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## Automated lab-scale production of PVA/PEG-enzyme immobilisates

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Nora C. Bieler, Marion B. Ansorge-Schumacher, Lasse Greiner, Lasse Greiner

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## Technical Report

### Automated Lab Scale Production of PVA/PEG-Enzyme Immobilisates

Nora C. Bieler<sup>1</sup>, Marion B. Ansorge-Schumacher<sup>1</sup> and Lasse Greiner\*<sup>2,3</sup>

<sup>1</sup>Institute of Chemistry, Enzyme Technology, TU Berlin, Berlin, Germany

<sup>2</sup>Institut für Technische und Makromolekulare Chemie, RWTH Aachen University, Aachen, Germany

<sup>3</sup>DECHEMA e.V. Karl-Winnacker-Institut,, Frankfurt am Main, Germany

**Keywords:** immobilisation, polyvinyl alcohol, automated production, biocatalysis, entrapment

**Correspondence:** Lasse Greiner, Dr. rer. nat., Institut für Technische Chemie und Makromolekulare Chemie, RWTH Aachen University, Worringerweg 1, 52056 Aachen, Germany.

Email: [greiner@dechema.de](mailto:greiner@dechema.de), Tel.: +49 69 7564 428, Fax: +49 241 806 264 84

**Abbreviations:** **BAL**, benzaldehyde lyase, **SEM**, scanning electron microscopy,

**PVA**, polyvinyl alcohol, **PEG**, polyethylene glycol

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6 **Abstract.** Entrapment of biocatalysts by cryogelation is a gentle method to  
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8 extend the scope of biocatalysis. To foster the use of this versatile method we  
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10 devised an automated injector for the production of polyvinyl alcohol  
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12 (PVA)/polyethylene glycol (PEG) beads. The device consists of a thermostated  
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14 reservoir connected to a programmable injector nozzle and an agitated receiving  
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16 bath for the droplets. This lab scale production unit yields up to 1500 beads with  
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18 immobilised enzyme per minute with a narrow size distribution and good  
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20 roundness.  
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## 1 Introduction

In the field of biocatalysis the advantages of immobilised biocatalysts were early recognised and exploited [1, 2]. Recently, it could be shown that entrapment of biocatalysts in hydrogel beads allows stable operation in otherwise deteriorating solvents [3]. Therefore, matrix entrapment of biocatalysts in natural and synthetic polymers provides a means to overcome the limitations implied by the aqueous environment which a broad range of biocatalysts require for activity and stability [4].

As entrapment matrix PVA/PEG cryogels show a number of distinct advantages [5]. They exhibit high micro- and macroporosities resulting in high mass transfer rates and show a high stability towards a wide range of compounds. The shear resistance allows application in a broad range of reactor types, which makes PVA-cryogels superior over commonly used thermoreversible gels. Furthermore the starting material is non-toxic and readily available at reasonable costs.

Entrapment in PVA cryogels is a widely applied method for the immobilisation of whole cells, and has also been described for palladium catalysts [5, 6, 7]. As isolated enzymes benzaldehyde lyase from *Pseudomonas fluorescens* Biovar I. (EC 4.1.2.38), carbonyl reductase from *Candida parapsilosis* (EC 1.1.1.1), alcohol dehydrogenase from

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6 *Lactobacillus kefir* (EC 1.1.1.2), and hog pancreas lipase (EC 3.1.1.3) have  
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8 recently been entrapped and successfully applied to synthetic reactions in  
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10 pure organic solvents [8, 9, 10]. Due to the mild entrapment conditions the  
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12 activity yield was high even for sensitive enzymes. Generally, the stability  
13  
14 towards organic solvents was increased by at least an order of magnitude.  
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18 PVA/PEG cryogels are most commonly applied as beads, because of the  
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20 favourable hydrodynamics and abrasion stability in reactors. They are  
21  
22 produced by cryogelation [11, 12, 13], i.e. a solution of PVA and PEG is  
23  
24 added dropwise to silicone oil at 250 K, and gelation is induced by successive  
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26 heating to room temperature [14]. Mostly, these are prepared manually.  
27  
28 However, the highly viscous PVA/PEG solution gives rise to handling issues  
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30 and large-scale production is prone to induce tenosynovitis when performed  
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32 manually. The JetCutter as developed by Vorlop and coworkers was  
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34 successfully employed for the production of enzyme immobilisates [15]. It is  
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36 well suited for solutions with lower viscosity such as Ca-pectinate, Ca-  
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38 alginate, Chitosan, gelatin and smaller bead diameters typically below 1 mm  
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40 [15]. However, losses of 5-20% induced by the shear from the cutting are  
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42 inevitable [16]. Lozinsky and coworkers hint towards an automated device as  
43  
44 a Russian patent (as cited in ref. 12) apparently using pressure driven sheath  
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46 flow to produce droplets but no quantitative data is accessible in literature.  
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48 Again, in our experience the pressure drop over the nozzle in such setups is  
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50 hard to predict or control, rising reproducibility issues.  
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6 In this study, a device for the automated production of spherical PVA/PEG  
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8 cryogels for enzyme entrapment is presented. Evaluation was performed with  
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10 regard to immobilisation performance, reproducibility, bead shape and size,  
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12 as well as morphology of the resulting material.  
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## 18 **2 Materials and Methods**

