

1 Apparent flow dimension approach to the study of heterogeneous fracture 2 network systems

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8 Abstract

9 The generalized radial flow (GRF) model in well-test analysis employs non-integer flow dimensions to represent
10 the variation in flow area with respect to radial distance from a borehole. However, the flow dimension is
11 influenced not only by changes in flow area, but also by permeability variations in the flow medium. In this paper,
12 the flow dimension from the combined effect of flow dimensionality and permeability/conductance variation is
13 interpreted and referred to as apparent flow dimension (AFD). AFD is determined using the second derivative of
14 the drawdown-time plot from pressure transient testing, which may have varied non-integer values with time. This
15 paper presents a systematic set of investigations starting from idealized channel networks in one, two and three
16 dimensions, and proceeding to a case study with a complex fracture network based on actual field data.
17 Interestingly, a general relation between the AFD upsurge/dip and the conductance contrast between adjacent flow
18 channels is established. The relation is derived from calculations for 1D networks but is shown to be useful even
19 for data interpretation for more complex 2D and 3D cases. In an application to fracture network data at a real site,
20 the presence of flow channel clusters is identified using the AFD plot. Overall, the AFD analysis is shown to be
21 a useful tool in detecting the conductance/dimensionality changes in the flow system, and may serve as one of the
22 different data types that can be jointly analysed for characterizing a heterogeneous flow system.

23 **Keywords:** Flow dimension, Channelling, Transient testing, Network systems, Site in Sweden

24 1. Introduction

25 Understanding the flow and transport in fractured rocks is critically important for a number of key
26 geotechnical and hydrogeological applications. In fractured rocks the flow can vary from being relatively evenly
27 distributed and space-filling to a system where most of the flow takes place in a few dominating channels. Various
28 hydrological and rock mechanical processes act differently in these extremely different systems and therefore it
29 is important to understand the prevailing flow system when doing any model predictions. Well testing is the

1 technique for determining an aquifer's hydraulic properties. In well tests, a disturbance in pressure or flow is
2 introduced in the test borehole and the propagation of this disturbance inside the formation is monitored in terms
3 of head/pressure variation and the results interpreted using a suitable model representing the flow in the formation.
4 The conventional well-test interpretation models assume an idealized flow geometry in a homogeneous and
5 infinite domain, such as the radial/cylindrical flow model by Theis (1935), the linear flow model by Miller (1962),
6 and the radial-to-spherical flow model by Moye (1967). Diagnostic plots in log-log scale showing the drawdown
7 and its logarithmic derivative as a function of time are often used in well-test analysis (Bourdet et al., 1983). The
8 concept of the use of logarithmic derivatives in the interpretation of well test results was introduced by Chow
9 (1952), who presented a graphical method to determine the formation constants of an artesian aquifer from
10 pumping test data. The logarithmic derivative is highly sensitive to minor changes in the variations of hydraulic
11 head and therefore enables the detection of behaviours that would be difficult to notice using the drawdown curve
12 only. To account for more complex hydrogeologic systems, especially encountered in fractured rocks, Barker
13 (1988) proposed a so-called generalised radial flow (GRF) model. In this method, an additional parameter named
14 flow dimension was included, which is the second derivative of the drawdown-time plot. Unlike the earlier
15 models, this model accounts even for non-integer flow dimensions. Flow dimension reflects the network's flow
16 geometry by indicating how the cross-sectional area to the flow varies in relation to the distance from the testing
17 well and can have non-integer values different from one, two or three. The flow-dimension diagnostic plots
18 inspired some simple approaches as a replacement of specialized models, for example Delay et al. (2004)
19 presented a new analytical method using Gauss-Newton algorithm to study the interference pumping tests in
20 Poitiers, France.

21 Doe and Geier (1990) were among the first ones to apply the GRF model for the analysis of field data to
22 identify the flow geometry of the fracture system and at the Stripa mine, Sweden, at about 360 m depth. The
23 impact of boundary effects was observed to be negligible indicating a well-connected fracture system. The spatial
24 dimension interpreted from the tests varied from sub-linear (conductivity decreasing with distance from the hole)
25 to spherical for a three-dimensional dense fracture system. During certain pressure tests, the flow dimension also
26 varied over time. Doe (1991) further discusses the use of the GRF method in terms of the interpretation of
27 constant-pressure well tests and points out that flow dimension also reflects aquifer conductivity heterogeneity
28 and that flow geometry and conductivity heterogeneity are actually interchangeable in the interpretation of flow
29 dimension. This was identified as a shortcoming of the GRF technique, but can also be seen as an opportunity,
30 as the method nevertheless allows to investigate different underlying conceptual models for flow, as pointed out

1 e.g. by Walker and Roberts (2003). Kuusela-Lahtinen et al. (2003) analysed a large data set from a low-
2 conductivity crystalline rocks down to 450 m depth from the Finnish nuclear waste investigation programme. The
3 results showed that the lower dimensions corresponding to linear and sub-linear flow were easy to distinguish
4 from dimensions over 2, while the dimensions 2 to 3 were more difficult to distinguish from each other. The latter
5 was usually because of practical difficulties in creating accurate early-time data, as required by the theory. The
6 results nevertheless gave good indications as of how flow dimension varied both with the scale of the measurement
7 (2m or 10m), the depth of the investigation and the character of the rock (fracture zone or average rock). Renard
8 et al. (2009) discussed the merits and demerits of using flow dimension diagnostic plots with the help of three
9 field examples and advised for caution due to their high sensitivity to small variations in drawdown which can
10 lead to misinterpretations. They emphasized that due to the certain degree of non-uniqueness in the interpretation,
11 the information on flow dimension must be combined with other information obtained from geological,
12 geophysical, and hydrological data, in order to build a valid fracture network model.

13 Gringarten (2008) and Ferroud et al. (2018) evaluated the historical development of flow dimension
14 study in aquifer characterization. Cello et al. (2009) examined the relationship between DFN parameters and flow
15 dimension by applying Monte Carlo analysis. Verbovšek (2009) performed the flow dimensional analysis to
16 correlate the flow dimension with hydraulic conductivities in the case of dolomites. The correlation was found to
17 be poor. They also compared the flow dimension with fractal (Euclidian) dimension in 3D, and found flow
18 dimension to be always less than its fractal dimension. Odling et al. (2013) investigated the effect of flow
19 dimensionality on flow and transport properties in the non-radial flow domain. They highlighted the significance
20 of recognizing non-radial flow regime when estimating aquifer parameters and interpreting tracer breakthrough
21 curves. Additionally, they noted that disregarding the existence of non-radial flow in the case of partly penetrating
22 boreholes might result in an overestimation of aquifer parameters. Ferroud et al. (2019) performed a thorough
23 investigation of well test data from different geologic settings and observed that in addition to the prevalence of
24 cylindrical-radial flow, non-cylindrical-radial flows are also common and may change in the course of a well test.
25 According to them the non-cylindrical-radial flow dimensions ($n < 2$, or $n > 2$) can be easily recognised. This is
26 also reported by other investigators (Cinco et al. 1978; Kuusela-Lahtinen et al., 2003, Kuusela-Lahtinen and Poteri
27 2010; Rafini et al. 2017).

28 In spite of the extensive work since the first development of the GRF model, a systematic study
29 combining the effects of flow dimensionality and permeability heterogeneity is presently lacking. With this in

1 mind, this study presents a set of model analyses, starting from one dimensional channel models and proceeding
2 to two- and three-dimensional systems, and investigates what an analysis of the flow dimension, or the apparent
3 flow dimension AFD, from a flow test can tell about the characteristics of the system. We investigate the effect
4 of conductance contrast between the connected flow channels in a constant flow transient well test with the
5 objective of formulating a relationship between conductance contrast and the AFD. The term AFD is used in the
6 following text to indicate the fact that we are analysing it from the observed well test, which combines not only
7 the effect of variable flow dimension but also the effect of permeability/conductance contrast.

8 **2. Methods**

9 A channel network model, CHAN3D, was developed by Gylling et al. (1999), which uses a lattice
10 channel network to represent a system of fractures where each node is connected to six adjacent nodes and the
11 channel conductance follows log normal distribution (Gylling et al., 1999; Moreno & Neretnieks, 1993). This
12 model was later enhanced to include more complex parameters such as stagnant water zones and rock matrix layer
13 properties in tracer transport (Mahmoudzadeh et al., 2013; Moreno et al., 2006; Neretnieks, 2006; Shahkarami et
14 al., 2016).

15 Our study uses a further development of the code by Dessirier et al. (2018), who modified the model to
16 automatically generate lattice networks as described by Gylling et al., (1999) and sparse lattice networks as
17 defined by Black et al. (2017). The resulting script, *pychan3D* code, also includes a customizable method to build
18 unstructured networks from scratch, amend existing networks, and apply boundary conditions as well as to select
19 different numerical solvers and to export the results for 3D visualization. For the present work this code was
20 further developed to include the transient test in the fracture network. It should be pointed out that even though
21 the structure of the code is that of channel network, it can be used to model uneven flow in fracture planes and
22 three-dimensional fracture networks, where small channel sections with different properties can be used to
23 represent local flow heterogeneities in fracture planes.

24 In the following text we will describe shortly the essential features of the model, for both steady state
25 and transient simulation, followed by how the actual apparent flow dimension is determined from the results of
26 the transient pressure-flow simulations.

1 2.1 Model for steady state groundwater flow

2 In *pychan3D* model (Dessirier et al., 2018), the steady state flow rate (Q) along a channel with
3 conductance C and head difference (Δh) at the two ends is formulated as:

$$Q = C \cdot \Delta h \quad (1)$$

4 The conductance of a channel with average transmissivity (T), width (w) and length (L) in simple
5 rectangular cross section can be defined as:

$$C = \frac{T \cdot w}{L} \quad (2)$$

6 The head h at every point in the network can then be solved form a linear system of equations by
7 introducing a Laplacian matrix in mass balance equation at each node (Li et al., 2014).

$$M_c \cdot h = B_c \quad (3)$$

8 Where, M_c = Laplacian matrix of the network of conductances;

9 B_c = vector of boundary conditions

10 2.2 Transient flow formulation

11 Analysis of flow dimension requires transient flow simulations, for which the model by Dessirier
12 et al. (2018) was further developed. For this we assume, as before, one-dimensional channel length
13 extending from $x=0$ to $x= L$, of width w, conductance C, and now also with constant storativity S. Taking
14 note of the Laplace variable p, the channel's ability to adjust to changes in conditions at its two ends can be
15 represented by an effective distance (x_p).

$$x_p = \sqrt{\frac{C \cdot L}{p \cdot S \cdot w}} \quad (4)$$

1 where the subscript shows the Laplace variable dependency. Then, the pressure head can be
 2 shown in the Laplace domain as a function of the initial head $h_i(x)$ and the pressures at the ends of the
 3 channel $H_0(p)$ and $H_L(p)$.

$$H(x,p) = \frac{h_i(x)}{p} + \frac{\left[H_L(p) - \frac{h_i(L)}{p} \right] \cdot \sin h \frac{x}{x_p} + \left[H_0(p) - \frac{h_i(0)}{p} \right] \cdot \sin h \frac{L-x}{x_p}}{\sin h \frac{L}{x_p}} \quad (5)$$

4 This analytical solution enables the calculation of transient flow variables at the channel ends:

$$Q_0(p) = -C \cdot L \cdot \left. \frac{\partial H(x,p)}{\partial x} \right)_{x=0} \quad \text{and} \quad Q_L(p) = -C \cdot L \cdot \left. \frac{\partial H(x,p)}{\partial x} \right)_{x=L} \quad (6)$$

5 Considering the vector of the transient pressure values being unknown at the network nodes, the
 6 matrix formulation of the steady state problem can be extended to the transient problem in the form of
 7 Laplace space.

