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# Development of a New Strategy for Production of Medium-Chain-Length Polyhydroxyalkanoates by Recombinant *Escherichia coli* via Inexpensive Non-Fatty Acid Feedstocks

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*Pseudomonas putida* KT2440 is capable of producing medium-chain-length polyhydroxyalkanoates (MCL-PHAs) when grown on unrelated carbon sources during nutrient limitation. Transcription levels of genes putatively involved in PHA biosynthesis were assessed by quantitative real-time PCR (qRT-PCR) in *P. putida* grown on glycerol as a sole carbon source. The results showed that two genes, *phaG* and the PP0763 gene, were highly upregulated among genes potentially involved in the biosynthesis of MCL-PHAs from unrelated carbon sources. Previous studies have described *phaG* as a 3-hydroxyacyl-acyl carrier protein (ACP)-coenzyme A (CoA) transferase, and based on homology, the PP0763 gene was predicted to encode a medium-chain-fatty-acid CoA ligase. High expression levels of these genes during PHA production in *P. putida* led to the hypothesis that these two genes are involved in PHA biosynthesis from non-fatty acid carbon sources, such as glucose and glycerol. The *phaG<sub>pp</sub>* and PP0763 genes from *P. putida* were cloned and coexpressed with the engineered *Pseudomonas* sp. 61-3 PHA synthase gene *phaCl* (STQK)<sub>ps</sub> in recombinant *Escherichia coli*. Up to 400 mg liter<sup>-1</sup> MCL-PHAs was successfully produced from glucose. This study has produced the largest amount of MCL-PHAs reported from non-fatty acid carbon sources in recombinant *E. coli* to date and opens up the possibility of using inexpensive feedstocks to produce MCL-PHA polymers.

Polyhydroxyalkanoates (PHAs) are carbon and energy storage materials synthesized by a variety of bacteria when grown under nutrient limitation in the presence of excess carbon (10, 11). These polymers have attracted extensive interest as environmentally friendly, biodegradable alternatives to petroleum-based plastics. Unlike petroleum-based plastics, PHAs can be obtained from renewable resources and are completely degraded to CO<sub>2</sub> and H<sub>2</sub>O (25). PHAs are generally grouped into three categories: short-chain-length PHAs (SCL-PHAs) that contain repeating units of 3 to 5 carbon atoms, medium-chain-length PHAs (MCL-PHAs) that contain repeating units of 6 to 14 carbon atoms, and SCL-co-MCL PHAs, which consist of both SCL and MCL repeating units. MCL-PHAs show promise as thermoelastomers and are attractive for biomedical applications, such as drug delivery (16) and tissue engineering (28).

*Pseudomonas* strains are known to produce large amounts of MCL-PHAs (23). The genome of *Pseudomonas putida* KT2440 is fully sequenced, and several genes involved with PHA synthesis have been identified (1, 14). Two PHA synthase genes, *phaC1* and *phaC2*, which are separated by the PHA depolymerase gene *phaZ*, are characterized as class II PHA synthases (3, 17). These synthases generally prefer 3-hydroxyacyl-coenzyme A (CoA) with chain lengths of 6 to 14 carbon atoms as substrates to produce MCL-PHA polymers (20). As shown in Fig. 1, precursors for PHA synthesis are thought to be derived from fatty acid biosynthesis when the microorganism is grown on unrelated carbon sources, such as glucose and glycerol, and  $\beta$ -oxidation when the microorganism is grown on related carbon sources, such as fatty acids (5, 11). The (*R*)-specific enoyl-CoA hydratase PhaJ is an enzyme that could potentially provide 3-hydroxyacyl-CoA precursors for PHA synthesis derived via the fatty acid  $\beta$ -oxidation pathway when the organism is grown on fatty acids (Fig. 1D) (4). For PHA production from unrelated carbon sources, an enzyme encoded by *phaG* was identified to be a key link between fatty acid biosynthesis and

