

## A lumped parameter model for kidney pressure during stone removal

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In this paper, we consider a lumped-parameter model to predict renal pressures and flow rate during a minimally invasive surgery for kidney stone removal, ureteroscopy. A ureteroscope is an endoscope designed to work within the ureter and kidney, and consists of a long shaft containing a narrow, cylindrical pipe, the *working channel*. Fluid flows through the working channel into the kidney. A second pipe, the *access sheath*, surrounds the shaft of the scope, allowing fluid to flow back out of the urinary system. We modify and extend a previously developed model (Oratis et al., 2018) through the use of an exponential, instead of linear, constitutive law for kidney compliance, and by exploring the effects of variable flow resistance, dependent on the presence of auxiliary *working tools* in the working channel and the cross-sectional shapes of the tools, working channel, scope shaft, and access sheath. We motivate the chosen function for kidney compliance, and validate the model predictions, with *ex-vivo* experimental data. Although the predicted and measured flow rates agree, we find some disagreement between theory and experiment for kidney pressure. We hypothesise that this is caused by spatial pressure variation in the renal pelvis that is unaccounted for in the lumped parameter model. We support this hypothesis through numerical simulations of the steady Navier–Stokes equations in a simplified geometry. We also determine the optimal cross-sectional shapes for the scope and access sheath (for fixed areas) to minimise kidney pressure and maximise flow rate.

*Keywords:* urology, pipe network modelling, ex-vivo experiments, kidney compliance

### 1. Introduction

Solid calcifications within the urinary tract have affected mankind for thousands of years, with the oldest known urinary stone discovered in the bladder of an Egyptian mummy (Shattock, 1905). Left untreated, large stones may lead to infection and eventual loss of kidney function, and can, on occasion, be life threatening (Kum et al., 2016). A common method for the destruction and removal of kidney stones is

provided by flexible ureterorenoscopy. The procedure is performed by passing auxiliary working tools through the working channel of a ureteroscope; an endoscope designed to visualise and work within the ureter and kidney (Figure 1). Via a miniscule light and a camera on the scope tip, the patient's ureter and kidney are viewed by a urologist.

A method for kidney stone destruction is laser lithotripsy, where a long, thin laser fibre is passed through the ureteroscope, and uses shock waves to fragment stones. The resulting particles and debris can then obstruct the field-of-view for the operating surgeon. To mitigate this, a saline solution flows from a bag above the patient, through a long, thin channel within the scope (the working channel), and out of the scope tip. To exit the body, the fluid flows back in the opposite direction along the outside of the scope shaft. There is only a narrow gap between the scope and the ureteral wall, and if too much saline is delivered, overfilling of the kidney (and hence elevated renal pressures) may occur. High kidney pressures during ureteroscopy have been linked to post-operative complications, such as sepsis (Wilson & Preminger, 1990). Thus, to prevent kidney pressures from rising unduly, many urologists insert the scope through a ureteral access sheath; a hollow cylinder that surrounds the scope, temporarily widening the ureter to allow irrigation fluid to flow more freely back out of the kidney alongside the shaft of the scope (Figure 1). If more flow is required in a procedural setting to clear the area in front of the camera, typical practice is to increase the inlet pressure by raising or pressurising the bag of saline solution in an *ad hoc* manner. It is clear that flow resistance, both through the working channel and back through the sheath, will play a crucial role in determining whether kidney pressures will remain below a physically safe threshold. Resistance to flow can be altered through modifications to the geometry of the surgical tools; in particular, the cross-sectional shapes of the working tools, channel, scope shaft, and ureteral access sheaths (Williams et al., 2019a). Hence, understanding the relationships between the size and shape of ureteroscopic instruments, inlet pressure, flow rate, and pressure within the kidney, have enormous potential to enhance surgical efficiency and safety as well as to revolutionise ureteroscope design.

Recent efforts have examined the effects of geometric parameters of the ureteroscope and working tools on components of irrigation flow with a mathematical modelling approach (Williams et al., 2019b). Flow through an isolated ureteroscope has been shown, through asymptotic analysis on the small aspect ratio of the working channel, and comparison with bench-top experiments, to obey a Poiseuille law for flow through a cylindrical pipe. Similarly, flow through a working channel with a working tool, or back through an access sheath, can be modelled as flow through a pipe containing a solid, co-axial cylindrical rod. Flow for a fixed pressure drop through these configurations is lowest when the solid rod is in the centre, and increases monotonically with rod proximity to the edge of the bounding channel. This highlights the importance of cross-sectional geometry on viscous resistance, motivating the discussion of optimally shaped elliptical working tool/channel (or similarly scope shaft/access sheath) configurations, which have been theorised to further decrease viscous resistance when compared to circles of equal cross-sectional area (Williams et al., 2019a).

In this article, we will extend the previous work on component modelling of ureteroscope irrigation and the effects of viscous resistance, to consider a lumped-parameter systems model, connecting flow through the working channel and back through the access sheath. Through this, we can understand how geometric changes to particular components of the irrigation system will affect flow rate and kidney pressure. Fluid is driven through the working channel via a prescribed inlet pressure, and by modelling the kidney as a compliant body, and equating fluxes in through the scope and back out through the sheath, a lumped-parameter model for flow rate and kidney pressure as functions of time can be derived (Oratis et al., 2018). The resulting ordinary differential equation depends on the ratio between the viscous resistances through the working channel and back through the sheath, and the relationship

between changes in kidney pressure and volume (compliance). In Oratis et al. (2018), flow through the working channel and access sheath were modelled as Poiseuille flow through an unobstructed pipe and a concentric annular pipe of circular cross-sections, respectively. The importance of low outflow resistance to maintain low intrarenal pressures was discussed in Oratis et al. (2018) only within the context of increasing access sheath size or intermittently withdrawing the scope. We will extend this work by varying the inflow and outflow resistances to represent: the addition of working tools, a non-concentric scope shaft, and modifying the cross-sectional shapes of the scope shaft and access sheath.

Additionally, in Oratis et al. (2018), the kidney is modelled as linearly elastic with constant renal pelvis stiffness,  $K$ . However, biological tissue is typically shown to be poorly compliant, represented by an increase in the slope of the stress-strain curve at higher strains (Holzapfel, 2001; Chagnon et al., 2018). This is often accounted for by constitutive laws that include exponential terms, ensuring that tissue stiffens as it stretches. An experimental study (Cruces et al., 2014) performed on porcine kidneys, measuring pressure within the parenchyma in response to fluid volume injected into the kidney also suggests an exponential relationship between kidney pressure and volume. We will validate the use of an exponential function for the kidney compliance with the use of *ex-vivo* experimental data, and will consider its effect on the predictions of the theoretical model.

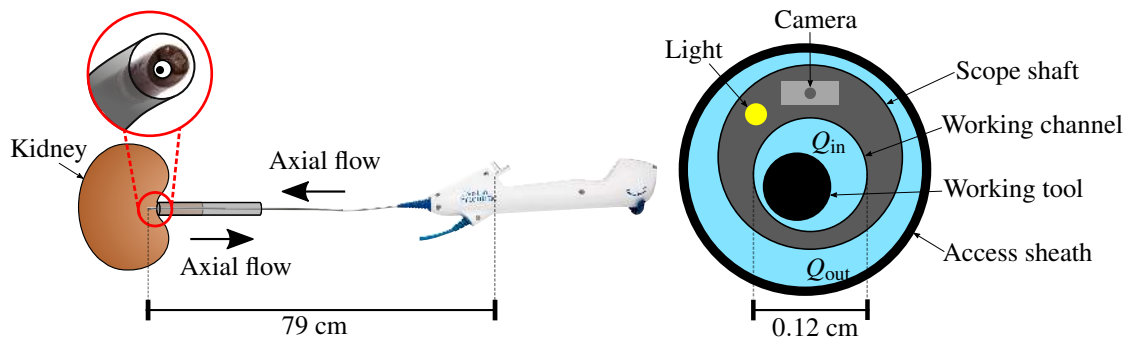


FIG. 1: A photograph of a Boston Scientific ureteroscope (left) with the tip of the scope circled and a zoomed-in schematic provided of the scope tip (right). The scope lies within an access sheath, and a working tool sits inside the working channel. A camera and a light are embedded in the scope wall. Dimensions of the scope shaft and working channel are labelled. The blue regions denote areas through which saline passes;  $Q_{in}$  flows into the kidney and  $Q_{out}$  back out through the access sheath.