8 2.3 Determining the flow dimension

9 After obtaining the flow solution in time domain for a pumping test, the pressure drawdown/build
 10 up curve can be used to determine the apparent flow dimension near the pump. With the help of pressure
 11 drawdown/build-up (h) at the well, the pressure derivative (h') and slope of pressure derivative are expressed as
 12 shown in equations 7 and 8 as follows. Also notice that the unit of the pressure derivative will be the same as the
 13 pressure itself since it is a log derivative.

$$h' = \log \frac{dh}{d \ln t} \quad (7)$$

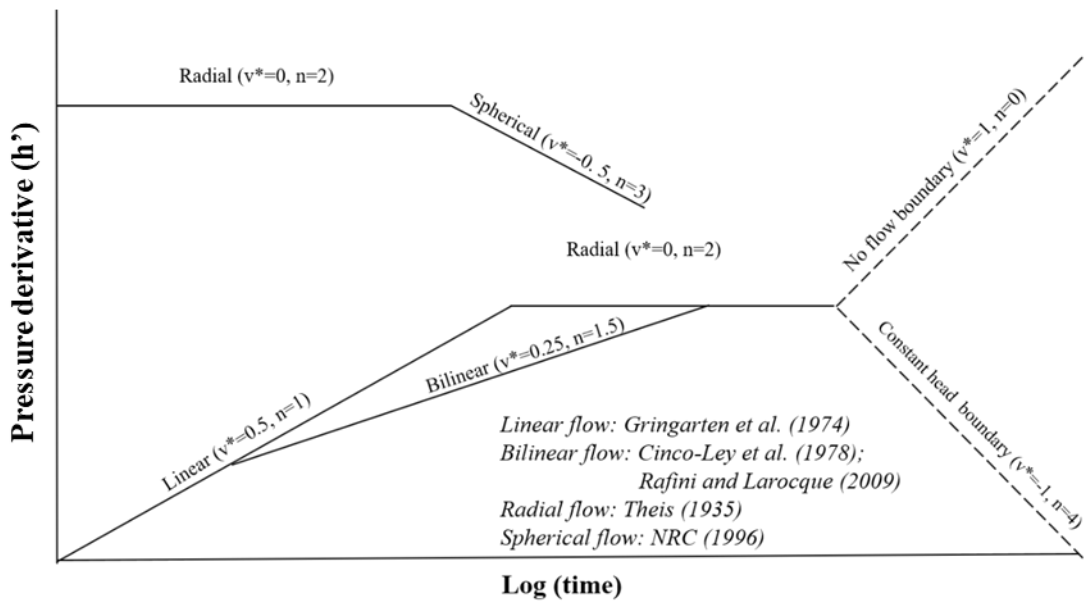
$$v^* = \frac{dh'}{d \log t} \quad (8)$$

14 The flow dimension n of the system can then be formulated as (Barker, 1988):

$$n = 2(1 - v^*) \quad (9)$$

1 In other words, the slope (v^*) between h' and $\log t$ is used to determine the flow dimension. For linear
 2 flow the integer flow dimension becomes $n=1$ ($v^*=0.5$), for radial flow $n=2$ ($v^*=0$) and for spherical flow $n=3$
 3 ($v^* = -0.5$) The fractional flow dimension values other than these three values are also possible and can represent
 4 realistic flow systems (Walker et al., 2006).

5 To exemplify how flow dimension appears in a log-log plot between pressure derivative (h') and time,
 6 Fig. 1 gives some examples of published flow dimension values (Cinco et al., 1978; Gringarten et al., 1974;
 7 National Research Council, 1996; Rafini & Larocque, 2009). Additionally, the flow dimensions at different
 8 boundaries are also shown, with $n=4$ representing a constant head boundary and $n=0$ a no-flow boundary (Fig. 1).



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Fig. 1 Examples of flow regimes and flow dimension presented in the literature

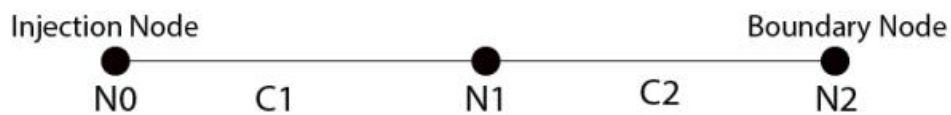
1 **3. Results**

2 **3.1 One Dimensional Channel and Effect of Conductivity Contrast on Apparent Flow Dimension**

3 As a first case, the simplest possible model consisting of one-dimensional channels was considered. A
4 systematic analysis of flow in 1D channels can provide useful insight assisting the analysis of later more complex
5 two- and three-dimensional channel networks.

6 **3.1.1 Effect of conductance contrast on flow dimension**

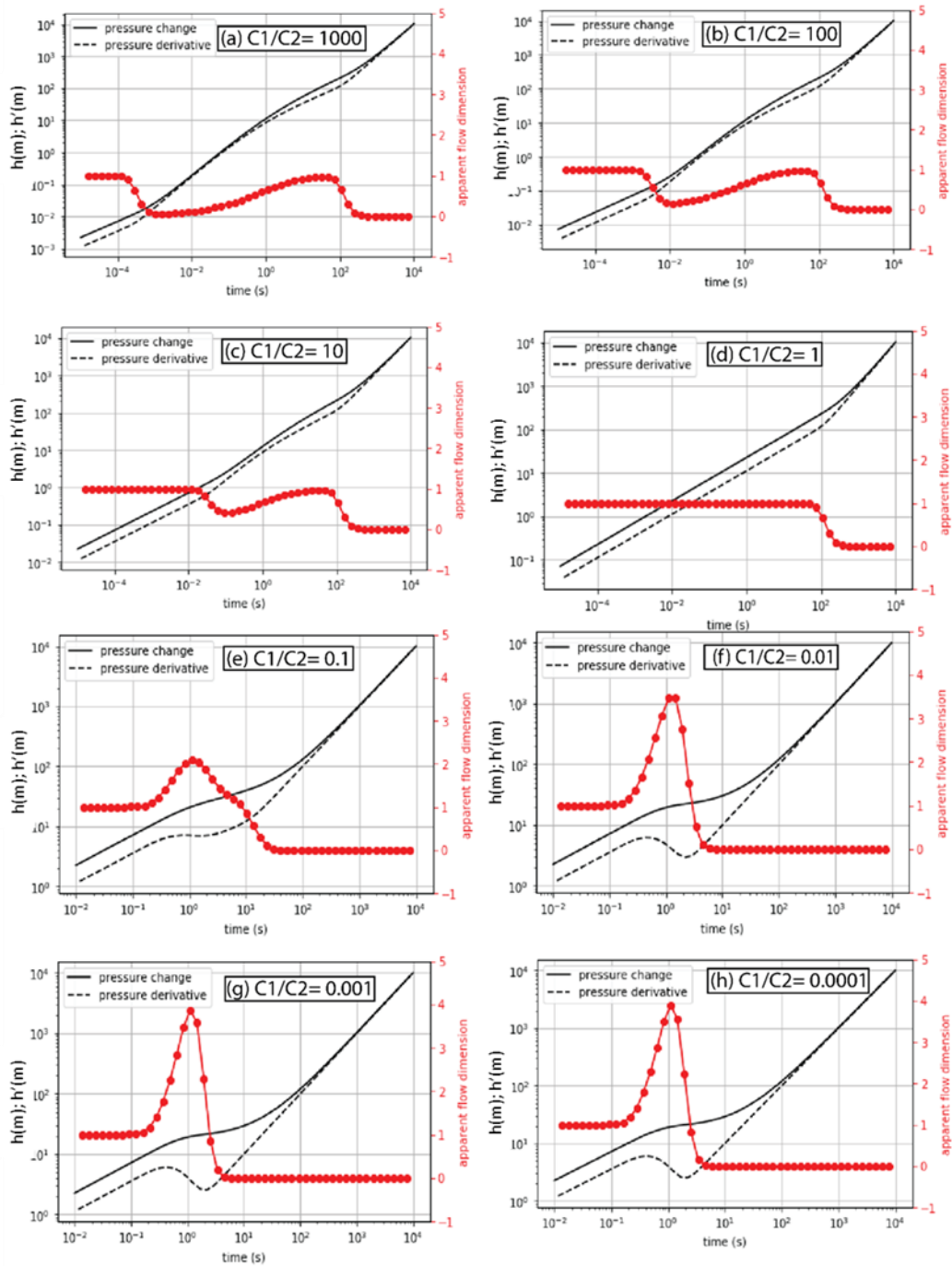
7 The simplest model (Fig. 2) consists of two sections having conductances C_1 and C_2 respectively. In
8 the Figure, N_0 is the injection node, N_1 is a junction between sections of two conductances and N_2 is a closed
9 boundary node. Steady state solution is first acquired by applying constant pressure at the boundary of the network
10 and then the system is used to test the transient response by imposing a constant flow injection at the injection
11 node with a closed outer boundary.



