



## Concentration Flux Dependent on Radiative MHD Casson Flow with Arrhenius Activation Energy: Homotopy Analysis Method (HAM) with an Evolutionary Algorithm

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### ABSTRACT

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*Stefan blowing, blood flow, Casson fluid, HAM, Arrhenius activation energy*

Heat transfer analysis in nanofluids is an active research field due to its extraordinary physical and chemical properties. In the current study, the focus lies on the effects of Stefan blowing when a non-Newtonian Casson base fluid flows over a surface which stretches linearly. A uniform transverse magnetic field is employed. The chemical reaction in the fluid with activation energy and radiation effects have also been engaging the attention. Fundamental laws of conservation are employed to model governing equations of flow. Similarity transform is introduced to reduce the said system of partial differential equations to ordinary differential equations which are in turn tackled analytically using Homotopy Analysis Method with genetic algorithms to optimise the series solution. The impact of pertaining parameters on the dimensionless velocity, temperature and concentration were presented explicitly. This study relevant to remedies for malign tissues, cells or clogged arteries of the heart.

## 1. INTRODUCTION

Non-Newtonian fluids are the center of attention of many engineers and scientists due to their wide variety of applications in biomechanics, engineering, and industry like the extraction of crude oil from petroleum products. The flow of blood in the body and transport of sewage, etc. Working in the field of non-Newtonian fluid flows challenges the mathematician and simulation engineers with its diversity and complexity. As the complexity of such fluids offers no unique constitutive equation which encounters all the properties of such fluids, resulting in several non-Newtonian models are presented [1-5]. In non-Newtonian fluids, Casson fluid have several properties. Casson fluid illustrated yield stresses. Its mathematical modelling was derived by Casson in 1995. The model helps to improve the accountability of adhesive slurry at a high shear - rate. Casson fluid is a fluid that exerts shear-thinning liquid which shows zero shear rate at infinite viscosity leads to no flow below particular yield stress (i.e., it behaves like a solid) [6]. Examples include tomato sauce, honey and jelly etc. Researchers had proven that blood rheology closest to Casson fluids [7].

Nadeem et al. [8] studied the three-dimensional flow of Casson fluid in porous space over a stretching sheet which is stretched linear under the effect of the uniform magnetic field. Tu and Deville [9] earlier show blood like the behaviour of Casson fluid and discussed pulsatile flow in arterial stenoses. More recently, Majeed et al. [10] investigated the influence of

higher-order wall slip of Casson fluid along with heat transfer and suction/injection. They also consider the uniform magnetic field and convective thermal boundary condition. Animasaun et al. [11] examined the flow of Casson liquid over a paraboloid with the stratified melting surface. Some recent studies regarding Casson fluids are found in the papers [12-15].

Engineering application like paper drying, thermal coating, hot rolling, glass fiber stretching, etc. divert one's focus towards mass and heat transfer of non-newtonian fluids over a stretching sheet. Crane [16] seems to be the first to identify and investigate the boundary layer flow due to linear stretching. Motivated by this, it stimulates an extensive literature in this field, which includes, analysis over a stretching cylinder and sheet with Cattaneo-Christov heat flux model [17, 18]. The results of the stretching cylinder can be reduced to the sheet if the curvature of the cylinder is minimised. Heat transfer with multiple modes in the presence of electric and buoyancy effects can be found in the papers [19, 20]. Different non-Newtonian Rheological fluids include [21-23]. Magnetic rheological behaviour [24, 25] and different types of stretching can be found in the papers [26, 27].

Mehmood presented some new solutions and similarities for these flows [28]. An interesting aspect of mass and heat transfer of non-Newtonian fluids are a chemical reaction which arises in many industrial processes. The chemical reaction sorts an essential role in the manufacturing of instruments like a solar antenna, rubbery isolation, humidity in

the gardens or dispersion of prescription in the blood. The first-order chemical reaction is proportional to the concentration of the fluid. Numerous readings linked to the present topic is available with diverse geometries [29-32].

However, given literature, not much is deliberated in the area of the mass transfer due to Arrhenius energy and binary chemical reaction. Bestman [33] was the first who examined the convective heat flow over a porous plate along with an activation energy. One of the essential components of a chemical reaction is its activation energy (below which the process is inert). The profound applications in geothermal reservoirs and oil industry make it an essential topic. Makinde et al. [34] worked with time-dependent flow through a porous space. Endo/exothermic reactions were explored by Maleque [35]. Awad et al. [36] employed SRM to find the solutions of rotating unsteady flow over an impulsively stretched sheet. For the stagnation point flow of Casson fluid, the work of Abbas et al. [37] is available. Mustafa et al. [38] discussed MHD nanofluid flow and Ellahi et al. [39] worked with Biofluid through flexible walls. In a process like paper dying via evaporation, sometimes occurs the effects of blowing, which are observed in Stefan's problem [40].

