



# A Critical Look at Bioproducts Co-cultured Under Solid State Fermentation and Their Challenges and Industrial Applications

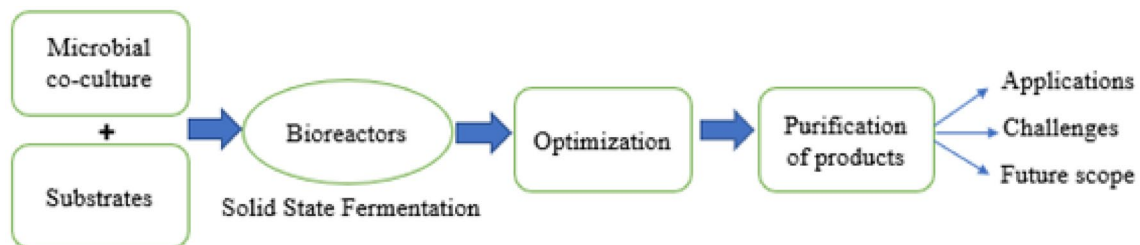
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## Abstract

The production of bioproducts from microorganisms is a common practice in many industries for a long time now. In recent years, studies have proved that co-culturing microorganisms increase the yield of products by synergistically degrading the solid substrate in comparison with individual cultures. The review highlights the benefits of co-culturing microorganisms using solid state fermentation (SSF) to achieve higher productivity. Filamentous fungi of genus *Trichoderma*, *Penicillium*, and *Aspergillus* are extensively studied and used for co-culturing and mixed culturing under SSF. Co-cultured microorganisms are beneficial because of the synergistic expression of metabolic pathways of all the microorganisms. Co-culture enables combined metabolic activity at optimal process conditions for better utilization of substrates. Depending on the nature of the process and microorganism, bioreactors are designed and operated. This review mentions various purification methods that are used to improve the purity of the products obtained. The strengths and weaknesses of various bioreactors and their effect on the microorganisms used are explained in detail. This review also identifies the challenges of co-culturing microorganisms and analyses the diverse set of fields in which SSF finds its applications.

## Graphical Abstract



**Keywords** Co-culture · Microbial bioproducts · Solid state fermentation · Bioreactors · Optimization · Purification · Applications

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## Statement of Novelty

This review provides updated literature on co-culture studies using Solid State Fermentation. Reports on new substrates and microorganisms with co-culture are elucidated for diverse applications. The paper highlights purification methods and approaches for enhancing the yields of products. Results of optimization studies carried out are also described in a separate section. Under the future scope, the scale-up of co-culture studies with different types of bioreactors that are suitable for solid state fermentation is explained.

## Introduction

### Co-culture

Co-culture is the method of culturing different microorganisms, to test the effect of one culture system over another. Microorganisms are not present as pure cultures in nature. Microorganisms belonging to the same genus have shown better compatibility with each other, hence are extensively used to produce various metabolites. This can be inferred from studies on pair of microorganisms such as *Bacillus cereus* and *Bacillus thuringiensis*, *Aspergillus niger* MS23, and *Aspergillus terreus* MS105, *Clostridium thermocellum* ATCC 27405 and *Clostridium beijerinckii* ATCC 51743, *Aspergillus flavus* and *Aspergillus penicillioides* [1–4].

Natural environments are distinguished by a variety of microorganisms that interact with one another in complex ways [5, 6]. The growth of pure culture is significant unlike its growth in a mixed culture, on account of several microbial interactions [7]. These microbial interactions can be antagonistic or synergistic, resulting in inhibited or enhanced proliferation respectively. The microbial co-cultures are living systems wherein there coexist varied interactions between two or more different microorganisms. The organisms grow with some level of contact amongst themselves within a definite, natural, or artificial media [8, 9]. The organisms can grow independently or at the same time depending on the strength of the synergic interactions between them [10].

A positive interaction amongst the microbial populations may result in an increased growth rate of one microorganism or a group of microorganisms in a particular habitat. Enhanced production of growth-associated metabolites is possible due to synergism. For example, in a pair of microorganisms *Bacillus subtilis* CDBB 555 and *Clostridium acetobutylicum* ATCC 824 were utilized for the production of butanol, in which *Bacillus subtilis* CDBB 555 maintained anaerobic condition by consuming oxygen required for *Clostridium acetobutylicum* ATCC 824 which in turn produced butanol as the metabolite [11]. The results of co-culture work on *Kluyveromyces marxianus* and *Saccharomyces cerevisiae* strains reported by Molefe [12] showed enhanced activities of both the invertase and inulinase enzymes required for the production of fructose by hydrolysis of inulin. Co-culturing fungi not only paves the way for enhancing the production of specific products but also may facilitate the detection of new biomolecules that are usually not produced when pure cultures are individually cultured [13] thus posing immense potential with industrial applications. Thus, co-culturing can be an alternate approach to improve the production of microbial bioproducts and metabolites [14].

A mixed culture could contain varieties of viruses, fungi, and bacteria, which may or may not be sustained by

sharing the available resources. These consortia could be made up of species that are known or unknown. Mixed cultures are used in many microbiological processes such as in waste treatments. Combining an ideal group of enzymes can result in the most efficient biodegradation process by mixed culturing of fungi on solid substrates [15]. The study of microbial interactions can be well explained in co-culturing and mixed culturing techniques to maximize the metabolite production along with the process optimization methods [16].

### Microbial Bioproducts

Microbial bioproducts have gained importance as they are eco-friendly, sustainable, easily available, and biodegradable. Enzymes, citric acid, and bioethanol produced from microorganisms are used on a large scale across various sectors [17, 18]. With the help of gene manipulations, microbial bioproducts can be cultured largely as per the need of a particular enzyme at the industrial level. Microorganisms excrete biological catalysts called enzymes during their growth and metabolism, to carry out the biochemical reactions and produce various fermentation products [16]. Microbial enzymes are classified as endo-cellular and exo-cellular enzymes. Enzymes produced in the cytoplasmic membrane or within the cell are endo-cellular enzymes. Exo-cellular enzymes are secreted by the cells and function outside the cell. These enzymes are liberated into the fermentation medium to hydrolyze and break down complex substances that are too huge to be transferred into the cell [19]. Studies have shown that many enzymes secreted by microbial fermentation for industrial applications are exocellular [11, 12]. In recent years, microbial bioproducts have acquired importance around the globe for their extensive uses in sectors like agriculture, medicine, food, chemicals, and energy [20]. Enzymes such as inulinase, amylase, protease, laccase, catalase, mannanase, pectinases, cellulase are extensively being used in various industrial sectors such as food and beverages, textile, pharma, detergents, and chemical [21]. Enzyme-mediated processes take less time, require low energy input, are eco-friendly, and are affordable. Because of these advantages and their widespread applications, microbial bioproducts are rapidly gaining interest worldwide [22]. Bioproducts research is becoming one of the most exciting topics of material science and engineering due to the increasing global demand and environmental friendliness.

