

## **A review on the purification and use of biogas in compression ignition engines**

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### **ABSTRACT**

Biogas is commonly produced during the decay of organic matter. It is a mixture of methane and some non-combustible gases such as CO<sub>2</sub> and H<sub>2</sub>S. Its viability as a renewable alternative fuel for internal combustion engines can be enhanced by methane enrichment, i.e. removal of the non-combustible constituents. One of the common techniques for using biogas in a compression ignition (CI) engine is to mix it with air in the intake manifold, induct, and compress this mixture and ignite it by injecting a small quantity of diesel or bio-diesel, which is termed as the pilot fuel. This is known as the dual fuel mode. The pilot fuel is injected close to the end of the compression stroke as in a conventional CI engine and the injected fuel quantity depends on the operating condition. An alternative approach is the Homogeneous Charged Compression Ignition (HCCI) mode. Here, a homogeneous mixture of biogas and air is inducted and compressed by the piston until it auto-ignites. While this concept combines the benefits of spark ignition (SI) and CI engines, the onset of combustion cannot be controlled directly. A detailed review of recent research pertaining to biogas purification techniques and operation of CI engines with biogas in dual fuel and HCCI modes is presented in this paper. The effects of various operating parameters on engine performance and emissions, and comparison with conventional diesel fuelled CI engines are discussed. Biogas improves combustion efficiency, NO<sub>x</sub>, and smoke emissions. However, it reduces brake thermal efficiency, volumetric efficiency, and increases HC and CO emissions. Biogas fuelling of CI engines is recommended for achieving high diesel substitution, especially under high torque operation.

**Keywords:** Biogas; CI engine; dual fuel; HCCI; methane enrichment

### **INTRODUCTION**

The world's primary energy resources such as petroleum, natural gas, coal, and nuclear fuels are not renewable. Their rapid depletion, consequent rise in prices, increased global energy demand, and concern for environmental protection have escalated the quest for alternative, renewable sources of energy like solar energy, hydro energy, wind energy, and biofuels [1]. Furthermore, petroleum reserves are largely concentrated in a few regions of the world. Countries in other regions face severe crisis in bridging the gap between energy demand and fuel supply [2]. Fossil fuel combustion also results in air pollution, acid rain, and build-up of carbon dioxide, thus putting human beings and the environment at risk [3-7]. Among the alternatives to fossil fuels, biofuels such as biogas, alcohols, and biodiesels have received considerable attention due to their renewable nature and their inherent potential to bring down net CO<sub>2</sub> emission [8-11].

Using biogas as a fuel addresses three major challenges; identifying a renewable source of energy, effective disposal of biological waste, and harnessing methane, a potent greenhouse gas emanating from decomposing biomass. Biogas offers several advantages over other fuels derived from biomass. It can be transported easily via pipelines or as a compressed gas in cylinders once the corrosive components, viz. CO<sub>2</sub>, H<sub>2</sub>S, and water vapour are removed [12]. Compared to solid fuels like coal, biogas burns faster and leaves no residue behind and is more environment-friendly. Biomass, which is the source of biogas, can ultimately be traced back to vegetation. These plants/trees absorb CO<sub>2</sub> during their lifetime, so despite the emission of CO<sub>2</sub> during combustion, biogas may be considered as a CO<sub>2</sub>-neutral fuel [13]. The production of biogas also requires less processing effort and cost compared to other biofuels like alcohols and biodiesel [14-17]. Biogas holds great potential for developing economies with a rural background. For example, India has a cattle population of about 300 million, which is about 20% of the world total. About 980 million tonnes of cow dung are produced annually. This can potentially generate about 63.8 trillion litres of biogas, which in turn translates into 1.3 trillion MJ of energy [18-20].

Owing to the difference in the structural, proximate, and ultimate analyses results of biomass, some properties of the biogas samples such as the fractions of hydrogen, CO<sub>2</sub>, and sulphur and the ignition temperature vary from sample to sample [13]. Typically, biogas contains 25 to 40% carbon dioxide by volume [21]. Unless it is removed, it forms a highly corrosive acid on reacting with water, destroying pipelines, and equipment. Being non-combustible, carbon dioxide also reduces the heating value and energy density of biogas on volume basis and waste pipeline capacity. In addition, the presence of CO<sub>2</sub> results in reduced flame velocity and flammability range compared to pure methane. Biogas resists knocking in SI engines by virtue of its high-self-ignition temperature [22]. However, this in turn makes ignition difficult in CI engines. A possible means of overcoming these drawbacks is to extract the CO<sub>2</sub> content of biogas, thereby increasing the combustible fraction and making it a more viable alternative fuel [6, 7, 23-26]. This purification process is known as methane enrichment. In the light of these aspects, the present work discusses details of biogas production, methane enrichment (biogas purification) techniques, application of biogas in CI engines in two modes viz. dual fuel and HCCI, effect on engine performance and emissions, and numerical models available in published literature.