This is different from transpiration at the surface as it can be observed on the impermeable wall. It tends to generate the bulk motion of the mass, and consequently, other motion in a fluid is observed. Fang and Jing [41] have presented the effects on starching plate. Latiff et al. [42] work with rotating the solid disk. Alamri et al. [43] examined the effects in internal flow with slip effects. Uddin et al. [44] discuss Stefan's blowing on moving plate with nanofluid.

A review of the relevant literature indicates that there have been no previous studies which considered the Casson fluid flow over a radiative stretching sheet with binary chemical reaction with activation energy and the effect of heat source/sink and Stefan blowing. The solution of coupled non-linear ODEs is handled by the homotopy method [45-47]. In the following sections, a mathematical model for the said problem is first developed, then in section three the analytical solution and its convergence is analysed, notable finds and results along with the comprehensive discussion is presented in section four, examined through graphs.

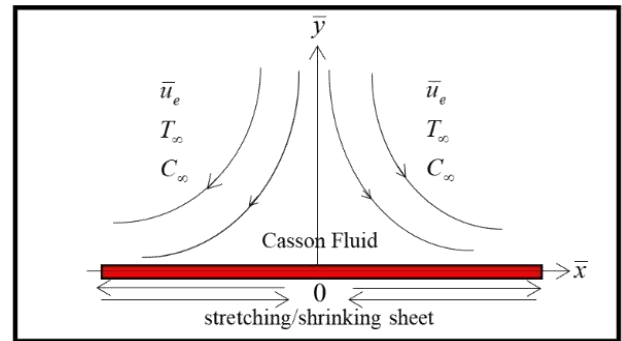
The main contributions of the paper are to:

- Expand the work of Maleque [35] to consider multiple convective and Stefan blowing boundary conditions.
- Utilize HAM with a genetic algorithm to arrive at the solutions.
- Scrutinise the impacts of different parameters on the velocity, temperature and concentration profiles of Casson fluids through graphs.
- Obtain an accurate solution from the proposed method could be a stepping stone to establishing mathematical formulations to describe the behaviour of the heat transfer and mass transport process.

## 2. MATHEMATICAL FRAME

The stagnation point flow of non-Newtonian Casson fluid with nanoparticles through a uniform magnetic field endure binary chemical reaction over a horizontal sheet stretched linearly is the matter of interest here. The essential component of a chemical reaction is the activation energy. Hence, Arrhenius activation energy, along with radiation, is also incorporated. It is assumed that fluid saturates the region

above the sheet ( $y > 0$ ), where the sheet is placed along the  $x$ -axis ( $y = 0$ ) and a uniform magnetic field is an applied parallel to the  $y$ -axis (see Figure 1). Further assumptions are that fluid conducts electricity and induced magnetic field is taken to be negligible as magnetic Reynolds number is small.



**Figure 1.** A schematic diagram of the problem (Adapted from Shehzad et al. [32])

Now, considering the temperature on the surface of the sheet and far away is  $T_f$  and  $T_\infty$  respectively. Similarly, concentrations are  $C_f$  and  $C_\infty$  respectively. The mixed convective radiative heat flow is observed along with heat source/sink. On the stretching surface, Stefan blowing effects are also included. The rheological constitutive equation for Casson fluid is [37].

$$\tau_{ij} = \begin{cases} 2 \left( \frac{P_y}{\sqrt{2\pi}} + \mu_B \right), & \pi > \pi_c \\ 2 \left( \frac{P_y}{\sqrt{2\pi_c}} + \mu_B \right), & \pi < \pi_c \end{cases} \quad (1)$$

$\pi = e_{ij}$ ,  $e_{ij}$  is the  $(i, j)$  th component of the deformation rate. The governing flow equations in the component form are [32]:

$$\frac{\partial v}{\partial y} + \frac{\partial u}{\partial x} = 0 \quad (2)$$

$$v \left( 1 + \frac{1}{\beta} \right) \frac{\partial^2 u}{\partial y^2} + u_e \frac{du_e}{dx} + \frac{\sigma B_0^2 (u_e - u)}{\rho} = u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \quad (3)$$

$$\alpha \frac{\partial^2 T}{\partial y^2} + \frac{Q_0 (T - T_\infty)}{(\rho c_p)_f} + \frac{16 \sigma_1 T_\infty^3}{3k^* (\rho c_p)_f} \frac{\partial^2 T}{\partial y^2} = u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \quad (4)$$

$$D \frac{\partial^2 C}{\partial y^2} - k_r^2 (C - C_\infty) \left( \frac{T}{T_\infty} \right)^m \exp \left( \frac{-E_a}{K^* T} \right) = u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} \quad (5)$$

