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A Robust Two-Equation Model for Transient-Mixed Flows

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Abstract

A finite volume model was built upon earlier work with the aim of simulating free surface flows, pressurized flows and their simultaneous occurrence (mixed flows) in single-liquid and two-phase flow conditions (entrapment and release of air pockets). The model presented herein is based on a two-governing equation model. Three main contributions are presented herein, namely: (1) the ability of the proposed model to simulate mixed flows without restriction of the flow type in the free surface region (e.g., supercritical flow), (2) extension of our single-phase flow model for simulating the entrapment and release of air pockets, and (3) formulation of an approach for handling numerical instabilities that may occur during numerical pressurization of the flow. The model presented herein is robust and simulates any transient-mixed flow condition for realistic pressure wave celerities.

Keywords: Air entrapment, air pockets, air release, mixed flow, open channel flow, pressurized flow, sewer, transient flow, two-phase flow, unsteady flow

1 Introduction

The simultaneous occurrence of free surface and pressurized flows (mixed flows) are simulated using one or two sets of governing equations (e.g., Capart *et al.* 1997, Trajkovic *et al.* 1999, León 2006, Vasconcelos *et al.* 2006, Politano *et al.* 2007, or León *et al.* 2009a). Mixed flow models that use only the single set of the Saint-Venant equations require an approximation for simulating pressurized flows. The most common approximation is the well-known Preissmann slot, which consist of a hypothetical narrow open-slot on top of the conduit (Capart *et al.* 1997, or Trajkovic *et al.* 1999). The main limitation of this model is its inability to simulate sub-atmospheric pressures in pressurized flow conditions. To overcome this limitation, Vasconcelos *et al.* (2006) modified the Saint-Venant equations to allow for over-pressurization, assuming that elastic behavior of the pipe walls will account for the gain in pipe storage. The main limitation of this approach is the presence of what these authors call “post shock oscillations” near open channel-pressurized flow interfaces. To keep these oscillations small, lower values for the pressure wave celerity may be used, yet this may compromise the simulation accuracy if pressurized transients are simulated. It is cautioned that numerical oscillations may produce unrealistic negative pressures and pollute the numerical solution.

Mixed flow models that are based on a one single set of governing equations use small values of the pressure wave celerity to avoid numerical instabilities (Trajkovic *et al.* 1999, or Vasconcelos *et al.* 2006). Good results are obtained when simulating mixed flows in a single pipe, in which the pressurized flow region is isolated and there is no interaction of pressurized waves (Trajkovic *et al.* 1999, Vasconcelos *et al.* 2006, or León *et al.* 2009a). However, as shown by León *et al.* (2009b), if there is interaction of pressurized waves, such as in multiple pipe flow, the results highly depend on the selection of the pressure wave

celerity. As discussed by León and Ghidaoui (2009), numerical oscillations in pipe filling bores can be minimized for realistic wavespeeds (e.g., ~ 1000 m/s) by choosing governing equations that best mimic the physics. The flow regime on one side of the filling bore is pressurized flow, while that on the other side is free surface flow. Hence, an appropriate approach enforces the waterhammer equations in the pressurized region, the Saint Venant equations in the free surface region and the jump relations across the filling bore.

Among the approaches for simulating mixed flows (single-phase flows), Finite Volume (FV) shock-capturing methods, in particular Godunov-Type Schemes (GTS), are gaining popularity for their ability to capture shocks in the solution automatically, without explicitly tracking them (Nujic 1995, Sanders 2001, or Toro 2001). These schemes were applied to the Saint-Venant equations and the two governing equations (Saint-Venant equations and compressible waterhammer equations). As mentioned above, a two-governing equation model must be used for simulating complex closed-conduit systems for transient mixed flows with a pressure wave celerity of ~ 1000 m/s. Regarding single-phase mixed flow models based on the application of FV schemes to both the Saint-Venant equations and the compressible waterhammer equations (two sets of governing equations), the present authors are aware of only two FV models, namely these of León (2006) and of Bourdarias and Gerbi (2007). León (2006) presented a shock-tracking-capturing method, in which open channel-pressurized flow interfaces are tracked, introducing or merging cells as the interfaces propagate in the pipe. The compatibility conditions are enforced across open channel-pressurized flow interfaces, and a shock-capturing approach is used in pure free surface and pressurized flows.

Bourdarias and Gerbi (2007) presented a shock-capturing approach for simulating mixed flows, in which the governing equations for free surface and pressurized flows were linearized. For a positive open channel-pressurized flow interface, the mass and momentum compatibility conditions were enforced across the mixed flow interface together with the Rankine-Hugoniot mass conservation condition across a linearized wave in the pressurized flow region. For negative interfaces, besides the equations used for positive interfaces, the energy equation was enforced across the interface and a linearized open channel flow Riemann problem was solved using the well-known linearized Riemann solver (Toro 2001, León *et al.* 2006, or León 2006). Song *et al.* (1983) defined an open channel-pressurized (mixed) flow interface as positive if it is moving towards the open-channel flow (Fig. 1 a), and negative if it is moving towards the region of pressurized flow (Fig. 1 b). The directional interface change from positive to negative is called interface reversal (Fig. 1 c). Bourdarias and Gerbi (2007) also used the linearized Riemann solver for computing the flow variables in the free surface and pressurized flow regions. As pointed out by Toro (2001), the linearized Riemann solver for free surface flows is not sufficiently robust to be generally used. In particular, this solver may give negative depths in cases involving strong rarefactions leading to very shallow water. Furthermore, the approach proposed by Bourdarias and Gerbi (2007) for negative interfaces (mixed flow) was formulated only for subcritical free surface flow. Thus, a model is desired with capabilities of simulating mixed flows without restriction of flow type in the free surface region (e.g., supercritical flow).

When using a two-governing equation model and simulating a pure free surface flow that is about to get pressurized, numerical instabilities, which may lead to program abortion, may occur, especially if pipe filling is slow. Numerical instabilities occur because of singularities in the equations for numerical pressurization of the flow. For instance, the wave speed of a mixed flow interface is singular at the threshold for changes from free surface to pressurized flow. If the piezometric heads of the free surface and the pressurized flows are similar, numerical instabilities may occur. These instability problems are increased due to the precision of the computer used. The lower the precision used the more instability problems are attained. To make a model robust, the instability problems due to numerical flow pressurization need to be addressed.

With regard to two-phase flow models (entrapment and release of air pockets) based on the application of FV schemes to both the Saint-Venant equations and the compressible waterhammer equations, no model appears to be currently available. This work is organized as follows: (1) governing equations for single and two-phase flow conditions are provided, (2) numerical solution of mixed flow interfaces is presented, (3) threshold levels for piezometric depths during numerical pressurization is presented, (4) accuracy and robustness of the proposed model are evaluated using experimental literature data, and (5) results are summarized.

