

## Research Article

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# A cost-effective and eco-friendly biosorption technology for complete removal of nickel ions from an aqueous solution: Optimization of process variables

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**Abstract:** The enormous industrial usage of nickel during its manufacture and recycling has led to widespread environmental pollution. This study was designed to examine the ability of *Gelidium amansii* biomass to biosorb  $\text{Ni}^{2+}$  ions from an aqueous solution. Six independent variables, including contact time (1.0 and 3.0 h), pH (4 and 7),  $\text{Ni}^{2+}$  concentration (25 and 200  $\text{mg}\cdot\text{L}^{-1}$ ), temperature (25°C and 50°C), *G. amansii* biomass (1.0 and 4.0  $\text{g}\cdot\text{L}^{-1}$ ), and agitation mode (agitation or static), were investigated to detect the significance of each factor using a Plackett–Burman design. The analysis of variance for the  $\text{Ni}^{2+}$  biosorption percentage indicated that three independent variables (contact time, temperature, and agitation–static mode) exhibited a high level of significance in the  $\text{Ni}^{2+}$  biosorption process. Twenty experiments were conducted containing

six axial, eight factorial, and six replicates points at center points. The resulting face-centered central composite design analysis data for the biosorption of  $\text{Ni}^{2+}$  exhibited a very large variation in the removal percentage of  $\text{Ni}^{2+}$ , which ranged from 29.73 to 100.00%. The maximum  $\text{Ni}^{2+}$  biosorption percentage was achieved in the 16th run with an experimental percentage quantified as 100.00% under the experimental conditions of 3 h of incubation time and 45°C with 100 rpm for agitation speed.

**Keywords:** *Gelidium amansii*, bioremediation, optimization, Plackett–Burman design, FCCCD analysis

## 1 Introduction

Water contamination is one of the global concerns as it is the main requirement for living organisms and human livelihood, and also the rapid rise of freshwater insufficiency and its limited availability increase additional environmental stresses [1]. The environment has been polluted with different pollutants such as organic, inorganic pollutants, radioactive isotopes, and gaseous pollutants [1]. Heavy metal pollution is one of the most environmental contaminants that need special attention and effective strategies among the different kinds of water pollution due to its toxicity, long residence, non-biodegradable nature, and uncontrolled dispersion [2,3]. Heavy metal elements exist naturally on the Earth's crust during the Earth's formation, but anthropogenic activities such as metal mining, using of chemical fertilizers, and industrial manufacturing resulted in an imminent surge of metallic substances in both the terrestrial and the marine environments [4,5]. Nickel (Ni) is a naturally arising element in great capacity in the earth's crust and core and can cause natural pollution to surface water and soil, but this is mainly due to industrial and mining

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activities [6]. Although nickel is an important biological element for the normal growth of several species of organisms, its increased amounts can cause toxic effects such as respiratory disorders, kidney inflammation, and extreme general weakness, and has been concerned as a probable carcinogen [7]. Nickel is one of the more toxic elements due to high solubility in the marine ecosystem, and it is simply absorbed by living organisms [8,9]. Individuals consume nickel and its derivative compounds through drinking water, food, air, tobacco, nickel-plated materials, and some medical body parts [7]. Nickel is found in the wastewater of different activities like electroplating, paint formulation, mineral processing, thermal power plants, porcelain enameling, and storage battery manufacture [10,11]. The acceptable concentration limit of nickel in the industrial effluent in wastewater is  $2.0 \text{ mg}\cdot\text{L}^{-1}$ , and meanwhile, the concentration limit in the drinking water is only  $0.01 \text{ mg}\cdot\text{L}^{-1}$  [8]. Removal of highly elevated concentrations of nickel to its acceptable limited range with cost-effective and environmental friendly techniques becomes an urgent need. Biological techniques, based on living microorganisms, nonliving dry matter, or even plants, can minimize the toxic heavy metal levels to their naturally acceptable limits in a cost-effective and environmentally friendly manner [12]. Biosorption is an energy-independent process in which heavy metal elements are adsorbed on the cell surface from wastewater using biomass of microorganism, seaweed, and plant residues or their polymeric substances; hence, it provides a renewable, reusable, and very cost-effective technique [13,14]. Marine life has huge biodiversity, and macroalgae (seaweeds) are one such group and are identified as a promising biosorbent due to their ability to produce phycocolloids compounds such as alginates and agar [15]. Seaweeds have considerable advantages such as natural origin, low cost, ready abundance of biomass, and effectiveness against a wide range of pollutants [16]. Alginic acid and fucoidan (sulfated polysaccharides) are essential compounds as they contain the functional groups that play a vital role in the biosorption of heavy metals. The cell wall of red algae contains cellulose that had biosorption capacities but is attributed to the presence of sulfated polysaccharides made of galactans [14,15]. The marine algal surface has high metal binding capacities due to the presence of the high amount of biological compounds such as polysaccharides, proteins, and lipids in the cell wall structure that contains the abundant number of the binding moiety functional groups, for example, carboxyl, hydroxyl sulfuryl, and sulfate, which act as connecting sites for heavy metals [16]. The brown, red, and numerous green algal cell walls are included in a

fibrillar skeleton and an amorphous surrounding matrix and also contain sulfated polysaccharides (fucoidan) or alginate that are responsible for binding heavy metals related to the stereochemical effects [17]. Red algae cell walls consist of galactanes (sulfated polysaccharides), which are also responsible for the complexation with metal ions [18]. Hence, seaweeds have several benefits such as high-efficiency metal elimination, nontoxic, and low cost [16]. The red alga *Gelidium amansii* was removed 100% of  $\text{Pb}^{2+}$  from the aqueous solution with  $200 \text{ mg}\cdot\text{L}^{-1} \text{ Pb}^{2+}$  [19].

This research aimed to statistically optimize the dry biomass of macro-red alga, *G. amansii*, and investigate its potentiality as a cost-effective biosorbent for the removal of nickel ions. The biomass of *G. amansii* is characterized before and after the biosorption process of nickel by scanning electron microscope (SEM) and Fourier-transform infrared spectroscopy (FTIR) analyses.

## 2 Materials and methods

### 2.1 Gathering and preparation of the biosorbent (marine alga)

*G. amansii* (red alga) used in this study was obtained from the Mediterranean Sea coast of Abu-Qir, Alexandria, Egypt, in July 2020. External sand and salts were removed by washing the collected biomass of *G. amansii* with running tap water followed by double immersion in distilled water. *G. amansii* biomass was ground with a blender to produce particles with sizes ranging from 1–1.2 mm and sieved using a standard laboratory test sieve (Endecotts/Ltd., London, England) after drying in an oven at  $65^\circ\text{C}$  for 3 days. Then, 20 grams of ground *G. amansii* biomass was mixed with distilled (1 L) and the suspension was stirred at ambient temperature for approximately 30 min. Finally, algal biomass was filtered with Whatman filter paper no. 1 and dried at  $65^\circ\text{C}$  for 3 days, and steady weight was achieved and then kept at  $4^\circ\text{C}$  for further use in the biosorption process.

### 2.2 Preparation of nickel solution

$\text{Ni}^{2+}$  aqueous solutions were concocted by dissolving  $\text{Ni}(\text{NO}_3)_2\cdot 6\text{H}_2\text{O}$  in deionized water, and the purity of  $\text{Ni}(\text{NO}_3)_2\cdot 6\text{H}_2\text{O}$  was 99.995%. The pH was adjusted by the appropriate addition of 0.1 M HCl or NaOH solutions.

### 2.3 Design of screening experiments for Ni<sup>2+</sup> biosorption using Plackett–Burman design

Plackett–Burman design (PBD) is an effective inspection tool to determine the noteworthy variables between different reacted variables that affect a process. PBD was recycled for the selection of the variables that had a noteworthy influence, either positively or negatively, on Ni<sup>2+</sup> biosorption out of six reacted independent variables. The six independent virtual factors included different incubation times (1 and 3 h), two different initial pH levels (4 and 7), Ni<sup>2+</sup> concentrations (25 and 200 mg·L<sup>-1</sup>), temperatures (25°C and 50°C), *Gelidium amansii* biomass concentrations (1 and 4 g·L<sup>-1</sup>), and static or agitation conditions. Each variable was examined at two levels: low (-1) and high (1) levels. Twelve PBD runs were performed to assess the influence of the six selected factors on the Ni<sup>2+</sup> biosorption efficiency. In the tentative design, each row signifies an experiment, and each column exemplifies an independent factor (Table 1). PBD is performed using the first-order model equation:

$$Y = \beta_0 + \sum \beta_i X_i \quad (1)$$

where  $Y$  is the response value of the Ni<sup>2+</sup> biosorption percentage,  $\beta_0$  is the model intercept,  $\beta_i$  is the linear coefficient, and  $X_i$  is the level of the independent factors. *G. amansii* biomass was blended with a solution of Ni<sup>2+</sup>, and the experiments were performed either wise static or

with agitation for a definite incubation time at the designated temperature.

