system (polyene chain) is strictly  
55 associated with the particular physicochemical properties of carotenoids. They are  
56 comparatively lipophilic compounds with octanol-water coefficients of ca. 10-18 (Cooper et  
57 al., 1997). They also easily isomerize and are oxidized; they absorb light, imparting their  
58 color features as well as exerting significant free radical scavenging ability, acting as singlet  
59 oxygen quenchers or electron donors/acceptors (Krinsky and Johnson, 2005).

60 At least in part due to their antioxidant properties, adoption of a carotenoid-rich diet has been  
61 suggested to confer important health benefits to humans by retaining main bodily functions  
62 and to prevent inflammation related disease such as cardiovascular, ophthalmological,  
63 pulmonary and neurodegenerative disorders as well as some types of cancer (Krinsky and  
64 Johnson, 2005; Stahl and Sies, 2005). This may be related to the carotenoids' impact on  
65 cellular signaling cascades such as various transcription factors, influencing the expression of  
66 genes associated with antioxidant defense, anti-inflammatory or anti-cancer properties  
67 (Kaulmann and Bohn, 2014; Stahl and Sies, 2005). Unfortunately, due to their required  
68 emulsification in form of mixed micelles in the gut prior to their uptake (Bohn, 2008),  
69 bioavailability from fruits and vegetables, their main dietary sources, is low, around 10-20%  
70 for carotenes, and up to 40% for xanthophylls (Bohn, 2008; Salar-Behzadi et al., 2013).

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71 In food industry, carotenoids are used as natural pigments to impart color or to recover color  
72 losses, following severe processing and prolonged storage of e.g. meat and dairy products, ice  
73 cream, beverages, or confectionaries (Britton and Khachik, 2009). Moreover, carotenoids are  
74 considered as natural antioxidants, preventing lipid oxidation in o/w and w/o emulsions such  
75 as in salad dressings, mayonnaises, dairy and fat spreads etc. (Dimakou and Oreopoulou,  
76 2012; Lee and Choe, 2013; Yanishlieva et al., 2001). Delivering carotenoids to humans via  
77 functional food carriers can improve their bioavailability through improving matrix release  
78 kinetics (Qian et al., 2012c), solubility (Ribeiro et al., 2010), and may reduce their  
79 degradation during digestion (Wang and Bohn, 2012). Such carriers may include dehydrated  
80 matrices produced by physical methods (e.g. spray-, freeze- or fluidized bed-drying), micro-  
81 or nano-emulsions, hydrogel-based microbeads, self-assembled biopolymer matrices,  
82 nanostructured particles and others. Moreover, specific food processing such as thermal  
83 processing, size reduction or emulsification may promote carotenoid bioavailability. On the  
84 other hand, abusive processing including prolonged storage time, exposure to oxygen, severe  
85 heat treatment etc. can damage carotenoids due to instability against heat and light (Wang  
86 and Bohn, 2012). Thus, maintaining carotenoid biological activity, particularly for processed  
87 food, is a challenge for the food industry. In the present paper, we review recent advances in  
88 carotenoid micro- and nano-encapsulation aiming to retain their stability under typical food  
89 processing and storage conditions (Fig. 1) and to ensure maximal bioavailability.

## 90 THE CONCEPT OF ENCAPSULATION

91 Encapsulation refers to a physicochemical process aiming to entrap active compounds, e.g.  
92 phytochemicals, living cells, essential oils etc. as core materials in a micro-environment of a  
93 composite compound (wall material), and generally fall into two main categories: *reservoir*  
94 and *matrix* type. The former is characterized by a shell-like structure with the active  
95 compound residing in the interior of the capsule. In the matrix type, the bioactive compound

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3 96 is uniformly distributed over the formed biopolymer carrier system, i.e. the active compound  
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5 97 can be found also on the encapsulate surface. Regardless of the encapsulation technique, the  
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7 98 carrier material should provide a thermodynamical and physico-chemical barrier against  
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10 99 external environmental or processing conditions, such as water vapor, heat, oxygen, light,  
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12 100 enzymes or pH (Augustin and Sanguansri, 2008). Furthermore, the carrier material should be  
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14 101 inert, consisting of natural food components (or such generally recognized as safe (GRAS)),  
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16 102 inexpensive, technologically (good film forming, gelling, water binding and emulsifying  
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18 103 capacity, low viscosity) and organoleptically (neutral taste and odor, colorless) versatile and  
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20 104 also, on specific occasions, should convey controlled release (Augustin and Sanguansri,  
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22 105 2008; Gonnet et al., 2010; Zuidam and Shimoni, 2010). With respect to carotenoids, the  
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24 106 design of the carrier system should consider also the solubility, crystallinity, and droplet  
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26 107 particle size changes during incorporation in the selected structure, as these parameters are  
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28 108 directly associated with release kinetics and bioaccessibility and therefore carotenoid  
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30 109 bioavailability (Ribeiro et al., 2010). For lipophilic compounds, the following various types  
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32 110 of microcarriers may be distinguished (McClements, 2010):

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36 111 a) Conventional emulsions: Consisting of a lipophilic emulsified particle and the  
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38 112 emulsifying agent;
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40 113 b) Nanoemulsions: as conventional emulsions, but of mean droplet size < ca. 250 nm;
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42 114 c) Liposomes: a lipid bilayer encapsulating an aqueous solution inside this hydrophobic  
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44 115 shield;
- 45  
46 116 d) Hydrogel particles: network of hydrophilic biopolymers trapping solvent molecules;
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48 117 e) Solid-lipid particles: solid (e.g. crystalline lipid) dispersed in oil.

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51 118 Typical ingredients for encapsulation include amorphous sugars (sucrose, lactose, trehalose),  
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53 119 polyols (sorbitol, mannitol) and non-crystalline polymeric materials such as chemically  
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55 120 modified starch, maltodextrins, polysaccharides (arabic, mesquite or gellan gum, alginates,  
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3 121 pectins) and proteins (gelatin, whey proteins, sodium caseinate, soy protein). Physical state  
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5 122 transitions (e.g. glassy to rubbery) in biopolymer matrices inducing their structural collapse  
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7 123 can also adversely impact the stability of the encapsulated material. **As a consequence**, the  
8  
9 124 release of lipophilic bioactive core material and the increased permeability and diffusivity to  
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11 125 gasses (water vapor, oxygen) of the encapsulating matrix may trigger **degradation**, e.g. lipid  
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13 126 oxidation, discoloration, off-flavor development etc. **It** has been reported that carotenoids  
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15 127 exert high stability at low ( $a_w$  : 0.11-0.3, glassy state) to intermediate water activities (glassy  
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17 128 state controlled by Williams-Landel-Ferry (WLF) kinetics), but low stability upon full matrix  
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19 129 plasticization (Desobry et al., 1997; Selim et al., 2000; Sutter et al., 2007).

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21 130 Selecting the appropriate encapsulation strategy of bioactive compounds **is challenging, as**  
22  
23 131 **core and** wall material properties, capsule-matrix characteristics (e.g. ease of dispersion,  
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25 132 particle size, morphology, structural aspects, solubility), the stability against **ageing** (e.g.  
26  
27 133 matrix collapse), and release mechanisms/kinetics during gastrointestinal (GI) digestion  
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29 134 should be considered. Finally, the encapsulation technique should be technically and  
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31 135 economically feasible, **up-scalable** from the laboratory to the industrial level and sustainable.

## 32 136 **MICROENCAPSULATION TECHNOLOGIES**

### 33 137 **1. Spray drying**

#### 34 138 ***General aspects***

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36 139 Spray drying is a unit operation where a solution, emulsion or suspension comprising the  
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38 140 capsule's wall and core material is atomized by passing through a nozzle and mixed with a  
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40 141 stream of hot air, usually around 140-180°C, in a drying chamber (Gharsallaoui et al., 2007).

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42 142 Spray **drying is a cost-effective** and high throughput/handling capacity process resulting in  
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44 143 controlled particle size formation, good technological powder characteristics and short  
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46 144 residence time in the drying **chamber (1-30 s)** (Gharsallaoui et al., 2007; Gouin, 2004).

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3 145 For lipophilic compounds such as for carotenoids, o/w emulsion formation is required prior to  
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5 146 atomization for high encapsulation efficiency and narrow particle size distribution (Ribeiro et  
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7 147 al., 2010). Ingredients with good emulsifying and film forming capacity, high solubility and  
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9 148 low viscosity are predominantly used (Gharsallaoui et al., 2007). Spray drying conditions,  
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11 149 e.g. air and carrier solution flow rates, inlet/outlet temperature, cyclone separator pressure,  
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13 150 and nozzle geometry can affect encapsulation efficiency, the particle size and morphology as  
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15 151 well as carotenoid degradation due to heat induced cis- isomerization, oxidation (Goula and  
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17 152 Adamopoulos, 2012; Nunes and Mercadante, 2007; Ribeiro et al., 2010; Shu et al., 2006),  
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19 153 epoxide (Perez-Galvez et al., 2005) and apo-carotenal formation (Boon et al., 2010).

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21 154 As a general rule, increasing the core to wall material ratio, lower feeding temperature and  
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23 155 inlet temperature of spray drying is associated with enhanced carotenoid encapsulation  
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25 156 efficiency (Goula and Adamopoulos, 2012; Mestry et al., 2011; Shu et al., 2006; Wang et al.,  
26  
27 157 2012b). In most of the cases, the retention of carotenoids in the spray dried matrices can be as  
28  
29 158 high as 90-94% (Table 1), with the remainder ending up uncoated, rather than oxidized. In  
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31 159 addition, carotenoid encapsulation efficiency can be further improved by reducing the mean  
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33 160 lipid droplet size due to faster water evaporation rates and the shorter film formation time  
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35 161 (Shen and Quek, 2014; Shu et al., 2006).

#### 162 ***Effectiveness of encapsulation depending on core:wall ratio and materials employed***

36  
37 163 Sufficient encapsulation requires a certain amount of wall material. Adverse effects on both  
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39 164 encapsulation efficiency and storage stability were detected when increasing the core:wall  
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41 165 material ratio from 1:19 to 3:17 for a broad range of wall materials including gelatin, gum  
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43 166 arabic, gellan gum, mesquite gum, and soluble soybean polysaccharide (Hojjati et al., 2011;  
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45 167 Rodríguez-Huezo et al., 2004; Shu et al., 2006).

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47 168 Starch derivatives such as maltodextrins and modified starches have also been successfully  
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49 169 employed to develop carotenoid loaded microcapsules (Loksuwan, 2007). The presence of  
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3 170 surface active functional groups (e.g. 1-octenyl succinate), the amount of free soluble  
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5 171 amylose, the thickening capacity of starch, are known to impact carotenoid encapsulation  
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7 172 efficiency. Acid modification of native tapioca starch enhanced  $\beta$ -carotene retention and  
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9 173 chemical stability upon storage and reduced its surface deposited amount. This was attributed  
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11 174 to the ability of amylose to form a continuous network via hydrogen bonds, immobilizing  
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13 175 carotene and increasing film forming capacity, creating a protective physical barrier against  
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15 176 heat and oxygen. Similarly, lycopene encapsulation by hydrophobically modified waxy maize  
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17 177 starch (Capsul®) allowed for efficient encapsulation and increased storage stability at 10 and  
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19 178 20°C, compared to its free form (Rocha et al., 2012).

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22 179 Protein ingredients such as whey protein concentrate, skim milk powder and sodium  
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24 180 caseinate have also been used to produce carotenoid loaded dried microspheres (Pu et al.,  
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26 181 2011; Shen and Quek, 2014). The formation of spray dried microcapsules via casein micelle  
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28 182 dissociation – re-assembly mechanisms was an efficient strategy to encapsulate and stabilize  
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30 183 bixin, a natural apocarotenoid and a food colorant (Zhang and Zhong, 2013). The  
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32 184 microcapsules exerted very good dispersibility over a broad pH range (2-10), while their  
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34 185 instability close to the casein isoelectric point was minimized by adding soluble soy  
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36 186 polysaccharides (Table 1), adsorbing onto casein particles under acidic conditions. Upon  
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38 187 rehydration, the spray dried microcapsules underwent structural reformation, resulting in  
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40 188 bixin core/casein shell particles of very small mean size (90 nm) and of high stability against  
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42 189 thermal/light induced carotenoid degradation.

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45 190 In addition to the wall materials, the purity of the carotenoid extract has been reported to  
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47 191 impact encapsulation efficiency, with a minimum purity being required to achieve adequately  
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49 192 high retention in the spray dried matrix (Shu et al., 2006). Investigating lycopene oleoresin it  
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51 193 was found that a purity of 52% was required to maximize encapsulation efficiency to approx.  
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53 194 80% in gelatin/sucrose based microcapsules, while further increases of oleoresin purity  
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3 195 conferred only minor improvement of the encapsulation. The reasons remain speculative, but  
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5 196 it was suggested that additional compounds present at lower purity, e.g. fatty acids,  
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7 197 glycerides, and unsaponifiable compounds hindered a proper wall formation.

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10 198 *Storage stability of encapsulated carotenoids and influence of water activity*

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12 199 Storage stability of carotenoids encapsulated in spray dried food matrices is affected by many  
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14 200 parameters, such as the thermal history, the composition, physical state and structural aspects  
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16 201 of the microparticles, the storage conditions such as relative humidity, temperature, presence  
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18 202 of light (Zhang and Zhong, 2013), vacuum, oxygen, inert gases etc., and the packaging  
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20 203 material properties, e.g. permeability to water vapor and oxygen, and light absorbance (Table  
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22 204 1). Matrix compositional elements govern carotenoid degradation either via their free radical  
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25 205 scavenging activity or their wall barrier properties.

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27 206 Using surface active ingredients such as milk proteins (whey protein concentrate, sodium  
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29 207 caseinate,  $\beta$ -lactoglobulin), chemically modified starches, gelatine, mesquite and arabic gum  
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31 208 have shown to enhance carotenoid storage stability (Barbosa et al., 2005; Liang et al., 2013b;  
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33 209 Loksuwan, 2007; Rocha et al., 2012; Shu et al., 2006; Wang et al., 2013) by up to 5 times.

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36 210 Their encapsulating potential relies primarily on their ability to interact with lipophilic  
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38 211 compounds via hydrogen bonds or van der Waals forces, diminishing the amount of  
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40 212 carotenoids deposited on the microcapsule surface (readily degradable) and interacting in the  
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42 213 air/liquid surface upon dehydration, creating protective films. Using surface active  
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44 214 compounds as primary (sole) or secondary (with other) encapsulating agents can drastically  
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46 215 (0.5 to 5-fold) enhance carotenoid stability over time compared to non-encapsulated ones. In  
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48 216 addition, carotenoid photostability can be influenced by the wall materials' ability to alter the  
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50 217 powder's reconstitution properties. For instance, it was demonstrated that bixin degradation  
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52 218 in solutions exposed to light, prepared by dispersing carriers containing Tween 80 or gum  
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3 219 Arabic, was reduced by 3-4 times (compared to control solutions with maltodextrins) due to  
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5 220 their lower water solubility and higher turbidity (Barbosa et al., 2005).

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7 221 Maintaining low temperature and low water activity, protecting the native carrier system  
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9 222 from structural collapse or physical ageing are pre-requisites to ensure maximum stability of  
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11 223 the core material. A direct relation between water activity of spray dried matrices and  
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13 224 carotenoid degradation upon storage has been shown. A linear correlation between  $\beta$ -carotene  
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15 225 degradation and glass transition temperature was observed for a critical range of  $a_w$  (i.e. 0.11-  
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17 226 0.75), while further increasing residual water abruptly reduced  $\beta$ -carotene degradation, due to  
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19 227 complete structural collapse of the carrier, lowering diffusion rates of oxygen (Liang et al.,  
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21 228 2013b; Prado et al., 2005; Serris and Biliaderis, 2001). Transitions from the glassy to the  
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23 229 rubbery state and matrix collapse increase solute molecular mobility and translational energy  
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25 230 of macromolecules and result in a shift from monolayer to multilayer water sorption states.  
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27 231 Liang et al. (2013b) demonstrated that degradation kinetics of  $\beta$ -carotene in the amorphous  
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29 232 state are driven by water vapor, oxygen diffusion and mobility constraints related to the  
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31 233 systems' microstructure and porosity. However, structural collapse may raise technological  
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33 234 concerns such impaired flowability and dispersibility, caking, microbial spoilage etc. and thus  
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35 235 production of high moisture carriers are rather undesired.

### 236 *Spray drying: Monodisperse and combined with other microencapsulation technologies*

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37 237 Single droplet (monodisperse) spray drying has been also implemented for  
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39 238 microencapsulating carotenoids promoting better control of microparticle size distribution,  
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41 239 allowing powder production under the same thermal conditions, and offering consistency of  
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43 240 biological activity (Dai et al., 2013; Schutyser et al., 2012). Microencapsulation of  
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45 241 astaxanthin with lactose and sodium caseinate by monodisperse droplet spray drying allowed  
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47 242 producing narrowly sized microparticles that exhibited good technological features with  
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49 243 respect to flowability, agglomeration, residual moisture, and oil surface coverage. Despite the  
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3 244 high temperature (105°C) in the drying chamber, the method did not significantly influence  
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5 245 the radical scavenging activity of astaxanthin. The authors further confirmed the controlled  
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7 246 release of astaxanthin in a buffer solution at neutral pH and at room temperature. However,  
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10 247 the method is much less cost effective compared to conventional spray drying, due to lack of  
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12 248 atomizing techniques able to handle large production capacities (Dai et al., 2013).  
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14 249 Spray drying can easily be combined with other microencapsulation techniques, such as  
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16 250 inclusion complexation. Supercritical fluid and self-assembled protein carriers such as casein  
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18 251 have been also successfully implemented (Jarunglumlert and Nakagawa, 2013). In their  
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20 252 study, protein aggregation under acidic conditions (pH = 5.5) improved  $\beta$ -carotene loading to  
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22 253 the matrix, due to the formation of cluster aggregates. Furthermore, aggregation at slightly  
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24 254 higher pH (6.0) reduced  $\beta$ -carotene deposition on microparticle surfaces, mainly due to the  
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26 255 structural rearrangement of the protein cluster aggregates, reducing the risk of heat induced  
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28 256 degradation of  $\beta$ -carotene throughout the drying as well as its release rate into water.  
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## 31 257 2. Freeze drying

### 32 258 *General aspects*

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36 259 Freeze drying is widely applied for heat labile bioactive compounds and living cells. The  
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38 260 method is based on freezing aqueous samples (solution, suspension or o/w emulsion) at very  
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40 261 low temperature (-80 to -40 °C) and their successive drying by water sublimation at low  
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42 262 pressure (< ca. 5 mbar). Although the method has found many applications particularly in the  
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44 263 case of anhydrobiotics and sensitive encapsulates including liposomes (Meng et al., 2008),  
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46 264 several disadvantages such as high operational costs (energy and time intensive), restricted  
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48 265 barrier properties (high porosity) of the capsules (Krokida and Maroulis, 1997) and often the  
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50 266 need for size reduction (e.g. grinding, pulverization) to facilitate rapid drying exist.  
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54 267 For carotenoids, freeze drying provides a considerable protection against oxidation and  
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56 268 isomerization occurring in other dehydration processes involving hot air streams (spray  
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3 269 drying, fluidized bed drying, air drying etc.). **Contrary** to convective heat processing, **freeze**  
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5 270 **drying, due to the low temperature and pressure**, has rather a low impact on the encapsulation  
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7 271 efficiency and carotenoid degradation, not triggering water phase reactions or oxidation.  
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10 272 Desobry and others (1997) compared spray, freeze and drum drying, finding that freeze  
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12 273 drying had only a minor impact on  $\beta$ -carotene encapsulation efficiency and microparticle  
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14 274 surface coverage compared to spray drying (8 vs 11% and 35 vs 38%, respectively), while  
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16 275 drum drying resulted in higher carotenoid degradation. On the other hand, the comparably  
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18 276 large mean size (up to 100  $\mu\text{m}$  **and high** porosity) together with the high surface  $\beta$ -carotene  
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20 277 load of the freeze-dried particles negatively affected  $\beta$ -carotene **stability throughout** storage  
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22 278 under controlled temperature and relative humidity compared to e.g. drum-drying.  
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24 279 Interestingly, **degradation** of  $\beta$ -carotene encapsulated in amorphous matrices such as  
25  
26 280 maltodextrins exhibited a transition from first to second order kinetics, resulting in decreased  
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28 281  **$\beta$ -carotene oxidation, ca. 20% (Desobry et al., 1997). Similarly, freeze- drying for developing**  
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30 282 **carotenoid (lutein, zeaxanthin, and canthaxanthin) rich egg yolk powders improved the**  
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32 283 **retention rates of xanthophylls compared to spray-dried samples by ca. 25%, though no**  
33  
34 284 **difference in encapsulation efficiency was detected (Wenzel et al., 2010).**  
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36 285 **Structural collapse occurring during freeze drying might also lead to enhanced carotenoid**  
37  
38 286 **retention during storage (Harnkarnsujarit et al., 2012a). Investigating the storage stability of**  
39  
40 287  **$\beta$ -carotene entrapped in freeze dried maltodextrin systems revealed that the structural**  
41  
42 288 **collapse upon freeze drying at temperatures below  $T_g'$  and  $T_m'$  was associated with**  
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44 289 **improved  $\beta$ -carotene retention. This** was mainly attributed to the reduced oxygen and water  
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46 290 vapor diffusivity of the matrices, due to the formation of a low **porosity crust. On the other**  
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48 291 hand, operating freeze dryers at high temperature leads to more **porous matrices**, with the  
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50 292 mean pore diameter and thickness govern carotenoid stability, with smaller and thinner pores  
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3 293 in conjunction with lower thickness known to cause highest degradation of  $\beta$ -carotene due to  
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5 294 increased oxygen exposure of the larger surface (Harnkarnsujarit et al., 2012a).

7 295 *Wall material for freeze drying encapsulation and additives*

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10 296 Amorphous sugars and polyols, gelatine, modified starch, maltodextrins, gum arabic,  
11  
12 297 pullulan, polyvinylpyrrolidone, sodium caseinate and  $\beta$ -cyclodextrins (CDs) have been used  
13  
14 298 for carotenoid encapsulating employing freeze drying (Table 1). For sugars and polyols,  
15  
16 299 physical state transitions e.g. from the amorphous to the fully crystalline, occurring due to  
17  
18 300 freeze-concentration may lead to poor encapsulation efficiency and storage stability. This  
19  
20 301 may be avoided by adding crystallization inhibitors such as amino acids, phosphate anions or  
21  
22 302 divalent cations, which enhance the ability of the sugar matrix to retain higher amounts of  
23  
24 303 carotenoids. Sutter et al. (2007) demonstrated that divalent cations ( $Zn^{2+}$ ,  $Ca^{2+}$ ,  $Mg^{2+}$  and  
25  
26 304  $Mn^{2+}$ ) and glycine, at concentrations of 20 mM, can improve  $\beta$ -carotene encapsulation  
27  
28 305 efficiency of phosphate buffered mannitol systems up to 3 fold, via cation-hydrogen bonding  
29  
30 306 via hydroxyl groups, forming a glycine physical barrier on the liquid-solid interfaces.

33  
34 307 Chemically modified starch and maltodextrins for carotenoid encapsulation were investigated  
35  
36 308 in a series of studies (Grattard et al., 2002; Ramoneda et al., 2011; Sousdaleff et al., 2012;  
37  
38 309 Spada et al., 2012a; Spada et al., 2012b). Their good filming and emulsifying properties  
39  
40 310 promote the formation of a physical barrier against oxidation. For example, in a study by  
41  
42 311 Sousdaleff et al. (2012) curcumin (a lipophilic polyphenol) encapsulated by freeze-drying,  
43  
44 312 using maltodextrin DE20 based matrices improved its stability against degradation in the  
45  
46 313 absence or presence of light and oxygen (air), resulting in a retention of 71% over 30 d.