In Section 2 we describe the *ex-vivo* experimental set-up and procedure. In Section 3 we derive a lumped-parameter model for kidney pressure and flow rate, considering an exponential renal stiffness, and present the analytical solution. The results in Section 4 are split into three main components. Firstly, in Section 4.1, we validate the use of an exponential renal compliance by fitting this constitutive law to the experimental data, and discuss its implications. In Section 4.2, we test the steady-state model predictions for flow rate and kidney pressure against the experimental data. This motivates a discussion of the spatial variance of kidney pressure, that is not accounted for in the lumped parameter model. Finally, in Section 4.3, we theorise on the addition of working tools in the working channel, and the effects of changing the geometries of the access sheath and scope shaft on flow rate and kidney pressure.

## 2. *Ex-vivo* experiments and data extraction

A suite of *ex-vivo* experiments were performed on porcine kidneys, with a laboratory configuration shown in Figure 2a. The experiments were conducted at room temperature and within several hours of harvesting the kidneys. Irrigation fluid flowed from a saline bag 60 cm above the height of the kidney, when measured from the base of the bag. A pressure cuff surrounded the bag, allowing the inlet pressure to be increased above hydrostatic, and a pressure probe was placed at the inlet to the scope. A 36 cm long 11/13 F Navigator access sheath was inserted through the ureter, with a pressure probe passed between the ureter and the wall of the sheath. A LithoVue ureteroscope was placed within the sheath, and the tips of the sheath, scope, and pressure probe were all within the renal pelvis. The kidney and a dish to collect the outflow from the sheath were on OHAUS Traveler mass balances, and FISO Fiber Optic Pressure Sensors recorded the inlet and intrarenal pressures. The pressure sensors were calibrated to atmospheric pressure.

Inflations of the pressure cuff surrounding the irrigation bag enabled control of the inlet pressure, and the resulting inlet pressure, kidney mass, kidney pressure, and outflow mass were all measured over time. Pressure data was collected at 8 ms intervals, and mass data collected at approximately 500 ms intervals. Experiments were performed on three different kidneys, which we refer to as kidneys A, B and C. Multiple experiments were performed in succession – without adjusting the positions of the experiment equipment – on each of the three kidneys. The kidneys were drained prior to the experiments, so the initial renal pressure before the insertion of irrigation fluid was approximately atmospheric. The inlet pressure was increased over time in two ways: I) continuously, and II) step-wise, maintaining the pressure of the cuff for approximately 30 seconds before further inflation. Examples of the resulting inlet pressure over time for data sets I and II are shown in Figure 2b and 2c, respectively. The number of data sets I and II collected from each kidney are summarised in Table 1, and more details on the data analysis is provided in Appendix A.

	A	B	C
Data set I	1	0	3
Data set II	4	2	1

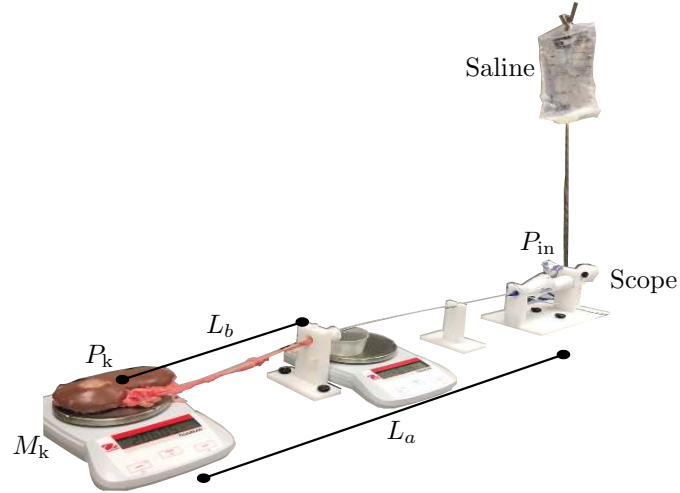
Table 1: Number of experiment runs on each kidney, for each type of data set.

The two data sets enable us to analyse two distinctly different features: (i) the rise of pressure to steady state, and (ii) flow and pressure conditions at steady state for varying inlet pressure. Since data set I consisted of a continuous rise in pressure, this data set was well suited for evaluating the pressure rise and estimating kidney compliance, by extracting a continuous curve (parametrised by time) relating fluid mass and pressure within the kidney. In data set II, since the inlet pressure was held constant for several seconds at each incremental value, this enabled the system to reach steady state flow (flow into the kidney equalling flow out of the kidney). Thus, this data set was used to study the steady state conditions, by extracting five-seconds of data from each interval of constant inlet pressure, and using this to determine the steady-state kidney pressure and flow rate as functions of inlet pressure.<sup>1</sup>

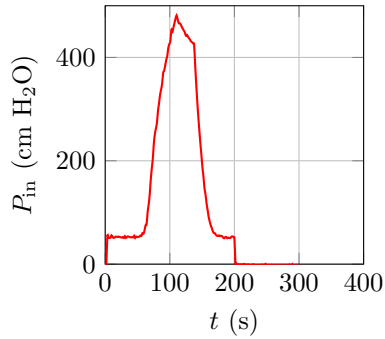
It is also important to note that the two regimes, (i) and (ii), are fundamentally separated in terms of

<sup>1</sup>Due to deflation of the pressure cuff, the inlet pressure slowly decreased at each ‘step’ (Figure A.7). However, the time-scale was sufficiently slow that the inlet pressure could be well-approximated as constant over each five-second interval.

(a) Experimental setup



(b) Data set I



(c) Data set II

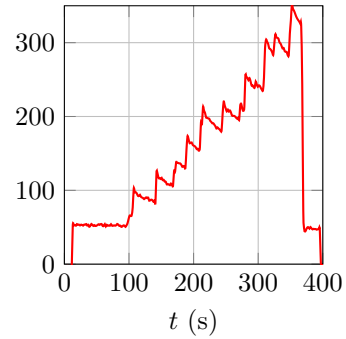


FIG. 2: Figure (a) shows a photograph of the experimental set-up, with measured variables labelled, along with the lengths of the scope and the access sheath. Figures (b) and (c) show examples of data collected from kidney A for data sets I and II, respectively.

the modelling. In particular, the steady state conditions are independent of the compliance, as we shall show below. Therefore, the compliance parameter fitting related to (i) is irrelevant to analysis of (ii).

Details on calculating error bars for all data figures are provided in Section A.4.

### 3. Theoretical formulation

We consider irrigation flow in an idealised setting, replicating the laboratory setup in Figure 2a. A scope of length  $L_a$  lies horizontally, with fluid of density  $\rho$  and viscosity  $\mu$  entering the working channel of radius  $a$  at fixed pressure  $P_{in}$ . The tip of the scope is inside the kidney which contains irrigation fluid of mass  $M_k$ , volume  $V_k$ , and pressure  $P_k$ , all functions of time. An access sheath of radius  $b$  and length

$L_b$  surrounds the scope, with one end within the kidney, and the other exposed to atmospheric pressure which, we take to be zero. We term the fluid volumetric flux into the kidney as  $Q_{\text{in}}$  and back out through the sheath as  $Q_{\text{out}}$ .

### 3.1 Governing equations

Conservation of mass provides

$$\frac{dM_k}{dt} = \rho(Q_{\text{in}} - Q_{\text{out}}). \quad (3.1)$$

The irrigation fluid is taken to be incompressible, and hence increases in fluid mass within the kidney and the volume of fluid within the kidney are correlated directly

$$M_k = \rho V_k. \quad (3.2)$$

Thus, to model kidney pressure as a function of time with equation (3.1), it remains to determine the kidney compliance: a constitutive relationship between changes in pressure and changes in volume. Defining  $P_k$  as the change in kidney pressure from atmospheric, we take

$$P_k = P^*(\exp(CV_k) - 1), \quad (3.3)$$

where  $C$  is a constant with units of inverse volume and  $P^*$  is a characteristic pressure scaling. Both  $C$  and  $P^*$  will be determined through a fit to experimental data in Section 4.1. The use of equation (3.3) is motivated by Cruces et al. (2014), Holzapfel (2001), and Chagnon et al. (2018), and has also been seen to provide a good approximation for bladder filling (Griffiths, 1980). Differentiating equation (3.3) with respect to time we obtain

$$\frac{dP_k}{dt} = P^*C \exp(CV_k) \frac{dV_k}{dt}, \quad (3.4)$$

and using equations (3.2) and (3.1) we obtain the following nonlinear differential equation

$$\frac{dP_k}{dt} = C(P^* + P_k)(Q_{\text{in}} - Q_{\text{out}}). \quad (3.5)$$

As an initial condition for equation (3.5) we take

$$P_k(0) = 0. \quad (3.6)$$

### 3.2 Viscous resistance

We consider steady, unidirectional flows through the working channel and access sheath. The assumption of unidirectional flow through the working channel has been previously validated through comparison with bench-top experiments (Williams et al., 2019b). Steady flow can be justified from the full Navier-Stokes equations and incompressibility condition by considering flow through a working channel (with a similar discussion for flow through the access sheath). Defining the radius-to-length ratio of the channel as  $\varepsilon = a/L_a$  and the Reynolds number of the flow as  $\text{Re} = QL_a\rho/\mu\pi a^2$  for a typical flow rate  $Q = \mathcal{O}(10^0)$  cm<sup>3</sup>/s, the key parameters governing the behaviour of the fluid are  $\varepsilon^2\text{Re}$  and  $a^2\rho/\mu T$ , where  $T$  is a chosen time-scale. Here, the relevant time-scale for equation (3.5) is the rise-time for kidney pressure (or flow rate) to adjust to steady-state after changing the inlet pressure. This can be estimated from the *ex-vivo* data to be  $T = \mathcal{O}(10^1)$  s. With values for  $a$ ,  $L_a$ ,  $\rho$ , and  $\mu$  taken from Table

2,  $\varepsilon^2 = \mathcal{O}(10^{-6})$ ,  $\varepsilon^2 \text{Re} = \mathcal{O}(10^{-1})$ , and  $a^2 \rho / \mu T = \mathcal{O}(10^{-2})$ . Thus, inertial and time-dependent effects within the fluid can be neglected, and we model flow through the working channel and back through the access sheath as steady, unidirectional flow through pipes of arbitrary cross-sections.