### 2.4 Design of statistical optimization for nickel (Ni<sup>2+</sup>) biosorption using FCCCD

Based on the resulting data from the PBD experimental design, three significant factors (contact time, temperature, and agitation speed) with three codes (-1, 0, and 1) were specified for each variable and marked. A five-level face-centered central composite design (FCCCD) was designed to detect and describe the optimum circumstances of the important factors, the individual factors, and the relationship between the particular factors with elevated effects on Ni<sup>2+</sup> biosorption. The three factors selected from PBD for further optimization using FCCCD were contact time, temperature (°C), and agitation speed, which were denoted as  $X_1$ ,  $X_2$ , and  $X_3$ , respectively. FCCCD had 20 different tests generated with Design-Expert version 7 for Windows software.

The interaction between Ni<sup>2+</sup> biosorption ( $Y$ ) and the significant independent variables ( $X_1$ ,  $X_2$ , and  $X_3$ ) is given by the following second-order polynomial equation:

$$Y = \beta_0 + \sum_i \beta_i X_i + \sum_{ii} \beta_{ii} X_i^2 + \sum_{ij} \beta_{ij} X_i X_j \quad (2)$$

where  $Y$  is the predicted Ni<sup>2+</sup> biosorption,  $\beta_0$  is the regression coefficient,  $\beta_i$  is the linear coefficient,  $\beta_{ii}$  is the

**Table 1:** Twelve-trial Plackett–Burman experimental design for evaluation of independent variables with coded and actual levels along with the observed and predicted values of Ni<sup>2+</sup> biosorption by *Gelidium amansii* biomass

Std	Run	Coded and actual levels of the independent variables						Ni <sup>2+</sup> removal (%)		Residuals
		Contact time	Ni <sup>2+</sup> conc.	pH	Temperature	Biomass	Agitation–static	Actual	Predicted	
12	1	-1	-1	-1	-1	-1	-1	97.65	97.67	-0.02
7	2	-1	1	1	1	-1	1	99	99.03	-0.03
5	3	1	1	-1	1	1	-1	98.36	98.39	-0.03
10	4	1	-1	-1	-1	1	1	98.6	98.62	-0.02
2	5	1	1	-1	1	-1	-1	98.6	98.57	0.03
1	6	1	-1	1	-1	-1	-1	98.22	98.21	0.01
3	7	-1	1	1	-1	1	-1	97.82	97.76	0.06
8	8	-1	-1	1	1	1	-1	97.91	97.96	-0.05
9	9	-1	-1	-1	1	1	1	98.62	98.56	0.06
6	10	1	1	1	-1	1	1	98.88	98.90	-0.02
11	11	-1	1	-1	-1	-1	1	98.54	98.55	-0.01
4	12	1	-1	1	1	-1	1	99.31	99.29	0.02
Level	Hours	mg·L <sup>-1</sup>		pH	°C	g·L <sup>-1</sup>		Agitation–static		
-1	1	25		4	25	1		Agitation		
1	3	200		7	50	4		Static		

quadratic coefficient, and  $\beta_{ij}$  is the interaction coefficient, and  $X_i$  is the coded level of the independent variable.

## 2.5 Statistical analysis

The statistical analysis and experimental designs were achieved using Minitab and Design Expert version 7 for Windows software. The regression model of the resulting actual data was achieved to estimate the analysis of variance. The contribution % of each variable was also calculated. To design the 3D surface plots, the statistical software package STATISTICA software (version 8.0, StatSoft Inc., Tulsa, OK) was used. Meanwhile, contour plots and response surfaces were used to measure the interaction between the various significant variables. The analysis of variance (ANOVA) significance of the variable mean differences was prescribed ( $p \leq 0.05$ ).

## 2.6 Analytical methods

The analysis of  $\text{Ni}^{2+}$  in the filtered solutions (0.2  $\mu\text{m}$  polytetrafluorethylene syringe filters) was done using inductively coupled plasma-atomic emission spectroscopy (ICP-AES, Thermo Scientific). The biosorption experimental data were obtained in triplicate ( $n = 3$ ). Meanwhile, the ability of *G. amansii* biomass to biosorb  $\text{Ni}^{2+}$  ions was estimated using the following equation:

$$\text{Biosorption efficiency (\%)} = \frac{(C_i - C_f)}{C_i} \times 100 \quad (3)$$

where  $C_i$  is the initial  $\text{Ni}^{2+}$  ion concentration ( $\text{mg}\cdot\text{L}^{-1}$ ) and  $C_f$  is the residual  $\text{Ni}^{2+}$  ion concentration ( $\text{mg}\cdot\text{L}^{-1}$ ).

## 2.7 Biosorbent characterization (*G. amansii* biomass)

Alga *G. amansii* biomasses were analyzed before and after biosorption process  $\text{Ni}^{2+}$  using FTIR spectral analysis, energy-dispersive spectroscopy (EDS) analysis, and SEM.

## 2.8 FTIR spectral analysis

FTIR analyses were performed to interpret the distinct chemical functional groups of the *G. amansii* biomass

samples that may be accountable for the biosorption of  $\text{Ni}^{2+}$ . *G. amansii* biomass analyzed before and after the  $\text{Ni}^{2+}$  biosorption process using FTIR spectroscopy (Thermo Fisher Nicolette IS10, USA spectrophotometer). The FTIR spectrum was analyzed over a spectral range from 400 to 4,500  $\text{cm}^{-1}$ .

## 2.9 Scanning electron microscopy

*Gelidium amansii* biomass samples before and after  $\text{Ni}^{2+}$  biosorption were scanned to illustrate the morphological changes and to demonstrate  $\text{Ni}^{2+}$  biosorption. *G. amansii* biomass samples were crusted with gold and inspected at various magnifications at 20 kV at Electron-Microscope-Unit of Mansoura University, Egypt.

## 2.10 EDX analysis

Energy-dispersive X-ray spectroscopy (EDX) analysis is an effective analytical tool that is used for the elemental analysis of *G. amansii* biomass before and after the biosorption process using an Oxford X-Max 20 Instrument at Electron Microscope Unit, Faculty of Science, Alexandria University, Alexandria, Egypt.

# 3 Results and discussion

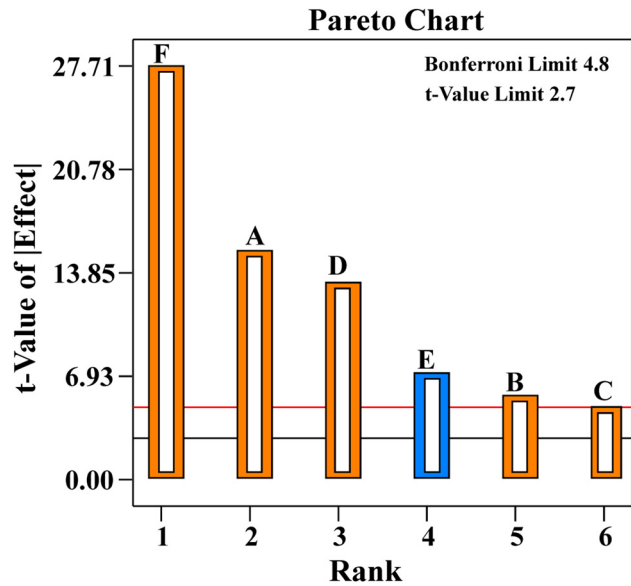
## 3.1 PBD experimental results and detection of significant variables

In the current survey,  $\text{Ni}^{2+}$  was removed using *G. amansii* as a biosorbent and PBD as an analytical screening method to detect the significance of multiple independent factors that influenced the biosorption process. The actual and coded levels of six independent variables, including contact time (1.0 and 3.0 h), pH (4 and 7),  $\text{Ni}^{2+}$  concentration (25 and 200  $\text{mg}\cdot\text{L}^{-1}$ ), temperature (25°C and 50°C), *G. amansii* biomass (1.0 and 4.0  $\text{g}\cdot\text{L}^{-1}$ ), and agitation mode (agitation or static), were coded using (-1 and 1) for each variable factor, as presented in Table 1.