MCL-PHA biosynthesis (18). PhaG was first reported as a 3-hydroxyacyl-acyl carrier protein (ACP)-CoA transferase and was thought to transfer the 3-hydroxyacyl group from the ACP moiety to the CoA moiety (18). However, our results suggest that PhaG functions as a 3-hydroxyacyl-ACP thioesterase to produce 3-hydroxy fatty acids. Therefore, at least one 3-hydroxyacyl-CoA ligase is hypothesized to be necessary to provide the PHA precursor (*R*)-3-hydroxyacyl-CoA (11), as shown in Fig. 1B. It has been previously shown that the AlkK enzyme from *Pseudomonas oleovorans* has 3-hydroxyacyl-CoA ligase activity and can catalyze conversion of 3-hydroxyalkanoate substrates into 3-hydroxyalkanoate-CoA thioester PHA precursors *in vitro* (21). Therefore, several *P. putida* KT2440 genes encoding proteins with homology to AlkK from *P. oleovorans* (AlkK<sub>po</sub>) were investigated in this study to find candidates for the 3-hydroxyacyl-CoA ligase putatively involved in PHA biosynthesis.

In this study, transcription levels of genes putatively involved in PHA synthesis and genes encoding putative proteins homologous to AlkK<sub>po</sub> were monitored by quantitative real-time PCR (qRT-PCR). Hypothetical MCL-PHA biosynthesis pathways were proposed by comparing the differences in gene transcription. A putative medium-chain-fatty-acid ligase gene (the PP0763 gene) displayed upregulated transcription levels when cells were grown under PHA-producing conditions. This gene was cloned and coexpressed with *phaG* from *P. putida* (*phaG<sub>pp</sub>*) and the PHA syn-

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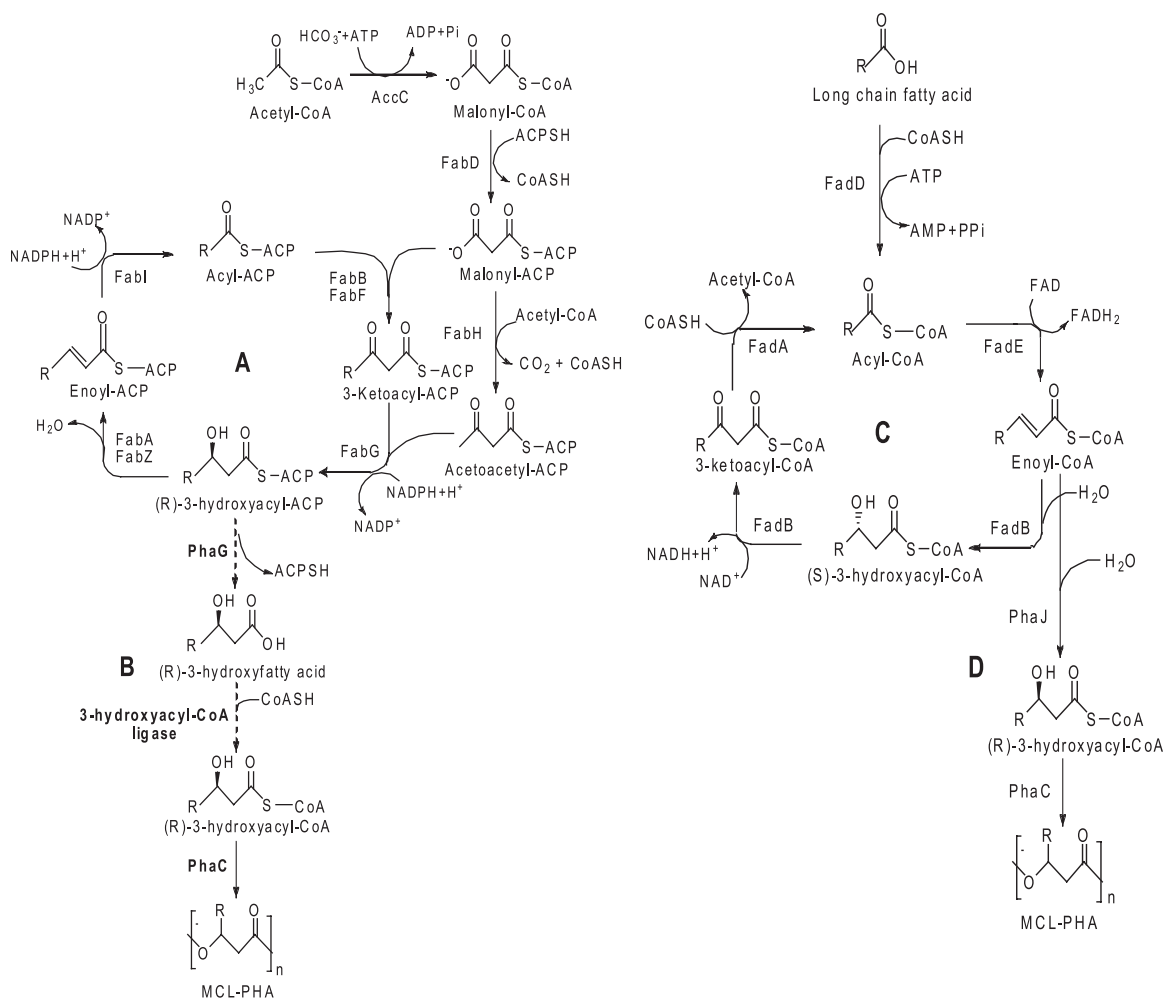