These are determined as solutions to

$$\nabla^2 w = \frac{1}{\mu} \frac{dp}{dz}, \quad (3.7)$$

where  $w$  is the axial velocity as a function of cross-sectional coordinates, and  $dp/dz$  is a constant pressure gradient along the length of the pipe (Lamb, 1895). Flow rate is obtained by integrating the solution to equation (3.7) for  $w$  over an arbitrary cross-section of the pipe to obtain

$$Q = \frac{1}{\mu} \frac{dp}{dz} \frac{1}{R}, \quad (3.8)$$

where  $R$  characterises the viscous resistance to the geometry of the pipe cross-section. Modelling the working channel as a hollow cylinder of radius  $a$ ,

$$Q_{\text{in}} = \frac{1}{\mu} \left( \frac{P_{\text{in}} - P_{\text{k}}}{L_a} \right) \frac{1}{R_{\text{in}}}, \quad R_{\text{in}} = 8/\pi a^4. \quad (3.9)$$

Assuming that the scope and the sheath are coaxial (although not necessarily concentric), flow back through the access sheath is

$$Q_{\text{out}} = \frac{1}{\mu} \frac{P_{\text{k}}}{L_b} \frac{1}{R_{\text{out}}}, \quad (3.10)$$

where  $R_{\text{out}}$  can be obtained for circular cylinders as a function of scope position from the analytical solution for flow through an offset annular domain (Heyda, 1959).  $R_{\text{out}}$  decreases monotonically as the scope is placed closer to the edge of the sheath. In practice, the position of the scope shaft within the sheath is unknown, so we allow  $R_{\text{out}}$  to take any value between its minimum (in the centre of the sheath) and its maximum (at the edge of the sheath).

### 3.3 Dimensionless model

Combining equations (3.5), (3.9), and (3.10) we obtain

$$\frac{dP_{\text{k}}}{dt} = (C/\mu)(P^* + P_{\text{k}}) \left( \frac{P_{\text{in}} - P_{\text{k}}}{L_a R_{\text{in}}} - \frac{P_{\text{k}}}{L_b R_{\text{out}}} \right). \quad (3.11)$$

We now make the following non-dimensionalisations

$$P_{\text{k}} = P^* \hat{P}_{\text{k}}, \quad t = (L_a R_{\text{in}} \mu / C P^*) \hat{t}, \quad (3.12)$$

where hats denote dimensionless variables. The dimensionless form of equation (3.11) is then

$$\frac{d\hat{P}_{\text{k}}}{d\hat{t}} = (1 + \hat{P}_{\text{k}})(\hat{P}_{\text{in}} - (1 + \mathcal{R})\hat{P}_{\text{k}}), \quad (3.13)$$

where we define the dimensionless parameters

$$\hat{P}_{\text{in}} = P_{\text{in}}/P^*, \quad \mathcal{R} = (L_a R_{\text{in}})/(L_b R_{\text{out}}). \quad (3.14)$$

$\hat{P}_{\text{in}}$  is the dimensionless inlet pressure and  $\mathcal{R}$  is the ratio of resistance in through the working channel to resistance out through the access sheath. The dimensionless initial condition, equation (3.6) is

$$\hat{P}_{\text{k}}(0) = 0. \quad (3.15)$$

### 3.4 Analytical solution

Equation (3.13) with initial condition (3.15) can be solved by separating variables to obtain the analytical solution

$$\hat{P}_k = \frac{(e^{\tau t} - 1)\hat{P}_{in}}{\hat{P}_{in} + e^{\tau t}(1 + \mathcal{R})}, \quad (3.16)$$

where  $\tau = 1 + \hat{P}_{in} + \mathcal{R}$ . The steady-state intrarenal pressure can be easily found by setting the time derivative in equation (3.13) to zero. We note the presence of  $(1 + \hat{P}_k)$  in equation (3.13) is due to the chosen exponential function for kidney compliance,  $dP_k/dV_k = P_k + P^*$ , equation (3.3). Hence we can exclude the non-physical steady-state solution  $\hat{P}_k = -1$  which corresponds to zero compliance. The relevant steady-state solution is thus

$$\hat{P}_k^{SS} = \frac{\hat{P}_{in}}{1 + \mathcal{R}}. \quad (3.17)$$

If  $\mathcal{R} \ll 1$ , and hence resistance through the sheath dominates, we see from equation (3.17) that  $\hat{P}_{SS} \approx \hat{P}_{in}$ . Conversely if  $\mathcal{R} \gg 1$ , and there is negligible resistance through the sheath,  $\hat{P}_{SS} \approx 0$ . We note that the steady state is not affected by the inclusion of a nonlinear kidney compliance, equation (3.3), and thus the parameters  $C$  and  $P^*$  determine only the time required to reach equilibrium pressure. The steady-state will be reached when  $Q_{in} = Q_{out} = Q^{SS}$ , and the dimensional value of the steady-state flow rate can be immediately determined from equation (3.17) and one of either (3.9) or (3.10) after redimensionalising and is

$$Q^{SS} = \frac{1}{\mu} \left( \frac{P_{in}}{L_a R_{in} + L_b R_{out}} \right). \quad (3.18)$$

## 4. Results

The parameters used to validate the model are taken from the experimental set-up and are summarised in Table 2.

	Symbol	Value	Unit
Working channel radius	$a$	$6.00 \times 10^{-2}$	cm
Scope shaft radius		$1.58 \times 10^{-1}$	cm
Access sheath radius	$b$	$1.93 \times 10^{-1}$	cm
Working channel length	$L_a$	$7.90 \times 10^1$	cm
Access sheath length	$L_b$	$3.60 \times 10^1$	cm
Fluid density	$\rho$	$1.00 \times 10^0$	g/cm <sup>3</sup>
Fluid viscosity	$\mu$	$1.00 \times 10^{-2}$	g/cm s

Table 2: Experimental parameters.

### 4.1 Estimating compliance (data set I)

We validate the use of an exponential compliance (equation (3.3)) in Figure 3a, by demonstrating a superior fit with experimental data (solid red line) when compared to a linear fit (dashed green line). Here, two data sets were chosen from kidney C, with the rationale behind their use detailed in Appendix A.2; we also note that using kidney A for the data fit results in very similar conclusions (see Appendix



A.9 in Appendix A.2). The exponential and linear relations are fitted to the mean of the experimental data. From the exponential fit, values are determined for

$$P^* = 5.24 \text{ cm H}_2\text{O}, \quad C = 0.43 \text{ mL}^{-1}. \quad (4.1a,b)$$

In Oratis et al. (2018), a linear renal stiffness was assumed with mean value  $K = 0.41 \text{ cm H}_2\text{O mL}^{-1}$ . This is plotted as the dashed blue line in Figure 3a. The shallow slope models the kidney as significantly more compliant than the data suggests; in fact, a linear fit to our data (dashed green line in Figure 3a) produces a renal stiffness values of  $K = 9.59 \text{ cm H}_2\text{O mL}^{-1}$ .