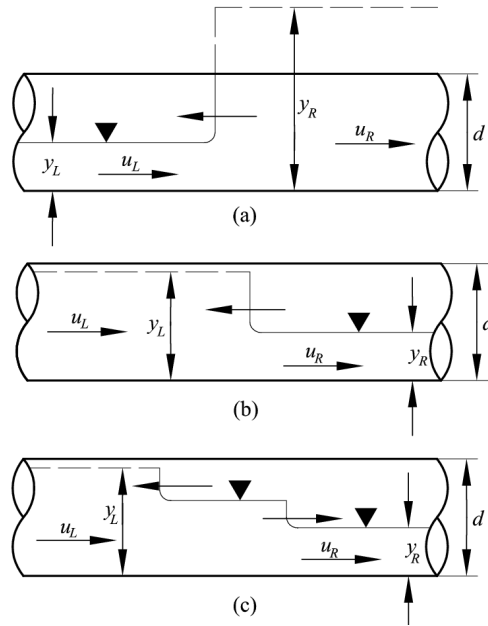


Figure 1 (a) Positive interface moving in upstream direction, (b) Negative interface moving in upstream direction, (c) Interface reversal

2 Mathematical description

2.1 Governing equations for free surface and pressurized flows

The governing equations used herein are identical to those of León (2006) for single-phase flows, except for the air-phase. In the single-phase flow model, the free surface region is simulated using the 1D Saint-Venant equations and the pressurized region is simulated using the 1D compressible waterhammer equations. The inclusion of the air-phase in the Saint-Venant equations is similar to the approach used by Arai and Yamamoto (2003) and Vasconcelos (2005). These equations are

$$\frac{\partial \mathbf{U}}{\partial t} + \frac{\partial \mathbf{F}}{\partial x} = \mathbf{S} \quad (1)$$

in which the vector variable \mathbf{U} , the flux vector \mathbf{F} and the source term vector \mathbf{S} for open-channel flows may be written as (León 2006, León *et al.* 2006)

$$\mathbf{U} = \begin{bmatrix} \rho_w A \\ \rho_w Q \end{bmatrix}, \quad \mathbf{F} = \begin{bmatrix} \rho_w Q \\ \rho_w \frac{Q^2}{A} + A \bar{p} + \rho_w g A_f H \end{bmatrix} \quad \text{and} \quad \mathbf{S} = \begin{bmatrix} 0 \\ (S_o - S_e) \rho_w g A \end{bmatrix} \quad (2)$$

For compressible water hammer flows these are (Guinot 2003, León 2006, León *et al.* 2008)

$$\mathbf{U} = \begin{bmatrix} \rho_f A_f \\ \rho_f Q \end{bmatrix}, \quad \mathbf{F} = \begin{bmatrix} \rho_f Q \\ \rho_f \frac{Q^2}{A_f} + A_f p \end{bmatrix} \quad \text{and} \quad \mathbf{S} = \begin{bmatrix} 0 \\ (S_o - S_e) \rho_f g A_f \end{bmatrix} \quad (3)$$

where the variables for free surface flows are A = cross-sectional flow area, Q = flow discharge, \bar{p} = average pressure of water column over the cross sectional area, H = gauge air pressure head, ρ_w = liquid density (assumed constant for free surface flows but not for pressurized flows), g = gravitational acceleration, S_o = slope of channel bottom, and S_e = slope of energy line. The variables for compressible water hammer flows (pressurized flows) are A_f = full cross-sectional conduit area, p = pressure acting on gravity center of A_f , and ρ_f = fluid density for compressible water hammer flows. For single-phase flow conditions (liquid only), $H = 0$ and the term $\rho_w g A_f H$ in Eq. (2) is dropped.

Equation (1) for compressible water hammer flows does not form a closed system because the flow is described using the three variables ρ_f , p and Q but only two equations are available. To close this system, the following equation relating p and ρ_f is used (León *et al.* 2007, 2008)

$$p = p_{ref} + a^2(\rho_f - \rho_{ref}) \quad (4)$$

where a = pressure wave celerity in single-phase flow conditions, ρ_{ref} and p_{ref} = reference density and reference pressure, respectively. The reference state (subscript *ref*) is defined at the phase change from free surface to pressurized flow, for which all flow parameters in both free surface and pressurized flow regime are identical. Note from Eq. (2), that the only variable associated with the air phase is the gauge air pressure head H , which computation for no air release and air release conditions is presented next.

2.2 No air release

Considering an isolated air pocket, the ideal gas law with the assumption of an isentropic process gives (e.g., Martin 1976)

$$\frac{dH}{dt} = -k \frac{H^*}{V} \frac{dV}{dt} \quad (5)$$

where H = absolute air pressure head, V = volume of air pocket and k = heat capacity ratio, $H^* = H + H_b^*$, where H_b^* = atmospheric pressure head.

For a confined air pocket with no air-release, Eq. (5) can be used to compute H required to estimate F in Eq. (2). To determine H , the volumetric change of an air pocket with time dV/dt needs to be determined. It is computed using the net flow discharge flux evaluated at the air pocket boundary as (Fig. 2)

$$\frac{dV}{dt} = Q_{r+1/2} - Q_{j-1/2} \quad (6)$$

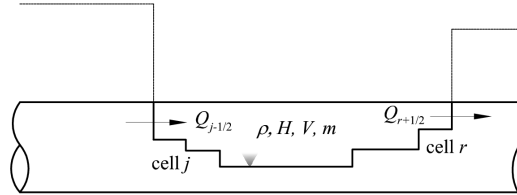


Figure 2 Sketch of confined air pocket

Note from Fig. 2 that the fluxes at cell interfaces inside the air pocket other than the boundaries cancel each other. Previous approaches used the speed of open channel-pressurized flow interfaces surrounding an air pocket for computing dV/dt (Wang *et al.* 2003, or Vasconcelos 2005). Tests with the proposed model using the latter approach lead to numerical oscillations and eventually the abortion of the program. These oscillations are caused by the extremely sensitive speed of the interface that changes rapidly, especially in fast pipe filling scenarios. Conversely, the approach of computing dV/dt using Eq. (6) leads to a robust model virtually free of numerical oscillations. If Eq. (6) is used, numerical instabilities may still be present due to other reasons such as the numerical scheme used for solving the governing equations, however the instabilities due to air volume computation are reduced. For computing air density, the air pocket volume at the new time step is updated as $V^{n+1} = V^n + dt(dV/dt)$. The new air density is computed using this new air pocket volume.

2.3 With air release

Considering air release, Eq. (5) can be modified to take into account the air flow discharge out of an air pocket. This new relation is (Martin 1976, or Zhou 2000)

$$\frac{dH}{dt} = -k \frac{H^*}{V} \frac{dV}{dt} + k \frac{H^*}{m} \frac{dm}{dt} \quad (7)$$

where m = mass of air with the mass flow rate given by

$$\frac{dm}{dt} = C_d Y \rho_a A_o \sqrt{2g \frac{\rho}{\rho_a} (H^* - H_b^*)} \quad (8)$$

where C_d = discharge coefficient, ρ_a = density of air, A_o = area of orifice and Y = expansion factor given by (Martin 1976, or Zhou 2000)

$$Y = \sqrt{\frac{k}{k-1} \left(\frac{H_b^*}{H^*} \right)^{\frac{2}{k}} \frac{1 - \left(\frac{H_b^*}{H^*} \right)^{\frac{k-1}{k}}}{1 - \frac{H_b^*}{H^*}}} \quad (9)$$

If $H^*/H_b^* > 1.89$, the orifice is choked and (Martin 1976)

$$\frac{dm}{dt} = \rho_a C_d A_o \sqrt{g \frac{\rho}{\rho_a} H^*} \sqrt{k \left(\frac{2}{k+1} \right)^{\frac{k+1}{k-1}}} \quad (10)$$

For the case of air release, dV/dt can be computed in the same way as for no air release. For computing air density, the mass of air inside the air pocket at the new time step is updated according to the air flow discharge. The new air density is computed using this new air mass and the new air pocket volume.