### Solid-State Fermentation

Solid-state fermentation (SSF) is the fermentation method that involves a solid matrix consisting minimum required amount of water. The amount of moisture in the substrate should be just enough to bear the growth and metabolism of

the selected microbial culture [23]. The selected solid matrix (substrate) will mimic an environment suitable for the development of microorganisms [24]. The solid matrix can either act as a nutrient source or only act as matrix support which has been impregnated with appropriate nutrients that allow the growth of the microorganisms [25]. Substrates should be able to absorb and provide the required moisture without getting dissolved [26]. Determination of a significant substrate is a vital step in the SSF process. Unlike SmF (Submerged fermentation), only limited types of microorganisms i.e., fungi and yeasts, can be used for SSF due to low freely available moisture. In some cases, bacteria also have been employed [27]. Factors affecting the fermentation process include a substrate, temperature, size of substrate particle, moisture, agitation, and aeration. Another key parameter in the SSF process is the water activity ( $a_w$ ) of the medium for transport of solutes and water beyond the microbial cell wall and is, therefore, one of the main parameters to control fungal metabolism [23, 28–30].

## The Industrial Importance of SSF

SSF is a common technique used to get various products economically. It is mainly used to produce enzymes, industrial chemicals, single-cell proteins, phenolics, food, biofuel, biologically active secondary metabolites (alkaloids, antibiotics, immune drugs, and toxins), metabolites and pharmaceutical products [31]. The morphology of many microorganisms which are composed of branched, thread-like hyphae provides conducive conditions in SSF to produce microbial secondary metabolites [32].

The beneficial features of SSF in comparison with SmF includes reduced energy consumption as it requires relatively lesser agitation, lower water requirement, and wastage as little or no free water is used in the fermentation bed, thereby leading to a reduction in the probability of contamination [33, 34]. Other advantages of SSF include smaller size fermenters, inexpensive fermentation media, ease of handling, and the enhanced yield of metabolites [35–39]. SSF uses a wide variety of solid or semi-solid substrates which vary in properties like size, composition, porosity, mechanical resistance, and water holding capacity. The substrates used are generally industrial or agricultural wastes which are usually cheap and resistant to various contaminants. The downstream processes are less expensive as it requires lower recovery cost and less solvent. Enzymes are present in the concentrated form and are easily extractable. Disadvantages of SSF include the difficulty in maintaining and controlling the physical parameters. For example, the initial moisture level in the substrate decreases over a period and must be checked periodically.

The objective of this review is to depict the benefits of co-culturing microorganisms owing to their synergism in SSF. The industrial applications of co-culturing microorganisms in a wide range of sectors such as biofuel, food, and pharmaceutical industries are elucidated. The challenges and future scope of co-culture systems are also discussed.

## Microorganisms and Substrates

Microorganisms have proved to be the main source for the production of commercial products in particular enzymes. The microorganisms utilized for the biosynthesis of industrial enzymes must possess good biological activity [40]. In this review, we focus on the importance and benefits of co-cultured microorganisms. Apart from the factors affecting solid state fermentation processes, the type and extent of interactions among the co-cultured microorganisms is the one that uniquely contributes to the observed difference between single-culture and co-culture systems, with regards to the product yield and overall efficiency of the SSF process. Both organisms in the co-culture can be isolated from the same or different sources. It has been noticed that organisms isolated from the same source often show synergism and hence, are favored. Synergism can be considered as the capability of two or more microorganisms, when grown together, leading to enhanced production of metabolites in comparison with total productivity observed when grown independently [41]. Synergistic interactions between different but compatible microorganisms under alike environmental conditions have proved to produce better yields than just individual pure cultures [11, 12]. The mixed microbial cultures used under SSF have been shown to achieve elevated levels of output of abundant bio-active molecules consisting of enzymes, amino acids, vitamins, and antibiotics. Commensalism among microorganisms is considered to be a relationship wherein one microorganism is benefitted while the other is neither benefitted nor harmed in any manner [42]. This can be observed in natural environments and has been exploited in several fermentation reactions to produce varieties of foods products such as cheese. An appropriate amount of information on the progress of growth and survival of interacting microorganisms is needed to confirm whether there is no effect on one of the microorganisms while the other thrives and benefits from this kind of association [42, 43]. When each of the participating microorganisms benefits from the interaction, it can be termed as a mutualistic type of interaction. Microorganisms are bound by a common interest in such an association [16]. Synergistic interactions between microorganisms also lead to securing mutual benefits as in the case of mutualism yet differ in the fact that involving microorganisms are fully capable of surviving on their own and are not obligated to

establish such an association [42, 44]. Generally, accessing the type of positive interaction or ensuring the compatibility between microorganisms in solid state fermentation, whether it is synergistic, mutualistic, or commensalistic is a tough and crucial task that demands meticulous analysis of their growth curves. The occurrence of such positive interactions amongst microbial populations (commensalism/ mutualism/ synergism) can potentially promote their overall growth resulting in an increased production of certain growth-associated products. Only those microbial strains are selected that exhibit synergism, mutualism, or commensalism [42]. Compatibility analysis is carried out by comparing the growth curves of both the microorganisms first in a single culture and then in a mixed culture. Fossi et al. [16] critically analyzed the growth curves of both pure and mixed cultures of *Bacillus amyloliquefaciens* 04BBA15 and *Saccharomyces cerevisiae* for the production of  $\alpha$ -amylase, which showed a notable increase in growth of *S. cerevisiae* while the growth of *B. amyloliquefaciens* 04BBA15 was unaffected when grown together. The commensalism relationship between these species could be justified by the fact that glucose released into the medium as a result of starch hydrolysis by *B. amyloliquefaciens* was consumed by non-starch utilizing *S. cerevisiae* for its efficacious growth. Fossi et al. [16] also reported mutualism of two strains by comparing the growth profiles of both pure and mixed cultures of *Saccharomyces cerevisiae* and *Lactobacillus fermentum* 04BBA19, which showed a significant rise in the growth of each of the two strains when cultured together. The  $\alpha$ -amylase activity of *L. fermentum* released glucose which was subsequently consumed by *S. cerevisiae* thereby suppressing the inhibitory effect of excess glucose [16].