FIG 1 Proposed metabolic pathways for PHA biosynthesis. (A) Fatty acid biosynthesis; (B) PHA biosynthesis via fatty acid biosynthesis; (C)  $\beta$ -oxidation; (D) PHA biosynthesis via  $\beta$ -oxidation.

these gene *phaC1*(STQK)<sub>ps</sub> in recombinant *Escherichia coli*. PhaC1(STQK) is an engineered PHA synthase originally derived from *Pseudomonas* sp. 61-3 that has two point mutations and has previously been shown to have increased activity toward 3-hydroxydecanoate (3HD)-CoA substrates in an *in vitro* assay (24). By coexpressing these genes, the production of MCL-PHAs in recombinant *E. coli* from non-fatty acid carbon sources was about 4-fold higher than that in *P. putida* KT2440. The results of this study have identified a new PHA biosynthesis pathway with the highest production of MCL-PHAs achieved to date in recombinant *E. coli* from inexpensive non-fatty acid carbon sources such as glucose and glycerol.

## MATERIALS AND METHODS

**Bacterial strains and cultivation conditions.** *P. putida* KT2440 was grown in 100-ml batches of a defined mineral salt (MS) medium (7) with high nitrogen (high N) (7.2 g liter<sup>-1</sup>) or low nitrogen (low N) (0.072 g liter<sup>-1</sup>) and glycerol as the carbon source at 20 mM. Growth was monitored by measuring the optical densities at 540 nm (OD<sub>540</sub>) at 0 h, 4 h, 8 h, 12 h, 24 h, and 48 h. *E. coli* JM109 was used as a host for plasmid construction and was grown on Luria-Bertani (LB) medium. When necessary, ampicillin (100  $\mu$ g ml<sup>-1</sup>) and/or kanamycin (50  $\mu$ g ml<sup>-1</sup>) were added to the medium. For PHA production, recombinant *E. coli* BL21(DE3) and *E.*

*coli* LS5218 strains were grown on LB medium with ampicillin (100  $\mu$ g ml<sup>-1</sup>) and kanamycin (50  $\mu$ g ml<sup>-1</sup>). IPTG (isopropyl- $\beta$ -D-thiogalactopyranoside) was added to a final concentration of 1 mM at 5 h when the OD<sub>540</sub> was  $\sim$ 1.0, and 20 g liter<sup>-1</sup> glucose was added at 8 h when the OD<sub>540</sub> was  $\sim$ 2.0. For measuring 3-hydroxy fatty acids in the medium, recombinant *E. coli* LS5218 cells were grown on high N MS medium with 20 g liter<sup>-1</sup> glycerol as the sole carbon source. All the experiments were performed in triplicate, and data are presented as the average  $\pm$  the standard deviation for each sample point.