47  
48 314 Similarly, freeze-dried matrices made of native pinhão starch exerted a poor retention of  $\beta$ -  
49  
50 315 carotene during storage, due poor interfacial properties (Spada et al., 2012b). Chemical  
51  
52 316 modification of native pinhão starch enhanced  $\beta$ -carotene binding and retention, attributed to  
53  
54 317 the increased flexibility and lower oxygen permeability of the dextrin-based matrices, as well  
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3 318 as to the presence of free soluble amylose. The latter can form gel-like structures at liquid-air  
4  
5 319 interfaces, creating a physical barrier under harsh conditions. Moreover, it can effectively  
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7 320 entrap  $\beta$ -carotene via hydrogen bond formation (Spada and others 2012b). The hydrolytic  
8  
9 321 breakdown of starch, has been reported to improve the encapsulation efficacy and retention of  
10  
11 322 carotenoids (Spada et al., 2012b; Wagner, 1995) as well as blending maltodextrins with other  
12  
13 323 biopolymers such as gelatin or gum arabic (Ramoneda et al., 2011).  
14  
15  
16 324 Spada et al. (2012a) showed that gelatin as a co-encapsulating agent does not enhance the  
17  
18 325 encapsulation efficiency of native and hydrolyzed starch based matrices, though a ca. 5 fold  
19  
20 326 reduction of surface deposited  $\beta$ -carotene was achieved. Furthermore, gelatin reduced the  
21  
22 327 matrices' solubility in cold water, indicating reduced diffusivity and permeability of the  
23  
24 328 freeze-dried matrices, possibly due to formation of an external coating layer.  
25  
26  
27 329 Using disaccharide – macromolecule blends to entrap carotenoids in freeze-dried matrices  
28  
29 330 can alternatively be employed to control phase transitions, reducing glass transition  
30  
31 331 temperature, enhancing carotenoid storage stability (Elizalde et al., 2002; Harnkarnsujarit et  
32  
33 332 al., 2012a; Tang and Chen, 2000). Studies have shown that biopolymers such as starch and  
34  
35 333 starch hydrolyzates, whey proteins or gelatin significantly hinder recrystallization even under  
36  
37 334 high RH (up to 84%). Alternatively, adding electrolytes has been suggested to control  
38  
39 335 physical state transitions in dehydrated food matrices, due to their ability to influence the  
40  
41 336 water phase and therefore the physicochemical interplay of the present biomolecules (Buera  
42  
43 337 et al., 2005). The retention of labile compounds (enzymes, bioactives, living cells) can also  
44  
45 338 be affected by the type of cations used to control recrystallization of amorphous sugar based  
46  
47 339 dry matrices. For example,  $Mg^{2+}$  and  $K^{+}$  in trehalose-salt based matrices lowered trehalose  
48  
49 340 recrystallization and improved the ability of the matrix to retain  $\beta$ -galactosidase. However,  
50  
51 341 adding  $Mg^{2+}$  to enhance  $\beta$ -carotene retention in freeze-dried gelatin–trehalose matrices via  
52  
53 342 attempting to delay sugar crystallization did not confer any beneficial effects in terms of  
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3 343 storage stability (Elizalde et al. (2002). This implies that benefits from electrolytes also  
4  
5 344 depend on the physicochemical profile of the wall material and its interaction with the  
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7 345 lipophilic components (e.g. changes in gelatin conformation at the lipid droplet interface  
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9  
10 346 induced by  $MgCl_2$ ) may also affect crystallization phenomena (Elizalde et al. 2002).  
11  
12 347 Modifying the sugar composition of maltodextrin-based freeze dried matrices can  
13  
14 348 dramatically change  $\beta$ -carotene stability during storage, due to their impact on  $\alpha$ -relaxation  
15  
16 349 time (solute molecular mobility) and water sorption and phase transition phenomena.  
17  
18 350 Harnkarnsujarit et al. (2012) demonstrated that  $\beta$ -carotene degraded according to the order  
19  
20 351 Fru/Glu/Suc<Glu<Fru<Suc, whilst all systems performed better compared to pure  
21  
22 352 maltodextrin one. This was explained by the sugars' ability to exert higher fluidity due to the  
23  
24 353 increased  $T-T_g$  (Harnkarnsujarit et al., 2012a; Harnkarnsujarit et al., 2012b), resulting in a  
25  
26 354 partial flow and protective coating, reducing porosity and oxygen diffusion.  
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### 30 355 3. Coacervation

31  
32 356 Coacervation refers to salting out or phase separation of lyophilic colloids into liquid  
33  
34 357 microdroplets rather than aggregates (Mellema, 2003). The phase with a higher concentration  
35  
36 358 of colloid components is the coacervate, while the biopolymer depleted phase is the  
37  
38 359 equilibrium solution (de Kruif et al., 2004). Simple and complex coacervation mainly refers  
39  
40 360 to single and at least binary biopolymer systems, respectively. Complex coacervation occurs  
41  
42 361 due to the electrostatic interaction of cationic (gelatin, chitosan, plant proteins) and anionic  
43  
44 362 (pectin, alginate, arabic gum, carboxymethylcellulose) biopolymers (de Kruif et al., 2004;  
45  
46 363 Ducel et al., 2004). At pH conditions at which the polyelectrolytes are oppositely charged the  
47  
48 364 biopolymer solution separates into a coacervated phase in form of microdroplets and a dilute  
49  
50 365 phase. The resulting system is characterized by highly viscous random-coil macromolecules  
51  
52 366 that allow water retention between the interspaces (Strauss and Gibson, 2004). Gelation of  
53  
54 367 the coacervate microdroplets can be achieved in different ways, such as by pH or temperature  
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3 368 change, as well as by adding inorganic electrolytes (Mellema, 2003), producing gelled  
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5 369 microparticles (de Kruif et al., 2004). Hardening the surrounding hydrogel-based shell of the  
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7 370 formed microparticles is usually carried out by chemical or enzymatic cross-linking means to  
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9 371 enhance barrier properties and to achieve sustained release (Gouin, 2004).  
10  
11 372 Compared to other microencapsulation methods such as emulsion templating, extrusion and  
12  
13 373 inclusion complexation, coacervation is more competitive in terms of bioactive throughput  
14  
15 374 (up to 99%), and the microcapsules' release properties under mechanical stress, temperature,  
16  
17 375 and GI conditions, e.g. pH, bile salts, enzymatic activity (de Kruif et al., 2004; Gouin, 2004).  
18  
19 376 However, coacervation is rather expensive and complex, using cross-linking agents that may  
20  
21 377 raise food safety issues, e.g. glutaraldehyde. Operational costs of coacervation can be reduced  
22  
23 378 by implementing inexpensive and straightforward techniques such as spray drying for  
24  
25 379 dehydrating the obtained microcapsules. On the other hand, conventional non-food grade  
26  
27 380 cross-linking agents can be sufficiently substituted by plant phenolics, enzyme cross-linkers  
28  
29 381 such as transglutaminase, or heat-induced molecular complexation (Jones et al., 2009; Lv et  
30  
31 382 al., 2014; Strauss and Gibson, 2004). Strauss and Gibson (2004) demonstrated that  
32  
33 383 polyphenols (from coffee or grape juice) formed cross-links in proteins (gelatin) under  
34  
35 384 oxidizing conditions. The cross-linked gelatin coacervates exerted high mechanical strength  
36  
37 385 and reduced swelling due to the presence of a dense polymer network. Also, the cross-linked  
38  
39 386 microparticles were more lipophilic and heat stable, suggesting an improved ability to uphold  
40  
41 387 lipophilic bioactive compounds without coalescing or disintegration.  
42  
43 388 To date, most of coacervation food applications refer to lipophilic compounds such as flavors  
44  
45 389 (Leclercq et al., 2009; Yang et al., 2014b), essential oils (Gan et al., 2008; Lv et al., 2014;  
46  
47 390 Prata et al., 2008; Sutaphanit and Chitprasert, 2014), oleoresins (Liu et al., 2007a; Zuanon et  
48  
49 391 al., 2013) and carotenoids (Qv et al., 2011; Rocha-Selmi et al., 2013b; SILVA et al., 2012;  
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3 392 Sun et al., 1995). Novel applications for encapsulating sweeteners (Rocha-Selmi et al.,  
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5 393 2013c; Rocha-Selmi et al., 2013a) and living cells (e.g. probiotics) have also been realized.  
6  
7 394 Microencapsulating carotenoids by coacervation is based on their emulsification in an  
8  
9 395 aqueous solution of the two biopolymer phases. Adjustment of pH of the colloid system leads  
10  
11 396 to associative phase separation which triggers the deposition of the coacervate phase around  
12  
13 397 the emulsified lipophilic core material. Carotenoid encapsulation efficiency and stability is  
14  
15 398 influenced by several parameters related to the coacervation process, e.g. pH (due to changes  
16  
17 399 of  $\zeta$ -potential) (SILVA et al., 2012), temperature and type of biopolymers and cross-linking  
20  
21 400 agents, the drying process (Qv et al., 2011; SILVA et al., 2012) and storage conditions (Qv et  
22  
23 401 al., 2011; Rocha-Selmi et al., 2013b; SILVA et al., 2012; Xiao et al., 2014).  
24  
25 402 Gelatin/gum arabic comprises the most common biopolymer blend for coacervation, mainly  
26  
27 403 due to the good interfacial properties of arabic gum (emulsifying the lipid core material) and  
28  
29 404 gelatin due to its acceptable melting behavior, flexibility and mechanical strength along with  
30  
31 405 its high resistance against the proteolytic activity of gastric juice (de Kruif et al., 2004;  
32  
33 406 Mellema, 2003). Encapsulating lutein in freeze dried gelatin/gum arabic coacervates  
34  
35 407 improved its stability under light, high temperature and high RH (Qv and others 2011). It was  
36  
37 408 demonstrated that vitrification significantly affected the structural collapse of the  
38  
39 409 microcapsules and therefore their ability to retain lutein upon storage.  
40  
41 410 The structural collapse and formation of structural imperfections during the drying has also  
42  
43 411 been reported to influence carotenoids encapsulated in gelatine based coacervates. Spray  
44  
45 412 drying appeared more efficient to retain the spherical/structural integrity of the coacervates  
46  
47 413 while freeze drying resulted in surface imperfections such as cracks, creases or fissures (Qv  
48  
49 414 et al., 2011; Rocha-Selmi et al., 2013b; SILVA et al., 2012). On the other hand, freezing can  
50  
51 415 generate carotenoid loaded coacervates via electrostatic interactions of oppositely charged  
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53 416 biopolymers in the cryo-concentrated aqueous phase (Nakagawa and Nagao, 2012).  
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3 417 Nakagawa & Nagao (2012) reported that freezing  $\beta$ -carotene containing emulsions (stabilized  
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5 418 by a blend of gelatin and gum acacia), resulted in core-shell type nanoparticulates enclosing  
6  
7 419  $\beta$ -carotene without affecting the structure of the surrounding membranes, whereas the  
8  
9 420 freezing rate impacted both encapsulation yield and release. On the other hand, freezing of  
10  
11 421 emulsions pre-adjusted to a pH where coacervation is induced may led to partial destruction  
12  
13 422 of the polymeric membranes of the microparticles by penetrating ice crystals.

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15  
16 423 Plant proteins have also been used successfully to develop complex coacervates for  
17  
18 424 encapsulating carotenoids (Xiao et al., 2014). Using chitosan and soy protein isolate to form  
19  
20 425 coacervates containing capsanthin, it was shown that the emulsification conditions  
21  
22 426 (homogenization speed, temperature), the core:wall ratio and wall material concentrations  
23  
24 427 influence microencapsulation yield and efficiency, as well as the microparticulate  
25  
26 428 morphological characteristics. Chitosan led to a noticeable improvement of the polymeric  
27  
28 429 membrane barrier, reducing water vapor and oxygen diffusion while reducing light  
29  
30 430 penetration. However, the hygroscopicity of proteins may be a restrictive factor for  
31  
32 431 stabilizing carotenoids, particularly at high RH (Qv et al., 2011; Xiao et al., 2014).

#### 33 34 35 36 432 **4. Liposomes**

37  
38 433 Liposomes consist of a molecular lipid bilayer that separates the inner aqueous phase from  
39  
40 434 the external continuous water phase. Liposomes are formed via hydrophilic-hydrophobic  
41  
42 435 interactions between an amphiphilic agent, e.g. phospholipids, and water molecules. They play  
43  
44 436 an important role for delivering hydrophobic drugs (Gonnet et al., 2010; Gouin, 2004). For  
45  
46 437 microencapsulation, the bioactive compound is entrapped either in the inner aqueous phase  
47  
48 438 (low loading capacity) or within the membrane (higher loading capacity), the size of carriers  
49  
50 439 varying from 30 nm to a few  $\mu$ m (Zuidam and Shimoni, 2010). Due to the limited chemical  
51  
52 440 and physical stability of liposomes (they easily undergo aggregation, coalescence,  
53  
54 441 phospholipid hydrolysis and oxidation) and low encapsulation efficiency, the formation of  
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3 442 large unilamellar vesicles is preferred for food ingredients (Gouin, 2004), allowing for higher  
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5 443 encapsulation efficiency, smaller capsule size, and higher cost effectiveness.  
6

7 444 In general, liposomes are natural, biodegradable and non-toxic, exert good stability against  
8  
9 445 high  $a_w$ , allow sustained release of bioactive compounds under specific temperature, i.e.  
10  
11 446 above the melting point of phospholipids (ca.180-200°C) (Gouin, 2004). Up-scaling liposome  
12  
13 447 production in their dry state (proliposomes) is particularly relevant for the food industry:  
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15 448 combining liposome formation with drying methods (spray drying, freeze drying,  
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17 449 supercritical fluid precipitation) can be a cost-effective and sustainable alternative for  
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19 450 encapsulation (Alves and Santana, 2004; Moraes et al., 2013; Xia et al., 2012).  
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22  
23 451 Moraes et al. (2013) reported that proliposome technology can be used to develop vehicles  
24  
25 452 for entrapping  $\beta$ -carotene, with very good technological properties (density, solubility, and  
26  
27 453 hygroscopicity) and high encapsulation capacity (up to 100%). Degradation of  $\beta$ -carotene in  
28  
29 454 proliposomes stored under vacuum remained as low as 8% during 60 days of storage, while  
30  
31 455 degradation in powders stored under air was 30%. Thermal degradation during spray drying  
32  
33 456 process, the formation of pre-oxidation products (triggering carotenoid auto-oxidation), the  
34  
35 457 oxygen permeability and the physical state (e.g. glassy or rubbery) of the proliposome matrix  
36  
37 458 have been reported to influence carotenoid storage stability (Moraes et al., 2013). Also  
38  
39 459 reconstituting proliposomes in water, e.g. containing xanthan gum (a liposome stabilizer), is  
40  
41 460 associated with acceptable colloidal stability (in terms of average hydrodynamic volume,  
42  
43 461 polydispersity index and zeta potential) and carotenoid losses of 25% were reported after 100  
44  
45 462 days of storing liposome aqueous suspension at room temperature (Moraes et al., 2013).  
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#### 48 49 50 463 **5. Inclusion complexation**

51  
52 464 CDs ( $\alpha$ -,  $\beta$ - or  $\gamma$ -), are cyclic oligosaccharides which can serve as carriers for incorporated  
53  
54 465 small lipophilic bioactive compounds (Blanch et al., 2007; Kim et al., 2010; Pinho et al.,  
55  
56 466 2014). The encapsulation of carotenoids in CDs is taking place on a supramolecular basis, i.e.  
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3 467 the enthalpy rich water molecules within the CDs are substituted by hydrophobic molecules,  
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5 468 without cleavage or formation of covalent bonds between the CD and the inclusion  
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7 469 compound (IC) (Pinho et al., 2014). The inclusion complexed carotenoids remain in the  
8  
9 470 interior of the CDs central cavity via hydrophobic forces, van der Waals interactions or  
10  
11 471 hydrogen bonds, rendering the inclusion complex thermodynamically stable (Blanch et al.,  
12  
13 472 2007; Mourtzinos et al., 2008; Pinho et al., 2014). CDs are inexpensive and non-toxic, exert  
14  
15 473 very low hygroscopicity and high thermal stability (up to 100°C), they permit taste  
16  
17 474 modification and mask undesired off-flavors, are not absorbed in the upper GI tract and they  
18  
19 475 are completely metabolized by the colon microflora (Szente and Szejtli, 2004).

20  
21  
22 476 Encapsulating carotenoids by CDs can enhance their water solubility, reduce oxidation, light-  
23  
24 477 and heat-induced degradation, or control their release, improving bioavailability (Polyakov et  
25  
26 478 al., 2004; Szente and Szejtli, 2004). The inclusion of  $\alpha$ - and  $\beta$ -carotene, lycopene and lutein  
27  
28 479 in a carotenoid-rich canola oil in  $\alpha$ - and  $\beta$ -CD complexes (molar ratio of CDs : carotenoids  
29  
30 480 1:0.5) enhanced carotene stability in the presence of air (Basu and Vecchio, 2001), and  
31  
32 481 astaxanthin encapsulated  $\beta$ -CD complexes showed 7-9 fold improved stability against heat  
33  
34 482 (65 to 100°C), UV-light, and oxygen (Kim et al., 2010).

35  
36  
37 483 Factors such as stability and release may be fine-tuned by altering CD structure, e.g. ring size  
38  
39 484 ( $\alpha$ -,  $\beta$ - and  $\gamma$ -CDs with 6, 7, and 8 membered sugar-rings, respectively) or  
40  
41 485 hydroxypropylation/methylation (Basu and Vecchio, 2001; Blanch et al., 2007; Huang et al.,  
42  
43 486 2002; Kim et al., 2010; Mele et al., 1998; Pfitzner et al., 2000; Yuan et al., 2013). According  
44  
45 487 to Blanch et al. (2007), the van der Waals surface area of lycopene was associated with the  
46  
47 488 encapsulation efficiency of CDs, with  $\beta$ -CD favoring complexation with *all-trans*-lycopene.  
48  
49 489 Similarly, the inclusion-complexation of CDs with astaxanthin was facilitated for  $\beta$ -CD,  
50  
51 490 decreasing complex mean size compared to native CDs, while no altered structure was found  
52  
53 491 for  $\alpha$ - and  $\gamma$ -CD (Blanch et al., 2007; Kim et al., 2010). In addition to enhancing solubility,  
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3 492 Pfitzner et al., (2000) showed that methyl- $\beta$ -CD complexes possess a high stability against  
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5 493 *cis-trans* isomerization, with all-*trans* isomers being of higher thermodynamic stability than  
6  
7 494 the *cis*-ones. Though additional chemical modification of CDs was reported to favor the  
8  
9 495 formation of ICs, it led to dark colored powder products, indicating poor encapsulating.  
10  
11 496 A method for including bixin rich plant extracts (1:1 ratio) with curcumin in  $\beta$ -CD (1:2 ratio)  
12  
13 497 was investigated (Marcolino et al., 2011). Co-precipitation for complexing curcumin and  
14  
15 498 bixin resulted in the most stable ICs (confirmed by TGA/DSC). Curcumin and bixin  
16  
17 499 complexes exerted high decomposition temperatures and low water evaporation enthalpies,  
18  
19 500 suggesting that the interaction between CDs and carotenoid-rich extracts is energetically  
20  
21 501 favorable, facilitating displacing water molecules from the central cavity of  $\beta$ -CD. Kneading  
22  
23 502 also exhibited a similar behavior to that of co-precipitating  $\beta$ -CD, while simple mixing did  
24  
25 503 not improve stability of the microencapsulated carotenoids.  
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## 30 504 6. Extrusion

31  
32 505 Fabricating microspheres by single or co-extrusion technology comprises entrapping  
33  
34 506 bioactive substance by a biopolymer cross-linked by ionotropic gelation. Though  
35  
36 507 microsphere formation via covalent cross-linking of reactive biopolymers (e.g. alginates,  
37  
38 508 pectins, chitosan or  $\kappa$ -carrageenan) is similar for single or co-extrusion, the techniques are  
39  
40 509 yielding microcapsules of different structure, e.g. matrix in the case of single extrusion and  
41  
42 510 core-shell in the case of co-extrusion. Modifications related to the technical set-up of  
43  
44 511 extrusion devices have also been reported, mainly focusing on the nozzle conformation (i.e.  
45  
46 512 single vs. dual feed) and atomization principle (i.e. stationary, rotating or vibrating) (Zuidam  
47  
48 513 and Shimoni 2010). Both techniques are suitable to produce spherical microcapsules (>160  
49  
50 514  $\mu\text{m}$  to few mm), depending on nozzle geometry, atomization process (jet cutter, vibration  
51  
52 515 nozzle, atomizing disc, electrostatic potential), biopolymer solution viscosity, feed rate, ionic  
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54 516 strength of gelling bath etc. (Zuidam and Shimoni 2010). To date, extrusion has proven to be  
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3 517 one of the most feasible techniques to encapsulate probiotics (Burgain et al., 2011), though  
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5 518 other bioactive compounds have been encapsulated such as hydrophilic (Lupo et al., 2014)  
6  
7 519 and lipophilic polyphenols (Waterhouse et al., 2014), and vitamins (Wichchukit et al., 2013).  
8  
9 520 Finally, extrusion has been successfully implemented for covalently gelled microbeads  
10  
11 521 (Donhowe et al., 2014; Kittikaiwan et al., 2007; Laos et al., 2007; Leach et al., 1998).  
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13 522 Sodium alginate is the most frequently used biopolymer for carotenoid loaded microbead  
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15 523 fabrication, while other biopolymers exerting ionotropic gelation such as furcellaran (a co-  
16  
17 524 polymer of  $\beta$ - and  $\kappa$ -carregeenan) have also been tested. Among the first applications, Leach  
18  
19 525 and others (1998) tested sodium alginate based microbeads for  $\beta$ -carotene encapsulation.  
20  
21 526 Increasing sodium alginate concentration (0.33, 0.47 and 0.73% w/v) decreased  $\beta$ -carotene  
22  
23 527 encapsulation efficiency during the complexation of  $\text{Ca}^{2+}$  with sodium alginate (from 45.5 to  
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25 528 19.1 g/kg from wet beads) and improved its chemical stability during fluidized bed drying  
26  
27 529 (losses declined from 21 to 13%). However,  $\beta$ -carotene chemical stability under detrimental  
28  
29 530 (light/oxygen) and non-detrimental (dark/nitrogen) conditions ameliorated for microbeads  
30  
31 531 comprising 0.33% w/v sodium alginate, indicating lower gas diffusion and light transmission.  
32  
33 532 Moreover, though fluidized bed drying resulted in high  $\beta$ -carotene isomerization (*9-cis*-  
34  
35 533 isomers increased from 36.5 to 50%), the obtained dry microbeads were quite stable against  
36  
37 534 isomerization during storage, depending on alginate concentration (Leach et al., 1998).  
38  
39 535 Recently, spray drying vs. extrusion for  $\beta$ -carotene encapsulation efficiency and release  
40  
41 536 kinetics under simulated digestion was compared (Donhowe et al., 2014). Although spray  
42  
43 537 drying (with maltodextrin as a carrier) resulted in smaller particles than extrusion (chitosan  
44  
45 538 coated alginate microbeads), i.e. 11 vs. 942  $\mu\text{m}$ , extrusion decreased surface deposition  
46  
47 539 (0.0004 vs. 39.5%) and increased encapsulation efficiency (54.7 vs. 37.7%), possibly due to  
48  
49 540 poorer  $\beta$ -carotene emulsification of the spray dried product. High  $\beta$ -carotene encapsulation  
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51 541 efficiency (ca. 97%) was also reported for microbeads comprised of covalently cross-linked  
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3 542 furcellaran with  $\text{Ca}^{2+}$  or  $\text{K}^+$  (Laos et al., 2007). Notably, parameters such as the ionic strength  
4  
5 543 of the cross-linker, the cation type and the carotenoid:biopolymer ratio should be considered  
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7 544 upon microbead formation, as they may impact the mechanical strength of the end-product.  
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10 545 Finally, coating microbeads using film forming biopolymers such as chitosan has been  
11  
12 546 reported to slow down carotenoid degradation during storage (Kittikaiwan et al., 2007). A  
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14 547 five-fold coating of astaxanthin loaded beads using a 1.5% w/v chitosan solution in glacial  
15  
16 548 acetic acid followed by an ionic setting using a  $\text{Na}_5\text{P}_3\text{O}_{10}$  solution led to the formation of a  
17  
18 549 100  $\mu\text{m}$  external film layer, improving the chemical stability of astaxanthin under abusive  
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20  
21 550 storage conditions. The coated pellets were characterized by higher astaxanthin retention  
22  
23 551 (after exposure to light and oxygen) compared to the uncoated systems. Both systems showed  
24  
25 552 notable antioxidant activity (ABTS method), though chitosan coated beads had lower  $\text{IC}_{50}$   
26  
27 553 after 24 weeks of storage (-18 and 30 °C), indicating superior antioxidant capacity.

## 554 NANOENCAPSULATION TECHNOLOGIES

### 555 1. Nano-liquid lipid carriers (LLCs)

556 Incorporating carotenoids into lipid droplets stabilized by an interfacial layer of surface active  
557 compounds is an efficient encapsulation strategy. Though microemulsions have a remarkable  
558 ability to retain lipophilic compounds, nanoemulsions as delivery carriers exert advantages  
559 such as high optical clarity, enhanced physical stability (gravitational separation, droplet  
560 coalescence), processability and bioavailability (Silva et al., 2012). Nanoemulsion generally  
561 refers to colloidal systems of lipid droplets (mean size 10-100 nm) dispersed into a  
562 continuous aqueous phase, stabilized by a surrounding interfacial layer of at least one  
563 emulsifier. Nanoemulsions loaded with carotenoids can be fabricated by their dissolution into  
564 the bulk lipid phase and emulsification into the water phase by high-energy (high pressure  
565 homogenization, microfluidization, sonication, high shearing homogenization) or low-energy  
566 (phase inversion temperature (PIT), solvent displacement, spontaneous emulsification)



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3 567 techniques (Ezhilarasi et al., 2013; Silva et al., 2012). The chemical stability of carotenoids  
4  
5 568 **during** emulsification and storage **depends** on compositional (carotenoid type, type/  
6  
7 569 concentration of the lipid phase, type/content of surfactants, presence of oxygen scavengers  
8  
9 570 etc.), colloidal (particles size, interfacial layer **composition**), intrinsic (pH, ionic strength,  
10  
11 571 droplet surface charge) and extrinsic (light, oxygen, temperature) conditions (Table 3).

### 14 572 *Effect of carrier lipid phase*

16 573 **Interfacial engineering of o/w emulsions**, e.g. tailoring of the emulsion phase domains (lipid,  
17  
18 574 aqueous and interfacial layers) **promote** chemical stability of the active substance. Focusing  
19  
20 575 on the lipid phase, it was shown that the oxidation/degradation patterns of carotenoids present  
21  
22 576 in the bulk (non-emulsified) or emulsified state are considerably different. **Carotenoid**  
23  
24 577 oxidation (in the bulk phase) is governed by oxygen transport in the air/oil interface, while  
25  
26 578 emulsified carotenoids are less prone to oxidation as oxygen transport follows a more  
27  
28 579 complicated pathway including oxygen dissolution in the continuous aqueous phase,  
29  
30 580 partitioning in the oil/water interface and diffusion to the lipid droplet surface. Thus,  
31  
32 581 parameters that control mass transfer (pressure, temperature, aqueous phase microviscosity)  
33  
34 582 or contribute to the formation of colloidal barriers on the lipid droplet surface (thickness and  
35  
36 583 density of the interfacial layers) such as the bulk oil and surface active compounds, do  
37  
38 584 influence carotenoid stability throughout storage.

42 585 **The type of carrier lipid phase is** inextricably associated with the chemical stability of  
43  
44 586 carotenoids, for two **main** reasons. First, the physicochemical properties of the oil interplays  
45  
46 587 with the colloidal aspects of the formed droplets and thus with the partitioning of pro-  
47  
48 588 oxidative components between the water and the oil phase. Second, the oil phase may carry  
49  
50 589 functional groups that are prone to oxidation or minor chemical compounds exerting  
51  
52 590 antioxidant activity, e.g. tocopherols. **Boon and others (2008) studied the impact of the fatty**  
53  
54 591 **acid composition of oils and their antioxidants on lycopene oxidation encapsulated in 5%**  
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3 592 (w/w) o/w corn oil based emulsions. Lycopene was rapidly degraded in stripped (purified)  
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5 593 corn oil emulsions, followed by lycopene dissolved in corn oil and hexadecane. Presumably,  
6  
7 594 the naturally inherent antioxidants in the oil provided protection of carotenoids against  
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9  
10 595 degradation. However, at the end of the storage trials, losses of ca. 80% of the initial  
11  
12 596 carotenoid amount were observed. On the other hand, the reduced formation of secondary  
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14 597 oxidation products such as hexanal (observed in the emulsified corn oil systems compared to  
15  
16 598 the stripped or bulk corn oil), suggested that both the emulsification and the chemical  
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18 599 composition of the oil carrier can enhance the ability of lycopene to quench alkoxy radicals,  
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20  
21 600 inhibiting  $\beta$ -scission reaction producing hexanal.