## **METHODS AND MATERIALS**

### **Biogas Production and Purification**

Various waste-to-energy (WTE) technologies for converting biological waste, e.g. industrial and municipal solid wastes (MSW) into biofuels have been investigated in recent years [14, 27, 28]. These methods can be broadly classified into four groups; a) hydrogenation, b) pyrolysis, c) gasification, and d) bioconversion. One of the most common means of producing biogas is using a digester, where anaerobic digestion of biomass generates biogas. Anaerobic digestion is a bioconversion process involving three stages viz. hydrolysis, acidification, and methane generation. The biogas obtained is thus predominantly a mixture of methane, CO<sub>2</sub>, and H<sub>2</sub>S [21]. Some common properties of raw biogas are given in Table 1. Methane produced by anaerobic digestion has cost and efficiencies comparable to those of other biomass energy forms such as synthesised gases and ethanol [29]. Anaerobic digesters exist in various designs such as fixed dome type and floating drum type [21].

Table 1. Properties of biogas.

Parameters description	Value
Composition of biogas (% by volume) [30]	Methane (CH <sub>4</sub> ) = 50 to 70 Carbon dioxide (CO <sub>2</sub> ) = 25 to 50 Hydrogen (H <sub>2</sub> ) = 1 to 5 Nitrogen (N <sub>2</sub> ) = 0.3 to 3 Water vapour (H <sub>2</sub> O) = 0.3 Hydrogen sulphide (H <sub>2</sub> S) in traces
Auto-ignition temperature (K) * [31]	1087
Calorific value (MJ/kg) * [31]	20.67
Density at 1 atm & 288 K (kg/m <sup>3</sup> )* [31]	0.91
Stoichiometric air-fuel ratio (kg of air/kg of fuel) [32]	6.05
Research octane number [30]	130
Flame speed (m/s) [33]	21
Flammability limit (vol. % in air) [33]	7.5 – 11.7

\*: for biogas containing 60% CH<sub>4</sub> and 40% CO<sub>2</sub>

Different methods have been used for purifying biogas by separating the unwanted species. Some of the commonly used physicochemical methods of separation involve water scrubbing, chemical reagents, molecular sieves, membranes, gas-liquid adsorption membranes, and cryogenic cooling. The conventionally used method of water scrubbing is a physical separation process, wherein compressed biogas is fed to the bottom of a packed column, and pressurised water is sprayed at the top, forming a counter-flow arrangement [34]. CO<sub>2</sub> dissolves in water at high pressure and can be released later by lowering the pressure, enabling water recycling. Bhattacharya, Mishra, and Singh [35], Khapre [36] and Dubey [37] developed different scrubbing mechanisms offering a high degree of CO<sub>2</sub> absorption. Vijay [18] developed a high pressure packed bed scrubber mechanism where up to 99% of CO<sub>2</sub> was removed at an operating pressure of 1 MPa. Organic liquid reagents like Monoethanolamine (MEA), Diethanolamine (DEA), and Triethanolamine (TEA) can be used as solvents in place of water for absorbing CO<sub>2</sub> and H<sub>2</sub>S, but this increases the equipment cost. Similarly, sodium or calcium hydroxide can also be used to absorb CO<sub>2</sub> by forming the respective carbonate salts [38]. Biswas, Kartha, and Pundarikakhadu [39] demonstrated the effectiveness of chemical absorption using the reagent monoethanolamine, which can be regenerated by boiling. Savery and Cruzan [40] used a solution of NaOH, KOH, and Ca(OH)<sub>2</sub> as the absorbing agent and found that turbulence generated by agitation enhanced the absorption capacity. Membrane separation technique has been in use for many years [41, 42]. The basic principle of membrane separation is that some species present in the raw gas could pass through thin membranes of ~ 1 mm thickness, while other species are retained. The difference in the partial pressures and permeability of species play an important role here. Molecules which are small and highly soluble in the membrane material permeate faster. Typically, when compressed biogas is fed to a polymer membrane, CO<sub>2</sub> molecules permeate, whereas methane is retained. Pressures in the range 25–40 bar are required for the process. By comparing the performance of different membrane materials, Basu et al. [43] identified polymers like cellulose acetate, ethyl

cellulose, silicon polycarbonate, polyimides, polysulfones, polydimethylsiloxane and polymethylpentene as the best suited for methane enrichment.