**Determination of gene transcription levels by qRT-PCR.** qRT-PCR was performed in a manner similar to that previously described (27). Briefly, a total volume of 500  $\mu$ l of *P. putida* KT2440 cell culture was harvested from MS medium when the OD<sub>540</sub> reached 1.0. RNAs were stabilized using RNaprotect bacteria reagent (Qiagen, Valencia, CA). The total RNA was isolated using the RNeasy minikit (Qiagen, Valencia, CA). Prior to reverse transcription, the trace DNA remaining in RNA samples was removed by digestion with RQ1 RNase-free DNase (Promega, Madison, WI). The cDNA libraries were synthesized with a SuperScript VILO cDNA synthesis kit (Invitrogen, Carlsbad, CA). Total RNA (1  $\mu$ g) was added to the reaction mixture as the template for each sample. All procedures using kits were performed according to the manufacturer's instructions. The qRT-PCRs were performed using the iQ SYBR green supermix kit with the iQ5 multicolor real-time PCR detection system (Bio-Rad, Hercules, CA). The primers used in qRT-PCR are listed in Table 2. The

TABLE 1 Plasmids and bacterial strains used in this study

Plasmid or strain	Relevant characteristics	Source or reference
<b>Plasmids</b>		
pCR-Blunt II-TOPO	TA cloning vector, Km <sup>r</sup>	Invitrogen
pBBRSTQK	pBBR1-MCS2 derivative, <i>Pseudomonas</i> sp. 61-3 <i>phaC1</i> (STQK)	15
pTOPOG	pCR-Blunt II-TOPO derivative, <i>P. putida</i> KT2440 <i>phaG</i>	This study
pTOPOK	pCR-Blunt II-TOPO derivative, <i>P. putida</i> KT2440 PP0763	This study
pTrc99A	Expression vector, Amp <sup>r</sup> P <sub>trc</sub> <i>rrnB</i> ori (pBR322) <i>lacI</i> <sup>q</sup>	Amersham
pTrcG	pTrc99A derivative, <i>P. putida</i> KT2440 <i>phaG</i>	This study
pTrcK	pTrc99A derivative, <i>P. putida</i> KT2440 PP0763	This study
pTrcGK	pTrc99A derivative, <i>P. putida</i> KT2440 <i>phaG</i> PP0736	This study
<b>Strains</b>		
<i>P. putida</i> KT2440	Wild type	
<i>E. coli</i> JM109	<i>recA1 endA1 gyrA96 thi-1 hsdR17</i> (r <sub>K</sub> <sup>-</sup> m <sub>K</sub> <sup>+</sup> ) <i>supE44 relA1 lac</i> [F' <i>proAB lacI</i> <sup>q</sup> $\Delta$ DM15]	Takara
<i>E. coli</i> BL21(DE3)	F <sup>-</sup> <i>ompT hsdS<sub>B</sub></i> (r <sub>B</sub> <sup>-</sup> m <sub>B</sub> <sup>-</sup> ) <i>gal dcm</i> (DE3)	9
<i>E. coli</i> LS5218	<i>fadR601 atoC2</i> (con)	6
<i>E. coli</i> LS11	<i>E. coli</i> LS5218 derivative, $\Delta$ <i>fadE</i>	This study

gene expression levels were assessed by comparing the ratios of the house-keeping gene *rpoD* threshold cycle ( $C_T$ ) values to target gene  $C_T$  values using the following equation: ratio of *rpoD*/target =  $2^{C_T(\text{rpoD}) - C_T(\text{target})}$ .

The *n*-fold induction was determined by the expression levels of genes of cells grown on low N MS medium versus those of cells grown on high N MS medium.