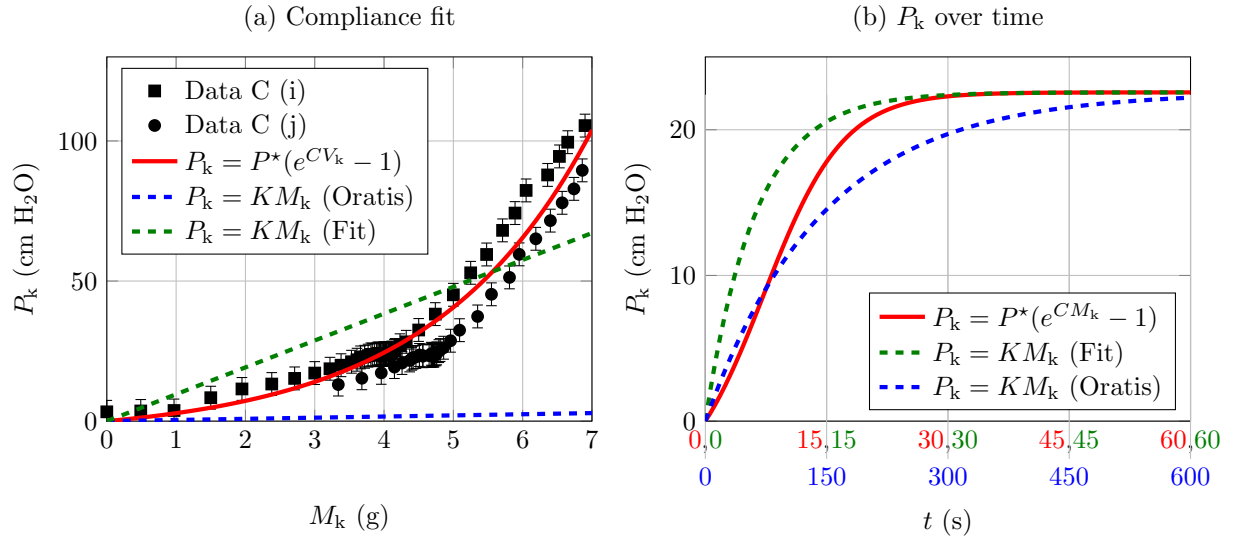


FIG. 3: (a) Data from kidney C runs (i) and (j) (see Appendix A). Exponential fit with  $P^* = 5.24 \text{ cm H}_2\text{O}$  and  $C = 0.43 \text{ mL}^{-1}$ . Linear model from Oratis et al. (2018),  $K = 0.41 \text{ cm H}_2\text{O/g}$ . (b) Comparison of theoretical kidney pressure  $P_k$  for the three different compliance models from (a). The different time-scales required to reach steady-state are indicated by the corresponding colored labels below the  $x$ -axis. The data in Figure 3b is for  $P_{in} = 60 \text{ cm H}_2\text{O}$ .

For the red line in Figure 3b, we consider a fixed inlet pressure of  $P_{in} = 60 \text{ cm H}_2\text{O}$ , and plot equation (3.16) using the best fit values of  $P^*$  and  $C$ , equations (4.1). The value for  $R_{out}$  is taken for a scope sitting concentrically in the access sheath. Using the same values for  $P_{in}$ ,  $R_{in}$ , and  $R_{out}$ , we plot the solution from Oratis et al. (2018) as the dashed blue line. We note that not only do the curves have slightly different shapes, but the time scales required to reach steady-state differ significantly. These are indicated by the corresponding colored labels below the  $x$ -axis. This result is intuitive from the two different compliance relationships, as a stiffer kidney will reach steady-state more quickly. Oratis et al. (2018) predicted a characteristic rise time of the order of several minutes, which does not correlate with experimental and clinical observations of  $\mathcal{O}(10^1 \text{ s})$ .

Using the stiffness value from the linear fit (dashed green line in Figure 3) we get the corresponding dashed green line in Figure 3b for kidney pressure over time. We see that the characteristic rise time is better captured by the fitted linear stiffness value compared to the dashed blue, although the shape of the curve still differs from the red curve corresponding to the exponential fit. In fact, as we are considering

kidney pressure  $P_k < 30$ , the fitted linear stiffness model estimates the material as stiffer than the more accurate exponential compliance, and thus the rise to steady-state is slightly shorter. For higher kidney pressures, the difference in slope will be more marked and the discrepancy between predicted  $P_k$  curves even more significant. It is also evident in Fig 3a that the exponential compliance fits the data much more closely, as a linear law cannot capture stiffening effects.

#### 4.2 Testing model predictions (data set II)

We now test the steady-state model predictions for kidney pressure and flow rate, equations (3.17) and (3.18), against the experimental data obtained from data set II. We note that there is no fitting required between the model and the data, as the steady state predictions are independent of kidney compliance. In Figure 4a, we plot the steady-state flow prediction, equation (3.18), along with experimental data, as functions of  $P_{in}$ . We consider both the minimum and maximum values for  $R_{out}$ , when the scope is centred within the sheath and fully offset, respectively (solid black lines), and shade the area between the two curves, corresponding to the predicted  $Q^{SS}$  over the range of feasible  $R_{out}$  values. The experimental flow-rate data for kidneys A, B, and C, estimated from the outflow mass values over time, is shown to lie within the predicted range (Figure 4a).

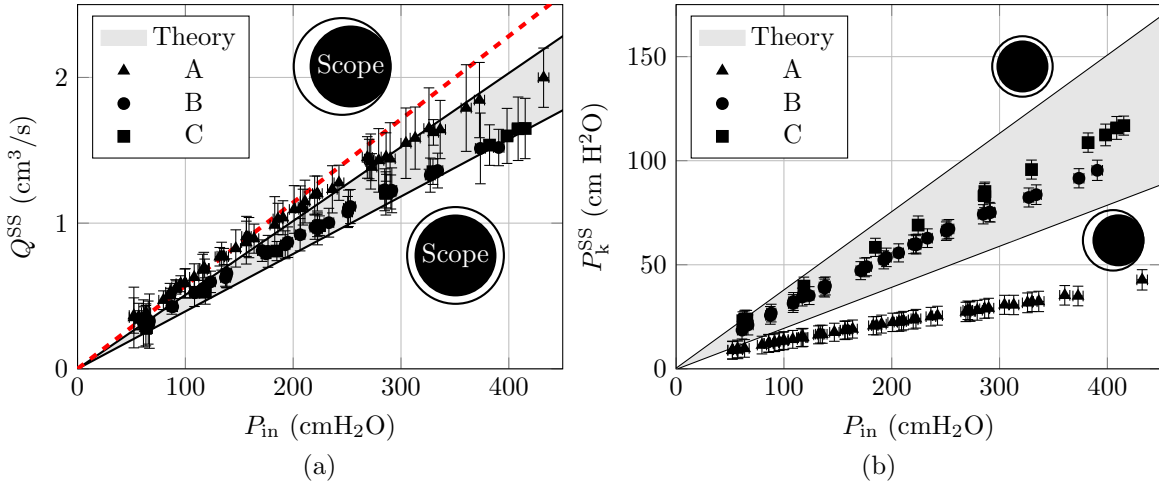


FIG. 4: (a) Equation (3.18) as the black lines compared to data collected from three different kidneys labelled A, B, and C. The dashed red line is the theoretical prediction for the optimal sheath/scope geometry (see Section 4.3) (b) Equation (3.17). The resistance ratio corresponding to a centred scope is  $\mathcal{R} = 1.7$ , and to an offset scope is  $\mathcal{R} = 4.1$ .

Accurately predicting the measured steady-state intrarenal pressure with equation (3.17) is more challenging, and in Figure 4b, we plot the wedge of predicted  $P_k^{SS}$ , and observe that the data from kidney A does not fall within the estimated range. One possible cause of the discrepancy is the position of the pressure probe within the kidney in the experiments; although it was placed proximal to the end of the scope, its position was likely to vary. Within the current modelling framework, we assume pressure within the kidney to be constant; i.e. the pressures at the exit of the working channel and entrance to the access sheath are identical, and equal to  $P_k$ . In actuality, there will be complex flow patterns and

pressure variation within the renal pelvis, dependent on flow rate, renal structure, and the ureteroscopic instruments in use. To test whether large variations in renal pressure are expected, and whether these can account for the observed discrepancy in Figure 4b, we solve the steady Navier–Stokes equations in the simplest representative geometry (see Appendix C for more details). We model the renal pelvis as a two-dimensional rectangular cavity, prescribing a Poiseuille inlet and zero-stress outlet boundary conditions. Defining the Reynolds number as  $Re = \rho Qa / (\mathcal{A}\mu)$ , where  $\mathcal{A} = \pi a^2$  is the cross-sectional area of the working channel, the relevant Reynolds numbers for simulations representing the flow rates in Figure 4a, and thus measured renal pressures in Figure 4b, range from  $Re = 0$  to  $Re = 1883$ . Results of the simulation for a representative flux  $Q = 1.4 \text{ cm}^3/\text{s}$  ( $Re = 1500$ ) are shown in Figures 5a,b. We consider the rectangular domain as a cross-sectional slice through the renal pelvis; thus, the half-width is taken to be the radius of the access sheath, and the radii of the sheath, scope, and working channel are taken from the experiments (Table 2) and indicated along the vertical axis of Figure 5a in cm units. The velocity streamlines in Figure 5a demonstrate the presence of multiple vortical structures, with the largest region of closed streamlines near the centre of the cavity. The corresponding pressure contour plot is shown in Figure 5b, and the colorbar indicates pressure in units of cm H<sub>2</sub>O. As flow is driven by pressure gradients, the same velocity solution will exist if an arbitrary constant is added to the pressure field; thus, we shift the pressure solution so the minimum value is at zero. Hence, Figure 5b indicates the pressure variation in the cavity, rather than absolute pressure values. We see that the pressure varies significantly on a spatial scale with a maximum variation of 90 cm H<sub>2</sub>O. In Figure 4b, the deviation between  $P_k$