The conditions at the boundary are given as [10, 43]:

$$\begin{aligned} u = u_w = bx, v = -\frac{D}{(1-C_f)} \frac{\partial C}{\partial y}, \\ -k_1 \frac{\partial T}{\partial y} = (-h_1 T + h_1 T_f), \\ -k_2 \frac{\partial C}{\partial y} = (-h_2 C + h_2 C_f) \text{ at } y = 0 \end{aligned} \quad (6)$$

$$u = u_e = cx, T = T_\infty, C = C_\infty \text{ as } y \rightarrow \infty \quad (7)$$

Considering the following the similarity variables [37]:

$$\eta = \sqrt{\frac{c}{\nu}}y, u = cx f'(\eta), v = -\sqrt{cv}f(\eta), \quad (8)$$

$$\theta(\eta) = \frac{T - T_\infty}{T_f - T_\infty}, \phi(\eta) = \frac{C - C_\infty}{C_f - C_\infty}.$$

Making use of (8), governing Eqns. (3) to (5) converted into the system of ordinary differential equations, obtained:

$$M(1 - f') + 1 + f f'' - f'^2 + \left(1 + \frac{1}{\beta}\right) f''' = 0 \quad (9)$$

$$\frac{(1+R)}{\text{Pr}} \theta'' + f \theta' + Q_c \theta = 0 \quad (10)$$

$$\frac{1}{Sc} \phi'' + f \phi' - K_E (1 + \theta \theta_w)^m \phi \exp\left(\frac{-E}{1 + \theta \theta_w}\right) = 0 \quad (11)$$

The transformed conditions at the boundary are as follows

$$f'(0) = \lambda, f(0) = s_1 \frac{1}{Sc} \phi', \theta'(0) = -Bi_1(1 - \theta(0)), \quad (12)$$

$$\phi'(0) = -Bi_2(1 - \phi(0)),$$

$$f'(\infty) = 1, \theta(\infty) = 0, \phi(\infty) = 0 \quad (13)$$

Here the  $s_1 > 0$  presents mass blowing at the sheet wall and  $s_1 < 0$ , presents the mass suction. Also, we fixed  $\text{Pr} = 21$  [48, 49], which refers to human blood. All the parameters are involved are used explained in the nomenclature section. The physical quantities of interest in given as follows: (Shehzad et al. [32])

$$C_f = \frac{1}{\rho u_w^2} \left( \mu_B + \frac{P_y}{\sqrt{2\pi}} \right) \frac{\partial u}{\partial y} \Big|_{y=0} \quad (14)$$

$$Nu_x = \frac{q_w x}{k(T_f - T_\infty)} \quad (15)$$

$$Sh_x = \frac{J_w x}{D_B(C_f - C_\infty)}, \quad (16)$$

where,  $q_w = -\left(k + \frac{16\sigma_1 T_\infty^3}{3k^*(\rho c_p)_f}\right) \frac{\partial T}{\partial y} \Big|_{y=0}$  and  $J_w = -D_B \frac{\partial C}{\partial y} \Big|_{y=0}$  are heat and mass flux, respectively. In the dimensionless form (14) - (16) can be presented as follows

$$f''(0) \left(1 + \frac{1}{\beta}\right) = C_f \text{Re}_x^{1/2} \quad (17)$$

$$-(1+R)\theta'(0) = Nu_x \text{Re}_x^{-1/2} \quad (18)$$

$$-\phi'(0) = Sh_x \text{Re}_x^{-1/2} \quad (19)$$

where,  $\text{Re}_x = \frac{u_e x}{\nu}$  signifies local Reynold number.