The data (Table 1) illustrate that the maximum biosorption percentage for  $\text{Ni}^{2+}$  was achieved in the 12th run, with percentages quantified as 99.31% and 99.29% for the actual and predicted values, respectively, followed by the

2nd run, which recorded biosorption percentages quantified as 99% and 99.03% for the actual and predicted values, respectively. Meanwhile, the 1st run recorded the minimum biosorption percentage. The maximum biosorption percentage was achieved at 3 h of contact time, 25 mg·L<sup>-1</sup> (Ni<sup>2+</sup> initial concentration), pH value (7), 50°C, and 1.0 g·L<sup>-1</sup> (*G. amansii* biomass) under static conditions. PBD was also conducted to define the most significant factors affecting the Ni<sup>2+</sup> biosorption percentage from aqueous solutions using *G. amansii* biomass, as illustrated in Table 1.

The correlation between the Ni<sup>2+</sup> biosorption percentage and the other independent factors was investigated with respect to their effects on the Ni<sup>2+</sup> biosorption process via PBD, as illustrated in Table 2. The coefficient values for each reaction factor exhibit the extent of the effect of this factor on the Ni<sup>2+</sup> biosorption process. The analysis of the regression coefficients and the cumulative effects of the six interacting factors (Table 2 and Figure 1) show that five factors, including contact time (A), Ni<sup>2+</sup> concentration (B), pH value (C), temperature (D), and agitation mode (F), had coefficient values quantified as 0.20, 0.07, 0.06, 0.17, and 0.37 with contribution percentages calculated as 20.833, 7.292, 6.250, 17.708, and 38.542, respectively, and had the positive effects on the Ni<sup>2+</sup> biosorption process, which means that the increase in these factors could enhance a positive effect on Ni<sup>2+</sup> biosorption. Conversely, *G. amansii* biomass exhibited the negative effects, which means that the decrease in *G. amansii* biomass concentration could enhance a positive effect on the Ni<sup>2+</sup> biosorption process. The effect of each variable on the Ni<sup>2+</sup> biosorption process is illustrated in Table 2 and Figure 1. High values, either



**Figure 1:** Pareto chart indicating the cumulative effects of independent variables on Ni<sup>2+</sup> removal by *G. amansii* biomass using Plackett–Burman design: the orange and blue colors represent the positive and negative independent variables, respectively.

positive or negative, indicate that the factor plays a key role and has an effective function on the Ni<sup>2+</sup> biosorption process, while low values (approximately zero) reflect a noneffective on the biosorption process.

Results indicated that the optimum pH value for maximum absorption of Ni<sup>2+</sup> by red alga *G. amansii* was at near 7, and the same results were obtained when *Aspergillus niger*, *Cystoseria indica*, and *Rhizopus arrhizus* were applied, and the maximum biosorption was at pH 6, but in the case of *Acinetobacter baumannii* UCR-2971, the pH level was 4.5 [20–23]. It took nearly 3 h for optimum

**Table 2:** Regression statistics and ANOVA for the experimental results of the Plackett–Burman design used for Ni<sup>2+</sup> biosorption by *G. amansii* biomass

Term	Coefficient	Effect	% Contribution	F-value	P-value prob > F
Intercept	98.46			164.76	<0.0001
Contact time (A)	0.20	0.40	20.833	181.24	<0.0001
Ni <sup>2+</sup> concentration (B)	0.07	0.14	7.292	24.31	0.0044
pH (C)	0.06	0.12	6.250	18.20	0.0080
Temperature (D)	0.17	0.34	17.708	134.07	<0.0001
Biomass (E)	-0.09	-0.18	9.375	39.19	0.0015
Agitation–static (F)	0.37	0.74	38.542	591.53	<0.0001
Std. Dev.	0.05	R <sup>2</sup>		0.9950	
Mean	98.46	Adj R <sup>2</sup>		0.9889	
C.V. (%)	0.05	Pred R <sup>2</sup>		0.9710	
PRESS	0.08	Adeq Precision		40.54	

Significant values, df: degree of freedom, F: Fishers’s function, P: level of significance.



$\text{Ni}^{2+}$  biosorption, and these results are nearly approved by Rodríguez and Quesada [23], and they also reported that the absorption of  $\text{Ni}^{2+}$  by *Acinetobacter baumannii* UCR-2971 was achieved after 100 min, pH 4.5, with biomass of  $4.0 \text{ g}\cdot\text{L}^{-1}$  (Table 3).

### 3.2 The adequacy of the model

The model should be validated before its acceptance as a statistically accurate model, and a normal probability plot (NPP) illustrates the normal distribution of the residuals to test the model's accuracy and adequacy [24]. Figure 2 shows the analyzed data to test the normality of residuals, whereas the NPP of the residuals and residuals vs predicted for  $\text{Ni}^{2+}$  biosorption by *G. amansii* biomass was determined using the first-order polynomial equation. The residuals are defined as the differences between the experimental values of the responses and

those predicted by the theoretical model. The closer residuals to the straight line with low residual values indicate that the data did not exhibit any abnormal action and achieved a very accurate prediction model [18,25].

Figure 2 displays the NPP of the residuals against the predicted values of the model. The data exhibit a normal distribution and demonstrate the model validity, as the residual points on the diagonal line are found close to each other.

### 3.3 Regression statistics and ANOVA for PBD

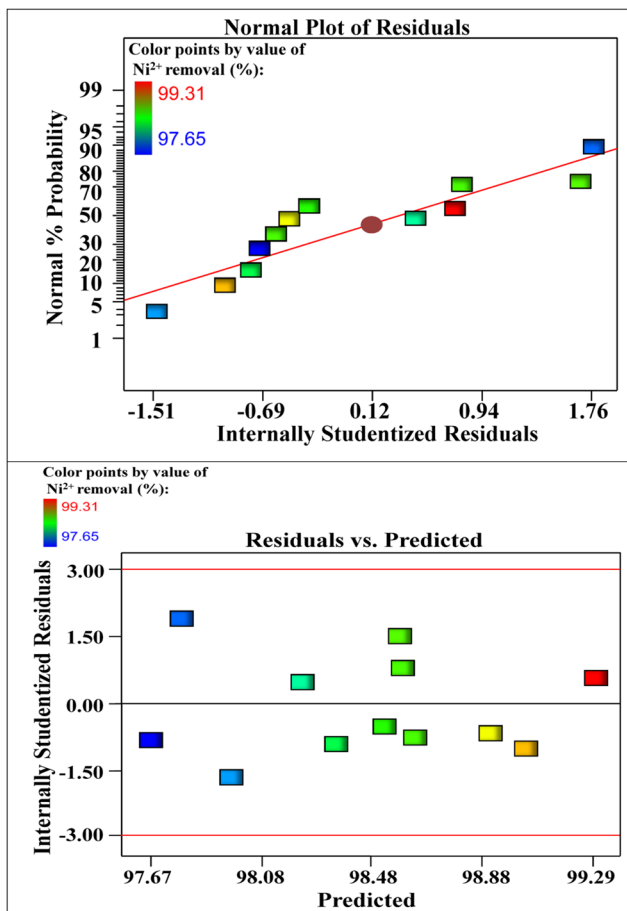
The model determination coefficient ( $R^2$ ) was 0.9950, which means that 99.59% of the variation in  $\text{Ni}^{2+}$  biosorption was dependent on the independent factors and that only 0.05% of the variation could not be explained by the regression model. A regression model with a high  $R^2$  value greater than 0.9 is considered to be highly

**Table 3:** Face-centered central composite design representing the response of  $\text{Ni}^{2+}$  removal % by *G. amansii* as influenced by contact time ( $X_1$ ), temperature ( $X_2$ ), and agitation speed ( $X_3$ ) along with the predicted  $\text{Ni}^{2+}$  removal % and residuals and the actual factor levels corresponding to coded factor levels