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13 Fig. 2 Simple 1D channel network with three nodes and two channels

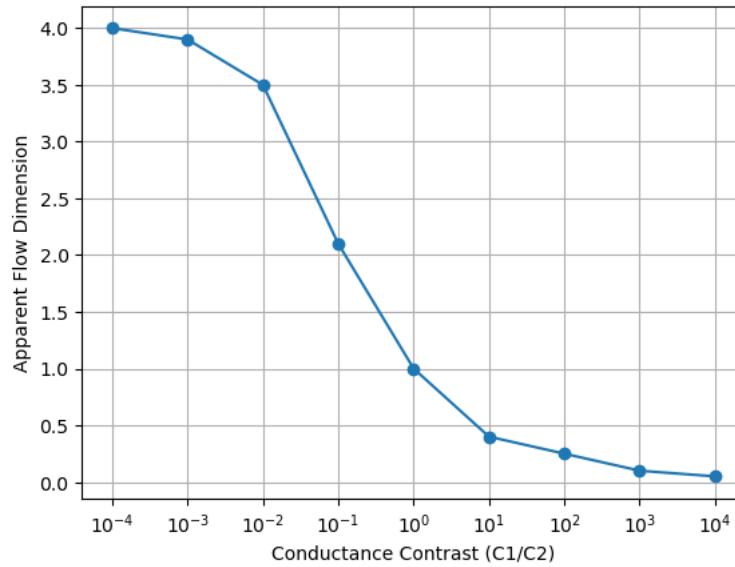
14 Fig. 3 shows the pressure, its derivative and the apparent flow dimension (n) for different conductance contrast.
15 When $C_1/C_2 = 1$, we have two channels with same conductance and the AFD plot is presented in Fig. 3(d),
16 showing a constant flow dimension of $n=1$ which drops to $n=0$, indicating the effect of the closed boundary node.
17 Fig. 3(a) demonstrates the case with $C_1/C_2=1000$ (highest drop in conductance). Here AFD initially starts with
18 value $n=1$ (indicating linear flow), then dips suddenly indicating the presence of the conductance contrast at C_1 -
19 C_2 junction but then reverts again to its initial value $n=1$. Then at a much later time, as before, it drops again to
20 zero due to the effect of the closed boundary. In the rest of the sub-figures under Fig.3 we can see that AFD
21 changes abruptly at the conductance contrast in each case. Depending on whether a higher or lower conductance
22 is encountered, there is an abrupt peak or dip of the apparent flow dimension at the conductance contrast, with
23 AFD increasing above $n=1$ when $C_1 < C_2$, and falling below $n=1$ when $C_1 > C_2$. Furthermore, it can be seen that
24 the magnitude of the peaking and dipping in ADF correlates well with the magnitude of the conductance difference
25 (Fig. 4).



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2 Fig. 3 Pressure (h), its derivative (h') and Apparent flow dimension (n) during a constant rate injection test
 3 along the two-conductance network with a no-flow far boundary

4 Fig. 4 shows the peak/dip of AFD value as a function of the conductance contrast $C1/C2$ and we can see
 5 a clear correlation. This kind of a general relationship between the AFD peak or dip and the conductance contrast
 6 is found to be useful (see below) even when analysing the behaviour of more complex multidimensional channel
 7 networks.



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Fig. 4 Relationship between the peak/drop in AFD and the conductance contrast (C1/C2)

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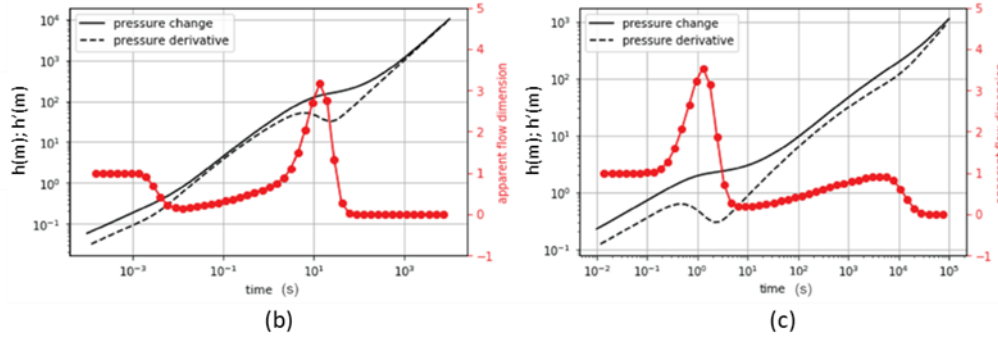
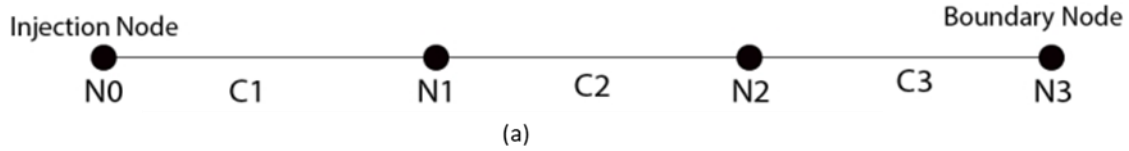
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Next, a three-section channel network is built (Fig. 5a) to examine the simultaneous effect of conductance increase and decrease within the same channel and also to verify the relationship established earlier in Fig. 4. The conductance of first and third sections, C1 and C3 are the same and the conductance of the middle section is varied. For the first case, the conductance of the middle section is *decreased* by two orders of magnitude, and the transient response of the network is then observed. In this case (Fig. 5b) we can observe that the AFD starts with value $n=1$ as expected and then drops to $n=0.2$ at the junction between C1 and C2, then attempts to recover its value of 1 again. At the C2-C3 junction with two orders of magnitude increase in conductance, AFD rises to value $n=3.1$ and then drops to zero at the boundary. These value pairs are in good agreement with the trend in Fig. 4. In the second case, conductance of the middle section of the network is instead *increased* by a hundred times and transient response is again observed (Fig. 5c) Similarly, at C1-C2 junction with two order of magnitude increase in conductance, AFD rises to $n=3.5$, and again drops to 0.2 at similar decrease in conductance. In other words, when the conductance contrast (C1/C2) is compared to the AFD upsurge ($n=3.1$ and 3.5) or dip ($n=0.1$ and 0.2), the result is in a good agreement with the generalized relationship depicted in Fig. 4. It also confirms that the AFD behaviour in the three-section example is consistent with the earlier two-section case.



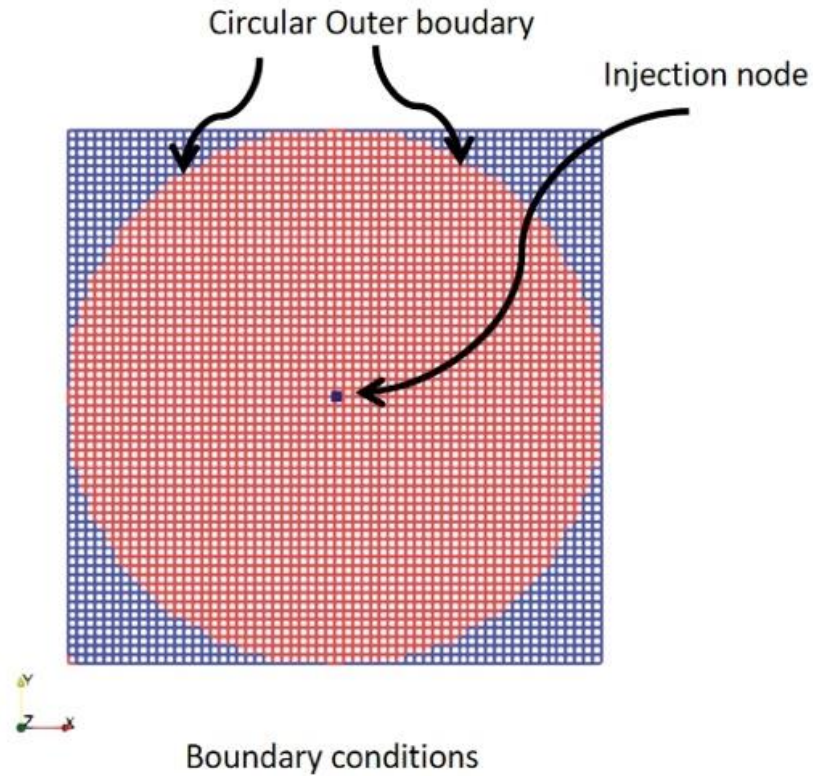
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2 Fig. 5 (a) 1D network with three sections. Pressure (h), its derivative (h') and Apparent flow dimension (n)
 3 during a constant rate injection test along the network with conductance contrast (b) $C1/C2=100$, and (c)
 4 $C1/C2=0.01$, with a no-flow far boundary

5 3.2 Two-Dimensional Channel Network with statistical heterogeneity ($\sigma = 1, 2, \text{ and } 3$)

6 As the next step, 2D channel networks were studied. For this, a 60×60 lattice of channels with
 7 conductance following an uncorrelated lognormal distribution were created with mean conductance of $10^{-10} \text{ m}^2/\text{s}$
 8 and four different standard deviation values: $\sigma = 0$ (homogeneous case), 1, 2 and 3. A standard deviation in log
 9 conductance of 3 in this case means a variance of conductance value of 3 (where the variance is the ratio of
 10 standard deviation in conductance to the mean conductance value). A larger standard deviation corresponds to a
 11 greater variation in conductances within the channel network and thereby a higher degree of heterogeneity. Fifty
 12 realizations were generated for each sigma value by means of random value generator built-in numpy, python
 13 library. A constant flow injection test was then simulated in these cases, with the injection well located at the
 14 centre of flow domain and a constant head boundary condition assigned to the outer circular boundary as shown

1 in Fig. 6. Constant injection with injection rate of $7.2 \text{ m}^3/\text{hour}$ for a duration of 3 hours, is simulated for the 50
2 realizations for each σ value.