22  
23 601 Szterk and others (2013) affirmed that  $\beta$ -carotene stability emulsified in refined palm olein,  
24  
25 602 linseed oil or rapeseed oil strongly depended on the susceptibility of the bulk lipid phase (oil  
26  
27 603 + carotenoids) to autoxidation. Highest  $\beta$ -carotene stability (12 wks, 2 °C) was found with  
28  
29 604 emulsified in palm olein, and lowest in linseed oil (higher PUFA content). A negative  
30  
31 605 correlation between the amount retained  $\beta$ -carotene and formed hydro-peroxides (PV) was  
32  
33 606 detected, underlining carotenoid antioxidant capacity.

#### 34 35 36 607 *Effect of surfactant type and content*

37  
38 608 Testing the effect of various polysorbates (Tweens 20, 40, 60 and 80) on the colloidal and  
39  
40 609 chemical stability of nanoemulsions containing  $\beta$ -carotene (Yuan and others (2008), Tween  
41  
42 610 20 induced the greatest size reduction, resulting in droplets of 132 to 173 nm, with finer  
43  
44 611 particles being obtained at highest surfactant amounts (12% w/w). Milk proteins (sodium  
45  
46 612 caseinate and whey proteins) were successfully adopted to produce physically and chemically  
47  
48 613 stable nanoemulsions containing carotenoids. Qian and others (2012a) used  $\beta$ -lactoglobulin  
49  
50 614 (2% w/w) as the primary surfactant in orange oil based o/w nanoemulsions (10% w/w oil)  
51  
52 615 containing  $\beta$ -carotene. Storage (2 wks at 5, 20, 37 and 55 °C) of the emulsions showed that  $\beta$ -  
53  
54 616 carotene content decreased by 43 to 100% with increasing temperature. Particle size analysis

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3 617 affirmed that higher temperature reduced their physical stability, primarily associated with  
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5 618 the ability of the globular proteins to undergo conformational transitions, favoring  
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7 619 hydrophobic interactions between the lipid droplets, leading to their flocculation. In the same  
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10 620 study,  $\beta$ -lactoglobulin exerted improved carotenoid retention compared to Tween 20, perhaps  
11  
12 621 due to the free radical scavenging ability of  $\beta$ -lactoglobulin at the oil-water interface (via  
13  
14 622 cysteine residues, disulfide bonds and thiol groups), its ability to form complexes with  
15  
16 623 carotenoids, and to improve the barrier properties of the interfacial layers surrounding the  
17  
18 624 lipid droplets (Qian et al., 2012b). In a successive study, WPI (0.5% w/w) was used to  
19  
20 625 stabilize 5% w/w MCT based o/w emulsions containing  $\beta$ -carotene (Xu et al., 2013b).  
21  
22 626 Storing the emulsions (55°C, 7 days) induced a pH and ionic strength dependent degradation  
23  
24 627 of  $\beta$ -carotene. Some amino acids, e.g. cysteine, tryptophan, and methionine, present in WPI,  
25  
26 628 may act as free radical scavenging and metal-chelating agents and WPI antioxidant ability is  
27  
28 629 controlled by the reactivity of free amino groups with carotenoid peroxy radicals.  
29  
30 630 Yi and others (2014) investigated sodium caseinate as a physical and chemical stabilizing  
31  
32 631 agent in o/w (10% w/w) emulsions containing  $\beta$ -carotene homogenized at different pressures  
33  
34 632 (10-103 MPa). Beta-carotene degradation exhibited a linear pattern over storage time (30  
35  
36 633 days, 25°C) with highly pressurized systems being the most unstable. Caseins are known to  
37  
38 634 control lipid oxidation by reducing the accessibility of metal ions or other pro-oxidants to  
39  
40 635 unsaturated fatty acids and carotenoids, and by binding ferric ions, shifting the equilibrium  
41  
42 636 from the hydroperoxide forming ferrous to ferric iron (Díaz et al., 2003; Yi et al., 2014).  
43  
44 637 However, producing very fine lipid droplets triggers carotenoid oxidation due to increased  
45  
46 638 surface area, minimizing the protective role of absorbed caseins (Yi et al., 2014).  
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51 639 Hydrophobically modified starch or maltodextrins and surface active polysaccharides (e.g.  
52  
53 640 arabic gum, pectins) can also be used as primary emulsifiers in nanoemulsions containing  
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55 641 lipophilic substances. Liang et al. (2013a) investigated the impact of sodium octenyl succinic  
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3 642 acid (OSA) modified starches on  $\beta$ -carotene stability. The starches' molecular properties  
4  
5 643 (molecular weight (MW), radius of gyration and dispersed molecular density) interfered with  
6  
7 644  $\beta$ -carotene degradation only at ambient storage (i.e. 25 °C), light and oxygen. Starches of high  
8  
9 645 MW and dispersed molecular density were associated with higher  $\beta$ -carotene retention during  
10  
11 646 30 days of storage, attributed to the starches' ability to form thicker and denser interfacial  
12  
13 647 layers surrounding the lipid droplets, providing a physical barrier against oxidation. However,  
14  
15 648 no significant differences in  $\beta$ -carotene retention were detected with OSA-modified starch  
16  
17 649 stabilized nanoemulsions stored at 4 °C in the absence of light and oxygen.

### 20 650 *Impact of pH and ionic strength*

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22  
23 651 Processing LLC containing carotenoids (blending with acidic formulations, salt or sugars)  
24  
25 652 may modify pH and ionic strength, directly influencing the physical stability of emulsions  
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27 653 (inducing droplet flocculation, phase separation or creaming), and indirectly the chemical  
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29 654 stability of carotenoids (Qian et al., 2012b; Xu et al., 2013a; Xu et al., 2013b; Yi et al., 2014).  
30  
31 655 For example, acidic conditions may produce ion-pairs that dissociate, forming carotenoid  
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33 656 carbocations undergoing cis-trans isomerization and degradation (Boon et al., 2010). Qian et  
34  
35 657 al. (2012a) reported that exposing emulsified  $\beta$ -carotene to pH 3-7 altered its degradation  
36  
37 658 kinetics at 25 °C, with acidic pH causing highest degradation, corroborating observations by  
38  
39 659 Boon et al., (2009) using hexadecane (5% w/w) based emulsions containing lycopene. Losses  
40  
41 660 at pH 7 and 3 during incubation (94 h, 15 °C) amounted to ca. 50% and 98%, respectively.  
42  
43 661 Carotenoid instability at acidic pH was attributed to formed ion-pairs promoting carotenoid  
44  
45 662 isomerization, increasing iron solubility, the binding of iron to the surface of emulsion  
46  
47 663 droplets, and metal-lipid interactions and oxidation reactions (Boon et al., 2009).  
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49  
50 664 Interfacial coating modification of the lipid droplets can improve the stability of emulsified  
51  
52 665 carotenoids (Xu and others 2013a,b). Whey proteins on the lipid droplet surface slightly  
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54 666 improved the stability of  $\beta$ -carotene containing nanoemulsions stored for 7 days at 55 °C. In  
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3 667 general,  $\beta$ -carotene degradation was higher at  $\text{pH} < \text{pI}$  for whey proteins, attributed to pH-  
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5 668 dependent changes of colloidal aspects of the emulsions. Emulsions adjusted to a pH of 6-7  
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7 669 exerted higher  $\beta$ -carotene retention (29-34%) vs. systems with a pH of 3-4 (21-12%). Though  
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9 670 the high stability of carotenoids at  $\text{pH} > \text{pI}$  appears to be associated with the binding of soluble  
10  
11 671 iron in the water-oil interface, the increased stability at low pH was attributed to their higher  
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13 672 cationic charge density, facilitating repulsive interactions with pro-oxidant metals (Xu and  
14  
15 673 others 2013b). Similarly, forming complex interfaces on lipid droplets, e.g. beet pectin-whey  
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17 674 protein isolate conjugates, enhanced  $\beta$ -carotene retention (Xu and others 2013a). However,  
18  
19 675 the stabilizing effect of protein-pectin conjugates was superior at pH 7 than under acidic  
20  
21 676 conditions. For a certain pH, no significant differences in the surface charge of lipid droplets  
22  
23 677 were detected, suggesting that the antioxidant role of protein-polysaccharide conjugates  
24  
25 678 emanates from their ability to create a dense and cohesive interfacial layer, preventing the  
26  
27 679 penetration of pro-oxidants (iron ions, free-radicals) present in the aqueous phase (Xu and  
28  
29 680 others 2013a). Thus, though ionic strength plays is important for reducing electrostatic  
30  
31 681 repulsions between lipid droplets, favoring particle aggregation via van der Waals and  
32  
33 682 hydrophobic attraction, increased salt concentration may improve the stability of carotenoids  
34  
35 683 in nanoemulsions. Qian et al. (2012a) reported enhanced  $\beta$ -carotene retention in  
36  
37 684 nanoemulsions (stored at 55°C for 7 days) when sodium chloride (400-500 mM) was added.

#### 685 *Presence of pro-oxidant scavengers*

686 Carotenoid oxidation in nanoemulsions can be triggered by many factors such as heat, light,  
687 singlet oxygen, transition metals and free radicals. Carotenoid autoxidation results in the  
688 formation of reaction products such as epoxides, endoperoxides, apocarotenals and  
689 apocarotenones (Krinsky and Yeum, 2003), with altered or decreased biological activity. Two  
690 groups of antioxidants are used to control carotenoid autoxidation: singlet oxygen or free  
691 radical scavengers and transition metal chelators. Depending on processing conditions,

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3 692 transition metals can be found either in aqueous phases or in oil-water interfaces. Emulsions  
4  
5 693 containing 200 and 500 mM of desferoxamine (an iron chelator) enhanced  $\beta$ -carotene content  
6  
7 694 after storage by 25% and 37% (7 days, 55°C) compared to nanoemulsions without chelator.  
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9 695 EDTA, even at low levels (1 mM), pronouncedly influenced the color stability of  $\beta$ -carotene  
10  
11 696 containing emulsions (Qian et al., 2012b). EDTA may prevent metal redox cycling, the  
12  
13 697 formation of insoluble metal complexes, the occupation of metal coordination sites, and  
14  
15 698 sterically hinder the interaction between metals and lipid substrates (Decker 1998). A similar  
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17 699 pro-oxidant scavenging activity for EDTA was reported for other carotenoids, e.g. for  
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19 700 lycopene (Boon et al., 2009). Contrarily, Bou et al. (2011) demonstrated that the effectiveness  
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21 701 of metal chelators not only depended on their amount, but also on the surface charge of lipid  
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23 702 droplets and pH, as well as the acid dissociation constant (pKa) of the metal chelating agents.  
24  
25 703 Using Tween 20, Bou et al. (2011) showed that lycopene retention in 5% w/w emulsions was  
26  
27 704 superior in systems without metal chelators compared to those containing EDTA, citric acid  
28  
29 705 or tripolyphosphate. The poor effectiveness of EDTA was attributed to its ability to increase  
30  
31 706 the solubility of ferric iron, favoring its interaction with lycopene, inducing autoxidation.  
32  
33 707 Qian et al. (2012b) investigated the impact of water (ascorbic acid) and oil soluble ( $\alpha$ -  
34  
35 708 tocopherol acetate, coenzyme Q10) antioxidants on the degradation of  $\beta$ -carotene  
36  
37 709 encapsulated in 10% corn oil (w/w) –  $\beta$ -lactoglobulin stabilized nanoemulsions. Though  
38  
39 710 ascorbic acid and coenzyme Q10 controlled  $\beta$ -carotene stability throughout storage (55°C, 15  
40  
41 711 days), different prooxidant-scavenging mechanisms were observed. While polar compounds  
42  
43 712 can act as prooxidant-scavengers via their ability to absorb to oil-water interfaces (where they  
44  
45 713 come into contact with peroxy radicals) or by chelating transition metals in the water phase,  
46  
47 714 lipophilic compounds mainly act as free radicals scavengers at the lipid droplet surface.  
48  
49 715 Research on  $\alpha$ -tocopherol pro-oxidant scavenging activity in nanoemulsions containing  
50  
51 716 carotenoids resulted in contradictory findings. According to Bou et al. (2011),  $\alpha$ -tocopherol  
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3 717 exerted the most pronounced carotenoid retention compared to more polar antioxidants  
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5 718 (gallic acid, propyl gallate). Contrarily, Qian et al., (2012b) reported that  $\alpha$ -tocopherol  
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7 719 conferred only minor scavenging activity compared to ascorbic acid and coenzyme Q10.  
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9  
10 720 Interestingly, Xu et al. (2013a) demonstrated that the antioxidant ability of  $\alpha$ -tocopherol (200  
11  
12 721 vs. 500 mg/kg) in nanoemulsions containing  $\beta$ -carotene stabilized by protein-polysaccharide  
13  
14 722 conjugates strongly depended on the pH, with free radical scavenging action increasing with  
15  
16 723 pH, with acidic conditions (pH 4) not showing improved carotenoid retention.

## 18 724 2. Nanoencapsulation using supercritical fluids

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21 725 A supercritical fluid (SCF) is a dense liquid with the physicochemical properties of gases.  
22  
23 726 Close to its critical point the fluids' solubility, viscosity, diffusivity, and thermal conductivity  
24  
25 727 change radically (Taleb 2010). Employing SFCs is an emerging method to extract and purify  
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27 728 heat labile compounds, as well as for the structural design of particles (Jung and Perrut, 2001;  
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29 729 Mattea et al., 2009b). SFC particle design is advantageous over conventional precipitation as  
30  
31 730 it promotes good particle size and morphology control, reduces isomerization and thermal  
32  
33 731 degradation of heat labile compounds, improves encapsulation and precipitation yield and  
34  
35 732 minimizes harmful chemical residues (Santos and Meireles, 2010). CO<sub>2</sub> is predominantly  
36  
37 733 used as an anti-solvent for food applications, exerting a low critical point temperature ( $T_c =$   
38  
39 734 31.1 °C,  $P_c = 7.38$  MPa), is non-toxic, inflammable, inexpensive, relatively inert, has  
40  
41 735 adjustable solvent power/selectivity and can easily be eliminated from the food matrix  
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43 736 (Gutiérrez et al., 2013; Santos and Meireles, 2010) by evaporation.

44  
45 737 Supercritical fluid precipitation techniques for carotenoid nanoencapsulation can be divided  
46  
47 738 into five main categories (Jung and Perrut, 2001; Mattea et al., 2009a): rapid expansion of  
48  
49 739 supercritical fluids (RESS), gas anti-solvent (GAS), supercritical anti-solvent (SAS/SEDS),  
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51 740 particles from gas-saturated solutions (PGSS), and supercritical extraction from an emulsion  
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53 741 (SFEE). Several factors can influence the physical state, morphology, mean particle size of  
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3 742 encapsulates, and micro-encapsulation efficiency, including pressure and temperature of the  
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5 743 supercritical fluid, the geometry of the precipitation vessel and the atomization nozzle, the  
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7 744 anti-solvent flow rate, type (e.g. emulsion, suspension, solution) and flow rate of the carrier  
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9 745 aliquot system, the carotenoid type and the carotenoid: wall material ratio (Table 2).  
10  
11 746 RESS assisted encapsulation uses the solvation power of supercritical fluids by adjusting  
12  
13 747 pressure and temperature. The bioactive compound and the polymeric coating material are  
14  
15 748 co-dissolved in supercritical CO<sub>2</sub> and then co-precipitated via rapid depressurization of the  
16  
17 749 obtained organic solution through a nozzle (Cocero et al., 2009; Jung and Perrut, 2001). The  
18  
19 750 poor solubility of many active substances and coating materials in supercritical CO<sub>2</sub> is the  
20  
21 751 major drawback of RESS (Cocero et al., 2009). In addition, the morphology and particle size  
22  
23 752 and thereby the bioactive payload are difficult to control, as co-precipitation is a rapid  
24  
25 753 process. Though RESS is scarcely used to encapsulate food bioactives, its feasibility for  
26  
27 754 micronization and encapsulation of carotenoids (astaxanthin) and organic pigments (rutin,  
28  
29 755 anthocyanins and quercetin) has been demonstrated (QUAN et al., 2009; Santos and  
30  
31 756 Meireles, 2013). Quan et al. (2009) showed that RESS assisted micronization of astaxanthin  
32  
33 757 produced small sphere-like particles (mean particle size 0.5 µm), being almost 10 times  
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35 758 smaller than microparticles obtained by solvent (n-hexane) assisted crystallization. Low  
36  
37 759 pressure and high temperature pre-expansion facilitated the formation of tiny particles,  
38  
39 760 possibly due to decreased critical nuclei size and increased concentration during atomization.  
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41 761 Studying rutin, it was demonstrated that the bioactive substance solubility in the supercritical  
42  
43 762 solvent (CO<sub>2</sub> with ethanol) determines the encapsulation mechanism and efficiency, particle  
44  
45 763 mean size and morphology. For bioactives with low solubility in the supercritical solvent, the  
46  
47 764 core material is not dissolved but suspended in the continuous phase. Upon expansion,  
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49 765 encapsulation is completed by depositing coating material on the suspended particles,  
50  
51 766 creating a polymeric layer on the particles' surface (Santos and Meireles, 2013).  
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3 767 The PGSS process consists of saturating a solution with the bioactive compound, using a  
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5 768 supercritical fluid. The gas-saturated solution is expanded under atmospheric pressure  
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7 769 through an atomization nozzle, the resulting vaporization of the dissolved gas induces cooling  
8  
9 770 of the solution (Joule-Thomson effect), promoting nucleation and precipitation (Martín and  
10  
11 771 Weidner, 2010). An advantage of the PGSS is that it allows particle formation from aqueous  
12  
13 772 solutions, and the combination with conventional drying methods, e.g. spray drying. Due to  
14  
15 773 the efficient atomization and the remarkably lower temperatures implemented in the spray  
16  
17 774 tower, PGSS is useful for carriers with low melting points (close to room temperature) or heat  
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19 775 sensitive bioactives (de Paz et al., 2012b; de Paz et al., 2012a; Martín and Weidner, 2010).  
20  
21 776 However, the mean size of the obtained particles is generally larger than those obtained by  
22  
23 777 other supercritical fluid based techniques, ranging from a few to several hundred microns.  
24  
25 778 Recently, encapsulating carotenoids by PGSS has been realized using soybean lecithin and  
26  
27 779 poly- $\epsilon$ -caprolactones (de Paz et al., 2012b; de Paz et al., 2012a). Using poly- $\epsilon$ -caprolactones  
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29 780 of low ( $4000 \text{ g mol}^{-1}$ ) and high MW ( $10000 \text{ g mol}^{-1}$ ) for  $\beta$ -carotene encapsulation was  
30  
31 781 challenging as apart from the MW, a thorough control of the operating conditions in the  
32  
33 782 precipitation vessel (homogenization time, pressure and temperature) and the molar ratio of  
34  
35 783  $\beta$ -carotene:polymeric carrier is required (de Paz et al., 2012b). Low MW polymers can  
36  
37 784 drastically improve encapsulation parameters (process yield, particle mean size,  
38  
39 785 agglomeration phenomena,  $\beta$ -carotene payload). This has mainly been attributed to the lower  
40  
41 786 viscosity (1690 vs. 9300 mPa\*s) and higher solubility in supercritical  $\text{CO}_2$  (2.7 vs. 5.4%  
42  
43 787 w/w). Thus, atomization is facilitated and the higher amount of solubilized supercritical gas  
44  
45 788 favors smaller droplets/smaller particle formation during the expansion in the nozzle.  
46  
47 789 However, compared to SFEE, PGSS appears inferior regarding encapsulation efficiency and  
48  
49 790 technological/morphological properties of the produced particles. De Paz et al. (2012a)  
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51 791 studied the effectiveness of PGSS combined with liposome technology to produce pro-  
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3 792 liposomes loaded with  $\beta$ -carotene. The process yield was higher (20-50%) compared to that  
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5 793 of the PGSS-poly- $\epsilon$ -caprolactone method (5-44%), whereas encapsulation efficiency ranged  
6  
7 794 from 40-60%. Particle size and morphology were influenced by the pre-expansion pressure  
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9  
10 795 and temperature in the homogenization vessel, with high pressure and low temperature  
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12 796 **reducing droplet size** during atomization. **It was also** demonstrated that increased gas to  
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14 797 product and lecithin to  $\beta$ -carotene ratios can hinder atomization, due to increased viscosity of  
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16 798 the gas saturated solution. However, the increased lecithin content in the solution improved  
17  
18 799 the encapsulation efficiency, by reducing interfacial tension of the gas saturated solution,  
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20 800 facilitating the interplay at the oil-water interfaces, forming a core surrounding shell that can  
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22  
23 801 be **soundly** maintained even during the expansion step. The reconstituted pro-liposomes in  
24  
25 802 water **produced** liposomes of 1-5  $\mu\text{m}$  mean size and of multilamellar structure, with  $\beta$ -  
26  
27 803 carotene being entrapped in the hydrophobic region (internal space of the lipid bilayer).  
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29  
30 804 **SAS/SEDS are based on mixing** a supercritical fluid **stream of a** desired temperature and  
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32 805 pressure conditions with a solution to induce recrystallization due to supersaturation (Cocero  
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34 806 et al., 2009; Mattea et al., 2009a). SAS/SEDS was successfully applied (Fig. 2) to carotenoid  
35  
36 807 extraction/micronization and encapsulation (Table 2) (Davarnnejad et al., 2008; Franceschi et  
37  
38 808 al., 2009; Miguel et al., 2006; Santos and Meireles, 2013). The encapsulation efficiency of  
39  
40 809 SAS/SEDS as well as the particles' size and morphological characteristics depend on several  
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42 810 parameters, e.g. the affinity between the core/coating compounds, the core to coating material  
43  
44 811 ratio, the pre-expansion pressure and temperature as well as the anti-solvent flow rate  
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46 812 (Franceschi et al., 2008; Martín et al., 2007). Co-precipitation with  $\beta$ -carotene and lutein  
47  
48 813 revealed that the encapsulation efficiency was affected by the type of carotenoid,  $\text{CO}_2$  flow  
49  
50 814 rate and core to coating ratio. Though in both cases prismatic/needle-like carotenoid particles  
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52 815 were covered by amorphous spherical PEG particles, lutein encapsulation efficiency  
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54 816 increased with high  $\text{CO}_2$  flow rates and high polymer:carotenoid ratios.  
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3 817 Franceschi et al. (2008) investigated the impact of pressure, solution, and anti-solvent flow  
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5 818 rate on the encapsulation efficiency and morphology of  $\beta$ -carotene – PHBV (poly-3-  
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7 819 hydroxybutyrate-*co*-hydroxyvalerate) SEDS co-precipitates. The formation of small particles  
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10 820 with good  $\beta$ -carotene coverage improved at high pressure and low solution flow rates, which  
11  
12 821 was attributed low viscosity **of the** solution and enhanced mass transfer and diffusion rates of  
13  
14 822 CO<sub>2</sub> to and from the droplets during **atomization**/depressurization. Corroborating previous  
15  
16 823 studies, the reduced  $\beta$ -carotene:PHBV ratio **also** reduced encapsulation efficiency and  
17  
18 824 increased surface deposited carotenoids due to the faster precipitation of the polymeric  
19  
20 825 material (Franceschi et al., 2008; Priamo et al., 2010). Successive studies on  $\beta$ -carotene- and  
21  
22 826 astaxanthin-PHBV SEDS produced nanoparticulates (Machado Jr et al., 2014; Priamo et al.,  
23  
24 827 2011; Priamo et al., 2010) confirmed that the encapsulation efficiency and the percentage of  
25  
26 828 carotenoids entrapped in the polymeric matrix were maximal at highest pressure (20 and 10  
27  
28 829 MPa, respectively) and carotenoid concentration in the organic solution (~1:1 and 1:2  $\beta$ -  
29  
30 830 carotene and astaxanthin to PHBV ratio).  $\beta$ -Carotene release in the organic phase depended  
31  
32 831 on the used solvent type **(being faster for ethyl acetate and n-hexane than for ethanol) and the**  
33  
34 832 **loaded bioactive amount** (Priamo et al., 2011).