Std	Run	Type	Variables			$\text{Ni}^{2+}$ removal (%)		Residuals
			$X_1$	$X_2$	$X_3$	Experimental	Predicted	
19	1	Center	0	0	0	95.37	94.82	0.55
2	2	Fact	1	-1	-1	89.88	89.69	0.19
20	3	Center	0	0	0	97.19	94.82	2.37
1	4	Fact	-1	-1	-1	78.23	77.70	0.54
17	5	Center	0	0	0	94.11	94.82	-0.71
16	6	Center	0	0	0	94.98	94.82	0.16
12	7	Axial	0	1	0	79.73	81.14	-1.41
11	8	Axial	0	-1	0	75.30	76.70	-1.40
6	9	Fact	1	-1	1	29.73	29.70	0.03
18	10	Center	0	0	0	96.40	94.82	1.58
10	11	Axial	1	0	0	86.07	86.51	-0.44
5	12	Fact	-1	-1	1	66.99	66.33	0.65
9	13	Axial	-1	0	0	95.31	97.69	-2.38
15	14	Center	0	0	0	96.51	94.82	1.69
7	15	Fact	-1	1	1	76.33	75.81	0.52
13	16	Axial	0	0	-1	100.00	101.45	-1.45
3	17	Fact	-1	1	-1	75.51	74.83	0.68
8	18	Fact	1	1	1	41.61	41.44	0.17
14	19	Axial	0	0	1	70.57	71.94	-1.37
4	20	Fact	1	1	-1	89.15	89.09	0.05

Variable	Variable code	Coded and actual levels		
		-1	0	1
Contact time (h)	$X_1$	2	3	4
Temperature ( $^{\circ}\text{C}$ )	$X_2$	30	45	60
Agitation speed (rpm)	$X_3$	100	150	200



**Figure 2:** NPP of the residuals and residuals vs predicted Ni<sup>2+</sup> removal by *Gelidium amansii* biomass determined by the first-order polynomial equation.

correlated, and the model is adequate to interpret the difference in the experimental data and theoretical values [26]. For further interpretation and assessment of the significance of the interacting variables on the Ni<sup>2+</sup> biosorption process, the obtained data were analyzed statistically in terms of ANOVA. The relationship between the six independent factors and Ni<sup>2+</sup> biosorption was determined using a multiple-regression model (Table 2). The adequacy of the model was tested by the estimation of the coefficient ( $R^2$  value), which is generally between 0.0 and 1.0. The model is considered to be strong and effective if the  $R^2$  value is closer to 1.0. Table 2 illustrates the adjusted determination coefficient (Adj.  $R^2$ ) and predicted (Pred.  $R^2$ ) values quantified as 0.9889 and 0.9710, respectively, which are considered to be very large values and illustrate a highly significant model and its suitability to interpret the interaction between reacted variables and the Ni<sup>2+</sup> biosorption percentage using *G. amansii* biomass. The calculated Adeq. The precision fraction (40.54) specifies a sufficient signal-to-noise ratio.

The experimental PBD data were fitted with a first-order polynomial equation that signified the Ni<sup>2+</sup> biosorption percentage as a function of the incubation time, Ni<sup>2+</sup> concentration, pH value, temperature, *G. amansii* biomass, and agitation–static mode.

Based on the ANOVA for the Ni<sup>2+</sup> biosorption percentage (Table 2), correlation significance indicated that some independent variables (contact time, temperature, agitation–static mode) exhibited a high level of significance ( $P < 0.0001$ ), while other factors (Ni<sup>2+</sup> concentration, pH level, and *G. amansii* biomass) displayed relatively low levels of significance ( $P = 0.0044, 0.0080, \text{ and } 0.0015$ ).

### 3.4 Optimization of Ni<sup>2+</sup> biosorption via FCCCD

The influence of the three significant independent variables (contact time, temperature, and agitation speed) was investigated. Applying FCCCD statistics illustrated the interaction between three variables and their optimal conditions for achieving the maximum bioadsorption percentage. By applying FCCCD and holding three parameters at three different levels, a total of 20 bioadsorption tests were performed, as illustrated in Table 3, which demonstrates the actual, predicted, and residual values for Ni<sup>2+</sup> biosorption. A face-centered central composite matrix was also conducted to examine the interactive, individual, and quadratic effects of selected variables in the biosorption of Ni<sup>2+</sup> using dry *G. amansii* biomass. Different combinations are represented in Table 3 ( $X_1$ : incubation time,  $X_2$ : temperature, and  $X_3$ : agitation speed). Twenty experiments were conducted containing six axial points, eight factorial points, and six replicates at center points. The resulting FCCCD analysis data for the biosorption of Ni<sup>2+</sup> exhibited a very large variation in the removal percentage of Ni<sup>2+</sup>, which ranged from 29.73% to 100.00%. The maximum Ni<sup>2+</sup> biosorption percentage was achieved in the 16th run with an experimental percentage quantified as 100.00% under the experimental conditions of 3 h of incubation time and 45°C and 100 rpm for agitation speed. The actual and predicted values of yields of Ni<sup>2+</sup> biosorption are also illustrated in Table 3.

### 3.5 Multiple regression analysis and ANOVA for FCCCD

The Ni<sup>2+</sup> biosorption percentage was statically analyzed using multiple regression analysis of the FCCCD model

**Table 4:** Analysis of variance for biosorption of Ni<sup>2+</sup> ions by *Gelidium amansii* biomass from aqueous solution obtained by FCCCD

Source of variance	Degrees of freedom	Sum of square	Mean of square	F-value	P-value	Coefficient estimate	
Model		1	6,598.70	733.19	270.46	<0.0001	94.82
Linear effect	$X_1$	1	312.91	312.91	115.43	<0.0001	-5.59
	$X_2$	1	49.29	49.29	18.18	0.0017	2.22
	$X_3$	1	2,176.80	2,176.80	802.99	<0.0001	-14.75
Interaction effect	$X_1X_2$	1	2.57	2.57	0.95	0.3536	0.57
	$X_1X_3$	1	1,182.67	1,182.67	436.27	<0.0001	-12.16
	$X_2X_3$	1	76.20	76.20	28.11	0.0003	3.09
Square effect	$X_1^2$	1	20.37	20.37	7.52	0.0208	-2.72
	$X_2^2$	1	694.95	694.95	256.36	<0.0001	-15.90
	$X_3^2$	1	181.62	181.62	67.00	<0.0001	-8.13
Error effect	Lack of Fit	5	20.61	4.12	3.17	0.1155	
	Pure Error	5	6.50	1.30			
$R^2$	0.9959	Std. dev.	1.65				
Adj. $R^2$	0.9922	Mean	81.45				
Pred. $R^2$	0.9844	C.V. [%]	2.02				
Adeq. precision	61.63	PRESS	103.64				

Significant values,  $F$ : Fisher's function,  $P$ : level of significance, C.V.: coefficient of variation.

and ANOVA, as illustrated in Tables 4 and 5. The analysis demonstrates the coefficient values, determination coefficient ( $R^2$ ) to detect the effectiveness of the polynomial regression model, the adjusted and predicted  $R^2$  values, the effect of each factor, probability  $P$  value, and Fisher test ( $F$ -test). Linear ( $X_1$ ,  $X_2$ , and  $X_3$ ), interactions ( $X_1X_2$ ,

$X_1X_3$ , and  $X_2X_3$ ), and quadratic effects ( $X_1^2$ ,  $X_2^2$ , and  $X_3^2$ ) of the three interacting process factors were also assessed.

The coefficient of determination ( $R^2$ ) of the model was calculated to be 0.9959 (Table 4), proving that 99.59% of the variation in the biosorption percentage of Ni<sup>2+</sup> was attributed to the interacting variables and that

**Table 5:** Fit summary for FCCCD for biosorption of Ni<sup>2+</sup> ions by *Gelidium amansii* biomass from aqueous solution

Lack of fit tests					
Source	Sum of squares	df	Mean <sup>2</sup>	F-value	P-value prob > F
Linear	4,080.32	11	370.94	285.34	<0.0001
2FI	2,818.89	8	352.36	271.05	<0.0001
Quadratic	20.61	5	4.12	3.17	0.1155
Sequential model sum of squares					
Source	Sum of squares	df	Mean <sup>2</sup>	F-value	P-value prob > F
Linear vs mean	2,538.99	3	846.33	3.31	0.0469
2FI vs linear	1,261.44	3	420.48	1.93	0.1739
Quadratic vs 2FI	2,798.28	3	932.76	344.08	<0.0001
Model summary statistics					
Source	Standard deviation	$R^2$	Adjusted $R^2$	Predicted $R^2$	PRESS
Linear	15.98	0.3832	0.2675	-0.1906	7,888.57
2FI	14.74	0.5736	0.3768	-1.9630	19,632.46
Quadratic	1.65	0.9959	0.9922	0.9844	103.64

Significant values, df: degree of freedom, PRESS: sum of squares of prediction error, two factor interaction: 2FI.



only 0.41% of the variation could not be interpreted via the model. A regression model with an  $R^2$  value is greater than 0.9, which was considered to be strongly correlated [10]. The highest  $R^2$  value also illustrates a good relation between the experimental data and the predicted values generated by model Box and Draper [27].