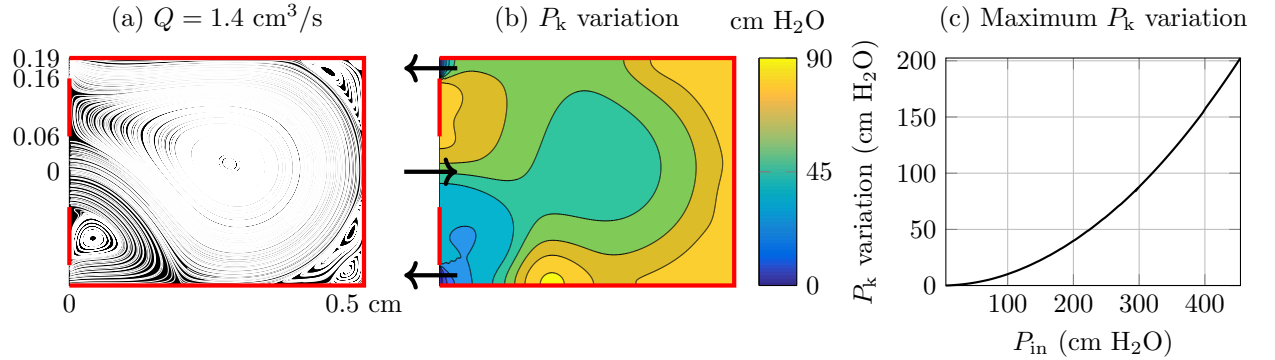


FIG. 5: Plot of predicted (a) streamlines and (b) pressure variation, within a rectangular cavity with prescribed parabolic inflow for  $Q = 1.4 \text{ cm}^3/\text{s}$  ( $Re = 1500$ ) and zero-stress outflow conditions. Cavity measurements labelled in (a) in cm units, corresponding to working channel, scope, and sheath dimensions. Pressure variation in (b) in cm H<sub>2</sub>O, shifted so the minimum pressure in the cavity is at zero. Figure (c) plots the difference between the minimum and maximum pressure values in the cavity, as a function of  $P_{in}$ . The relationship between  $P_{in}$  and  $Q$  prescribed for each simulation is determined from equation (3.18) with  $R_{out}$  taken as the value for a scope centred in the sheath.

for kidney A and the predicted values increases with  $P_{in}$ . To estimate  $P_{in}$  for a given simulation with a prescribed flow rate, we use the relationship for the steady-state flow rate, equation (3.18), assuming  $R_{out}$  for a scope centred within the access sheath. Using this approximation, the simulation in Figures 4a,b corresponds to  $P_{in} = 276 \text{ cm H}_2\text{O}$ . We can then plot the maximum pressure variation (difference between maximum and minimum pressures in the cavity) as a function of  $P_{in}$  (Figure 5c), and we see that the variation increases as a function of  $P_{in}$ . In a sense, this predicted variation corresponds to large

error bars on the  $P_k^{SS}$  data points in Figure 4b, explaining our inability to always accurately predict the pressure detected by the probe. Additionally, the pressure variation in the cavity increases with  $P_{in}$ , possibly explaining the increase in deviation between the experiments and prediction for kidney A in Figure 4b.

### 4.3 Effects of working tools and access sheath geometry

The presence of working tools, such as laser fibres or stone baskets within the working channel, can be included in equations (3.17) and (3.18) by increasing  $R_{in}$  according to the size, geometry, and placement of the working tool within the working channel. Hence, for fixed  $P_{in}$ , adding a working tool to the channel will decrease  $P_k^{SS}$  and hence  $Q^{SS}$ . Kidney pressure as a function of working tool radius (where we recall that the working channel has radius 0.06 cm) is plotted in Figure 6a as the dashed black line. As a minimum flow rate is often required to maintain a clear view-field during ureteroscopic surgery, the reduction in flow may motivate an increase in inlet pressure to maintain flow and subsequent visualisation. From equation (3.18), the inlet pressure required to maintain the steady-state flow rate at  $Q^{SS}$  is  $P_{in} = Q^{SS} \mu (R_{in} L_a + R_{out} L_b)$ . The corresponding steady-state kidney pressure, equation (3.17), will simply be

$$P_k^{SS} = Q^{SS} \mu L_b R_{out}, \quad (4.2)$$

which is independent of  $R_{in}$ . This indicates that if a constant flow rate is required, the kidney pressure will be independent of the size of the working tools, or their position in the working channel. Equation (4.2) is plotted as the solid black line in Figure 6a.

In Figure 6b, we consider the effect of scope shaft placement within the access sheath on the time-dependent kidney pressure for fixed  $P_{in} = 60$  cm H<sub>2</sub>O. We plot equation (3.16) (multiplied by  $P^*$  to re-dimensionalise), shading the region between solutions for minimum and maximum  $R_{out}$  (indicated by the diagrams of centred and offset scopes). Here we have taken  $R_{in}$  for an empty working channel (without a working tool). For efficient and safe ureteroscopy, we seek a combination of high flow rate and low kidney pressure. We have shown, through the wedge predictions in Figures 4a,b, and 6b, that these can be achieved simultaneously by decreasing  $R_{out}$ . We have previously analysed optimising the geometry of the annular sheath/scope shaft (or working tool/working channel) cross-sections to minimise axial resistance by considering elliptical cross-sections of fixed areas for the scope shaft (or working tool) and sheath (or working channel) (Williams et al., 2019a). Here we will restrict our attention to modifying the shapes of the sheath and scope shaft, as it is these that influence  $R_{out}$ . Theoretically, we could also optimise the geometry for the working tool and working channel to minimise  $R_{in}$ , although as discussed, this will induce the unwanted effect of decreasing  $Q$  for fixed  $P_{in}$ . Using the optimisation method outlined in Williams et al. (2019a), with details provided in Appendix B, we determine the optimal shapes for the scope and access sheath, indicated in red in Figure 6b. This configuration has a dimensionless resistance ratio of  $\mathcal{R} = 9.6$ , compared to a value of  $\mathcal{R} = 4.1$  for the offset circular scope in a circular sheath. We return to Figures 4a and 6b to show the theoretical predictions for this optimal design (dashed red lines), showing a further increase in flow rate (Figure 4a), and reduction in kidney pressure (Figure 6b).

## 5. Discussion

We have considered a lumped-parameter model for irrigation during ureteroscopy. The basic modelling framework approximates the system by two distinct pipes, representing flow into the kidney through

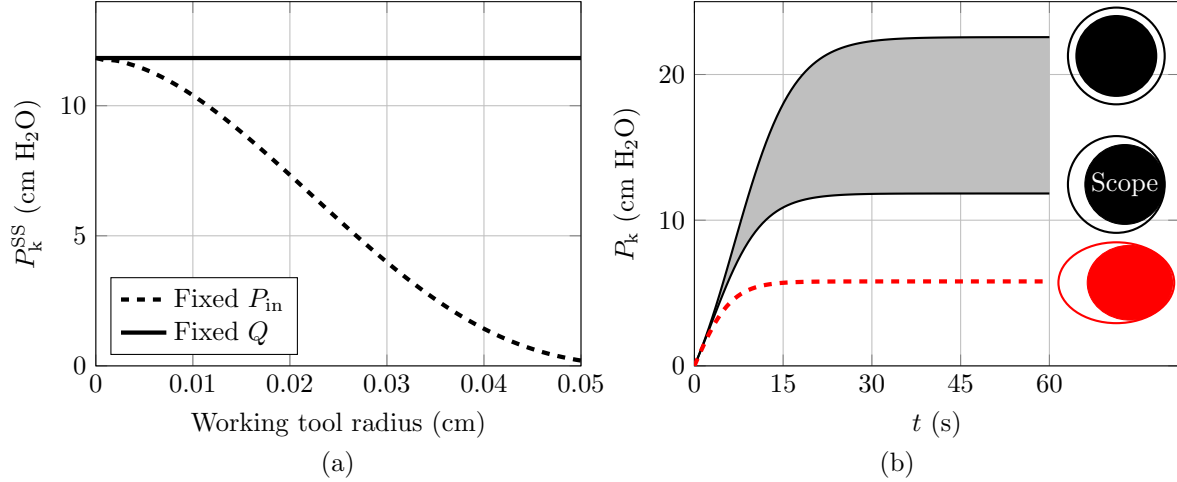


FIG. 6: Plot (a) plots  $P_k^{SS}$  for a fully offset working tool as a function of working tool radius. The value of  $R_{out}$  is taken to be for a fully offset sheath. Plot (b) shows the effect of  $R_{out}$  on  $P_k$  as a function of time. Geometries corresponding to the different values are indicated.

the working channel and flow back out through the access sheath, connected by a pressure point, representing the renal pressure. A similar model was previously developed (Oratis et al., 2018), although we include a data-motivated exponential, rather than linear, kidney compliance. We also improve on the model by Oratis et al. (2018), by focussing on the effects of flow resistance; in particular, modifying inflow resistance to include working tools and outflow resistance to account for the unknown position of the scope shaft within the access sheath.