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Fig. 6 Two-Dimensional channel network with boundary condition

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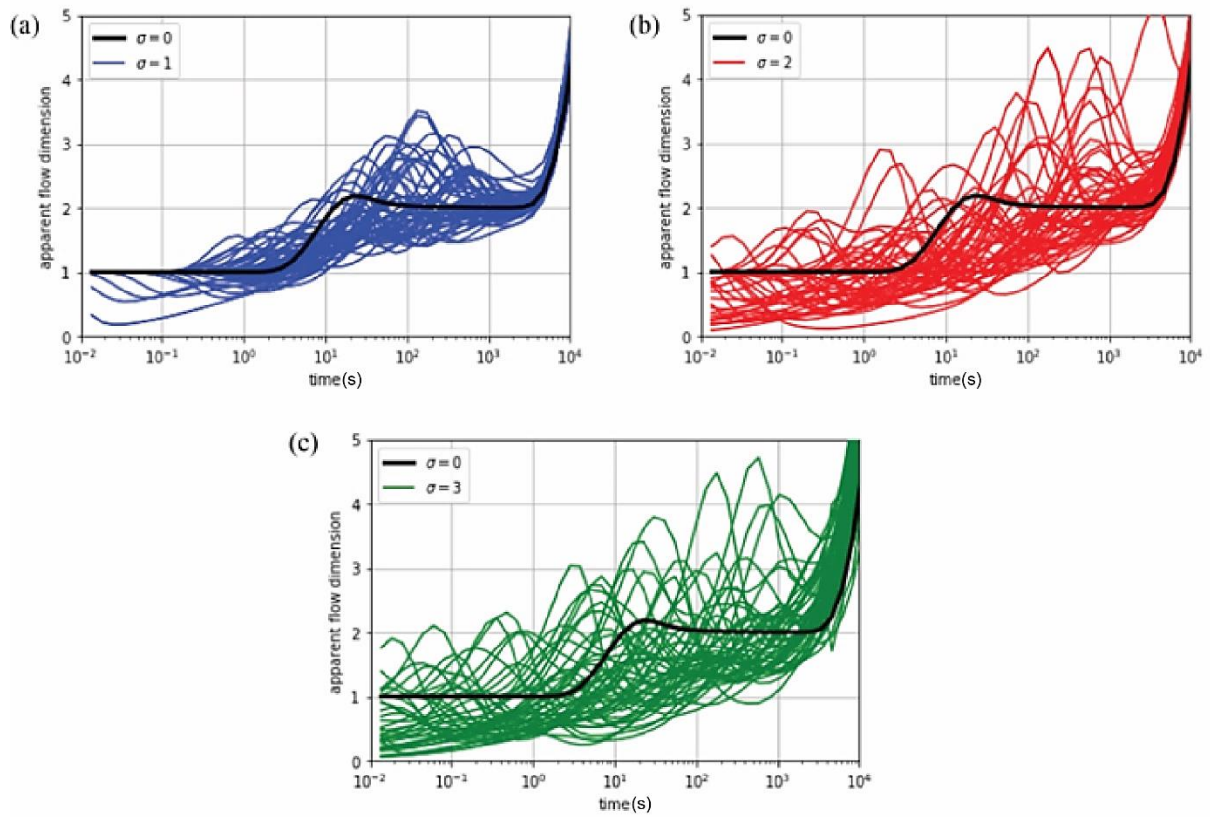
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Fig. 7 illustrates the obtained apparent flow dimension for all 50 realizations as a function of time for each of the $\sigma = 1, 2,$ and 3 cases. For comparison the homogeneous case ($\sigma=0$) is also shown in all figs. It can be seen that for the homogeneous case the flow dimension always starts from a value of 1, indicating an early-time channelized flow when the flow is taking place in individual channels. After that there is a transition period followed by a long stable stage of 2-dimensional (cylindrical) flow, indicating that the flow is taking place radially throughout the system. Finally, a sharp increase to a high flow dimension is encountered when the flow encounters the constant pressure boundary. In contrast, results for $\sigma = 1, 2,$ and 3 cases display a strong oscillatory behaviour in AFD, indicating the pressure front encountering steps of conductivity contrasts.

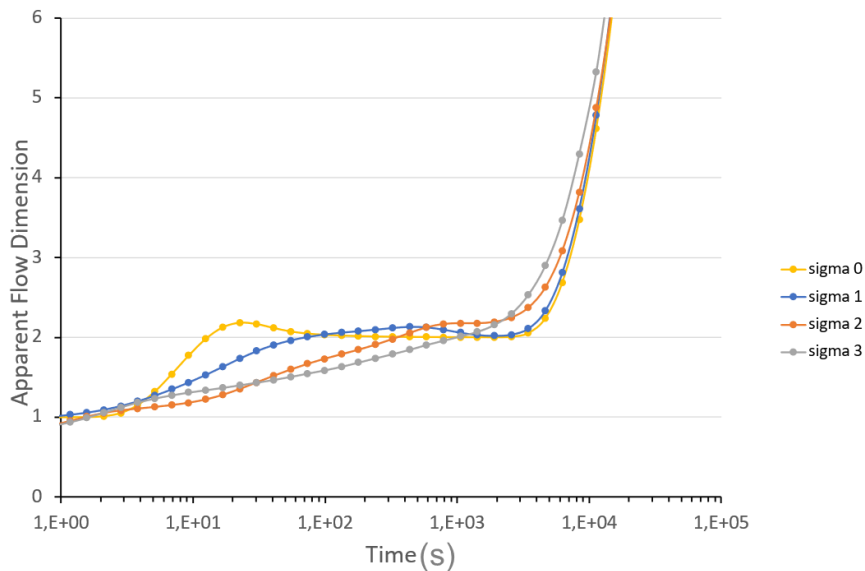


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Fig. 7 AFD variation over time for three realisations having (a) $\sigma=1$, (b) $\sigma=2$, and $\sigma=3$

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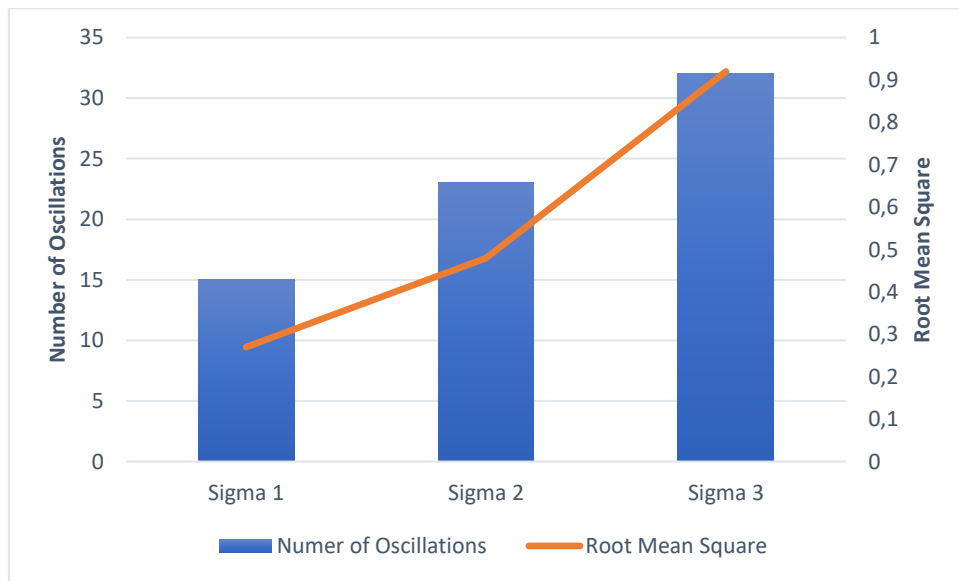


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Fig. 8 Mean Apparent flow dimension for 50 realisations as a function of time

1 In Fig. 8 the arithmetic mean of AFD from all 50 realizations is shown for each σ . The figure implies
 2 that with an increase in σ , flow is taking more time to stabilize to the value of AFD=2 that indicates cylindrical
 3 flow. The flow dimension for higher σ values does not stabilize properly at value AFD=2 and ranges between 1
 4 and 2 indicating a persistent bilinear flow behaviour. This points to the dominance of flow in sparse channels.
 5 Heterogeneity of the conductance field tends to reduce the expected apparent flow dimension and speed up the
 6 propagation of the pressure signal to the boundaries of the model, which are two of the characteristics of the
 7 channelling effect. For the individual realizations with $\sigma > 0$ the behaviour is much more heterogeneous and
 8 characterized by a number of sharp fluctuations. The number of the fluctuations in the flow dimension as well as
 9 their magnitude increases when σ increases. The number of distinct AFD fluctuations around the mean for each
 10 σ and the root mean square (RMS) of AFD deviations from the mean is presented in Fig. 9 as a measure of the
 11 amplitude of AFD fluctuations. The increase of the amplitude of AFD fluctuation with an increase in the σ value
 12 is clearly seen in this figure, and further study will be made to explore its possible use in the estimation of the σ
 13 value of the underlying heterogeneity of the flow domain.

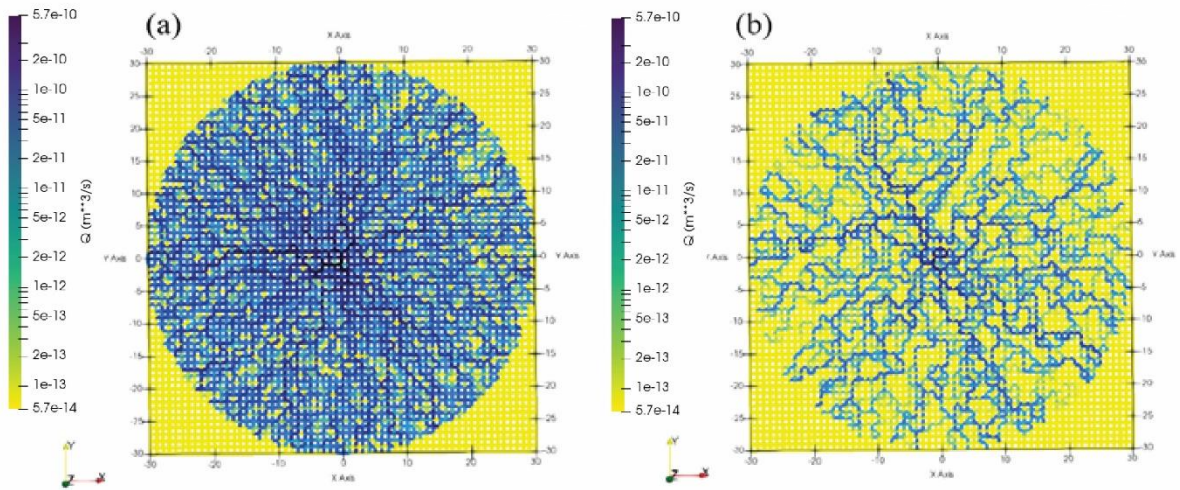


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15 Fig. 9 Number of Oscillations and Root Mean Square of AFD deviation for each σ case

16 In Fig. 10, the steady state flow for one example realization is shown for the two standard deviations
 17 $\sigma=1$ and $\sigma=2$, to visually examine the appearance of channelization in them. It can be seen that the flow is more
 18 evenly distributed in the $\sigma=1$ case whereas in the $\sigma=2$ case it is concentrated into a smaller number of channels.

1 Flow rates for both sigma values and three example realisations from transient simulations at the time
2 when the flow dimension becomes stable (at $t=10^3$ seconds) is shown in Fig. 11. From the flow rate distribution,
3 it is visually evident that the flow gets more channelized with an increase in σ in all three realizations. In all the
4 statistically heterogeneous cases, the flow dimension gets stable at the value lower than the corresponding
5 Euclidian dimension, which also indicates the channelling phenomenon in the system.