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38 833 Pre-expansion temperature plays an important role for **co-precipitating** active substances with  
39  
40 834 biopolymers. Operating precipitation vessels at high temperature (above the glass transition  
41  
42 835 temperature of the coating material) can result in obstructed particle formation, development  
43  
44 836 of fibrous, film-like or highly agglomerated **particles** (Nalawade et al., 2006). Mattea et al.  
45  
46 837 (2008) studied the effect of temperature on the **morphology** of  $\beta$ -carotene loaded PEG  
47  
48 838 microparticles produced by SEDS. **Fabricating** microparticles was arduous above 288K, due  
49  
50 839 to strong agglomeration and film forming phenomena, **due** to the apparition of a liquid-liquid  
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52 840 phase instead of a supercritical phase, thus supersaturation and precipitation kinetics were  
53  
54 841 considerably slowed down. Experiments at a constant temperature of 288K (threshold for  
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3 842 particle precipitation) and increasing the PEG :  $\beta$ -carotene ratio improved coverage of the  
4  
5 843 precipitated carotenoid particles and transition from the initial irregular structure to hollow  
6  
7 844 spheres and finally to concavity-absent microspheres (Mattea et al., 2008).  
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9  
10 845 Proteins can also constitute carotenoid co-precipitants as they facilitate absorption on their  
11  
12 846 interfaces, and due to their good sustained released properties. Zein constituted a primary  
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14 847 substrate for lutein encapsulation by SEDS (Hu et al., 2012). Lutein encapsulation efficiency  
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16 848 increased with higher pressure, temperature, and decreased lutein:zein ratio. Adopting these  
17  
18 849 conditions, morphological (from large spherical particles with less agglomeration to uniform  
19  
20 850 nanospheres) and particle size changes (198 to 355 nm) were also observed. The lutein-zein  
21  
22 851 blend and their SEDS co-precipitate (10MPa, 45°C, 1:18) showed a glass transition region  
23  
24 852 (50-80°C) in both systems, though a clear lutein melting peak ( $T_m$  180-190°C) was observed  
25  
26 853 only for the zein-lutein blend, indicating that zein with lutein was embedded in the  
27  
28 854 amorphous state, as well as good thermodynamical compatibility of both materials (lutein-  
29  
30 855 zein interactions via intermolecular hydrogen bonds). Finally, the SEDS zein-lutein co-  
31  
32 856 precipitate exhibited slower release in PBS with no detectable burst point (near zero order  
33  
34 857 kinetics), contrarily to pure lutein or lutein-zein blends, revealing that the release of the SEDS  
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36 858 zein-lutein precipitate was associated with water molecule diffusion to the matrix, increasing  
37  
38 859 zein polymeric network interspaces, facilitating diffusion of lutein to the bulk aqueous phase.  
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41 860 SAS/SEDS techniques have also been successfully combined with other microencapsulation  
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43 861 technologies such as liposome or inclusion-complexation (Lesoin et al., 2011; Nerome et al.,  
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45 862 2013; Xia et al., 2012). SAS implementation to produce pro-liposomes may bring advantages  
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47 863 compared to conventional organic solvent methods (Bangham method), as it is more efficient,  
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49 864 environmental-friendly, is carried out under mild temperature, and reduces the amount of  
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51 865 residual organic solvent in the final dry product (Lesoin et al., (2011). However, no  
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3 866 significant differences were noticed between SAS and the Bangham process in terms of  
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5 867 encapsulation efficiency (approx. 20%), liposome storage stability and mean particle size.  
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7 868 Xia et al. (2012) presented a SEDS assisted method to produce lutein loaded pro-liposomes.  
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10 869 Lutein loading of the carrier substrate was pressure – temperature dependent; operating  
11  
12 870 conditions of 35°C and 8 MPa provided highest encapsulation efficiency (90%). The SEDS  
13  
14 871 obtained microparticles were free flowing microspheres of 100–300 nm diameter, due to the  
15  
16 872 ability of CO<sub>2</sub> to form a single phase, increasing nucleation rates. Nerome et al. (2013)  
17  
18 873 introduced an SEDS assisted method to produce lycopene/β-CD inclusion complexes in dry  
19  
20 874 form, resulting in nanoparticles with a mean size of 40-150 μm, depending on phase  
21  
22 875 equilibria conditions (pressure, temperature) and organic solution and anti-solvent flow rates.  
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24 876 High pressure, temperature and solution flow rate resulted in smaller, uniform and spherical  
25  
26 877 particles due to enhanced lycopene solubility in the solvent phase (DMF), and a turbulent  
27  
28 878 flow in the jet edge region, promoting supersaturation and droplet break-up.  
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31 879 SFEE is an alternative to emulsion templating/precipitation methods where the bioactives  
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33 880 incorporated in o/w emulsions are recrystallized, implementing the supercritical anti-solvent  
34  
35 881 method. SFEE is considered advantageous over conventional emulsion templating techniques  
36  
37 882 due to reduced amounts of organic solvents needed during the precipitation process.  
38  
39 883 Moreover, SFEE overcomes the challenges related to SAS, that is, the difficulty to produce  
40  
41 884 small (nanoscale) particles and the tendency of the obtained powders to agglomerate (Mattea  
42  
43 885 et al., 2009a). The presence of surface active compounds in the emulsion promotes  
44  
45 886 nanoparticle formation without agglomeration, while their growth is restricted due to high  
46  
47 887 nucleation rates (Mattea et al., 2009a).  
48  
49 888 Santos et al. (2012) produced nanoparticles containing β-carotene or lycopene by SFEE. An  
50  
51 889 increased emulsion flow (from 2.5 to 4.5 mL/min) was found to be associated with improved  
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53 890 encapsulation efficiency (61 to 89% and 34 to 71% for β-carotene and lycopene, respectively)  
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3 891 though isomerization also increased slightly. The lower encapsulation efficiency of lycopene  
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5 892 was mainly attributed to its higher solubility in supercritical CO<sub>2</sub> and better partitioning in the  
6  
7 893 antisolvent phase), but differences in the nucleation rate, particle specific surface area, and  
8  
9 894 interactions between the carrier and carotenoids were also stated.  
10  
11 895 However, carotenoid isomerization during SFEE processing seems to occur mainly during  
12  
13 896 solvent extraction, i.e. after particle formation (Mattea et al., 2009b), as increased emulsion  
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15 897 flow rates lead to prolonged solvent extraction and higher isomerization (Santos et al., 2012).  
16  
17 898 Using SFEE, pressure and temperature remarkably effected both encapsulation efficiency and  
18  
19 899 isomerization of carotenoids ( $\beta$ -carotene, lycopene, astaxanthin) (Mezzomo et al., 2012;  
20  
21 900 Santos et al., 2012). An optimum temperature and pressure needs to be found to maximize  
22  
23 901 encapsulation efficiency, as they influence thermodynamic properties of carotenoids and  
24  
25 902 coating material (Mezzomo et al., 2012). While low pressure reduces carotenoid solubility in  
26  
27 903 the antisolvent phase (de la Fuente et al., 2006), higher pressure may prevent film formation  
28  
29 904 of the polymeric coating material (Mezzomo et al., 2012). It should also be emphasized that  
30  
31 905 the encapsulation carrier and carotenoid strongly determine the impact of pressure on the  
32  
33 906 encapsulation efficiency, using SFEE. Depending on the carotenoid, pressure may influence  
34  
35 907 carotenoid trans-cis-isomerization, though literature data are contradictory. While Santos et  
36  
37 908 al. (2012) reported that a pressure increase from 7 to 13 MPa reduced lycopene isomerization  
38  
39 909 (from 2 to 0.02%), an increase of cis-isomers was reported at higher pressure operating  
40  
41 910 conditions, i.e. 20 to 40 MPa (Yi et al., 2009). Though it is unclear how pressure influences  
42  
43 911 isomerization, the increased density of the antisolvent phase (increased pressure in the  
44  
45 912 precipitation vessel) may be the key point (Santos et al., 2012).  
46  
47 913 SFEE appears also efficient to maintain carotenoid storage stability (de Paz et al., 2013;  
48  
49 914 Mezzomo et al., 2012; Santos et al., 2012). Mezzomo and others (2012) compared the  
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51 915 stability of astaxanthin in systems prepared by reconstituting SFEE or SAS co-precipitates,  
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3 916 reporting that the SFEE obtained systems exhibited the highest stability (7 days of storage),  
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5 917 whereas the stability of SAS derived systems strictly depended on supercritical co-  
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7 918 precipitation conditions and astaxanthin extract concentration. In addition to high  
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9 919 encapsulation efficiency, small particle size and enhanced morphological features, the carrier  
10  
11 920 type may also influence the storage stability of carotenoid nanoparticulates produced by  
12  
13 921 SFEE. de Paz et al. (2013) revealed that  $\beta$ -carotene retention in SFEE received freeze-dried  
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15 922 nanoparticles improved with high MW/high melting point poly- $\epsilon$ -caprolactones compared to  
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17 923 lower MW/melting point analogues.

### 20 924 **3. Protein self-assembled nanoparticles**

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23 925 The broad range of techno-functional and physicochemical properties of proteins renders  
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25 926 them as natural vehicles for the encapsulation and sustained release of bioactive compounds.  
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27 927 Ion binding, binding of hydrophobic compounds, surface active properties, ability to form  
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29 928 molecular self- or co-assemblies, complexation with oppositely charged polysaccharides, acid  
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31 929 or heat induced gelation, pH triggered gel swelling, adsorption at the air/water or oil/water  
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33 930 interfaces, formation of covalent conjugates via Maillard reaction, UV light absorbance, and  
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35 931 enhanced bioavailability by controlling the access of digestive enzymes are the most  
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37 932 important properties of proteins for constituting effective carriers to deliver bioactive  
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39 933 compounds and living cells (e.g. probiotic bacteria) to the human host (Livney, 2010).  
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41 934 For instance, milk proteins (casein micelles,  $\beta$ -lactoglobulin) are well known for their  
42  
43 935 excellent self-assembly/co-assembly properties (Fig. 4). The formed protein nano-vehicles  
44  
45 936 can easily be loaded with lipophilic bioactive compounds and provide an effective physical  
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47 937 barrier against harsh environmental conditions (Livney, 2010; Zimet et al., 2011; Zimet and  
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49 938 Livney, 2009). Proteins are further widely available, inexpensive, have high nutritional value  
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51 939 and satisfactory sensory characteristics and are generally recognized as safe (GRAS).  
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3 940 Casein micelles are clusters of  $\alpha$ -,  $\beta$ - and  $\kappa$ -caseins, **stabilized** by hydrophobic interactions  
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5 941 and serine-calcium **phosphate bridges**. The micelles are further electrostatically and sterically  
6  
7 942 stabilized by  $\kappa$ -casein “hairy” layers on the micelle surface. Encapsulating lipophilic  
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10 943 compounds in casein nanoparticles can be achieved via two main strategies: a) ethanol and  
11  
12 944 heat assisted dissociation of casein micelles, **binding the bioactive ligand** to soluble caseins  
13  
14 945 ( $\alpha$ -,  $\beta$ -,  $\kappa$ -CN) and micelle formation via reconstitution of the native mineral milk  
15  
16 946 composition, and b) incorporating lipophilic compounds into casein micelles by ethanol  
17  
18 947 assisted high pressure homogenization, followed by solvent evaporation or emulsification-  
19  
20 948 evaporation (Esmaili et al., 2011; Mantzouridou et al., 2012; Pan et al., 2013; Trejo and  
21  
22 949 Harte, 2010). Encapsulating lipophilic compounds in self-assembled casein nanoparticles  
23  
24 950 facilitates the incorporation of bioactive compounds into the food matrix. In addition, casein  
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26 951 nanoparticles are of higher stability compared to microemulsions or liposomes, are cost  
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28 952 efficient and environmentally friendly (Gutiérrez et al., 2013).  
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31 953 Casein self-assembled nanoparticles have been successfully used to encapsulate many  
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33 954 lipophilic bioactive compounds including curcumin (Esmaili et al., 2011; Pan et al., 2013)  
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35 955 and  $\beta$ -carotene (Agüeros Bazo et al., 2013; Danino et al., 2011; Sáiz-Abajo et al., 2013).  
36  
37 956 According to Sáiz-Abajo and others (2013),  $\beta$ -carotene encapsulation in self-assembled  
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39 957 casein nanoparticles allowed its complete entrapment in the interior of the matrices, though  $\beta$ -  
40  
41 958 carotene degradation due to heat, light and oxygen was approx. 40%. However, casein  
42  
43 959 nanoparticles improved the stability of  $\beta$ -carotene under heat (80 °C, 8 h) and high  
44  
45 960 hydrostatic pressure processing, compared to its free form. Incorporating  $\beta$ -carotene loaded  
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47 961 CN nanoparticles into cookie dough and baking (180°C) resulted in a 42%  $\beta$ -carotene  
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49 962 degradation, compared to 67% for free  $\beta$ -carotene.  
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52 963 Elucidating **protective mechanisms** of r-CN on  $\beta$ -carotene, Sáiz-Abajo and others (2013)  
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54 964 reported that  $\beta$ -carotene was linked via hydrophobic interactions to the hydrophobic domain  
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3 965 of CN micelles ( $\kappa$ -casein) following heat/ethanol assisted dissociation (Fig. 4). During the  
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5 966 CN re-assembly,  $\beta$ -carotene remained inside the hydrophobic core of the micelles, **protected**  
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7 967 from external conditions. Using purified  $\beta$ -CN to develop nanoparticles has been reported an  
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9 968 alternative efficient strategy for encapsulating carotenoids (Danino et al., 2011; Esmaili et al.,  
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11 969 2011; Pan et al., 2013). Nanoparticles from self-assembled  $\beta$ -CN formed under acidic  
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13 970 conditions (i.e.  $\text{pH} < \text{pI}$ ) **showed** high stability between **pH 2.4-4.2 and 1-45°C**. The narrow  
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15 971 particle size distribution provided satisfactory organoleptic aspects when incorporated into  
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17 972 food matrices, including clear beverages (Danino et al., 2011; Semo et al., 2007).

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19 973 Bovine  $\beta$ -lactoglobulin ( $\beta$ -LG) is the main whey protein in cow milk, **characterized by** cold,  
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21 974 hot or acid induced gelation, interaction at the air/liquid interfaces, foam and emulsion  
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23 975 stabilizing capacity, film forming ability, and water and oil binding capacity (Nicolai et al.,  
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25 976 2011). The central cavity of  $\beta$ -LG provides a ligand-binding site for hydrophobic molecules,  
26  
27 977 including **carotenoids (Mensi et al., 2013a), and opening its hydrophobic pocket (by**  
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29 978 **increasing pH and ionic strength) could enhance binding affinity (Zhang et al., 2013b).**  
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31 979 **Investigating the binding affinity of several carotenoids to variants A, B of milk derived  $\beta$ -**  
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33 980 **LGs,  $\beta$ -carotene exhibited a better binding affinity to  $\beta$ -LG compared** to  $\alpha$ -carotene and  $\beta$ -  
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35 981 cryptoxanthin, while no significant differences in their binding affinities as a function of  $\beta$ -  
36  
37 982 LG variants were observed (Mensi et al., 2013a). **The potential of  $\beta$ -LG as** an encapsulating  
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39 983 agent is associated with its ability to form aggregates under controlled temperature, pH and  
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41 984 ionic strength or by high pressure via hydrophobic attraction and disulphide/sulphydryl (S-  
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43 985 S/SH) bridges (Mensi et al., 2013b; Nicolai et al., 2011). For example, encapsulation  
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45 986 efficiency of  $\alpha$ -tocopherol in nanoparticles formed by  $\text{Zn}^{2+}$  induced  $\beta$ -LG cold gelation  
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47 987 improved by increasing the  $\alpha$ -TOC/ $\beta$ -LG molar fraction, while low amounts of  $\text{Ca}^{2+}$   
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49 988 conferred benefits on the binding affinity of the lipophilic compound, due to lowering  
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51 989 electrostatic repulsions between  $\beta$ -LG molecules (Somchue et al., 2009).  
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3 990 Implementing heat induced aggregation-encapsulation, an increased encapsulation efficiency  
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5 991 of  $\beta$ -LG aggregates with both the amount protein and the  $\beta$ -LG/EGCG molar ratio was  
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7 992 reported (Sphigelman et al., 2012). The authors suggested a cooperative effect between  
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9 993 ligands and  $\beta$ -LG, as protein molecules complexed together more easily entrap a larger  
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11 994 amount of (stacked) ligands. Binding ligands to  $\beta$ -LG aggregates primarily takes place via  
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13 995 hydrophobic interactions/hydrogen bonding, and the negligible changes in the electrophoretic  
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15 996 mobility of the nanoparticles on the modification of the ligand :  $\beta$ -LG ratio omit the  
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17 997 possibility of electrostatic interactions (Shpigelman et al., 2012). Of note, the colloidal  
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19 998 stability of globular milk protein assembled nanoparticles as flocculation phenomena are  
20  
21 999 constrained due to electrostatic repulsions and Brownian motion, whereas freeze drying and  
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23 1000 reconstituting the nanoparticles had only minor effects on their colloidal aspects.

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25 1001 High hydrostatic treatment of  $\beta$ -LG can be adopted as a minimal processing and sustainable  
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27 1002 alternative to develop self-assembly nanovehicles. Mensi et al. (2013b) investigated the  
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29 1003 impact of high pressure processing (pressurization conditions,  $\beta$ -LG amount, pH and ionic  
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31 1004 strength adjustment) on the efficiency of nanoassemblies to load and retain  $\beta$ -carotene during  
32  
33 1005 storage and under simulated GI conditions. The encapsulation efficiency was high (e.g. 89-  
34  
35 1006 99%), depending on ionic strength and pH (low pH and salt concentration facilitated the  
36  
37 1007 aggregates' loading with carotenoids). High pressure formed nanocomplexes of enhanced  
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39 1008 storage photostability at 4°C, compared to  $\beta$ -carotene bound to native  $\beta$ -LG or in its free  
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41 1009 form, with all-*trans*  $\beta$ -carotene retention being 75-100, 62 and 17%, respectively.

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43 1010 The natural (cold, heat, pressure or acid) self-assembly capacity of  $\beta$ -LG can be further  
44  
45 1011 improved via its ability to interact with other biopolymers through covalent conjugation or  
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47 1012 electrostatic complexation (Nicolai et al., 2011). Maillard reaction-formed conjugates  
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49 1013 between proteins and polysaccharides can self-assemble or absorb to oil-water interfaces  
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51 1014 creating a 'hairy layer' with the polysaccharide block. This layer can stabilize the colloidal  
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3 1015 emulsion by steric exclusion or by increased microviscosity of the continuous water phase  
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5 1016 around the droplets (Nicolai et al., 2011). Maillard reaction conjugates have been  
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7 1017 successfully used to encapsulate  $\beta$ -carotene (Kosaraju et al., 2009; Pan et al., 2007). Protein-  
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9 1018 dextran copolymers formed by Amadori rearrangement to encapsulate  $\beta$ -carotene exhibited  
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11 1019 adequate encapsulation efficiency (up to 54%), stability against  $\text{FeCl}_3$  induced oxidation and  
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13 1020 promoted stability against pepsin/trypsin (Pan et al., 2007).

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16 1021 Electrostatic complex formation of oppositely charged biopolymers is an established method  
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18 1022 to encapsulate bioactive compounds, including living cells. For lipophilic molecules, layer-  
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20 1023 by-layer deposition can be applied to nano-coated emulsion droplets (containing the  
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22 1024 bioactives), via attractive molecular forces forming core-shell type nanoparticles. Proteins  
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24 1025 such as  $\beta$ -LG and caseins can be used as they interact with anionic or cationic (below or  
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26 1026 above their pI, respectively) compounds, stabilizing emulsions (Nicolai et al., 2011). Though  
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28 1027 molecular complexation can also occur above the pI of proteins, a reduced pH favors stable  
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30 1028 precipitates via electrostatic interactions between the anionic groups of the polysaccharide  
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32 1029 (e.g. pectin, chitosan etc.) and the cationic patches of globular protein surfaces (Jones et al.,  
33  
34 1030 2009). Ionic strength, pH, temperature, molecular characteristics (charge density and  
35  
36 1031 distribution) and the molar ratio of the biopolymers govern the nature of the complexes  
37  
38 1032 (Jones et al., 2009; Matalanis et al., 2011).

#### 1033 4. Solid lipid nanoparticles (SLNs)

1034 Solidifying the lipid phase (fully or partially crystalline fat droplets) of liquid-liquid  
1035 nanoparticles (LLNs) such as o/w nano-emulsions and liposomes, results in novel delivery  
1036 systems known as solid liquid nanoparticles (SLNs), which owe certain advantages over  
1037 LLNs. SLNs are commonly fabricated using a lipid phase with a narrow melting range, e.g.  
1038 pure TAGs or hydrocarbons in order to produce a highly ordered crystalline structure,  
1039 enabling the physical entrapment of lipophilic bioactive compounds. There is great interest of

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3 1040 SLNs for food industry applications, as they combine the high bioaccessibility/  
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5 1041 bioavailability of emulsions, the membrane permeability of liposomes and the ability of  
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7 1042 biopolymer nanoparticles for controlled release. SLN technology also reduces the  
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9 1043 disadvantages of conventional delivery systems (organic solvents), i.e. low bioactive  
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11 1044 compound payload, low chemical stability, bio-toxicity of the carrier, and challenges of LLN  
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13 1045 up-scaling. The major drawback of SLN delivery rests in the expulsion of bioactive  
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15 1046 compounds due to polymorphic transitions of the crystalline lipid structures (i.e.  $\alpha \rightarrow \beta' \rightarrow \beta$ -  
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17 1047 crystal) during storage. Polymorphic transitions result in conformational modification of the  
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19 1048 lipid nanoparticles (from spherical to platelet-like), increasing their surface area and inducing  
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21 1049 particle aggregation due to hydrophobic interactions, decreasing stability. Using lipid  
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23 1050 ingredients with a broad melting range or blending lipids of different melting profile can be  
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25 1051 strategies to increase the structural disorder of the lipid crystal lattices and to alter the  
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27 1052 physical stability of SLNs towards particle aggregation or gelation. For food applications,  
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29 1053 delivery systems should employ food grade lipid sources with acceptable mouth-melting  
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31 1054 properties with have neutral effects on blood lipids. Biopolymers for stabilizing fat crystalline  
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33 1055 structures must be edible, biodegradable and have sufficient barrier properties against water  
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35 1056 vapor and oxygen, without hindering the release of the bioactive compounds.  
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37 1057 A growing number of studies have investigated the efficacy of SLN based carotenoid  
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39 1058 delivery systems in terms of encapsulation/loading efficiency, physical/colloidal stability,  
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41 1059 carotenoid stability, stability of the lipid phase against primary/secondary oxidation as well as  
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43 1060 sustained release (Cornacchia and Roos, 2011; De Lara Gomes et al., 2013; Eltayeb et al.,  
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45 1061 2013; Helgason et al., 2009; Hentschel et al., 2008; Lacatusu et al., 2013; Liu and Wu, 2010;  
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47 1062 Nik et al., 2012; Qian et al., 2013). The physicochemical properties of the lipid phase (e.g.  
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49 1063 melting profile, crystalline state, TAG composition) and physicochemical (melting point) and  
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51 1064 molecular characteristics (head and tail groups) of the surfactants have been reported to be  
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3 1065 crucial for the physical stability of the nanostructured lipid carriers (NLCs) and the chemical  
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5 1066 stability of the encapsulated carotenoids (Helgason et al., 2009; Qian et al., 2013).  
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7 1067 Lucatusu et al. (2013), using a lipid carrier (carnauba wax), glycerol stearate and fish oil  
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9 1068 fortified with lutein reported an encapsulation efficiency of 56-89% with 200 nm or smaller  
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11 1069 particles, with lower amounts of fish oil decreasing encapsulation efficiency. Improved  
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13 1070 oxygen scavenging ability was detected for the antioxidant activity of lutein entrapped in  
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15 1071 SLNs vs. free lutein, though this did not depend on lutein content. The colloidal features of  
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17 1072 the lutein loaded SLNs, though significantly affected by the amount of oil carrier and lutein  
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19 1073 (both with increasing amounts reducing the hydrodynamic volume of the nanovehicles),  
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21 1074 exerted good physical stability against particle aggregation at 25°C. Contrarily, Qian and  
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23 1075 others (2013), Helgason and others (2009) and Cornacchia and Roos (2011) found that  
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25 1076 entrapped  $\beta$ -carotene SLNs reduced chemical stability, postulating that the restricted stability  
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27 1077 of  $\beta$ -carotene in SLNs was related to its expulsion from the fat crystals, undergoing  
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29 1078 aggregative (through non-polar patches of the particles or partial fat coalescence) and  
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31 1079 polymorphic changes. Helgason et al. (2009) investigated the impact of several emulsifiers  
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33 1080 (differing in their molecular conformation and melting points), emphasizing that  $\beta$ -carotene  
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35 1081 degradation during SLNs storage was associated with lipid phase structural modification  
36  
37 1082 upon crystallization. When nucleation was initiated on the fat droplet surface, a solid was  
38  
39 1083 formed that protected against pro-oxidants in the aqueous phase. In contrast, when nucleation  
40  
41 1084 starts in the interior of the fat droplets,  $\beta$ -carotene may be expelled to the water/oil interface,  
42  
43 1085 exposing it to pro-oxidants (Helgason et al., 2009). Similarly, Hentschel et al. (2008) reported  
44  
45 1086 that  $\beta$ -carotene degradation in propylene glycol monostearate (PGMS) based SLNs started  
46  
47 1087 shortly after storage at 20°C, though no polymorphic transitions were detected. It was also  
48  
49 1088 demonstrated that co-encapsulating of  $\beta$ -carotene with antioxidants, including  $\alpha$ -tocopherol,  
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51 1089 protected against degradation, even when NLCs were dispersed in water.  
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3 1090 **5. Nanostructured lipid carriers (NLCs)**

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5 1091 **The challenges of SLNs**, e.g. low payload, high water content and tendency to form  
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7 1092 aggregates **that expulse** the bioactives, have led to development of a second generation of  
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9 1093 SNLs known as nanostructured lipid carriers (NLCs) (Müller et al., 2002; Tamjidi et al.,  
10  
11 1094 2013). NLCs are considered as modified SLNs in which the lipid phase comprises both solid  
12  
13 1095 (fat) and liquid (oil) lipids at room or body **temperature**. Regarding the solid lipid phase, fat is  
14  
15 1096 found either in a partially crystalline or amorphous state, **increasing** the structural disorder of  
16  
17 1097 the nanoparticulates, thus minimizing the expulsion of the bioactive **due** to fat **polymorphism**  
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19 1098 (Tamjidi et al., 2013). The major advantage of NLCs is their higher payload **as** imperfections  
20  
21 1099 within the fat structure can accommodate more efficiently the bioactives. Three conformation  
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23 1100 types of NLCs exist: the imperfect, the amorphous and the multiple (Fig. 5). In the imperfect  
24  
25 1101 case, the “tightly packed” fat structure of SLNs is disrupted by creating internal voids, using  
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27 1102 lipid components exerting high spatial incompatibility (large enough distances between the  
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29 1103 fatty acids of the glycerides). This can be achieved by blending solid lipids with liquid lipids  
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31 1104 of different chemical composition, e.g. mixing tristearin with MCT (Yang et al., 2014a). The  
32  
33 1105 amorphous type is based on controlling the fat crystallization to produce crystalline  
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35 1106 conformations **prone to** polymorphic transitions, i.e. structureless solid amorphous matrices.  
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37 1107 This can be realized by blending specific lipids (e.g. hydroxyl-octacosanylhydroxystearate  
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39 1108 with isopropylmyristate), where lack of crystallinity leads to enhanced stability against  
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41 1109 expulsion of the bioactive. Finally, for multiple systems, a complex oil-in-fat-in-water  
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43 1110 emulsion comprising tiny liquid oil nanocompartments is produced, with **the bioactive being**  
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45 1111 dissolved in the oil phase (Müller et al., 2002; Tamjidi et al., 2013).

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47 1112 Depending on the **carrier specification** (**heat** stability, hydrophobicity of the bioactive  
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49 1113 compounds, emulsifier cloud point etc.), NLCs can be produced by hot or cold  
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51 1114 homogenization. In the former, the bioactive compound is dissolved in the molten fat/oil



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3 1115 emulsifier system. After high pressure homogenization or ultrasonication, the nanoemulsion  
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5 1116 is cooled to initiate fat crystallization and precipitation of the nanoparticles. In the second  
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7 1117 case, the emulsion is quenched by liquid nitrogen and the resulting solid matrix is cold-milled  
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9 1118 to obtain fine particulates. Though the latter method appears to be advantageous for heat  
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11 1119 sensitive compounds, most NLC applications for carotenoids rely on hot homogenization,  
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13 1120 due to sufficient heat stability of carotenoids (retention >80-90%) (Helgason et al., 2009;  
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15 1121 Hentschel et al., 2008). In addition, problems related to uncontrollable fat crystallization can  
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17 1122 be overcome by proper selection of the emulsifying system (Gutiérrez et al., 2013).

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20 1123 Recently, solvent diffusion (dissolution of lipid phase into ethanol followed by blending with  
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22 1124 a hydrophilic emulsifier in water) has been successfully applied for  $\beta$ -carotene loaded NLCs  
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24 1125 (Hejri et al., 2013). The method provided good  $\beta$ -carotene stability (up to 98%), though  
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26 1126 degradation depended on the amount of lipid phase, surfactant concentration, and dissolution  
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28 1127 temperature. PIT was also successfully used to produce NLCs at low energy, cost efficiency  
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30 1128 and minor equipment demand (Zhang et al., 2013a).