**Plasmid construction.** The putative 3-hydroxyacyl-ACP thioesterase gene *phaG* was amplified by PCR from *Pseudomonas putida* KT2440 genomic DNA using the primers F\_KpnI and R\_XbaI (see Table 2). The putative medium-chain-fatty-acid CoA ligase gene (the PP0763 gene) was also amplified by PCR from *P. putida* KT2440 genomic DNA using the primers F\_SacI and R\_KpnI (see Table 2). The *phaG* and PP0763 PCR products were cloned into the vector pCR-Blunt II-TOPO (Invitrogen, Carlsbad, CA) to produce pTOPOG and pTOPOK. The orientation and overall correctness were confirmed by restriction digest and DNA sequencing. The 1-kb fragment including *phaG* was removed by restriction digest with KpnI and XbaI from pTOPOG and subcloned into pTrc99A to construct the plasmid pTrcG. The 1.7-kb fragment including the PP0763 gene was removed by restriction digest with SacI and KpnI from pTOPOK, and the fragment was subcloned into the plasmids pTrc99A and pTrcG, generating the constructs pTrcK and pTrcKG, respectively. The plasmids pTrcG, pTrcK, and pTrcKG were cotransferred with pBBRSTQK (15) into *E. coli* BL21(DE3) and *E. coli* LS5218 (Table 1). The gene PP2795 from *P. putida* KT2440 was also amplified and inserted into pTrcG to generate the plasmid pTrc2795G using the same strategy as described above and cotransferred with pBBRSTQK into *E. coli* BL21(DE3).

**Gene knockouts in *E. coli* LS5218.** The method for chromosomal gene inactivation in *E. coli* developed by Datsenko and Wanner (2) was used to inactivate the *fadE* gene in *E. coli* LS5218. The kanamycin-resistant cassette from the plasmid pKD13 was amplified by the primers (Table 2) containing 50-bp regions homologous to the *fadE* gene. The PCR product was transformed via electroporation into *E. coli* LS5218 that had expressed the  $\lambda$ -Red system from the pKD46 plasmid. Transformants were selected on LB agar plates with 50  $\mu$ g ml<sup>-1</sup> kanamycin. Complete elimination of the gene from the chromosome was confirmed by PCR with *fadE* check primers (Table 2). The pKD46 plasmid was removed by growth at 37°C. After *fadE* was disrupted, the kanamycin-resistant cassette was removed by expression of FLP recombinase from the pCP20 plasmid. The pCP20 plasmid was removed by growth at 37°C. The *fadE* mutant strain *E. coli* LS11 was confirmed by failure to grow on fatty acids as the sole carbon source.

**Analytical procedures.** For measuring glycerol concentrations in the supernatant, free glycerol reagent (Sigma, St. Louis, MO) was used ac-

ording to the manufacturer's instructions. Briefly, 10  $\mu$ l of NANOpure water (blank), glycerol standard (2.5 mg ml<sup>-1</sup>), or supernatant from medium was mixed with 0.8 ml of the free glycerol reagent and incubated for 5 min at 37°C. The absorbance (*A*) was measured at 540 nm. The glycerol concentration in supernatant was calculated by the following equation: glycerol content = ( $A_{\text{supernatant}} - A_{\text{blank}}$ )/( $A_{\text{standard}} - A_{\text{blank}}$ )  $\times$  2.5 mg ml<sup>-1</sup>.

