A Simple Method for Prediction of Gas Permeability of Polymers from Their Molecular Structure

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ABSTRACT: A method for the prediction of gas permeabilities (P) through polymers from their chemical structure has been developed on the basis of the ratio of molar free volume to molar cohesive energy, V_f/E_{coh}. The permeation of small gas molecules through polymer membranes is dependent on the chain packing density measured by V_f and segmental motion of polymer chains measured by E_{coh} . But no simple relationship between P and V_f or E_{coh} alone was found. The permeability data of more than 60 polymers covering 7 orders of magnitude for six gases have been treated with linear regression analysis. All plots of log P vs. V_f/E_{coh} gave good straight lines. It is also found that a linear relationship holds when plotting both the intercepts and slopes of log P vs. V₁/E_{coh} lines against square of the diameters of gas molecules. Therefore, the permeabilities of all the non-swelling gases through a great variety of polymers can be estimated using two correlations above. Moreover, this method is more accurate than others in the literature and may found useful for the selection of gas separation or barrier membrane materials.

KEY WORDS Polymer Membranes / Gas Permeability / Free Volume / Cohesive Energy / Gas Separation / Barrier /

Permeation of small molecules through polymer membranes is very important for many applications, including separation processes, barrier packaging and controlled release devices for medicine and agriculture. It is significant to have a simple method for predicting what chemical strutures will provide permeabilities in the range desired for a particular use.

In an attempt to relate the penetrant to the polymer, Lee¹ put forward a prediction technique for gas permeability from polymer structure on the basis of a specific free volume (SFV) diffusive theory. Recently, Salame² suggested so called "Permachor" approach to predict gas permeability in polymers and he found that there is a good linear relationship between the logarithm of gas permeability and a polymer structure parameter Permachor (π), which can be calculated from both the cohesive energy density (CED) and fractional free volume (V_f) of the polymer. L. JIA and J. XU

However, it is clear from the discussion later that the linear relationship between log P and π is not so good as mentioned above. Furthermore, only 20 individual segmental values (π) of the backbones and side groups of polymers are available for the calculation of polymer Permachor. So, the permachor values of many polymers can not be calculated easily.

The object of the present study is to relate gas permeability with gas molecule diameters and two polymer molecular structure parameters i.e. cohesive energy (E_{coh}) and free volume (V_f) without taking into account such factors as crystallinity, orientation and rubbery or glassy state. These parameters can be obtained easily from group contributions. Therefore, the advent of this method simplified greatly the selection of membrane materials for different kinds of applications.

FOUNDATION AND APPROACH

The permeability of non-swelling gas through polymer is given by: P = D S

where P is the permeability, D -- the diffusion coefficient and S -- the solubility of the penetrant in given polymer. The temperature dependence of diffusion coefficint and solubility over small temperature range can be represented by:

$$D = D_0 \exp(-E_d/RT)$$
(2)

 $S = S_0 \exp(-\Delta H_s/RT)$ (3)where E_{d} is the apparent activation energy for the diffusion process and ΔH_{a} -- the heat of solution which may be expressed by the molar heat of condensation ΔH_{cond} and the partial molar heat of mixing ΔH_1 : (4)

 $\Delta H_s = \Delta H_{cond} + \Delta H_1$

The value of ΔH_1 can be estimated from the cohesive energy density (CED) of the penetrant and the polymer by means of the Hildebrand equation³:

$$\Delta H_1 \approx \Delta E_1 = v_1 (\delta_1 - \delta_2)^2 \phi_2^2$$
(5)

The solubility parameters δ_1 and δ_2 are the square roots of the CED of the penetrant and polymer respectively, v_1 --the partial molar volume of the penetrant and ϕ_2 -the volume fraction of polymer in the mixture. For gases well above their critical point (e.g. H_2 , H_2 , H_2 , N_2 at room temperature) the hypothetical value of ΔH_{cond} would be very small and Δ Hs is governed by Δ H₁. Utilization of the Flory-Huggins equation⁴ leads to an expression for the solubility coefficients:

$$S = f_2 / [f_1p_1^{o}exp(1+\chi_1)]$$
 (6)
where p_1^{o} is the saturated vapor pressure of penetrant, χ_1 is the Flory-
Huggins interaction parameter and f_1 , f_2 are the fractional free volume
of penetrant and polymer respectively

very. spe As for E_d, Meares⁵ derived the expression:

 $E_{d} = (1/4) \pi d^2 N \lambda (CED)$

(7) where d is the collision diameter of the penetrant molecule, N -- the Avogadros' number and λ -- the jump distance.