Free surface flow tests in circular pipes (Hamam and McCorquodale 1982) demonstrated that flow instabilities occur for piezometric depths greater than $0.8d$, causing oscillations that lead with a sudden jump to pressurized flow. As mentioned above, the phase change from free surface to pressurized flow (not from pressurized to free surface flow) is assumed to occur if the piezometric depth exceeds $y = y_{ref}$, where y = piezometric depth and y_{ref} = reference depth. Herein, $y_{ref} = 0.95d$. Note that the results are not significantly sensitive to y_{ref} . However, when using a small value of y_{ref} , large mass conservation errors may occur. The reference area A_{ref} is the hydraulic area below $y_{ref} = 0.95d$ and A_f in the previous equations is replaced with A_{ref} . This results in a reduction of the hydraulic area for pressurized flows of less than 2%. If using the present model to simulate pure pressurized flows, A_{ref} can be set equal to A_f . The reduction in hydraulic area for pressurized flows of less than 2% is then eliminated. For the phase change from pressurized to free surface flow, the criterion of Yuan (1984) is used.

The above presented governing equations relate to free surface and pressurized flows. Consider now an interface between free surface and pressurized flow regions moving with a speed w . The weak form of Eq. (1) is (Toro 2001)

$$w\Delta\mathbf{U} + \Delta\mathbf{F} = 0 \quad (11)$$

where Δ = jump across the interface. Denoting by subscript L the state variables to the left and by R the state variables to the right of the interface, and assuming that the flow to the left of the interface is free surface and pressurized to the right, the weak form of Eq. (1) is

$$w[(\rho_f A_f)_R - (\rho_w A)_L] = (\rho_f Q)_R - (\rho_w Q)_L \quad (12)$$

$$w[(\rho_f Q)_R - (\rho_w Q)_L] = (\rho_f \frac{Q^2}{A_f} + A_f p)_R - (\rho_w \frac{Q^2}{A} + A\bar{p} + \rho_w g A_f H)_L \quad (13)$$

The flow variables used herein are $(\rho_w A)$ and $(\rho_w Q)$ for free surface flows, and $(\rho_f A_f)$ and $(\rho_f Q_f)$ for pressurized flows. However, the engineering community prefers to use the piezometric head h and discharge Q . The latter variables can be determined from the flow variables as

- Free surface flow

$$\begin{aligned} h &= y & (y \text{ is a geometric function of } A) \\ Q &= (\rho_w Q) / \rho_w \end{aligned} \quad (14)$$

- Pressurized flow

$$\begin{aligned} h &= y_{ref} + \frac{a^2}{g} \left(\frac{\rho_f A_f}{\rho_{ref} A_{ref}} - 1 \right) \quad (\text{where } \rho_{ref} = \rho_w) \\ Q &= \frac{(\rho_f Q_f)}{(\rho_f A_f)} A_f \end{aligned} \quad (15)$$

where h is measured from the conduit bottom. For convenience, subscripts “ f ” and “ w ” are now dropped.

After a given node has been pressurized, free surface flow is not necessarily generated at this node if its head drops below the pipe crown. As reported by Cardle (1984), Yuan (1984), or Cardle *et al.* (1989), there is a negative pressure on the pressurized side of the interface in negative interfaces. The latter implies that if a pipe system has been fully pressurized, the only way to start the depressurization process is through ventilated boundaries by dropshafts or reservoirs [e.g., Cardle 1984].

3 Numerical solution of mixed flow interfaces

3.1 Overview

A part of our model for simulating mixed flows only is presented. For pure free surface and pressurized single-phase flows the reader is referred to León (2006) and León *et al.* (2006, 2008). A mixed flow is composed of one region in free surface flow and another adjacent in pressurized flow conditions. The numerical scheme used for updating the solution from one time step to the next for mixed flows is the same as presented by León (2006) and León *et al.* (2006, 2008) for free surface and pressurized flows. This scheme is an explicit FV method first-order accurate near shocks and discontinuities and second-order accurate away from discontinuities. When using the FV scheme, to update the flow variables U at cell “ i ” from a time step to the next the numerical flux F at the cell interfaces $i-1/2$ and $i+1/2$ need to be estimated. For computing vector F in Eqs. (2) or (3), the flow variables at the cell interface $[(\rho A)_{i+1/2}$ and $(\rho Q)_{i+1/2}]$ need to be estimated. This section focuses on the computation of these if the flow regime at the sides of the cell interface $i+1/2$ are different. If the flow regime changes across the cell interface, it is named herein mixed flow interface. The approach used herein for estimating the flow variables is similar to that used by Song *et al.* (1983), Cardle (1984), Cardle and Song (1988), or Bourdarias and Gerbi (2007). Note that the treatment of boundary conditions is not presented herein due to space limitations. The reader is referred to León *et al.* (2009b).

3.2 Positive interface propagating upstream

In this case a mixed flow interface is moving upstream towards the open-channel flow region. The treatment for such a positive interface propagating downstream is identical to this case but will not be presented. The flow across a positive interface is equivalent to a flow across a hydraulic bore or, in compressible gas flow, a shock, which means that the flow changes from supercritical or supersonic to subcritical or subsonic flow as it moves in relative coordinates (Cardle 1984). A classical statement in hydraulics used in the video “Waves in fluids” (Bryson 1964) reads: “A disturbance behind a shock moving towards the shock interface catches up with it and disturbances in front of the shock are overtaken by it”. This statement is simply that the Froude (Mach) number behind a shock < 1 and ahead of it > 1 . By making use of this classical statement the $x-t$ diagram for a positive interface having subcritical flow in the free surface region was constructed (Fig. 3), similar to the diagram of Song *et al.* (1983), or Cardle and Song (1988).

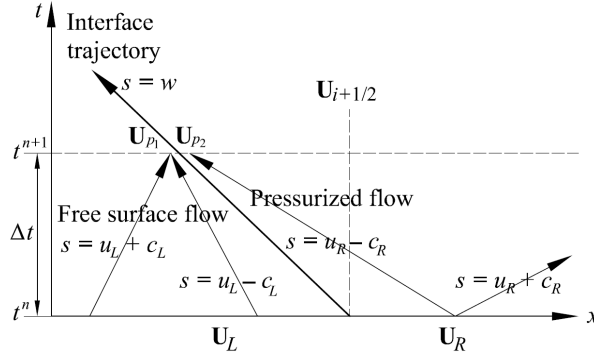


Figure 3 x - t diagram for a positive interface propagating upstream

Recall that the flow variables at the cell interface $i+1/2$ at time t^{n+1} ($\mathbf{U}_{i+1/2}^{n+1}$) are sought to compute the fluxes at this interface. In Fig. 3, the flow variables at left and right of the cell interface $i+1/2$ at time t^{n+1} are \mathbf{U}_{p1}^{n+1} and \mathbf{U}_{p2}^{n+1} , respectively. Because a shock-capturing approach is used, the location of the moving mixed flow interface and that of the cell interface separating the free surface and pressurized flow cells (fixed grid) are identical at time t^n . The flow variables at $i+1/2$ and time t^n are \mathbf{U}_L^n and \mathbf{U}_R^n , respectively. These flow variables at time t^n are already known from the previous time step computations. To estimate $\mathbf{U}_{i+1/2}^{n+1}$, only \mathbf{U}_{p2}^{n+1} need to be determined because $\mathbf{U}_{i+1/2}^{n+1} = \mathbf{U}_{p2}^{n+1}$. However, \mathbf{U}_{p2}^{n+1} is related to \mathbf{U}_{p1}^{n+1} and w^{n+1} . Thus, to determine $\mathbf{U}_{i+1/2}^{n+1}$ the five variables $(\rho A)_{p1}^{n+1}$, $(\rho Q)_{p1}^{n+1}$, $(\rho A)_{p2}^{n+1}$, $(\rho Q)_{p2}^{n+1}$, and w^{n+1} need to be estimated. The number of variables needed can be reduced in two as is shown next.