For analysis of polymer production and composition, liquid cultures (100 ml) were centrifuged at 5,000  $\times$  *g* for 15 min at 4°C, washed with 15 ml NANOpure water, and lyophilized for a minimum of 24 h, and ~15 mg dry cells per sample was treated with 2 ml of methanol-sulfuric acid (85:15) solution and 2 ml chloroform at 100°C for 140 min and assayed using a GC 2010 gas chromatograph (Shimadzu Scientific Instruments, Inc., Marlborough, MA) (7). Cell materials for extraction and purification of PHA polymer were prepared and lyophilized as described above. The lyophilized cells were added to 100 ml chloroform and were shaken at 60°C, 100 rpm overnight, to extract polymer produced in the cells. The chloroform-polymer solution was vacuum filtered through Whatman filter paper 1, and polymers were precipitated by pouring the filtrate into a 10 $\times$  volume of methanol. Precipitates were separated from the liquid by centrifugation at 5,000  $\times$  *g* for 15 min. The supernatant was poured off, and the pellet containing the polymers was allowed to dry at room temperature. Once dry, the polymers were dissolved again in chloroform, and the solution was cast in a glass petri dish. The chloroform was removed by evaporation at room temperature for 48 h. The purified polymers were analyzed by <sup>1</sup>H nuclear magnetic resonance (NMR) spectroscopy and <sup>13</sup>C NMR using a Bruker BioSpin AVANCE 600 (Bruker BioSpin Corp., Billerica, MA) operating at 600 MHz (31). For analyzing extracellular 3-hydroxy fatty acids, 10 ml supernatant of each sample was lyophilized for at least 24 h, and the lyophilized materials were subjected to methanolysis and assayed by GC (7).

## RESULTS AND DISCUSSION

**Growth of *P. putida* KT2440 on low-nitrogen or high-nitrogen MS medium.** The OD<sub>540</sub> of *P. putida* KT2440 grown on either high-nitrogen (high N) or low-nitrogen (low N) MS medium was measured at different time points (Fig. 2). The doubling time of cells grown on high-nitrogen MS medium (2.5 h) was considerably shorter than that of cells grown on low-nitrogen MS medium (3.4 h) during the exponential phase (from 0 h to 16 h). However, the cells grown on high N MS medium stopped growing after 24 h, while the cells grown on low N medium grew until 48 h. The concentration of glycerol in the supernatant of high N MS me-

TABLE 2 Primers used in this study

Primers	Sequence(s) <sup>a</sup>
Primers used in qRT-PCR	
<i>phaC1</i>	F, 5'-CAGGTTGCTTTGTTTGTGTC-3'; R, 5'-TTGTTTACCCAGTAGTTCC-3'
<i>phaZ</i>	F, 5'-AGTTTGCTCACGATTAC-3'; R, 5'-CACCTGGGCTTGC-3'
<i>phaC2</i>	F, 5'-ATGAGCAGACCATCG-3'; R, 5'-GTTTACCCAGTAGTTCC-3'
<i>phaG</i>	F, 5'-TTCAAACGCTTCAAC-3'; R, 5'-CGGTCTTGTCTCC-3
<i>phaJ</i>	F, 5'-TGTCCCAGGTCAC-3'; R, 5'-GGAACATGCTCTTG-3'
<i>phaJ3</i>	F, 5'-CCGAGGCTGAAGATGGTATC-3'; R, 5'-ACGGCACTGAGATGGATAGG-3'
<i>phaJ4</i>	F, 5'-ATGGTTTCTGACCTTGTGCG-3'; R, 5'-AAAACAGAGCGACAGCGACT-3'
PP0763	F, 5'-CCAAGGGCGTGTATTCAGT-3'; R, 5'-CCTGGGTACACCTGCTTCAT-3'
PP3553	F, 5'-ACACGGTGTGAAGGGCTAC-3'; R, 5'-CTGGCTTTAAGGCAACGAAG-3'
PP2795	F, 5'-GAAAGGCTACCTGCACAACC-3'; R, 5'-ATTCCACATAGCCGTCCAG-3'
PP3458	F, 5'-CCGAAGTGCAGATTGCCTAT-3'; R, 5'-GCTTTGGGGTGTTCAGTA-3'
PP2038	F, 5'-CTGACCGAACAGGACCATT-3'; R, 5'-AGTAGCCCTGCATGATGTCC-3'
PP4063	F, 5'-GCCACGCTCAGTCACTACAA-3'; R, 5'-GAAAGCATCGTTGGGGTAGA-3'
PP4549	F, 5'-ACGTATACCCCAACGAGCTG-3'; R, 5'-CGGTACCTTGTAGCCGGTAA-3'
PP4550	F, 5'-GCAGAAGGCTGGTTCAAGAC-3'; R, 5'-GGGTACTTTGTAGCCGGTGA-3'
PP4487	F, 5'-GAGCACCGCAACATCACTTA-3'; R, 5'-ACCACCTTGGATTTGCAGTC-3'
PP2213	F, 5'-GATCAAGGCGTTCGTGGTAT-3'; R, 5'-ATTCGATTTCCCTGGGGTAG-3'
PP2351	F, 5'-ACCACGGTGTCTACGAAGG-3'; R, 5'-AGCGAGCTGAGGTCATGTTT-3'
PP4702	F, 5'-CGGATGGTCGACACCTACTT-3'; R, 5'-CCAGTGCACCTTCCACTTCA-3'
PP3071	F, 5'-CCGTTACCACGATGCCTACT-3'; R, 5'-CCACAACCTGTTTCGACCTTT-3'
PP2709	F, 5'-CGCTTGTGTGCAGCTCTATC-3'; R, 5'-ATCAGGCTCTGAGCACCCT-3'
Primers used for plasmid construction and knockout mutant	
<i>phaG</i> F_KpnI	5'- <b>GGTACCGGCAAATGCCTACCTGTCAT</b> -3'
<i>phaG</i> R_XbaI	5'- <b>TCTAGACTGCGGGTAT TGGCTACAAG</b> -3'
PP0763 F_SacI	5'- <b>GAGCTCTTTT</b> CAGAAAAGGGATCCCC-3'
PP0763 R_KpnI	5'- <b>GGTACCTTACAACGTGGAAGGAACG</b> -3'
$\Delta$ <i>fadE</i> forward	5'-CTCGCGTGTGCAAAAACCTC <b>TC</b> CGGGCGTGAGCGGGATCTGGCGATTACCGTGTAGGCTGGAGCTGCTTC-3'
$\Delta$ <i>fadE</i> reverse	5'-CGTTGACGTCATTGTTCT <b>TC</b> CGCCGCTCCATCTCTCCAGCACGTACCGAATCCCGGGATCCGTCGACC-3'
<i>fadE</i> Check	F, 5'-GGAGTTGTGGCGTACCTTA-3'; R, 5'-AGCCTGATACAGCGCATCTT-3'