Molecular sieve method, also called Pressure Swing Adsorption (PSA) works based on the selective affinity of species for certain adsorbing materials. This technique involves three steps, viz. CO<sub>2</sub> adsorption at a high pressure, regeneration after decompression, and pressure build-up for adsorption. Porous materials having high surface area such as activated carbon, alumina, silica gel and zeolites are used as adsorbents in PSA-systems [34]. One of the earliest reported studies involved a naturally occurring zeolite [44], wherein the breakthrough curves demonstrated good feasibility in methane enrichment. Pandey and Fabiani have used Neapolitan Yellow Tuff, a naturally occurring zeolite which acts as a molecular sieve to adsorb CO<sub>2</sub>. Cryogenic separation is carried out at a low temperature (~ -90°C) and high pressure (~ 40 bar) [34]. During this process, the CO<sub>2</sub> fraction of biogas gets liquefied early on and is separated from the gaseous portion which is rich in methane. This method is still in the early stage of the research. One of the most recent developments in the area of biogas purification involves carbon nanotubes (CNTs). Liu et al. [45] used molecular dynamics to evaluate the CO<sub>2</sub> permeability potential of CNTs. They predicted better performance in windowed CNT compared to ordinary CNT. Carbon nanotubes can also be potentially used as inorganic filler for mixed matrix membrane in biogas separation membranes as the nanomaterials enhance the yield and permeability [46].

Table 2. Comparison of biogas purification methods.

Technique	References	Benefits	Disadvantages
Water scrubbing	[18, 34-37]	Low CH <sub>4</sub> losses High efficiency and simple operation	Expensive operation and investment High likelihood of clogging
Chemical reagents	[38-40]	Low CH <sub>4</sub> losses High efficiency and low cost	Expensive operation High likelihood of corrosion
Molecular sieves	[44]	Less energy usage Compactness Simple construction and operation	More CH <sub>4</sub> losses Expensive operation
Membranes	[41-43]	Low cost	More CH <sub>4</sub> losses
Cryogenic cooling	[34]	High purity	Expensive operation

Table 2 shows a comparison of the various purification methods outlined above. Scrubbing and membrane separation do not need special equipment or chemicals to run and hence are the simplest processes to operate. While the operation of pressure swing adsorption is also quite simple, where the plant needs to be shut down several times annually to replace the catalyst as H<sub>2</sub>S gradually poisons the adsorbent material. In contrast, the high pressure and very low temperatures required for cryogenic separation demand sophisticated equipment and thorough checking of insulation and sealing. Membrane separation offers a number of significant advantages such as compactness and modularity of devices. Membrane systems can be operated in mild conditions and

are energy efficient on account of very low electricity and fuel consumption [34]. Mixed Matrix Membranes with CNT and silicon nanoparticles are still at research level.

### Applications Of Biogas

In addition to direct combustion in burners and boilers, biogas has been used to power prime movers such as gas engines. There is an even greater potential for biogas if it can be utilised as a transportation fuel. The use of biogas in conventional SI and CI engines has been a topic of extensive research over the past few decades [1, 4, 47-51]. Table 3 illustrates the difference in composition of biogas used by various researchers. Biogas is commonly used in two modes of a CI engine which are discussed below.

Table 3. Composition of biogas used by various researchers.

Biogas composition (% vol.) CH <sub>4</sub> :CO <sub>2</sub>	References
57.37:42.1	[52]
60:30	[47]
60:40	[31, 32, 53-56]
73:17.37	[33, 57]
73:19	[58]
30-73:20-40	[50, 59]
50-70:25-50	[30]
95:3 & 65:32	[48]
59:41, 70:30 & 80:20	[22]
90:10, 80:20, 70:30 & 60:40	[49]
100:0, 70:30, 59.9:40.1, 49.7:50.3 & 39.9:60.1	[60]
100:0, 87.5:12.5, 75:25 and 50:50	[61]

### Dual Fuel Mode

In the dual fuel mode, biogas is mixed with air in the intake manifold and inducted into the engine cylinder, where it undergoes compression. Towards the top dead centre (TDC), a small quantity of diesel or bio-diesel termed as the pilot fuel is injected. The self-ignition of the pilot fuel initiates a flame which traverses the combustion chamber, consuming the biogas-air mixture. A comparison of combustion, performance and emission characteristics of CI engines operated on biogas in dual fuel mode vis-à-vis conventional diesel-only operation is presented below.