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34 1129 To date, NLCs are predominantly employed for drug delivery, though there is an increasing  
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36 1130 number of applications for delivering dietary derived compounds, including hydrophobic  
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38 1131 polyphenols (Aditya et al., 2013) and carotenoids (Hejri et al., 2013; Hentschel et al., 2008;  
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40 1132 Hung et al., 2011; Nik et al., 2012; Quan et al., 2013; Zhang et al., 2013a) in food items.

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42 1133 Homogenization conditions (Hung et al., 2011; Liu and Wu, 2010), melting profile of the  
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44 1134 lipid ingredients (Yang et al., 2014a; Zhang et al., 2013a), surfactants (Hejri et al., 2013),  
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46 1135 concentration of the lipid phase (Hejri et al., 2013), fat crystallization, and ionic strength of  
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48 1136 the emulsion (Zhang et al., 2013a) all influence the encapsulation efficiency and the stability  
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50 1137 of carotenoids during storage. Liu and Wu (2010), studying ultrasonication effecting lutein  
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52 1138 encapsulation by NLCs, found a decreased NLC mean size (from 228 to 110 nm) with  
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54 1139 increasing ultrasonication time (from 2 to 10 min). No re-aggregation was detected with  
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3 1140 excess energy input as previously stated (Kentish et al., 2008), though excessive  
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5 1141 ultrasonication did not enhance lutein loading efficiency.

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7 1142 Surfactant type and amount directly impact carotenoid payload in NLCs and their stability  
8  
9 1143 during storage. This is generally associated with the surfactants' ability to reduce the surface  
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11 1144 area of the lipid particles, affecting fat polymorphic transitions, controlling mass transfer  
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13 1145 phenomena, e.g. oxygen diffusion (Hejri et al., 2013; Helgason et al., 2009). In the latter  
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15 1146 study,  $\beta$ -carotene stability improved with increasing surfactant amount until a maximum;  
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17 1147 further increase significantly impaired stability against oxidation, likely due to the formation  
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19 1148 of a rigid shell protecting carotenoids. Zheng et al. (2013) investigated several hydrophilic  
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21 1149 surfactants (Tween 20, arabic gum, sucrose esters, and polyglycerol fatty acid esters) for  
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23 1150 colloidal aspects, crystallinity and physical stability of NLCs. The loading efficiency and  
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25 1151 storage stability of  $\alpha$ -lipoic acid improved by surfactants with small and flexible hydrophilic  
26  
27 1152 head groups such as Tween 20 or PGFE. Contrarily to sucrose esters and arabic gum, these  
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29 1153 systems were stable towards flocculation and fat polymorphic transitions.

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31 1154 Ionic strength can also affect the effectiveness of surfactants. Depending on surfactant to  
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33 1155 ionic strength ratio, the formation of gels or phase separation may take place. Zhang et al.  
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35 1156 (2013a), implementing the PIT method to fabricate NLCs loaded with  $\beta$ -carotene reported  
36  
37 1157 that increasing NaCl concentration (from 0 to 1.0 M) decreased PIT and facilitated NLC  
38  
39 1158 formation at lower temperature. Moreover, adjusting ionic strength during NLC production  
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41 1159 enhances their physical stability (absence of coalescence or Ostwald ripening phenomena)  
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43 1160 and also remarkably reduces  $\beta$ -carotene degradation during storage.

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45 1161 It was shown that NLC nanoparticles can be used to fabricate the core of gelatine-arabic gum  
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47 1162 coacervates containing fucoxanthin (Quan et al., 2013). The physicochemical properties of  
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49 1163 the lipid core components (cetyl palmitate vs. canola oil) significantly affected the  
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51 1164 morphological, payload and release properties of the capsules. Increasing the fat crystalline  
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3 1165 fraction in the lipid core increased the irregularity of the obtained microspheres and lowered  
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5 1166 the efficiency to uphold fucoxanthin due to the build-up of a “brick-like” structure devoid of  
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7 1167 internal pockets for taking up fucoxanthin. However, the presence of compact lipid core  
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9 1168 structures (due to the increase of the solid to liquid fraction) lowered disintegration and  
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11 1169 slowed the release after incubation in gastric/intestinal fluids, and enhanced storage retention  
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13 1170 at various RH. The ability of high melting point lipid components to control mass transport  
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15 1171 phenomena (oxygen and GI-fluids) even under conditions where structural collapse of the  
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17 1172 hydrogel shell structure was noticed, was made responsible (Quan et al., 2013).

## 20 1173 **6. Solvent displacement**

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22 1174 Solvent displacement or anti-solvent precipitation is generally based on altering the “quality”  
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24 1175 of the solvent around the biopolymer molecules, to induce a spontaneous self-assembly when  
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26 1176 a critical solvent concentration is attained (Joye and McClements, 2013; Matalanis et al.,  
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28 1177 2011). This can be achieved by adding a miscible anti-solvent to a biopolymer solution where  
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30 1178 the active compound comprises a co-solute of the initial biopolymer solution. Nanoparticle  
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32 1179 formation takes place by rapid diffusion of the organic solvent in the aqueous phase and the  
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34 1180 deposition of the active substance in the solvent – anti-solvent interface (Chu et al., 2007a).  
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36 1181 The polymer molecules (in the solvent phase) diffuse together with the solvent and self-  
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38 1182 assemble at the interface, incorporating the active substance (Fig. 6). The surfactant in the  
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40 1183 anti-solvent phase stabilizes the formed nanoparticles, preventing aggregation. The solvent  
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42 1184 can then be eliminated by evaporation. As for supercritical fluid induced precipitation (e.g.  
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44 1185 SAS/SEDS), supersaturation is the driving force of encapsulation effectiveness, determining  
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46 1186 mean size, crystallinity, purity and morphology of the formed particles.

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48 1187 **In general, high supersaturation and low surface tension enable fast nucleation and small**  
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52 1188 crystal growth (controlled by secondary crystallization and Ostwald ripening) and particle  
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55 1189 formation with narrow size distribution (Joye and McClements, 2013; Liu et al., 2007b).  
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3 1190 Nanoparticles formed by anti-solvent precipitation show low polydispersity and high  
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5 1191 encapsulation efficiency/stability. This is achievable either thermodynamically (by  
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7 1192 stabilizers/media controlling colloidal interactions between nanoparticles) or kinetically  
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10 1193 (energy input to compensate excess surface energy due to the particles' high surface area)  
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12 1194 (Thorat and Dalvi, 2012). Parameters such as anti-solvent to solvent ratio, the speed of anti-  
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14 1195 solvent to solvent addition or vice versa, active substance concentration, precipitation  
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16 1196 temperature, the physicochemical profiles of the anti-solvent, surfactant and biopolymers  
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18 1197 (e.g. polarity, surface charge, aggregation ability, interfacial properties) impact the size,  
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21 1198 crystallinity and morphology of the nanoparticles (Joye and McClements, 2013).

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23 1199 With respect to food industry, nanoprecipitates produced by solvent displacement mainly aim  
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25 1200 to incorporate active substances that degrade under common processing conditions (heat, pH,  
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27 1201 light and mechanical stress), enhancing bioactive payload compared to conventional  
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29 1202 encapsulation, and to achieve customized release under GI digestion conditions. Solvent  
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31 1203 displacement nanoprecipitation is regarded as a very efficient method to entrap and stabilize  
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33 1204 lipophilic substances including carotenoids or hydrophobic polyphenols (curcumin), in food  
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35 1205 matrices, as well as to improve bioavailability (Chu et al., 2007a; Faisal et al., 2013; Kakran  
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37 1206 et al., 2012; Lobato et al., 2013; Mitri et al., 2011; Panagiotou and Fisher, 2013; Patel et al.,  
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39 1207 2010; Ribeiro et al., 2008; Tachaprutinun et al., 2009; Yin et al., 2009).

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43 1208 Though solvent displacement appears to be advantageous for up-scaling, proper selection of  
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45 1209 nanoparticle components (e.g. polymers, surfactants, water miscible organic solvents) may be  
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47 1210 demanding (Joye and McClements, 2013). The most commonly employed organic solvents  
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49 1211 are ethanol and acetone, while a great number of surface active compounds have been  
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51 1212 successfully used for nanoprecipitation, including milk proteins (whey protein isolates/  
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53 1213 concentrates, sodium caseinate), plant proteins (zein), polysorbates, and sucrose esters (Chu  
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55 1214 et al., 2007a; Ribeiro et al., 2008; Yin et al., 2009). Polymers can also be used as supportive

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3 1215 coating materials, particularly when sustained release of the bioactive substances is required.  
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5 1216 For most applications, polymeric materials exerting fair interfacial properties (gelatin, poly-  
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7 1217 D,L-lactide (PLA), poly-D,L-lactide-co-glycolide (PLGA), poly- $\epsilon$ -caprolactone (PCL), arabic  
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9 1218 gum) are used for anti-solvent nanoprecipitation (Lobato et al., 2013; Ribeiro et al., 2008),  
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11 1219 though in many cases polymers as co-stabilizer are not required.  
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13 1220 Chu et al. (2007) and Ribeiro et al. (2008) used solvent displacement to investigate colloidal  
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15 1221 and stability characteristics of nanoparticles loaded with  $\beta$ -carotene and stabilized either by  
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17 1222 different types of milk proteins or by a blend of surfactants (Tween 20) and surface active  
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19 1223 polymers (gelatin, PLA and PGLA). Though nanoparticle formation mechanisms were  
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21 1224 similar in both cases (movement of the lower surface tension phase to the aqueous one and  
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23 1225 creating a solvent boundary layer where supersaturation, nucleation and  $\beta$ -carotene crystal  
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25 1226 formation took place), the formed particles were stabilized either only by the surfactants or  
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27 1227 by synergistic actions of the surfactants and polymeric material. In the latter case, the  
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29 1228 surfactants rapidly adsorbed on the oil-water interfaces, preventing droplet coalescence due to  
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31 1229 electrostatic repulsion, while the polymer material deposited on the stabilized particles,  
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33 1230 creating a rigid and thick outer layer, hindering particle growth due to Ostwald ripening.  
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35 1231 It was also shown that the surfactant type was the main factor affecting mean particle size,  
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37 1232 whereas surfactant concentration, the emulsification process and amount of  $\beta$ -carotene loaded  
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39 1233 may interplay with the colloidal aspects of the obtained particles. Among different types of  
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41 1234 milk proteins, sodium caseinate was optimum to stabilize  $\beta$ -carotene nanoparticles, as casein  
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43 1235 submicelles (primarily) and micelles (secondarily) undergo conformational changes upon  
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45 1236 solvent displacement, interacting with  $\beta$ -carotene via hydrophobic binding (Chu et al., 2007).  
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47 1237 Whey protein concentrates were the least effective stabilizing agents, increasing particle  
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49 1238 polydispersity (due to their lower protein purity, MW homogeneity, and structural flexibility  
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51 1239 compared to SC). In the same study, it was shown that a minimum amount of SC (0.5% wt)

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3 1240 was required to ensure an adequate number of casein submicelles to stabilize the precipitated  
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5 1241  $\beta$ -carotene via self-assembled caseins. Further increasing the SC concentration did not  
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7 1242 significantly change  $\beta$ -carotene uptake. Fabricating particularly small nanoparticles may  
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9 1243 increase  $\beta$ -carotene susceptibility to degradation during storage. Yin et al., (2009), studying  
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11 1244 the influence of several surfactant systems on colloidal aspects and stability of  $\beta$ -carotene  
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13 1245 loaded nanoparticles revealed that larger particles improved biological activity due to better  
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15 1246 protection by the thicker crust/envelop of the surface nanodeposited emulsifiers.  
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17 1247 Recently, bixin was successfully encapsulated in PCL-sorbitan monostearate stabilized  
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19 1248 nanoparticles by anti-solvent (1:8 ethanol : acetone ratio) precipitation (Lobato et al., 2013).  
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21 1249 The approach allowed a very high encapsulation efficiency (>98.6%), probably due to the  
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23 1250 capric/caprylic TAG based core, promoting bixin solubilization. The loaded nanoparticles  
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25 1251 exerted good stability against Ostwald ripening and coalescence during storage (119 days,  
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27 1252 room temperature), though bixin retention declined to 46%.

### 1253 7. Emulsification evaporation

1254 This method comprises dissolving the active substance in an organic solvent and emulsifying  
1255 the apolar phase using an aqueous phase containing the surfactant. The formed o/w emulsion  
1256 is then converted to a nanodispersion by solvent evaporation (Fig. 7). The particles'  
1257 morphology rests usually in the thermodynamically stable crystal structure, as solid formation  
1258 takes place by evaporation crystallization at low supersaturation (Chu et al., 2007b). The  
1259 morphological characteristics and polydispersity of the nanoparticles are influenced by many  
1260 parameters, i.e. the surfactant, the homogenization process and conditions (pressure, number  
1261 of passes), the organic : aqueous phase ratio, the organic solvent and amount, evaporation  
1262 temperature etc. (Anarjan et al., 2011b; Anarjan and Tan, 2013b; Cheong and Tan, 2010; Chu  
1263 et al., 2007b; Tan and Nakajima, 2005). Together with storage conditions, these parameters  
1264 may also indirectly impact the stability of the encapsulate (Anarjan and Tan, 2013c).

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3 1265 Emulsifiers are the driving force for nanoparticle formation, reducing interfacial tension  
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5 1266 between immiscible phases, reducing the energy required to disrupt the droplets during  
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7 1267 emulsification. Surfactants absorb on the oil-water interfaces, forming a protective layer  
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9 1268 surrounding the droplets, preventing coalescence (Chu et al., 2007b). Chu and others (2007b)  
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11 1269 investigated milk protein emulsifiers (sodium caseinate, whey protein concentrate (WPC) and  
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13 1270 isolate (WPI) and hydrolyzate (WPH)) with respect to properties of  $\beta$ -carotene containing  
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15 1271 particles. Factors such as interfacial tension reduction, molecular flexibility and structural  
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17 1272 packing of the protein, MW, protein purity as well as exposure of hydrophobic areas affected  
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19 1273 nanoparticle characteristics. SC was the most efficient surfactant, favoring formation of  
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21 1274 monomodally distributed fine nanoparticles, followed by WPH, WPI and WPC. Anarjan and  
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23 1275 Tan (2013a) studied polysorbates (Tween 20, 40, 60 and 80) and sucrose ester emulsifier  
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25 1276 functionality, reporting that Tweens more efficiently reduced the mean size of astaxanthin  
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27 1277 loaded nanodispersions than sucrose esters, due to their higher HLB and shorter fatty acid  
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29 1278 chain lengths. On the other hand, the polydispersity of nanoparticles was lower for sucrose  
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31 1279 esters; perhaps due to their higher entrapment efficiency or critical micelle concentration than  
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33 1280 polysorbates, facilitating the formation of astaxanthin nanodispersions.  
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35 1281 Using co-surfactants can remarkably modify mean nanoparticle diameter as well as their  
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37 1282 polydispersity index (Anarjan and Tan, 2013b). Blending non-adsorbing emulsifiers such as  
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39 1283 sodium caseinate or arabic gum with Tween 20 to create binary surfactant systems  
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41 1284 significantly increased the mean size of astaxanthin loaded nanodispersions. Several  
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43 1285 mechanisms were proposed for these adverse effects, such as competitive adsorption  
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45 1286 (restricting the non-adsorbing emulsifiers in a small area, leading to a thicker interfacial  
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47 1287 layer), depletion flocculation (increased attractive forces between the droplets leading to  
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49 1288 droplet coalescence) and bridging flocculation (droplet collision due to electrostatic  
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51 1289 interactions between charged domains of the biopolymers). However, using ternary systems  
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3 1290 (Tween 20 and two non-adsorbing emulsifiers) significantly reduced nanoparticle mean size;  
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5 1291 emphasizing the synergy of the surfactants in terms of stabilizing and emulsifying ability,  
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7 1292 forming a closely-packed interfacial layer of the intercalating surfactant molecules.  
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10 1293 Microfluidization is the most common homogenization technique for nanoparticles  
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12 1294 production by solvent-diffusion. In several studies (Anarjan et al., 2011b; Chu et al., 2007b;  
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14 1295 Tan and Nakajima, 2005), increased homogenization pressure and cycles was generally  
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16 1296 associated with finer nanoparticles, as higher shear forces and turbulence was achieved.  
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18 1297 However, parameters such as the evaporation temperature and the organic to aqueous ratio  
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20 1298 can also effect the homogenization to control fine particle formation. Anarjan et al. (2011)  
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22 1299 reported that a minimum critical temperature was required for fine nanoparticle fabrication.  
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24 1300 In addition, increasing the amount of organic solvent produces larger particles, mainly due to  
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26 1301 increased microviscosity at the polar-apolar interfaces, reducing disruptive forces due to  
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28 1302 cavitation (Tan and Nakajima, 2005). An antagonistic action on astaxanthin nanodispersion  
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30 1303 particle size and polydispersity index was observed with water immiscible (dichloromethane)  
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32 1304 and water miscible (acetone) solvents. Tuning the ratio of water miscible to immiscible  
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34 1305 solvents proved effective to control nanoprecipitation. Adjusting solvent proportions controls  
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36 1306 solvent diffusion in the aqueous phase, the active substance solubility and stabilizer as well as  
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38 1307 the interfacial properties of the system. Therefore, a critical apolar : polar solvent ratio exists  
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40 1308 to obtain the finest particles with narrow particle size distribution. This critical point is  
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42 1309 generally associated with rapid nucleation rates, controlled particle growth, hindered particle  
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44 1310 collision phenomena, and adequately low surface tension (Anarjan et al., 2011a).  
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46 1311 In general, emulsification-evaporation (due to relatively mild processing conditions) allows  
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48 1312 rather high encapsulation yields (up to 97%). Homogenization conditions (pressure, number  
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50 1313 of cycles), the organic solvent and stabilizer type as well as the evaporation temperature are  
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52 1314 the most crucial parameters for carotenoid degradation during the nanoprecipitation process.  
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3 1315 Tan and Nakajima (2005) reported a 1-8 %  $\beta$ -carotene loss after the emulsification-  
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5 1316 evaporation process, which was mainly attributed to the temperature raise during  
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7 1317 **microfluidization and the presence of heat, light and oxygen during the evaporation.**  
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9 1318 **Anarjan et al.** (2011b) demonstrated that astaxanthin losses (**4-45%**) during nanoprecipitation  
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11 1319 were predominantly influenced by increasing cycle numbers and homogenization pressure,  
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13 1320 while evaporation temperature conferred only a minor effect. Anarjan and Tan (2013a)  
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15 1321 investigated the impact of surfactant type on astaxanthin losses during nanoprecipitation,  
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17 1322 revealing that emulsifiers carrying unsaturated fatty acids (e.g. Tween 80 or oleic acid  
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19 1323 sucrose esters) **increased oxidation. Astaxanthin losses were also** lower for nanodispersions  
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21 1324 with larger particle mean size (e.g. sucrose ester based), **due to** larger interfacial layers  
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23 1325 **providing** protection of the lipophilic active substance. In a successive study, Anarjan and  
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25 1326 Tan (2013b), using a ternary emulsifying system (**Tween 20, arabic gum and sodium**  
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27 1327 **caseinate**), reported that the emulsifier amount as well as the emulsifier to organic phase ratio  
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29 1328 can influence astaxanthin losses during **emulsification-evaporation. Generally,** a high  
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31 1329 emulsifier and organic phase concentration enhanced astaxanthin stability, primarily due to  
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33 1330 their impact on the oil-water interfaces and limited exposure of carotenoids to external  
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35 1331 conditions. Using binary solvent systems (water immiscible and water soluble solvents) has  
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37 1332 also been highlighted **as an alternative to** control carotenoid losses during nanoprecipitation.  
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39 1333 Anarjan and others (2011a) showed that trans-cis- isomerization of astaxanthin was higher in  
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41 1334 nanodispersions fabricated using pure dichloromethane (24%) compared to using acetone  
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43 1335 (13%). The authors reported that astaxanthin cis-isomer concentration was minimized with a  
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45 1336 dichloromethane to acetone ratio at 3:7 (for 9-cis) and 5:5 (for 13-cis).  
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47 1337 **Incorporating** antioxidants ( $\alpha$ -tocopherol, ascorbic acid) into astaxanthin loaded  
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49 1338 nanodispersions can improve autoxidation induced losses of carotenoids during  
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51 1339 emulsification-evaporation (Anarjan et al., 2013). **Lipophilic antioxidants** ( $\alpha$ -tocopherol)

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3 1340 were more effective against carotenoid oxidation, due to their ability to react with free radical  
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5 1341 intermediates of carotenoid peroxidation and peroxides as well as due to their ability to act as  
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7 1342 reducing agents for transition metals. Controlling carotenoid stability in nanodispersions is  
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10 1343 challenging, as it is not only affected by storage conditions but also by other factors such as  
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12 1344 carotenoid oxidation induced during processing, the morphological and compositional profile  
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14 1345 of the nanoparticles, the presence of antioxidants as well as the targeted food matrix (Anarjan  
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16 1346 and Tan, 2013a; Anarjan and Tan, 2013c). In general, storing carotenoid loaded  
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18 1347 nanodispersions at high temperature and light/oxygen exposure accelerate their oxidation. For  
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21 1348 example, increasing storage temperature by 10 °C resulted in 7- and 24-fold increased  
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23 1349 astaxanthin oxidation in nanodispersions stabilized by Tween 20 and sodium caseinate,  
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25 1350 respectively. Similarly, astaxanthin containing nanodispersion exposure to fluorescent/UV  
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27 1351 light resulted in a respective 3/5-fold increased oxidation for Tween 20 based systems and a  
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29  
30 1352 5/ 9-fold increase for sodium caseinate based ones (Anarjan and Tan, 2013c).

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32 1353 **Severe homogenization conditions triggered**  $\beta$ -carotene autoxidation (retention **decreased**  
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34 1354 from 56 to 36%) when homogenization pressure increased (from 60 to 140 MPa) during  
35  
36 1355 nanodispersion storage (4 °C, 12 weeks). Moreover, the increased ratio of the organic to  
37  
38 1356 water phase from 1:9 to 2:8 significantly improved  $\beta$ -carotene storage. The formation of free  
39  
40 1357 radicals during homogenization and the impact of the solvent phase and stabilizing agents on  
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42  
43 1358 the specific surface area of the particles and the colloidal aspects of the protective interfacial  
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45 1359 layers surrounding the formed nanoparticles are the main explanations for these results (Tan  
46  
47 1360 and Nakajima 2005). Scavenging free radicals produced during homogenization by adding  
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49 1361 antioxidants appears to be effective to extend the shelf-life of astaxanthin loaded  
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51  
52 1362 nanodispersions. **Using ascorbic acid (40 mg/L) and  $\alpha$ -tocopherol (60 mg/L) as additives in**  
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54 1363 **astaxanthin nanodispersions produced very low degradation rates (<0.00001/ week),** while no  
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56 1364 significant differences in astaxanthin content within the first month (at 5 °C) were observed  
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3 1365 (Anarjan et al., 2013). Anarjan and Tan (2013b) also scrutinized the effect of the food system  
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5 1366 (deionized water, skimmed milk or orange juice) on the stability of astaxanthin encapsulated  
6  
7 1367 in nanodispersions stabilized by a ternary surfactant system (Tween 20, sodium caseinate,  
8  
9 1368 arabic gum). Astaxanthin stability was higher in skimmed milk and orange juice compared to  
10  
11 1369 deionized water, whereas orange juice was the best matrix to incorporate astaxanthin, which  
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13 1370 was attributed to the high ascorbic acid content of orange juice and low pH, retarding free  
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15 1371 radical induced carotenoid autoxidation (Anarjan and Tan 2013b).

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18 1372 **ENCAPSULATION TO IMPROVE BIOACCESSIBILITY AND BIOAVAILABILITY**  
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20 1373 **OF CAROTENOIDS**

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23 1374 Bioavailability of a compound is generally defined as the fraction that can be absorbed and  
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25 1375 used for physiological functions and/or storage. The bioavailable fraction ( $F$ ) of lipophilic  
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27 1376 bioactives can be expressed as (McClements et al., 2008; McClements and Li, 2010):

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30 1377 
$$F = F_B \times F_C \times F_M \quad (1)$$

31  
32 1378 where  $F_B$  is the bioaccessibility,  $F_C$  equals transport (the fraction of the released bioactive  
33  
34 1379 compound that is transported across the intestinal epithelium) and  $F_M$  represents metabolism  
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36 1380 (here: the fraction that ends up in circulatory system via the lymph), though also further  
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38 1381 biodistribution and excretion (half-life in tissues) would play a role.