From an expression similar to the Doolittle equation as modified for diffusion:

 $D = RT A_a \exp(-B_a/f)$ (8) where A_d is a parameter which is dependent on the size and shape of the penetrant and B_a is a parameter characterizing the "efficiency" of using the available free volume fraction, f, in the diffusion processes.

Material	V _f /E _{coh} x104	logVf, Eco	ь л	1/SFV (g/cc)	02	N ₂	P (ba He	rrer) H ₂	C02	CH4	Ref.
	10.40	2.000			2000		2200		10000		
Poly[1-(trimethylsilyl)-1-propyne]	10.46	-2.980 -3.092	-	3.565 3.603	3000	1800	2200 180	5200 300	19000 560	4300	15
Poly(tert-butylacetylene)	8.10		-		130	43	÷			85	15
Poly(1-n-hepty1-propyne)	7.20	-3.143	-	4.413	35	14	48	76	130	40	15
Poly[o-(trimethylsilyl)phenylacetylene]		-3.167	-	5.022	78	24	170	290	290	38	15
Poly(1-chloro-2-n-butylacetylene)	6.31	-3.200	-	5.324	35	10	59	100	180	30	15
Poly(1-chloro-2-n-hexylacetylene)	6.26	-3.203	-	5.357	32	11	41	66	130	33	15
Poly(1-chloro-2-n-octylacetylene)	6.24	-3.205	-	5.38	47	16	43	76	170	46	15
Poly[o-(trifluoromethyl)phenylacetylene		-3.218	-	7.420	25	7.3	130	140	130	6.6	15
Poly(1-n-hexyl-2-phenylacetylene	5.90	-3.229	-	5.165	14	5.5	30	45	48	14	15
Poly(1-ethyl-2-phenylacetylene	5.83	-3.234	-	5.035	12	4.5	40	57	40	4.4	15
Poly(1-phenyl-1-propyne)	5.80	-3.237	-	4.987	6.3	2.2	30	43	25	2.8	15
Poly(o-methyl phenylacetylene)	4.92	-3.308	-	5.959	8.1	3.0	29	39	15	3.0	15
Poly(1-chloro-2-phenylacetylene)	4.87	-3.312	-	6.448	5.1	1.0	23	29	23	1.3	15
Poly(oxydimethylsilylene)	9.50	-3.022	-23#	4.437	600	280	340	650	3230	940	14
Hydrogenated Polybutadiene	5.70	-3.244	15	5.874	11.3	3.98	15.7		48.2	13	13
Poly(1,3-butadiene)	6.50	-3.187	6#	4.471	19	6.42	32.6	41.9	138		13
Polyisoprene (NR)	6.03	-3.220	-	4.939	24	8.1	31	49	131	30	14
Polychloroprene	6.40	-3.194	-	4.343	3.95	1.17	13	13.57	25.74	3.27	14
Polydimethylbutadiene	5.73	-3.242	-	5.276	2.1	0.472	14.4	17	7.47	0.79	13
Rubber hydrochloride	5.00	-3.301	38.3		0.43	0.106		1.6	1.02		11
Polysulfide (Thiokol Rubber)	4.39	-3.358	-	8.763	7.7				10.63		12
LD Polyethylene	4.76	-3.322	25#	7.03	2.88	0.969	4.9	8.7×	12.6	2.88	14
HD Polyethylene	2.86	-3.544	39#	11.688	0.40	0.143	1.14	6	0.36	0.39	13
Polypropylene	4.80	-3.319	31#	6.101	0.88	0.219	6.22	5.98	2.89		13
Poly(vinyl chloride)	3.80	-3.420	61#	9.328	0.04		2.05	1.70	0.157	0.029	13
Polystyrene	4.86	-3.313	27	6.017	2.63	0.788	18.7	23.3	10.5	0.84	13
Poly(vinyl alcohol)	0.81	-4.092	157#	18.375	0.009				0.01		13
Poly(vinyl acetate)	4.57	-3.340		6.830	0.384		10.8	7.25		0.05	13
Poly(vinyl toluene)	4.44	-3.353		6.754	3.5	0.46			10.81		12
Poly(vinylidene chloride)	1.83	-3.738	86#	21.6	0.008		0.248				13
Poly(vinyl fluoride)	1.87	-3.728	59#	27.08	0.02	0.0042			0.09	0.0057	12
Poly(vinylidene fluoride)	1.39	-3.857		60.99	0.04			0.41	0.36		
Poly(trifluorochloroethylene)	4.95	-3.305	64	15.43	0.48	6 0,119	34.08)	• • • • •	1.82	0.0348	13
Poly(tetrafluoroethylene)	5.50	-3.260	04 30	27.03	4.2	1.4	25×	9.8	11.7	0. 0J40	13
i orgetetta i aoroethytehe)	0.00	0.200	70	C1.02			204	3.0	- i + 1		1.5