## 2.1 Numerical procedure and its optimisation

Considering Eqns. (9)-(11) and solving using HAM [49] the  $n$ th order deformation takes the form:

$$\left. \begin{aligned} (1-q)L_1[f(\eta, q) - f_0(\eta)] &= qh_1 N_1[f(\eta, q), \theta(\eta, q), \phi(\eta, q)], \\ (1-q)L_2[\theta(\eta, q) - \theta_0(\eta)] &= qh_2 N_2[f(\eta, q), \theta(\eta, q), \phi(\eta, q)], \\ (1-q)L_3[\phi(\eta, q) - \phi_0(\eta)] &= qh_3 N_3[f(\eta, q), \theta(\eta, q), \phi(\eta, q)]. \end{aligned} \right\} \quad (20)$$

To get an analytical solution, HAM is utilised Initial approximations  $u_0(\eta)$ ,  $\theta_0(\eta)$ ,  $\phi_0(\eta)$  such that it satisfies boundary condition. The choice of initial guess is

$$\left. \begin{aligned} f_0(\eta) &= \frac{s_1 Bi_2}{Sc(1+Bi_2)} - (1-\lambda) + x + (1-\lambda) \text{Exp}[-\eta], \\ \theta_0(\eta) &= \frac{Bi_1}{1+Bi_1} \text{Exp}[-\eta], \\ \phi_0(\eta) &= \frac{Bi_2}{1+Bi_2} \text{Exp}[-\eta]. \end{aligned} \right\} \quad (21)$$

and the supplementary linear operators  $L_1$  for velocity and  $L_2$  for temperature and concentration profiles, which are

$$\left. \begin{aligned} L_1 &= \frac{\partial^3}{\partial \eta^3} + \frac{\partial^2}{\partial \eta^2}, \\ L_2 &= \frac{\partial^2}{\partial \eta^2} - 1. \end{aligned} \right\} \quad (22)$$

The corresponding solutions for the homogenous problem should be of the form.

$$\left. \begin{aligned} f &= c_1 + c_2 \eta + c_3 e^{-\eta}, \\ \theta &= c_4 e^{-\eta} + c_5 e^{\eta}, \\ \phi &= c_6 e^{-\eta} + c_7 e^{\eta} \end{aligned} \right\} \quad (23)$$

At each iteration, constant will be evaluated using Eq. (12)-(13).

Finally, the nonlinear operators  $N_1$ ,  $N_2$  and  $N_3$  for velocity, temperature and concentration wrote according to Eq. (9) through to (11) are:

$$\left. \begin{aligned} N_1[f(y, q), \theta(y, q), \phi(y, q)] &= \left(1 + \frac{1}{\beta}\right) f'''(y, q) \\ &\quad - M(f'(y, q)) - f'(y, q)^2 + f(y, q) f''(y, q) + \chi(1+M), \\ N_2[f(y, q), \theta(y, q), \phi(y, q)] &= \frac{(1+R)}{\text{Pr}} \theta''(y, q) \\ &\quad + f(y, q) \theta'(y, q) + Q_c \theta(y, q), \\ N_3[f(y, q), \theta(y, q), \phi(y, q)] &= \frac{1}{Sc} \phi''(y, q) \\ &\quad + f(y, q) \phi'(y, q) + K_E E (1 + \theta(y, q) \theta_w)^{m-1} \phi(y, q). \end{aligned} \right\} \quad (24)$$

Defining the following expansion

$$\left. \begin{aligned} f(y, q) &= f_0(y) + \sum_{k=1}^n q^k f_k(y) \\ \theta(y, q) &= \theta_0(y) + \sum_{k=1}^n q^k \theta_k(y) \\ \phi(y, q) &= \phi_0(y) + \sum_{k=1}^n q^k \phi_k(y) \end{aligned} \right\} \quad (25)$$

Utilising the expensing arrangement characterised in term of  $(f(y, q), \theta(y, q)$  and  $\phi(y, q)$ ) as referenced in Eq. (25) into the Eq. (20). We get an arrangement of direct differential equations with their significant limit conditions. The solution deforms from initial guesses to approximate value when  $q$  changes continuously from 0 to 1. Here  $h_1, h_2$  and  $h_3$  are convergence control parameters whose values are optimised to get the minimum “Residual Error” using a genetic algorithm. A flow chart is drawn below, showing the procedure followed in the optimisation process.

### 2.2 Genetic algorithm

The theory of inheritance and evolution of living organisms explains the evolution and survival of the fittest organism, not the strongest. Based on this theory, an optimisation technique evolves known as “Genetic algorithm (GA)”. It assumes some approximate values for the requested parameter (in this case convergence control parameter). These values called chromosomes first combined (crossover) to generate new daughter chromosomes. After the crossover process, some of its values are changed to initiate mutation. The so formed daughter chromosomes and parent chromosomes are tested for best fitness values. The process will be repeated until an optimum value is achieved (See Figure 2). Optimisation Tool GUI in Matlab is employed to find the convergence control parameters of HAM. The flow chart is drawn to explain the current method.