<sup>a</sup> F, forward; R, reverse. Underlining indicates 50-bp regions homologous to the *fadE* gene; restriction sites are indicated in bold.

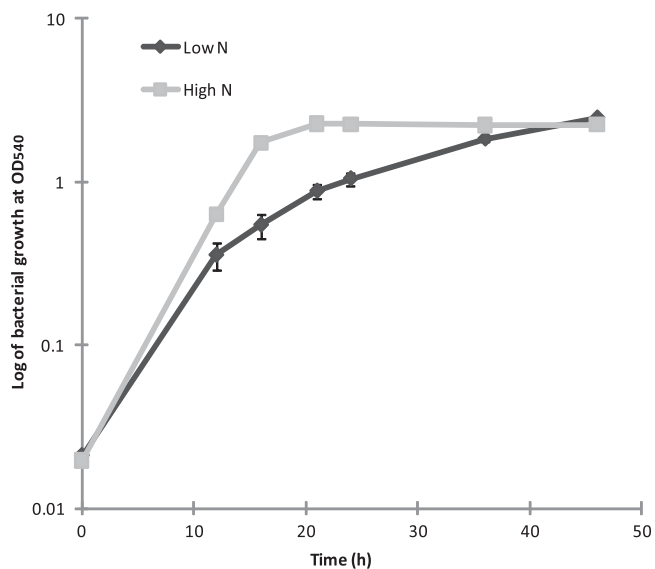


FIG 2 Differences in growth rates of *P. putida* KT2440 grown on mineral salt (MS) medium with different nitrogen concentrations. Growth curves of *P. putida* KT2440 grown on MS medium with either high N (0.072 g liter<sup>-1</sup>), represented by squares, or low N (0.072 g liter<sup>-1</sup>), represented by diamonds. Points represent the average absorbance of three independent data points (OD<sub>540</sub>) ± standard deviation.

dium dropped from 20 mM to zero at 48 h, but the concentration of glycerol in low N MS medium decreased from 20 mM to 3 mM. Therefore, depletion of the carbon source was the main reason that the cells stopped growing in high N MS medium.