### Combustion Indices

Dual fuel mode shows similar performance trends as those of an SI engine [53, 62]. The energy release from the pilot diesel spray is several orders of magnitude higher than that of a spark, thus improving the ignitability of the inducted mixture. Compared to diesel operation, the biogas dual fuel mode has longer ignition delay on the account of the CO<sub>2</sub> content causing a high initial heat release. Consequently, the cylinder peak pressure increases and occurs closer to the TDC with increase in biogas concentration [33, 50, 63]. Studies on an IDI engine with biogas in dual fuel mode with diesel substitution up to 48% indicated a reduction in combustion duration and consequently lower exhaust gas temperatures [58]. In a study involving biogas-diesel dual fuel operation, the maximum Net Heat Release Rate (NHRR) was observed to be around 30% greater for the dual fuel mode compared to diesel-only mode under similar loading and speed

conditions [64]. The increase in ID can be offset by using higher quantity of pilot fuel. However, for pure methane combustion, it is seen that the ID is nearly independent of the quantity of pilot fuel injected [65]. Bora et al. [31] observed that the quantity of pilot fuel supplied can be reduced by using high compression ratios because of the shorter ignition delay of biogas at elevated temperatures. They used compression ratios in the range of 16-18. The reduction in ignition delay can also be achieved by oxygen enrichment, i.e. by increasing the oxygen content of air. This improves the reaction rate and flame propagation. Raising the oxygen content in air from 21% to 27% has been reported to shorten the ignition delay by nearly 3 °CA [32]. Ignition delay is lower for thermal barrier coated dual fuel engine compared to normal dual fuel engine [66]. Methane enrichment increases cylinder peak pressure and combustion duration and reduces ignition delay [67].

Ray, Mohanty, and Mohanty [68] reported that the ignition delay of the pilot fuel is directly proportional to the ratio of biogas to diesel. Pilot diesel injection of around 10- 20% of the amount used in diesel-only mode is sufficient for dual fuel operation. Biogas supply requires to be regulated by means of a gas control valve depending on the load. The authors have noted that in governed engines, the control of the pilot fuel by the governor is enough to get the desired output. The diesel substitution is relatively low in such cases. Park and Yoon [69] compared diesel-biogas mode with diesel-gasoline mode. It was reported that an increase in port injection ratio leads to an increase in ignition delay compared to diesel-gasoline mode. Investigations by Königsson et al. [63] on a biogas-diesel dual fuel engine showed that by advancing the crank angle for 50% heat release, the average in-cylinder temperature and combustion efficiency can be enhanced. This also extends the lean limit of the engine. A similar effect can be achieved by increasing the inlet temperature. Up to 40% exhaust gas recirculation (EGR) can be used in dual fuel mode, while still allowing up to 95% diesel substitution. EGR reduces the lean operating limit and combustion efficiency. The use of EGR also favours near-stoichiometric operation. This allows the use of three-way catalyst, promising reduced after-treatment cost. Stoichiometric combustion with EGR and low inlet temperature is the recommended operating condition for dual fuel mode [63]. The use of biogas in a dual fuel engine with dimethyl ether (DME) as the pilot fuel was studied by Park et al. [59]. The proportion of biogas (on energy release basis) was varied from 0% (only DME) to 80%. Higher biogas:DME ratio resulted in a fall in peak rate of heat release, burning rate, and cylinder pressure besides causing unstable combustion reflected as higher Coefficient of Variance (COV) of peak pressure. For injection earlier than 20° bTDC, ignition delay was longer and start of ignition (SOI, defined as the crank angle of 10% of cumulative heat release) retarded for higher biogas energy ratio. However, both ignition delay and SOI were nearly independent of the biogas content for retarded injection.

Barik and team used Karanja methyl ester (KME) with biogas in dual fuel mode. They studied the effects of various concentrations of diethyl ether (DEE) as an ignition improver [70] and different injection timings [71]. Addition of DEE increases cylinder peak pressure and reduces combustion duration. Advancing the injection timing increases the ignition delay. Bora and Saha [72, 73] reported the effect of compression ratio in CI engine using rice bran biodiesel as pilot fuel and biogas as primary fuel at various compression ratios and injection timings. An increase in compression ratio increases cylinder peak pressure and reduces ignition delay. Cylinder peak pressure increases with advance in injection timings.