Figure 2. Flow chart of genetic algorithm

### 3. RESULT AND DISCUSSION

In this section, we investigated the behaviour of Casson fluid parameter  $\beta$ , chemical reaction parameter  $K_E$ , constant of

temperature difference  $\theta_w$ , Stefan’s blowing coefficient  $s_1$  and activation energy  $E$  on  $f'(\eta)$ ,  $\theta(\eta)$  and  $\phi(\eta)$ . Also,  $C_f Re_x^{1/2}$  (skin friction),  $Nu_x Re_x^{-1/2}$  (Nusselt Number),  $Sh_x Re_x^{-1/2}$  (Sherwood number) are plotted to emulate the variation in the flow. The following discussion and results are obtained by using appropriate values of emerging parameters:  $M=Sc=0.2, Bi_1, Bi_2, Q_c=0.2, R=0.2, s_1, \lambda=1, Sc=0.7, \theta_w=7, E=1, K_E=1$  and  $\beta=1$ .

With the rise of  $\beta$  the overall viscosity decline and as  $\beta$  approaches infinity, the non-Newtonian behaviour tends to disappear, which lead to enhancement of the flow velocity as  $\beta$  increases. Similar to the temperature profiles, with the increase of  $\beta$  (Figure 3) the However, concentration decrease due to a reduction in viscosity and consequently, the reduction is resistances. Figure 4 shows variation observed in  $f'(\eta)$ ,  $\theta(\eta)$  and  $\phi(\eta)$  when a slight variation in chemical reaction parameter  $K_E$  is observed.

It is detected that the velocity of the fluid rises with growth in values of  $K_E$ . It is also realized that for generative reaction, i.e.,  $K_E < 0$  fluid flow enhances. Whereas, in destructive reaction  $K_E > 0$ , drop in the fluid flow is observed. Moreover, the temperature of nanofluid and volume fraction concentration tends to decrease as  $K_E$  shows an increasing trend, which is due to the weak effect of buoyancy force concentration gradient. Figure 5 elucidates the increasing behaviour in the concentration of nanofluid when activation energy  $E$  is increased.

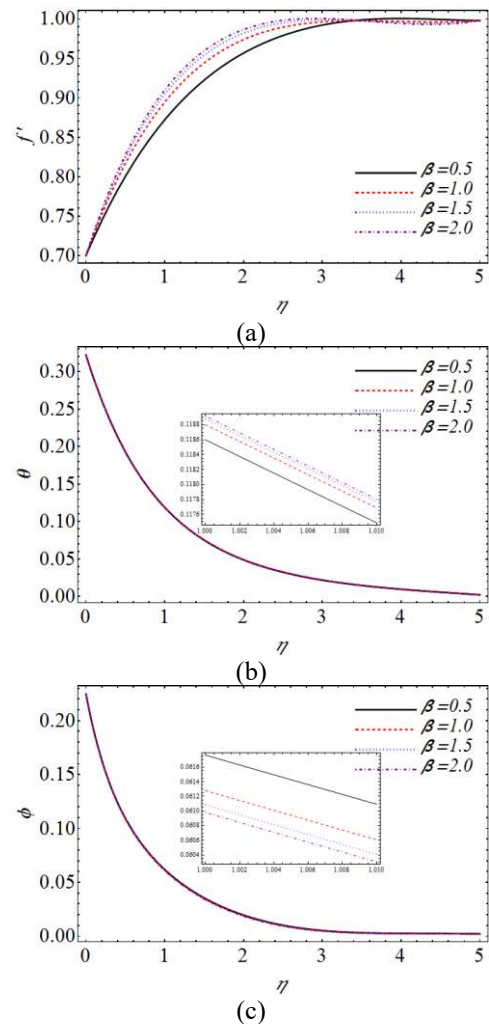
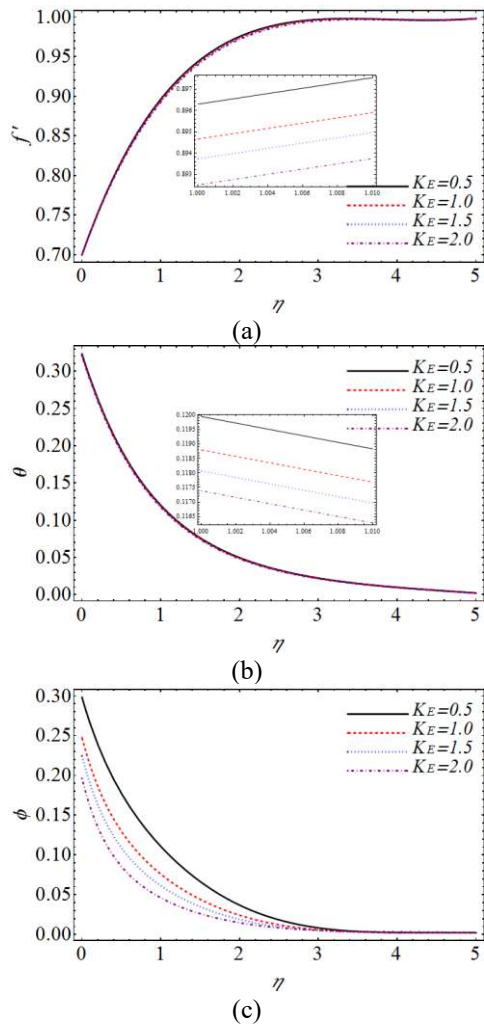


