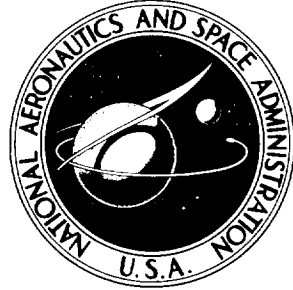


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**FORTRAN PROGRAM FOR PREDICTING
OFF-DESIGN PERFORMANCE
OF CENTRIFUGAL COMPRESSORS**

by Michael R. Galvas

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and

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FORTRAN PROGRAM FOR PREDICTING OFF-DESIGN PERFORMANCE OF CENTRIFUGAL COMPRESSORS

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SUMMARY

A FORTRAN program for calculating the off-design performance of centrifugal compressors with channel diffusers is presented. Use of the program requires complete knowledge of the overall impeller and diffuser geometries. Individual losses are computed using analytical equations and empirical correlations which relate loss levels to velocity diagram characteristics and overall geometry. On a given speed line compressor performance is calculated for a range of inlet velocity levels. At flow rates between surge and choke, individual efficiency decrements, compressor overall efficiency, and compressor total pressure ratio are tabulated. An example case of performance comparison with a compressor built by a commercial engine manufacturer is presented to demonstrate the correlation with limited experimental data.

INTRODUCTION

Centrifugal compressors are frequently used in refrigeration cycles, refining systems, aircraft auxiliary systems, turboshaft engines, and other systems where lightweight compact compression is required. The off-design performance characteristics of centrifugal compressors are of interest because of the large effects that compressor component performance has on overall cycle performance and because the compressor is required to operate at off-design conditions much of the time. For turboshaft engines assuming a drive turbine inlet temperature of 1422 K and efficiency of 90 percent, a 2.6-percent loss in compressor efficiency results in a 2-percent increase in engine specific fuel consumption (SFC) and a 2.8-percent loss in engine power at design speed. These losses become more pronounced at part-power settings. In addition to good performance at off-design flow rates it is important that the compressor operate stably over

the range of flows and speeds required by the engine operating envelope. The usable range of the compressor pressure ratio-mass flow characteristic is bounded by the surge and choke mass flow rates. Operation at flows less than the surge point flow should be avoided because of potentially dangerous vibrations induced by the intermittent flow reversals and power loss. Operation with the compressor choked is generally avoided because of the poor compressor efficiency and pressure ratio at the choke point. The problem undertaken in this analysis is to determine the centrifugal compressor performance characteristics over a range of rotative speeds and flow rates and predict the usable range of flow rates at which the compressor can operate. The method of analysis uses the loss correlations and equations of reference 1 with surge and choke criteria added to predict compressor operating range.

A FORTRAN program has been developed at NASA Lewis Research Center which predicts centrifugal compressor performance through utilization of empirical correlations which are related to the compressor geometry and velocity diagram characteristics. A complete knowledge of the compressor overall geometry and working fluid inlet total conditions is required for its use. Working fluid state conditions and flow properties are calculated using a mean streamline one-dimensional analysis. The program is limited to centrifugal compressors with channel diffusers operating up to their choke point. A comparison of calculated and experimental performance is given to demonstrate the correlation with limited experimental data. The experimental data presented for comparison were obtained from a compressor developed by Solar Aircraft Company, Division of International Harvester, Inc. Shock losses in the rotor are neglected. Clearance losses are considered to be inherent in the impeller losses since good performance correlation is achieved on compressors operating with reasonable clearances.

METHOD OF ANALYSIS

Input values of $(V/V_{cr})_0$ are used to determine compressor mass flow rate. (Symbols are defined in appendix A and compressor stations are shown in fig. 1.) Individual losses are calculated using velocity diagram characteristics and empirical correlations determined by the input absolute velocity level and compressor geometry. For compressors having inlet guide vanes it is assumed that the vanes are placed in a constant-area annulus having no wall curvatures or slopes. Overall compressor efficiency, total pressure ratio, and mass flow rate are tabulated for each operating point inside the predicted range for each speed line that is input. A complete discussion of the loss calculations is discussed in appendix B.

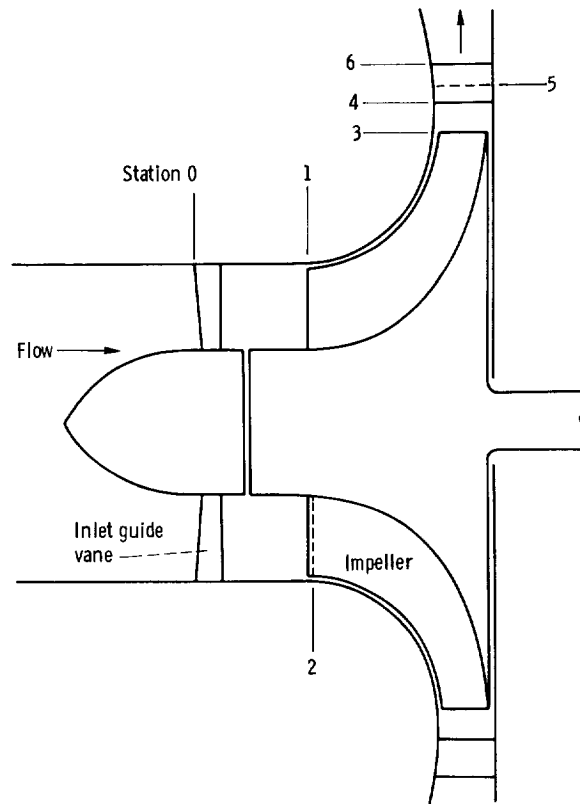


Figure 1. - Meridional cross section of compressor.

Required Information

The compressor data needed to use the FORTRAN program are the following: inducer inlet tip diameter, inducer inlet hub-tip diameter ratio, inducer inlet blade angle at the root-mean-square diameter, inducer blade blockage at the rms diameter, inducer inlet hub and tip wall slopes, inducer inlet hub and tip wall curvatures, inlet solid-body swirl angle at the rms diameter, inducer-tip to impeller-exit diameter ratio, impeller exit blade angle, impeller blade exit height, number of impeller blades at exit, vaneless diffuser diameter ratio, vaned diffuser setting angle, total vaned diffuser throat area, vaned diffuser area ratio, skin friction coefficient of the wetted surfaces, design rotative speed, and the fraction of design rotative speed for which the calculations are to be performed.

The working fluid properties and state conditions required are: inlet total pressure, inlet total temperature, inlet dynamic viscosity based on total conditions, specific heat ratio, and gas constant.

Two control variables are used to select the options of solid-body prewhirl and impellers with splitter blades. Inducer inlet hub and tip wall slopes and curvatures are all

set equal to zero for compressors with inlet guide vanes.

Information which corresponds to the design speed line for the example compressor is as follows:

Compressor data	
Design rotative speed, N , rpm	72 000
Inducer inlet tip diameter, D_{1T} , m	0.0813
Inducer hub-tip diameter ratio, λ	0.5313
Inducer inlet hub wall curvature, C_{1H} , m^{-1} (positive around axis of rotation)	0
Inducer inlet tip wall curvature, C_{1T} , m^{-1} (positive around axis of rotation)	0
Inducer inlet hub wall slope, χ_H , deg from axial	7
Inducer inlet tip wall slope, χ_T , deg from axial	0
Inducer inlet blade angle at the rms diameter, β_{1MFb} , deg from meridional	49.0
Inducer-tip to impeller-exit diameter ratio, D_{1T}/D_3	0.5614
Number of impeller blades at exit, Z_3	32
Impeller blade exit angle, β_3 , deg from meridional (positive opposite to direction of rotation)	25
Impeller exit blade height, b_3 , m	0.0051
Vanless diffuser diameter ratio, D_4/D_3	1.14
Vaned diffuser setting angle, α_4 , deg from meridional	78
Total vaned diffuser throat area, A_5 , m^2	0.00071
Vaned diffuser area ratio, A_6/A_5	2.7
Friction coefficient, C_f	0.004
Working fluid properties and state conditions	
Specific heat ratio, γ	1.4
Gas constant, R , $J/(kg)(K)$	287.05
Inlet total pressure, p'_0 , N/m^2	101 325
Inlet total temperature, T'_0 , K	288.15
Inlet dynamic viscosity based on total conditions, μ'_0 , $N\text{-sec}/m^2$	1.788×10^{-5}
Velocity diagram properties	
Number of values of compressor inlet absolute critical velocity ratios used in calculating performance	15
Compressor inlet absolute critical velocity ratios, $(V/V_{cr})_0$	0.47 to 0.61
Inducer inlet solid-body swirl angle at the rms diameter, α_{1MF} , deg from meridional	0
Splitter control variable, SPLT (SPLT = 0, no splitter blades; SPLT = 1, splitters)	1

Calculated Losses

Inlet guide vane loss. - Equations relating working fluid kinetic energy level, boundary layer, and blade geometry were developed for axial turbine stators in reference 2. These equations were used to calculate state conditions downstream of the inlet guide vanes; thus the velocity diagram characteristics were found by satisfying one-dimensional continuity.

An inlet guide vane loss coefficient is calculated using the same assumptions about blade geometry and boundary layer characteristics as used in reference 3. The inlet guide vane loss is then calculated as a fraction of the ideal kinetic energy at the rms diameter.

Inducer incidence loss. - Reference 4 developed equations for optimum inducer incidence angle of centrifugal compressors with axial inlets. The optimum incidence angle is calculated from the inlet velocity diagram characteristics and blade blockage at the rms diameter assuming an incompressible working fluid. The enthalpy loss due to incidence is calculated assuming that the relative velocity component normal to the optimum incidence angle is lost. Therefore, the incidence loss is simply

$$\Delta h_{\text{INC}} = \frac{W_{\text{L}}^2}{2C_{\text{p}}}$$

where

$$W_{\text{L}} = W_{1\text{MF}} \sin |\beta_{\text{opt}} - \beta_{1\text{MF}}|$$

Blade loading loss. - Boundary layer growth in the impeller is highly dependent on the diffusion of the working fluid internal to the impeller itself. Reference 5 proposed an equation for calculating the diffusion factor of the impeller based on a uniform velocity loading along the blade chord. This equation is used to calculate the impeller diffusion factor for impellers without splitters. A modified form, with reduced penalty due to aerodynamic work input, is used for impellers which have a set of splitter blades. With the diffusion factor calculated by these methods the blade loading loss was expressed as

$$\Delta h_{\text{BL}} = 0.05 D_{\text{f}}^2 u_3^2$$

Skin friction loss. - In addition to the losses resulting from the aerodynamic loading of the impeller blades, the impeller incurs losses due to skin friction of the impeller

and shroud wetted areas. Reference 5 developed an equation for this loss based on fully developed turbulent pipe flow. In the case of impellers with splitter blade rows, the empirical constant appearing in the equation is modified to account for the higher mean channel relative velocity caused by the addition of splitters. The general equation used for skin friction loss is

$$\Delta h_{SF} = K_{DF} C_f \frac{\frac{L}{D_3}}{\frac{D_{HYD}}{D_3}} \left(\frac{W}{u_3} \right)_{av}^2 u_3^2$$

where $K_{SF} = 5.6$ for conventional impellers and $K_{SF} = 7.0$ for impellers with tandem blades.

Disk friction loss. - The specific loss due to windage on the compressor back face is calculated using the equation

$$\Delta h_{DF} = 0.01356 \frac{\rho_3}{w Re^{0.2}} u_3^3 D_3^2$$

This is a form of the disk friction power loss of reference 6.

Recirculation loss. - Losses resulting from work done on the working fluid due to backflow into the impeller are expressed as

$$\Delta h_{RC} = 0.02 \sqrt{\tan \alpha_3} D_f^2 u_3^2$$

This is a modification of the equation proposed in reference 5.

Vaneless diffuser loss. - The flow angle and Mach number variation with radius in the vaneless space are determined by numerical solution of the differential equations for vaneless space flow developed in reference 7. The equations are simplified through the assumptions of adiabatic flow and constant geometric depth passage. The radial total pressure distribution in the vaneless space is calculated using the equation derived in reference 5. When the fluid state and flow properties are determined at the vaned diffuser leading edge radius by the methods described previously, the vaneless diffuser loss is calculated from the equation

$$\Delta h_{VLD} = C_p T_3' \left[\left(\frac{p_4}{p_4'} \right)^{(\gamma-1)/\gamma} - \left(\frac{p_4}{p_3'} \right)^{(\gamma-1)/\gamma} \right]$$

Vaned diffuser loss. - Curves of maximum static pressure recovery coefficient at a given area ratio were extrapolated from the test data for square throat diffusers reported in reference 8 for various combinations of vaned diffuser throat Mach number, aerodynamic blockage, and area ratio. These data were recorded for channel diffusers with symmetrical pressure loadings about the channel centerline. The vaned diffuser in a centrifugal compressor is loaded with a pressure gradient across the channel. In this analysis it was assumed that the difference in the loadings between the test diffusers of reference 8 and the compressor diffusers would have no effect on calculated diffuser recovery. A one-seventh power velocity distribution in the boundary layer along the vaneless space endwalls is used to calculate the displacement thickness representing vaned diffuser throat blockage. The value of static pressure recovery coefficient C_p^{**} corresponding to the vaned diffuser geometric area ratio, inlet Mach number, and aerodynamic blockage is extrapolated from the test data.