In SSF, insoluble solid substrates act not only as a nutrient source but also as solid support for the upsurge of microbes. Nearly all the substrates that are employed in SSF are inexpensive agricultural residues generated from agro-industrial activities, those of which are otherwise under-utilized. Fungi with their extensive network of hyphae are capable of growing over and utilizing the agro-industrial waste conveniently as it mimics their natural habitat. Nutrient-rich substrates decompose steadily which can be used for a longer time and be reprocessed later. This diminished the need for replenishing substrates under SSF [45].

One of the prime components that indifferently affect single cultures and co-culture systems under the operation of SSF is the property of the solid substrate utilized. Factors such as moisture level and particle size are essential for the optimal microbial activity and growth on a specific substrate [46, 47]. The particle size of the solid substrate directly influences its surface area to volume ratio and hence indirectly affects the extent to which microorganisms are in contact with the nutrient and oxygen diffusivity [48]. Smaller particle size contributes to a larger surface area to volume

ratio which in turn provides a higher contact between microorganisms and nutrients but hinders the diffusion of oxygen. On the other hand, larger particles having a smaller surface area to volume ratio lessen the contact with nutrients but aid excellent oxygen diffusivity [27]. Therefore, appropriate particle size must be chosen to ensure optimum mycelial growth, oxygen, and nutrient supply [49]. The metabolic activities of microbial cultures and accordingly the resultant products have been observed to be affected by higher and lower initial moisture levels [50]. This can be understood by the fact that lower moisture levels result in the poor dissolution of nutrients from the solid substrate and increased water tension. Likewise, it has been reported that higher moisture levels lead to reduced porosity, poor gas exchange, the disappearance of particulate structure, the occurrence of stickiness, and increased formation of an aerial type of mycelium [51]. As per the above discussions, these factors are applicable for all microorganisms including co-cultured microorganisms. Ideally, a solid substrate used in SSF must be capable of acting as physical support, source of essential nutrients needed for the growth of all desired microorganisms involved, and as an appropriate inducer in case of enzyme production, all of which is difficult to be satisfied by a single substrate. Thus, this bottleneck can be overcome by the utilization of mixed substrates under SSF for co-cultures [52] which have been shown to enhance the product yield adequately [53]. While employing mixed substrates under SSF to nurture the given microbial co-culture, their nature and proportions are deciding factors for achieving an optimal product yield [54]. Some of the substrate combinations such as pineapple peels, banana peels, and papaya peels [55], corn cob and Bermuda grass [56], wheat bran, pulse husk, and mustard peel [57], freeze-dried okara and pork lard [58] are utilized to facilitate better nutrition for growth and thus improving the yield of the product.

Table 1 depicts that  $\alpha$ -amylase can be produced either from a bacterial co-culture of *Bacillus thuringiensis* and *Bacillus cereus* [1] or by employing fungal co-cultures of *Phanerochaete chrysosporium* and *Schizophyllum commune* [55] or *Aspergillus niger* GS1 and *Trichoderma reesei* [56]. Cellulase enzymes can be synthesized by using various combinations of not only fungal co-cultures as mentioned [10, 59] but also from a bacteria-fungi co-culture of *Bacillus-Trichoderma* [60]. It can be deduced that a particular product can be obtained by co-culturing different combinations of microorganisms. This shows the existence of synergism between several microorganisms. Fungal co-cultures are widely studied when compared with bacterial co-cultures in SSF as it supports low water content which is favorable for the growth of fungi. *Aspergillus sp.* and *Trichoderma sp.* are extensively used for co-culturing. These fungi are isolated from diverse sources to produce a broad spectrum of products under SSF.

**Table 1** Sources and substrates utilized for microbial co-culture under solid state fermentation

Sources	Substrate	Product	References
<i>Bacillus thuringiensis</i> and <i>Bacillus cereus</i>	Wheat bran	$\alpha$ -amylase	[1]
<i>Aspergillus terreus</i> MS105 and <i>Aspergillus niger</i> MS23	Lime peels	Cell wall degrading enzymes	[2]
<i>Clostridium beijerinckii</i> ATCC 51743 and <i>Clostridium thermocellum</i> ATCC 27405	Corn stover and silvergrass ( <i>miscanthus</i> )	Ethanol, acetic acid, lactic acid, butyric acid, acetone and butanol	[3]
<i>Aspergillus penicillioides</i> and <i>Aspergillus flavus</i>	Wheat bran	Xylanase, Fpase, $\beta$ -xylosidase, CMCCase	[4]
<i>Trichoderma reesei</i> , <i>Aspergillus oryzae</i> , and <i>Phanerochaete chrysosporium</i>	Soyabean cotyledon fiber and distiller's dried grains	Xylanase, Cellulase	[10]
<i>Aspergillus niger</i> ATCC 10864 and <i>Trichoderma reesei</i> LM-1	Extracted sweet sorghum silage	Cellulase, Xylanase	[15]
<i>Cladosporium sphaerospermum</i> , <i>Aspergillus flavus</i> and <i>Epicoccum purpurascens</i>	Sawdust and wheat bran	Xylanase	[54]
<i>Phanerochaete chrysosporium</i> and <i>Schizophyllum commune</i>	Pineapple peels, banana peels and papaya peels	$\alpha$ -amylase, Cellulase	[55]
<i>Trichoderma reesei</i> and <i>Aspergillus niger</i> GSI	Corn cob and Bermuda grass	Fpase, Amylase, Xylanase	[56]
<i>Trametes hirsuta</i> and <i>Phanerochaete sp</i>	Wheat bran, pulse husk and mustard peel	Laccase, Pectinase	[57]
<i>Aspergillus penicillioides</i> and <i>Aspergillus flavus</i>	Freeze-dried okara and pork lard	Bio valorisation of the product with antimicrobial activity and antioxidant	[58]
<i>Penicillium citrinum</i> NCIM 768 and <i>Trichoderma reesei</i> NCIM 1186	Wheat bran	Cellulase	[59]
<i>Bacillus-Trichoderma</i> co-culture	Palm kernel cake	Cellulase	[60]
<i>Eupenicillium crustaceum</i> and <i>Paceliomyces sp.</i>	Paddy straw	Endoglucanase, Xylanase, Filter paperase, $\beta$ -glucosidase	[91]
<i>Trichoderma reesei</i> and <i>Aspergillus niger</i>	Kinnow fruit pulp and peel	Filter paperase, CMCCase, $\beta$ -glucosidase	[92]
<i>Trichoderma reesei</i> and <i>Aspergillus fumigatus</i>	<i>Dioscorea zingiberensis</i> (a species of yam)	Diosgenin	[90]
<i>Trichosporonoides oedocephalis</i> and <i>Penicillium italicum</i>	Orange peels	Mannanase	[93]
<i>Daldinia concentrica</i> and <i>Xylaria polymorpha</i>	Bean husks	Decolorization and the detoxification of Cibacron brilliant red 3B-A	[94]
<i>Rhizopus stolonifera</i> and <i>Aspergillus niger</i>	Orange peel	Citric acid	[17]
<i>Trichoderma sp.</i> And <i>Saccharomyces cerevisiae</i>	Sweet potato flour	Bioethanol	[77]
<i>Aspergillus ornatus</i> and <i>Alternaria alternata</i>	Apple pomace	Citric acid	[18]