Figure 3. Effect of the Casson fluid parameter on a) velocity b) temperature c) concentration



**Figure 4.** Effect of the chemical reaction on a) velocity b) temperature c) concentration

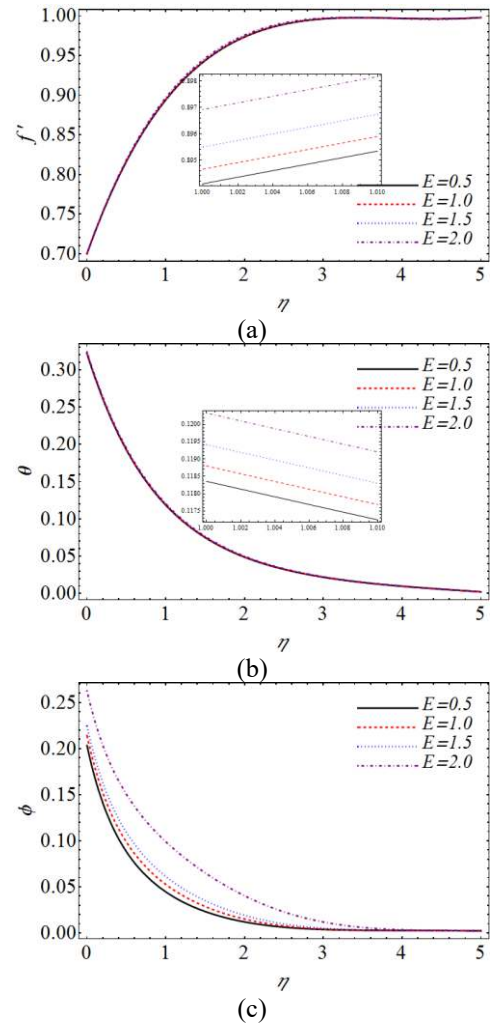
Physically, due to the higher activation energy, it takes the greater temperature to start a chemical reaction hence at a lower temperature, the reaction rate is less, consequently, reduce the chemical reaction. Increasing value  $E$  also tends to reduce velocity and temperature.

Figure 6 demonstrate the impact of Stefan mass blowing or suction coefficient  $s_1$ . Here, it is found that velocity for larger values of  $s_1$  reduces far away from the wall, while its boosts up in the neighborhood of walls as mass flow boosted the velocity. For temperature profile, it is apparent that the thermal performance reduces as the system is cooled in case of suction, so boundary layer thickness shrinkages. It is consequently blowing effects by raising the temperature. For concentration profile, Figure reflects that concentration function increased with the increase of  $s_1$ . The effects of  $\beta$  and Stefan blowing parameter  $s_1$  on  $C_f Re_x^{1/2}$  are shown in Figure 7.