The vaned diffuser exit critical velocity ratio is calculated using one-dimensional continuity. Vaned diffuser loss is then calculated using the equation

$$\Delta h_{VD} = C_p T_3' \left[\left(\frac{p_6}{p_6'} \right)^{(\gamma-1)/\gamma} - \left(\frac{p_6}{p_5'} \right)^{(\gamma-1)/\gamma} \right]$$

Calculation of Compressor Choking Flow

Two criteria are used in the prediction of compressor choking flow: (1) inducer choke and (2) vaned diffuser choke. Reference 9 presented data on inducer choking incidence levels as functions of relative Mach number and blade angle at the rms diameter for inducer pitch-chord ratios of 0.5 and thickness-chord ratios of 0.05. These data were used to predict compressor choking flow due to inducer choke.

Vaned diffuser choke is predicted from one-dimensional continuity using the computed values of weight flow, total temperature, total pressure, aerodynamic blockage, and the geometric throat area. The maximum value of the one-dimensional weight flow function is calculated from the equation

$$\left(\frac{w \sqrt{T_3}}{p_5^* A_{5B5}} \right)_{\max} = \sqrt{\frac{\gamma}{R(\gamma + 1)} \left(\frac{2}{\gamma + 1} \right)^{(\gamma + 1)/(\gamma - 1)}}$$

At the first input critical velocity ratio where the left side of the equation equals or exceeds the right side the compressor is choked. One would expect the speed lines to have infinite slopes at the choke point. The vertical portions of the speed lines are approximated through the assumption of zero static pressure recovery in the vaned diffuser for the cases of vaned diffuser choke. The impeller characteristic should exhibit a vertical slope at the impeller choke point but this is not predicted by the correlations used.

Calculation of Compressor Surge Point

The vaned diffuser is assumed to be the component which governs the location of the compressor surge point. Examination of performance characteristics of centrifugal compressors covering a range of pressure ratios indicates that compressor flow range can be expressed as a function of the vaned diffuser leading edge Mach number. With a good impeller-diffuser throat area match the flow range will vary with the diffuser leading edge Mach number as shown in figure 2. This curve was deduced from unpublished operating range data for centrifugal compressors with design point pressure ratios ranging from 1.9 to 10.0.

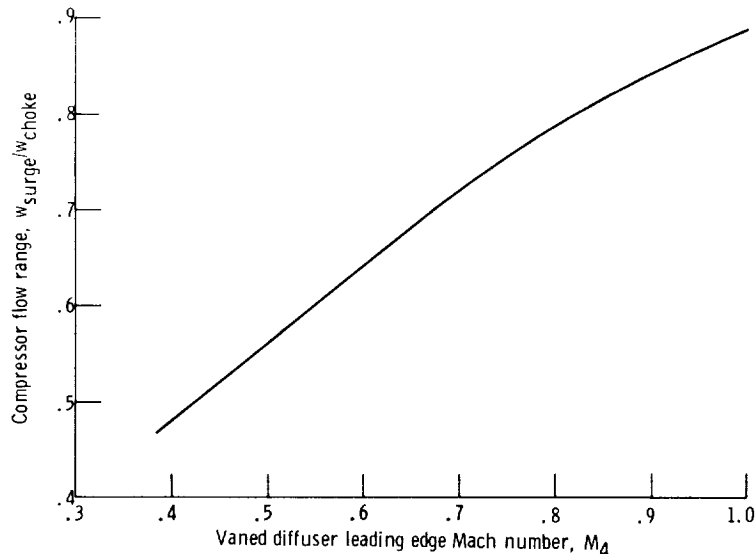


Figure 2. - Compressor flow range as a function of vaned diffuser leading edge Mach number.

Comparison of Estimated and Experimental Performance

This section compares the results obtained by the analytical procedure described herein to the experimental results obtained with a commercially manufactured centrifugal compressor.

Figure 3 shows the comparison between calculated and experimental pressure ratios as functions of corrected flow for 60, 80, 90, and 100 percent rotative speeds. Choking flow is caused by inducer choke at 100 percent speed and by diffuser choke at the other speeds. The assumption of zero static pressure recovery at the vaned diffuser choke point permits an estimate of the flow rate at which the compressor pressure ratio characteristic becomes vertical. Experimentally, the impeller characteristic exhibits behavior similar to that of the diffuser at the choked condition. However, the multi-dimensional effects that characterize this behavior apparently cannot be approximated accurately with strictly one-dimensional correlations. Modifying the correlations for evaluation at the hub, mean, and tip sections and averaging the results may help to predict the gradual pressure ratio reduction in moving toward choke. The potential refinements offered by this approach have not yet been considered herein. Maximum error in predicting the choking weight flow occurs at the 90 percent speed line and is 25 percent. Maximum error in predicting the compressor operating range (w_{surge}/w_{choke}) occurs at the 80 percent speed line and is 8.1 percent.

Figure 4 shows the comparison between calculated and experimental efficiencies as

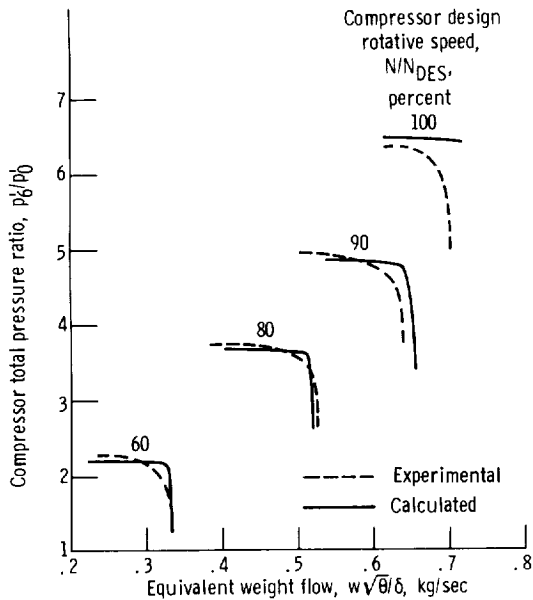


Figure 3. - Comparison of calculated and experimental compressor total pressure ratios as functions of equivalent weight flow and rotative speeds.

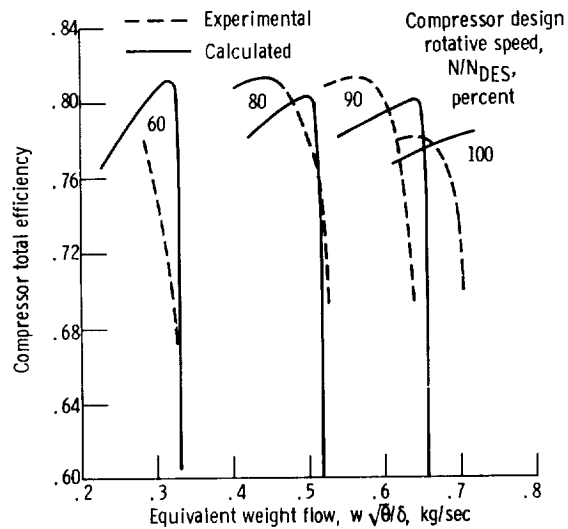


Figure 4. - Comparison of calculated and experimental compressor total efficiencies as functions of equivalent weight flow and rotative speeds.

functions of corrected flow. The worst estimate of peak efficiency occurs at the 90 percent speed line and is in error by 1.2 points. Only partial data is shown for the efficiency contour at 60 percent speed. This results because the data is replotted from a performance map that had efficiency contours and more data could not be accurately interpolated. Predicted surge point efficiencies for all speed lines are considerably lower than those experimentally measured. This can be attributed to predicted diffuser pressure recovery being lower than that attainable experimentally. Aerodynamic blockage growth may not be as rapid as that predicted by the model in moving toward surge.

Compressor efficiency increases with increasing flow until the choke point is reached. At the choke point vaned diffuser static pressure recovery decreases, resulting in a decrease in overall compressor efficiency. At the impeller choke point one would expect the impeller losses to increase substantially, resulting in a decrease in overall compressor efficiency. However, this behavior is not predicted through the use of the empirical correlations.

CONCLUDING REMARKS

This section summarizes the pertinent characteristics of the prediction method, discusses the limitations of the method, and notes the effect of the limitations on the results.

For inducers with relative Mach numbers appreciably in excess of unity the predicted compressor total pressure ratio and efficiency are greater than that attainable experimentally. This is a result of neglecting shock losses in the inducer inlet.

Predicted static pressure recovery for vaned diffusers with throat Mach numbers greater than unity will be too large. Extrapolation of the channel diffuser data used in the program is valid only in the subsonic flow regime.

The prewhirl option available in the program is for solid-body vortex swirl. This type of swirl is used primarily because it minimizes inducer inlet tip relative Mach number.

Compressor total pressure ratio and efficiency are not adequately predicted with the one-dimensional correlations when the compressor mass flow rate is limited by the impeller rather than the vaned diffuser. The predicted total pressure ratio and efficiency levels are higher than those measured experimentally.

Predicted surge point efficiencies are considerably lower than those measured on the example compressor. Correlation with experimental data from other compressors indicates that the predicted surge point efficiencies are sometimes higher and sometimes lower than the corresponding experimental values. This may be due in part to the difficulty encountered in making precise measurements at this flow condition.

CF	skin friction coefficient, C_f
CHIH	inducer inlet hub wall slope, χ_{1H} , deg from axial
CHIT	inducer inlet tip wall slope, χ_{1T} , deg from axial
CURVH	inducer inlet hub curvature, C_{1H} , m^{-1}
CURVT	inducer inlet tip curvature, C_{1T} , m^{-1}
DRAT	inducer-tip to impeller-exit diameter ratio, D_{1T}/D_3
DIT	inducer tip diameter, D_{1T} , m
GAM	specific heat ratio, γ
LAMX	inducer hub-tip diameter ratio, λ
MU0	total inlet dynamic viscosity, μ'_0 , N-sec/ m^2
N	compressor design rotative speed, N_{DES} , rpm
NONDES	percent compressor design rotative speed, N/N_{DES}
NVOVCR	number of input values of $(V/V_{cr})_0$
P0P	total inlet pressure, p'_0 , N/m^2
RGAS	gas constant, R , $J/(kg)(K)$
SPLT	control variable for splitter calculations (SPLT = 0, conventional impeller; SPLT = 1, impeller with splitters)
T0P	inlet total temperature, T'_0 , K
VLDRR	vaneless diffuser diameter ratio, D_4/D_3
VOVCR	values of inlet critical velocity ratio, $(V/V_{cr})_0$
Z	number of impeller blades at exit, Z_3

Sample Output

In the normal mode of operation the program performs two iterations over the range of inlet absolute critical velocity ratios which are specified. On the first iteration the compressor choking flow rate is determined. On the second iteration the printout of compressor performance at flow rates outside the usable range is deleted. A listing of the input information is tabulated for the compressor configuration studied. Then the compressor surge and choke flow rates are printed out. Finally, for each calculated point inside the operating range, compressor equivalent weight flow, total pressure ratio, total efficiency, and individual efficiency decrements are printed out. Sample output for the example compressor is as follows:

INLET TOTAL PRESSURE 101325.0
 NUMBER OF BLADES 32.
 INLET TOTAL TEMPERATURE 288.15
 FRICTION COEFFICIENT 0.04
 INLET TOTAL DYNAMIC VISCOSITY 0.000179
 DESIGN SPEED 72000.
 INDUCER RMS SWIRL ANGLE 1.4
 INDUCER RMS BLOCKAGE FACTOR 3.9
 INDUCER RMS BLADE ANGLE 49.0
 INDUCER HUB-TIP DIAMETER RATIO 0.5313
 INDUCER TIP-IMPELLER EXIT DIAMETER RATIO 0.5614
 IMPELLER BLADE EXIT BACKSWEEP 25.0
 IMPELLER BLADE EXIT HT. 0.0510
 VANELESS DIFFUSER DIAMETER RATIO 1.140
 VANED DIFFUSER AREA RATIO 2.70
 TOTAL VANED DIFFUSER THROAT AREA 0.00710
 INLET CRITICAL VELOCITY RATIO ARRAY 0.54
 0.47 0.48 0.49 0.50 0.51 0.52 0.53 0.54
 0.55 0.56 0.57 0.58
 *T FLOW LESS THAN SURGE FOR V/VCR=0.47

PERCENT NDES

		SURGE FLOW RATE		100.0		CHOKED FLOW RATE		0.719	
		MEQ		PRESSURE RATIO		ETAT		DETAVD	
DETAIGV	DETAICG	0.616	0.616	6.485	6.485	0.768	0.768	0.2551	0.2551
.	.	DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3264	0.3264	0.5138	0.5138	0.2885	0.2885	0.2604	0.2604
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.626	0.626	6.485	6.485	0.770	0.770	0.2511	0.2511
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3233	0.3233	0.5199	0.5199	0.2828	0.2828	0.2561	0.2561
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.636	0.636	6.484	6.484	0.773	0.773	0.2542	0.2542
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3205	0.3205	0.5259	0.5259	0.2776	0.2776	0.2520	0.2520
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.646	0.646	6.481	6.481	0.775	0.775	0.2520	0.2520
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3177	0.3177	0.5321	0.5321	0.2726	0.2726	0.2481	0.2481
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.656	0.656	6.477	6.477	0.776	0.776	0.25239	0.25239
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3150	0.3150	0.5384	0.5384	0.2678	0.2678	0.2443	0.2443
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.665	0.665	6.472	6.472	0.778	0.778	0.25163	0.25163
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3123	0.3123	0.5448	0.5448	0.2632	0.2632	0.2407	0.2407
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.675	0.675	6.465	6.465	0.780	0.780	0.25096	0.25096
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3097	0.3097	0.5513	0.5513	0.2587	0.2587	0.2372	0.2372
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.684	0.684	6.458	6.458	0.781	0.781	0.2338	0.2338
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3072	0.3072	0.5579	0.5579	0.2544	0.2544	0.2306	0.2306
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.693	0.693	6.448	6.448	0.782	0.782	0.24983	0.24983
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3047	0.3047	0.5647	0.5647	0.2503	0.2503	0.2498	0.2498
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.702	0.702	6.438	6.438	0.783	0.783	0.2498	0.2498
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3024	0.3024	0.5716	0.5716	0.2463	0.2463	0.2275	0.2275
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.710	0.710	6.427	6.427	0.784	0.784	0.2245	0.2245
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.3000	0.3000	0.5785	0.5785	0.2425	0.2425	0.2245	0.2245
DETAIGV	DETAICG	MEQ	MEQ	PRESSURE RATIO	PRESSURE RATIO	ETAT	ETAT	DETAICG	DETAICG
.	.	0.719	0.719	6.414	6.414	0.785	0.785	0.2245	0.2245
		DETABL	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG	DETAICG
		0.2978	0.2978	0.5856	0.5856	0.2388	0.2388	0.2245	0.2245