The optimum correlation between the expected and experimental values of  $\text{Ni}^{2+}$  biosorption was designated by a reasonable correlation between the Pred.  $R^2$  of 0.9844 and the Adj.  $R^2$  of 0.9922. Adeq. precision with a ratio of 61.63 shows an adequate sign-to-noise ratio. Predicted residual sum of squares (PRESS) and CV values were quantified as 103.64 and 2.02, respectively, while the low value of CV indicated good precision of the experimental performance [27]. This model also displays standard deviations and mean values calculated as 1.65 and 81.45, respectively (Table 4). The presence of negative coefficient values (Table 4) suggests a reverse correlation among the factors, while the positive values suggest a synergistic relationship between the factors [28]. Subsequently, the negative coefficient values of the linear, interaction, and square effects of the three process parameters mean that they have a negative effect on the  $\text{Ni}^{2+}$  biosorption process by *G. amansii* biomass, while the positive coefficient values mean that they enhance the  $\text{Ni}^{2+}$  percentage by *G. amansii* biomass in the tested ranges of the selected three process factors. Table 4 indicates that the linear effect of  $X_2$  and the interaction effect of  $X_1X_2$  and  $X_2X_3$  had a positive effect on the  $\text{Ni}^{2+}$  biosorption process, while the linear effect of  $X_1$  and  $X_3$ , the interaction effect of  $X_1X_3$ , and the square effect of  $X_1^2$ ,  $X_2^2$ , and  $X_3^2$  had a negative effect on the biosorption process. To estimate the correlation between dependent and independent factors and to detect the optimum conditions for  $\text{Ni}^{2+}$  biosorption percentage, the three interacting variables  $X_1$  (contact time),  $X_2$  (temperature), and  $X_3$  (agitation speed), and a second-order polynomial regression model was suggested to estimate the maximum levels of three variables and detect the predicted response ( $Y$ ) in terms of the independent process factors as follows:

$$\begin{aligned} \text{The predicted value of the } \text{Ni}^{2+} \text{ biosorption percentage (Y)} \\ = 94.82 - 5.59X_1 + 2.22X_2 - 14.75X_3 \\ + 0.57X_1X_2 - 12.16X_1X_3 \\ + 3.09X_2X_3 - 2.72X_1^2 - 15.90X_2^2 - 8.13X_3^2 \end{aligned} \quad (4)$$

where  $Y$  is the predicted value of the  $\text{Ni}^{2+}$  biosorption percentage,  $X_1$  is the contact time,  $X_2$  is the temperature, and  $X_3$  is the agitation speed.

The ANOVA of the FCCCD, as well as the mean square, the sum of square,  $F$ -value,  $P$ -value, and confidence level,

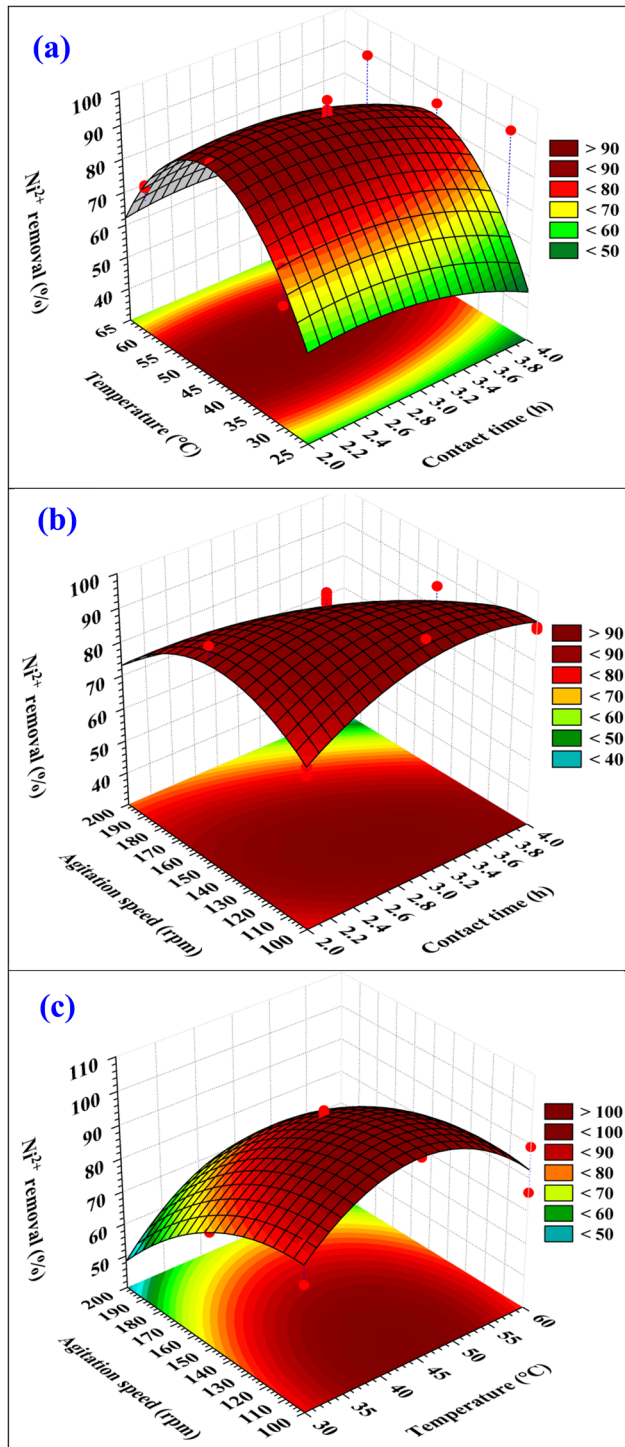
was calculated. The corresponding probability values ( $P$  values) are shown in Table 4 and used to explain and clarify the significance of each coefficient, which is a key point to recognize the pattern of the interaction between the tested factors. Lower  $P$  values exhibit more significance in the corresponding coefficient. The current ANOVA data (Table 4) show that Fisher's  $F$  test is 270.46, and a very low probability value was quantified ( $P < 0.0001$ ). Both values prove that the model is highly significant for the  $\text{Ni}^{2+}$  biosorption process. Furthermore, variables with confidence levels greater than 90% and  $P$  values less than 0.1 were considered to be significant [29]. Therefore, the linear, interaction, and square coefficient terms had very significant effects ( $P < 0.1$ ) on the  $\text{Ni}^{2+}$  biosorption process, except that the interaction effect between incubation time and temperature ( $X_1X_2$ ) had no significant contribution to the  $\text{Ni}^{2+}$  biosorption process. The current model recorded an adequate precision value quantified as 61.63, while the PRESS value was calculated as 103.64.

Table 5 presents the fit summary data applied to detect the maximum polynomial model among the linear, interaction, and square models appropriate for the experimental results. The fitting model was selected depending on both the significant model terms and nonsignificant lack of fit test [28]; moreover, the statistics of the model summary focused on the model with lower SD and higher adjusted and predicted  $R^2$ . The current fit summary data (Table 5) revealed that the quadratic model is a very significant and adequate model fitting the FCCCD of the  $\text{Ni}^{2+}$  biosorption percentage using *G. amansii* biomass from the aqueous solution and has a very low  $P$  value of less than 0.0001. Moreover, the lack of fit  $F$  value and probability  $P$  value are not significant (quantified as 3.17 and 0.1155, respectively). The summary statistics of the model displayed the minimum value of standard deviation (1.65), the largest adjusted  $R^2$  value of 0.9922, and a predicted  $R^2$  of 0.9844.