Table 1. Gas Permeabilities at 25°C and Polymer Structural Parameters

Material	V _f /E _{coh} x10 ⁴	logV _f /E _{co}	h Л	1/SFV (g/cc)	02	Nz	P (bari He	rer) H ₂	CO2	CH4	Ref.
Poly(ethylene oxide)	4.90	-3.310	33	6.067	0.46						11
Poly(methylmethacrylate)	3.80	-3.420		8.342	0.102	0.023					11
Poly(ethylmethacrylate)	4.45	-3.352		7.222	1.4	0.25	15		5.0		11
Poly(4-methylpentene-1)	6.50	-3.187	7#	4.527	32.3	7.83	101	136	92.6		13
Poly(2, 6-dimethylphenyl oxide)	5.68	-3.246	13	5.427	15.8	3.81	78.1	112.8	75.7	4.3	13
Poly(oxymethylene)	3.00	-3.523	42.5	9.677	0.09	0.024			0.45		i ii
Poly-p-xylene	4.30	-3.367	30	7.35	0.47	0.132		3.54	2.64		12
Poly(chloro-p-xylene)	3.14	-3.507	50 66	10.845	0.03	0.004			0.07		
	1.50	-3.824	80#	9.203	0.006	0.0015		0.54	0.021		
Nylon 6		-3.824	41.7	9.203 10.976	0.12	0.03	1.95×	1.78×	0.021		11, 13
Nylon 11	1.58			10.343	0.034	0.008	1.33*	1.10	0.17		14
Nylon 6,6	1.34	-3.873	73#			0.000			0.074		11
Nylon 6,10	1.10	-3.959	52	14.27	0.02						
Nylon 6,9	1.82	-3.740	54.2		0.035						
Nylon 8	1.90	-3.721	51.8	8.115	0.058						
Nylon 12	2.60	-3.585	39.5	7.16	0.36						11
Bisphenol-A-Polycarbonatexx	4.5	-3.347	31#	6.75	1.484	0.289	15.0	13.6	6.0	0.257	16
Hexafluorobisphenol-A-Polycarbonate**	6.01	-3.221	58.5	7.53	6.9+	1.7+	60.0++		24++	1.05++	18
Tetramethylhexafluorobisphenol-A- Polycarbonate**	7.39	-3.131		5.949	32+	7.7+	206++		111++	4.7++	18
Tetramethylbisphenol-A-Polycarbonate**	5.20	-3.284	-21	6.027	5.59	1.09	46.2		17.58	0.80	16
Tetrabromobisphenol-A-Polycarbonate**	4.25	-3.372		10.975	1.36	0.182	17.6		4.23	0.126	16
Tetrachlorobisphenol-A-Polycarbonate**	4.43	-3.354	72	7.896	2.29	0.36	27.4		6.66	0.224	16
Tetramethylbisphenol-A-Polysulfonexx	4.54	-3.343		6.56			47.1		33.0	1.34	17
Bisphenol-A-Polysulfone	3.66	-3.437		7.93	1.3	0.25	9.6××	10.8	5.7	0.16××	11, 17
Polyepichlorohydrin (Hydrin 100)	3.83	-3.417	45	8.607	0.42						11
Polyisobutylene	5.51	-3.259	-2.5	5.687	9.0						11
Poly(ethylene terephthalate)	2.70	-3.569	65	11.648	0.059	0.013	3.28	0.6	0.30	0.009	13
Poly-4, 4'-diphenylether pyromellitimid		-3.569		12.773	0.15	0.036		1.5	0.27		11
(Kapton, H-film)]	0,000		10110	0010	0.000					
*: at 30° C;	at 2 atr	1.; ++	: at	10 atm.;	#: fr	om ref.	[2].				