The chosen exponential function for kidney compliance was shown to predict a reasonable rise time of  $\mathcal{O}(10^1 \text{ s})$  to steady state flow and kidney pressure for fixed inlet pressure. This was in contrast to the predictions of a compliant linear renal stiffness (used in the model by (Oratis et al., 2018)), which estimated uncharacteristically long rise times of  $\mathcal{O}(10^2 \text{ s})$ . Accurately predicting the rise time to maximum renal pressure for a fixed inlet pressure is crucial. For instance, an overestimation of the rise time could lead to significant underestimates of renal pressure, leading to improper procedural decisions, such as leaving the scope inserted when withdrawal could lower pressures back to a physically safe threshold (Oratis et al., 2018). Although fitting a stiffer linear relationship between our pressure and volume also results in predicted rise time of  $\mathcal{O}(10^1 \text{ s})$ , the pressure-volume data clearly displays a non-linear trend, and established stiffening effects cannot be captured with a linear correlation. It is also worth noting that while an exponential function provides a good fit for pressure-volume relationship, a more detailed description would be required to make accurate mechanical predictions, for instance of the stress within the kidney tissue.

Incorporating a degree of uncertainty into the model from the variable position of the scope shaft within the sheath effected predictive ‘wedges’ for steady-state flow rate and kidney pressure as functions of inlet pressure. The results of *ex-vivo* experiments for flow rate were within the estimated range, but the renal pressure was not so accurately predicted, with measurements from one particular kidney, kidney A, falling systematically below the estimated interval. We suggested a plausible explanation for this discrepancy: variations in the position of the pressure probe within the renal cavity during the

experiments. A downfall of the lumped-parameter model is that it assumes a constant renal pressure, but through numerical simulations of the steady Navier–Stokes equations in a simplified geometry, we determined that complex flow structures may exist within the kidney, leading to large spatial variations in kidney pressure. The simulations predicted a maximal variation in pressure that increased with inlet pressure and that matched, in order of magnitude at least, with the observed experimental discrepancy. While this is not proof that a different location of the pressure probe in kidney A was the cause of the discrepancy, the simulations were at least consistent with this hypothesis. The large variation in pressure in the numerical simulations also suggests that some caution may be needed when interpreting pressure readouts from the end of the ureteroscope.

The presence of general terms for viscous resistance through the working channel, and back through the access sheath, provides a simple platform for theorising on the effects of working tools and changing the geometry of the access sheath and scope shaft. We found that adding a working tool to the working channel decreases both the steady-state flow rate and kidney pressure for fixed inlet pressure. However, if a particular flow rate is sought during ureteroscopy, and the inlet pressure is adjusted accordingly to compensate for the presence of working tools, then the kidney pressure is unaffected by working tools and their size. Decreasing the outflow resistance increases flow rate and decreases kidney pressure for fixed inlet pressure. As this is a desirable combination, we determined the optimal elliptical shapes for the scope and access sheath (of fixed areas) to minimise outflow resistance.

The application of mathematical models to improve ureteroscopy is emerging, with Williams et al. (2019b), Williams et al. (2019a), Oratis et al. (2018), and this article providing groundwork for predicting system variables and optimising the design of pertinent biomedical devices. To bring this work closer to clinical translation, several model extensions would be useful. As we have shown, flow within the kidney can be complex, with both variable pressure and large vortical structures. These features may have strong impact on the removal of stone dust, as well as the predictions of a systems-level model. Hence, there is a clear need to both explore flow within the kidney cavity in more detail, as well as to couple such a flow description explicitly to a systems-level description of the procedure. Similarly, our model here takes the simplest possible mechanical description of the kidney as a tissue; another useful avenue of future study would be to develop a more detailed biomechanical description. Here, a natural addition would be viscoelastic effects, as suggested by the hysteresis observed in Fig. A.7. Though added modelling detail comes with a computational cost, so a significant challenge will be integrating such detailed modelling within a tractable systems model.

Given such advances, we can speculate on the potential integration of mathematical modelling and computational techniques in a modern operating room: we envision a ureteroscopic procedure in which the design of the medical equipment has been advised by optimisation techniques; an intelligent feedback system continually monitors quantities (such as irrigation flow rates), computes hidden quantities (such as intrarenal pressure), and automatically adjusts tuneable parameters (such as inlet pressure); additionally, if a different flow rate is required, e.g. to improve visualisation, predictions are made as to which factors should be varied to produce the desired result. While this describes an idealised scenario, there is a strong potential for improved procedural efficiency and reducing patient risk, and studies based on fundamental physics and mathematical modelling can provide critical first steps.

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## A. Data analysis

### A.1 Raw data

The independent variable in the experiments,  $P_{in}$ , is shown as a function of time for each experimental run in Figure A.7. The three rows show data for kidneys A, B, and C, respectively, and the corresponding data set (I or II) is indicated in the figure titles.

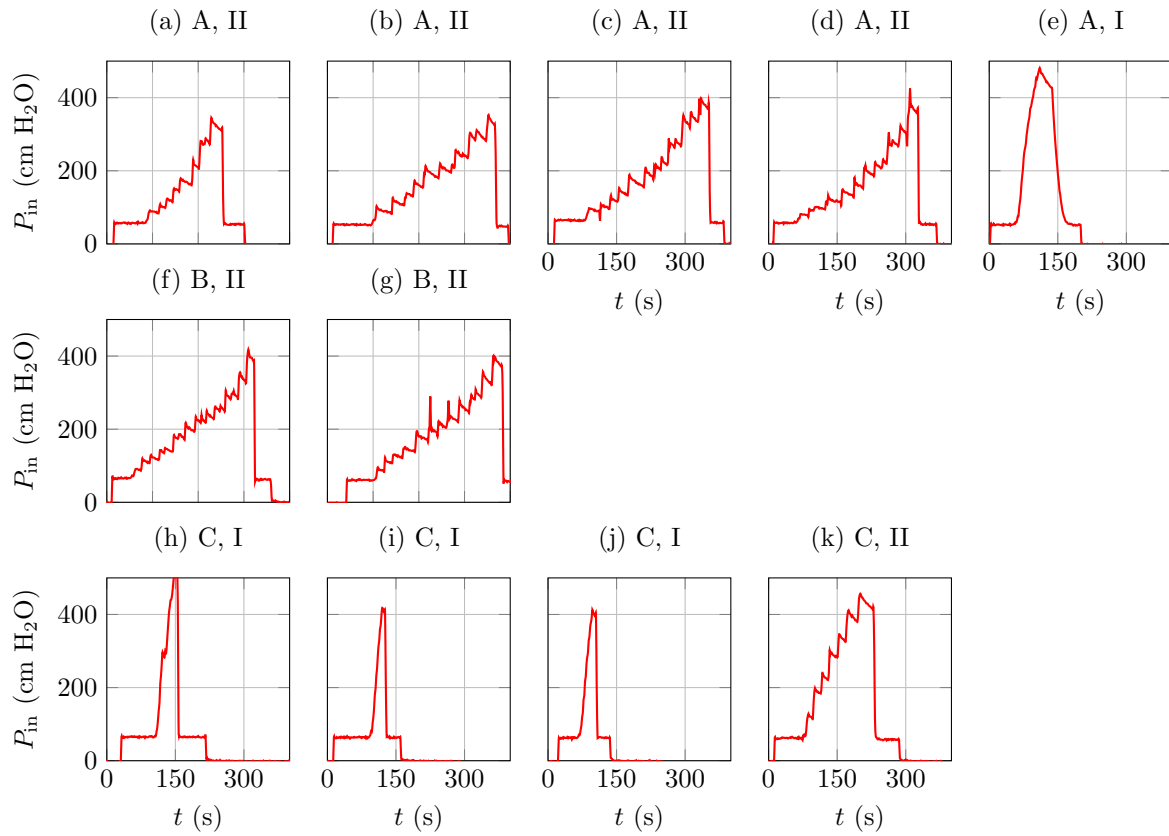


FIG. A.7: Inlet pressure ( $P_{in}$ ) over time. All vertical axes go from 0-500 cm H<sub>2</sub>O and horizontal axes from 0-400 s.