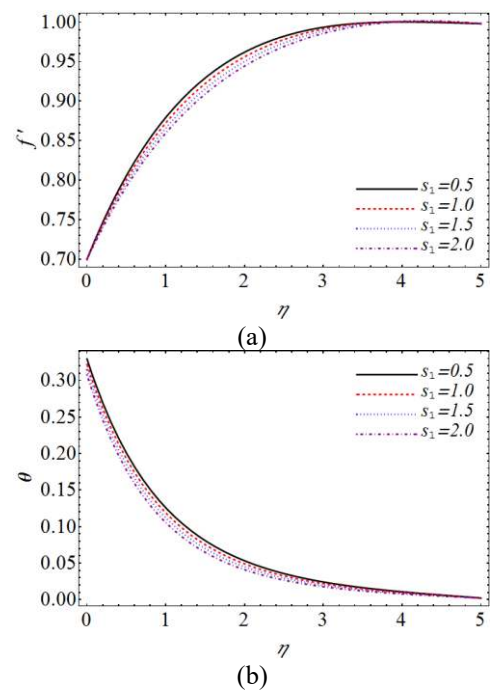
It is noted from said figure that the Stefan parameter and Casson fluid parameters have the same proportional to each other but opposite trend measure for skin friction. In results as the Casson and Stefan parameter increased, then the skin friction on the surface of geometry decreases. Figure 8 depicts the influences of temperature difference parameter  $\theta_w$  and activation energy  $E$  on  $C_f Re_x^{1/2}$ .

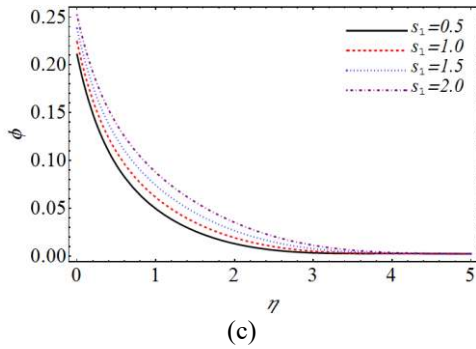
$C_f Re_x^{1/2}$  is increasing with the increase of activation energy parameter but reverse behaviour for the temperature difference parameter is noted for skin friction. In Figures 9 and

10 show the effects of Casson fluid, Stefan blowing, temperature difference and activation energy parameters on Nusselt number.