Table 1. Gas Permeabilities at 25°C and Polymer Structural Parameters(Continued)

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It is clear from the equations (2)-(8) that both the diffusion and solution, and thus the permeation of given gas molecule through polymer membranes is predominantly dependent on free volume (V_r) and cohesive energy (E_{coh}) . The V_r term can be considered as a measure of chain packing density or the "tightness" of the polymer structure. The Ecoh term can be considered as a measure of interaction of polymer chains and mainly determined the ability in segmental motion of polymer chains. The larger the V_f or the smaller the E_{coh} , the larger the P will be. But no simple relationship between permeability (P) and V_f or E_{coh} of polymer was found⁸. It was found from the data of over 60 different polymers that there is a simple linear relationship between log P and the ratio of V_f/E_{coh} for a given gas (Fig. 1), i.e. the following equation exists: $\log P = a_1 + b_1 (V_f / E_{coh})$ (9)

where a₁ and b₁ are constants for a given penetrant and different from penetrant to penetrant. The molar free volume V_r , is defined as: $V_r = V_t - V_o$ (10) where V_t and V_o are the molar volume of polymer at t (usually 298K) and

at O K respectively. A good approximation to V_o is⁸:

 $V_{o} = 1.3 V_{w}$ (11) where V_{w} , the van der Waals volume can be obtained through group contribution consideration⁸. If no experimental data on V, are available, the values of V_{g} or V_{r} estimatied by group contribution⁷ was adopted. Thus, the gas permeability of other existing or new polymer can be estimated by calculating V_r and E_{con} from group contribution⁷ and interpolating the ratio of V_f/E_{coh} on Figure 1. Furthermore, it was found also that a linear relationship holds when plotting the values of both intercept(a_1) and slope(b_1) of the lines on the log P vs. V_r/E_{coh} plots against the square of diameter d^2 of penetrant molecules (Figure 2). Therefore, the plots of log P vs. V_f/E_{coh} for other gases can be drawn from the values of intercept and slope found by interpolating their molecular diameters on Figure 2. This simple method for predicting gas per-

meability may found useful for the selection of gas separation and barrier membrane materials.

RESULTS AND DISCUSSION

The permeability data of about sixty homopolymers covering 7 orders of magnitude for six common gases i.e. O_2 , N_2 , H_2 , H_2 , H_2 , CO_2 and CH_4 from different sources are listed in Table 1. Almost all of the homopolymers published in the literature to date no matter whether it is in rubbery or glassy state, amorphous or partially crystalline are included in the table. The temperature and pressure at which the permeability was measured are not quite the same, although most of the data were measured at 25 °C.

In order to compare with Lee's and Salame's technique, 1/SFV, π value and log (V_f/E_{coh}) are also included in Table 1. According to Lee¹, the specific free volume, SFV, is defined as: SFV = V_f / M (12)where M is the molecular weight of repeating structural unit in Dalton

 V_r is given in eq.(10). At a given temperature Lee's expression became: $\log P = a_2 + b_2/SFV$ (13)if S is assumed to be not strongly SFV dependent as Lee did.

Here a_2 and b_2 are constants. From Salame's equation²

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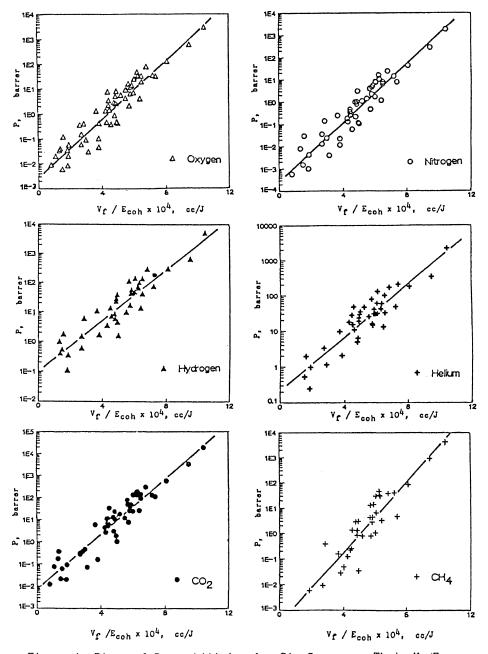


Figure 1. Plots of Permeabilities for Six Gases vs. Their $V_{\rm f}/E_{\rm coh}$

$P = A \exp[-s\pi]$	(14)
the following expression can also be obtained:	
$\log P = \log A - s\pi = a_3 + b_3\pi$	(15)
where $a_3 = \log A$ and $b_3 = -s$	
$s = (1/RT - B')\upsilon + \beta$	(16)
and s is in direct proportion to the square of gas molecule diam	eter.
Because ⁹ $\pi = 57 \ln(\text{GED}/f_v) - 325$	
where $\text{CED} = E_{\text{coh}} / V_t$, $f_v = (V_t - V_o) / V_t = V_f / V_t$	
Salame's eq.(14) can be rewritten as:	
$\log P = a_4 + b_4 \log(V_f/E_{coh})$	(17)
where a and b are constants and $a = 1 \text{ and } 1 \text{ and } b = 570$	