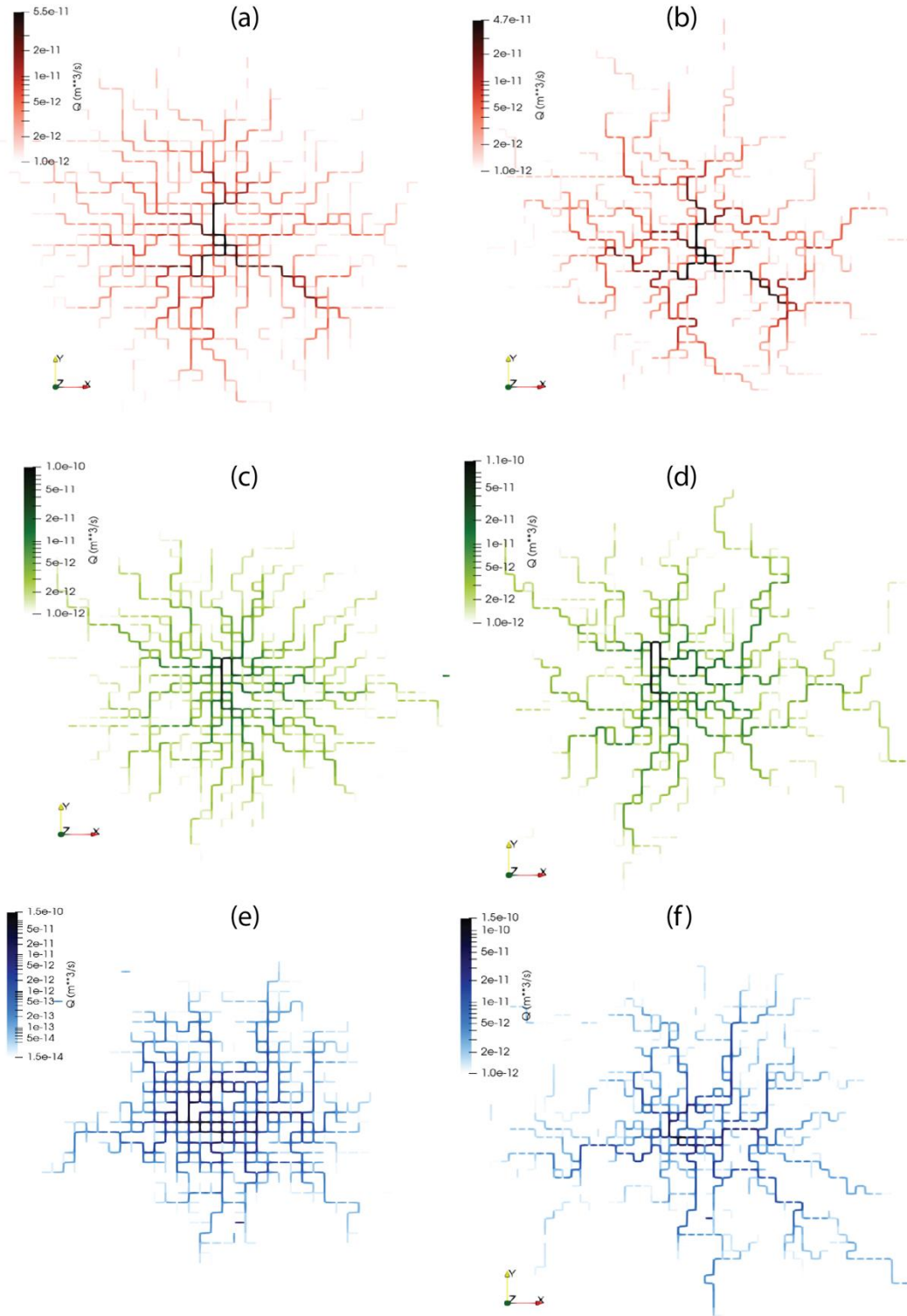


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7 Fig. 10 Steady state flow rate for the 2-dimensional networks with conductance distribution a) $\sigma=1$ and b) $\sigma=2$

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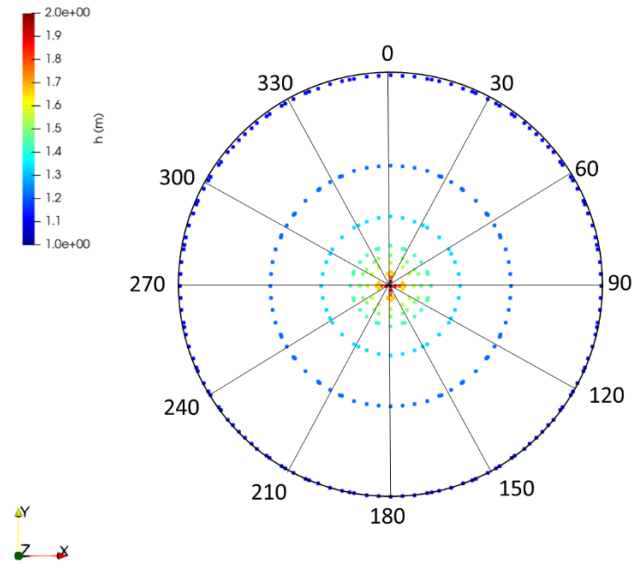


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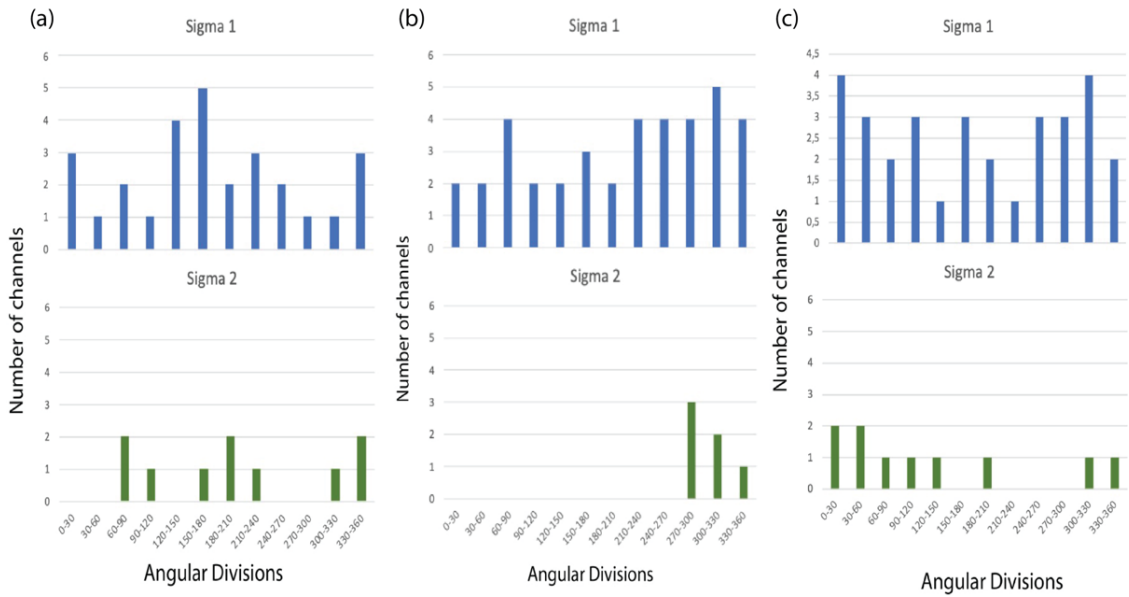
Fig. 11 Flow rate distribution at $t=1000$ seconds (a) $\sigma=1$, first realization, (b) $\sigma=2$, first realization, (c) $\sigma=1$, second realization (d) $\sigma=2$, second realization (e) $\sigma=1$, third realization (f) $\sigma=2$, third realization



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2 Fig. 12 Circle overlapping the pressure contour for an example realization of homogeneous conductance at
 3 t=1000 seconds

4 To determine the degree of channelization in a more quantitative way the flow domain was divided into
 5 sections of 30 degrees as shown in Fig. 12 and the number of channels intersecting an imaginary circle in each
 6 section was calculated. The radius of the imaginary circle was chosen by looking the pressure contour at the time
 7 t=1000 seconds from the homogeneous conductance case (the time when the flow dimension in the homogeneous
 8 case stabilizes). The number of channels intersecting the circumferential divisions are shown in Fig. 13. In all
 9 three realisations, the number of active channels intersecting the outer circumferential boundary is significantly
 10 reduced in case with $\sigma=2$ as compared to case with $\sigma=1$. The difference is especially pronounced in the case of
 11 the second realization (Fig. 13b), where most of the flow channels disappear and the most dominant flow channels
 12 are found in the direction between 270° to 360°.

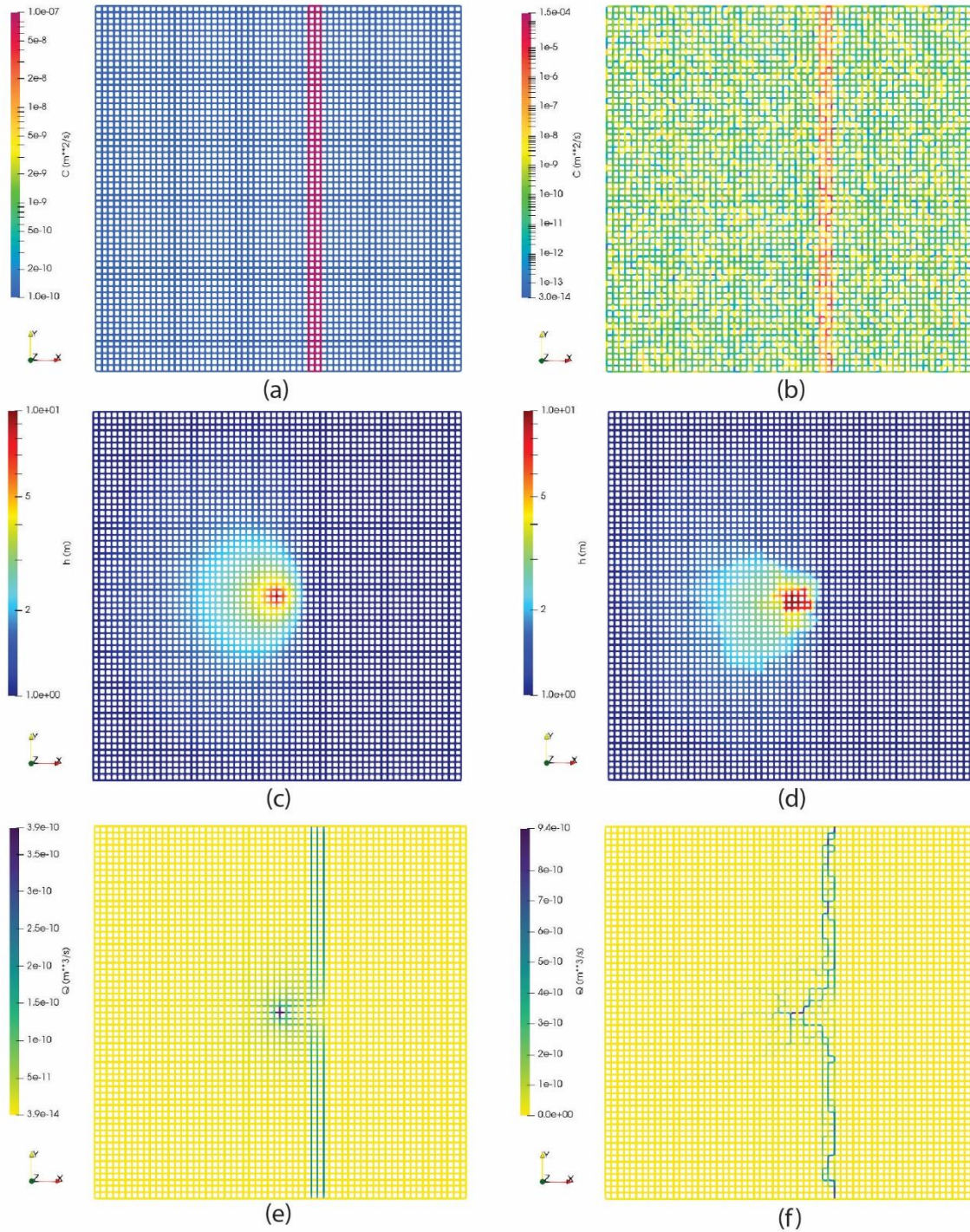


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2 Fig. 13 The number of channels intersecting the circumferential boundary divisions for three realizations (a), (b)
 3 and (c) for σ_1 and σ_2