## A.2 Data set I

Intrarenal pressure is plotted against mass for data set I, (Figures A.7 (e), (h), (i), and (j)) in Figure A.8a. The mass and pressure data have been appropriately interpolated so they can be plotted against each other, with time parameterising the curve. The interval including both increasing and decreasing  $P_{in}$  is plotted, providing both ‘loading’ and ‘unloading’ curves. We note the presence of hysteresis, particularly prevalent for the data from kidney A in Figure A.8a; i.e., the loading and unloading data follows different curves. Additionally, with repeated loading and unloading cycles on a single kidney (kidney C), the hysteretic curves shift to the right.

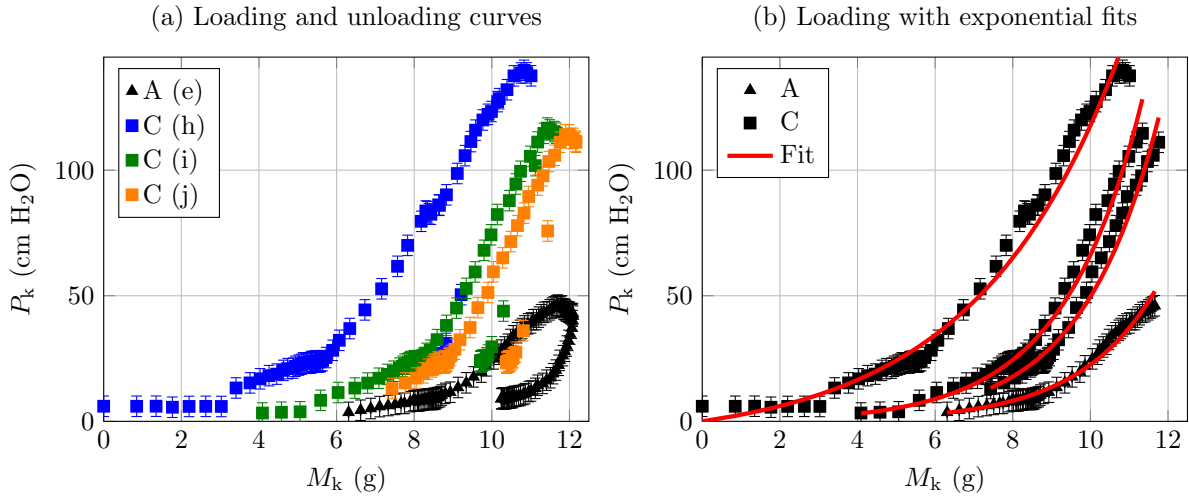


FIG. A.8: All continuous-loading data sets.  $P_k$  is plotted against  $M_k$  for the loading and unloading curves for (e), (h), (i), and (j) in Figure A.7.

It is well-established that biological tissue displays properties of viscoelastic solids (Humphrey, 2003). Thus, stress depends not only on the applied strain, but on the rate of strain. This leads to viscoelastic features such as hysteresis (difference in loading and unloading stress-strain curves), and stress relaxation, where if a material is suddenly strained and the strain is maintained constant, the stress in the material will decrease over time (Gregersen, 1996). Additionally, with repeated loading and unloading cycles, the load-deformation curves will shift to the right, and the hysteretic effects will diminish. By repeated cycling, eventually a steady-state is reached at which no further change will occur unless the cycling routine is changed. In this state the tissue is said to be preconditioned (Kauer, 2001).

By looking at the plots of inlet pressure over time (Figure A.7), we see that Figures (h)-(j) will lend themselves best to tissue preconditioning. This is reflected in Figure A.8a, where we see that the corresponding curves shift to the right, and curves (i) and (j) appear to be nearly indistinguishable. We thus use the loading curves of these two data sets in Section 4.1 to estimate the kidney compliance. We note, however, that all loading curves fit the exponential trend of equation (3.3) shown as the red lines in Figure A.8b. This further validates the use of an exponential kidney compliance, where  $P^*$  and  $C$  may depend on the kidney, loading rate, and any previous loading.

We have chosen two datasets for kidney C to determine the best-fit values for the exponential compliance model  $P^* = 5.24$  cm H<sub>2</sub>O and  $C = 0.43$  mL<sup>-1</sup> – equation (4.1) – as for these runs we could



be most confident that the kidney had been preconditioned. We note, however, that choosing the loading curve for kidney A (the black symbols in Figure A.8) results in values of  $P^* = 8.83$  cm H<sub>2</sub>O and  $C = 0.35$  mL<sup>-1</sup>. The data for kidney A (black triangles) along with the best-fit exponential curve (red line) are shown in Figure A.9. Using these values in the model for kidney pressure, equation (3.16), we obtain the red curve in Figure A.9b. As a comparison, we reproduce the red curve from Figure 3b, which uses the fitted  $P^*$ ,  $C$  values for kidney C as the dashed black line in Figure A.9b. Of interest is to note the similarity of the two curves produced with different values of  $P^*$  and  $C$ , indicating that different kidney compliances will yield similar qualitative – and even quantitative – kidney pressures over time.

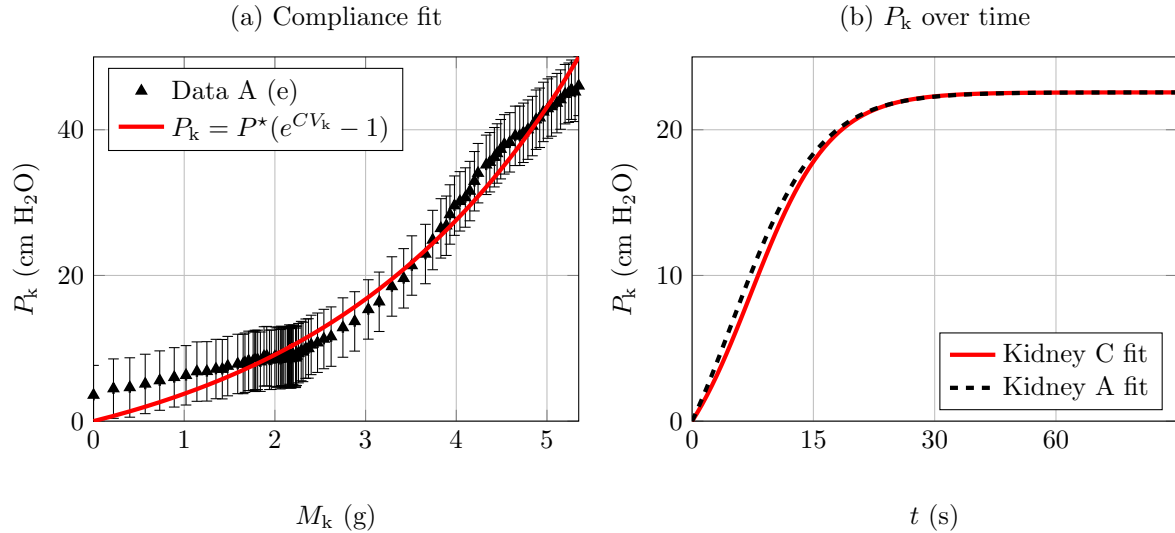


FIG. A.9: All continuous-loading data sets.  $P_k$  is plotted against  $M_k$  for the loading and unloading curves for (e), (h), (i), and (j) in Figure A.7.

### A.3 Data set II

The data in set II, with inlet pressure shown in Figures A.7 (a)-(d), (f), (g), (j), and (k), is used to estimate steady-state flow rate and pressure data. Multiple five-second intervals, where the inlet pressure is approximately constant, are extracted from each data set. The flow rate as a function of time is estimated by taking the difference between successive outflow mass measurements, divided by the time step. A plot of the mean flow rate against the mean inlet pressure over each five-second interval provides the data points in Figure 4a. The error bars in Figures 4a,b combine the standard deviation between successive mass measurements within each five-second interval and the measurement error, as described in the following section. Note that all data from set II is included in Fig 4; since the data from different runs on each kidney was very similar, we have not delineated between the runs, only between the different kidneys.