INLET TOTAL PRESSURE 101325. INLET TOTAL TEMPERATURE 288.15 INLET TOTAL DYNAMIC VISCOSITY .0000179 SPECIFIC HEAT RATIO 1.4 GAS CONSTANT 287.05
NUMBER OF BLADES 32. FRICTION COEFFICIENT .004 SPLT 1 DESIGN SPEED 72000. INDUCER RMS SWIRL ANGLE 0. INDUCER RMS BLOCKAGE FACTOR 0.90
INDUCER RMS BLADE ANGLE 49.0 INDUCER HUB-TIP DIAMETER RATIO 0.5313 INDUCER TIP-IMPELLER EXIT DIAMETER RATIO 0.5614
IMPELLER BLADE EXIT HUB-IMPELLER BLADE EXIT HT. .03510 VANELESS DIFFUSER DIAMETER RATIO 1.140 VANELESS DIFFUSER SETTING ANGLE 78.00
25.0 TOTAL VANELESS DIFFUSER THROAT AREA .000710 VANELESS DIFFUSER AREA RATIO 1.140 VANELESS DIFFUSER SETTING ANGLE 78.00

0.39 0.40 0.41 0.42 0.43 0.44 0.45 0.46
0.47 0.48 0.49 0.50 0.51 0.52 0.53
BT FLOW LOSS THAN SURGE FOR V/VCR=0.39
BT FLOW LOSS THAN SURGE FOR V/VCR=0.40

PERCENT NDES

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.00034		.00034
	DETAIGV		DETAIGV
	.00035		.00035
	DETAIGV		DETAIGV
	.00036		.00036
	DETAIGV		DETAIGV
	.00037		.00037
	DETAIGV		DETAIGV
	.00039		.00039
	DETAIGV		DETAIGV
	.00040		.00040
	DETAIGV		DETAIGV
	.00041		.00041
	DETAIGV		DETAIGV
	.00043		.00043
	DETAIGV		DETAIGV
	.00044		.00044
	DETAIGV		DETAIGV
	.00045		.00045
	DETAIGV		DETAIGV
	.00046		.00046
	DETAIGV		DETAIGV
	.00048		.00048
	DETAIGV		DETAIGV
	.02535		.02535

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.02233		.02233
	DETAIGV		DETAIGV
	.02285		.02285
	DETAIGV		DETAIGV
	.05074		.05074
	DETAIGV		DETAIGV
	.02193		.02193
	DETAIGV		DETAIGV
	.02151		.02151
	DETAIGV		DETAIGV
	.04651		.04651
	DETAIGV		DETAIGV
	.04698		.04698
	DETAIGV		DETAIGV
	.02034		.02034
	DETAIGV		DETAIGV
	.01999		.01999
	DETAIGV		DETAIGV
	.04316		.04316
	DETAIGV		DETAIGV
	.01932		.01932
	DETAIGV		DETAIGV
	.01893		.01893
	DETAIGV		DETAIGV
	.0591		.0591
	DETAIGV		DETAIGV
	.01901		.01901
	DETAIGV		DETAIGV
	.02768		.02768

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.03316		.03316
	DETAIGV		DETAIGV
	.03254		.03254
	DETAIGV		DETAIGV
	.03195		.03195
	DETAIGV		DETAIGV
	.02260		.02260
	DETAIGV		DETAIGV
	.02144		.02144
	DETAIGV		DETAIGV
	.02090		.02090
	DETAIGV		DETAIGV
	.02038		.02038
	DETAIGV		DETAIGV
	.01988		.01988
	DETAIGV		DETAIGV
	.01939		.01939
	DETAIGV		DETAIGV
	.01965		.01965
	DETAIGV		DETAIGV
	.01893		.01893
	DETAIGV		DETAIGV
	.0591		.0591
	DETAIGV		DETAIGV
	.01901		.01901
	DETAIGV		DETAIGV
	.02768		.02768

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.03086		.03086
	DETAIGV		DETAIGV
	.03034		.03034
	DETAIGV		DETAIGV
	.02893		.02893
	DETAIGV		DETAIGV
	.02849		.02849
	DETAIGV		DETAIGV
	.02789		.02789
	DETAIGV		DETAIGV
	.02808		.02808
	DETAIGV		DETAIGV
	.03381		.03381
	DETAIGV		DETAIGV
	.02768		.02768

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.03086		.03086
	DETAIGV		DETAIGV
	.03034		.03034
	DETAIGV		DETAIGV
	.02893		.02893
	DETAIGV		DETAIGV
	.02849		.02849
	DETAIGV		DETAIGV
	.02789		.02789
	DETAIGV		DETAIGV
	.02808		.02808
	DETAIGV		DETAIGV
	.03381		.03381
	DETAIGV		DETAIGV
	.02768		.02768

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.03086		.03086
	DETAIGV		DETAIGV
	.03034		.03034
	DETAIGV		DETAIGV
	.02893		.02893
	DETAIGV		DETAIGV
	.02849		.02849
	DETAIGV		DETAIGV
	.02789		.02789
	DETAIGV		DETAIGV
	.02808		.02808
	DETAIGV		DETAIGV
	.03381		.03381
	DETAIGV		DETAIGV
	.02768		.02768

SURGE FLOW RATE		CHOKE FLOW RATE	
90.0		90.0	
DETAIGV	0.540	DETAIGV	0.540
	MEQ		MEQ
	0.540		0.540
	DETAIGV		DETAIGV
	.03086		.03086
	DETAIGV		DETAIGV
	.03034		.03034
	DETAIGV		DETAIGV
	.02893		.02893
	DETAIGV		DETAIGV
	.02849		.02849
	DETAIGV		DETAIGV
	.02789		.02789
	DETAIGV		DETAIGV
	.02808		.02808
	DETAIGV		DETAIGV
	.03381		.03381
	DETAIGV		DETAIGV
	.02768		.02768

INLET TOTAL PRESSURE 101325. INLET TOTAL TEMPERATURE 288.15 INLET TOTAL DYNAMIC VISCOSITY 0.000179 SPECIFIC HEAT RATIO 1.4 GAS CONSTANT 287.05
 NUMBER OF BLADES 32. FRICTION COEFFICIENT 0.004 SPLT 1 DESIGN SPEED 72000. INDUCER RMS SWIRL ANGLE 0. INDUCER RMS BLOCKAGE FACTOR 0.90
 INDUCER RMS BLADE ANGLE 49.0 INDUCER HUB-TIP DIAMETER RATIO 0.5313 INDUCER TIP-IMPELLER EXIT DIAMETER RATIO 0.5614
 IMPELLER BLADE EXIT BACKSWEEP 25.0 IMPELLER BLADE EXIT HT. 0.00510 VANELESS DIFFUSER DIAMETER RATIO 1.140 VANELESS DIFFUSER DIAMETER RATIO 0.5614
 TOTAL VANE DIFFUSER THROAT AREA 0.00710 VANE DIFFUSER AREA RATIO 2.70

WT FLOW LESS THAN SURGE FOR V/VCR=0.27
 WT FLOW LESS THAN SURGE FOR V/VCR=0.28
 WT FLOW LESS THAN SURGE FOR V/VCR=0.29
 WT FLOW LESS THAN SURGE FOR V/VCR=0.30

PERCENT NDES

		SURGE FLOW RATE 80.0		CHOKED FLOW RATE	
		0.409		0.518	
		MEQ	PRESSURE RATIO	ETAT	ETARC
DETAIGV	0.27	0.421	3.677	.781	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2912	0.5321	0.3395	0.2311
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.434	3.676	.786	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2845	0.5416	0.3306	0.2243
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.446	3.676	.790	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2780	0.5512	0.3225	0.2180
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.458	3.674	.794	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2717	0.5611	0.3148	0.2121
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.470	3.672	.798	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2654	0.5714	0.3075	0.2065
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.482	3.654	.799	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2592	0.5821	0.3006	0.2013
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.494	3.651	.802	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2532	0.5932	0.2941	0.1963
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.506	3.648	.806	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2472	0.6046	0.2879	0.1916
		MEQ	PRESSURE RATIO	ETAT	
DETAIGV	0.27	0.518	2.717	.596	DETAI
.	0.35	DETABL	DETAUF	DETAUF	DETAUF
		0.2414	0.6164	0.2820	0.1872
		MEQ	PRESSURE RATIO	ETAT	

INLET TOTAL PRESSURE	INLET TOTAL TEMPERATURE	INLET TOTAL DYNAMIC VISCOSITY	SPECIFIC HEAT RATIO	GAS CONSTANT
101375.	288.15	.0000179	1.4	287.05
NUMHFR CF PLACES	FRICTION COEFFICIENT	DESIGN SPEED	INDUCER RMS SWIRL ANGLE	INDUCER RMS BLOCKAGE FACTOR
32.	.004	72000.	0.	0.90
INDUCER RMS BLADE ANGLE	INDUCER HUB-TIP DIAMETER RATIO	INDUCER TIP-IMPELLER EXIT DIAMETER RATIO		
49.0	0.5313	0.5614		
IMPELLER BLADE EXIT BACKSWEEP	IMPELLER BLADE EXIT HT.	VANELESS DIFFUSER DIAMETER RATIO	VANED DIFFUSER SETTING ANGLE	
25.0	.00510	1.140	78.00	
	TOTAL VANED DIFFUSER THROAT AREA	VANED DIFFUSER AREA RATIO		
	.000710	2.70		
	INLET CRITICAL VELOCITY RATIO ARRAY			
	0.19 0.20 0.21 0.22			
0.15 0.16 0.17 0.18 0.23 0.24 0.25 0.26				
WT FLOW LESS THAN SURGE FOR V/VCR=0.15				
PERCENT NDES				
SURGE FLOW RATE 60.0				
CHOKED FLOW RATE				
0.223				
DETAIGV	DETAICV	DETAIF	DETAIF	DETAIF
.	0.0014	0.224	0.209	0.766
		DETABL	DETAIF	DETAIF
		0.3086	0.3944	0.2711
		MEQ	PRESSURE RATIO	ETAT
		0.238	2.209	.775
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0016	0.258	0.3750	0.2377
		MEQ	PRESSURE RATIO	ETAT
		0.251	2.198	.777
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0017	0.2831	0.3576	0.2253
		MEQ	PRESSURE RATIO	ETAT
		0.265	2.198	.785
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0019	0.278	0.420	0.2142
		MEQ	PRESSURE RATIO	ETAT
		0.278	2.199	.793
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0021	0.2583	0.3278	0.2041
		MEQ	PRESSURE RATIO	ETAT
		0.292	2.199	.801
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0023	0.2462	0.3148	0.1950
		MEQ	PRESSURE RATIO	ETAT
		0.305	2.199	.809
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0025	0.2343	0.3030	0.1868
		MEQ	PRESSURE RATIO	ETAT
		0.318	2.198	.817
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0027	0.2224	0.2919	0.1791
		MEQ	PRESSURE RATIO	ETAT
		0.331	1.814	.606
DETAIGV	DETAICV	DETABL	DETAIF	DETAIF
.	0.0029	0.2109	0.2819	0.1722

Definitions of the abbreviated FORTRAN output variables are:

DETABL	efficiency decrement due to impeller blade aerodynamic loading, $\Delta\eta_{BL}$
DETADF	efficiency decrement due to disk friction, $\Delta\eta_{DF}$
DETAIGV	efficiency decrement due to inlet guide vane loss, $\Delta\eta_{IGV}$
DETAINC	efficiency decrement due to inducer incidence, $\Delta\eta_{INC}$
DETARC	efficiency decrement due to recirculation, $\Delta\eta_{RC}$
DETA SF	efficiency decrement due to skin friction, $\Delta\eta_{SF}$
DETA VD	efficiency decrement due to vaned diffuser losses, $\Delta\eta_{VD}$
DETA VLD	efficiency decrement due to vaneless diffuser losses, $\Delta\eta_{VLD}$
ETAT	compressor total efficiency, η
WEQ	equivalent flow rate, $w\sqrt{\theta}/\delta$, kg/sec

Error Messages

If the compressor choking flow rate is not reached with the specified values of inlet absolute critical velocity ratios, the operating range cannot be determined with the methods used in this analysis. When this happens, the calculated performance output is deleted and the message **COMPRESSOR CHOKING FLOW HAS NOT BEEN REACHED** is printed.

If the first input value of $(V/V_{cr})_0$ results in calculated weight flow greater than the compressor choking weight flow, the message **VOVCR ARRAY TOO LARGE** is printed.