### 3.6 Three-dimensional plots for $\text{Ni}^{2+}$ biosorption

The 3D graphs were plotted to demonstrate the pairwise combination of the selected independent variables and the  $\text{Ni}^{2+}$  biosorption percentage on the  $z$ -axis against two independent factors, while the other factors were held at the zero level. Graphs 3D illustrate the change in the response surface and detect the ideal levels of three selected process factors for achieving the maximum

biosorption percentage from  $\text{Ni}^{2+}$  using *G. amansii* biomass. Figure 3a–c demonstrate the three-dimensional plots generated for  $\text{Ni}^{2+}$  biosorption percentages as a



**Figure 3:** Three-dimensional surface plot for biosorption of  $\text{Ni}^{2+}$  ions by *G. amansii* biomass from aqueous solution, showing the interactive effects of the three tested variables: (a) agitation speed, (b) temperature, and (c) contact time was held at their zero.

function of contact time, temperature, and agitation speed.

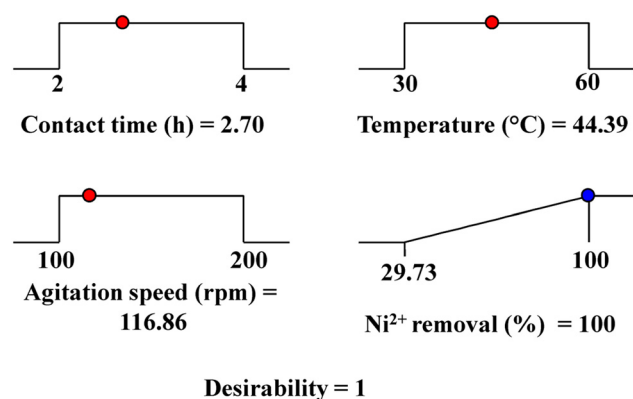
Figure 3a represents the effect  $X_1$  (contact time) and  $X_2$  (temperature), while  $X_3$  (agitation speed) was held at their zero (center) levels (150 rpm). The maximum  $\text{Ni}^{2+}$  biosorption percentage appeared at moderate temperature and contact time, whereas the  $\text{Ni}^{2+}$  biosorption percentage increased with increasing temperature and increasing incubation time until the midpoint; however, a greater increase in the temperature and incubation time caused a gradual decrease in the  $\text{Ni}^{2+}$  biosorption percentage.

Figure 3b represents the effects  $X_3$  (agitation speed) and  $X_1$  (contact time), while  $X_2$  (temperature) was held at their zero (center) levels (45°C). The maximum  $\text{Ni}^{2+}$  biosorption percentage appeared at moderate contact time and agitation speed, whereas the  $\text{Ni}^{2+}$  biosorption percentage increased with increasing contact time and increasing agitation speed until the midpoint; however, a greater increase in the contact time and agitation speed resulted in a gradual decrease in the  $\text{Ni}^{2+}$  biosorption percentage.

Conversely, Figure 3c represents the holding of contact time at zero level (3 h) and studies the effect of two other factors (agitation speed and temperature) on the  $\text{Ni}^{2+}$  biosorption percentage. It also revealed that the maximum  $\text{Ni}^{2+}$  biosorption percentage appeared at moderate temperature and agitation speed, whereas the  $\text{Ni}^{2+}$  biosorption percentage increased with increasing temperature and increasing agitation speed until the midpoint; however, a greater increase in the temperature and agitation speed resulted in a gradual decrease in the  $\text{Ni}^{2+}$  biosorption percentage.

The biosorption percentage of  $\text{Ni}^{2+}$  was elevated by increasing the incubation time from 2 to 3 h, which could be a result of the availability of  $\text{Ni}^{2+}$  ion reaching sites in the biosorbent with time [30]. However, the decrease in the  $\text{Ni}^{2+}$  biosorption percentage observed at 4 h was caused by the repulsion powers between solute molecules and the bulk phase, and the remaining surface sites became saturated [31,32]. The decrease in the  $\text{Ni}^{2+}$  biosorption percentage could also be explained in the view of Liu *et al.* [33] who attributed this decrease to the interaction between the functional groups allocated on the biosorbent surface and intercellular accumulation.

Temperature plays a key role in the biosorption process as it affects the viscosity and kinetic energy of metal ions in the solution and hence the diffusion rate as well as the metal ion binding capacity to the biosorbent [34]. The effect of temperature on the heavy metal biosorption process can be negligible, positive, or negative [35], although elevated temperatures can cause physical damage to the biosorbent [34].



**Figure 4:** The optimization plot displays the DF and the optimum predicted values for the maximum percentage for biosorption of  $\text{Ni}^{2+}$  ions by *G. amansii* biomass from aqueous solution.

Zu et al. [36] reported that the biosorption of copper ions was enhanced under shaking conditions compared to static conditions using *Candida utilis* as a result of shearing power, which wrinkles the surface of yeast cells. Shaking makes conditions more available for metal uptake, as it is linked to external metal concentrations [37]. An increase in shaking velocity caused a decrease in the boundary layer resistance and increased the driving forces of diffusion of ions in the biofilm; meanwhile, the decrease in removal percentage at a higher speed was assigned to vortex formation [38].

### 3.7 Desirability function

The key point of the experimental design is to achieve the ideal predicted circumstances for maximizing the responses.

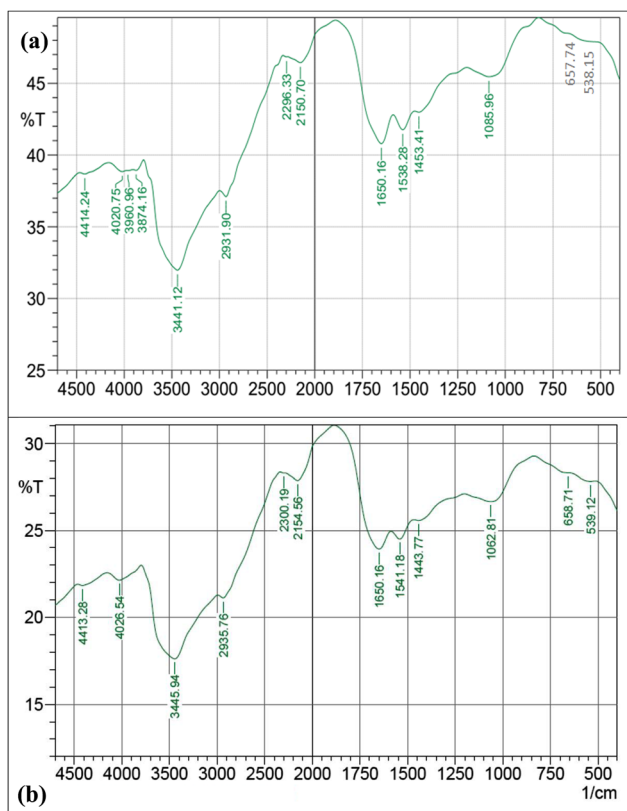
The program's desirability function (DF) ranged from zero (undesirable) to one (desirable) for each variable. The numerical optimization detects the points at which the DF achieves the maximum  $\text{Ni}^{2+}$  biosorption percentage using the DF option in Design Expert Software. In the current study, the optimum predicted conditions were achieved using DF for the maximum simultaneous biosorption of  $\text{Ni}^{2+}$  using *G. amansii* biomass (Figure 4) with contact time, temperature, and agitation speed quantified as 2.70 h, 44.39°C, and 116.86 rpm, respectively, which achieved 100%  $\text{Ni}^{2+}$  biosorption. To confirm the biosorption percentages of  $\text{Ni}^{2+}$  by *G. amansii* biomass using the optimal predicted conditions, the experiments were conducted in triplicate, and the experimental data were compared with the predicted values. The average biosorption percentages of  $\text{Ni}^{2+}$  were also 100.0%, which revealed a high degree of correlation between the experimental and expected data. The optimization conditions for removal lead by *Turbinaria ornata* were lead concentration 99.8  $\text{mg}\cdot\text{L}^{-1}$ , agitation speed 250 rpm, and adsorbent dose 16.2  $\text{g}\cdot\text{L}^{-1}$  [39].