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41 1382 Due to their limited solubility in lipids and aqueous solutions including saliva and intestinal  
42  
43 1383 fluids, carotenoids exhibit low bioavailability, that is, up to 20% for carotenes and up to ca.  
44  
45 1384 40% for xanthophylls (Bohn, 2008). Emulsification of carotenoids in the bulk lipid phase by  
46  
47 1385 surface active lipids (phospholipids, FFAs, MAGs or DAGs) can enhance their solubility in  
48  
49 1386 the intestine (Borel et al., 1996; Huo et al., 2007). In addition, lipase hydrolytic activity  
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51 1387 promoting micellization is generally higher in the case of emulsified TAGs, indicating that  
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53 1388 liquid lipid carriers (emulsions) are natural systems promoting carotenoids bioavailability  
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3 1389 (Huo et al., 2007). Taking into account the structural, colloidal and physicochemical diversity  
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5 1390 of LLCs, a large number of factors can influence carotenoid bioavailability (Fig. 8):  
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- 7 1391 a) the molecular conformation of the lipid carrier, e.g. type and position of the fatty acid  
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9 1392 chains of the glycerol backbone;  
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11 1393 b) the colloidal and interfacial properties of the lipid phase components as well as the  
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13 1394 presence of surface active compounds in the food matrix or in intestinal fluids;  
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15 1395 c) the physical state of the lipid phase, e.g. presence and amount of crystalline fat,  
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17 1396 polymorphic state of crystalline fat;  
18  
19 1397 d) the structure of the food matrix and its disintegration during digestion; and  
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21 1398 e) the direct/ indirect interaction of food matrix with the lipid phase, modulating  
22  
23 1399 digestion (prevention of lipid droplet disruption, reduction of lipase activity, binding  
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25 1400 of bile salts) and absorption (modulation of mass transfer, e.g. enzyme or bile salt  
26  
27 1401 diffusion, micelle hydrodynamic volume) (Bohn, 2008; McClements et al., 2008).  
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32 1402 Thus, encapsulation of carotenoids adopting interfacial and structural engineering practices  
33  
34 1403 can also promote the bioavailability of carotenoids, via: i) improved stability against  
35  
36 1404 isomerization and degradation, such as being the case for epoxy-carotenoids (undergoing  
37  
38 1405 epoxide-furanoid transition due to the acid gastric pH); ii) enhanced solubility and increased  
39  
40 1406 bioaccessibility in the gut; iii) target release kinetics e.g. for a precise delivery or release  
41  
42 1407 patterns over time in the small intestine (main organ for carotenoid absorption), likewise  
43  
44 1408 minimizing potential negative effects of other matrix constituents such as dietary fiber.  
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#### 47 *LLCs encapsulated carotenoids*

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49 1410 Most studies scrutinizing the impact of encapsulation on carrier physicochemical and  
50  
51 1411 colloidal characteristics have been conducted on o/w micro- or nano-emulsions. Carotenoid  
52  
53 1412 type and amount of added to delivery systems are known to influence their bioaccessibility.  
54  
55 1413 In general, increasing the carotenoid amount is related with a higher recovered fraction at the  
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3 1414 end of the digestion process (Wang et al., 2012a). However, higher doses tend to lower  
4  
5 1415 bioavailability, possibly due to saturation processes during absorption (Bohn, 2008).  
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7 1416 The molecular structure of the lipid carrier is critical for carotenoid bioaccessibility; their  
8  
9 1417 bioaccessibility is enhanced by long chain TAGs compared to medium or small chain TAGs  
10  
11 1418 (Qian et al., 2012a; Tyssandier et al., 2001), in part as the latter are taken up via the portal  
12  
13 1419 vein and contribute less to micelle formation. The bioaccessible  $\beta$ -carotene fraction in in-  
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15 1420 vitro digested nanoemulsions prepared with long-chain (corn oil), medium chain triglycerides  
16  
17 1421 (MCT) or orange oil was drastically reduced by decreasing TAG chain length (Qian et al.,  
18  
19 1422 2012a), (Table 3), possibly due to the ability of LCT to form mixed micelles with a large  
20  
21 1423 hydrophobic core, adequately accommodating  $\beta$ -carotene. In addition, orange oil was very  
22  
23 1424 poorly digested. Similarly,  $\beta$ -carotene bioaccessibility emulsified either in corn oil or lemon  
24  
25 1425 oil was lower in the non-digestible oil system, as carotenoids may become trapped in the oil  
26  
27 1426 droplets (Rao et al., 2013). A linear relationship between  $\beta$ -carotene bioaccessibility and the  
28  
29 1427 amount of FFAs released during lipolysis was also detected. It is also noticeable that TAG  
30  
31 1428 lipolysis is more crucial for carotenes than for xanthophylls (Tyssandier et al., 2001).  
32  
33 1429 Xanthophylls are situated mainly in the oil/water interface rather than in the hydrophobic  
34  
35 1430 core of lipid droplets, facilitating their transport to aqueous medium during the micellization  
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37 1431 process (Tyssandier et al., 2001) and their release for subsequent enterocyte uptake.  
38  
39 1432 Synergism between TAG composition (LCT vs MCT) and oil concentration regarding  $\beta$ -  
40  
41 1433 carotene bioaccessibility in low (1% w/w) and high (4% w/w) fat nanoemulsions was  
42  
43 1434 recently studied. Though oil digestibility was linearly reduced in the high fat and high LCT  
44  
45 1435 content systems, the amount of oil in the lipid phase modifying  $\beta$ -carotene bioaccessibility  
46  
47 1436 was MCT to LCT ratio dependent (Salvia-Trujillo et al., 2013a). For low fat systems, a  
48  
49 1437 negative linear correlation between FFAs released during digestion and  $\beta$ -carotene  
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51 1438 bioaccessibility was observed, with a higher LCT:MCT ratio favoring  $\beta$ -carotene  
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3 1439 bioaccessibility. For high fat systems,  $\beta$ -carotene bioaccessibility decreased when the LCT  
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5 1440 concentration in the oil phase increased from 0 to 50%, whereas a further increase of the LCT  
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7 1441 **percentage** (from 50 to 100%) enhanced bioaccessibility. The reduced bioaccessibility at high  
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9 1442 to intermediate MCT:LCT ratios was associated with an increase of non-digested TAGs,  
10  
11 1443 leading to higher retention of  $\beta$ -carotene in the core of the non-digested lipid droplets.  
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13 1444 **Mean lipid droplet size** is another factor that may modify carotenoid bioaccessibility. **For**  
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15 1445 **example**, reducing lipid droplet size in microfluidized LLCs improved the bioaccessibility of  
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17 1446 zeaxanthin (**3 to 33%**), and  $\beta$ -carotene (**2 to 18%**) (Cha et al., 2011). Though lipid droplet  
18  
19 1447 size can dramatically be affected by physicochemical phenomena (droplet coalescence,  
20  
21 1448 disruption, dissolution) during **digestion**, the presence of small lipid droplets may enhance  
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23 1449 carotenoid bioaccessibility, due to the increased surface area of the lipid droplets exposed to  
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25 1450 lipolytic enzymes and surface active compounds, facilitating **micellization** (Yonekura and  
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27 1451 Nagao, 2007). Salvia-Trujillo et al. (2013b) showed that reducing lipid droplet size from 23  
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29 1452 to 0.23  $\mu\text{m}$  (4% corn oil based o/w emulsions containing 0.5% (w/w)  $\beta$ -carotene, 1.5%  
30  
31 1453 Tween 20) increased  $\beta$ -carotene bioaccessibility from 34 to 59%. A positive correlation of  
32  
33 1454 carotenoid bioaccessibility and the completeness of lipid digestion was **also** detected.  
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35 1455 Droplet size is also associated with carotenoid bioaccessibility due to the effect of bile salts  
36  
37 1456 and lipase. (Wang et al., 2012a) demonstrated that bile and lipase exert a governing role on  
38  
39 1457 micellar carotenoid recovery in the presence of large lipid droplets (e.g. 0.68 to 18  $\mu\text{m}$ ) while  
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41 1458 no influence on carotenoid solubilization and micelle formation was detected when  
42  
43 1459 nanodispersions with particles  $<100$  nm were tested. However, the latter systems improved  $\beta$ -  
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45 1460 carotene bioaccessibility (**48 to 61%**). This suggests the existence of a lower particle size  
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47 1461 threshold where the disruption of the lipid droplets via the action of bile and pancreatic lipase  
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49 1462 can be achieved, whereas a further size reduction can enhance carotenoid bioaccessibility  
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51 1463 only via facilitating **transport** of the carotenoid molecules to mixed micelles.  
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3 1464 The composition and colloidal properties of the interfacial layers surrounding the lipid  
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5 1465 droplets may also influence carotenoid availability. This may be attributed to the: a) increased  
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7 1466 stability of lipid droplets against coalescence or disruption during GI passage, b) modulation  
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10 1467 of lipid droplet exposure to intestinal enzymes and bile salts, and c) control of the transfer of  
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12 1468 carotenoids from the lipid droplets to the mixed micelles, via competitive absorption of  
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14 1469 surface active compounds to the lipid droplets during digestion.  
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16 1470 Parameters such as electrostatic charge, thickness, permeability, microviscosity, and  
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18 1471 environmental response of the lipid droplets are known to impact the transfer of lipophilic  
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20 1472 compounds to mixed micelles (McClements et al., 2008; Troncoso et al., 2012). The  
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22 1473 bioaccessibility of carotenoids loaded into interfacial engineered lipid droplets via surface  
23  
24 1474 active compounds such as milk proteins (sodium caseinate, whey proteins), soy protein  
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26 1475 isolates, sucrose esters, polysorbates or polyglycerol esters of fatty acids has been extensively  
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28 1476 studied (Table 3). Liu et al., (2012) investigated the impact of the interfacial layer  
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30 1477 composition (whey protein isolate, decaglycerol monostearate and soybean soluble  
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32 1478 polysaccharides) of lipid droplets of LCCs loaded with  $\beta$ -carotene on their bioaccessibility.  
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34 1479 The authors reported that the surfactant type pronouncedly affected the stability of lipid  
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36 1480 particles during in vitro digestion. Whey protein stabilized interfacial layers exerted the  
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38 1481 lowest stability (droplet size increased from 0.6 to 18  $\mu\text{m}$ ) in the gastric phase, probably due  
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40 1482 to their susceptibility to pepsin, disintegrating the interfacial layers, promoting droplet  
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42 1483 flocculation (Liu et al., 2012; Nik et al., 2011). Emulsion exposure to duodenal and intestinal  
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44 1484 fluids remarkably reduced particle size, with the WPI- and SSPS-stabilized ones showing the  
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46 1485 strongest response. Whey proteins in the interfacial layers surrounding the lipid droplets were  
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48 1486 of highest  $\beta$ -carotene bioaccessibility. This was primarily attributed to the ability of the whey  
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50 1487 proteins absorbed to the oil/water interface to unfold and covalently cross-link, enhancing the  
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52 1488 lipase action at the interfaces and therefore the extent of emulsified  $\beta$ -carotene. The lower  
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3 1489 biaccessibility of the SSPS stabilized lipid droplets was attributed to soluble dietary fiber,  
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5 1490 suppressing  $\beta$ -carotene transport to the aqueous phase (Yonekura and Nagao, 2009).

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7 1491 Soluble dietary fiber present in the continuous phase of LLCs has been identified to adversely  
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9 1492 impact carotenoid bioaccessibility (Yonekura and Nagao, 2009). Several mechanisms have  
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11 1493 been suggested, including a) reduced enzyme activity (pancreatic lipase); b) adsorption of  
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13 1494 fiber to the interfacial layers surrounding the lipid droplet, reducing the accessibility to  
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15 1495 lipolytic enzymes; c) increased bulk and viscosity of the aqueous phase, reducing the mass  
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17 1496 transfer (diffusion) rates of molecules (e.g. bile salts, enzymes, micelles) to and from the lipid  
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19 1497 droplet surface; d) binding bile salts, hindering their emulsifying activity.

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21 1498 Yonekura and Nagao (2009) investigated the effect of several soluble dietary fibers (medium-  
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23 1499 and high-viscosity sodium alginate, apple and citrus pectin, methyl- and carboxymethyl-  
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25 1500 cellulose) on the micellization and (Caco-2) cellular uptake of  $\beta$ -carotene/ lutein emulsified in  
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27 1501 soybean oil droplets. Though all fiber-containing systems reduced carotenoid  
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29 1502 bioaccessibility, the mechanisms depended on the hydrocolloid type. Sodium alginate  
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31 1503 appeared to reduce carotenoid bioaccessibility mainly by increasing the macroviscosity of  
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33 1504 the bulk aqueous phase and forming hydrogel aggregates, entrapping lipophilic matter in  
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35 1505 the gastric phase, while pectins exerted a more complex activity that did not solely rely on  
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37 1506 their viscosifying action but presumably on their bile salt binding activity as well.

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39 1507 Recently, the impact of pectin concentration and degree of methyl-esterification (DE) on the  
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41 1508 bioaccessibility of  $\beta$ -carotene loaded LLCs was studied (Verrijssen et al., 2014). Increasing  
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43 1509 pectin concentrations did not significantly change colloidal structures and bioaccessibility of  
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45 1510  $\beta$ -carotene during GI passage (Table 3). However, DE affected both the colloidal state of the  
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47 1511 lipid droplets and microviscosity of the bulk aqueous phase throughout GI transit, and  
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49 1512 consequently bioaccessible  $\beta$ -carotene. Most bioaccessible  $\beta$ -carotene (ca. 60%) was detected  
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51 1513 in digested emulsions comprising high DE pectin (66 or 99%), whereas digesta containing

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3 1514 low DE pectin (14%) bioaccessible  $\beta$ -carotene was lower (ca 35%). This was attributed to the  
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5 1515 formation of gel-like aggregates (via ionotropic interactions of galacturonic acid units with  
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7 1516  $\text{Ca}^{2+}$ ), entrapping  $\beta$ -carotene, reducing lipase activity due to sterical hindrance associated  
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10 1517 with constrained mass transport (controlled by viscosity) or reduced droplet surface area,  
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12 1518 limiting enzymatic attack. Furthermore, the low DE pectins were associated with limited lipid  
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14 1519 digestibility and adsorption of lipophilic compounds to the droplet interfaces.

#### 1516 *Bioaccessibility of carotenoids encapsulated in solid micro- and nano-particulates*

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1521 Solid encapsulation matrices include dry particulates, hydrogel microbeads, molecular  
1522 assemblies, solid lipid carriers etc. To date, a rather limited number of studies have been  
1523 conducted on the impact of structural aspects of solid-based encapsulation vehicles, their  
1524 disintegration, and the colloidal changes of their particular components on the bioavailability  
1525 of encapsulated bioactive compounds. Donhowe et al., (2014) evaluated the release and  
1526 bioaccessibility of  $\beta$ -carotene encapsulated either in maltodextrin spray dried microcapsules  
1527 or alginate-chitosan microbeads (prepared by ionotropic gelation), incorporated in two  
1528 different fat-free food products (tapioca pudding, yogurt). Highest  $\beta$ -carotene bioaccessibility  
1529 was achieved in the spray dried matrices (13 and 1% for pudding and yogurt, respectively),  
1530 while the amount of bioaccessible  $\beta$ -carotene in the gelled microbeads was as low as 0.2 %,  
1531 regardless the food matrix. This was ascribed to the restricted mass transport of pancreatic  
1532 lipases and bile to and from the lipid droplets interfaces embedded in the hydrogel matrix and  
1533 limited micellization due to soluble dietary fiber present at the intestinal phase.

1534 Encapsulation of  $\beta$ -carotene in WPI-alginate-chitosan microbeads was assessed as a strategy  
1535 to enhance the carotenoid content of almond butter and to improve its bioaccessibility  
1536 (Roman et al., 2012). The authors reported that the bioaccessible fraction of both free and  
1537 encapsulated  $\beta$ -carotene was below 1%. It was deduced that especially the binding of  
1538 carotenoids (via the emulsification of lipid phase) by whey protein and the hindrance of the

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3 1539 micellization process (due to soluble fiber) were responsible for these results. On the other  
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5 1540 hand, nanoparticles based on low MW chitosan cross-linking initiated by tripolyphosphate  
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7 1541 resulted in 28% higher lutein bioaccessibility compared to artificial mixed micelles  
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9 1542 (Arunkumar et al., 2013). It was believed that the restricted hydrophobic interaction between  
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11 1543 chitosan and lutein was the major parameter enhancing carotenoid micellization.

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14 1544 NLCs also showed good release in vitro compared to conventional LLCs. Lutein release from  
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16 1545 encapsulated NLCs (glycerol stearate, fish oil and carnauba wax in buffered saline media)  
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18 1546 increased by ca. 30% compared to conventional nanoemulsions (no fish oil, Lacatusu et al.  
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20 1547 (2013)). Fish oil was crucial for lutein release, probably as it modulated carotenoid  
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22 1548 hydrophobic binding in the emulsified lipid phase. A similar lutein release was found using  
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24 1549 diffusion cells with dialysis membranes (Liu and Wu 2010). However, lutein encapsulated in  
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26 1550 lyophilized NLCs of solid lipids (glyceryl palmitostearate, palmitic acid MAGs, C:12-C:16  
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28 1551 FA.), surfactants (polysorbates, Pluronic F68) and corn oil was of slower release (in media)  
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30 1552 compared to LLCs (based on caprylic/capric TAGs, identical to NLCs surfactants) after 24h.  
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32 1553 Lutein released in simulated gastric/intestinal fluids followed the order of SIF>SIF (no  
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34 1554 pancreatin)>GF(no pepsin)>GF. Only for SIF there was an increased lutein release rate  
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36 1555 during the first 6h, indicating disintegration of the lipid structures due to pancreatic lipase. In  
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38 1556 the other systems, a gradual increase of the released lutein during the first 24h was observed,  
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40 1557 reaching eventually a plateau, suggesting good resistance of the NLCs to gastric juice.

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43 1558 In vitro release (in PBS-SDS medium) of lutein encapsulated in nanoparticles prepared by  
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45 1559 supercritical fluids exhibited differences compared to pure lutein and a lutein-zein mixture  
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47 1560 (Hu et al., 2012). A near zero-order release was detected for the latter, without an initial  
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49 1561 release burst as for pure lutein/the zein-lutein mixture. The slow release was attributed to the  
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51 1562 restricted diffusion of the solute molecules from the bulk aqueous phase into the solid matrix  
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53 1563 due to the zein polymeric network. However, the amount of lutein released after 300 min was

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3 1564 equal for all test systems, indicating that temporal water upholding leads to the relaxation of  
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5 1565 polymeric entanglements, facilitating the transfer of lutein to the bulk aqueous phase.  
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7 1566 *Cellular uptake of encapsulated carotenoids*

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10 1567 Carotenoid absorption is a complex dynamic process involving different physicochemical and  
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12 1568 biochemical phenomena, including their release from the food matrix, solubilization into  
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14 1569 mixed micelles in the gut, uptake by enterocytes, incorporation into chylomicrons and  
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16 1570 secretion into the lymph (Harrison, 2012). Carotenoid absorption efficacy as well as their  
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18 1571 tissue concentrations are known to depend on the molecular structure and physicochemical  
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20 1572 profile, e.g. hydrophobicity (logP, logD) (Sy et al., 2012). Though human studies are still  
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22 1573 perceived as the “gold standard” to assess carotenoid bioavailability, restrictions such as the  
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24 1574 need to administer high amounts of carotenoids in order to observe significant variations in  
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26 1575 plasma, and ethical and cost constraints pose limits (Biehler and Bohn, 2010). In vitro testing  
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28 1576 of carotenoids using cells mimicking the human intestinal epithelium (e.g. Caco-2) can be a  
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30 1577 convenient, inexpensive and reproducible tool to evaluate the digestive stability,  
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32 1578 micellization, uptake and transport as well as metabolism. Parameters such as dissolution  
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34 1579 rate, hydrophilicity, particle size and surface area, cis-trans-isomerization, lipid  
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36 1580 polymorphism, surfactants (e.g. lysophosphatidylcholine, FFA), presence of free vs.  
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38 1581 esterified protein bound complexes, and interactions with dietary compounds (lipids, fiber,  
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40 1582 phytosterols etc.) have been reported to affect carotenoid cellular uptake (Failla et al., 2008;  
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42 1583 Kotake-Nara and Nagao, 2012; Yonekura and Nagao, 2009).  
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44 1584 Ribeiro et al. (2006) assessed the Caco-2 and HT-29 cellular uptake of astaxanthin and  
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46 1585 lycopene in o/w emulsions prepared by different emulsifiers, namely Tween 20, sucrose  
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48 1586 laurate, whey protein isolate (BiPro®), and hydrolyzed whey protein isolate (BioZate®), both  
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50 1587 containing Tween 20). The presence of whey proteins in the encapsulation carrier system  
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52 1588 resulted in a significant increase of astaxanthin and lycopene cellular uptake (ca. 7- and 11-  
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3 1589 fold, respectively). The enhanced carotenoid uptake in the presence of  $\beta$ -lactoglobulin was  
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5 1590 attributed to its binding capacity through hydrophobic bonds as well as to its molecular  
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7 1591 conformation, facilitating carotenoid emulsification. Takaishi et al., (2012) examined the  
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9 1592 Caco-2 cellular uptake of  $\beta$ -cryptoxanthin in Satsuma mandarin fruit pulp, juice and LLCs  
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11 1593 (5% mandarin extract, 5% triglycerides, 76% glycerol, 9% polyglyceryl fatty acid esters and  
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13 1594 5% water). Emulsified  $\beta$ -cryptoxanthin was incorporated 5-times higher than mandarin juice,  
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15 1595 whereas its esterified : free form ratio decreased by approx. 23% compared to mandarin juice.  
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17 1596 This was explained by the preferential absorption of free  $\beta$ -cryptoxanthin and conversion of  
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19 1597 the esterified to free form during Caco-2 cellular uptake.

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23 1598 Soluble dietary fiber as a main or co-encapsulation component may compromise carotenoid  
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25 1599 absorption. Caco-2 cell uptake of  $\beta$ -carotene/lutein from artificial micelles declined in the  
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27 1600 presence of high viscosity sodium alginate (60% and 51% for  $\beta$ -carotene and lutein  
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29 1601 respectively), apple (66%, 58%) and citrus (78%, 72%) pectins (Yonekura and Nagao (2009).  
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31 1602 In high viscosity aqueous environments, cellular uptake is constrained by slow diffusion.  
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33 1603 Anarjan et al., (2011a) investigated the cellular uptake (HT-29) of astaxanthin loaded in  
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35 1604 nanodispersions prepared with different organic-phases, e.g. DCM, acetone and their  
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37 1605 mixtures. Astaxanthin cellular uptake was maximized with a blend of 31% DCM and 69%  
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39 1606 acetone. Factors such as particle mean size, PDI and concentration of 9-*cis* and 13-*cis*  
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41 1607 isomers significantly influenced astaxanthin uptake, which was higher from fine particulates,  
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43 1608 exerting a high level of polydispersity and low *trans*- to *cis*- isomerization.

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47 1609 Encapsulation of carotenoids via molecular inclusion has been associated with reasonable  
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49 1610 cellular uptake. Pfitzner et al. (2000) investigated several carotenoids in methyl-CD based  
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51 1611 vehicles, using human skin fibroblasts. Beta-carotene within methyl- $\beta$ -CD complexes had a  
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53 1612 40% higher cellular uptake compared to free carotenoids in organic solvent, suggesting good  
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55 1613 bioavailability due to the high solubility and continuous release of the bioactive. However, GI

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3 1614 digestion was not studied. Lancrajan et al. (2001), assessing the impact of liposomes vs. ICs  
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5 1615 based on  $\beta$ -CDs on the incorporation of  $\beta$ -carotene, lutein and canthaxanthin into natural  
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7 1616 membrane fractions (mitochondrial, microsomal and plasma) found that carotenoid  
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9 1617 lipophilicity and membrane characteristics (cholesterol to phospholipid ratio) affected  
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11 1618 absorption into pig liver cells and retinal epithelial cells. While  $\beta$ -CD-lutein complexes  
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13 1619 exerted highest plasma membrane uptake of ICs vs. liposomes (explained by less competition  
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15 1620 with cholesterol),  $\beta$ -carotene showed similar availability for both liposome and  $\beta$ -CD ICs.  
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18 1621 Fernández-García et al. (2010) studied the uptake of  $\beta$ -carotene, lutein and lycopene  
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20 1622 encapsulated in ICs with  $\beta$ -CD by brush border membrane vesicles (BBMVs). Carotenes  
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22 1623 exerted a higher uptake compared to lutein both in their free (carotenoids + Tween 20) and  
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24 1624 microencapsulated (ICs with  $\beta$ -CD) form. Due to the increased  $\beta$ -CD concentration in the  
25  
26 1625 donor solution, a higher amount of carotenoids was available for later assimilation due to the  
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28 1626 shift of the dissociation equilibrium toward the free forms of the inclusion complexes.  
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30 1627 Interestingly, substances hindering receptors involved in carotenoid absorption such as  
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32 1628 lipoproteins did not adversely impact the assimilation process. On the contrary, for both  
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34 1629 carotenes and xanthophylls, a synergistic interaction between  $\beta$ -CDs and lipoproteins  
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36 1630 occurred, promoting the dissociation and release of carotenoids and therefore, their  
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38 1631 bioavailability. Similarly, (Madhavi and Kagan, 2008) disclosed that Caco-2 cellular uptake of  
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40 1632 lutein in CD inclusion complexes was remarkably influenced by parameters such as the  
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42 1633 drying method (spray vs. freeze drying), the CD type ( $\alpha$ -,  $\beta$ -,  $\gamma$ - or hydroxypropyl- $\beta$ -CD) as  
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44 1634 well as the excipient to dissolve the dry CD-carotenoid complexes. Lutein uptake into Caco-  
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46 1635 2 cells was higher for the freeze dried  $\alpha$ - and  $\gamma$ -CD complexes dispersed in vegetable oil  
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48 1636 containing lecithin. These formulations exerted also a better bioavailability in-vivo, affirmed  
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50 1637 in a clinical trial with six healthy subjects following a modest carotenoid rich diet. Plasma  
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3 1638 lutein levels after 24h were 60% higher in subjects who ingested the lutein-CD-vegetable oil-  
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5 1639 lecithin formulation and only 20% when consuming the lutein-vegetable oil.  
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7 1640 Liposomal encapsulation of astaxanthin and uptake into hepatic (Hep3B, HepG2) cells was  
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10 1641 studied by Peng and others (2010). Liposomes were fabricated using phosphatidyl- choline  
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12 1642 (4% w/v/DMSO), cholesterol (1% w/v/DMSO), PLGA (1% w/v/DMSO) added into a binary  
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14 1643 blend of chloroform/methanol, sonicated, solvent evaporated and vacuum dried. The obtained  
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16 1644 liposomes (due to their fine particle size and excellent dispersion) displayed a higher cellular  
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18 1645 uptake than free astaxanthin (in THF or DMSO). After 18h of incubation, astaxanthin  
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20 1646 concentration was 2.4, 1.2 and 0.7 µg/dish (Hep3B), and 2.0, 0.9 and 0.5 µg/dish (HepG2) for  
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22 1647 liposomes, DMSO and THF. Antioxidant activity of intracellular enzymes such as superoxide  
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24 1648 dismutase, catalase and glutathione S-transferase was also 3-fold higher in cells treated with  
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26 1649 the liposome encapsulated astaxanthin compared to its free form.  
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29 1650 Encapsulation of β-carotene in protein (sodium caseinate, whey protein isolate or soybean  
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31 1651 protein isolate) nano-assemblies via emulsification-solvent displacement slightly enhanced its  
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33 1652 antioxidant properties (in Caco-2 cells) compared to its crystalline form. The authors deduced  
34  
35 1653 that the larger particles' surface area and enhanced β-carotene solubility in the aqueous  
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37 1654 medium due to its amorphous state and the intermolecular hydrophobic interactions with  
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39 1655 proteins were associated with this observation. Similarly, carotenoid bioavailability from β-  
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41 1656 CN microparticles was improved due to their distribution over a very large surface area of the  
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43 1657 caseins, promoting digestion, mixed micelles incorporation and absorption. In addition, the  
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45 1658 open tertiary molecular structure of the re-assembled β-CN facilitates access to proteases and  
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47 1659 the sustained release of carotenoids (Danino et al., 2011). Finally, in-vitro studies have  
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49 1660 suggested that the cytotoxicity of lipophilic bioactive compounds, e.g. curcumin can be reduced  
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51 1661 upon their enclosure in β-CN assembled matrices contrarily to other encapsulating agents  
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3 1662 such as chemically modified starches or CDs (Esmaili et al., 2011; Pan et al., 2013), though  
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5 1663 results may depend on **cell lines** and resulting uptake and metabolism capabilities.  
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7 1664 *In vivo studies related to bioavailability of encapsulated carotenoids*