The substrates listed in Table 1 are a wide variety of cost-effective solid substrates and are easily available. The widely used substrates are agro-industrial wastes mainly wheat bran, fruit peels, and sugarcane bagasse. Most of these compounds are polymeric molecules and constitute a rich source of nutrients. The choice of considering crude or purified substrates for enzyme production in SSF also has an impact on the outcome [2]. In the case of xylanase production, the use of purified substrates such as xylan accounted for 0.007 g total reducing sugar whereas banana peels being a natural substrate showed 0.28 g per 0.5 g of substrate. Generally, the substrates used are heterogeneous and sparingly soluble or insoluble in water. Most of the time, pre-treatment of substrates is required to enhance their accessibility

before it is used for the fermentation process [61]. Pretreatment methods can be either physical, chemical, biological, or a combination of these methods [62–64]. The nature of the substrate greatly affects the choice of the pretreatment method. Physical methods include grinding, milling, densification, irradiation, and high temperature which can improve product yields by increasing the available surface area and size of pores [65–67]. Chemical type of pretreatment widely involves the use of acids, alkali, ammonia, and related methods [68]. Biological methods of pretreatment include enzymatic methods of degradation. It has proven to be an inexpensive, low-energy, safe and eco-friendly way to remove lignin from lignocellulose [69]. Corn stover substrates used for butanol production were subjected to the



biological type of pre-treatment utilizing solid state cultivation of *Phanerochaete chrysosporium* ATCC MYA-4764 to degrade the lignin content. This is because the butanol-producing bacterial co-culture is incapable of catabolizing complex lignocellulosic substrates [3]. Thus, such pretreatment techniques hold immense potential to improve the overall process efficacy and lessen the cost through extensive research and development [70].

## Fermentation and Optimization Techniques

### Fermentation Process

The factors that affect the fermentation process of co-culture are the compositions of fermentation media, water activity, moisture content, inoculum volume, sequence of inoculation, incubation temperature, and nature of the substrate. These physicochemical factors contribute immensely to the

production of the desired products [71]. Pre-treatment of the substrate is recommended as it enhances its properties as described in the previous section. Industrial SSF processes are carried out in trays, packed-bed, horizontal drum, and fluidized-bed reactors [33].

The major role of SSF bioreactors is to incorporate the substrate, maintain aseptic conditions, meet the oxygen requirement for aerobic fermentation, monitor the heat transfer and mass transfer effects and regulate the environmental conditions to enhance the growth of microorganisms and therefore improve the product yield [72, 73]. Figure 1 explains the types of lab-scale, pilot, and industrial-scale bioreactors. It also explains the various aeration strategies used in these different bioreactors.

The bioreactors in group 1 (Fig. 1, upper-right quadrant) have trays stacked one on top of the other and consist of a chamber. The air blown into the chamber is conditioned and controlled. Trays used are usually made of wood, metal, plastic, or bamboo. The agitation is generally done by hand