where a_4 and b_4 are constants and $a_4 = \log A + 141s$, $b_4 = 57s$. All the data were treated with linear regression analysis and the results are listed in Table 2. It is evident that the eq. (9) has the highest linear correlation coefficient(r) among all of the four equations (13), (15), (17) and (9) for all the six gases studied. In other words, the method of predicting gas permeabilities from the ratio of molar free volume to molar cohesive energy of polymers is more accurate than others. It is also simpler and easier in use. However, it is clear from those plots in Figure 1 that the scattering of gas permeability data is still considerable, in fact, there is a correlation band instead of a single line between log P and V_f/E_{coh} . The possible reason for this is the variety of the sources of permeability data. If the conditions at which the permeabilities were measured were kept just the same, a better correlation between $\log P$ and V_r/E_{coh} would result, the authors believe. Even though, this correlation in its present form will work satisfactorily for predicting the molecular structure dependence of gas permeabi-lity of polymers and lend itself as a useful criteria for gas separation and barrier material selections.

Furthermore, it can be seen from Figure 2 that the intercepts of lines in Figure 1 were decreased linearly with increasing gas molecule diameters, while the slopes were increased linearly. It indicated that the larger the gas molecules, the smaller the permeability through polymer membranes and the gas permeabilitlies varied more rapidlys with the ratios of V_r/E_{coh} of polymers. This is conformable with actual situation.

Although similar relationship also existed between a_4 , b_4 and d^2 , it is clear from Table 2 that the linear correlation of equation (17) is much less than that of equation (9). As to other two equations (13) and (15), such correlation was absent either between a_3 (or a_2) and d^2 , or between b_3 (or b_2) and d^2 .

Having above correlations we can estimate the permeabilities of all the non-swelling gases through a great variety of polymer membranes from gas diameters and the ratios of V_f/E_{coh} of polymers.

CONCLUSION

The good linear relationship between log P and the ratio of V_f/E_{coh} of polymers suggested that in a first order approximation, the permeabilities of a given gas through polymer membranes were governed by the ratio of molar free volume to molar cohesive energy V_f/E_{coh} of polymers. And there is also a good linear relationship between both the intercepts and the slopes of the lines on the log P vs. V_f/E_{coh} plots and the square of gas molecule diameters. Therefore, the permeabilities of all nonswelling gases through almost all the polymer membranes can be estimated

	•••		•	•••			
		He	H ₂	C02	02	Nz	CH4
	d(nm)*	0.260	0.289	0.33	0.346	0.364	0.380
Eq. (9)	n	43	40	53	60	51	35
	a 1	-0.6186	-0.9975	-2.1381	-2.5229	-3.5123	-3.4446
	b,	0.3702	0.4345	0.6261	0.5857	0.6590	0.6870
	r	0.9128	0.9220	0.9475	0.9417	0.9439	0.9012
Eq. (17)	n	43	40	53	60	51	35
	a4	13.3096	13.9338	17.8195	16.1515	18.1503	26.2167
	b₄	3.6191	3.8078	5.0302	4.7095	5.4903	7.8865
	r	0.8927	0.8753	0.8958	0.8912	0.8891	0.8734
Eq. (15)	n	21	21	29	34	27	14
•	a ₃	1.6623	1.9841	1.5313	0.8842	0.546	0.9086
	b3	-0.0184	-0.0322	-0.0287	-0.0285	-0.0304	-0.0343
	r	-0.6854	-0.9296	-0.7828	-0.7925	-0.8123	-0.7784
Eq. (13)	n	43	40	53	60	51	35
	a2	1.9810	1.6965	1.5808	0.9065	1.1186	1.9078
	b_2	-0.0821	-0.0547	-0.0770	-0.0804	-0.1661	-0.2137
	r	-0.5832	-0.5518	-0.5017	-0.5112	-0.6291	-0.6948

Table 2. Comparison of linear regression analysis of gas permeability data among Eqs. (9), (17), (15) and (13)

* from ref.10.

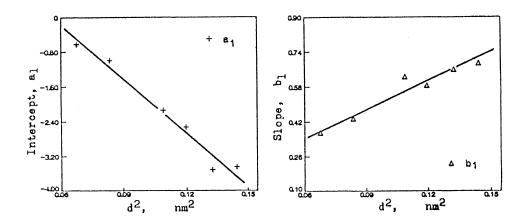


Figure 2. Plots of Intercept a_1 and Slope b_1 in Eq. (9) from Figure 1 vs. d^2 of Gases

from the relationships mentioned above. Morever, this method is more accurate and simpler than others in the literature, thus should serve as a useful tool for the selection of gas separation membrane and barrier materials from polymer structures for industrial applications.

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