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10 1665 **Though** in vitro studies can provide insights into the colloidal, physicochemical and structural  
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12 1666 principles governing the bioavailability of nutrients, in most cases (due to the complexity of  
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14 1667 the human digestive system), in vivo studies with animals or humans are necessary to obtain  
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16 1668 a more reliable perception of the processes of **digestion and absorption**. With respect to  
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18 1669 carotenoids, only few studies have been conducted using encapsulated forms, in contrast to  
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20 1670 studies with raw or processed plant food matrices, e.g. fruits and vegetables. With respect to  
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22 1671 animal studies, one of the main parameters to be considered is the cleavage efficacy of  
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24 1672 provitamin A carotenoids (Biehler and Bohn, 2010; Borel, 2012), with **ferrets**, preruminant  
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26 1673 calves, and gerbils being regarded as best models to study carotenoid absorption.  
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29 1674 Faisal et al., (2013) created a self-emulsifying drug delivery system (SEDDS) comprised of  
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31 1675 40% LCT (olive oil), 20% surfactant (Cremophor RH), and co-surfactant (Tween 85), a solid  
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33 1676 dispersion (SD) based on 100% gelucire, as well as a lipid based solid dispersion (LBSD) for  
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35 1677 oral lycopene administration. Following **dosing to fasted pigs, lycopene encapsulated in**  
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37 1678 **SEDDS was not quantifiable, while for SD, after an initial lag phase, lycopene was detected**  
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39 1679 **in the plasma of pigs, reaching a maximum concentration (5.5 ng/mL) at 10h. Comparing the**  
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41 1680 **bioavailability of micellar amorphous and LBSD encapsulated lycopene, a 2.4-fold increase**  
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43 1681 **in plasma was detected compared to the more delayed peaking of the micellar form ( $t_{peak} =$**   
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45 1682 **10.8h). It was deduced that the formulation solubilization and the ability of the excipients to**  
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47 1683 **stimulate lymphatic carotenoid transport were bioavailability determinants.**  
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50 1684 **Absorption of lutein encapsulated in self-emulsifying suspensions (SEPS) by rats and beagle**  
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52 1685 **dogs was studied by Shanmugam et al., (2011). A lutein suspension (25 mg, 40% in**  
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54 1686 **sunflower oil) was emulsified in a blend of MCT phospholipids (0, 250, 500 mg), Tween 80**  
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3 1687 (75 mg), glycerol (30 mg),  $\alpha$ -tocopherol (10 mg) and propylene glycol caprylate (50 mg). The  
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5 1688 emulsions were filled into hard gelatine capsules. Lutein emulsified by phospholipids  
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7 1689 increased plasma concentrations 4-11 fold compared to those without phospholipids or the  
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10 1690 commercial suspension (CF) of (non-emulsified) lutein. Similarly, relative bioavailability of  
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12 1691 the emulsion systems containing 250 and 500 mg of MCT phospholipids was 180 and 470%  
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14 1692 higher compared to that of LLCs without phospholipids. The ability of phospholipids to  
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16 1693 facilitate the transition of lutein from the lipid phase to mixed micelles and therefore its  
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18 1694 enterocyte uptake can explain these observations. In the same study, lutein amounts in eye  
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20 1695 tissues of rats fed with SEPS delivered lutein was 16 and 4 times higher compared to placebo  
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22 1696 (vegetable oil without lutein) and CF. High amounts of phospholipids may promote HDL  
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24 1697 formation, known lutein transfer vehicles to extrahepatic tissues including the eye.  
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26 1698 Taha and others (2007) studied the vitamin A bioavailability enhancing capacity of a SEDDS  
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28 1699 system composed of vitamin A acetate and palmitate, emulsified into a lipid phase containing  
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30 1700 soybean oil, polyoxyl 35 castor oil, MC mono- and di-glycerides, either filled into HPMC  
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32 1701 hard capsules or mixed with microcrystalline cellulose and compressed into tablets. Vitamin  
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34 1702 A bioavailability of SEDDS in form of capsules and tablets was 207 and 144% higher than  
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36 1703 that of soybean oil-vitamin A suspensions. The authors deduced that dissolution is the rate-  
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38 1704 limiting step in absorption and bioavailability of vitamin A and therefore the presence of  
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40 1705 surfactant/co-surfactant facilitates the incorporation of retinol into mixed micelles.  
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42 1706 Arunkumar et al., (2013) determined the appearance of lutein in plasma, eye or liver tissue of  
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44 1707 mice fed with either a chitosan encapsulated form or with micellar lutein prepared by organic  
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46 1708 solvent dissolution and evaporation. The encapsulation of lutein in chitosan carriers was  
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48 1709 associated with higher lutein appearance in plasma (55%), liver (54%) and eye tissues (63%).  
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50 1710 It was assumed that the fine particle size and the prolonged plasma half-life of the  
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52 1711 nanocapsules increased lutein tissue levels.  
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1712 **CONCLUSIONS**

1713 A variety of strategies have been sought to encapsulate labile nutritious and health beneficial  
1714 compounds such as carotenoids **to reap** their full benefits as bioactive functional food  
1715 ingredients, including spray drying, freeze-drying, liposome formation, coacervation,  
1716 extrusion, or via inclusion complexes. Strategies to enhance carotenoid stability against  
1717 detrimental environmental conditions during processing and/or storage such as light,  
1718 temperature, oxygen, and undesired reactions with other food compounds such as reactive  
1719 oxygen species or metal ions have **focused** on micro- and nanoencapsulation, including  
1720 particles generated by LLCs, SLNs, NLCs, SCF or self-assembly. Promising materials to  
1721 generate emulsions **include proteins** (e.g. caseins), Tween, maltodextrins or other  
1722 polysaccharides such as pectins, and inclusion complexes **such as by** CDs could constitute  
1723 promising candidates. Many strategies have highlighted the technological feasibility to  
1724 produce carotenoid encapsulated materials that are sufficiently stable, with a high loading  
1725 capacity, and being of sufficiently small size to be integratable into a variety of products  
1726 without causing detrimental effects on quality attributes such as sensorial ones.

1727 Another, less studied aspect is the potential positive effect that encapsulated carotenoids  
1728 could pose on bioavailability. Especially emulsions with particles of small size and being  
1729 digestible **GI**, such as gelatins, have shown promising results in terms of bioaccessibility and  
1730 in part in bioavailability, by facilitating matrix release, enhancing micelle formation and  
1731 promoting rapid transfer to the enterocytes, allowing for targeted GI **delivery**. Future studies  
1732 on food grade formulations will have to enhance the body of evidence that such formulations  
1733 will not only be beneficial with respect to product **stability**, but can also enhance the  
1734 bioactivity of these promising compounds via improving aspects of bioavailability.

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2323 **FIGURE CAPTIONS:**

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2325 **FIG. 1:** Cause and effect diagram illustrating parameters associated with processing  
2326 conditions and matrix compositional and structural characteristics influencing the chemical  
2327 stability of carotenoids

2328 **FIG. 2:** Visualization of the microstructural aspects of micronized (A: crystalline structure),  
2329 and microencapsulated (B: amorphous structure)  $\beta$ -carotene implementing supercritical fluid  
2330 technology. In both cases, the nanoprecipitates were obtained using a pressure of 120 bar, and  
2331 a temperature of 313K; flow rates of organic solution and antisolvent were  $1 \text{ mL min}^{-1}$  and  $40$   
2332  $\text{mL min}^{-1}$  and  $\beta$ -carotene content was set at  $4 \text{ mg mL}^{-1}$  (image adopted by Priamo et al.,  
2333 (2010) and reproduced with the permission of Elsevier).

2334 **FIG. 3:** Formation of carotenoids loaded into casein self-assemblies.

2335 **FIG. 4:** Mechanistic overview of the formation of Maillard reaction derived protein-  
2336 carbohydrate conjugates for encapsulating carotenoids.

2337 **FIG. 5:** Illustration of different strategies for the formation of solid liquid nanoparticles  
2338 (SLNs) or nanostructured lipid carriers (NLCs). In general, the NLCs exert a better stability  
2339 against polymorphic transitions occurring during processing and storage and therefore  
2340 enhanced controlled release properties and chemical stability of carotenoids.

2341 **FIG. 6:** Schematic representation of the fabrication of carotenoid loaded nanoparticles using  
2342 the solvent displacement method (modified from Ribeiro et al., (2008)).

2343 **FIG 7:** Illustration of the production of encapsulated carotenoids into nanoparticles using the  
2344 emulsification – solvent evaporation method.

2345 **FIG. 8:** Schematic overview of structural and colloidal transformations of encapsulation  
2346 carrier systems taking place during oral, gastric and duodenal/small intestine phase  
2347 (illustration of the human digestive system reproduced from Wikipedia as a free- licensed  
2348 material).

TABLE 1: Effects of wall material, drying and storage conditions on the encapsulation efficiency, particle mean size and morphology, and carotenoid stability in dried microparticulates.

Ingredient	Drying method and conditions	Carotenoid type	Encapsulation efficiency (%)	Surface coverage (%)	Particle mean size ( $\mu\text{m}$ )	Morphology of microcapsules	Retention rate throughout storage (% , days, conditions)	Reference
Native tapioca starch	Spray drying 170°C, 95°C	$\beta$ -carotene	68.4	104	106-250	Spherical, inner hollow	nd	(Loksuwan, 2007)
Acid modified tapioca starch	Spray drying 170°C, 95°C	$\beta$ -carotene	82.2	19.6	75-150	Spherical, inner hollow	nd	(Loksuwan, 2007)
Chemically modified maize starch (Capsul®)	Spray drying 180°C, 98°C, 0.6L/h	lycopene	21-30	nd	nd	Spherical, inner hollow, surface dents	78-83% (73 d, 10°C, air) 58-67% (73 d, 25°C, air)	(Rocha et al., 2012)
Maltodextrin DE24	Spray drying 170°C, 95°C	$\beta$ -carotene	46.7	73	106-250	Spherical, inner hollow	nd	(Loksuwan, 2007)
Maltodextrin DE25	Spray drying 170°C, 95°C	$\beta$ -carotene	nd	nd	nd	nd	nd	(Loksuwan 2007)
Gum arabic – sucrose (4:1)	Spray drying 170°C, 113°C	lycopene	94-96	nd	nd	Spherical, surface dents, absence of cracks	nd	(Nunes and Mercadante, 2007)
Gum arabic – sucrose (19:1) Maltodextrin DE20 Maltodextrin DE20 – sucrose (4:1) Maltodextrin DE20 – Tween 80 (499:1)	Spray drying	nd	nd	nd	nd	nd	nd	(Barbosa et al., 2005)
Sodium caseinate – lactose (1:1)	Spray drying 180°C, 83°C, 433kg/h	astaxanthin	86.1	0.04	6-100	Spherical, surface dents	74, 60 and 47% (26 d, 5,25 and 40°C, air)	(Pu et al., 2011)
Whey protein isolate – maltodextrin DE20	Spray drying 160-180°C, 70-80°C, 2L/h	astaxanthin	63-93	nd	2-25	Spherical, surface dents	45-54% (10 d, 33%RH, 45°C, air or nitrogen)	(Shen and Quek, 2014)
Soybean polysaccharide (SSPS)	Spray drying 170°C, 95°C, 0.3L/h	canthaxanthin	78.5 – 90.1	10.3-14.3	0.02-0.2	Spherical, smooth surface	44-57% (16 wks, 25°C, air) 63-75% (16 wks, 25°C, dark)	(Hojjati et al., 2011)
Gelatine – sucrose (3:7)	Spray drying	lycopene	12-82 (6-90% extract purity)	nd	2-15	Spherical, bee-net like inner structure	80% (28 days, 0°C, air)	(Shu et al., 2006)
Gellan gum-maltodextrin DE10 Arabic gum – maltodextrin DE10 Mesquite gum – maltodextrin DE10	Spray drying 170°C, 80°C, 1.2L/h	nd	nd	nd	nd	Spherical, inner hollow, surface dents, porous shell	nd	(Rodríguez-Huezo et al., 2004)
Arabic gum-pequi fruit	Spray drying	total	8-52	nd	1-500	Spherical, smooth	nd	(Santana et

pulp	152-200°C, 108-149°C,	carotenoids				surface		al., 2013)
Microalgal paste	Spray drying 180°C, 70°C	fucoxanthin, diadinoxanthin	75	nd	nd	nd	negligible (35 d, -20, 5 and 20°C vacuum, dark)	(Ryckeboosch et al., 2011)
Tomato pulp	Spray drying	lycopene	nd	nd	nd	Nd	nd	(Goula et al. 2012)
Paprika oleoresin	Spray drying 160-200°C, 110°C	total carotenoids	nd	nd	nd	nd	(vacuum, P)	(Rascón et al., 2011)
Casein plus SSPS ( 0.3% w/v)	Spray drying	bixin	90	nd	0.09	nd	nd	Zhang and Zhong (2013)
Maltodextrin DE25	Freeze drying -35°C	β-carotene	92%	35%	80	nd	50% (105 d, 25°C, 32% RH, air, light exposure)	(Desobry et al., 1997)
Pullulan	Freeze drying -18°C,	saffron carotenoids	nd	nd	nd	nd	nd	(Selim et al. 2000)
Egg yolk solids	Freeze drying -	lutein zeaxanthin canthaxanthin	nd	nd	nd	nd	nd	(Wenzel et al. 2010)
Gelatine – trehalose	Freeze drying -110°C, 4×10 <sup>-1</sup> mbar	β-carotene	nd	nd	nd	nd	(156 d, 25°C, 11,44 and 75% RH, air)	(Elizalde et al., 2002)
β-cyclodextrin carotenoid to β-CD molar ratios 1:1 and 1:4	Freeze drying -18°C	lycopene	50% for 1:4 no complex formation for 1:1	nd	nd	Irregular structures of varying size Presence of small CD fragments	nd	(Nunes and Mercadante, 2007)

Nd: not determined; CD: cyclodextrin, DE: dextrose equivalent, RH: relative humidity.

TABLE 2: Overview of methods for encapsulating carotenoids by supercritical fluid techniques, including parameters characterizing the performance of the employed methods.

Method	Carotenoid and coating type	Pressure (MPa)	Temperature (°C)	CO <sub>2</sub> flow rate (mL/min)	Solution flow rate (mL/min)	Core to coating ratio	Encapsulation efficiency (EE) or variation coefficient (CV), (%)	Particle mean size (µm)	Particle morphology	Reference
RESS	Rutin, PEG	20	40	nd	nd	1:2, 1:10	EE: 22.6 for 1:2; EE: 44.2 for 1:10	42.9	Amorphous, flaky agglomerates	(Santos and Meireles, 2013)
SAS	Bixin extract, PEG	10	40	0.6, 1.5	1	1:2, 1:10	EE: 62	33	Flaky agglomerates	(Santos and Meireles, 2013)
SAS	β-carotene, lutein, PEG	8 for β-carotene 8-10 for lutein	15	2.5, 3.5	1.7 kg/h	1:10, 3:40 for β-carotene 1:4-1:12 for lutein	nd	~1 for β-carotene ~50 for lutein	Spherical PEG particles deposited on β-carotene Spherical and amorphous PEG particles	(Martín et al., 2007)
SEDS	β-carotene, PHBV	8-12	40	20-40	1	1:10-2:5	VC: 21-31	0.28 – 0.57	Quasi spherical interconnected particles	(Franceschi et al., 2008)
SEDS	β-carotene, PHBV	8-20	40	40	1	1:15-1:1	EE: 1.8-55.5	<1.5	Quasi spherical interconnected particles	(Priamo et al., 2010)
SEDS	astaxanthin, PHBV	8, 10	35	20	1	1:4-1:2	EE: 21.5-48.3	0.13-0.27	nd	(Machado Jr et al., 2014)
SEDS	lutein, zein	10-15	32-45		0.5 to 1	1:24-1:12	nd	nd	nd	(Hu et al., 2012)
SEDS	lycopene, β-CD	10-14	40-50	15-25	0.25-0.75		nd	0.04-0.15	Spherical particles of varied level of agglomeration	(Nerome et al., 2013)
SEDS	β-carotene, PHBV	8	40	39	1	1:40-2:5	EE: 16.7-34.7	nd	Quasi spherical particles of varied porosity; evidence of β-carotene deposited on surface at low PHBV amounts	(Franceschi et al., 2010)
PGSS	β-carotene, soybean lecithin	8.1-10.2	102-132	n/a	GPR: 21-32	1:169 - 1:221	EE: 29-59	13.4-448	Collided spherical particles exerting high agglomeration	(de Paz et al., 2012a)
PGSS	β-carotene, poly-ε-caprolactones (CAPA) (MW 4000 & 10000)	11, 15	50, 70	n/a	n/a	1:8-1:4	EE:	111-652	Flat or sphere like particles attached and agglomerated by long polymer filaments (MW 10000); no agglomeration for CAPA MW 4000	(de Paz et al., 2012b)

SFEE	$\beta$ -Carotene, lycopene, OSA-modified starch	7-13	80	n/a	2.5-5.5	n/a	EE: 34-89	345-366	Spherical shaped particles of low porosity (spray dried material obtained from the SF treated nanoemulsions)	(Santos et al., 2012)
SFEE	Astaxanthin, Pluronic F127	8-12	35-45	1-5	1-5	1:5-5:6	EE:19.7-93.1	nd	Flat, flaky particles (co-precipitates); Spherical particles with evidence of very low agglomeration (spray dried material)	(Mezzomo et al., 2012)

CD: cyclodextrin; GAS: gas anti-solvent; GPR: gas to product ratio, n/a: not applied; MW: molecular weight; nd: not determined; OSA: octenyl succinic acid; PEG: polyethyleneglycol; PGSS: particles from gas-saturated solutions; PHBV: copolymer of 3-hydroxybutanoic acid and 3-hydroxypentanoic acid; RESS: rapid expansion of supercritical fluids; SAS: supercritical anti-solvent; SEDS: solution enhanced dispersion by supercritical fluids; SF: supercritical fluid; SFEE: supercritical extraction from an emulsion.

TABLE 3: **Compositional, physicochemical and bioavailability** aspects of carotenoids encapsulated in liquid lipid carriers (LLCs).

Carotenoid, concentration	Lipid phase composition	Surfactants	Lipid droplet size ( $\mu\text{m}$ )	Carotenoid retention during storage	Bioavailability aspects				Reference
					Digestion conditions at 37°C	Extent of lipolysis	Bioaccessible fraction	Cellular uptake	
$\beta$ -carotene (0.15% w/w)	MCT (10% w/w)	Decaglycerol monolaurate (ML750); WPI; SSPS (4% w/w)	0.2 (ML750), 0.58 (WPI) and 0.75 (SSPS)	nd	Gastric (pH 2), duodenal and small intestine fluids	nd	64 (ML750), 69 (WPI) and 48% (SSPS)	nd	(Liu et al., 2012)
$\beta$ -carotene (0.05% w/w)	Soybean oil (10% w/w)	SPI (1.5% w/w)	0.31	nd	Gastric (SFGs, pH 2, 1h.), duodenal (PC, COL, PL, BS, pH 6.5, 2h)	80%	32% (without PL) 80% (PL presence)	nd	(Nik et al., 2011)
$\beta$ -carotene (0.05% w/w)	Soybean oil (10% w/w)	SPI (1.5% w/w)	0.23	nd	Gastric (SFGs, pH 2, 1h.), duodenal (BS, BS-COL, BS-PL, BS-PL-COL, BS-PL-COL-LPL, pH 6.5, 2h)	51 to 79%	34 to 80%	nd	(Malaki Nik et al., 2011)
$\beta$ -carotene (0.01% w/w)	Corn oil (10% w/w)	Sodium caseinate (2% w/w)	0.12-37 (fine emulsions); 10.7 (coarse emulsion)	nd	Gastric (SFGs, pH 2, 1h.), duodenal (pH 7, 2h)	66 to 82% (fine emulsions); 60% (coarse emulsion)	50 to 73% for fine emulsions	nd	(Yi et al., 2014)
$\beta$ -carotene (0.01% w/w)	Soybean oil (10% w/w)	WPI (0.5% w/w)	0.18	nd	Gastric (SFGs, pH 2, 1h.), duodenal (BS, BS-COL, BS-PL, BS-PL-COL, BS-PL-COL-LPL, pH 6.5, 2h)	47 (BS), 44 (BS-PL & BS-PL-COL), 64 (BS-COL), 72% (BS-PL-COL-LPL)	31 (BS & BS-PL), 29 (BS-PL-COL), 42 (BS-COL), 49% (BS-PL-COL-LPL)	nd	(Nik et al., 2010)
$\beta$ -carotene (n/a)	Olive oil (5% w/w)	Citrus pectin of varying esterification level e.g. 14, 66 & 99% (1 & 2% w/w)	8.1 and 4.5 for CP99; 5.8 and 4.8 for CP66 3.6; 4.5 for CP14	nd	Gastric (pH 1.3, 2h) and small intestine fluids (urea, pancreatin, lipase, bile extract, pH 7, 2h)	nd	57 to 62% for CP99; 56 to 60% for CP66; 33 to 37% for CP14	nd	(Verrijssen et al., 2014)
$\beta$ -carotene (0.025% w/w)	Soybean oil (10% w/w)	ML750 (0.9% w/w)	0.68- 1.8 for HP (10, 50, 140 MPa) homogenized systems; 18.3 (coarse emulsion)	nd	Gastric (pH 2, 1h), small intestine fluids (pancreatin, bile extract, pH 7.5, 2h)	nd	7.2 to 10% for sub-micron LLCs 5.6 to 6.2% for coarse emulsions	nd	(Wang et al., 2012a)
<b><math>\beta</math>-carotene</b>	<b>Orange oil, 4% oil phase,</b>	<b>1.5% Tween 20</b>	<b>0.2 (initial); 0.8 (intestine)</b>	<b>nd</b>	Oral (pH 6.8, 10min), gastric (pH 2.5, 2h), small intestine fluids (pancreatin, bile extract,	<b>nd</b>	<b>66% for LCT and 2% for MCT</b>	<b>nd</b>	<b>Qian et al., 2012a)</b>

					pH 7, 2h				
$\beta$ -carotene (0.025% w/w)	Orange oil (10% w/w)	$\beta$ -lactoglobulin (2% w/w)	0.078	0, 7, 44 and 57% (5, 20, 37 and 55 °C, 14d, dark, ambient air)	nd	nd	nd	nd	(Qian et al., 2012b)
$\beta$ -carotene (0.075% w/w)	MCT (5% w/w)	WPI (0.5% w/w)	0.2 to 0.5	21, 12, 40, 44 % (pH 3, 4, 6, & 7, 55 °C, 7d, dark, ambient air). 82% (pH 7, 200 $\mu$ m $\alpha$ -tocopherol) (55 °C, 7d, dark, ambient air)	nd	nd	nd	nd	(Xu et al., 2013b)
$\beta$ -carotene (0.02% w/w)	Corn oil + MCT at 0, 25, 50, 75, 100%; 1 & 4% w/w	Tween 20 (1.5% w/w)	0.15 to 0.42	nd	Small intestine fluids (pancreatin, bile extract, pH 7.0, 2h)	85 to 124% at 1% w/w LLCs 32 to 88% at 4% w/w LLCs	14 to 88% at 1% w/w 20 to 91% at 4% w/w	nd	(Salvia-Trujillo et al., 2013a)
$\beta$ -carotene (0.1% w/w)	Linseed oil, rapeseed oil refined palm olein (5% w/w)	Arabic gum (12% w/w)	0.34, 0.36 & 0.43 for LO, RO and RPO	73, 82 & 84% for LO, RO and RPO (2 °C 12 weeks)	nd	nd	nd	nd	(Szterk et al., 2013)
$\beta$ -carotene (0.02% w/w)	Corn oil blended with lemon oil at varying ratios (0, 33, 50, 66 & 100%)	Sucrose monopalmitate (0.4% w/w) Lysolecithin (0.1% w/w)	0.13-0.24 lemon oil presence led to higher lipid hydrodynamic volumes	nd	Oral (mucin, pH 6.8, 10min), gastric (SFG, pH 2.5, 2h), intestinal phase (pancreatin, bile, pH 7, 2h)	0-0.57 mmol/L FFA released Pure lemon oil did not induce lipolysis	5-75%; pure lemon oil systems exerted the lowest $\beta$ -carotene bioaccessibility	nd	(Rao et al., 2013)
$\beta$ -carotene (0.09% w/w)	MCT (30% w/w)	Sodium octenyl succinate starches (HI-CAP 100, CAPSUL, CAPSUL-TA) (21% w/w)	ca. 0.14 for CAPSUL and CAPSUL-TA ca. 0.16 for HI-CAP 100	64-78% for HI-CAP 100; 51-76% for CAPSUL; 56-77% for CAPSUL-TA; LLCs stored at 4 or 25 °C under dark or light and with or without N <sub>2</sub>	Gastric (SGF, pH 2.0, 1h) and small intestine phase (pancreatin, bile extract, pH 7.5, 2h)	120% for HI-CAP 100 & CAPSUL 117% for CAPSUL-TA	19% (HI-CAP 100), 25% (CAPSUL-TA), 35% (CAPSUL) 3% in pure MCT	nd	(Liang et al., 2013a)
lycopene astaxanthin (n/a)	Fractionated palm oil (10% w/w)	Tween 20, sucrose laurate in their binary blends with WPI or hydrolyzed WPI (n/a)	0.2 to 0.35 for lycopene, 0.15 to 0.35 for astaxanthin containing LLCs	100% in WPI systems with/without $\alpha$ -tocopherol; 68-75% (lycopene); 74-84% (astaxanthin), systems with/without $\alpha$ -tocopherol	n/a	nd	nd	HT-29: 50-270 lycopene) 130-270 (astaxanthin) pmol/g protein. Lower in Tween 20, WPI systems	(Ribeiro et al., 2006)

SFGs: simulated gastric fluids, PC: pancreatin, COL: colipase, BS: bile salts, PL: phospholipase, LPL: lyso-phospholipase, nd: not determined, n/a: not available, MCT: medium-chain triglycerides; WPI: whey protein isolate; FFA: free fatty acids; SPI: soybean protein isolate; PC: phosphatidylcholine; BS: bile salts; LO: linseed oil; **RO: rapeseed oil**; RPO: refined palm olein; SSPS: soy soluble polysaccharides; SFG: small fat globules.