### A.4 Error estimation

The mass balance used was the OHAUS Traveler, which has a readability of 0.01 g. Therefore, the systemic error in mass measurements was taken to be  $\Delta_M = \pm 0.005$  g. This is displayed as the (indiscernible) horizontal error bars in Figures 3, A.8, and A.9. A FISO Fiber Optic Pressure Sensor FOP-M260-21 was used to record pressure measurements, and has an accuracy of 0.5% of the  $-300$  to  $300$  mmHg pressure scale. Therefore, the systematic error in pressure measurements was taken to be  $\Delta_P = \pm 0.005 \times 600 = \pm 3$  mmHg. This is taken as the vertical error bars in Figures 3, A.8, and A.9 (conversion between mmHg and H<sub>2</sub>O requires multiplication by a factor of approximately 1.36).

For the steady-state experiments we calculate a series of  $n$  flow rates over a five-second interval

$$Q_i = \sum_{k=1}^n \frac{M_k^{i+1} - M_k^i}{\Delta t_i}, \quad (\text{A.1})$$

where  $\Delta t_i = 500$  ms (so  $n \approx 10$ ). The standard deviation of the series of flow rates then has an associated mean  $\mu_Q$  and standard deviation  $\zeta_Q$ . As flow rate is estimated by subtracting successive mass measurements, the total systematic error in flow rate was  $\Delta_Q = \sqrt{2}\Delta_M \sqrt{\sum_{i=1}^n (1/\Delta t_i)^2} / (n-1)$ . We assume that the standard deviation in the flow rates and the measurement errors due to the readability of the mass balance are independent and thus the total error

$$T.E. = \sqrt{\zeta_Q^2 + \Delta_Q^2}, \quad (\text{A.2})$$

is taken as the vertical error bars in Figure 4a. The vertical error bars on the approximated steady state pressure in Figure 4b is given by

$$T.E. = \sqrt{\zeta_P^2 + \Delta_P^2}, \quad (\text{A.3})$$

where  $\zeta_P$  the standard deviation of the approximately 625 pressure measurements over each five-second interval.

## B. Determining the optimal elliptical shape

In our previous study of flow through elliptical annular pipes (Williams et al., 2019a) we sought to determine the optimal elliptical geometry – elliptical shapes of the outer and inner boundaries and the position and orientation of the annulus core – to minimise flow resistance. We formulate the optimisation problem

$$\min_{\mathbf{g}} -Q, \quad \text{s.t. } \mathbf{c} \geq 0, \quad (\text{A.1})$$

where  $Q$  is determined as the solution to

$$\nabla^2 w = -1, \quad Q = \iint_{\Omega} w \, d\Omega, \quad (\text{A.2a,b})$$

and  $\Omega$  is the annular space between the inner and outer ellipses representing the scope shaft and access sheath. In equation (A.1),  $\mathbf{c}$  is a vector of six geometric non-linear constraints which ensure that the inner ellipse is fully contained within the outer ellipse (Williams et al., 2019a). We solve equation (A.2) using open-source finite element library `Firedrake`, and implement `MATLAB`'s optimisation routine, `fmincon`, to solve the optimisation problem (A.1) with an interior-point method from eight randomly generated starting points in the feasible five-dimensional parameter space. As the optimisation routine

seeks local minima, a multi-start approach allows for global optimisation. The optimal geometry found through this method is shown in Figure A.10 with major and minor axis of the scope shaft (0.17, 0.15) cm and of the access sheath (0.23, 0.16) cm indicated. The contour lines in Figure A.10 provide contours of  $w$ ;  $Q \approx 1.2$  is obtained by equation (A.2) $b$ .

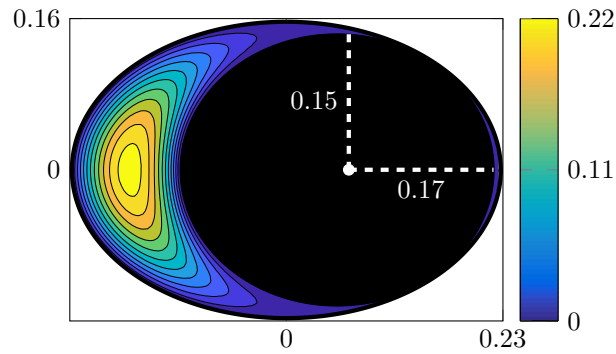


FIG. A.10: The optimal geometry for scope shaft/access sheath with measurements provided in cm. The colorbar provides contours of  $w$  (dimensionless).

### C. Pressure variation in the renal pelvis

To model pressure variation in the renal pelvis (Figures 5), we consider the light-pink two-dimensional domain in Figure A.11, where irrigation fluid enters through  $\Gamma_{in}$  (the tip of the working channel), and exits through  $\Gamma_{out}$  (the gap between the scope shaft and the access sheath). We model irrigation flow in the

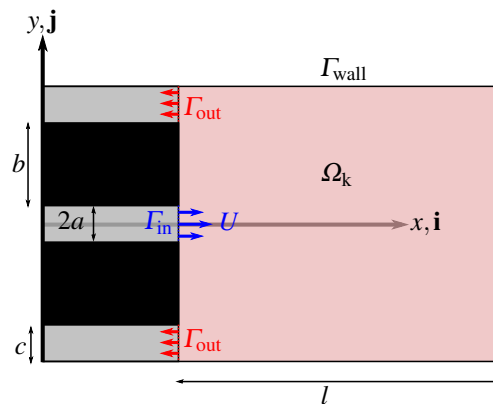


FIG. A.11: The geometric domain where  $a$  represents the radius of the working channel,  $b$  the radius of the scope shaft minus the radius of the working channel, and  $c$  the gap between the scope and access sheath for a centred scope. The light pink domain represents the domain,  $\Omega_k$ , in which the Navier–Stokes equations are solved numerically.

cavity with the steady Navier–Stokes equations, considering a velocity field in Cartesian coordinates,

$\mathbf{u} = u\mathbf{i} + v\mathbf{j}$ . We impose a fully-developed parabolic profile with maximum velocity  $U$  at the inlet boundary. Non-dimensionalising  $(x, y)$  with the half-width of the inflow channel ( $a$  in Figure A.11),  $\mathbf{u}$  with  $U$ , and pressure  $p$  with  $\mu U/a$ , the dimensionless steady Navier–Stokes equations are

$$\text{Re}(\mathbf{u} \cdot \nabla)\mathbf{u} = -\nabla p + \nabla^2 \mathbf{u}, \quad \nabla \cdot \mathbf{u} = 0, \quad (\text{A.1a}, b)$$

where  $\text{Re} = \rho U a / \mu$ . The prescribed dimensionless inflow is then

$$u = 1 - y^2, \quad v = 0, \quad \text{on } \Gamma_{\text{in}}. \quad (\text{A.2})$$

At the outflow boundaries  $\Gamma_{\text{out}}$ , we prescribe zero normal and tangential stress,  $\boldsymbol{\sigma}\mathbf{n} = \mathbf{0}$ , which provides

$$2u_x - p = 0, \quad u_y + v_x = 0, \quad \text{on } \Gamma_{\text{out}}. \quad (\text{A.3a}, b)$$

On the walls (black solid lines in Figure A.11), we assume no-slip

$$u = v = 0, \quad \text{on } \Gamma_{\text{wall}}. \quad (\text{A.4})$$

For a particular experiment of flow rate  $Q$ , we can approximate the maximum inflow velocity,  $U = 2(Q/\pi a^2)$ , and hence the Reynolds number

$$\text{Re} = \rho 2Q / \pi a \mu. \quad (\text{A.5})$$

Equations (A.1) are solved subject to (A.2), (A.3), and (A.4) are solved with finite elements implemented in `Firedrake` (Balay et al., 2018, 1997; Dalcin et al., 2011; Rathgeber et al., 2016; Hendrickson & Leland, 1995; Mitchell & Müller, 2016; Kirby & Mitchell, 2018; Amestoy et al., 2001, 2006; Deuffhard, 2011). The solver we use was provided by the authors of Farrell et al. (2019), but extends the work of that paper to use the exactly divergence-free Scott-Vogelius element instead, as explained in (Wechsung, 2019).

The relevant Reynolds numbers for simulations representing the flow rates in Figure 4a, and thus measured renal pressures in 4b, range from  $\text{Re} = 0$  to  $\text{Re} = 1883$ . Results of the simulation for  $\text{Re} = 1500$  ( $Q \approx 1.4 \text{ cm}^3/\text{s}$ ) are shown in Figures 5a,b. We have previously determined the existence of multiple solutions to the steady Navier–Stokes equations solved in the domain pictured in Figure A.11, with the asymmetric solution branch theorised to be stable, where it exists (Williams, 2019). By initially placing a no-slip condition on one of the outflow boundaries, we ensure the asymmetric solution branch.

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