### **Performance Indices**

Bora et al. [31] and Yoon and Lee [50] reported a reduction in brake thermal efficiency and an increase in BSFC (Brake Specific Fuel Consumption) in dual fuel mode compared to diesel operation. This was attributed to early occurrence of peak pressure, low combustion temperature, and flame speed as well as higher pumping work due to the presence of CO<sub>2</sub>. Duc and Wattanavichien [58] operated an IDI engine with biogas in dual fuel mode with diesel substitution up to 48%. Dual fuel and diesel modes showed almost equal fuel conversion efficiencies at full load operation whereas efficiency of the dual fuel mode was lower at part loads. Bora et al. [31] suggested increasing the compression ratio as a means to partially negate the reduction in brake thermal efficiency of the dual fuel mode. Simulated biogas is used by various researchers in dual fuel mode [56, 74-76]. Feroskhan and Ismail [77] used simulated biogas and reported that methane enrichment will enhance the brake thermal efficiency at low biogas flow rates. Mustafi et al. [64] also observed that the brake specific energy consumption of the biogas-diesel dual fuel and diesel-only modes was nearly the same. Sorathia and Yadav [78] also reported almost no deterioration in brake thermal efficiency in a CI engine operated in dual fuel mode with diesel and biogas. Percentage of fuel energy lost to the coolant was higher for dual fuel mode, whereas exhaust losses were lower. Exergy efficiency was found to be higher and percentage exergy destruction lower for the dual fuel mode. Raising the oxygen content in air from 21% to 27% has been reported to improve the brake thermal efficiency of a biogas-diesel dual fuel engine from 15 to 18% [32]. In a biogas-DME dual fuel engine, IMEP was observed to fall with an increase in biogas content for retarded pilot injection, whereas the trend was opposite for injection advance more than 20 °bTDC [59].

Experiments with different methane:CO<sub>2</sub> ratios have indicated that a 7:3 ratio provides the highest brake thermal efficiency [62]. The authors attributed this to the dissociation of CO<sub>2</sub> into CO and O<sub>2</sub> due to the high temperature of the diesel flame. CO is a fast burning gas, hence accelerating the burning rate. The additional oxygen concentration also improves combustion. However, for higher CO<sub>2</sub> content, the dilution effect dominates and lowers the thermal efficiency. Sahoo, Sahoo, and Saha [79] reviewed various works dealing with dual fuel gas diesel engines. They confirmed that biogas containing up to 20-30% CO<sub>2</sub> offers lower BSFC compared to diesel-natural gas operation, whereas BSFC increases with further increase in CO<sub>2</sub> content on account of the inert gas effect. For above 40% CO<sub>2</sub>, the engine operation becomes rough due to irregular combustion. For increasing CO<sub>2</sub> content, the engine speed and power can be maintained by increasing either the biogas or the pilot fuel flow rate. Compared to diesel-only operation, the dual fuel mode results in marginally lower volumetric efficiency on account of the displacement of air. This effect is enhanced by increasing the carbon dioxide fraction of biogas. Luijten and Kerkhof [60] observed that with biogas containing 70% methane, the volumetric efficiency dropped from 95% for the diesel mode to 91-92% for dual fuel operation, when the energy released from diesel and biogas were equal. They also noted that while biogas with 70% methane can substitute up to 55% diesel on energy release basis, the substitution was limited to 35% for biogas with 40% methane. Light end gas knock was reported for high methane:diesel ratio [60]. Addition of CeO<sub>2</sub> nanoparticles in diesel, EGR, split injection, and induction of hydrogen in dual fuel mode increase brake thermal efficiency [80, 81].

Barik and Sivalingam [82] worked on a biogas-diesel dual fuel engine where the pilot fuel flow rate was controlled by the governor and the biogas flow rate was varied

manually from 0 - 0.6 kg/h. At full load, the maximum diesel substitution (on energy basis) was 30%. Volumetric efficiency was reported to be lower and brake specific energy consumption higher for dual fuel mode as the CO<sub>2</sub> displaces air and deteriorates the burning rate. Barik and Murugan [33] also noted a reduction in volumetric and brake thermal efficiencies on increasing the biogas flow rate. Increase of DEE concentration in KME-biogas has been shown to reduce brake thermal efficiency and exhaust gas temperature and increase BSFC of a dual fuel engine [70]. Advancing injection timing increases brake thermal efficiency and exhaust gas temperature and reduces BSFC. Optimum injection timing is reported as 24.5° CA bTDC[71]. An increase in compression ratio of rice bran biodiesel-based dual fuel engine increases brake thermal efficiency and volumetric efficiency and reduces BSFC and exhaust gas temperature [72].