For input values of $(V/V_{cr})_0$ much too small for the compressor of interest a velocity diagram solution at the impeller exit cannot be obtained. When this occurs the message **IRRATIONAL EXIT TRIANGLE** is printed. All of these problems can be corrected by making the appropriate adjustments to the VOVCR array used.

Main Program FORTRAN Variables and Corresponding Engineering Symbols

A1	a_1
A2	a_3
ACOUSR	a/a'

ADTH	A_5
AL1	α_{1T}
AL1MF	α_{1MF}
AL2	α_3
AL3	α_4
ALPH1	temporary storage
ALPHA	α
AMT	M_5
AMU	μ
AMULT	$\exp\left(\int_{r_{1H}}^{r_{1MF}} C \, dn\right)$
ANU	ν
AR	A_6/A_5
B	B_5
B0	B_0
B1	β_{1T}
B1H	β_{1H}
B1MF	β_{1MF}
B1MFB	β_{1MFB}
B2	b_3
B2X	β_{3b}
BARR	array of vaned diffuser throat blockages
BLOCK	B_1
BMULT	$\exp\left(\int_{r_{1MF}}^{r_{1T}} C \, dn\right)$
BOPT	β_{1MFopt}
BT	vaned diffuser inlet blockage
CF	C_f

CHIH	λ_{1H}
CHIMF	λ_{1MF}
CHIT	λ_{1T}
CINC	inducer choking incidence
CINC1	interpolation variable
CINC2	interpolation variable
CINC40	choking incidence array for 40 ⁰ rms inducer blade angles
CINC50	choking incidence array for 50 ⁰ rms inducer blade angles
CINC60	choking incidence array for 60 ⁰ rms inducer blade angles
CONST1	K_{BL}
CONST2	K_{SF}
COSA	$\cos \alpha_{1T}$
CP	C_p
CPSTAR	C_p^{**}
CURVH	C_{1H}
CURVMF	C_{1MF}
CURVT	C_{1T}
D1H	D_{1H}
D1T	D_{1T}
D2	D_3
DEBL	$\Delta\eta_{BL}$
DEDF	$\Delta\eta_{DF}$
DEEXIT	$\Delta\eta_{exit}$
DEIGV	$\Delta\eta_{IGV}$
DEINC	$\Delta\eta_{INC}$
DELTA	δ
DELTAB	ΔB
DELTAR	Δr
DELTAS	$\Delta\delta^*$

DERC	$\Delta\eta_{RC}$
DESF	$\Delta\eta_{SF}$
DEV D	$\Delta\eta_{VD}$
DEVLD	$\Delta\eta_{VLD}$
DF	D_f
DHACT	Δh_{act}
DHAERO	Δh_{aero}
DHBL	Δh_{BL}
DHDF	Δh_{DF}
DHDIF	Δh_{VD}
DHEST	Δh_{est}
DHIGV	Δh_{IGV}
DHINC	Δh_{INC}
DHRC	Δh_{RC}
DHSF	Δh_{SF}
DHVLD	Δh_{VLD}
DHYD	D_{HYD}/D_3
DIFLEM	M_4 array
DMF	D_{1MF}
DRAT	D_{1T}/D_3
EPS	ϵ
ETAD	η_{AD}
ETAR	η_R
EW F	$w \sqrt{\theta}/\delta$
F1	C_p^{**} at vaned diffuser area ratio of 1.2
F2	C_p^{**} at vaned diffuser area ratio of 2.0
F3	C_p^{**} at vaned diffuser area ratio of 3.0
F4	C_p^{**} at vaned diffuser area ratio of 4.0
F5	C_p^{**} at vaned diffuser area ratio of 5.0

FINT	$\int_{r_{1H}}^{r_{1MF}} C \, dn$
FLFUNC	$\sqrt{\frac{\gamma}{R} \left(\frac{2}{\gamma + 1} \right)^{(\gamma+1)/(\gamma-1)}}$
FLRNG	$w_{\text{surge}}/w_{\text{choke}}$
G1	$\gamma + 1$
G2	$\gamma - 1$
GAM	γ
GINT	$\int_{r_{1H}}^{r_{1T}} C \, dn$
H0	$r_{1MF} - r_{1H}$
H1	$r_{1T} - r_{1MF}$
HIS	Δh_{is}
INC	$\beta_{1MF} - \beta_{1MFb}$
J	index variable
JAN	iteration counter
K	choke indication variable
L	index variable
LAMX	λ
LOD	L/D_3
MIN	index variable
MU0	μ'_0
MWRMS	array of inducer rms relative Mach numbers
N	N_{DES}
NO	index variable
NONDES	N/N_{DES}
NVOVCR	number of values of $(V/V_{cr})_0$
NWRITE	output control variable

P0P	p'_0
P1	p_{1MF}
P1P	p'_{1MF}
P2	p_3
P2P	p'_3
P3P	p'_4
P4	p_6
P4PG	iteration variable
P4PL	iteration variable
PEXIT	p_6
PHI	φ
PIMF	p_{2MF}
PIPMF	p'_{2MF}
POPP1	$(p/p')_{1MF}$
PP	storage variable
PPEXIT	p'_6
PPOP1	$(p'/p)_{1MF}$
PR	p'_6/p'_0
PREC1	array of C_p^{**} at area ratio 1.2
PREC2	array of C_p^{**} at area ratio 2.0
PREC3	array of C_p^{**} at area ratio 3.0
PREC4	array of C_p^{**} at area ratio 4.0
PREC5	array of C_p^{**} at area ratio 5.0
PTH	p_5
PTHP	p'_5
Q	Q
QAERO	q_{aero}
R	r
R0P	ρ'_0
R1	ρ_1

R1P	ρ'_1
R2	r_3
R2G	$\rho_{3,est}$
RANGE	w_{surge}/w_{choke}
RARRAY	temporary storage
RE	Re
RGAS	R
RHO2	ρ_3
RHOH	ρ_{1H}
RHOMF	ρ_{1MF}
RHOR	ρ/ρ'
RHOT	ρ_{1T}
RMRMS	W_{1MF}/a_1
RTHP	ρ'_5
RVOEST	$(\rho V/\rho' V_{cr})_2$
RVORP1	$(\rho V/\rho' V_{cr})_1$
RVORVC	$(\rho V/\rho' V_{cr})_1 p'_1/p_{iMF}$
RVRVC4	$(\rho V/\rho' V_{cr})_6$
RVRVTH	$(\rho V/\rho' V_{cr})_5$
S	integral of M^3
SINA	$\sin \alpha_{1T}$
SPLT	splitter control variable
SW	w
T0	T_0
T0P	T'_0
T0PP	T''_0
T1	T_1
T1PP	T''_1

T2	T_3
T2P	T'_3
T2PEST	T'_{3est}
T2PP	T''_3
TALPH	$\tan \alpha$
THETA	θ
TOT0	T_1/T_0
TOT1	T_2/T_1
TPL	p'/p'_3
TX	$\eta_R \Delta h_{aero}/C_p T'_o + 1$
U1H	u_{1H}
U1MF	u_{1MF}
U1T	u_{1T}
U2	u_3
V1MF	V_{1MF}
V1T	V_{1T}
V2	V_3
VARAL	$\Delta \tan \alpha$
VARAL1	temporary storage
VARM	ΔM^2
VARM1	temporary storage
VCR	$(V_{cr})_0$
VCRTH	$(V_{cr})_5$
VLDRR	D_4/D_3
VM1	V_{m1T}
VM1H	V_{m1H}
VM1MF	V_{m1MF}
VM2	V_{m3}
VM1MF	V_{m1MF}

VOVCR	$(V/V_{cr})_0$
VOVCR4	$(V/V_{cr})_6$
VOVCR1	$(V/V_{cr})_1$
VSL	V_{SL}
VU1H	V_{u1H}
Vu1MF	V_{u1MF}
VU1T	V_{u1T}
VU2	V_{u3}
W1H	W_{1H}
W1MF	W_{1MF}
W1MFEF	W_{1MFeff}
W1T	W_{1T}
W2	W_3
W2OW1T	W_3/W_{1T}
WCHK	w_{choke}
WCR	W_{cr}
WFUNC	$w\sqrt{T'_3/p'_5}A_5^B$
W1MF	W_{1MF}
WL	W_L
WOU2	$(W/u_3)_{av}^2$
WSURGE	w_{surge}
WU1H	W_{u1H}
WU1MF	W_{u1MF}
WU1T	W_{u1T}
WU2	W_{u3}
X1	$\alpha - \alpha_4$

XC	K_{vu}
XK	K_{vm}
XM	M
XM1	temporary storage
XM2	M_3
XMACH	M_5
XMARR	array of vaneless diffuser Mach numbers
Z	Z_3
ZETA	ζ

Program Listing

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DIMENSION VOVCR(15)
DIMENSION P3P(20),XMARR(20)
DIMENSION F(20),S(20)
DIMENSION AMT(4),BARR(6),PREC1(4,6),PREC2(4,6),PREC3(4,6)
DIMENSION PREC4(4,6),PREC5(4,6)
DIMENSION MWRMS(8),CINC60(8),CINC50(8),CINC40(8)
DIMENSION FLRNG(7),DIFLEM(7)
INTEGER SPLT
REAL LAMX,LCD,MUO,NONDES,MWRMS,INC,N
DATA(AMT(I),I=1,4)/.2,.4,.6,.8/
DATA(BARR(I),I=1,6)/.02,.04,.06,.08,.10,.12/
DATA((PREC1(I,J),I=1,4),J=1,6)/.234,.244,.257,.269,.215,.224,.233,
1.243,.207,.215,.223,.232,.193,.199,.206,.212,.183,.190,.196,.202,.
2169,.176,.182,.188/
DATA((PREC2(I,J),I=1,4),J=1,6)/.644,.67J,.696,.722,.620,.638,.656,
1.674,.590,.606,.623,.639,.562,.576,.590,.605,.538,.551,.564,.578,.
2510,.524,.538,.552/
DATA((PREC3(I,J),I=1,4),J=1,6)/.782,.789,.796,.802,.750,.756,.762,
1.768,.708,.716,.724,.732,.672,.680,.687,.695,.652,.648,.654,.660,.
2604,.612,.619,.626/
DATA((PREC4(I,J),I=1,4),J=1,6)/.842,.838,.833,.828,.8,.8,.8,.8,.75
12,.756,.760,.763,.710,.713,.716,.719,.675,.678,.680,.683,.630,.635
2,.640,.646/
DATA((PREC5(I,J),I=1,4),J=1,6)/.878,.865,.852,.838,.832,.825,.818,
1.812,.78,.78,.78,.78,.736,.735,.735,.734,.692,.694,.695,.696,.644,
2.647,.650,.652/
DATA(CINC60(I),I=1,8)/-10.5,-5,-2,.1.5,2.5,4.,5.,5./
DATA(CINC50(I),I=1,8)/-15.,-7.5,-3.,1.5,4.,6.5,9.,11./
DATA(CINC40(I),I=1,8)/-20.,-12.,-5.,1.5,5.,8.,11.5,14.5/
DATA(MWRMS(I),I=1,8)/.5,.6,.7,.8,.9,1.,1.1,1.2/
DATA(DIFLEM(I),I=1,7)/.4,.5,.6,.7,.8,.9,1./
DATA(FLRNG(I),I=1,7)/.48,.56,.64,.72,.79,.84,.89/
NAMELIST /INPUT/ GAM,POP,TOP,N,DIT,MUO,CF,VOVCR,NVOVCR,RGAS,
IDRAT,IAMX,B2X,Z,VLDRR,B2,B1MFB,AR,BLOCK,AL3,ADTH,NONDES,SPLT,
2 ALIMF,CHIH,CHIT,CURVH,CURVT
1 READ(5,INPUT)

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WRITE(6,309)
WRITE(6,315) POP, TOP, MUO, GAM, RGAS
WRITE(6,310)
WRITE(6,316) Z, CF, SPLT, N, AL1MF, BLOCK
WRITE(6,311)
WRITE(6,317) B1MFB, LAMX, DRAT
WRITE(6,312)
WRITE(6,318) B2X, B2, VLDRR, AL3
WRITE(6,313)
WRITE(6,319) ADTH, AR
WRITE(6,314)
WRITE(6,320) (VOVCR(I), I=1, NVOVCR)
PERDS=NONDES*100.
G1=GAM+1.
G2=GAM-1.
CP =GAM*RGAS/G2
B2X=.01745*B2X
AL3=AL3*.01745
AL1MF=.01745*AL1MF
CHI H=.01745*CHI H
CHIT=.01745*CHIT
FLFUNC=SQRT(GAM/RGAS*(2./G1)**(G1/G2))
ROP=POP/RGAS/TOP
VCR=SQRT(2.*GAM/G1*RGAS*TOP)
UIT=3.14159*N*NONDES*DIT/60.
NWRITE=1
DO 18 L=1.2
MIN=1
2 DO 17 J=MIN, NVOVCR
K=0
B1MFB=.01745*B1MFB
VUIT=0.
VU1MF=0.
VUIH=0.
VM1H=VOVCR(J)*VCR
U2=UIT/DRAT
D2=DIT/DRAT
U1H=UIT*LAMX
D1H=DIT*LAMX
DMF=SQRT(DIT**2*(1.+LAMX**2)/2.)
U1MF=UIT*DMF/DIT
CH1MF=(CHIT-CHI H)*(DMF-D1H)/(DIT-D1H)+CHI H
CURVMF=(CURVT-CURVH)*(DMF-D1H)/(DIT-D1H)+CURVH
H0=(DMF-D1H)/2.
H1=(DIT-DMF)/2.
FINT=H0/2.*(CURVH+CURVMF)
AMULT=EXP(FINT)
VM1MF=AMULT*VM1H
GINT=(H0+H1)/6.*((2.-H1/H0)*CURVH+(H0+H1)**2/H0/H1*CURVMF+(2.-H0
1/H1)*CURVT)
BMULT=EXP(GINT)
VM1T=BMULT*VM1H
VM1HN=VM1H*COS(CHI H)
VM1MFN=VM1MF*COS(CH1MF)
VM1TN=VM1T*COS(CHIT)
RHOH=ROP*(1.-VM1H**2/2./CP/TOP)**(1./G2)
RHCMF=RUP*(1.-VM1MF**2/2./CP/TOP)**(1./G2)
RHCT=ROP*(1.-VM1T**2/2./CP/TOP)**(1./G2)
FCN1=RHOH*VM1HN*D1H/2.
FCN2=RHCMF*VM1MFN*DMF/2.