### 21 **Technical set up**

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24 Micro-Liquid-Dispenser SMLD 300G was purchased from Fritz Gyger AG  
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26 (Thun-Gwatt, Switzerland). Electronical equipment was build by the  
27  
28 university workshops of RWTH Aachen University and TU Berlin. Wacker  
29  
30 AP 100 Silicone oil (Wacker Chemie AG, Burghausen, Germany) was used  
31  
32 as hardening solvent for PVA/PEG solution. An Ecoline Staredition RE300  
33  
34 thermostat with external temperature sensor from Lauda (Lauda-Königshofen,  
35  
36 Germany) with silicone oil M10 (Carl Roth, Karlsruhe, Germany) as coolant,  
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38 was used. The sample container was thermostated by a water bath (MgW  
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Lauda Thermo-star C3).

### 48 **Preparation of PVA/PEG solution**

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51 Polyvinyl alcohol Mowiol 10-98 (polymerisation degree: 1400) and  
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53 polyethylene glycol 1000 were purchased from Fluka (Neu-Ulm, Germany).  
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55 A mixture of 10% (w/v) PVA and 10% (w/v) PEG was dissolved in deionised  
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water at 90°C, 30 mg NaOH/g PVA was added at room temperature and the



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6 solution was stirred for 30 minutes to cleave ester residues in the commercial  
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8 PVA solution. The pH was adjusted to 8.0 with concentrated HCl [8].  
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### 10 **PVA bead analysis**

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12 For analysis of size distribution PVA beads were removed from the silicone  
13  
14 oil bath, washed with distilled water and sieved (ISO 3310/1, Retsch, Haan,  
15  
16 Germany). Size exclusions in sieve analysis were 5.00, 4.00, 3.55, 3.15, 2.50,  
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18 2.00, 1.40, 1.00, 0.80, 0.60, 0.50, 0.40, 0.30 and 0.10 mm.  
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24 For shape analysis PVA beads were prepared by dyeing with ethanol/aqueous  
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26 solution (20%, (v/v)) of 0.1% (w/v) Bromocresol green for 30 seconds. A  
27  
28 digital picture (Olympus SP-500UZ) was converted to greyscale with  
29  
30 maximum contrast via GIMP (Version 2). The pictures were subsequently  
31  
32 analysed for bead roundness with the software Image Tool® (Version 3.0).  
33  
34 The bead shape was described by roundness and compactness. Roundness is  
35  
36 defined as  $(4*\pi*area)/perimeter^2$  where perimeter is the length of the outside  
37  
38 boundary of the object. Compactness is given by  $(4*area/\pi)^{1/2}/major\ axis$   
39  
40 length. Both parameters are the closer to unity the rounder or closer to ideal  
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42 circular the object is.  
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48 For scanning electron microscopy (SEM) PVA beads were prepared by shock  
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50 freezing in liquid nitrogen and freeze drying (Alpha 1-2 LD plus, Christ,  
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52 Riedstadt, Germany). SEM was conducted using a Hitachi S-2700 instrument  
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54 at an acceleration voltage of 20 kV. Samples were fixed on double-sided  
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56 adhesive foils and sputtered with thin gold films.  
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### Activity assay