### ***Emission Indices***

The low temperatures are caused by the presence of CO<sub>2</sub> in biogas augment CO and unburned hydrocarbon (UHC) emissions, while oxides of nitrogen (NO<sub>x</sub>) and particulate matter (PM) emissions are less compared to diesel mode [33, 50, 53, 62]. Barik and Sivalingam [82] found that exhaust gas temperature was lower by 2.8%, CO and HC higher by 16% and 21%, respectively, while NO<sub>x</sub> and soot lower by 35% and 41.3%, respectively, as compared to diesel operation for maximum diesel substitution at full load. At higher CO<sub>2</sub> fractions, it remained undissociated, thereby acting as an inert gas and reducing the thermal efficiency. NO<sub>x</sub> emissions decrease with the increasing CO<sub>2</sub> content of biogas, similar to the effect produced by EGR. CO and HC emissions can be brought down by increasing the compression ratio by virtue of the higher temperatures. However, this causes a notable increase in CO<sub>2</sub> and NO<sub>x</sub> emissions [31]. The extent of variation of these parameters can be controlled by adjusting the pilot diesel injection quantity [64, 65]. Barik and Murugan [33] observed that a biogas flow rate of 0.9 kg/h provided the optimum combination of performance and emissions. This corresponds to the replacement of 0.215 kg/h of diesel.

Oxygen enrichment lowers the methane emissions. CO emissions do not show a definite trend. By attenuating combustion instabilities, oxygen enrichment allows greater substitution of diesel by biogas [32]. EGR reduces the lean operating limit and combustion efficiency, while NO<sub>x</sub> emissions are lowered. NO<sub>x</sub> formation can be attributed to the pilot diesel spray for lean mixtures ( $\lambda > 1.6$ ) and to the high temperature combustion of methane-air mixture under rich conditions [63].

Biogas in a dual fuel engine with DME as the pilot fuel reduced indicated specific NO<sub>x</sub> emissions, while ISHC and ISCO emissions increased upon increasing the proportion of biogas. Soot emissions were close to zero [59]. In a dual fuel engine operated with biogas and Karanja Methyl Ester (KME) as pilot, it was observed that about 22% replacement of the pilot fuel was possible with a biogas flow rate of 0.9 kg/h at full load. The study also showed that NO<sub>x</sub> and PM emissions can be simultaneously reduced for the dual fuel operation, though CO and HC emissions increased [57]. Effects of DEE in KME-biogas dual fuel mode were reported by Barik and team [70]. An increase in DEE reduces CO, NO<sub>x</sub>, and smoke emissions. However, it increases HC emissions. Optimum injection timing is reported as 24.5°CA bTDC with reduction of 17.1% CO emission, 18.2% HC emission, and 2.1% smoke emission compared to 23°CA bTDC [71]. Thermal barrier coated dual fuel engine is used to reduce the smoke emissions [66]. An increase in CO<sub>2</sub> fraction reduces NO<sub>x</sub> and smoke but, increases HC and CO emissions [67]. An increase of compression ratio and injection timings in rice



bran biodiesel based dual fuel engine reduces CO and HC emissions and increases CO<sub>2</sub> and NO<sub>x</sub> emissions [72, 73]. A summary of the effects of increasing biogas flow rate on various combustion, performance, and emission parameters vis-à-vis conventional diesel operation is presented in Table 4.

Table 4. Effect of increasing biogas flow rate on engine parameters in dual fuel mode.

Parameter	Effect	References
Ignition delay	Increases	[32, 33, 50]
Maximum heat release rate	Increases	[32, 33, 50]
Cylinder Pressure	Increases	[32, 33, 50]
Exhaust Temperature	Decreases	[58]
Brake Thermal Efficiency	Decreases	[31, 50]
Specific Brake Fuel Consumption	Increases	[31, 50]
Volumetric Efficiency	Decreases	[60]
NO <sub>x</sub> Emission	Decreases	[50, 53, 62]
Particulate Matter	Decreases	[50, 53, 62]
HC Emission	Increases	[50, 53, 62]
CO Emission	Increases	[50, 53, 62]
Combustion Duration	Decreases	[58]
Fuel Energy Conversion Efficiency	Same	[64]
Combustion efficiency	Increases	[63]
Lean Limit	Increases	[31, 50]
Flame Speed	Decreases	[31, 50]
BSEC	Increases	[82]

### HCCI Engine

An alternative approach for using biogas in a CI engine is the Homogeneous Charged Compression Ignition (HCCI) mode. This has emerged as a promising concept combining the benefits of SI and CI engines [83]. Biogas can be effectively used in the HCCI mode by introducing it into the intake manifold. This allows the fuel and air to be completely mixed prior to combustion and the mixture auto-ignites as a result of the temperature rise during the compression stroke. HCCI engines offer high thermal efficiencies on account of low equivalence ratios and rapid energy release. These conditions also ensure low NO<sub>x</sub> and particulate emissions [83]. In spite of these benefits, a major drawback of HCCI engines is that the user has no direct control over the onset of combustion unlike conventional SI or CI engines. Various means of controlling combustion such as pilot diesel injection, spark, charge preheating, exhaust gas recirculation (EGR), fast thermal management, turbocharging, fuel reactivity control, and variable compression ratio have been employed [83-86].