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FCN3=RHGT*VM1TN*01T/2.
Sw=(H0+H1) /6.*((2.-H1/H0)*FCN1+(H0+H1)**2/H0/H1*FCN2+(2.-H0/H1)*
1FCN3)*6.28318
DFIGV=0.
V1MF=SQRT(VM1MF**2+VU1MF**2)
T1=TOP-V1MF**2/2./CP
P1P=POP
POPP1=(1.-V1MF**2/2./CP/TOP)**(GAM/G2)
P1=P1P*POPP1
R1F=P1P/REGAS/TOP
R1 = R1P*(P1/P1P)**(1./GAM)
RE=U2*D2/MU0*ROP
ALSTAG=AL1MF/2.
FS=0.0076/(COS(AL1MF)-.025)*(1.+COS(ALSTAG)/0.7)
VOVCR1=VOVCR(J)
IF(AL1MF.LT.0.001) GO TO 36
9 VOVCR1=VOVCR1+.001
AKE=(VCVCR1*VCR)**2/2.
POPP1=(1.-AKE/CP/TOP)**(GAM/G2)
AKEID=AKE/(1.-ES)
P1OPPO=(1.-AKEID/CP/TOP)**(GAM/G2)
P1P=POP*P1OPPO/POPP1
R1F=P1P/REGAS/TOP
P1=P1P*POPP1
R1=R1P*(POPP1)**(1./GAM)
Q1=3.14159*01T**2*(1.-LAMX**2)*VOVCR1*VCR*COS(AL1MF)/4.
WTCHK=Q1*R1
IF(WTCHK.LT.SW) GO TO 9
VU1MF=VOVCR1*VCR*SIN(AL1MF)
VM1MF=VOVCR1*VCR*COS(AL1MF)
V1MF=SQRT(VU1MF**2+VM1MF**2)
T1=TOP-V1MF**2/2./CP
XK=VU1MF**2+2.*VM1MF**2
XC=VU1MF/DMF*2.
VUIT=XC*01T/2.
VUIH=XC*01H/2.
VM1T=SQRT(XK-2.*VUIT**2)
VM1H=SQRT(XK-2.*VUIH**2)
DFIGV=ES*AKEID
36 V1T=SQRT(VM1T**2+VUIT**2)
AL1=ARSIN(VUIT/V1T)
WUIT=UIT-VUIT
B1=ATAN(WUIT/VM1T)
W1T=SQRT(VM1T**2+WUIT**2)
WUIH=UIH-VUIH
B1H=ATAN(WUIH/VM1H)
W1H=SQRT(VM1H**2+WUIH**2)
A1=SQRT(GAM*REGAS*T1)
WU1MF=U1MF-VU1MF
W1MF=SQRT(VM1MF**2+WU1MF**2)
RMRMS=W1MF/A1
B1MF=ATAN(WU1MF/VM1MF)
INC=(B1MF-B1MFB)*57.29577
EPS=ATAN((1.-BLOCK)*TAN(B1MF)/(1.+BLOCK*(TAN(B1MF))**2))
BOPT=B1MF-EPS
T1FP=T1+W1MF**2/2./CP
WCR=SQRT(2.*GAM/G1*REGAS*T1FP)
TC10=1.-G2/G1*(W1MF/WCR)**2
W1MFEF=W1MF*COS(BOPT-B1MFB)

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TOT1=1.-G2/G1*(W1MFEF/WCR)**2
TI=T1PP*TOT1
WL=W1MF*SIN(ABS(BOPT-B1MF))
DHINC=WL**2/2.
PIPMF=PIP*EXP(-DHINC/TI/RGAS)
DELTA=POP/101325.35
THETA=TOP/288.15
EWF=SW*SQRT(THETA)/DELTA
B1MFB=B1MFB*57.29577
IF(B1MFB.GE.40..AND.B1MFB.LE.50.) GO TO 71
I=2
81 IF(RMRMS.GE.MWRMS(I-1).AND.RMRMS.LE.MWRMS(I)) GO TO 80
I=I+1
GC TC 81
80 CINC1=(RMRMS-MWRMS(I-1))/(MWRMS(I)-MWRMS(I-1))*(CINC60(I)-CINC60(I
I-1))+CINC60(I-1)
CINC2=(RMRMS-MWRMS(I-1))/(MWRMS(I)-MWRMS(I-1))*(CINC50(I)-CINC50(I
I-1))+CINC50(I-1)
CINC=CINC1+(60.-B1MFB)/10.*(CINC2-CINC1)
IF(INC.LE.CINC) K=1
GO TO 74
71 I=2
72 IF(RMRMS.GE.MWRMS(I-1).AND.RMRMS.LE.MWRMS(I)) GO TO 73
I=I+1
GC TC 72
73 CINC1=(RMRMS-MWRMS(I-1))/(MWRMS(I)-MWRMS(I-1))*(CINC50(I)-CINC50(I
I-1))+CINC50(I-1)
CINC2=(RMRMS-MWRMS(I-1))/(MWRMS(I)-MWRMS(I-1))*(CINC40(I)-CINC40(I
I-1))+CINC40(I-1)
CINC=CINC1+(50.-B1MFB)/10.*(CINC2-CINC1)
IF(INC.LE.CINC) K=1
74 CCNTINUE
IF(K.EQ.1.AND.J.EQ.1) GO TO 202
IF(K.EQ.1.AND.L.EQ.1) GO TO 18
T2PP=T1PP+(U2**2-U1MF**2)/2./CP
PHI=VM1MF/U2
EPSLIM=1./EXP(8.16*COS(B2X)/Z)
VSL=SQRT(COS(B2X))*U2/Z**.7
IF((DMF/D2).GT.EPSLIM) VSL=U2*(SQRT(COS(B2X))/Z**.7)*(1.-((DMF/D2-
1EPSLIM)/(1.-EPSLIM))**3)+U2*((DMF/D2-EPSLIM)/(1.-EPSLIM))**3
DHEST=U2**2
T2PEST=(DHEST/CP/TOP+1.)*TOP
R2G=R1*(T2PEST/TOP)**(1./G2)
4 RHD2=R2G
VM2=SW/(3.14159*RHD2*D2*B2)
VU2=U2-VM2*TAN(B2X)-VSL
MIN=J
IF(VM2.LT.0..AND.L.EQ.2) GO TO 200
IF(VM2.LT.0.) GO TO 17
IF(VU2.LT.0..AND.L.EQ.2) GO TO 201
IF(VU2.LT.0.) GO TO 17
WU2=U2-VU2
W2=SQRT(WU2**2+VM2**2)
IF((VSL*COS(B2X)/W2).GT.1..AND.L.EQ.2) GO TO 202
IF((VSL*COS(B2X)/W2).GT.1.) GO TO 17
T2=T2PP-W2**2/2./CP
A2=SQRT(GAM*RGAS*T2)
W2CW1T=W2/W1T
WOU2=(PHI**2+(DMF/D2)**2+W2CW1T**2*(PHI**2+DRAT**2))/2.

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AL2=ATAN(VU2/VM2)
V2=SQRT(VU2**2+VM2**2)
T2P=T2+V2**2/2./CP
DHAERO=CP*TOP*(T2P/TOP-1.)
QAERO=CHAERO/U2**2
DF= W1T/U2*(Z/3.14159*(1.-D1T/D2)+2.*D1T/D2)
CONST1=0.75
IF(SPLT.EC.1) CONST1=0.6
DF=1.-W20W1T+CONST1*QAERO/CF
DHBL=0.05*DF**2*U2**2
LOD=(1.-DMF/.3048)/COS(B2X)/2.
DHDF=-0.1356*RHO2*U2**3*D2**2/SW/RE**2
DHYD=Z/3.14159/COS(B2X)+D2/B2
DHYD=1./DHYD+D1T/D2/(2./(1.-LAMX)+2.*Z/3.14159/(1.+LAMX)
1*SQRT(1.+(1.+LAMX**2)/2.*(TAN(B1)**2))
DHRC=0.02*SQRT(TAN(AL2))*DF**2*U2**2
CONST2=5.6
IF(SPLT.EC.1) CONST2=7.0
DHSF=CONST2*CF*LOD/DHYD*WOU2*U2**2
DHACT=CHAERO+DHDF+DHRC
HIS=DHAERO-DHBL-DHSF-DHIGV-DHINC
ETAR=HIS/DHAERO
TX=ETAR*DHAERO/CP/TOP+1.
51 P2P=TX**((GAM/G2)*PIPMF
P2=P2P*(T2P/T2)**(-GAM/G2)
R2G=P2/RGAS/T2
IF(ABS((RHO2-R2G)/RHO2).GT.0.001) GO TO 4
XM2= V2/A2
R2=D2/2.
AMU=1.4579E-6*T2**1.5/(T2+110.4)
ANL=AMU/R2G
BO=1.
XM=XM2
ALPHA=AL2
R=1.0
F(1)=XM2**3/(1.+G2/2.*XM2**2)**(G1/2./G2)
P3P(1)=P2P
XMARR(1)=XM2
DELTAR=(VLDRR-1.)/10.
ZETA=CF*R2/B2
AS=0.
DC 1000 NO=2,10
XM1=XM
ALPH1=ALPHA
DS=DELTAR*R2/COS(ALPHA)
AS=AS+DS
DELTAS=.037*AS**(-.2)*(V2/ANU)**(-.2)*DS
R=BO-2.*DELTAS/B2
DELTAB=BO-B
VARM=-2.*(1.+G2/2.*XM**2)/(XM**2-1./COS(ALPHA)**2)*((GAM*XM**2-TAN
1(ALPHA)**2)*ZETA/BO/COS(ALPHA)+1./BO*DELTAB/DELTAR-1./COS(ALPHA)**
22/R)*XM**2*DELTAR
VARAL=1./COS(ALPHA)**2/(XM**2-(1./COS(ALPHA))**2)*((1.+G2 *XM**2
1)*ZETA/BO/COS(ALPHA)+1./BO*DELTAB/DELTAR-XM**2/R)*TAN(ALPHA)*DELTA
2R
VARM1=VARM
VARAL1=VARAL
B1=B
H=BO

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AS=AS-DS
XM=XM1**2+VARM
XM=SQRT(XM)
TALPH=TAN(ALPH1)+VARAL1
ALPHA=ATAN(TALPH)
DS=DELTAR*R2/COS(ALPHA)
R=R+DELTAR
AS=AS+DS
DELTAS=.037*AS**(-.2)*(V2/ANU)**(-.2)*DS
B=B0-2.*DELTAS/B2
DELTAR=B0-B
VARM=-2.*(1.+G2/2.*XM**2)/(XM**2-1./COS(ALPHA)**2)*((GAM*XM**2-TAN
1(ALPHA)**2)*ZETA/B0/COS(ALPHA)+1./B0*DELTAB/DELTAR-1./COS(ALPHA)**
22/R)*XM**2*DELTAR
VARAL=1./COS(ALPHA)**2/(XM**2-(1./COS(ALPHA))**2)*((1.+G2
1)*ZETA/B0/COS(ALPHA)+1./B0*DELTAB/DELTAR-XM**2/R)*TAN(ALPHA)*DELTA
2R
VARM=(VARM1+VARM)/2.
7 VARAL=(VARAL1+VARAL)/2.
B=(B+R1)/2.
XM=XM1**2+VARM
XM=SQRT(XM)
TALPH=TAN(ALPH1)+VARAL
ALPHA=ATAN(TALPH)
B0=B
ACCUSR=SQRT(1./(1.+G2/2.*XM**2))
RHOR=1./(1.+G2/2.*XM**2)**(1./G2)
F(NO)=XM**3*ACOUSR*RHOR*R
IF(NO.EQ.2) S(NO)=(F(NO)+F(NO-1))*0.5*DELTAR
IF(NO.EQ.2) GO TO 8
CALL FNTGRL(NO,DELTAR,F,S)
8 TPL=1./(1.+GAM*CF*R2*S(NO)/COS(AL2)/B2/XM2*(1.+G2/2.*XM2**2)**(G1/
12./G2))
PP=TPL*P2P
P3P(NO)=PP
XMARR(NO)=XM
XMACH=XMARR(NO)
1000 PTHP=P3P(NO)
IF(L.EQ.1) GO TO 30
M=2
21 IF(XMACH.GE.DIFLEM(M-1).AND.XMACH.LE.DIFLEM(M)) GO TO 22
M=M+1
GO TO 21
22 RANGE=(XMACH-DIFLEM(M-1))/(DIFLEM(M)-DIFLEM(M-1))*(FLRNG(M)-FLRNG(
1M-1))+FLRNG(M-1)
WSURGE=RANGE*WC+K
IF(EWF.LT.WSURGE) GO TO 203
30 CONTINUE
PTH=PTHP/(1.+G2/2.*XMACH**2)**(GAM/G2)
DHVLD=CP*T2P*((PTH/PTHP)**(G2/GAM)-(PTH/P2P)**(G2/GAM))
BT=1.-B
XMACH=XMACH*COS(ABS(ALPHA-AL3))
PTHP=PTH*(1.+G2/2.*XMACH**2)**(GAM/G2)
X1=(ALPHA-AL3)*57.29577
WFUNC=SW*SQRT(T2P)/ADTH/PTHP/B
IF(WFUNC.GE.FLFUNC) CPSTAR=0.
IF(WFUNC.GE.FLFUNC) K=1
IF(WFUNC.GE.FLFUNC) GO TO 14
IF((AR-1.2).GT.0..AND.(AR-2.).LT.0.) GO TO 10
IF((AR-2.).GT.0..AND.(AR-3.).LT.0.) GO TO 11