Benzaldehyde lyase (BAL) from *Pseudomonas fluorescens* Biovar I [E.C.4.1.2.38] was expressed and purified using the recombinant *E. coli* SG13009<sub>prep4</sub> [pBAL-his<sub>6</sub>] as described previously [17]. In the PVA/PEG solution lyophilised BAL (0.5 U mL<sup>-1</sup>), thiamine diphosphate (0.1 mmol L<sup>-1</sup>), and MgSO<sub>4</sub> (2.5 mmol L<sup>-1</sup>) were dissolved [8]. The activity of BAL immobilised in PVA/PEG beads was determined by monitoring the BAL-catalysed carbonylation of benzaldehyde to benzoin by gas chromatography (Shimadzu 2010 using a BTX column from SGE). Reactions were performed at 303 K in closed glass vessels containing 17 g of immobilisates and 10 mL of 200 mM benzaldehyde (Sigma-Aldrich, Steinheim, Germany) in *tert*-butyl methyl ether (Carl Roth, Karlsruhe, Germany).

## 3 Results

### Set up

It was aimed for a device which would give spherical beads with narrow size distribution. Besides, thermal stress on the enzyme should be reduced to minimum. Also the influence of temperature on the cryogelation process was target of our investigations both the storage temperature and the bath temperature should be varied. The overall setup consists of the dosing unit and a thermostated bath.

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6 The dosing unit is a double jacket tube (50 mL inner volume) with top side  
7 connection for either compressed air or nitrogen. The outlet consists of a  
8 commercially available microvalve which was embedded into an electrically  
9 heated block allowing dosage of viscous solutions at low pressures.  
10 Temperature and valve parameters were controlled electronically. Typically,  
11 the PVA/PEG enzyme solutions were transferred to the tube and pressurised  
12 to 5 kPa with nitrogen. The scheme of the dosing unit is shown in figure 1.  
13 For the investigated system the injection temperature could be kept at room  
14 temperature. Thereby, thermal stress of the enzyme was minimised.

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The outlet of the valve was directed into a double jacket insulated silicone oil  
bath. Circulation in the receiving bath was maintained by a stirrer. The bath  
layout prevented the agglomeration of beads by coalescence of droplets. The  
distance from the valve outlet to the bath surface was adjusted to give  
spherical beads. Too short distances lead to the distortion of shape and a  
distance of 20 cm was found to give best results (Figure 1).

The PVA/PEG enzyme solution was injected into the receiving bath at 248 K.  
The frozen beads were collected into a dent of the bath by the induced flow.  
After the injection process the temperature was increased to 298 K over  
500 minutes [18, 19]. Shortening to 180 minutes led to PVA beads with no  
apparent differences in stability, flexibility, and porosity. Higher initial  
temperatures of 268 K for the receiving bath were tested in accordance with  
literature [12, 20]. The obtained beads showed deviations from spherical

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6 shape, presumably because freezing time is prolonged, so that beads were  
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8 deformed by the stirrer.  
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### 10 **Bead size and shape**

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12 Size of PVA/PEG beads is a function of opening and closing times of the  
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14 valve. We tested three time programs at 20 ms, 40 ms, and 60 ms opening  
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16 times with 20 ms, 25 ms, and 30 ms pause, respectively (Figure 2). This  
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18 theoretically equates to 25, 15, and 11 beads per second allowing the  
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20 formation of beads needed for a typical lab scale continuous fluidised bed  
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22 reactor within minutes [21].  
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28 With 60 ms 47% of all obtained beads were within 2.5 to 3.15 mm in  
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30 diameter correlating to 73% of the total mass. 83% of the mass of the beads  
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32 were contained within 2.5 and 3.55 mm. At 40 ms smaller PVA beads with  
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34 80% of all the produced beads within a diameter of 2.0 to 2.5 mm were  
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36 obtained. 72% of the beads showed a diameter of 2.5 mm. The shortest tested  
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38 impulse length of 20 ms led to a size distribution of PVA immobilisates  
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40 where 83% had a diameter between 1.4 and 2 mm. 88% of all these beads  
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42 were ranged in size between 1 and 2 mm. On average the yield of beads per  
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44 mass was around 75% and is due to losses in the storage vessel and at the  
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46 nozzle.  
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52 So far, the production of beads is only limited by clogging after time which  
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54 occurs as a result of gelation taking place at the nozzle. As the gelation  
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56 process is envisaged to be induced by local high concentrations of PVA  
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6 during the thawing process favouring the formation of hydrogen bonds [13]  
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8 the reason for this gel formation at the nozzle is unclear. Here, deeper  
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10 understanding of the gelation process as well as the probable role of wetted  
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12 materials in the nozzle is needed for further improvement.  
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15 Besides the size distribution roundness is an issue for mass transfer and  
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17 robustness [22]. Bead shape analysis was performed for four bead batches. As  
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19 indicator for a perfectly round shape roundness =  $(4 \pi \text{ area perimeter}^{-2})$  and  
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21 compactness =  $(4 \text{ area } \pi^{-1})^{1/2}$  major axis length can be applied. Both indicators  
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23 approach unity for ideal spheres. An average roundness of  $0.85 \pm 0.03$  was  
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25 determined. Compactness was determined as  $0.95 \pm 0.02$ . Both parameters  
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27 indicate a close spherical shape of the beads.  
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### 33 **Gel morphology**