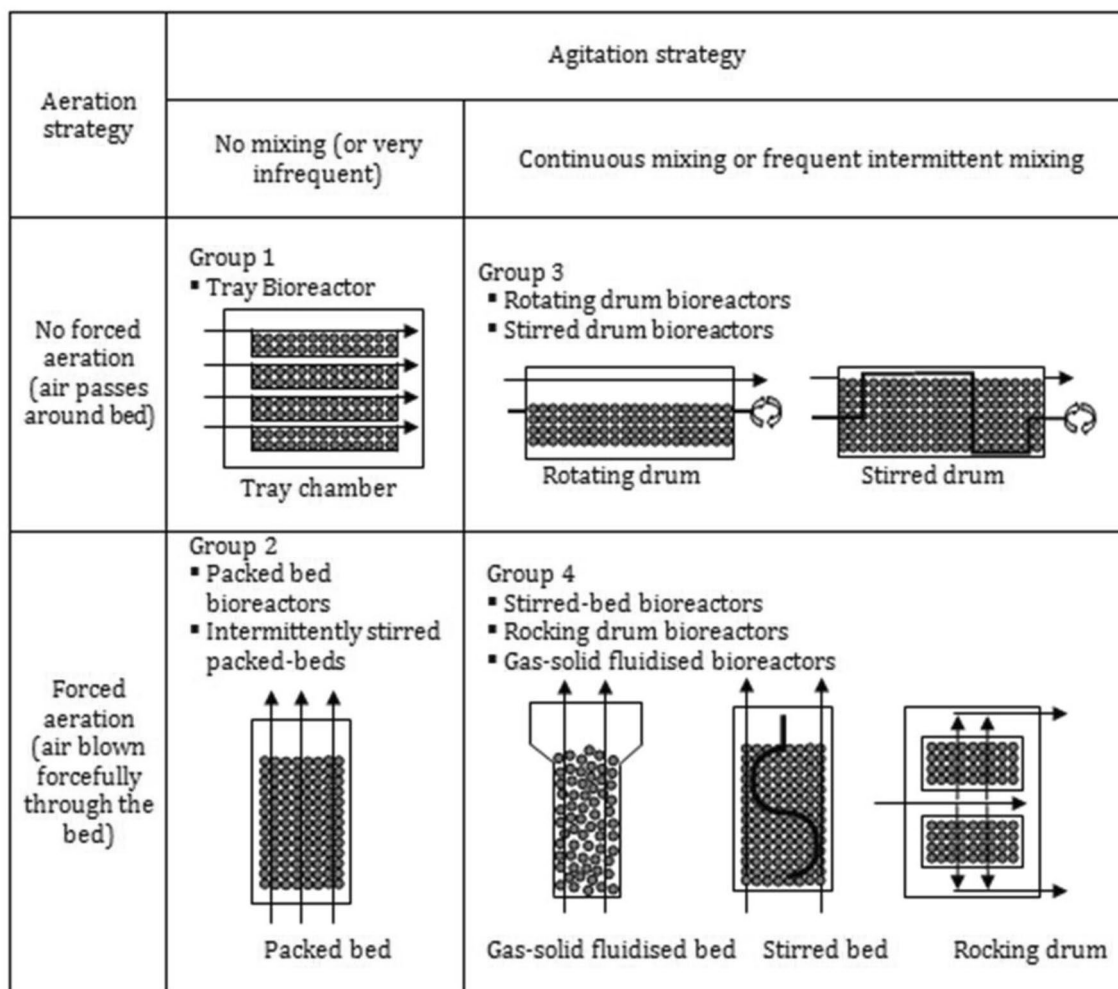


Fig. 1 Agitation strategy of bioreactors under solid state Fermentation [33]

and hence is not very frequent. The chamber is open at the top and has perforated bottoms to increase the accessibility to oxygen. Group 2 (Fig. 1, lower-left quadrant) is a characteristic packed-bed bioreactor consisting of a column of rectangular or cylindrical cross-section, in which the air is blown up through the base plate. Such bioreactors are typically oriented vertically with a perforated base plate at the bottom which supports the substrate bed. The bioreactors in group 3 (Fig. 1, upper-right quadrant) are generally horizontal and consist of a drum of a cylindrical cross-section. The whole drum rotates around its central axis to mix the substrate bed in rotating drums. As for the stirred drums, the bioreactor body remains stationary and paddles or scrapers mounted on a shaft running along the central axis of the bioreactor rotate within the drum. The mixed and forcefully aerated bioreactors in group 4 (Fig. 1, lower-right quadrant) can be operated with continuous or discontinuous mixing [33].

The selection criteria of bioreactors for single cultured and co-cultured organisms depends on the optimum operating parameters such as type of microorganisms used, oxygen requirement, the resistance of the microorganisms to mechanical agitation, moisture level, and temperature [30, 39]. The same bioreactors can be used for both the above-mentioned types of organisms used. Parameters like diffusion, pore size are applicable for single as well as for co-cultured systems. The different types of industrial and

pilot-scale bioreactors are unmixed SSF bioreactors with and without forced-air circulations, intermittently mixed-bed bioreactors with air circulation, and continuously mixed SSF bioreactors with air circulation [30, 39, 72, 73]. The features and limitations of some commonly used bioreactors under SSF are tabulated in Table 2. There are no studies reported on bioreactors for SSF using co-culture systems. Research on the design and operation of bioreactors for SSF with co-culture offers an opportunity for future studies.

Apart from the above-mentioned bioreactors (Fig. 1), rotating disc reactors, stirred drum bioreactors, zymotis packed-bed bioreactor, spouted-bed bioreactor, air pressure pulsation solid state bioreactors, and immersion bioreactors are used under controlled conditions. The zymotis bioreactor is grouped as a packed bed fermenter as the moist solid substrate is packed into the rectangular box fermenter. It is a novel large-scale solid-state fermenter, that not only can control various vital process parameters such as temperature, moisture content, and aeration but is also equipped with a novel cooling system for the easy removal of the huge amount of metabolic heat generated. Zymotis with its simple design and ease of operation has shown abundant potential in encouraging SSF technologies for industrial utilization and thus directing the harvest of several economical merits of SSF. The main advantages are that it overcomes problems like heat removal and leads to the stable and

**Table 2** List of broadly used solid state fermentation bioreactors' features and limitations [33, 72]

Bioreactor	Bioreactor features	Limitations
Bench scale, Erlenmeyer flask, petri dish	Quicker optimization of the experimental and process values Cheap, small amount of substrate used and lower risk of contamination Passive aeration, easy regulation of airflow rate and temperature	Heat accumulation, non-mixed and inadequate aeration
Tray bioreactors	Substrate is spread on the reactors made of flat trays forming a thin layer Aeration is maintained through airflow at constant temperature and pressure	Required many trays and therefore larger area and volume which makes it tedious and extremely unattractive for industrial scale Non-uniform growth
Packed-bed bioreactors	The substrate is retained on the perforated base of the main body of the bioreactor A jacket is fitted around the bioreactor to adjust the temperature to the desired value	Difficulties for sampling, scaling up problems, bed caking, non-uniform growth, low heat removal and labour-intensive
Horizontal drum bioreactors	Mixing is achieved by the agitation of baffles and paddles Mixing of the substrate and proper aeration	Due to agitation, the product and the inoculum can get damaged Only 30% of the drum is filled, otherwise mixing is not efficient
Fluidized-bed bioreactor	The reactor uses continuous agitation with forced air This prevents the aggregation and adhesion of solid particles High heat and mass transfer rate	The final yield of the product can be affected due to inoculum damage and heat build-up Difficult to fluidize large, sticky and coarse particles

controlled performance of the bioreactor [74]. Whereas in the spouted-bed reactor, only a part of the substrate bed is fluidized as air is blown upwards through the central axis of the bed. The solid slips to the bottom of the bioreactor due to its sloped sides because of the vigorous contact between the solid substrate particles and the gas (Fig. 2) [75]. It has reduced power requirements when compared with fluidized-bed systems. It is good at handling large, non-uniformly sized, coarse, and sticky particles. The advantage of the spouted-bed bioreactor is that it stops particle accumulation created by high-speed collisions in the spouted bed's core region [33, 76]. However, the tray bioreactor is most used for enzyme production and is the most suitable for the scale-up process [31, 77, 78].