4 3.3 Two-Dimensional channel network with a linear high-conductance zone

5 In this subsection, the effect of a geometrically-defined, deterministic heterogeneity in the previous 2D
 6 stochastically heterogeneous flow domain is investigated. A linear zone where the channel conductances are
 7 increased 1000 times is introduced into a rectangular lattice (Fig. 14a and b). The linear high conductive zone
 8 may represent a deterministic feature such as a large fracture or fault zone. The conductance of the rest of the
 9 network is distributed log-normally as before, with standard deviation of either $\sigma=0$ (homogeneous case) or $\sigma=1$.
 10 The effect of the outer boundary on the transient test was also investigated by applying two different boundary
 11 conditions at the outer boundary; a constant pressure boundary representing an open outer boundary as well as a
 12 closed outer boundary. For the constant-pressure boundary case the simulated steady state pressure distributions
 13 for a sample realization for both conductance distributions ($\sigma=0$ and $\sigma=1$) shown in Fig.14c and d. A uniform
 14 circular pressure distribution around the injection point is observed for the homogeneous conductance case ($\sigma=0$),
 15 skewing away from the linear zone of higher conductance where pressure drop is instantaneous. In the
 16 heterogeneous case ($\sigma=1$) similar behaviour can be seen at the high permeability zone but now the hydraulic head
 17 distribution is not circular but shows local heterogeneity effects.



1

2

Fig. 14 (a) Rectangular lattice network with log normally distributed conductance, $\sigma=0$, and (b) $\sigma=1$ with a linear zone of higher conductance. (c) Simulated hydraulic head distribution, $\sigma=0$, and (d) $\sigma=1$. (e) Flow rate

3

distribution, $\sigma=0$, and (f) $\sigma=1$.

4

5

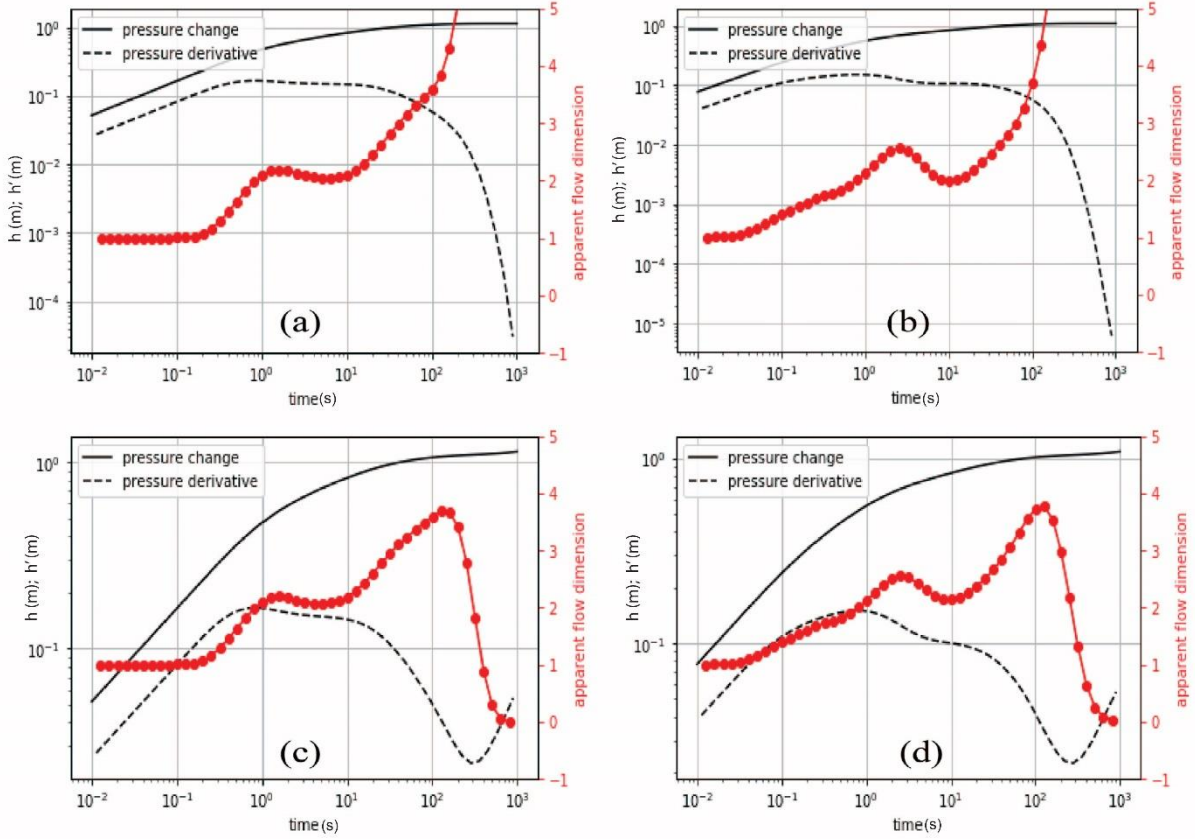
Fig. 14 (e and f) demonstrates the steady state flow rate distribution in the two cases. The effect of the deterministic high-conductivity zone dominates the flow pattern in both cases. The flow initiates from the centre injection node and follows an outward trajectory towards the outer boundaries, until reaching the deterministic

6

7

1 fault zone after which most of the flow preferentially follows the high-conductive channels towards the outer
2 boundary. This is evident in both cases. In the heterogeneous case (Fig. 14 f), flow is even channelized within the
3 deterministic high-conductance zone. Two degrees of channelization can be observed in this case; the primary
4 channel of high flow occurs along the high conductance linear zone and the secondary channelization appears
5 within the linear zone, due to the local conductance distribution with $\sigma=1$.

6 The effects of these geometrically defined heterogeneous systems during a transient well-test is examined next,
7 in order to study how the various heterogeneity effects can be observed. A constant flow injection test using both
8 open and closed outer boundary conditions is simulated in both geometries. Fig. 15 shows the AFD evolution with
9 time for the two geometries (with conductance distributions of $\sigma=0$ and $\sigma=1$), for both open and closed outer
10 boundary conditions. Fig. 15 (a) and (c) show the results for the uniform conductance $\sigma=0$, for open and closed
11 boundary, respectively. At the open boundary, the AFD goes to a very large value when the pressure front reaches
12 the boundary whereas at the closed boundary AFD drops to zero. We can see that AFD in both cases starts with
13 $n=1$, corresponding to the flow in channels in the immediate vicinity of the injection point. It then stabilizes at
14 $n=2$, as expected in a 2-dimensional, radial domain. Next, when the flow encounters the high-conductivity zone
15 Fig. 15(c), the AFD increases to 3.8, as a result of the three orders of magnitude increase in the overall
16 conductivity. This observation is consistent with the observed correlation between conductance contrast and AFD
17 found earlier in the case of the one-dimensional channels (Fig. 4). Similarly, for the case with non-uniform
18 conductance distribution $\sigma=1$ (Fig. 15b and d), AFD starts with $n=1$, but varies with time depending on what
19 channel conductivity is encountered and no stable 2D flow is reached (Fig. 15b and d). For this σ value, the
20 presence of the high-conductivity zone is also seen in Fig. 15d as the AFD=3.8 peak.

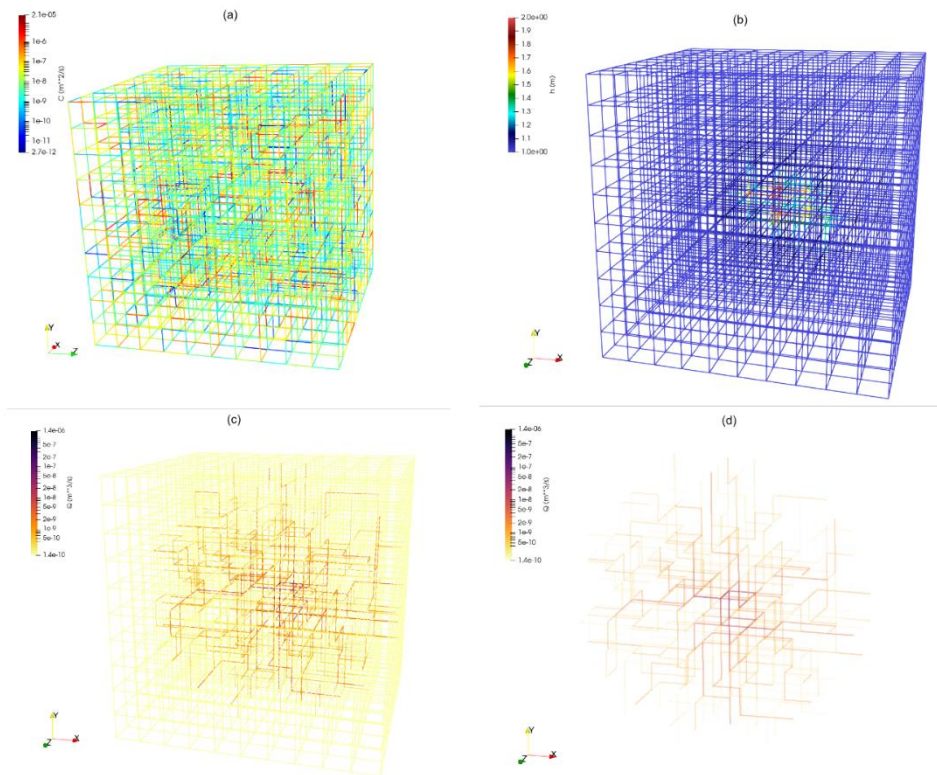


1

2 Fig. 15 AFD plot from transient test in (a) uniform conductance case ($\sigma=0$), (b) non-uniform conductance case
 3 with constant head boundary ($\sigma=1$), (c) uniform conductance case with closed boundary ($\sigma=0$), and (d)
 4 non-uniform conductance with closed boundary ($\sigma=1$)