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35 The structure and the pore size of the PVA/PEG cryogels resulting from the  
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37 automated production were determined via scanning electron microscopy  
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39 (SEM) (Figure 3). Typical sponge structure and pore sizes around  $1 \mu\text{m}$  are in  
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41 line with previously obtained results [23]. In contrast to manually produced  
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43 PVA beads gas inclusions of varying sizes were observed in 80% of the  
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45 beads.  
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51 However, the activity tests with entrapped BAL showed within the error  
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53 margin the same activity and storage stability as the manually produced  
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55 beads. Typically a productivity of  $40 \mu\text{mole h}^{-1}$  per immobilised U of BAL  
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57 were obtained.  
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#### 4 Conclusion

We set up a means for standardised automated PVA/PEG immobilisate lab scale production. Our method achieves high productivity of up to 1500 beads per minute. The size distribution of the PVA beads is narrow and the diameter can be varied by the valve pulse interval. The obtained beads are spherically shaped and robust allowing the use in a range of reactor configurations. Temperature stress during production of PVA/PEG immobilisates is low as temperatures are at or below room temperature. Furthermore the presented set up for automated bead production is straightforward and the additional costs are low. The used liquid dispenser is readily available. Our design for routine lab-scale production of beads now enables application of these promising immobilisates in larger scale.

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The authors have declared no conflict of interest.

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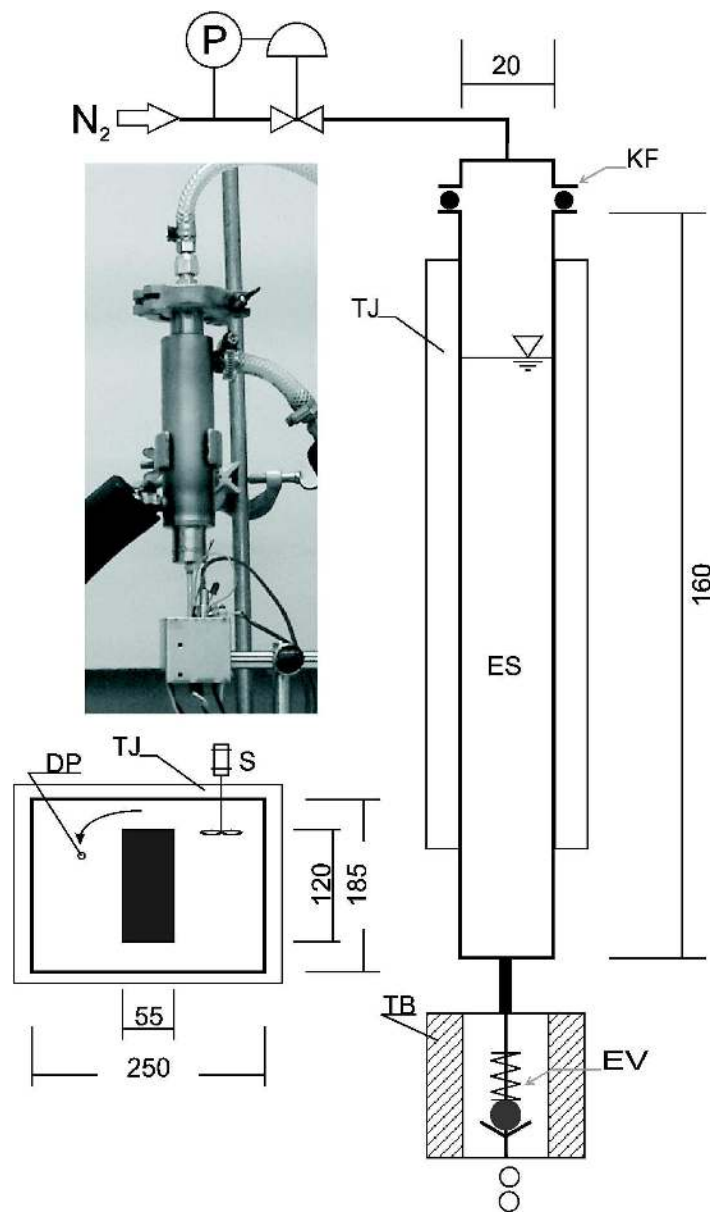