The application of the concept of Riemann invariants along the characteristics $u_L + c_L$ and $u_L - c_L$ in Fig. 3, respectively, gives (León *et al.* 2006)

$$\begin{aligned} u_L^n + \phi_L^n &= u_{p1}^{n+1} + \phi_{p1}^{n+1}, \text{ along } dx/dt = u_L + c_L \\ u_L^n - \phi_L^n &= u_{p1}^{n+1} - \phi_{p1}^{n+1}, \text{ along } dx/dt = u_L - c_L \end{aligned} \quad (16)$$

where $\theta = 2\arccos(1-2y/d)$ and ϕ is (León *et al.* 2006)

$$\phi = \sqrt{g \frac{d}{8}} \left[\sqrt{3} \theta - \frac{\sqrt{3}}{80} \theta^3 + \frac{19\sqrt{3}}{448000} \theta^5 + \frac{\sqrt{3}}{10035200} \theta^7 + \frac{491\sqrt{3}}{27 \times 7064780800} \theta^9 + \dots \right] \quad (17)$$

In the system of Eqs. (16) $\mathbf{U}_{p1}^{n+1} = \mathbf{U}_L^n$ and $\phi_{p1}^{n+1} = \phi_L^n$. Because $\mathbf{U}_{p1}^{n+1} = \mathbf{U}_L^n$, only the three variables $(\rho A)_{p2}^{n+1}$, $(\rho Q)_{p2}^{n+1}$, and w^{n+1} are needed to determine $\mathbf{U}_{i+1/2}^{n+1}$. Since three equations are required the equations of conservation of mass, momentum and energy across the mixed flow interface can be used. However, from Fig. 3, p_2 and R are connected by the characteristic $u_R - c_R$ and therefore, one equation must relate p_2 to R . Because it is difficult to quantify the energy losses in the conservation of energy equation, the equations of conservation of mass and momentum are used, namely Eqs. (12) and (13), where subscripts L and R must be replaced by p_1 and p_2 , respectively (Fig. 3). To obtain the third equation, the concept of Riemann invariants is enforced along the characteristic $s = u_R - c_R$ (Fig. 3), which gives

$$u_R^n - a \ln(\rho A)_R^n = u_{p2}^{n+1} - a \ln(\rho A)_{p2}^{n+1} \quad (18)$$

The derivation of Eq. (18) is similar to that presented for Eqs. (8) and (9) by León *et al.* (2006) using the constant a instead of c .

To reduce the number of equations by one, w was eliminated from Eqs. (12) and (13). For solving the resulting two equations, the Newton-Raphson method for nonlinear systems of equations was used. When implementing this approach for actual storm-sewer systems, the Newton-Raphson method may not always converge. In those cases a set of adaptive and more robust solvers such as HOMPAC or MINPACK may be needed. Having thus determined \mathbf{U}_{p2}^{n+1} [$(\rho A)_{p2}^{n+1}$ and $(\rho Q)_{p2}^{n+1}$] and therefore $\mathbf{U}_{i+1/2}^{n+1}$ ($\mathbf{U}_{i+1/2}^{n+1} = \mathbf{U}_{p2}^{n+1}$), the flux at the cell interface $i+1/2$ can be determined using the flux vector term in Eq. (3).

For a supercritical free surface flow moving in the downstream direction, the concept of Riemann

invariants along the characteristics $u_L + c_L$ and $u_L - c_L$ in Fig. 3 can still be applied and as for subcritical flows $U_{p1}^{n+1} = U_L^n$. The latter means that for a positive interface, the flux at the cell interface does not depend on the flow type in the free surface region.

3.3 Negative interface propagating upstream

In this case a negative mixed flow interface is moving upstream towards the pressurized flow region (Fig. 1 b). The treatment for a negative interface propagating downstream is identical and will not be presented. It is noted from Fig. 1 (b), that the propagation of a negative interface results in the depressurization of the pressurized region. However, as mentioned earlier, depressurization does not occur if the piezometric head on the pressurized region drops below the pipe crown (Cardle 1984, Yuan 1984, or Cardle *et al.* 1989), but if the piezometric depth drops below a threshold value. For circular conduits this is about $0.84d$ (Yuan 1984). Notice that the threshold value for depressurization is different to that of pressurization. Herein the pressurization of the free surface region is assumed to occur if the piezometric head exceeds $y = y_{ref}$.

In a similar way to the case of a positive interface, the x - t diagram for a negative interface propagating upstream is shown in Fig. 4. Notice that the negative mixed flow interface overtakes the pressurized flow waves and that the free surface flow waves do not interact at all with the negative interface. These characteristics of a negative interface are different to those of a positive interface (shock-wave).

A reader familiar with the solution of a Riemann problem can notice from Fig. 4 that to estimate $U_{i+1/2}^{n+1}$, only U_{p2}^{n+1} need to be determined. The reason is that if U_{p2}^{n+1} is known, an open-channel flow Riemann problem can be solved to estimate $U_{i+1/2}^{n+1}$ using as left, intermediate and right states, U_{p2} , U_* (star region) and U_R , respectively (e.g., Toro 2001, León *et al.* 2006). However, U_{p2}^{n+1} is related to U_{p1}^{n+1} and w^{n+1} . Thus, five variables [$(\rho A)_{p1}^{n+1}$, $(\rho Q)_{p1}^{n+1}$, $(\rho A)_{p2}^{n+1}$, $(\rho Q)_{p2}^{n+1}$, and w^{n+1}] need to be determined, and naturally five equations are required to determine these variables. In a way similar to the positive interface, the first two equations are obtained by enforcing the conservation of mass and momentum across the negative interface (Eqs. 12 and 13), where subscripts L and R must be replaced by p_1 and p_2 , respectively.

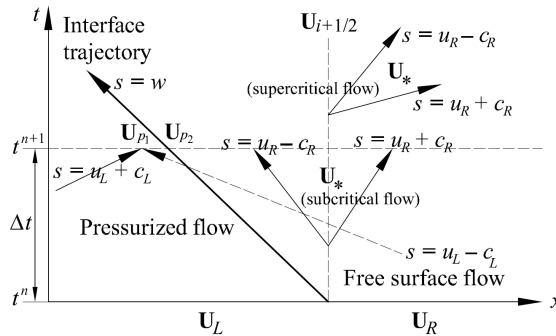


Figure 4 x - t diagram for a negative interface propagating upstream

Note from Fig. 4 that the concept of Riemann invariants can be enforced only along the characteristic $s = u_L + c_L$. The characteristics $s = u_R - c_R$ and $s = u_R + c_R$ do not connect p_2 and R , and the characteristic $s = u_L - c_L$ cuts the mixed flow interface, and therefore the concept of Riemann invariants can not be enforced along these characteristics. Thus, for a negative interface, only one extra equation is obtained with this concept along the characteristic $s = u_L + c_L$. This third equation is given by

$$u_L^n + a \ln (\rho A)_L^n = u_{p1}^{n+1} + a \ln (\rho A)_{p1}^{n+1} \quad (19)$$

The derivation of Eq. (19) is similar to that presented in Appendix 1 by León *et al.* (2006) using the constant a instead of c . Experimental results show that the speed of a positive and negative interfaces is nearly constant (e.g., Cardle 1984, Cardle *et al.* 1989). Thus it is common to estimate the interface speed w at time $n+1$ using flow variables at the previous time step n (Song *et al.* 1983 or Cardle and Song 1988). Since w^{n+1} is computed explicitly, only four variables [$(\rho A)_{p1}^{n+1}$, $(\rho Q)_{p1}^{n+1}$, $(\rho A)_{p2}^{n+1}$ and $(\rho Q)_{p2}^{n+1}$] need to be determined and consequently only one more equation is needed.