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      IF ((AR-3.).GT.0..AND.(AR-4.).LT.0.) GO TO 12
      IF ((AR-4.).GT.0..AND.(AR-5.).LT.0.) GO TO 13
10  CALL LININT(XMACH,BT,AMT,BARR,PREC1,4,6,F1)
      CALL LININT(XMACH,BT,AMT,BARR,PREC2,4,6,F2)
      CPSTAR=(AR-1.2)/.8*(F2-F1)+F1
      GO TO 14
11  CALL LININT(XMACH,BT,AMT,BARR,PREC2,4,6,F2)
      CALL LININT(XMACH,BT,AMT,BARR,PREC3,4,6,F3)
      CPSTAR=(AR-2.)*(F3-F2)+F2
      GO TO 14
12  CALL LININT(XMACH,BT,AMT,BARR,PREC3,4,6,F3)
      CALL LININT(XMACH,BT,AMT,BARR,PREC4,4,6,F4)
      CPSTAR=(AR-3.)*(F4-F3)+F3
      GO TO 14
13  CALL LININT(XMACH,BT,AMT,BARR,PREC4,4,6,F4)
      CALL LININT(XMACH,BT,AMT,BARR,PREC5,4,6,F5)
      CPSTAR=(AR-4.)*(F5-F4)+F4
14  CONTINUE
      IF(K.EQ.1.AND.J.EQ.1) GO TO 202
      IF(K.EQ.1.AND.L.EQ.1) GO TO 18
      IF(K.NE.1.AND.J.EQ.NVOVCR) GO TO 204
      PEXIT=CPSTAR*(PTHP-PTH)+PTH
      RTHP=PTHP/RGAS/T2P
      VCRTH=SQRT(2.*GAM/G1*RGAS*T2P)
      RVRVTH=SW/RTHP/VCRTH/ADTH/B
      VOVCR4=.020
100 P4PL=PEXIT/(1.-G2/G1*VOVCR4**2)**(GAM/G2)
      RVRVC4=(1.-G2/G1*VOVCR4**2)**(1./G2)*VOVCR4
      P4PG=RVRVTH*PTHP/AR/RVRVC4
      VCVC4=VOVCR4+.001
      IF(P4PL.LT.P4PG) GO TO 100
      PPEXIT=P4PG
15  DHCIF=T2P*CP*((PEXIT/PPEXIT)**(G2/GAM)-(PEXIT/PTHP)**(G2/GAM))
      PR=PPEXIT/POP
      ETAD=DHAERO-DHSF-DHBL-DHVLC-DHDIF-DHIGV-DHINC
      ETAD=ETAD/DHACT
      DEIGV=DHIGV/DHACT
      DERL=DHBL/DHACT
      DESF=DHSF/DHACT
      DEDF=DHCF/DHACT
      DERC=DHRC/DHACT
      DEVLD=DHVLD/DHACT
      DEVD=DHDIF/DHACT
      DEINC=DHINC/DHACT
      IF(L.EQ.2) GO TO 19
17  CONTINUE
      IF(L.EQ.1) GO TO 18
19  IF(NWRITE.NE.1) GO TO 35
      WRITE(6,300)
      WRITE(6,301) PERDS
      WRITE(6,302)
      WRITE(6,303) WSURGE,WCHK
      NWRITE=NWRITE+1
35  MIN=MIN+1
      WRITE(6,304)
      WRITE(6,305) EWF,PK,ETAD
      WRITE(6,306)
      WRITE(6,307) DEIGV,DEINC,DEBL,DESF,DEDF,DERC,DEVLD,DEVD
      IF(K.NE.1.AND.MIN.LE.NVOVCR) GO TO 2

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      IF(K.FC.1.AND.L.EQ.2) GO TO 1
200 WRITE(6,400)
      MIN=MIN+1
      IF(MIN.GT.NVOVCR) GO TO 1
      GO TO 2
201 WRITE(6,400)
      MIN=MIN+1
      IF(MIN.GT.NVOVCR) GO TO 1
      GO TO 2
202 WRITE(6,402)
      GO TO 1
203 WRITE(6,403) VOVCR(J)
      MIN=MIN+1
      IF(MIN.GT.NVOVCR) GO TO 1
      GO TO 2
204 WRITE(6,308)
      GO TO 1
      18 WCHK=Sw*SQRT(THETA)/DELTA
      GO TO 1
300 FORMAT(59X,13H PERCENT NDES)
301 FORMAT(63X,F5.1)
302 FORMAT(45X,16H SURGE FLOW RATE,10X,15HCHOKE FLOW RATE)
303 FORMAT(51X,F5.3,20X,F5.3)
304 FORMAT(44X,4H WEO,10X,14HPRESSURE RATIO,10X,4HETAT)
305 FORMAT(44X,F5.3,13X,F5.3,15X,F4.3)
306 FORMAT(11X,8H DETAIGV,8X,7HDETAINC,8X,6HDETABL,8X,6HDETSF,8X,6HDE
      ITADF,8X,6HDETARC,8X,7HDETAULD,8X,6HDETAVD)
307 FORMAT(13X,F6.5,9X,F6.5,8X,F6.5,8X,F6.5,8X,F6.5,8X,F6.5,9X,F6.5,
      18X,F6.5,9X,F6.5)
308 FORMAT(45H COMPRESSOR CHOKING FLOW HAS NOT BEEN REACHED)
309 FORMAT(21HINLET TOTAL PRESSURE,5X,23HINLET TOTAL TEMPERATURE,5X,2
      19HINLET TOTAL DYNAMIC VISCOSITY,5X,19HSPECIFIC HEAT RATIO,5X,12HGA
      2S CONSTANT)
310 FORMAT(17H NUMBER OF BLADES,5X,20HFRICITION CCEFFICIENT,5X,4HSPLT,5
      1X,12HDESIGN SPEED,5X,23HINDUCER RMS SWIRL ANGLE,5X,27HINDUCER RMS
      28BLOCKAGE FACTOR)
311 FORMAT(11X,24H INDUCER RMS BLADE ANGLE,5X,30HINDUCER HUB-TIP DIAME
      1TFR RATIO,5X,40HINDUCER TIP-IMPELLER EXIT DIAMETER RATIO)
312 FORMAT(30H IMPELLER BLADE EXIT BACKSWEEP,5X,23HIMPELLER BLADE EXIT
      1 HT.,5X,32HVANELESS DIFFUSER DIAMETER RATIO,5X,28HVANED DIFFUSER S
      2SETTING ANGLE)
313 FORMAT(33X,33H TOTAL VANED DIFFUSER THROAT AREA,5X,25HVANED DIFFUS
      1ER AREA RATIO)
314 FORMAT(47X,36H INLET CRITICAL VELOCITY RATIO ARRAY)
315 FORMAT(7X,F7.0,21X,F6.2,23X,F8.7,24X,F3.1,16X,F6.2)
316 FORMAT(7X,F3.0,20X,F4.3,15X,11.9X,F6.0,17X,F4.2,26X,F4.2)
317 FORMAT(24X,F4.1,27X,F6.4,34X,F6.4)
318 FORMAT(13X,F4.1,26X,F6.5,27X,F6.3,30X,F5.2)
319 FORMAT(47X,F7.6,28X,F4.2)
320 FORMAT(8F10.2)
400 FORMAT(1X,24HIRRATIONAL EXIT TRIANGLE)
402 FORMAT(1X,21HVOVCR ARRAY TOO LARGE)
403 FORMAT(1X,34HWT FLOW LESS THAN SURGE FOR V/VCR=,F4.2)
      END

```

Subroutine LININT(X1, Y1, X, Y, TN, MX, MY, F)

This subroutine interpolates a value of maximum pressure recovery coefficient C_p^{**} from a table of vaned diffuser throat Mach numbers and aerodynamic blockage given as input.

X1 input, vaned diffuser throat Mach number
 Y1 input, throat aerodynamic blockage
 X input array of throat Mach numbers
 Y input array of throat blockages
 TN input two-dimensional array of C_p^{**} corresponding to throat Mach numbers and blockages
 MX input, number of throat Mach numbers
 MY input, number of throat blockages
 F output, interpolated value of C_p^{**}

\$/BFTC LININT