### Combustion Indices

The research groups [53, 54, 87] (2007, 2009, and 2010) studied the performance of an HCCI engine when fuelled with diesel and with a biogas-diesel mixture. A comparison with biogas-diesel dual fuel mode was also presented. In the diesel HCCI case, in-cylinder injection timing was varied from 5° bTDC to 20° aTDC during suction. Stable operation was achieved only for injection after TDC during suction. BMEP was varied in the range of 2.15 to 4.32 bar. Very high heat release rates were observed at higher BMEP conditions because of rapid combustion [87]. In the biogas-diesel HCCI mode,

manifold injection was employed for both fuels. Biogas ratio, charge temperature and BMEP were varied. It was found that the presence of CO<sub>2</sub> and higher self-ignition temperature of CH<sub>4</sub> increased the ignition delay. Subsequent heat release rate was found to be within safe limits compared to the diesel HCCI mode. Lower amount of biogas produced knocking and higher amounts led to misfire [53, 54]. Biogas-diesel HCCI operation provided higher heat release rates compared to biogas-diesel dual fuel mode for the same biogas:diesel ratio.

Ibrahim et al. [30] investigated biogas-diesel PPCCI (predominantly premixed charge compression ignition) mode. Biogas was inducted and in-cylinder diesel injections with very advanced timings were employed to attain conditions similar to HCCI. The effects of injection timing, intake charge temperature, and biogas energy ratio were studied. The best injection timing, intake charge temperature, and biogas energy ratio were found to be 55-70 ° BTDC, 50 – 90 °C. and 80%, respectively. By advancing the diesel injection timing, the homogeneity of the lean mixtures was enhanced. This resulted in delayed combustion and lower energy release rates [30].

The effects of charge temperature, boost pressure, and equivalence ratio were investigated by Bedoya et al. [55] using a biogas fuelled 4-cylinder engine in HCCI mode. It was reported that higher inlet pressures and temperatures reduce the self-ignition temperature and provide higher burning rates [56]. Jun and Iida [88] reported that increasing the in-cylinder temperature improves the combustion efficiency. An increase in CO<sub>2</sub> fraction of biogas enhances the BMEP without the adverse effect of knocking [89].

### ***Performance Indices***

Compared to conventional CI mode, thermal efficiency is lowered by nearly 40% in the diesel HCCI mode because of wall wetting and improper combustion phasing [87]. While the use of biogas normally causes a drop in thermal efficiency in both SI and CI engines, it is observed to maintain high thermal efficiency in HCCI mode [54]. Swaminathan et al. [53] showed that biogas-diesel HCCI mode offers poorer brake thermal efficiency compared to dual fuel mode in general but the efficiency can be improved by preheating the intake to about 135°C and using higher biogas energy ratios. The highest brake thermal efficiency in PPCCI mode was obtained with a biogas energy ratio of 80% [30]. Power output and indicated efficiency can be enhanced by increasing inlet pressure and charge temperature for lean mixtures [56]. Sudheesh and Mallikarjuna [52] explored the use of diethyl ether (DEE) as an ignition improver for biogas combustion in HCCI engines. They showed that biogas-DEE in HCCI mode offers wider operating load range and higher brake thermal efficiency at all loads compared to biogas-diesel dual fuel and biogas SI operation. Different strategies have been experimentally evaluated by Bedoya et al. [55] in order to extend the operating range of a biogas fuelled HCCI engine and ensure safe operation and stable combustion. Oxygen enrichment at constant biogas flow rates and gasoline pilot injection were separately tested at the low load limit. Delayed combustion phasing was tested at high load limit. The operating range of equivalence ratios for stable combustion was identified as 0.2 - 0.5. Employing a free piston arrangement has been proposed as a strategy to enable the use of extremely lean mixtures in HCCI engines [90].