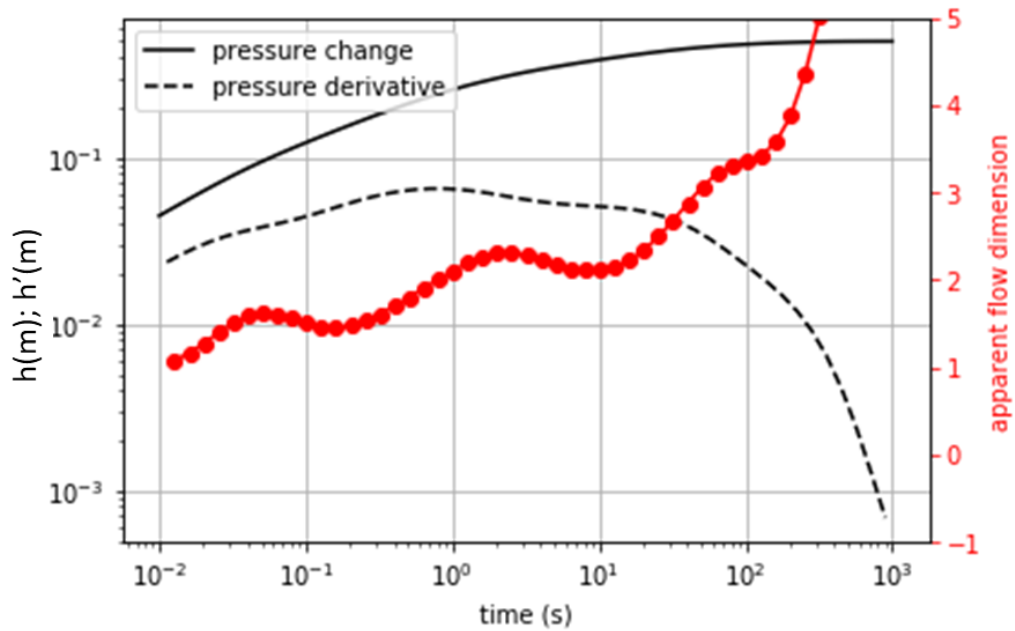
5 3.4 Three-Dimensional Channel Network

6 After studying the 1D and 2D networks, similar concepts are extended to the 3D channel networks to
 7 check the validity in 3D domain. A channel network (10x10x10m) is generated and the conductance is log-
 8 normally distributed with a mean value of 10^{-8} m^2 and a standard deviation of $\sigma=1$ (Fig. 16a). Within the cubic
 9 lattice network, a spherical constant-pressure outer boundary is created with hydraulic head difference of 2m
 10 between the injection point and the boundary, and the resulting distribution of pressure head is shown in Fig. 16b
 11 and the steady state flow solution is computed and the resulting flow rate distribution is shown in Fig. 16c. For
 12 better visualization, dominant channels with higher flow rate are plotted in Fig. 16d by making the low flow rate
 13 channels transparent (i.e., not shown). The so-called sparse channel networks can be created by eliminating very
 14 low flow channels to decrease the complexity and computational demands of the fracture system for further study.
 15 Pychan3D (Dessirier et al., 2018) can easily be modified to create these sparse networks based on cut-off
 16 threshold values of flow or any other parameters. Methods such as this may prove very useful when the network
 17 consists of thousands of fractures, representing a realistic site.



1

2 Fig. 16 Three-Dimensional channel network Geometry (a) conductance distribution, (b) hydraulic head
 3 distribution, (c) flow rate distribution, (d) channel network showing only channels of dominant flow



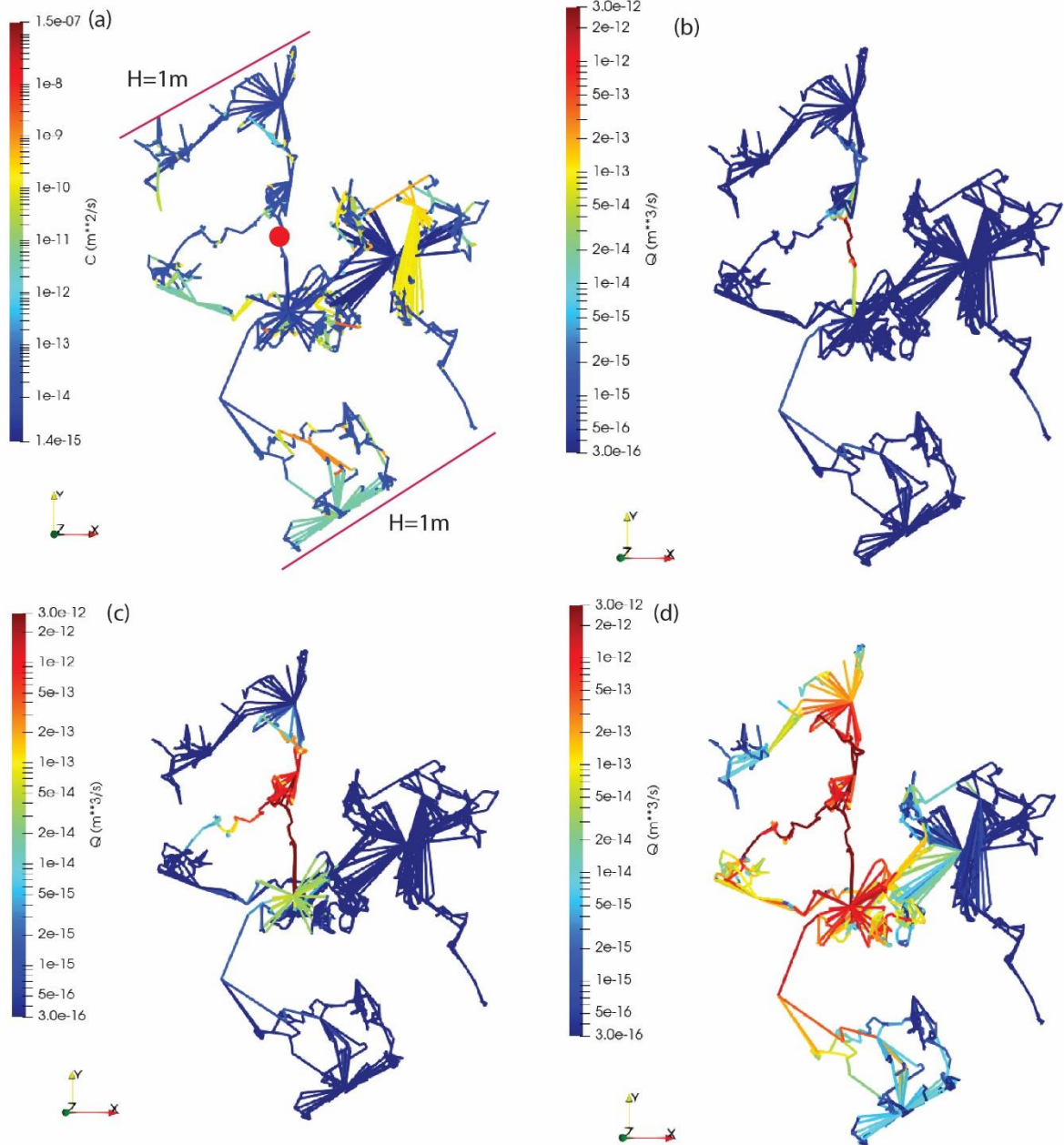
4

5 Fig. 17 Pressure and AFD variation against time in constant flow transient test in 3D network

1 Transient flow response of this 3D lattice network is investigated by performing a constant flow rate test
2 at the centre node. With a constant pressure applied at the outer boundaries, the pressure and AFD variation are
3 plotted with respect to injection time in Fig. 17. It is evident in this figure that AFD starts with $n=1$, try to stabilize
4 at $n=1.5$ (bilinear flow) and then goes to $n=2$ (radial) and 3 (spherical) before hitting the boundary. This study is
5 performed primarily to demonstrate the use of the model to simulate the multidimensional channel network to
6 solve steady state and transient problems.

7 **3.5 Application of transient AFD model to a site-specific fracture network data**

8 After the previous studies in idealized systems, it is of interest to study realistic site data as well.
9 Extensive data sets exist from Forsmark site in Sweden (Selroos et al. 2002). This is site investigated by the
10 Swedish Nuclear Fuel and Waste Management Company (SKB) for the purpose of final disposal of high-level
11 nuclear waste. The site is of low-conductivity crystalline rock and has been extensively characterized in multiple
12 investigation phases (SKB, 2008). To demonstrate the practical application of the AFD model, the approach is
13 used to examine the transient pressure response in a fracture network generated with a data from this site, Sweden.
14 Geometric and hydraulic attributes of the fractures are derived from repository scale DFN models reported by
15 SKB (SKB, 2011), and a corresponding channel network model is built by Sharma et al. (2022) using the approach
16 described by Cacas et al. (1990). The generated 3D fracture network has 3276 fractures and 4353 fracture
17 intersections in a 0.1 km^3 domain, based on which a channel network model (CNM) is developed using the
18 Pychan3D code. Since isolated and dead-end fractures and fracture clusters do not participate in the flow, they are
19 identified and removed from the original network and a hydraulically active backbone structure is obtained
20 (Sharma et al., 2022) as shown in Fig. 18.