The energy equation across the interface was finally used as (Cardle 1984, Yuan 1984, Cardle and

Song 1988, Bourdarias and Gerbi 2007)

$$\frac{(u_{p_1} - w)^2}{2g} + h[(\rho A)_{p_1}] = \frac{(u_{p_2} - w)^2}{2g} + h[(\rho A)_{p_2}] + hl \frac{u_{p_1} - w}{|u_{p_1} - w|} \quad (20)$$

where hl = energy loss across a negative interface and $(u_{p_1} - w)/(|u_{p_1} - w|)$ gives its correct sign. Note that Eq. (20) is written for single-phase flows. If considering air pressurization, the term H must be included in the left or right sides of Eq. (20), depending on which region is in free surface flow conditions. As is typically assumed, $hl = 0$ in the proposed model. The energy loss across a negative interface is negligible because this wave is similar to an expansion wave which is known to have negligible losses. Having determined $(\rho A)_{p_2}^{n+1}$ and $(\rho Q)_{p_2}^{n+1}$, $(\rho A)_{i+1/2}^{n+1}$ and $(\rho Q)_{i+1/2}^{n+1}$ can be estimated by solving an open-channel flow Riemann problem using as left, intermediate and right states (Fig. 4) U_{p_2} , U_* and U_R , respectively (Toro 2001, or León *et al.* 2006). For solving this Riemann problem, several solvers are available, such as the HLL, the two-rarefaction wave approximation, the linearized solver, among others (Toro 2001, LeVeque 2002, León *et al.* 2006, León 2006). Herein the HLL solver was used because its robustness for near dry-bed flows and because it handles sub- and supercritical flows automatically (Toro 2001).

To show that effectively the HLL solver handles supercritical flows, consider for instance that the flow at the right of the mixed flow interface in Fig. 4 is supercritical moving to the right. In this case $U_{i+1/2}^{n+1}$ $[(\rho A)_{i+1/2}^{n+1}$ and $(\rho Q)_{i+1/2}^{n+1}]$ is equal to $U_{p_2}^{n+1}$ (Fig. 4), so that the flow variables at the cell interface $x_{i+1/2}$ are determined. Having thus determined $U_{i+1/2}^{n+1}$, the flux at the interface $i+1/2$ is determined using the flux vector term in Eq. (2) [free surface flows]. If the flow at the right of the mixed flow interface in Fig. 4 is subcritical, the flow variables in the intermediate region between the characteristics $s = u_R - c_R$ and $s = u_R + c_R$ need to be determined. The reader is referred to León *et al.* (2006) for the HLL method applied to circular conduits. Unlike other mixed flow models that were not formulated for negative interfaces if the flow in the free surface region is supercritical (Cardle 1984, Yuan 1984, Cardle and Song 1988, Bourdarias and Gerbi 2007), the proposed approach is able to simulate negative interfaces without restriction to the flow type in the free surface region.

4 Threshold levels for piezometric depths

As mentioned in the Introduction, when using a two-governing equation model and if simulating a pure free surface flow that is about to get pressurized, numerical instabilities, which may lead to program abortion, may occur, especially if pipe filling is slow. To overcome the numerical instabilities that may be produced during numerical pressurization ($y = y_{ref}$), two threshold levels are defined. These are $y = (1 - \text{tol}_1)y_{ref}$ and $y = (1 - \text{tol}_2)y_{ref}$ subjected to

$$(1 - \text{tol}_1)y_{ref} < (1 - \text{tol}_2)y_{ref} < y_{ref} \quad (21)$$

where by trial and error tol_1 was found between 10^{-3} and 10^{-8} and $\text{tol}_2 = 10^{-14}$ if using double precision in the computations. For computations double or higher precision is suggested. For achieving convergence due to tol_1 , first use a high value for tol_1 of e.g. 10^{-3} and then decrease gradually this value to e.g. 10^{-4} . If the solutions for two values of tol_1 are similar, then the solution has converged.

For illustrating the use of the two defined threshold levels, three cases, which are depicted in Figs. 5 (a), 5 (b) and 5 (c), are presented herein. For the first case illustrated in Fig. 5 (a) the flow at the old time step t^n in cell i and its adjacent cells $i-1$ and $i+1$ are in free surface regime. If after updating the solution to cell i for t^{n+1} , the piezometric depth in this cell falls between $(1 - \text{tol}_1)y_{ref}$ and y_{ref} , the flow in cell i at the new time step t^{n+1} remains in free surface flow conditions with a piezometric depth equal to $y = (1 - \text{tol}_1)y_{ref}$. For the second case illustrated in Fig. 5 (b) the flow at old time time step t^n in cell i and its adjacent cells $i-1$ and $i+1$ are identical as in the first case. If after updating the solution at cell i for t^{n+1} , the piezometric head exceeds y_{ref} , cell i at t^{n+1} is assumed to be pressurized (shaded region in Fig. 5 b). The third case, shown in Fig. 5 (c), corresponds to the pressurization of cell i adjacent to the positive interface ($i+1/2$). The flows at old time time step t^n in cells i and $i+1$ are in free surface and pressurized regime, respectively, and the positive interface $i+1/2$ is traveling to the left. Note that cell i (free surface flow conditions) may get pressurized due to the flow advected by the positive interface so that it may seem obvious that no constraint should be specified for the pressurization of this cell. However, if the piezometric head in cells i ($y < y_{ref}$)

and cell $i+1$ ($y > y_{ref}$) are similar, it may lead to numerical instabilities. Thus, if the piezometric head in cell i falls between $(1-\text{tol}_2)y_{ref}$ and y_{ref} , the flow in cell i at the new time step t^{n+1} remains in free surface flow conditions with a piezometric head equal to $y = (1-\text{tol}_2)y_{ref}$. Because tol_2 is very small, the constraint imposed does not affect significantly the accuracy of the results. As in the second case, if the piezometric head exceeds y_{ref} , the cell i at t^{n+1} is assumed to be pressurized.

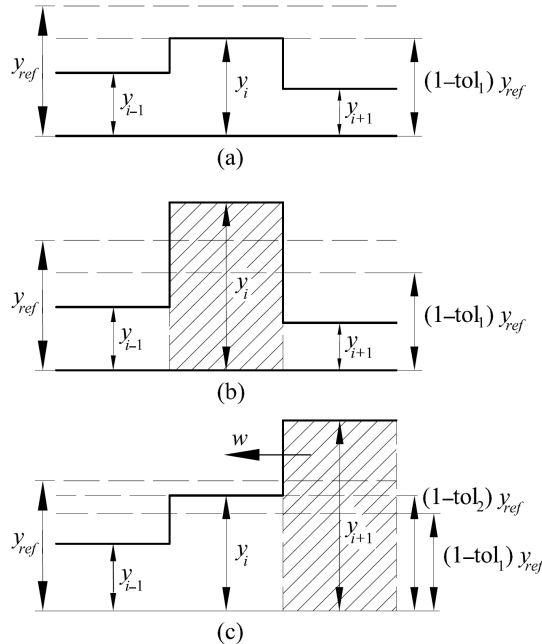


Figure 5 Threshold levels for piezometric head during numerical pressurization

A similar approach to that presented for numerical pressurization can be implemented for numerical depressurization. However, in all the simulations performed no numerical instabilities associated to cell depressurization were experienced.