```

SUBROUTINE LININT (X1,Y1,X,Y,TN,MX,MY,F)
DIMENSION X(MX), Y(MY), TN(MX,MY)
DO 1 J3=2,MX
1 IF (X1.LE.X(J3)) GO TO 2
J3=MX
2 DO 3 J4=2,MY
3 IF (Y1.LE.Y(J4)) GO TO 4
J4=MY
4 J1=J3-1
J2=J4-1
EPS1=(X1-X(J1))/(X(J3)-X(J1))
EPS2=(Y1-Y(J2))/(Y(J4)-Y(J2))
EPS3=1.-EPS1
EPS4=1.-EPS2
F=TN(J1,J2)*EPS3*EPS4+TN(J3,J2)*EPS1*EPS4+TN(J1,J4)*EPS2*EPS3+TN(J
13,J4)*EPS1*EPS2
RETURN
END
  
```

Subroutine FNTGRL(NO, DELTAR, F, S)

This subprogram is used to integrate the function $M^3(\rho a/\rho' a')$ in the vaneless dif-
 fuser.

NO number of equally spaced radii
 DELTAR radius ratio between stations
 F function $M^3(\rho a/\rho'a')$
 S integral of F

No FORTRAN listing of the subprogram is available but a brief description of the method of integration is as follows:

The subprogram uses Simpson's rule in the following manner:

First interval:

$$\int_{x_1}^{x_1} f(x)dx = 0$$

Second interval:

$$\int_{x_1}^{x_2} f(x)dx = \Delta x(5f_1 + 8f_2 - f_3)/12$$

Remaining intervals:

$$\int_{x_i}^{x_{i+1}} f(x)dx = \Delta x(5f_{i+1} + 8f_i - f_{i-1})/12$$

Lewis Research Center,
 National Aeronautics and Space Administration,
 and
 U.S. Army Air Mobility R&D Laboratory,
 Cleveland, Ohio, August 2, 1973,
 501-24.

APPENDIX A

SYMBOLS

A	area, m^2
AR	area ratio
a	local acoustic velocity, m/sec
B	effective depth ratio
b	blade height or passage depth, m
C	wall curvature, m^{-1}
C_f	skin friction coefficient
C_p	specific heat, J/(kg)(K)
C_p^{**}	maximum pressure recovery coefficient at a constant area ratio
D	diameter, m
D_f	diffusion factor
e_s	inlet guide vane loss coefficient
h	spacing for numerical integration
Δh	incremental compressor specific enthalpy, J/kg
K	constant
L	blade length, m
M	Mach number
N	rotative speed, rpm
n	distance along radius, m
p	pressure, N/m^2
Q	volumetric flow rate, m^3/sec
q	dimensionless enthalpy
R	gas constant, J/(kg)(K)
\bar{R}	radius ratio
Re	Reynolds number based on inlet total conditions
r	radius, m
s	arc length, m

Δs	incremental arc length, m
T	temperature, K
t	blade thickness, m
u	blade speed, m/sec
V	absolute gas velocity, m/sec
W	relative gas velocity, m/sec
w	mass flow rate, kg/sec
Z	number of impeller blades
α	absolute flow angle, deg from meridional plane
β	relative flow angle, deg from meridional plane
β_b	blade angle, deg from meridional plane
γ	specific heat ratio
δ	ratio of inlet total pressure to standard sea-level pressure
$\Delta\delta^*$	incremental boundary layer displacement thickness, m
ϵ	difference between compressor inlet relative flow angle and optimum incidence angle
ζ	vaneless diffuser loss coefficient
η	total efficiency
$\Delta\eta$	total efficiency decrement
θ	ratio of inlet total temperature to standard sea-level temperature
λ	inducer hub-tip diameter ratio
μ	dynamic viscosity, N-sec/m ²
ν	kinematic viscosity, m ² /sec
ρ	gas density, kg/m ³
φ	flow coefficient
χ	wall slope or streamline angle, deg from axial

Subscripts:

act	actual
AD	adiabatic
aero	aerodynamic

av	average
BL	blade loading
calc	calculated
choke	value at choking flow rate
cr	critical condition
DES	design
DF	disk friction
eff	effective
eq	equivalent
est	estimated
exit	exit
H	hub
HYD	hydraulic
i	iteration subscript
id	ideal
IGV	inlet guide vane
INC	incidence
is	isentropic
L	lost
m	meridional
max	maximum
MF	rms
n	normal
opt	optimum
R	rotor
RC	recirculation
SF	skin friction
SL	slip
st	stagger
surge	value at surge flow rate

T	tip
u	tangential
v	vortex
VD	vaned diffuser
VLD	vaneless diffuser
0	station just upstream of inlet guide vanes
1	impeller inlet upstream of blade
2	impeller inlet just downstream of blade leading edge
3	impeller exit
4	vaned diffuser leading edge
5	vaned diffuser throat
6	vaned diffuser exit

Superscripts:

'	absolute total condition
''	relative total condition

APPENDIX B

EQUATIONS

This section presents a more detailed discussion of the method of calculating compressor performance than was presented in the section Method of Analysis.

The equations used in calculating the flow solution through the compressor are listed here in the approximate order of solution in the FORTRAN program. The known constants are the input fluid state and thermodynamic properties, compressor geometry, and velocity diagram data. The working fluid properties and state conditions are specific heat ratio γ , inlet total pressure p'_0 , inlet total temperature T'_0 , and inlet dynamic viscosity based on total conditions μ'_0 . The velocity diagram data are compressor design rotative speed N_{DES} , the fraction of design rotative speed for which performance data is desired N/N_{DES} , the number of values of $(V/V_{cr})_0$ for which performance is to be calculated, the values of $(V/V_{cr})_0$ to be used, and the inducer solid-body swirl angle at the rms diameter α_{1MF} . The compressor data are inducer inlet hub and tip wall slopes χ_{1H} and χ_{1T} , inducer inlet hub and tip wall curvatures C_{1H} and C_{1T} , inducer inlet tip diameter D_{1T} , inducer inlet hub-tip diameter ratio λ , inducer-inlet-tip to impeller-exit diameter ratio D_{1T}/D_3 , number of blades at impeller exit (including splitters) Z_3 , impeller blade exit angle (positive opposite to direction of rotation) β_{3b} , impeller exit blade height b_3 , inducer inlet blade angle at the rms diameter β_{1MFb} , inducer inlet blockage factor calculated at the rms diameter, vaneless diffuser diameter ratio D_4/D_3 , vaned diffuser setting angle α_4 , total vaned diffuser throat area A_5 , vaned diffuser area ratio A_6/A_5 , and wetted surface friction coefficient C_f . With these known values compressor performance can be evaluated by the method described.

Calculation of Inlet Velocity Triangles and Compressor Weight Flow

Calculation of the inducer inlet velocity diagrams and weight flow are handled by two methods depending on whether the inlet is swirl-free or subject to solid-body swirl. For the swirl cases it is assumed that the inlet guide vanes are located in a constant area annulus with zero wall slope with respect to the axial direction. The inner and outer diameters of the annulus are assumed to be equal to the inducer inlet hub and tip diameters. For the swirl-free cases it is assumed that the flow orthogonal can be approximated by a radial line. These assumptions greatly simplify calculation of the velocities specified by the general velocity gradient equation.

Swirl-free inlets. - For compressor configurations with swirl-free inlets the input value of $\left(\frac{V}{V_{cr}}\right)_0$ is used as the hub streamline value of V/V_{cr} . The variation of inlet velocity with radius is calculated from the general velocity gradient equation simplified for swirl-free flow. This equation is (in simplified form from ref. 10)

$$V_m = V_{m1H} e^{\int_0^n C \, dn} \quad (B1)$$

where V_{m1H} is the hub absolute velocity, C is the streamline curvature, and n is the distance along a radius. Streamline curvature and slope at the rms inlet diameter are approximated by linear interpolation of the input hub and tip values. The integral in the previous equation is approximated by the trapezoidal rule at the rms diameter and by Simpson's rule for unequal intervals at the tip. The numerical approximations are

$$V_{m1MF} = V_{m1H} e^{\left[\frac{h_0}{2} (C_{1H} + C_{1MF}) \right]} \quad (B2)$$

and

$$V_{m1T} = V_{m1H} e^{\left\{ \left(\frac{h_0 + h_1}{6} \right) \left[\left(2 - \frac{h_1}{h_0} \right) C_{1H} + \frac{(h_0 + h_1)^2}{h_1 h_0} C_{1MF} + \left(2 - \frac{h_0}{h_1} \right) C_{1T} \right] \right\}} \quad (B3)$$

where

$$h_0 = r_{1MF} - r_{1H} \quad (B4)$$

and

$$h_1 = r_{1T} - r_{1MF} \quad (B5)$$

Static densities at the hub, rms, and tip diameters are determined from the inlet total density and the calculated velocity at each station. Velocity components normal to the annular inlet plane are calculated using the velocities and streamline angles at the three stations:

$$V_{m1n} = V_{m1} \cos \chi \quad (B6)$$

where χ is the streamline angle. Inlet mass flow is then computed using Simpson's rule for unequal intervals

$$w = 2\pi \left\{ \frac{h_0 + h_1}{6} \left[\left(2 - \frac{h_1}{h_0} \right) (\rho r)_{1H} V_{m1Hn} + \frac{(h_0 + h_1)^2}{h_0 h_1} (\rho r)_{1MF} V_{m1MFn} + \left(2 - \frac{h_0}{h_1} \right) (\rho r)_{1T} V_{m1Tn} \right] \right\} \quad (B7)$$

Inlets with solid-body swirl. - For impeller inlets with inlet guide vanes producing solid-body swirl the equations presented in reference 2 for kinetic energy loss were iteratively solved for state conditions and velocities downstream of the inlet guide vanes. Conditions at the rms diameter were assumed to be representative of the flow distribution at the impeller inlet. The inlet guide vane stagger angle was assumed to be one-half of the turning angle at the rms diameter; that is,

$$\alpha_{ST} = \frac{\alpha_{1MF}}{2} \quad (B8)$$

The inlet guide vane loss coefficient was calculated from the equation

$$e_S = \frac{0.0076}{\cos \alpha_{1MF} - 0.025} \left(1 + \frac{\cos \alpha_{ST}}{0.7} \right) \quad (B9)$$

Using the input value of $(V/V_{cr})_0$ as a first approximation to the value of V/V_{cr} downstream of the inlet guide vanes at the rms diameter, the following equations are solved iteratively with successive increments in V/V_{cr} until continuity checks the calculation of equation (B7):

$$KE = \frac{\left(\frac{V}{V_{cr}} V_{cr}\right)^2}{2} \quad (\text{B10})$$

$$\left(\frac{p}{p'}\right)_{1MF} = \left(1 - \frac{KE}{C_1 T'_0}\right)^{\gamma/(\gamma-1)} \quad (\text{B11})$$

$$KE_{id} = \frac{KE}{1 - e_S} \quad (\text{B12})$$

$$\frac{p_{1MF}}{p'_0} = \left(1 - \frac{KE_{id}}{C_p T'_0}\right)^{\gamma/(\gamma-1)} \quad (\text{B13})$$

$$p'_{1MF} = p'_0 \frac{\frac{p_{1MF}}{p'_0}}{\left(\frac{p}{p'}\right)_{1MF}} \quad (\text{B14})$$

$$\rho'_{1MF} = \frac{p'_{1MF}}{RT'_0} \quad (\text{B15})$$

$$p_{1MF} = p'_{1MF} \left(\frac{p}{p'}\right)_{1MF} \quad (\text{B16})$$

$$\rho_{1MF} = \rho'_{1MF} \left(\frac{p}{p'}\right)_{1MF}^{1/\gamma} \quad (\text{B17})$$

$$Q_1 = \frac{\pi}{4} D_{1T}^2 (1 - \lambda^2) \left(\frac{V}{V_{cr}}\right)_{1MF} V_{cr} \cos \alpha_{1MF} \quad (\text{B18})$$

$$w = Q_1 \rho_{1MF} \quad (\text{B19})$$

When continuity is satisfied downstream of the inlet guide vanes, the impeller inlet velocity triangles are calculated. Combination of the Euler equation with the solid-body vortex equation and simple radial equilibrium equation shows that the meridional velocity distribution can be expressed as

$$V_{m1} = \sqrt{K_{Vm} - 2V_{u1}^2} \quad (B20)$$

Using the value of V/V_{cr} which satisfies continuity downstream of the inlet guide vanes and the input value of the rms turning angle allows solution of the constant in equation (B20). The tangential components of the inlet absolute velocity at the hub and tip are calculated from the vortex condition. Then the hub and tip meridional velocities can be determined as follows:

$$V_u = K_{Vu} r \quad (B21)$$

where

$$K_{Vu} = \frac{V_{u1MF}}{r_{1MF}} \quad (B22)$$

The following general inducer inlet velocity diagram characteristics are calculated after the particular swirl-free or solid-body swirl calculations are completed:

$$V_{1T} = \sqrt{V_{m1T}^2 + V_{u1T}^2} \quad (B23)$$

$$\alpha_{1T} = \sin^{-1} \left(\frac{V_{u1T}}{V_{1T}} \right) \quad (B24)$$

$$W_{u1T} = u_{1T} - V_{u1T} \quad (B25)$$

$$\beta_{1T} = \tan^{-1} \left(\frac{W_{u1T}}{V_{m1T}} \right) \quad (B26)$$

$$W_{1T} = \sqrt{V_{m1T}^2 + W_{u1T}^2} \quad (\text{B27})$$

$$W_{u1H} = u_{1H} - V_{u1H} \quad (\text{B28})$$

$$\beta_{1H} = \tan^{-1} \left(\frac{W_{u1H}}{V_{m1H}} \right) \quad (\text{B29})$$

$$W_{1H} = \sqrt{V_{m1H}^2 + W_{u1H}^2} \quad (\text{B30})$$

$$V_{1MF} = \sqrt{V_{u1MF}^2 + V_{m1MF}^2} \quad (\text{B31})$$

$$W_{u1MF} = u_{1MF} - V_{u1MF} \quad (\text{B32})$$

$$W_{1MF} = \sqrt{V_{m1MF}^2 + W_{u1MF}^2} \quad (\text{B33})$$

$$\beta_{1MF} = \tan^{-1} \left(\frac{W_{u1MF}}{V_{m1MF}} \right) \quad (\text{B34})$$

The wheel speeds used in the previous equations are obtained from the following input constants:

$$u_{1T} = \frac{\pi \left(\frac{N}{N_{DES}} \right) N_{DES} D_{1T}}{60} \quad (\text{B35})$$

$$u_{1H} = \lambda u_{1T} \quad (\text{B36})$$

$$u_{1MF} = u_{1T} \frac{D_{1MF}}{D_{1T}} \quad (\text{B37})$$

where

$$D_{1MF} = \sqrt{\frac{1}{2} D_{1T}^2 (1 + \lambda^2)} \quad (B38)$$

Individual Losses

Inlet guide vane loss. - When the inducer inlet velocity diagram characteristics have been determined by the method described in the section Inlets With Solid-Body Swirl, the inlet guide vane loss is computed using the equation found in reference 1, subject to the assumptions made in reference 3.

$$\Delta h_{IGV} = e_S KE_{id} \quad (B39)$$

Inducer incidence loss. - The equations developed in reference 4 are used to determine the optimum inducer incidence angle for incompressible flow. Compressibility effects are ignored because the incidence loss is evaluated at the rms diameter and compressibility effects are insignificant except at the hub according to reference 4. Using the input blade blockage factor at the rms diameter the optimum incidence angle is found by