### ***Emission indices***

Swaminathan et al. [87] noted that compared to conventional CI operation, NO<sub>x</sub> emissions were lower in diesel HCCI mode. This is attributed to lower operating

temperatures in the latter case. However, diesel HCCI mode had higher smoke, HC, and CO emissions. Impingement of the fuel on the cylinder wall leading to non-homogeneous mixtures and improper combustion was pointed out as the major reasons for the increase in emissions. Higher HC emissions could also be the result of the fuel escaping through the exhaust port during the valve overlap period at advanced injection timings. In subsequent studies, they showed that biogas-diesel HCCI mode has lower  $\text{NO}_x$  and smoke compared to dual fuel and CI modes [53, 54]. Considering both performance and emission aspects, they recommended CI, biogas-diesel HCCI, and dual fuel operation for low, moderate, and high loads respectively. On brake specific basis, NO, smoke, HC, and CO in PPCCI mode were found to be comparable to those of dual fuel mode [30]. Low HC and CO emissions were reported for lean mixtures at increased inlet temperature and charge pressure [55]. Jun and Iida [88] observed that CO emissions can be reduced by increasing in-cylinder temperature in natural gas-based HCCI engines. Biogas in HCCI mode produces lower HC emissions compared to SI mode [52]. Kozarac et al. [91] reported that biogas-based HCCI engine with n-heptane as ignition promoter lowers  $\text{NO}_x$  emission. Reducing methane fraction in biogas leads to better BHC emission [89].

### **Simulation**

Simulation of the IC engine operating cycle helps us in gaining better understanding of the effects of various physicochemical parameters on performance and emissions. The mathematical models used in simulations can be classified as single-zone, multi-zone, probability-based, and multi-dimensional models [8]. Compared to the large number of articles in published literature dealing with the modelling of conventional engines, works pertaining to dual fuel and HCCI engines, particularly those operated on biogas are scarce. The following paragraph summarises simulation methodologies of various degrees of complexity followed for dual fuel and HCCI engines in general.

For the closed part of the cycle, the simplest approach is to use a zero-dimensional single zone model. Such a model has been developed for diesel [92] and natural gas [93]. One of the major drawbacks of these models is that the underlying assumption of uniform gas temperature reduces the accuracy of prediction of heat release rate, duration of combustion, and emissions. This can be overcome to an extent by employing quasi-dimensional or multi-zone models. Here the cylinder contents are divided into two or more finite number of homogeneous zones, each having uniform composition and thermodynamic state. Heat, work, and mass exchanges between zones are also accounted for. While quasi-dimensional models combine accuracy with computational efficiency, one drawback is their inability to describe mixture stratification/heterogeneity, which requires specification of the conditions within each zone. In the CFD models, the requisite governing equations are solved for all the zones or cells, providing a more accurate but computationally expensive solution. Two CFD-based approaches exist. In the first one, the CFD code solves the governing equations without considering chemical reactions. The velocity and temperature fields thus predicted provides the input to an equivalent multi-zone model which uses a chemical kinetics solver to update the temperature and species concentration [94]. Alternatively, a simultaneous solution of all governing equations can be performed in the CFD solver considering reaction kinetics in all cells [95]. Computational requirements can be minimised by employing reduced reaction mechanisms [96]. CFD models are also classified as 2D [97] and 3D [94-96, 98-100]. Mosbach et al. [101] used a stochastic

reactor model based on probability density functions (PDFs) to study the HCCI combustion of biofuel blends.

Visakhamoorthy et al. [102] used a multi-zone model to predict the pressure history, energy release, and emissions in a diesel engine adapted to operate on simulated biogas in HCCI mode. The multi-zone model comprises an interior core surrounded by nine annular zones. Simulation was carried out from IVC to EVO using a parallelised Fortran code. The zones were treated as stirred constant volume reactors wherein the chemical kinetics was modelled using CHEMKIN. They reported good predictions of pressure history and energy release rate, except close to the misfire limit. Awate et al. [103] carried out numerical simulation of an HCCI engine using a zero dimensional single zone model and CHEMKIN. They studied the effects of initial temperature, equivalence ratio, engine speed, and compression ratio on ignition timing and peak pressure.

## **CONCLUSIONS**

Biogas holds several advantages as an alternative fuel. In order to make it viable for use in engines, biogas needs to be purified by removing its non-combustible constituents such as CO<sub>2</sub> - a process known as methane enrichment. Various techniques used for purifying biogas have been explained and their pros and cons summarised. The state of the art in the utilisation of biogas in CI engines in dual fuel and HCCI modes and the influence on performance and emissions were discussed in the light of existing literature and compared to the trends of conventional diesel fuelled CI engines. Simulation methodologies pertinent to dual fuel and HCCI operating modes were also reviewed. Advanced biogas purification techniques are such as nanotechnology based membranes and cryogenic separation, development of on-board purification techniques to improve the viability of biogas as an automotive fuel, HCCI engines operated on biogas, simulation of biogas fuelled engines, and combustion control methods for HCCI engines.

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