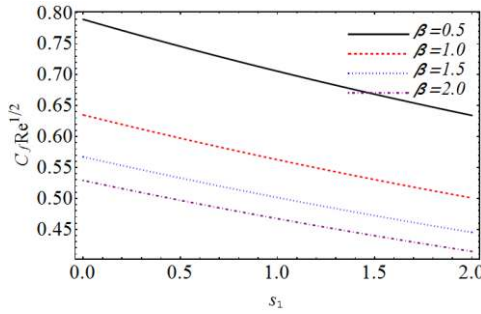


**Figure 5.** Effect of the activation energy on a) velocity b) temperature c) concentration

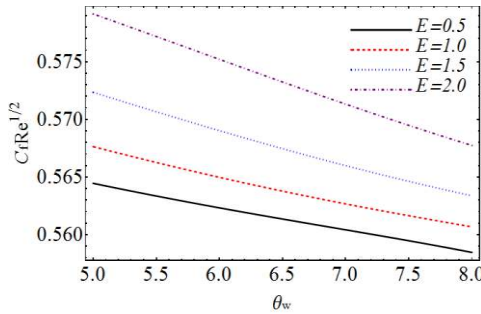




**Figure 6.** Effect of the Stefan mass blowing on a) velocity b) temperature c) concentration

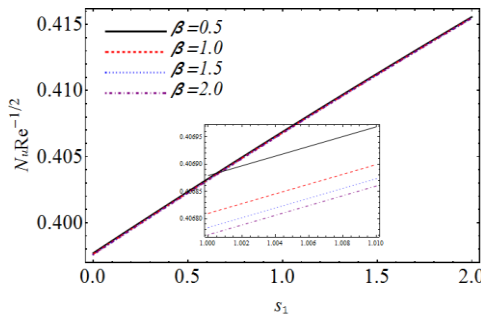


**Figure 7.** Effect of Casson fluid and Stefan parameters on the skin friction coefficient

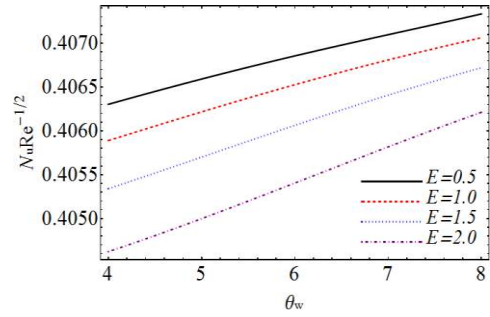


**Figure 8.** Effect of temperature difference and Activation Energy on the skin friction coefficient

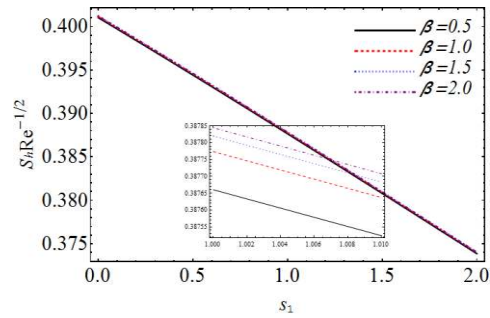
In both Figures 9-10,  $Nu_x Re_x^{-1/2}$  is growing up with the large values of Stefan blowing and temperature difference parameters but the drop in heat transfer is observed for large values of Casson fluid and activation energy parameters. Figure 11 scrutinizes the  $Sh_x Re_x^{-1/2}$  versus Stefan blowing parameter  $s_1$  for different values of Casson fluid parameter  $\beta$ .



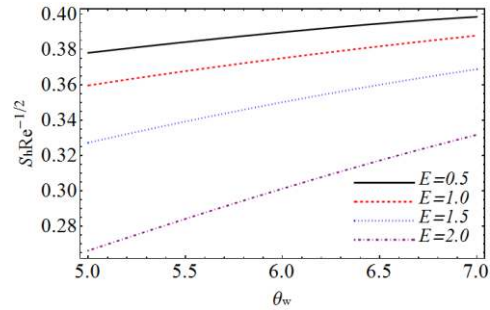
**Figure 9.** Effect of Casson fluid and Stefan parameters on the Nusselt number



**Figure 10.** Effect of temperature difference and Activation Energy on the Nusselt number



**Figure 11.** Effect of Casson fluid and Stefan parameters on the Sherwood number



**Figure 12.** Effect of temperature difference and Activation Energy on the Sherwood number

The  $Sh_x Re_x^{-1/2}$  expressively rises with growth in Casson fluid parameter  $\beta$ . However, there is an exponential decay in  $Sh_x Re_x^{-1/2}$  when Stefan blowing is amplified. Figure 12 shows the effect of temperature difference parameter  $\theta_w$  on the  $Sh_x Re_x^{-1/2}$  for variation of activation energy  $E$ . This figure exposes that wall mass flux has a reverse trend with  $\theta_w$  and  $E$ .

#### 4. CONCLUSIONS

The following conclusions can be drawn from the present exploration:

- Velocity decays for larger chemical reaction and Stefan blowing parameter while the reverse trend is noticed for the higher Casson fluid parameter, and activation energy.
- Concentration decreases as the Casson fluid parameter and chemical reaction are increased while the opposite behaviour is perceived for higher Stefan blowing and activation energy.

- Temperature profile increases for larger Casson fluid parameter and activation energy, but the contradictory trend is observed for higher chemical reaction and Stefan blowing parameter.
- As in Table 1, surface drag force reduces for higher Casson fluid parameter and activation energy while the reverse behaviour is observed for higher temperature difference and Stefan blowing parameter. The reduced Nusselt number is directly proportional to the activation energy and inversely proportional to the temperature difference, Casson fluid parameter and Stefan blowing parameter. The reduced Sherwood number is inversely proportional to the temperature difference parameter, and an align increment to the

activation energy, Casson fluid parameter and Stefan blowing parameter.

- As in Figures 7-12, the reduced Nusselt number towards temperature difference, Stefan blowing parameter are the highest, while the Casson fluid parameter and activation energy are at the minimal. Also, the reduced Sherwood number decreases toward the Stefan blowing and activation energy while reverse behaviour is noticed for higher temperature difference and Casson fluid parameter. The surface drag force is directly proportional to the activation energy and inversely proportional to the temperature difference, Casson fluid parameter and Stefan blowing parameter.

**Table 1.** Values  $(1 + \frac{1}{\beta})f''(0)$ ,  $-(1 + R)\theta'(0)$ ,  $-\phi'(0)$  as the governing parameters vary

Activation energy, $E$	Temperature difference, $\theta_w$	Casson parameter, $\beta$	Stefan blowing, $s_1$	$(1 + \frac{1}{\beta})f''(0)$	$-(1 + R)\theta'(0)$	$-\phi'(0)$
0.5	0.5	1	0.75	0.576297	0.675464	0.298973
0.75				0.575685	0.67557	0.303952
1				0.57505	0.675681	0.308992
	0.75			0.576965	0.67535	0.29305
	1			0.579098	0.674986	0.273698
		5		0.411362	0.674156	0.387892
		10		0.3855	0.674142	0.391307
			0.5	0.397798	0.670338	0.394673
			0.0	0.423833	0.662577	0.401282

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