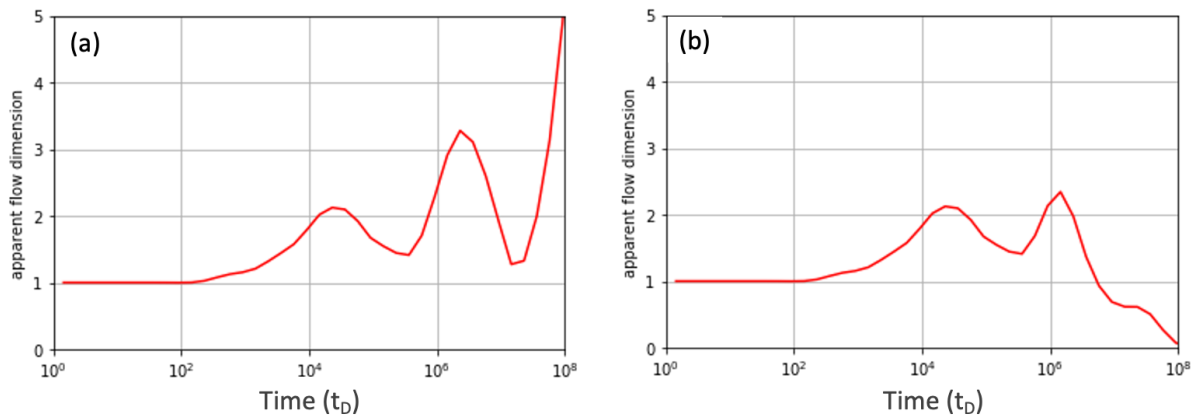


1

2 Fig. 18 A site-specific channel network model. (a) Conductance Distribution, (b) Pseudo steady state flow rate
 3 at injection time, $t_d=2 \times 10^2$, (c) at $t_d=1.3 \times 10^4$, and (d) at $t_d=2 \times 10^5$.

4 To simulate a transient well test, in Fig. 18a, the outer NW and SE boundaries, representing nearby fault
 5 zones, were set at constant hydraulic head of 1m and water was injected at the constant rate of $1 \times 10^{-6} \text{ m}^3/\text{s}$ at a
 6 location shown by red dot near the centre of the domain. In this study, the injection time (t_D) is scaled as t/S where
 7 S is the storativity of the flow medium. The pseudo-steady state flow rate distribution at different dimensionless
 8 times is shown in the Fig. 18b, c, and d. To evaluate the effect of the boundary conditions in an AFD plot, an

1 additional calculation was made by setting the NW and SE boundaries as closed boundaries, which will result in
 2 $AFD=0$ at the large time limit. The obtained apparent flow dimension is shown in Fig. 19. The figure shows that
 3 the flow starts with dimension one and gradually changes depending on the flow geometry and conductance of
 4 the channels encountered by the pressure front before it hits the boundary. The presence of the specified pressure
 5 head boundary as open or closed is observed when flow dimension either rises very sharply at large time to a
 6 value of 5 or more (Fig. 19a), or goes to 0 (Fig. 19b). The flow dimension study using channel network shown in
 7 Fig. 18 unveils two AFD peaks between the early time AFD of 1 and the late time when the boundary effect sets
 8 in. The first AFD peak has a value of 2.1 at about $t_D=10^4$, and the second AFD peak occurs at about $t_D=10^6$. To
 9 account for the impact of the boundary condition, the value of the second peak is estimated to be 2.8 by taking the
 10 average of 3.3 and 2.4 from Fig. 19a and b respectively. In Fig. 18c and d, the flow passes through the clusters
 11 precisely at the same time (t_D) when AFD peaks observed in Fig. 19. The result can well be explained by the
 12 presence of the two clusters of channels on the two sides of the injection point (see Fig.18 a).



13

14 Fig. 19 AFD as a function of time, t_D (t/S) (a) with open boundary, and (b) close boundary for a site-specific
 15 study

16 The AFD behaviour as shown in Fig. 19 may give very useful insight into the changes in conductivity in
 17 space due to branching channels or channels with a larger conductance. The observation that the first peak is
 18 smaller than the second suggests that, along the route of the pressure pulse, it hits the smaller cluster first and then
 19 the larger cluster. If we compare these results with the correlation of conductance increase versus AFD developed
 20 in Fig. 4, the first and second peaks may indicate, respectively, encountering first a channel cluster with one order
 21 of magnitude larger conductance and then a second cluster with one-and-a-half orders of magnitude larger
 22 conductance. Further work may involve multiple injection tests at different locations and aggregate the results. In

1 this way, the AFD method has the potential of providing extra information useful in characterizing the
2 heterogeneity of the flow system.

3 On principle, S in the scaled time $t_D=t/S$ shown in Fig. 19 can be estimated from pressure tests or
4 interference tests using e.g., Theis type curve fitting method. It can also be calculated from a detailed analysis of
5 fracture geometry of the network assuming a fracture storativity value, which however is strongly dependent on
6 in-situ conditions at the site and can vary by several orders of magnitude (Rutqvist et al., 1998). Investigations on
7 this issue are beyond the scope of the present demonstrative application and the time will be simply presented as
8 $t_D = t/S$ in Fig. 19. Different storativity values would move the position of the curve horizontally, but would show
9 the same changes of AFD, which is the focus of our study.

10 **4. Discussion and Conclusion**

11 Flow dimensional analysis in fractured subsurface rock can be quite useful in understanding the system's
12 heterogeneity structure. Since the majority of the flow regimes are non-radial (Ferroud et al. 2018), oversimplified
13 analytical flow models may not be appropriate for studying fractured rock systems. This article discusses the
14 transient testing technique for determining flow dimension in various scenarios, including the real-site case. A
15 flow dimension analysis for a heterogeneous fracture network system was conducted utilizing a channel network
16 model built using the pychan3D model. The study systematically proceeds from idealized 1D, 2D and 3D systems
17 to a field case based on real data.

18 Our results in the 1D cases demonstrate that the AFD substantially changes as a function of channel
19 conductance variation. When encountering a channel with greater conductance the AFD first abruptly increases
20 before decreasing again to $AFD=1$. Conversely, when the flow is encountering a channel with lower conductivity,
21 a clear dip in the AFD is observed. A systematic relationship correlating the magnitude of the conductance contrast
22 and the magnitude of the upsurge/dip in the apparent flow dimension was established from the results (Fig. 4).
23 Such a relationship appears to be useful to estimate the permeability variability in the flow domain from the results
24 of transient well tests even in more complex situations.

25 The study was next extended to 2D domains. Heterogeneity was introduced statistically through
26 conductance distributions with different standard deviation (σ) values. From ensemble averages of 50 realizations,
27 it can be seen that for all σ values the AFD starts from a value of 1, indicating an early-time channelized flow
28 near the borehole. Then, for low σ values (0 and 1) the AFD then converges towards 2, indicating that the flow is

1 taking place radially throughout the system. For higher σ values the AFD does not stabilize at the value of 2 but
2 ranges between 1 and 2, indicating a more channelized flow. The AFD for individual realizations is highly
3 oscillating, with more oscillations and oscillations with higher amplitude with increasing σ . In field situations,
4 such single realizations (corresponding to a single well test) could be used to observe the variation of conductance
5 as the pressure front proceeds through the rock medium, according to the relationship presented in Fig. 4. If,
6 instead, a number of realizations (corresponding to a number of well tests at different locations in the same
7 network) are available, an ensemble mean could give an indication of the overall heterogeneity characteristics of
8 the system.

9 A study was also conducted for a geometrically specified (deterministic) heterogeneity introduced into
10 the 2D stochastic network. This was implemented by considering a linear zone of constant width within which
11 the conductances were made significantly greater than that of the surrounding area. As to be expected for $\sigma=0$,
12 the flow is found to be channelled through the high conductive linear zone, while for the $\sigma=1$ case, two degrees
13 of channelized flow was observed: a primary channelization occurs in the linear zone and a secondary
14 channelization also occurs within this zone due to the local conductance variability.

15 As the next step, the study was extended to 3D channel networks. In this case the channels have
16 conductance values that follow a lognormal distribution with $\sigma=1$. As could be expected, the AFD in this case
17 first starts with $n=1$, then successively proceeding to $n=1.5$, 2 and 3, when the flow becomes more space-filling
18 and is going from bilinear to radial and spherical before finally encountering the boundary.

19 After these idealized cases, the study was extended to investigate the AFD in a set of actual site-specific
20 fracture data (Sharma et al., 2022) from Forsmark, Sweden (Fig. 18). Here two peaks were observed in the AFD
21 variation before the onset of the boundary effects. The behaviour could be explained by the presence of two main
22 clusters of channels in the flow domain on the two sides of the injection point. When compared with the correlation
23 between conductance contrast and AFD presented in Fig. 4, the two channel clusters may represent a conductance
24 increase of 1 and 1.5 orders of magnitude respectively. If such transient well test data were available from several
25 injection wells at different locations in the channel network, a joint AFD analysis of all results may provide useful
26 data in the characterization of flow heterogeneity of the domain.

27 It should be emphasized that characterizing the heterogeneity structure of a flow domain, especially for
28 fractured rock, is a challenging task. It requires multiple and complementary inputs from different types of data,

1 such as fracture mapping on outcrops or tunnel surfaces, downhole imaging of fractures on borehole walls, flow
2 (dilution) tests, single hole pressure tests, multiple hole interference tests, and tracer tests. The AFD analysis of
3 transient pressure data over a long-time frame is an additional input that will help in this effort.

4 The main limitation and challenge of the AFD approach is the use of pressure derivatives in its analysis,
5 which are very sensitive to minor variations in pressure data. Perhaps this can be alleviated by the use of data
6 smoothing techniques and/or joint analysis of transient pressure data from multiple injection points in the flow
7 domain and multiple repeated well tests from the same well. Another limitation is the time scale required for the
8 pressure transient tests, which strongly depends on the overall permeability and storativity of the flow domain.
9 Thus, the time to observe AFD variations may be too short (too fast) or too long to make this method practical in
10 some field applications.

11 Finally, it should be noted that determination of hydraulic properties of a flow domain by assuming
12 uniform properties and ignoring its heterogeneity structure may lead to significant errors, unless the heterogeneity
13 is of very small range compared with the size of flow domain of interest. For fractured rocks and even for many
14 aquifer systems, this assumption may well be invalid. The present paper presents a systematic study with some
15 insight gained on the particular AFD approach, and further work will be carried out to address its limitations and
16 better define its ranges of applicability under field conditions.

17 **Acronyms and symbols**

<i>GRF</i>	Generalized Radial Flow
<i>AFD</i>	Apparent Flow Dimension
<i>RMS</i>	Root mean square
<i>DFN</i>	Discrete Fracture Network
<i>CNM</i>	Channel network model
<i>C</i>	Conductance
<i>Q</i>	Flow Rate
<i>h</i>	Pressure drawdown/build up
<i>T</i>	Transmissivity
<i>w</i>	Width of the channel
<i>L</i>	Length of the channel
<i>Mc</i>	Laplacian matrix
<i>Bc</i>	Vector of boundary condition
<i>n</i>	Flow dimension
<i>h'</i>	Pressure derivative
<i>t</i>	time
<i>V*</i>	Slope of pressure derivative
<i>t_d</i>	Scaled injection time
<i>S</i>	Storativity
<i>N</i>	nodes
<i>σ</i>	Standard deviation

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6 **Conflicts of interest**

7 The authors have no conflicts of interest.

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