### Optimization Techniques

Optimization of process parameters plays a very important role in any type of fermentation process to enhance the yield of microbial metabolite [71]. Various optimization techniques are adopted to find the optimum values of process parameters. The most used optimization techniques are Evolutionary operation factorial design technique (EVOP), Plackett–Burman's Design (PBD), one factor at a time (OFAT), central composite design (CCD), Box–Behnken design (BBD), artificial neural network (ANN) and genetic algorithm (GA). Design of the fermentation process is a tedious task and each optimization technique used would show its impact on the result of the process. Generally, these techniques are used in combinations to obtain the required outcome. The simple and the most preferred optimization technique is OFAT, wherein only one factor is changed at a time by retaining the remaining operational parameters [79]. PBD, a two-level design is phenomenal in eliminating the non-contributing parameters and helps in screening the process factors [80]. Factorial design technique employs

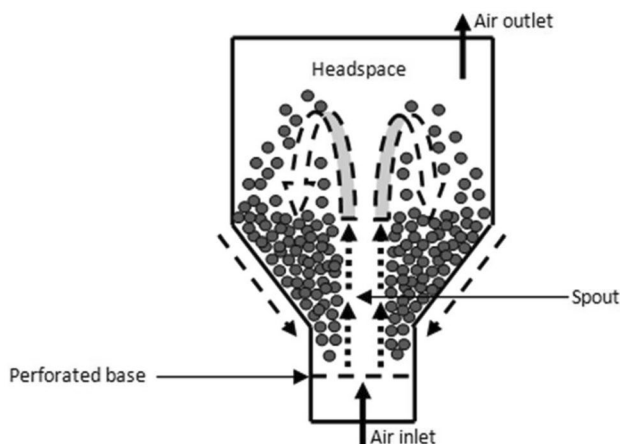


Fig. 2 Spouted-bed bioreactor [33]

independently varying levels of factors or parameters, each factor at two or more levels whereas evolutionary operation uses factorial design to better the yield. EVOP being the hybrid child of factorial design and evolutionary operation possesses the capacity to both, design experiments with  $n$  parameters and to systematically analyze the experimental results and provide conclusive data on optimum fermentation conditions [79].

Table 3 depicts that *Bacillus cereus* and *Bacillus thuringiensis* co-culture yielded an amylase production of 44.0 U/mL/min using wheat bran as the substrate in SSF [1] whereas *Aspergillus niger* GS1 and *Trichoderma reesei* fungal co-culture provided a profound amylase yield of 181.4 U/g.h using bermudagrass and corn cob used as the substrate [56]. As mentioned before, it can be observed that under SSF, bacterial co-cultures give comparatively lesser yield than fungal co-cultures owing to the fungal growth favorable environment of SSF. To achieve better growth and higher enzyme production, the inoculation sequence of different microorganisms can be studied to recognize the one that provides the best interaction among the microorganisms. Thus, the order in which the microorganisms are inoculated for co-culturing purposes is also one of the deciding factors to get a higher yield [10].

Co-culture of microorganisms with optimization techniques is a strategy to enhance enzyme production. Mostafa et. al. [54] reported the fungal co-culture for the production of xylanases using three organisms *C. sphaerospermum*, *A. flavus*, and *E. purpurascens* under SSF with sawdust and wheat bran (1.5:1.5) for a higher yield. The three co-cultured organisms produced a higher activity of xylanases when compared to the activity observed under single culture. The three co-cultured organisms increased the enzyme activity by 55.41%, 63.31%, and 156.22% when compared to *C. sphaerospermum*, *A. flavus*, and *E. purpurascens* respectively when grown individually. The synergic interactions between these three strains aided the production of xylanases [54]. According to the study reported by Lio and Wang [10], *Trichoderma reesei* and *Phanerochaete chrysosporium* were inoculated and incubated for 36 h, followed by *Aspergillus oryzae* for an additional 108 h. This inoculation scheme resulted in the highest xylanase activity of 399.2 IU/g compared to other fungus combinations using distiller's dried grains with solubles (DDGS) as a substrate under SSF [10].

### Purification

Purification is a crucial step in product recovery and the process starts with the separation of cells from the fermentation broth to recover desired metabolites. The purification step plays a major role in the yield of the metabolite and the separation of byproducts. Depending on the nature and the purity of the metabolite produced by an organism, the



**Table 3** Process optimization conditions used for microbial co-culture under solid-state fermentation

Organisms	Substrate	Product	Optimization technique	Fermentation conditions			Final yield		References
				pH	Temperature	Incubation period	Inoculum volume	Moisture content	
<i>Bacillus cereus</i> and <i>Bacillus thuringiensis</i>	Wheat bran	$\alpha$ -amylase	OFAT	7.0	37 °C	48 h	4 mL / 50 mL	1:1 (w/v)	44 U/mL/min [1]
<i>Aspergillus niger</i> GSJ and <i>Trichoderma reesei</i>	Granulated corn cob and Bermuda grass	FPase Xylanase	OFAT	5.5	50 °C	16 h 12 h	10 <sup>7</sup> conidia (g dry forage mixture) <sup>-1</sup>	80% (w/v)	141.5 ± 12.8 U g <sup>-1</sup> [56] 505.2 ± 39.8 U g <sup>-1</sup>
<i>Trametes hirsuta</i> and <i>Phanerochaete</i> sp.	Pulse husk, wheat bran, and mustard peel (1.75:1.75:1.5)	Pectinase	EVOP	4.5	34 °C	7 days	1.8 × 10 <sup>8</sup> spores/mL	1:2 (w/v)	2176.5 ± 179.8 U g <sup>-1</sup> [57] 247 U/gds
<i>Trichoderma reesei</i> and <i>Phanerochaete chrysosporium</i> + <i>Aspergillus oryzae</i>	Soybean fiber	Laccase Xylanase	NS	5.0	30 °C	36 h, 108 h	NS	75%	250 U/gds [10] 757.4 IU/g
<i>Trichoderma reesei</i> and <i>Phanerochaete chrysosporium</i> + <i>Aspergillus oryzae</i>	Distiller's dried grains with solubles (DDGS)	Cellulase Xylanase	NS					85%	3.2 IU/g [10] 399.2 IU/g
<i>Phanerochaete chrysosporium</i> and <i>Schizophyllum commune</i>	Papaya peels, pineapple peels, and banana peels	Cellulase	OFAT	NS	32 °C	6 days	1 × 10 <sup>8</sup> spores/mL	80% humidity	40 IU/gds [55]
<i>Cladosporium sphaerospermum</i> , <i>Aspergillus flavus</i> and <i>Epicoccum Purpurascens</i>	Sawdust and wheat bran (1.5:1.5)	Amylase Xylanase	OFAT	NS	32 °C	7 days	1 mL/15 mL	NS	395.6 IU/gds [54] 29.09 U/g
<i>Penicillium citrinum</i> NCIM 768 and <i>Trichoderma reesei</i> NCIM 1186	Wheat bran	Cellulase	NS	5.0	30 °C	6 days	10 <sup>6</sup> spores	70% (w/v)	6.71 FPU/gds [59]
<i>Bacillus Cereus</i> and <i>Trichoderma</i> sp.	Defatted palm kernel cake	Cellulase	OFAT	NS	30 °C	5 days	12 × 10 <sup>6</sup> conidia/mL	NS	1.856 FPU/mL [60]