5 Evaluation of model

The purpose of this section is to evaluate the accuracy and robustness of the proposed model to simulate transient mixed flows in storm-sewers in single (pure liquid) and two-phase flow conditions (entrapment and release of air pockets). Four test cases are considered in this section. These are:

- (1) Experiments type A of Trajkovic *et al.* (1999) [Single-phase mixed flow].
- (2) Experiment of Vasconcelos *et al.* (2006) [Single-phase pressurized flow].
- (3) Experiments of Zhou (2000) [Air pocket entrapment with no air release].
- (4) Experiments of Zhou (2000) [Air pocket entrapment with air release].

5.1 Experiments of Trajkovic

Herein, the proposed model is used to reproduce a set of experiments conducted at the Hydraulics Laboratory, University of Calabria, by Trajkovic *et al.* (1999). The ability of the proposed model is tested to simulate a positive mixed flow interface (single-phase) reversing its direction and becoming a negative interface. The test setup consisted of a perspex pipe about 10 m long, having an inner diameter of 10 cm and a Manning roughness coefficient $n = 0.008 \text{ m}^{1/6}$ (Yen 1991). The initial conditions for this test were a constant discharge of $0.0013 \text{ m}^3/\text{s}$, $S_o = 2.7\%$ resulting in supercritical flow with an approach flow Froude number of $F = [u/(gh)^{1/2}] = 2.9$, an upstream sluice gate opening of $e_1 = 0.014 \text{ m}$, and the downstream sluice gate totally opened. The transient flow was generated after a rapid but not instantaneous closure of the downstream sluice gate causing the formation of an open channel surge moving upstream. This surge was continuously strengthened by the inflow and after few seconds became a positive mixed flow interface

moving upstream. After 30 s from gate closure, the gate was partially reopened. Different reopening values e_2 were tested. Herein, the three values $e_2 = 0.008$ m, $e_2 = 0.015$ m, and $e_2 = 0.028$ m are considered.

Simulated (proposed and from Trajkovic *et al.*'s (1999) model) and measured pressure heads 0.6 m from the downstream gate for the three reopenings are shown in Fig. 6. The results for the proposed model were generated using 400 cells, a Courant number of $C = [(u+c)\Delta t/\Delta x]$ (free surface flow) or $(u+a)\Delta t/\Delta x$ (pressurized flow) = 0.80 and $a = 500$ m/s. The results of Trajkovic *et al.*'s model were generated using a pressure wave celerity of about 4 m/s. Even though the comparison of results between our model and that of Trajkovic *et al.* (1999) may not seem relevant because different pressure wave celerities were used, the results indicate that our model is robust for large pressure wave celerities.

As can be observed from Fig. 6, the simulated piezometric head h for both numerical models have a good agreement with the corresponding tests measurements. In particular, the formation of the filling bore and its propagation velocity are accurately predicted. However, all the computed shock fronts are steeper than those measured, because of rapid gate closure, yet not instantaneous, as assumed in the simulations. Figure 6 also shows a drop in the piezometric head after the partial reopening of the downstream gate at $t = 30$ s. In both simulations, an instantaneous partial reopening was assumed which caused a steeper front of the pressure drop as compared to the experimental results. The smaller pressure drop in both simulations may be in part due to the inaccuracies in representing the partial opening at the downstream boundary, where the orifice equation of Trajkovic *et al.* (1999) was used.

For a reopening of 0.008 m (Fig. 6 a), after a small drop in the piezometric head, it continuously increased in both models and the test. This is because the pipe outflow was smaller than the inflow. For a reopening of 0.015 m (Fig. 6 b), a steady mixed flow interface was observed and computed for the test and proposed model in the pipe after the drop in piezometric head. For a reopening of 0.028 m (Fig. 6 c), the mixed flow interface traveled downstream for the test and the proposed model, because the outflow was larger than the inflow. It is acknowledged that the numerical results of Trajkovic *et al.* (1999) for a reopening of 0.015 and 0.028 m (Fig. 6 b and c) are not shown after about $t = 32$ s (shortly after partial gate reopening). Numerical instabilities were reported by Trajkovic *et al.* (1999) even though a small wave celerity of ~ 4 m/s was used.

According to Trajkovic *et al.* (1999), Vasconcelos *et al.* (2006), or León *et al.* (2009a), the results are almost independent of the pressure wave celerity when simulating mixed flows in a single pipe, in which the pressurized flow region is isolated and if there is no interaction of pressurized waves. This explains why researchers using very low pressure wave celerities obtained good agreement with tests when simulating mixed flows. However, as demonstrated by León *et al.* (2009b), the results depend significantly on the selection of the pressure wave celerity if there is an interaction of pressurized waves such as in multiple pipes. In the latter case only a pressure wave celerity equal to the water hammer wavespeed gives accurate results of the frequency and magnitude of pressurized transients.

From Fig. 6 (b) and (c), it can be noted that shortly after the gate was reopened to 0.015 m or 0.028 m, the positive interface reversed its direction becoming a negative interface. This is particularly evident for a reopening of 0.028 m (Fig. 6 c). Also, the initial Froude number was about 2.9, corresponding to supercritical flow. As mentioned above, one of the present contributions is that the proposed model can simulate mixed flows without restriction of the flow type in the free surface region. Fig. 6 (b) and (c) demonstrates that our model simulates a negative interface for supercritical flow in the free surface region.

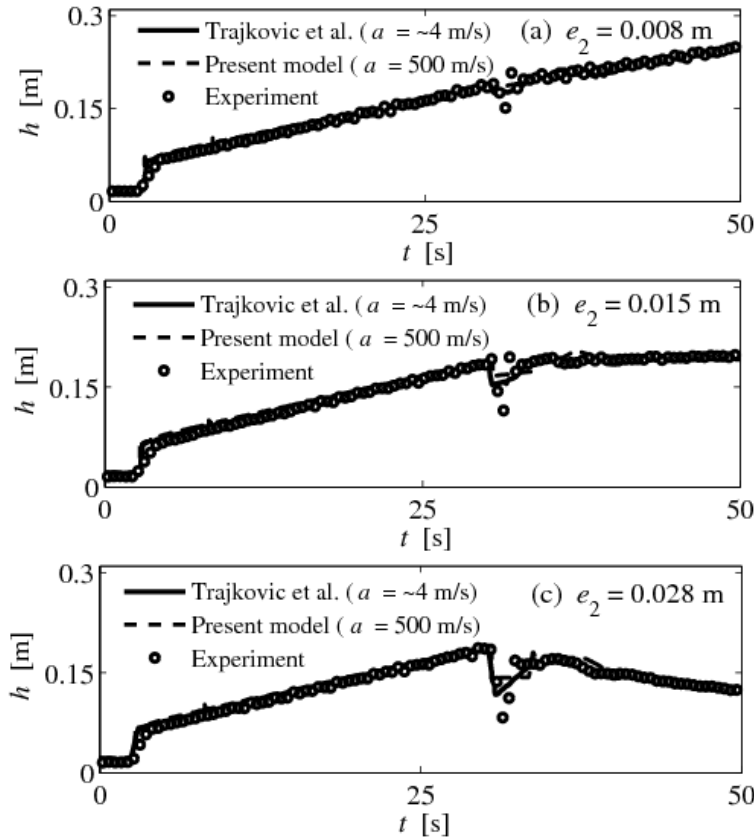


Figure 6 Measured and computed piezometric depths 0.6 m from downstream gate for type A tests of Trajkovic *et al.* (1999) for different reopenings