$$\epsilon = \tan^{-1} \frac{(1 - B_1) \tan \beta_{1MF}}{1 + B_1 \tan^2 \beta_{1MF}} \quad (B40)$$

where

$$B_1 = 1 - \frac{Z_1 t_u}{2\pi r_{1MF}} \quad (B41)$$

The optimum relative flow angle is then

$$\beta_{opt} = \beta_{1MF} - \epsilon \quad (B42)$$

and the component of the relative velocity lost is

$$W_L = W_{1MF} \sin |\beta_{opt} - \beta_{1MF}| \quad (B43)$$

The enthalpy loss due to incidence is expressed as

$$\Delta h_{INC} = \frac{W_L^2}{2C_p} \quad (B44)$$

and the total pressure just inside the blade row is

$$p'_{2MF} = p'_{1MF} e^{\left(\frac{-\Delta h_{INC}}{T_{2R}}\right)} \quad (B45)$$

Impeller work and losses. - The impeller exit density is obtained through iteration of the impeller loss equations and calculated state properties. The enthalpy rise in the impeller is initially approximated as

$$\Delta h_{est} = u_3^2 \quad (B46)$$

and the corresponding impeller exit total temperature is then

$$T'_{3est} = \left(\frac{\Delta h_{est}}{C_p T'_0} + 1\right) T'_0 \quad (B47)$$

The impeller exit density is initially approximated to be

$$\rho_3 = \rho_{1MF} \left(\frac{T'_{3est}}{T'_0}\right)^{1/(\gamma-1)} \quad (B48)$$

The meridional component of exit absolute velocity is calculated from continuity

$$V_{m3} = \frac{w}{\pi \rho_3 D_3 b_3} \quad (B49)$$

The tangential component of exit absolute velocity is then

$$V_{u3} = u_3 - V_{m3} \tan \beta_{3b} - V_{SL} \quad (B50)$$

where the slip velocity V_{SL} is calculated by the method of reference 11.

$$V_{SL} = \frac{u_3 \sqrt{\cos \beta_{3b}}}{Z_3^{0.7}} \quad (B51)$$

The remaining state and flow properties at the exit were calculated from the following relations:

$$T_3'' = T_{1MF}'' + \frac{u_3^2 - u_{1MF}^2}{2C_p} \quad (B52)$$

$$W_{u3} = u_3 - V_{u3} \quad (B53)$$

$$W_3 = \sqrt{V_{m3}^2 + W_{u3}^2} \quad (B54)$$

$$T_3 = T_3'' - \frac{W_3^2}{2C_p} \quad (B55)$$

$$V_3 = \sqrt{V_{m3}^2 + V_{u3}^2} \quad (B56)$$

$$T_3' = T_3 + \frac{V_3^2}{2C_p} \quad (B57)$$

The work loss due to blade loading is calculated from the equation

$$\Delta h_{BL} = 0.05 D_f^2 u_3^2 \quad (B58)$$

which is given by reference 5. The diffusion factor D_f is defined as

$$D_f = 1 - \frac{W_3}{W_{1T}} + \frac{K_{BL} q_{aero}}{\frac{W_{1T}}{u_3} \left[\frac{Z_3}{\pi} \left(1 - \frac{D_{1T}}{D_3} \right) + 2 \frac{D_{1T}}{D_3} \right]} \quad (B59)$$

where a value of 0.75 is used for K_{BL} for conventional impellers and a value of 0.6 is used for impellers with splitters. A parametric study of calculated diffusion factors with a variation in the number of blades indicated that changing the constant to 0.6 would compensate for the changing solidity near the exit. The dimensionless actual head is obtained by dividing the enthalpy rise by the exit blade speed squared

$$q_{aero} = \frac{\Delta h_{aero}}{u_3^2} \quad (B60)$$

where

$$\Delta h_{aero} = C_p T'_0 \left(\frac{T'_3}{T'_0} - 1 \right) \quad (B61)$$

Impeller disk friction loss is computed using the method of reference 6

$$\Delta h_{DF} = 0.01356 \frac{\rho_3}{wRe^{0.2}} u_3^3 D_3^2 \quad (B62)$$

The Reynolds number in this equation is based on impeller exit dimensions and inlet total conditions

$$Re = \frac{u_3 D_3 \rho'_1 MF}{\mu'_0} \quad (B63)$$

Skin friction loss is calculated from the correlation found in reference 5

$$\Delta h_{SF} = K_{SF} C_f \frac{\frac{L}{D_3} \left(\frac{W}{u_3}\right)_{av}^2}{\frac{D_{HYD}}{D_3}} u_3^2 \quad (B64)$$

where the mean flowpath blade length-diameter ratio is expressed as

$$\frac{L}{D_3} = \frac{1}{2} \frac{1 - \frac{D_{1MF}}{0.3048}}{\cos \beta_{3b}} \quad (B65)$$

The ratio of mean hydraulic-exit diameter ratio is calculated from the equation

$$\frac{D_{HYD}}{D_3} = \frac{1}{\frac{Z_3}{\pi \cos \beta_{3b}} + \frac{D_3}{b_3}} + \frac{\frac{D_{1T}}{D_3}}{\frac{2}{1-\lambda} + \frac{2Z_3}{\pi(1+\lambda)} \sqrt{1 + \tan^2 \beta_{1T} \left(1 + \frac{\lambda^2}{2}\right)}} \quad (B66)$$

and the ratio of mean relative velocity-impeller exit velocity is determined by

$$\left(\frac{W}{u_3}\right)_{av}^2 = \frac{1}{2} \left\{ \left(\frac{V_{m1MF}}{u_3}\right)^2 + \left(\frac{D_{1MF}}{D_3}\right)^2 + \left(\frac{W_3}{W_{1T}}\right)^2 \left[\left(\frac{V_{m1MF}}{u_3}\right)^2 + \left(\frac{D_{1T}}{D_3}\right)^2 \right] \right\} \quad (B67)$$

Some studies of the effects of the addition of splitter blades on the impeller flow indicated that the mean channel relative velocity is increased in the splitter region. The ratio of mean flow path blade length and hydraulic diameter-exit diameter ratio remain virtually unchanged. Computation of the mean relative velocity ratios for an impeller both with and without splitters showed that, for splitters, the average relative velocity is about 14 percent higher than for conventional impellers. This phenomenon is accounted for by using the constant 7.0 for impellers with splitters and 5.6 for impellers without splitters.

At this point in the iteration procedure the impeller ideal enthalpy rise is calculated as follows:

$$\Delta h_{id} = \Delta h_{aero} - \Delta h_{IGV} - \Delta h_{INC} - \Delta h_{SF} - \Delta h_{BL} \quad (B68)$$

Defining the impeller efficiency as

$$\eta_R = \frac{\Delta h_{id}}{\Delta h_{aero}} \quad (B69)$$

the state conditions at the impeller exit are calculated from the relations

$$p'_3 = p'_{2MF} \left(\frac{\eta_R \Delta h_{aero}}{C_p T'_0} + 1 \right)^{\gamma/(\gamma-1)} \quad (B70)$$

$$p_3 = \frac{p'_3}{\left(\frac{T'_3}{T_3} \right)^{\gamma/(\gamma-1)}} \quad (B71)$$

$$\rho_3 = \frac{p_3}{RT_3} \quad (B72)$$

The value of ρ_3 obtained from equation (B72) is compared to the value estimated in equation (B48).

If the values do not compare within 0.1 percent, the former value is used as a new approximation and equations (B49) to (B72) are iterated until two consecutive values of exit density agree within the tolerance specified.

Recirculation loss. - Recirculation of the working fluid from the vaneless space back into the impeller results in additional work which is lost to the system. Reference 5 expresses this loss as a function of the impeller exit absolute flow angle, impeller diffusion factor, and impeller exit tip speed. The following modified form of the equation of reference 5 is used to calculate the recirculation loss:

$$\Delta h_{RC} = 0.02 \sqrt{\tan \alpha_3} D_f^2 u_3^2 \quad (B73)$$

Vaneless diffuser loss. - Reference 7 developed differential equations relating Mach number, flow angle, and total temperature to vaneless diffuser radius ratio through the

fundamental relations of continuity, equilibrium, heat transfer, and fluid state. These equations are evaluated at ten equally spaced intervals in the vaneless space. Two iterations of the equations are performed at each station; the first iteration uses the calculated properties at the point of interest to compute the variation in Mach number and flow angle to the next point; the second iteration uses the estimated properties of the downstream point to compute the same variations. The arithmetic average of the two iterations is then used for the solution.

These equations, simplified for adiabatic flow in a geometrically constant depth radial passage are

$$\frac{1}{M^2} \frac{dM^2}{d\bar{R}} = \frac{-2 \left(1 + \frac{\gamma - 1}{2} M^2 \right)}{M^2 - \sec^2 \alpha} \left[(\gamma M^2 - \tan^2 \alpha) \frac{\zeta}{B \cos \alpha} + \frac{1}{B} \frac{dB}{d\bar{R}} - \frac{\sec^2 \alpha}{\bar{R}} \right] \quad (B74)$$

and

$$\frac{1}{\tan \alpha} \frac{d \tan \alpha}{d\bar{R}} = \frac{\sec^2 \alpha}{M^2 - \sec^2 \alpha} \left\{ \left[1 + (\gamma - 1) M^2 \right] \frac{\zeta}{B \cos \alpha} + \frac{1}{B} \frac{dB}{d\bar{R}} - \frac{M^2}{\bar{R}} \right\} \quad (B75)$$

where

$$\zeta = \frac{C_f r_3}{b_3} \quad (B76)$$

$$\bar{R} = \frac{r}{r_3} \quad (B77)$$

$$B = \frac{b}{b_3} \quad (B78)$$

The schedule of effective passage depth is determined by boundary layer displacement thickness growth on the end walls. The end walls in the vaneless diffuser are assumed to be parallel and have a spacing equal to the impeller exit blade height. The flow pattern between the end walls is approximated as a log spiral between adjacent calculation stations. With these assumptions the incremental flow path length is

$$\Delta S = \frac{r_2 \overline{\Delta R}}{\cos \alpha} \quad (\text{B79})$$

and the incremental boundary layer displacement thickness is

$$\Delta \delta^* = 0.037 S^{-0.2} \left(\frac{V_2}{\nu} \right)^{-0.2} \Delta S \quad (\text{B80})$$

where

$$S = \sum_{i=1}^n \Delta S_i \quad (\text{B81})$$

The effective passage depth is

$$B_{i+1} = B_i - \frac{2 \Delta \delta^*}{b_3} \quad (\text{B82})$$

and

$$\Delta B = B_i - B_{i+1} \quad (\text{B83})$$

Loss the total pressure in the vaneless space is computed from the following equation derived in reference 4:

$$\frac{1}{\left(\frac{p_4'}{p_3'} \right)} = 1 + \frac{\gamma C_f}{\cos \alpha_3} \frac{r_3}{b_3} \frac{\int_1^{\overline{R}} M^3 \frac{a}{a'} \frac{\rho}{\rho'} \overline{R} d\overline{R}}{M_3 \left(\frac{a}{a'} \right)_3 \left(\frac{\rho}{\rho'} \right)_3} \quad (\text{B84})$$

The integral in equation (B84) is determined by numerical methods. Vaned diffuser leading edge static pressure is calculated from the isentropic relation using the total pressure obtained from equation (B84) and the Mach number obtained from the distribution prescribed by equation (B74)

$$p_4 = \frac{p_4'}{\left(1 + \frac{\gamma - 1}{2} M_4^2\right)^{\gamma/(\gamma-1)}} \quad (\text{B85})$$

Vaneless diffuser loss is then determined by

$$\Delta h_{\text{VLD}} = C_p T_3' \left[\left(\frac{p_4}{p_4'}\right)^{(\gamma-1)/\gamma} - \left(\frac{p_4}{p_3'}\right)^{(\gamma-1)/\gamma} \right] \quad (\text{B86})$$

Vaned diffuser loss. - Vaned diffuser performance is predicted by use of the test data reported in reference 8. Lines of maximum pressure recovery coefficient at a given area ratio were estimated from the performance maps reported for single plane divergence diffusers with square throats. The component of the vaned diffuser leading edge Mach number parallel to the vane setting angle is used as the throat Mach number. A loss in total pressure associated with this incidence is calculated holding static pressure constant between the leading edge and throat. The throat blockage is estimated from the displacement thickness growth on the vaneless diffuser end walls. Using these conditions of throat Mach number, total pressure, and blockage the pressure recovery of the vaned diffuser is extrapolated for the specified geometric area ratio. Vaned diffuser exit static pressure is then calculated from the relation

$$p_6 = C_p^{**} (p_5' - p_5) + p_5 \quad (\text{B87})$$

The exit total pressure and velocity are determined by trial and error using estimated values of exit critical velocity ratio. The total pressure at the vaned diffuser throat is assumed to be constant across the free-stream area outside the boundary layer displacement thickness. The total pressure and velocity at the vaned diffuser exit are calculated assuming full flow across the geometric area. Starting with a low value of $(V/V_{\text{cr}})_6$ the lower estimate of exit total pressure is expressed as

$$p_6' = \frac{p_6}{\left[1 - \frac{\gamma - 1}{\gamma + 1} \left(\frac{V}{V_{\text{cr}}}\right)_6^2\right]^{\gamma/(\gamma-1)}} \quad (\text{B88})$$

and the higher estimate is

$$p'_6 = \frac{\left(\frac{\rho V}{\rho' V_{cr}}\right)_5 p'_5}{AR \left(\frac{\rho V}{\rho' V_{cr}}\right)_6} \quad (\text{B89})$$

where

$$\left(\frac{\rho V}{\rho' V_{cr}}\right)_5 = \frac{w}{\rho'_5 (V_{cr})_5 A_5 B_5} \quad (\text{B90})$$

Equations (B88) and (B89) are solved using increasing values of $(V/V_{cr})_6$ until convergence is achieved. The vaned diffuser loss is then calculated from the relation

$$\Delta h_{VD} = C_p T'_3 \left[\left(\frac{p_6}{p'_6}\right)^{(\gamma-1)/\gamma} - \left(\frac{p_6}{p'_5}\right)^{(\gamma-1)/\gamma} \right] \quad (\text{B91})$$

Efficiency decrements. - Decrements in efficiency caused by the individual losses are obtained from the following equations:

$$\Delta \eta_{IGV} = \frac{\Delta h_{IGV}}{\Delta h_{act}} \quad (\text{B92})$$

$$\Delta \eta_{INC} = \frac{\Delta h_{INC}}{\Delta h_{act}} \quad (\text{B93})$$

$$\Delta \eta_{BL} = \frac{\Delta h_{BL}}{\Delta h_{act}} \quad (\text{B94})$$

$$\Delta \eta_{SF} = \frac{\Delta h_{SF}}{\Delta h_{act}} \quad (\text{B95})$$

$$\Delta h_{DF} = \frac{\Delta h_{DF}}{\Delta h_{act}} \quad (B96)$$

$$\Delta \eta_{RC} = \frac{\Delta h_{RC}}{\Delta h_{act}} \quad (B97)$$

$$\Delta \eta_{VLD} = \frac{\Delta h_{VLD}}{\Delta h_{act}} \quad (B98)$$

$$\Delta \eta_{VD} = \frac{\Delta h_{VD}}{\Delta h_{act}} \quad (B99)$$

where

$$\Delta h_{act} = \Delta h_{aero} + \Delta h_{RC} + \Delta h_{DF} \quad (B100)$$

Overall efficiency. - The overall total efficiency is calculated as follows:

$$\eta_{AD} = \frac{\Delta h_{aero} - (\Delta h_{IGV} + \Delta h_{INC} + \Delta h_{BL} + \Delta h_{SF} + \Delta h_{VLD} + \Delta h_{VD})}{\Delta h_{aero} + \Delta h_{RC} + \Delta h_{DF}} \quad (B101)$$

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