Table 3 (continued)

Organisms	Substrate	Product	Optimization technique	Fermentation conditions				Final yield	References
				pH	Temperature	Incubation period	Inoculum volume		
<i>Trichoderma reesei</i> and <i>Aspergillus fumigatus</i>	<i>Dioscorea zingiberensis</i> (DZW)	Diosgenin	OFAT	5.8	35 °C	144 h	7.5 × 10 <sup>6</sup> T. <i>reesei</i> spores/g DZW and 1.5 × 10 <sup>7</sup> A. <i>fumigatus</i> spores/g DZW	68.2 μmol/g	[90]
<i>Rhizopus stolonifera</i> and <i>Aspergillus niger</i>	Orange peel	Citric acid	OFAT	5.5	30 °C	48 h	6 mL	7651 μg/mL	[17]
<i>Trichoderma sp.</i> and <i>Saccharomyces cerevisiae</i>	sweet potato ( <i>Ipomoea batatas L.</i> ) flour	Bioethanol	OFAT	5.0	30 °C	72 h	10%	172 g/kg substrate	[77]

NS not specified

various options available for separation include filtration, centrifugation, precipitation, dialysis techniques [81]. Ultra-filtration, chromatography, and electrophoresis techniques can be employed for highly purified products [14, 82].

Ammonium sulfate precipitation is considered a crude separation step. It is generally used in the initial stages of purification, followed by dialysis and a combination of chromatographic steps [81, 83] as mentioned in Fig. 3 and Table 4. The dialysis step is employed to purify the crude metabolite. Usually, this part of downstream processing operation includes a series of sequential chromatography steps, but several pre-treatment methods (e.g., membrane filtration, precipitation, aqueous two-phase partitioning) can also be used either alone or in combination to improve the performance of purification. Chromatography is being widely used in industries as it has proved to be very efficient due to its high-resolution capacity. Size exclusion, anion, and cation exchange chromatography are the various chromatographic techniques used to further purify the product obtained. Several purification steps can be capped to three to maximize the purity and yield of the products [84].

## Applications

An extensive range of technological operations is observed in the co-culture systems in numerous industries such as food, textile, pharmaceutical, polymer, biofuel, paper, and pulp industries. Various applications of the same are mentioned in Table 5. A mixture of co-culturally produced hydrolytic enzymes such as xylanase, amylase, and cellulase is useful for animal feed improvement as it breaks down the fibrous substrates and improves its digestibility, especially in non-ruminant animals [10, 56, 85]. Cellulase and hemicellulase enzyme mixture inclusion aids in the utilization of fibrous cellulosic part of feed resulting in increased starch saccharification to sugars and their successive fermentation to produce products like ethanol [86]. The enzyme tannase is mainly used for the synthesis of an antibacterial and antifolate drug trimethoprim owing to the enzymatic capability by which it hydrolysis gallotannin to gallic acid [87]. β-mannanases inclusion in the manufacturing of chocolate, instant coffee, and cocoa liquor aids by decreasing the viscosity of extracts thereby lowering drying costs [88]. Sustainable processes like the development of high-value compounds through biomass transformation and the development of biorefinery platforms are possible due to the technology of co-culture systems [89].

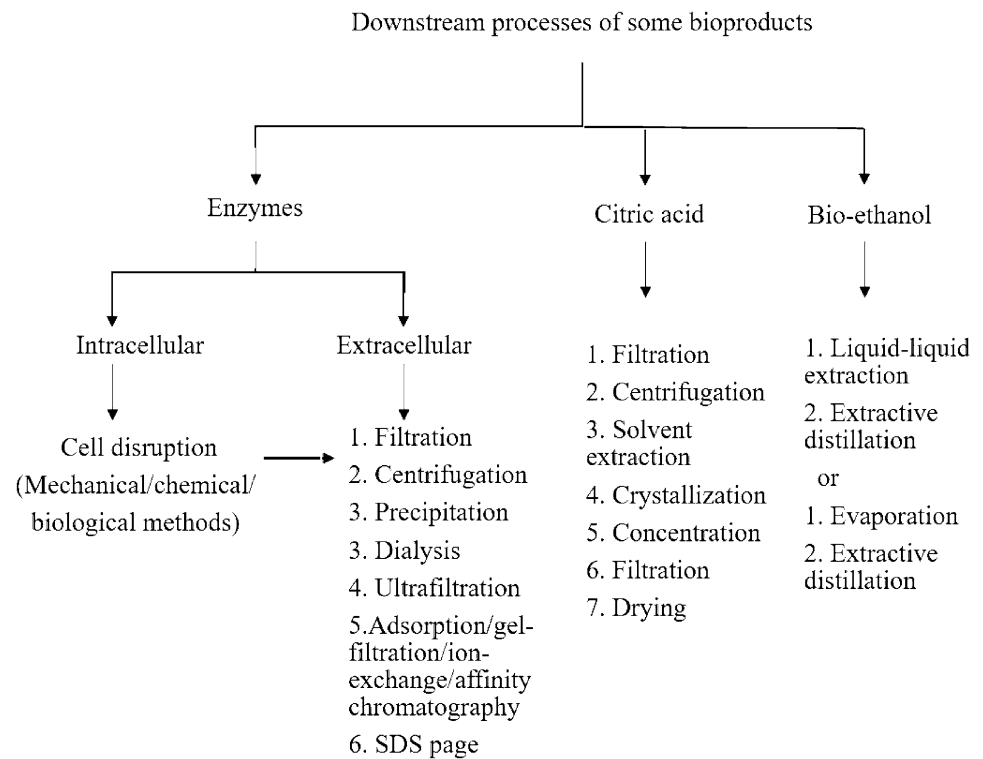
## Challenges in Microbial Co-culture Method

Practical aspects should be considered systematically while depicting the natural phenomenon of the co-culture system in various bio-manufacturing industries. The properties of

the microorganism used in the pilot and industrial-scale bioreactors depend on its oxygen requirement, its resistance to mechanical steering, and the temperature range. Contamination is one of the major challenges faced while co-culturing microorganisms [30, 39]. While selecting the organisms, it is preferred that organisms that show maximum synergism

among them should be selected and worked upon. If there is antagonism, one organism could suppress or interfere with the normal functioning of the other organism. Culturing several species together sometimes results in unstable systems. This happens due to multiple pathways of each organism which makes it difficult to analyze, monitor, and