5.2 Experiments of Vasconcelos *et al.*

The purpose of this section is to test the ability of the proposed model to simulate sub-atmospheric pressures in pressurized flow regime (single-phase). The test considered was conducted at the University of Michigan and is reported by Vasconcelos *et al.* (2006). The setup consisted of an acrylic pipeline 14.33 m long, of 9.4 cm inner diameter. Its center portion was raised about 15 cm with respect to both ends to create conditions for the occurrence of sub-atmospheric pressures. The pipeline was connected at its upstream end by a box tank and by a cylindrical tank at its downstream end. The test considered was obtained by filling the system to a level of 0.30 m at the box tank and the system allowed to come to rest. Then a syphon outflow was suddenly initiated at the box tank at $t = 0$. The water level in the box tank then decreased to a level that created sub-atmospheric pressures at the pipe center portion. As the water level in the box tank dropped below the pipe crown just downstream of this tank, a complex flow pattern was developed. The flow just downstream of the box tank was then in sub-atmospheric conditions, and air flowed from the tank into the pipe. This constitutes a two-phase flow problem which is outside of the present scope. The intrusion of air flow in the test occurred at about $t = 42.5$ s, and in the model about 1.7 s earlier. Since this work is limited to single-phase flows, the comparison between model prediction and test results is only presented until just before the occurrence of air intrusion ($t < \approx 40.8$ s).

If the present model is used to simulate fully pressurized flows, as in this test case, $A_{ref} = A_f$. Then, the 2% reduction in hydraulic area for pressurized flows assumed for mixed flow conditions is eliminated. The pressure wave celerity used in the simulations was 300 m/s based on test measurements. The outflow was assumed constant at 0.45 l/s by observing the change in water volume over time. For estimating energy losses, Vasconcelos *et al.* (2006) used $0.012 \text{ m}^{1/6}$. However Manning's equation is only applicable to fully rough flows. Since the tests were performed under laminar and transitional flow conditions with $R < 4,300$, the Darcy-Weisbach equation would be better suited. For comparison, the numerical simulations were performed using both the equations of Manning and Darcy-Weisbach.

The simulated and tests velocities 9.9 m downstream of the box tank are shown in Fig. 7. The model predictions and tests for the piezometric head at 14.1 m downstream of the box tank are shown in Fig. 8. The simulated results were generated using 400 cells and $C = 0.80$. The results for the velocities (Fig. 6) show a good agreement between model and tests for the frequency of oscillations. However, the velocity amplitudes are overestimated by the model. As suggested by Vasconcelos *et al.* (2006), this may be in part because of assuming uniformity outflow. The differences between model prediction and tests may also be associated with the neglect of unsteady friction in the model. As can be seen from Fig. 7, the simulated results using the Manning and the Darcy-Weisbach equations are almost the same, the former being slightly more dissipative. The results for the piezometric head (Fig. 8) have a good agreement between model predictions and tests. The differences between the simulated and test piezometric heads may be explained similarly as for the velocities.

The reason for the velocity oscillations (Fig. 7) may not be clear at first. However, by taking a look at the piezometric head plot (Fig. 8), the aforementioned oscillations start to make sense. The velocity at a given section is associated with the local difference in piezometric head at both sides of the section. In the test, the outflow from the upstream tank creates a variation of piezometric head in the whole pipeline. Since both tanks are relatively small and as the system tends to steady state, oscillations in the piezometric head are produced (Fig. 8). These in turn cause oscillations in the flow velocity.

5.3 Experiments of Zhou: No air release

The test setup of Zhou (2000) consisted of an horizontal galvanized steel pipe of variable length with an inside diameter of 35 mm connected to a pressure tank at its upstream end. Inflow to the pressure tank provided with a pressure regulator facilitated a range of approximately constant driving heads at the pressure tank. The galvanized steel pipe consisted of three sections, separated by three quarter-turn valves. These provided three different initial air volume and water column length scenarios. The downstream pipe end was either sealed to form a dead-end, or outfitted with a cap containing a centered sharp-edged orifice. The initial conditions for the tests with and without air release consisted of two columns of fluid separated by a valve, in which the upstream column was always filled with water (pressurized) and the downstream column (receiving pipe) was either filled totally with air at atmospheric pressure (dry receiving pipe) or partially filled with water (wet receiving pipe). The air-water flow interaction in all tests was achieved by manually opening the quarter-turn valve separating the two columns of fluid. The tests were repeated up to five times because the recorded data sets varied significantly.

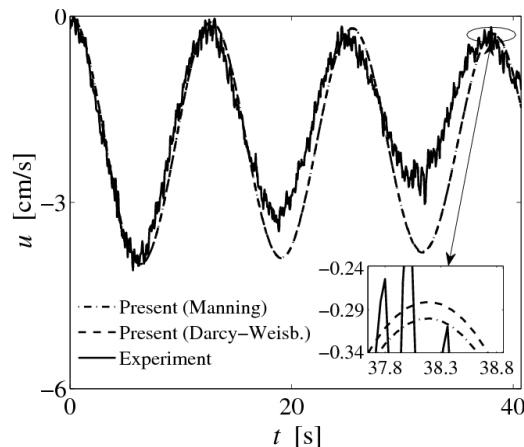


Figure 7 Measured and computed velocities 9.9 m from upstream end (Vasconcelos *et al.* 2006)

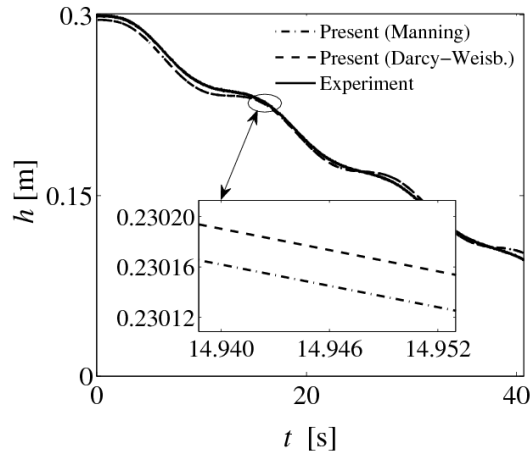


Figure 8 Measured and computed piezometric heads 14.1 m from upstream end for tests of Vasconcelos *et al.* (2006)

Zhou (2000) defined three types of pressure oscillation patterns depending on the relative size of the leakage orifice. Type 1 (zero or relative small orifice size) pattern is characterized by the dominant effect of the air cushioning and a negligible effect of water hammer impact pressure. Type 2 (relative intermediate orifice size) pattern is characterized by similar effects of the air cushioning and water hammer impact pressure. Type 3 (relative large orifice size) pattern is defined by the dominant effect of water hammer impact pressure and a negligible effect of air cushioning.