### 3.8 The FTIR analysis

The FT-IR patterns of *G. amansii* biomass were recorded before and after  $\text{Ni}^{2+}$  biosorption, as illustrated in Table 6 and Figure 5, to identify the variations resulting from the interaction between the chemical functional groups on the *G. amansii* surface and  $\text{Ni}^{2+}$  ions during the biosorption process. Generally, red algal cell walls contain celluloses as well as sulfated polysaccharides such as agar

**Table 6:** Analysis of FTIR spectrum results of *Gelidium amansii* biomass before and after  $\text{Ni}^{2+}$  ion biosorption from aqueous solution

Before $\text{Ni}^{2+}$ ions biosorption (A)		After $\text{Ni}^{2+}$ ions biosorption		Difference	References
Wavenumber ( $\text{cm}^{-1}$ )	Annotations	Wavenumber ( $\text{cm}^{-1}$ )	Annotations		
4,414.24	O-H and C-O stretching combination band	4,413.28	O-H and C-O stretching combination band	+0.96	[40]
4,020.75	CH and C-O-C stretches and C-C vibration	4,026.54	CH and C-O-C stretches and C-C vibration	-5.79	[40]
3,960.96	Hydroxyl (OH) group	—	—	—	[44]
3,874.16	Hydroxyl (OH) group	—	—	—	[44]
3,441.12	N-H stretch	3,445.94	N-H stretch	-4.82	[47]
2,931.90	$\text{CH}_2$ groups	2,935.76	$\text{CH}_2$ groups	-3.86	[49]
1,650.16	C=O stretching	1,650.16	C=O stretching	0.0	[50]
1,538.28	C=O amide stretch	1,541.18	C=O amide stretch	-2.9	[52]
1,453.41	Stretch of C=C-C	1,443.77	Stretch of C=C-C	+9.64	[50]
1,085.96	O-H stretch	1,062.81	O-H stretch	+23.15	[53]
657.74	C-H bending vibration	658.71	C-H bending vibration	0.97	[54]
538.15	Glycosidic linkage	539.12	Glycosidic linkage	0.97	[55]



**Figure 5:** FTIR spectra of *Gelidium amansii* biomass: (a) before Ni<sup>2+</sup> ion biosorption and (b) after Ni<sup>2+</sup> ion biosorption from aqueous solution.

and carrageenan [40], the latter representing more than 75% of the dry weighted biomass [41], and carboxylic groups form the bulk acidic functional group and algal adsorption capacity are directly proportional to the existence of these active sites [19]. The weak recorded peaks at approximately 4,414.24 and 4,413.28 cm<sup>-1</sup> correspond to O–H and C–O stretching combination bands, while the peaks at 4,020.75 and 4,026.54 cm<sup>-1</sup> are assigned to the combination band of both CH and C–O–C stretches and C–C vibrations. All these peaks belong to cellulose [42]. Previous studies recorded that the cell walls of *G. amansii* generally contain cellulose [43]. The recorded bands

between 3,400–3,900 cm<sup>-1</sup> are related to hydroxyl (OH) groups, demonstrating the presence of carbohydrates [44–46], whereas galactan is a main polysaccharide in *G. amansii* [47]. The bands allocated at 3,441.12 and 3,445.94 cm<sup>-1</sup> could be attributed to N–H stretches existing in aromatic amines, primary amines, and amides [48,49]. Sukwong *et al.* [50] reported that *G. amansii* contains proteins such as R-phycoerythrin and R-phycoerythrin. The weak signals centered at approximately 2,931.90 and 2,935.76 cm<sup>-1</sup> are related to CH<sub>2</sub> groups [51]. The obtained peaks at approximately 1,650.16 cm<sup>-1</sup> exhibited C=O stretching related to carboxylic acids [52], while aromatic functions could be identified at approximately 1,538.28 and 1,541.18 cm<sup>-1</sup> [53]. Pugazhendhi *et al.* [54] reported the appearance of a C=O amide stretch at approximately 1,500 cm<sup>-1</sup>. Peaks at approximately 1,453.41 and 1,443.77 cm<sup>-1</sup> displayed symmetric and asymmetric stretches of C=C–C related to aromatic rings [52]. Moreover, the FTIR peaks centered at approximately 1,085.96 and 1,062.81 cm<sup>-1</sup> could be related to O–H stretching, a sign of the presence of carbohydrates and polysaccharides [52,55]. The weak resulting bands at 658.71 and 657.74 cm<sup>-1</sup> can be attributed to the C–H bending vibration, which is also a sign of the presence of carbohydrates [56]. Finally, the last bending at approximately 539.13 and 538.15 cm<sup>-1</sup> illustrates the presence of glycosidic linkage peaks in polysaccharides [57]. Biosorption of Ni<sup>2+</sup> ions enhanced shifts of some peaks, which illustrate the interaction between different chemical functional groups of the *G. amansii* biomass surface and Ni<sup>2+</sup> ions [58]. Table 7 illustrates the effects of different biosorbents related to various factors such as pH, initial Ni<sup>2+</sup> ions concentrations, biomass used, temperature, and time consumed in biosorption of Ni<sup>2+</sup> ions.

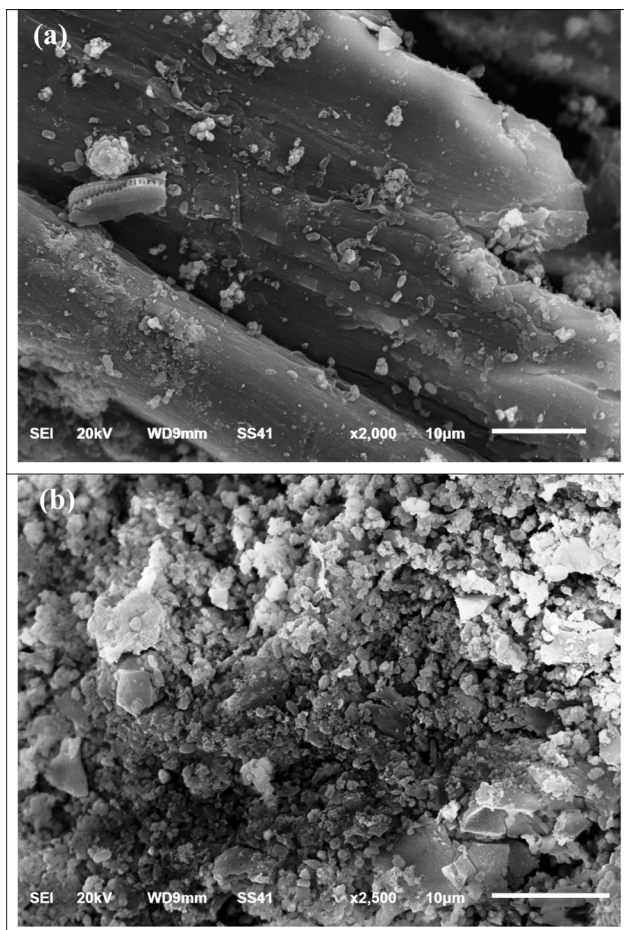
### 3.9 Scanning electron microscopy analysis

The micrograph obtained from SEM illustrated the morphological features of *G. amansii* biomass before and after the Ni<sup>2+</sup> biosorption process. As exhibited in

**Table 7:** Effect of different biosorbent and different factors in nickel ions removal

Bio-sorbent	Initial conc. (mg·L <sup>-1</sup> )	pH	Biomass	Absorption	Temperature	Time	Reference
<i>Aspergillus niger</i>	30	6.25	2.98	70.30%	—	—	[20]
<i>Rhodotorula glutinis</i>	—	—	—	43%	70°C	—	[57]
<i>Trichoderma viride</i>	—	—	—	99.77%	—	—	[58]
Pistachio hull powder	—	—	—	14 mg·g <sup>-1</sup>	25 ± 3°C	1 h	[57]
<i>Cystoseria indica</i>	100	6	—	75%	—	20 m	[21]
<i>Rhizopus arrhizus</i>	100	6	—	44.2%	—	—	[22]
<i>Acinetobacter baumannii</i> UCR-2971	—	4.5	4.0 g·L <sup>-1</sup>	3.5 mg·g <sup>-1</sup>	—	100 m	[23]
<i>Gelidium amansii</i>	25	7	1 g·L <sup>-1</sup>	100%	44.39°C	2.7 h	This research





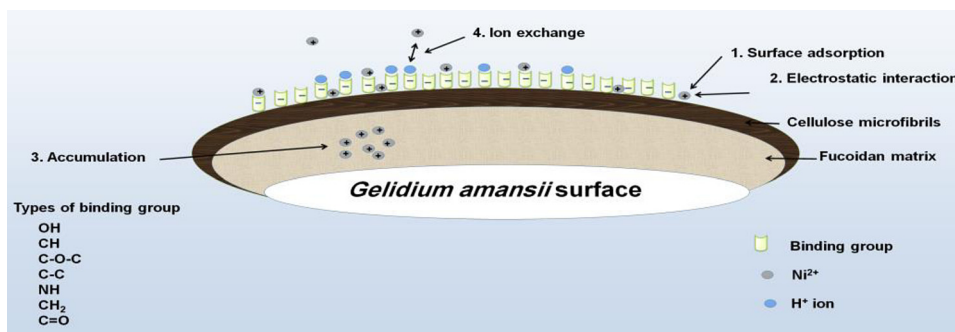
**Figure 6:** SEM micrograph of *G. amansii* biomass: (a) before and (b) after adsorption of  $\text{Ni}^{2+}$  ions from aqueous solution.