**Fig. 3** Downstream processes of some bioproducts [42–44]



**Table 4** Techniques used for purification of enzymes produced by microbial co-culture under SSF

Product	Purification methods	Purification fold	References
Tannase	Ammonium sulfate precipitation, DEAE Sephadex A-50 column chromatography	1.33	[95]
Protease	Ammonium sulfate precipitation, centrifugation	3.3	[96]
Pectinase	Centrifugation, ammonium sulfate precipitation, lyophilization, gel filtration column chromatography (2 × 20 cm)	5.59	[97]
Galacto oligosaccharides	Simulated moving bed (SMB) chromatography, like selective adsorption in activated carbon, selective precipitation with ethanol	NS	[98]
Xylanase	Anion exchange chromatography, SDS page	2.35	[99]
Lacasse	80% ammonium sulphate fractionation, dialysis, DEAE liquid column chromatography, SDS page	1.23	[100]
Inulinase	Ammonium sulfate precipitation, ion-exchange chromatography	NS	[101]
Amylase	Ammonium sulfate precipitation, centrifugation, dialysis, SDS page	1.41	[102]
Cellulase	Ammonium sulfate precipitation, DEAE-cellulose column chromatography, CM-cellulose column chromatography	9.7	[103]
β-mannanase	Ultrafiltration, fast protein liquid chromatography (FPLC), concentration, centrifugation, Sephacryl S-200HR (16/60) column, SDS page	10.3	[104]
β-glucosidase	Ammonium sulfate precipitation, dialysis, centrifugation, gel filtration on Sephadex G-75	86	[105]

NS not specified

interpret the results. The microbial growth curve should be observed, and measures should be taken that one organism does not outgrow the other [16]. Even slight variations in the co-culturing system destabilize their synergistic balance and modify the behavior of the organisms which eventually leads to loss of product. Identifying the metabolites, proteins, and peptides released by all the organisms within a co-culture helps to understand the population dynamics and underlying communication to develop a successful industrial consortium [67].

## Future Scope

Co-culturing of microorganisms can be used to study both synthetic as well as natural cell–cell interactions. By understanding these interactions, new pathways for organisms that are difficult to culture can be re-engineered [8]. Strategies for microbial strain improvement can prove beneficial to promote the utilization of complex substrates, their efficient assimilation, and to minimize the formation of undesired by-products of the fermentation process. In addition, recombinant or mutated strains can be made to have increased tolerance to environmental variations. Mutant microbial strains may also be manipulated to have better synergy with each other. Co-culturing these will in turn provide improved product yields. Epigenetics modifications can be done to modulate DNA or histones for initiating the transcription of the silent genes. DNA methyltransferase inhibitors or

histone deacetylase are epigenetic modifiers that are used to treat microorganisms. Accumulation of new compounds is possible due to this modulation [68]. Industrial products like pharmaceutical drug precursors, biofuels, amino acids, vitamins, valuable pigments, and antibiotics can also be obtained by co-culturing microorganisms [9, 90]. As stated in the section “[Fermentation process](#)”, there are no studies reported on bioreactors for SSF using co-culture systems. Research on the design and operation of bioreactors for SSF with co-culture offers an opportunity for future studies.

## Conclusion

Co-cultured organisms have proved to be beneficial over mono cultured organisms. Fungal co-cultures are more beneficial and hence widely used over bacterial co-cultures. An extensive range of fungal and bacterial organisms can be co-cultured under different conditions if they have good synergy between them. The pharmaceutical, industrial, food, textile sectors are benefited from the products of co-cultured microorganisms. As mentioned above, not only enzymes but also other products are being produced using co-culture through SSF such as citric acid, bio-butanol, and ethanol. Specific purification protocols are tailored to increase the yield and purity of the products obtained. The process conditions and protocols for a particular product are optimized based on the type of organism, substrate, and other process variables.

**Table 5** Applications of bioproducts in various industries produced under SSF using co-culture

Industry	Enzyme	Products	References
Food Industry	Lacasse and pectinase	Modify the colour and increase the yield of drinks like beer, wine	[106–108]
	Xylanase, amylase and cellulase	To improve animal feed digestibility	[10, 56, 86]
	Citric acid, lacasse and pectinase	To improve existing flavour and colour	[17]
	B-mannanases	Clarification of fruit juices and extraction of oils	[109]
	Cellulose and hemicellulose	Increased ethanol production	[86, 87]
	$\beta$ -mannanases	Production of chocolate, instant coffee and cocoa liquor	[89]
Pharmaceutical Industry	Tannase	Synthesis of an antifolate and antibacterial drug trimethoprim	[88]
	Diosgenin	Synthesis of oral contraceptives, sex hormones and other steroids	[90]
	$\beta$ -mannanases	Production of single-cell proteins	[90]
	Citric acid	To increase existing flavours	[17]
Textile Industry	Lacasse and pectinase	Finishing, washing off treatment, bio-sourcing, dyeing, bio bleaching and printing	[90, 110]
	B-mannanases	Facilitates bio-bleaching	[111]
	Xylanase and laccase	Total degradation of lignocellulose for its effective use	[2]
Biofuel Industry	Bioethanol and butanol	Both used as a green alternative to fossil fuels. Butanol is an exceptional fuel as it is miscible with diesel and gasoline fuel, has high calorific value, is less miscible with water and has a lower vapor pressure	[18, 112–114]
Polymer Industry	Lacasse and pectinase	Generation of monomers, cross-linking of the monomers and synthesis of biopolymers	[115, 116]
Wastewater Treatment	Lacasse	Biodegradation as well as detoxification of the pollutant	[94]

Various types of bioreactors are used for SSF depending on the nature of the organisms and products. The bioreactors are each designed and operated differently for each process. Apart from the generally used bioreactors, some uncommon bioreactors such as zymotis, fluidized beds, and spouted beds are reviewed. Bioreactors assist in diversifying the protocol which can result in increased production and less wastage.

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**Data availability** The datasets used and/or analyzed during the current study are available from the first author on reasonable request.

## Declarations

**Conflict of interest** The authors declare that they have no competing interests.

**Ethical approval** Not applicable.

**Consent to participate** Not applicable.

**Consent for publication** Not applicable.

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