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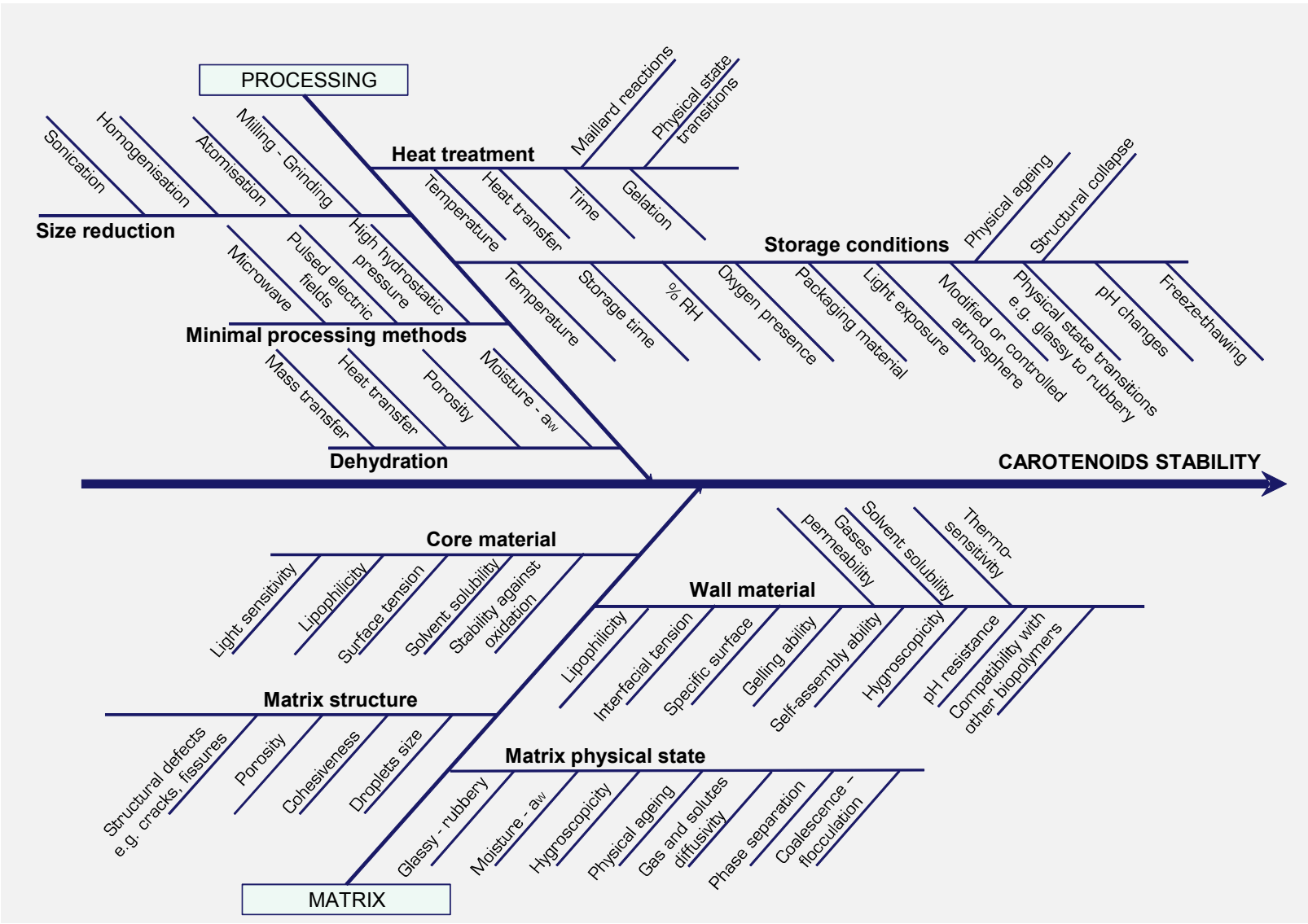


FIGURE 1

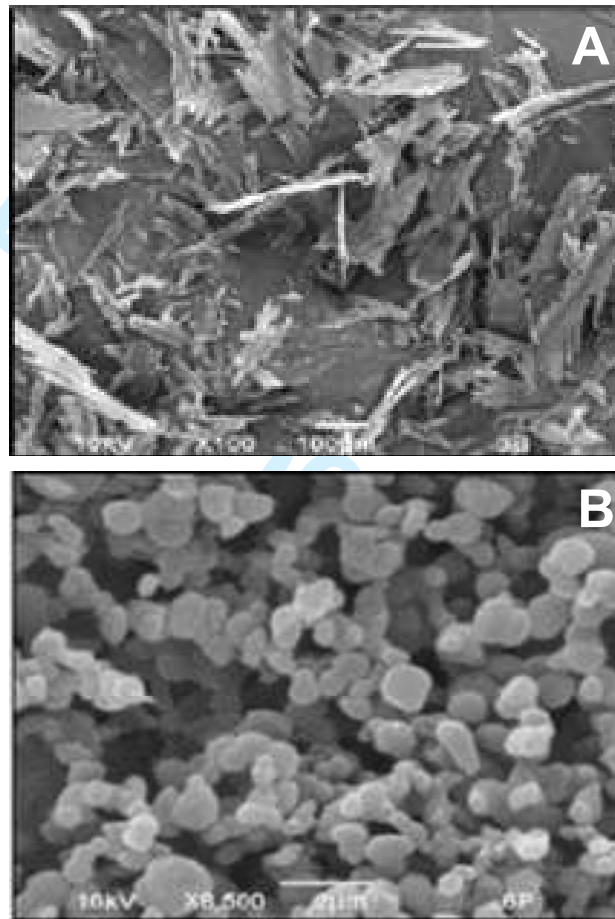


FIGURE 2

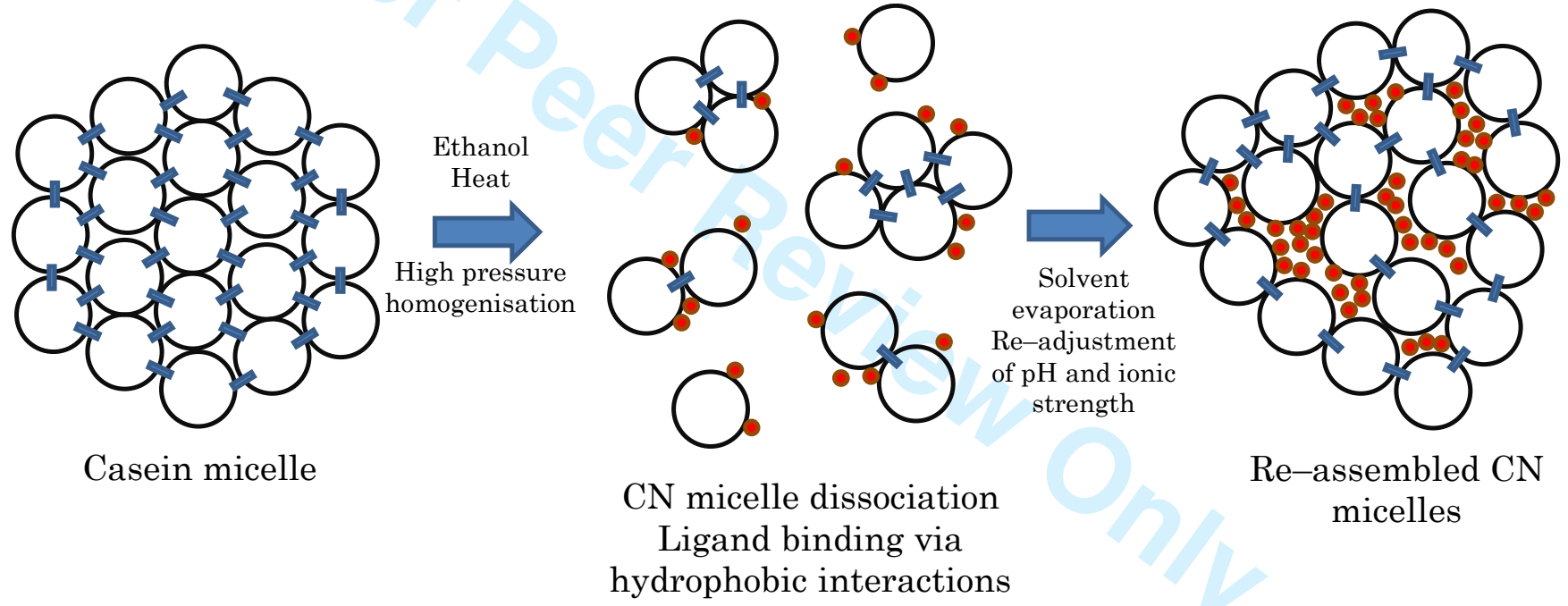


FIGURE 3

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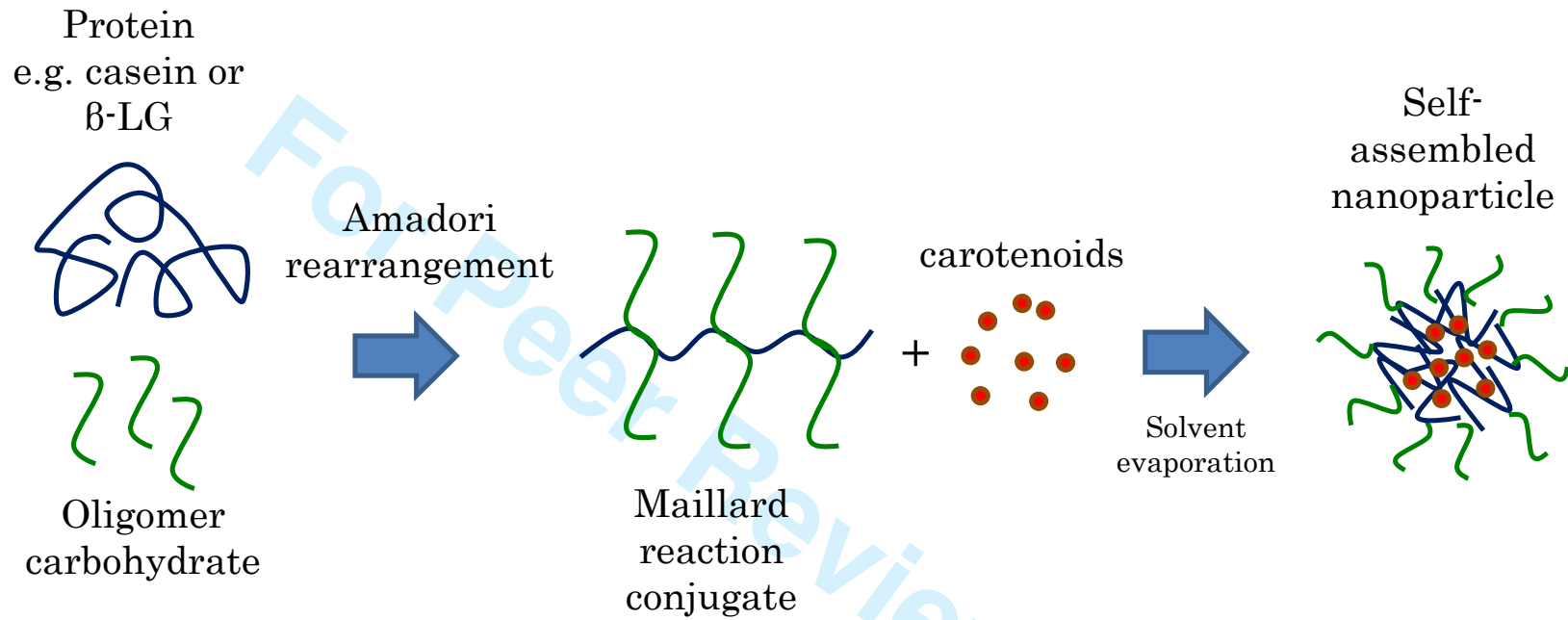


FIGURE 4

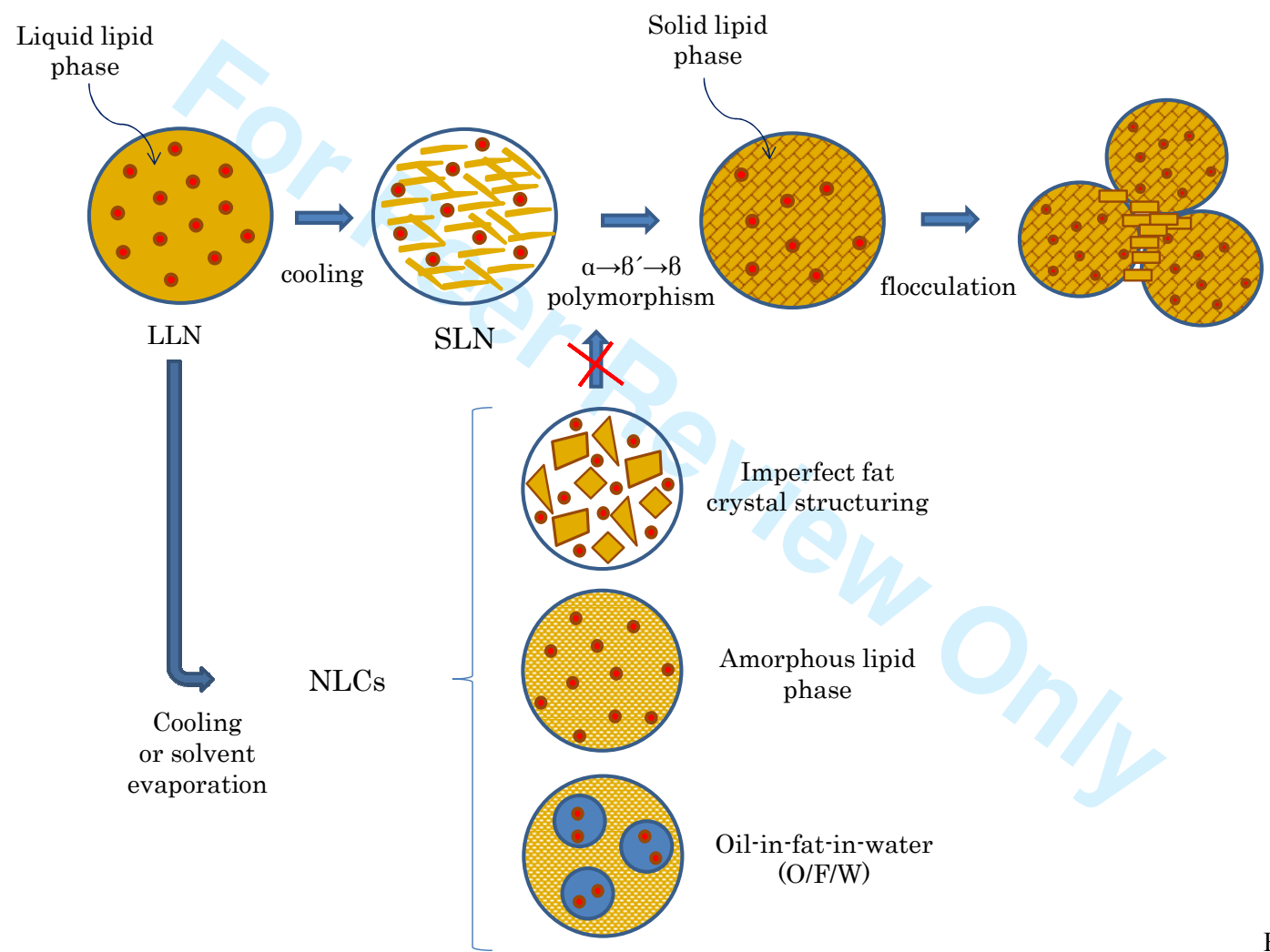


FIGURE 5

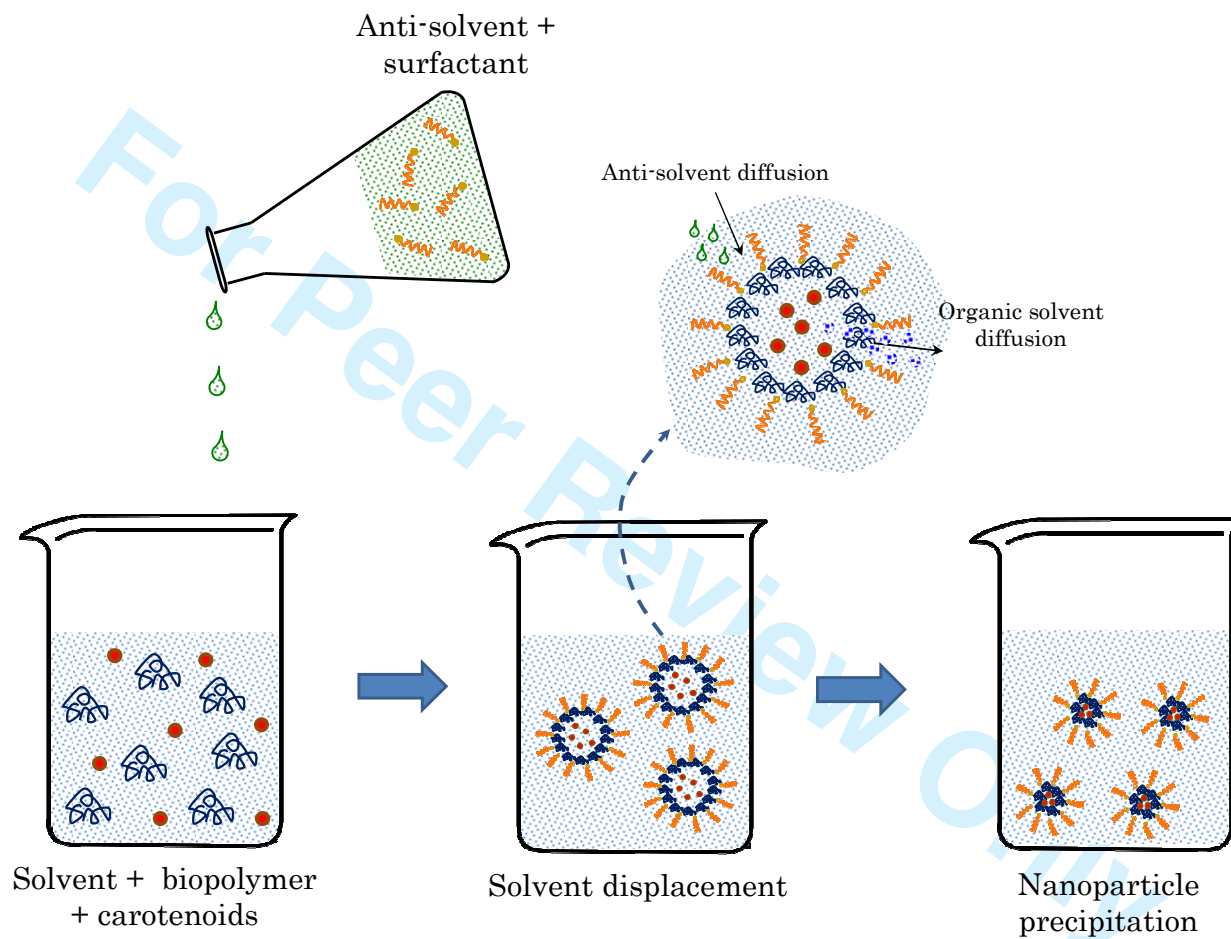


FIGURE 6

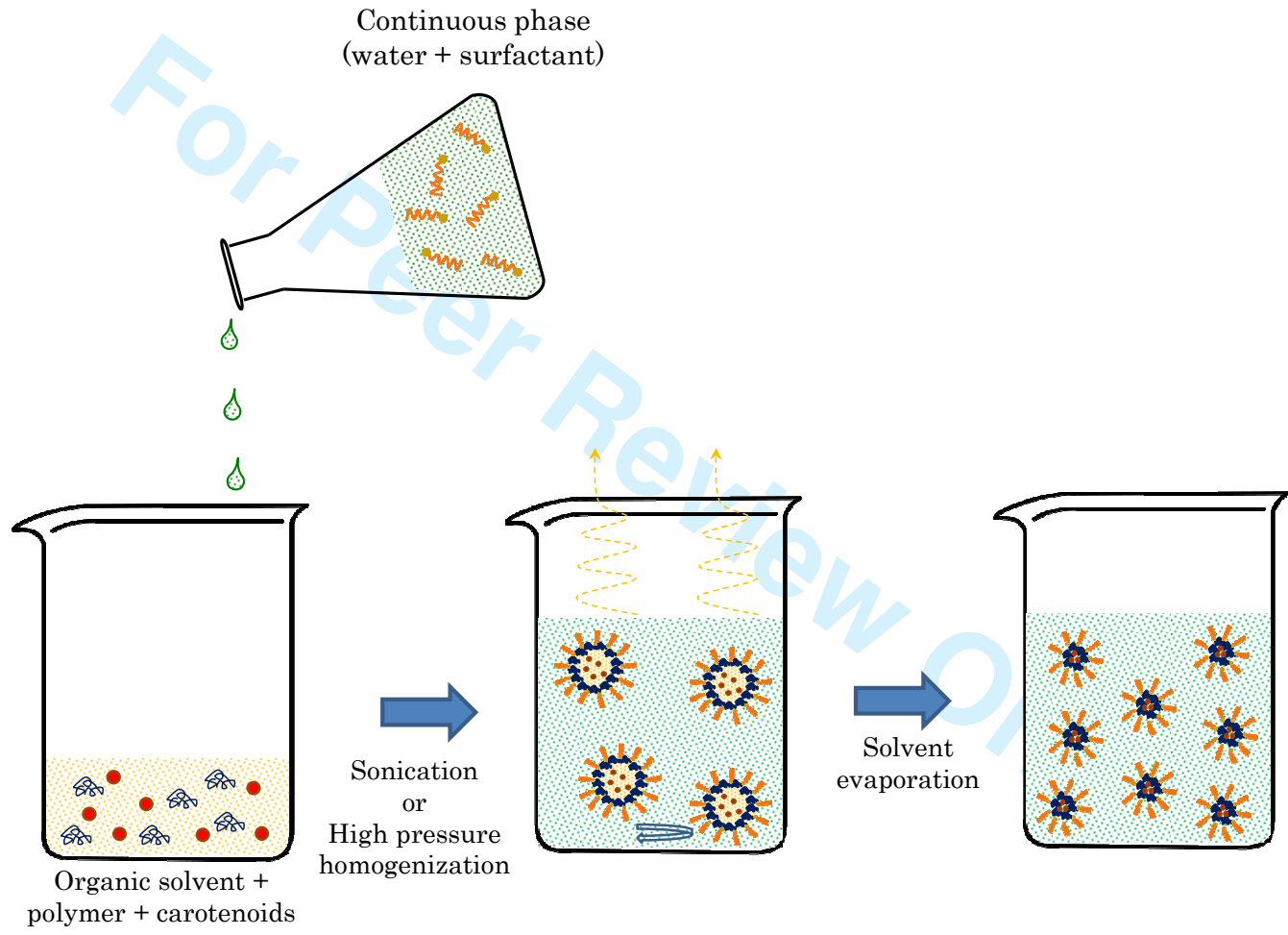


FIGURE 7



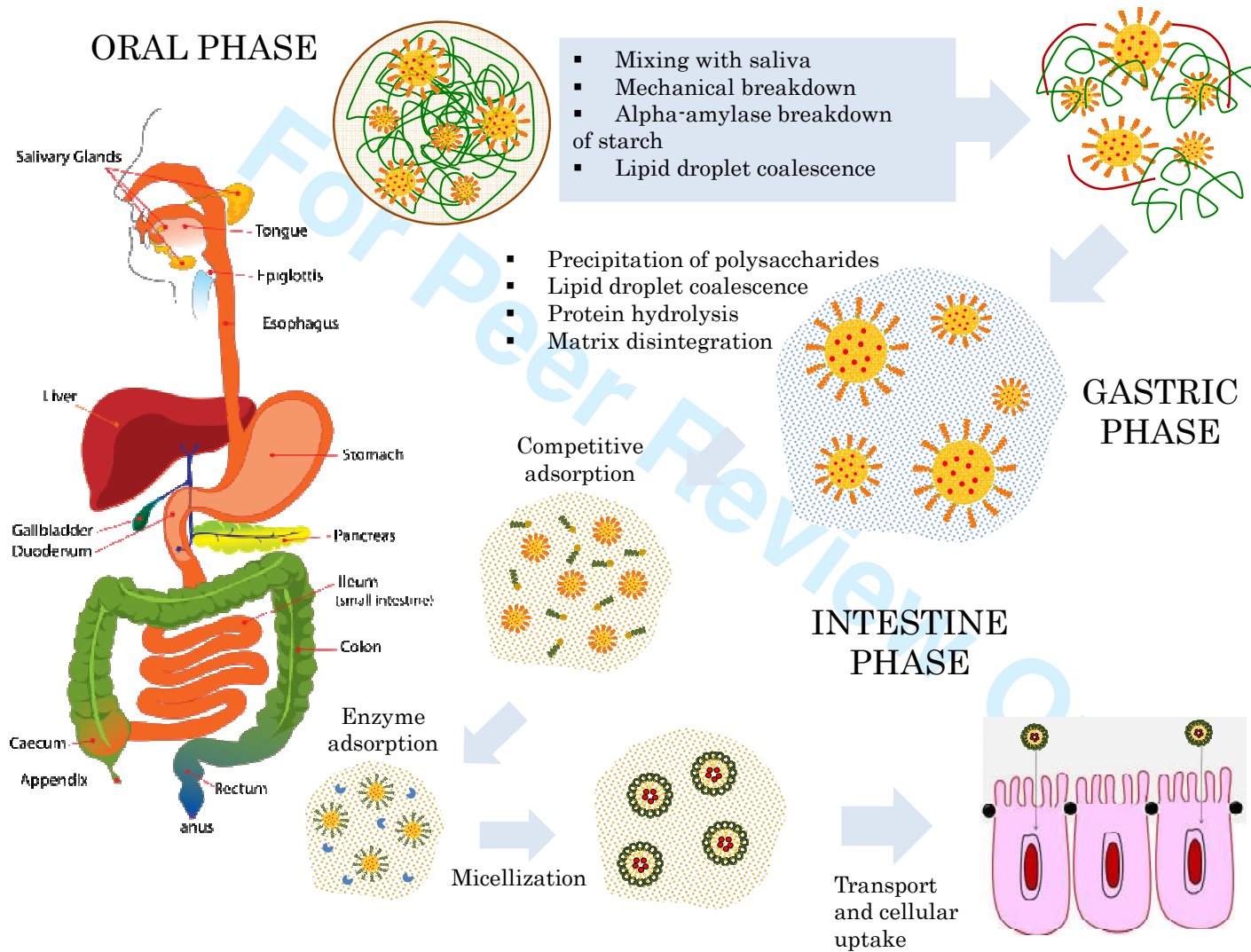


FIGURE 8

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