Due to space limitations only one test of Zhou (2000) with no air release is considered herein. This test resembles Type 1 pattern. The pipe length used by Zhou (2000) was 8.96 m, and 10 m for the test used in the next section (air release). The absolute pressure head in the pressure tank was for this test case $H_o^*/H_b^* = 2.43$, the initial water column length was 89% of the total pipe length ($\lambda_o = 0.89$), and $y/d = 0.4$ (wet receiving pipe). For the initial model conditions, the air volume above the free surface zone was an air pocket of zero gauge pressure head and atmospheric pressure air density. The simulated and measured absolute pressure head traces at the downstream pipe end are shown in Fig. 9. The simulated pressure head trace was obtained using 200 cells, a Courant number of $C = 0.80$, a Manning roughness coefficient of $0.012 \text{ m}^{1/6}$, and the experimentally obtained pressure wave celerity of $a = 700 \text{ m/s}$.

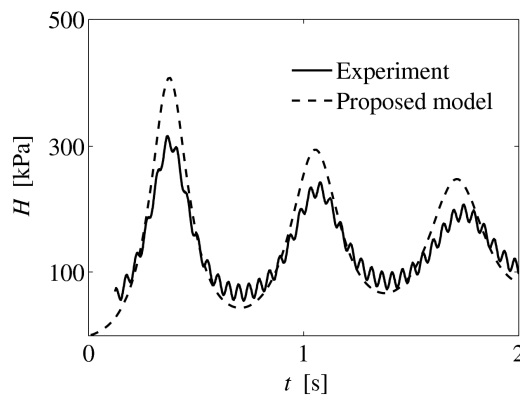


Figure 9 Experimental and simulated gauge pressure heads for $H_o^*/H_b^* = 2.43$, $\lambda_o = 0.89$, $y/d = 0.4$

As is observed from Fig. 9, the simulated pressure head trace has a fair agreement with that of the test. In particular, the amplitude and frequencies of the pressure oscillations are reproduced fairly well. The differences between the numerical simulation and the test may be attributed to the simplicity of the 1-D model for simulating complex hydrodynamic-thermodynamic processes such as the dynamics of formation and propagation of air pockets in pipelines. It is acknowledged that the simulation results for air release and no air release were not significantly sensitive to the value of the pressure wave celerity used.

5.4 Experiments of Zhou: With air release

Due to space limitations only one test of Zhou (2000) with air release is considered below of which the parameters were $H_o^*/H_b^* = 4.57$, $\lambda_o = 0.8$, $y/d = 0$ and $d_o/d = 0.028$. The pipe length used for this test was 10 m. The simulated and measured absolute pressure head traces at the downstream pipe end are shown in Fig. 10. The simulated pressure head traces were generated using 200 cells, $C = 0.80$, $n = 0.012 \text{ m}^{1/6}$, and $a = 1000 \text{ m/s}$, obtained experimentally.

As is seen from Fig. 10, the simulated results fairly agree with the test measurements. As mentioned above, the proposed model gives a fair agreement with tests only for no air release or under small air release conditions. For intermediate or large release conditions ($d_o/d > \sim 5\%$), the air-water flow is far from being one-dimensional (Zhou *et al.* 2002) so that a 1-D model can not be used. If the proposed model is used for intermediate or large release conditions, large discrepancies with test data result are obtained (not shown).

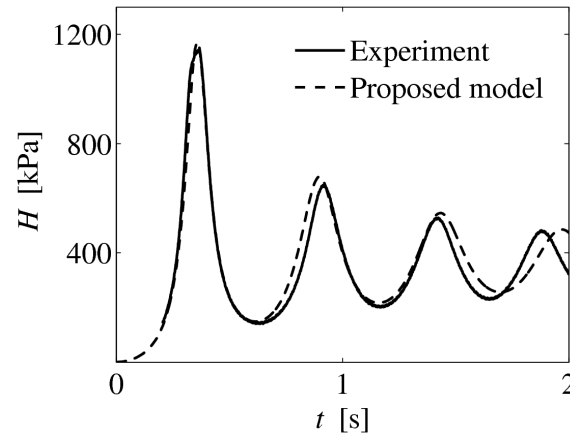


Figure 10 Experimental and simulated gauge pressure heads for $H_o^*/H_b^* = 4.57$, $\lambda_o = 0.8$, $d_o/d = 0.028$, $y/d = 0$

6 Conclusions

A Finite Volume model was built upon earlier work with the aim of simulating free surface flows, pressurized flows and their simultaneous occurrence in single and two-phase flow conditions. This research presents part of this model for simulating mixed flows in single and two-phase flow conditions. In our model, the free surface region is simulated using the modified 1D Saint-Venant equations accounting for air pressurization, the pressurized region is simulated using the classical 1D compressible waterhammer equations and open channel-pressurized flow interfaces are simulated by enforcing mass, momentum and energy relations across open channel-pressurized flow interfaces. The accuracy and robustness of the proposed model are investigated using four test cases. The key results are:

- (1) The proposed model accurately describes complex flow features, such as positive and negative mixed flow interfaces, interface reversals and open channel surges. In particular, the model simulates negative interfaces in mixed flow conditions having supercritical flow in the free surface region. This is achieved by using the HLL-Riemann solver in the free surface region that automatically handles subcritical and supercritical flows. It appears that no mixed flow model was formulated for negative interfaces for supercritical flow in the free surface region. The model also simulates negative pressures in pressurized flow regime.
- (2) In two-phase flow conditions, the proposed model reproduces with fair accuracy the frequency and amplitude of the pressure oscillations only for small air release conditions. For intermediate or large release conditions, the air-water flow is far from being one-dimensional so that a 1-D model can not be used. If the proposed model is used for intermediate or large release conditions, large discrepancies with the test data result.
- (3) Unlike previous approaches that rely on the speed of open channel-pressurized flow interfaces at the boundaries of an air pocket for computing the volume change of the air pocket, the volumetric change is herein computed using the net flow discharge flux evaluated at the air pocket boundaries which leads to a robust model.
- (4) Overall, the proposed model is robust and capable of simulating transient flows ranging from dry-

bed flows, to free surface flows, to partly free surface-partly pressurized flows, to fully pressurized flows in single and two-phase flow conditions. Furthermore, it can simulate any transient mixed flow condition for realistic pressure wave celerities.

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Notation

a = pressure wave celerity
 A = hydraulic area
 c = gravity wave celerity
 C = Courant number
 d = conduit diameter
 F = Froude Number
 \mathbf{F} = flux vector
 g = acceleration due to gravity
 h = piezometric depth
 H = gauge air pressure head
 $\bar{h} = \bar{p}/(\rho g)$
 k = heat capacity ratio
 m = mass of air
 n = Manning roughness coefficient
 p = pressure acting on center of gravity
 \bar{p} = average pressure of water column
 Q = discharge
 R = Reynolds number
 \mathbf{S} = vector containing source terms
 s = wave speed
 T = top width
 t = time
 \mathbf{U} = vector of flow variables
 u = water velocity
 V = volume of air pocket
 w = speed of mixed flow interface
 x = longitudinal coordinate
 y = piezometric depth above channel bottom
 Y = expansion factor

Superscripts

n = computational time level
 $*$ = absolute values (e.g., absolute pressure)

Subscripts

a = refers to air
 b = atmospheric conditions
 f = pressurized flow state
 i = mesh point location in x direction
 p_1 = left side of mixed flow interface

p_2 = right side of mixed flow interface
 ref = reference state
 w = water

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