## Figure legends

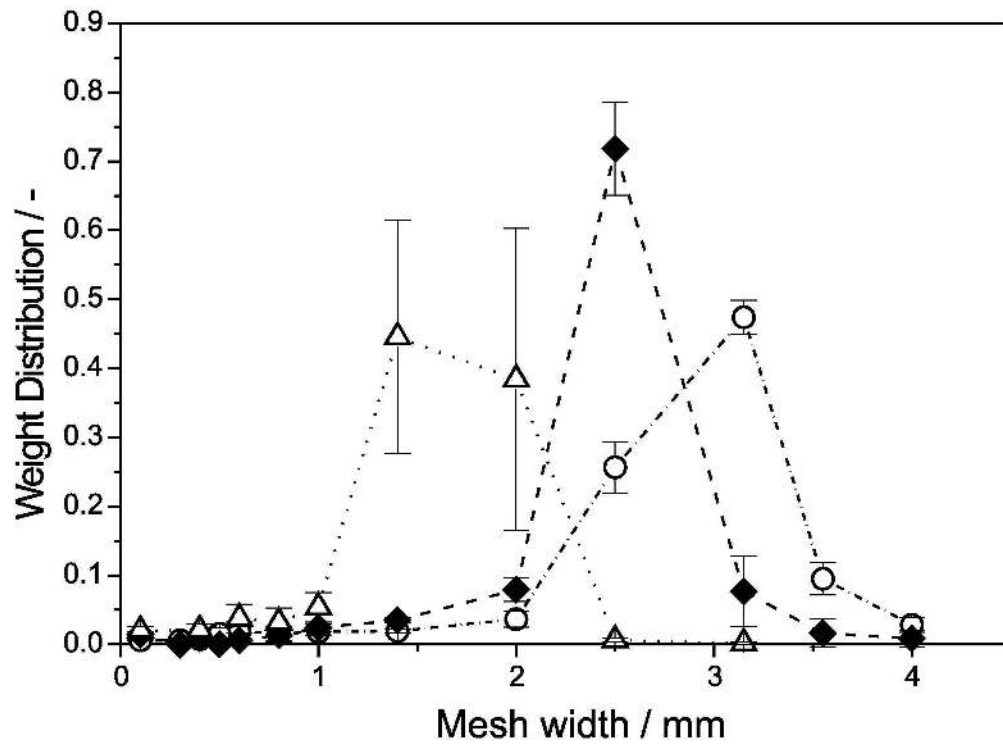
**Figure 1.** Setup of the apparatus, right: dosing unit with electronic valve (EV) and thermostated storage for the enzyme solution (ES); middle left: photograph of the injection module; lower left: top view of the receiving bath with flow direction and drop point (DP) (dimensions in mm, KF: flange with O-ring, P: manometer, S: stirrer, TJ; thermostated jacket, TB: thermoblock).

**Figure 2.** Size distribution of automatically produced PVA/PEG immobilisates as a function of valve opening time (open spheres) 60 ms, (closed diamonds) 40 ms and (open triangles) 20 ms.