Figure 6a, native *G. amansii* has a plain, smooth, and uniform surface with a continuous interconnected structure, and this surface structure provides large active sites for the  $\text{Ni}^{2+}$  biosorption process. Conversely, Figure 6b demonstrates irregular, rough, and crashed surfaces accompanied by the presence of shiny spots as a result of  $\text{Ni}^{2+}$  accumulation. These variations may have resulted from

vigorous cross-linking binding between negatively charged functional groups in the cell walls and positively charged  $\text{Ni}^{2+}$  [59]. The biosorption and attachment of  $\text{Ni}^{2+}$  ions on the biosorbent surface are able to perform these changes [60]. This morphological variation confirms the ability of *G. amansii* biomass to perform biosorption processes. Figure 7 shows the mechanisms of biosorption  $\text{Ni}^{2+}$  ions by *G. amansii* biomass, which demonstrates that metal ions complex with active groups in the cell wall on the cell surface in the adsorbents, and the bond formation could be covalent or electrostatic [61]. The principal binding mechanisms of the biosorption by the algae include ion exchange, formation of complex between heavy metal contaminants cations and the ligands on the algal surface, diffusion interior of the cells or surface precipitation, chelation, and bioaccumulation within the cells [62]. Red algae cell wall contains calcium carbonate beside a variety of functional groups on the surface of the algal biomass such as  $\text{CH}_2$ ,  $\text{C-H}$ ,  $\text{C=O}$ ,  $\text{N-O}$ ,  $\text{C-N}$ ,  $-\text{OH}$ ,  $\text{PO}_4$ , and  $-\text{NH}_2$ ; these groups can assist adsorption sites that are responsible for metal ions biosorption [63]. There are many factors affecting heavy metals sorption mechanisms by algae. Tang et al. [64] reported that there were mutual effects between pH and heavy metal ion elimination by algae. The factor affecting the sorption mechanisms (pH, temperature, types of contaminants, and time) depends on the type of the biosorbent [65].

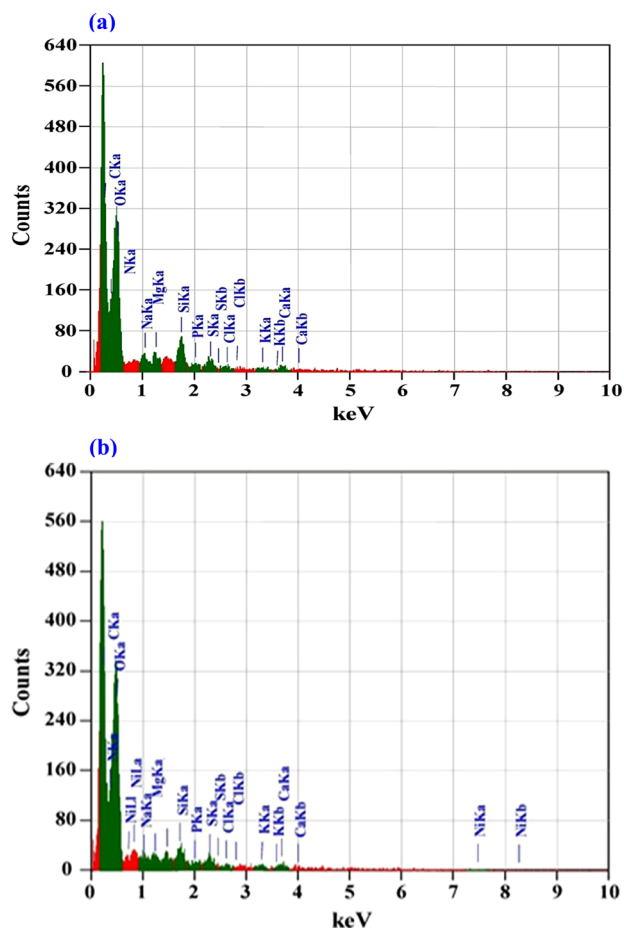
### 3.10 Electron dispersive spectroscopy analysis

EDS analysis mapping illustrates the atomic percentages of various elements for both *G. amansii* biomasses before and after adsorption of  $\text{Ni}^{2+}$  ions from the aqueous solution (Figure 8 and Tables 8 and 9). Figure 8a and Table 8 demonstrate the native *G. amansii* biomass composition



**Figure 7:** Mechanism of bio-removal nickel ions by *G. amansii* biomasses.





**Figure 8:** EDS analysis of *G. amansii* biomass: (a) before and (b) after adsorption of  $\text{Ni}^{2+}$  ions from aqueous solution. For reference, please see Tables 8 and 9.

with the dominance of carbon and oxygen with some traces of other elements, such as Na, Mg, Si, P, S, Cl, K,

**Table 8:** EDS analysis of *G. amansii* biomass before adsorption of  $\text{Ni}^{2+}$  ions from aqueous solution

Element	keV	Mass%	Error%	At%	Compound mass% cation K
C K	0.277	45.95	0.54	55.72	32.7379
O K	0.525	42.35	1.85	38.55	47.8738
Na K	1.041	1.27	1.24	0.8	1.6625
Mg K	1.253	1.17	1.03	0.7	1.4643
Si K	1.739	3.98	1.1	2.06	6.4767
P K	2.013	0.67	1.18	0.32	1.1435
S K	2.307	1.49	1.06	0.68	2.7445
Cl K	2.621	0.8	1.3	0.33	1.4863
K	3.312	0.52	1.93	0.19	0.9552
Ca K	3.69	1.8	2.36	0.56	3.4553
Total		100.00		100.00	100.00

**Table 9:** EDS analysis of *G. amansii* biomass after adsorption of  $\text{Ni}^{2+}$  ions from aqueous solution

Element	keV	Mass%	Error%	At%	Compound mass% cation K
C K	0.277	46	0.47	55.38	35.2614
O K	0.525	44.68	1.75	40.38	50.1642
Na K	1.041	0.27	1.26	0.17	0.3252
Mg K	1.253	0.8	1.02	0.48	0.9542
Si K	1.739	1.71	1.1	0.88	2.6077
S K	2.307	1.52	1.03	0.69	2.6697
Cl K	2.621	0.49	1.27	0.2	0.8692
K K	3.321	0.96	1.89	0.36	1.7094
Ca k	3.69	1.01	2.31	0.37	1.8648
Ni K	7.471	2.55	12.18	1.1	3.5441
Total		100.00		100.00	100.00

and Ca. Figure 8b illustrates the presence of a newly formed peak of  $\text{Ni}^{2+}$ , which confirmed the biosorption process. Overall, the algae and seaweed biomass can be used to sustainably remove heavy metals from wastewater [66].

## 4 Conclusions

In the current study, *G. amansii* biomass displayed an effective capability as a sustainable biosorbent for the biosorption of  $\text{Ni}^{2+}$  from the aqueous solution. Three independent variables (contact time, temperature, and agitation–static mode) exhibited a high level of significance on the  $\text{Ni}^{2+}$  biosorption process. The maximum  $\text{Ni}^{2+}$  biosorption percentage was quantified as 100.00% under the experimental conditions of 3 h of incubation time and 45°C and 100 rpm for agitation speed. The DF confirmed optimum predicted conditions for the maximum simultaneous biosorption of  $\text{Ni}^{2+}$  using *G. amansii* biomass with contact time, temperature, and agitation speed quantified as 2.70 h, 44.39°C, and 116.86 rpm, respectively, which achieved 100%  $\text{Ni}^{2+}$  biosorption. The interaction between the *G. amansii* surface and  $\text{Ni}^{2+}$  ions during the biosorption process was illustrated using FTIR, SEM, and EDX analyses. The micrograph obtained by SEM demonstrated irregular, rough, and crashed surfaces conveyed by the occurrence of shiny spots as a result of  $\text{Ni}^{2+}$  accumulation. *G. amansii* biomass contents have dominance of carbon and oxygen with some trace elements such as Na, Mg, Si, P, S, Cl, K, and Ca as proved by EDX.

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