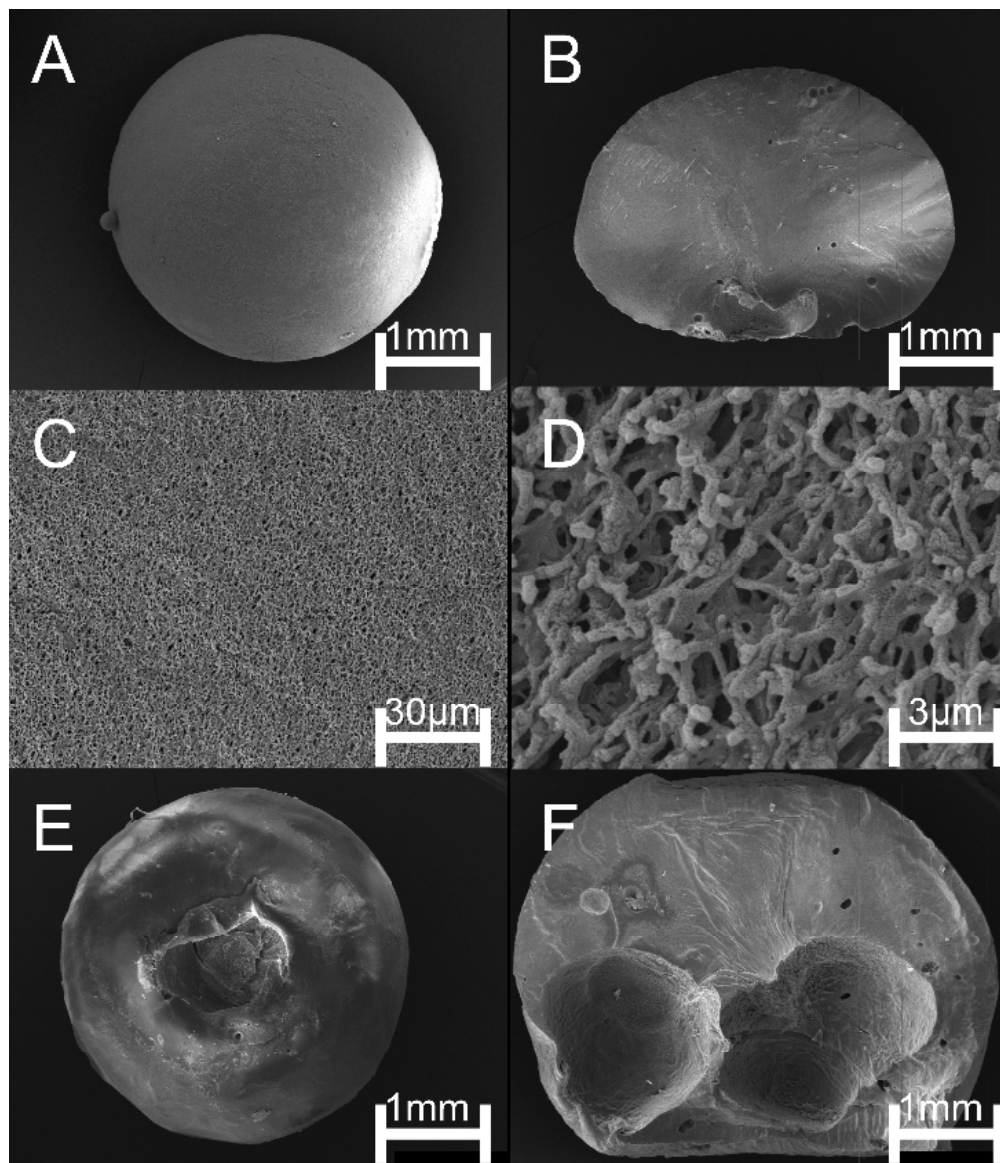
**Figure 3.** SEM images of beads (A) surface, (B-D) cross sections with increasing magnification, (E+F) surface and cross section of a bead with gas entrapment.



Setup of the apparatus, right: dosing unit with electronic valve (EV) and thermostated storage for the enzyme solution (ES); middle left: photograph of the injection module; lower left: top view of the receiving bath with flow direction and drop point (DP) (dimensions in mm, KF: flange with O-ring, P: manometer, S: stirrer, TJ: thermostated jacket, TB: thermoblock).  
150x257mm (600 x 600 DPI)



Size distribution of automatically produced PVA/PEG immobilisates as a function of valve opening time (open spheres) 60 ms, (closed diamonds) 40 ms and (open triangles) 20 ms. 90x68mm (600 x 600 DPI)



SEM images of beads (A) surface, (B-D) cross sections with increasing magnification, (E+F) surface and cross section of a bead with gas entrapment.  
123x142mm (600 x 600 DPI)