**Transcription levels of genes involved in PHA synthesis in cells grown on low N MS medium versus cells grown on high N MS medium.** In order to determine the best conditions for sampling cells to determine the expression levels of genes potentially involved in PHA biosynthesis from non-fatty acid carbon feedstocks, *P. putida* was grown in two sets of media with different nitrogen (N) concentrations to induce PHA production and get RNA for qRT-PCR analysis. The PHA production of *P. putida* KT2440 on low N medium was 71-fold higher than that on high N medium (Table 3). In order to identify genes upregulated in cells grown under PHA-producing conditions, candidate gene transcription levels for cells grown on low N medium versus transcription levels of cells grown on high N medium were assayed by qRT-PCR as described in Materials and Methods. Specifically, the transcription levels of genes involved in PHA synthesis, which were homologous to genes known in other *Pseudomonas* species to be involved in PHA production, and homologs of the *alkK* gene from *P. oleovorans* that encodes an acyl-CoA ligase (26) were investigated. The transcription of the *rpoD* gene encoding the housekeeping sigma70 factor was used as the housekeeping gene

TABLE 3 PHA production in the *P. putida* KT2440 strain on MS medium with high N or low N<sup>a</sup>

Culture <sup>b</sup>	CDW (g liter <sup>-1</sup> )	PHA produced (mg liter <sup>-1</sup> )	% PHA	Composition (mol%)			
				3HHx	3HO	3HD	3HDD
High N	0.6 ± 0.04	2.0 ± 0.1	0.4 ± 0.02	ND	ND	56.8 ± 4.4	44.2 ± 4.4
Low N	0.4 ± 0.08	109 ± 21	28.4 ± 1.0	2.6 ± 0.02	26.0 ± 0.05	67.5 ± 0.1	3.9 ± 0.2

<sup>a</sup> CDW, cell dry weight; 3HHx, 3-hydroxyhexanoate; 3HO, 3-hydroxyoctanoate; 3HD, 3-hydroxydecanoate; 3HDD, 3-hydroxydodecanoate; ND, not determined.

<sup>b</sup> The cells were grown on MS medium with either high N (7.2 g liter<sup>-1</sup>) or low N (0.072 g liter<sup>-1</sup>).

for qRT-PCR since it has already been identified as an ideal house-keeping gene for this task due to its stable expression levels in *Pseudomonas aeruginosa* (22). The ratios of transcription levels of genes from cells grown on low N MS medium versus those of cells grown on high N MS medium that were >1 were defined as induced by low-nitrogen conditions. The transcription levels of all three genes in the PHA synthesis cluster (*phaC1*, *phaZ*, and *phaC2*) were higher when cells were grown on low N MS than on high N MS medium. The *phaJ4* gene had the highest transcription level among all three *phaJ* genes, and this result was consistent with previous research showing that PhaJ4 was the major enzyme channeling  $\beta$ -oxidation for PHA biosynthesis (27). Surprisingly, the *phaG* gene had significantly higher transcription levels (~220-fold) when cells were grown on low N MS medium than on high N MS medium (Table 4). This result suggested that the PhaG enzyme plays an important role in PHA biosynthesis from unrelated carbon sources, and it was most likely to be a critical step for PHA biosynthesis in *P. putida*. Growing cells on a non-fatty acid carbon source, such as glycerol, under nitrogen limitation led to PHA production. PHA biosynthesis under these conditions is highly likely to be derived from fatty acid biosynthesis rather than  $\beta$ -oxidation. Results indicated that *phaG* was highly upregulated when the cells were grown under nitrogen limitation conditions in *P. putida* KT2440 and suggest that *phaG* expression and PHA production are stress induced.

Transcription levels of all of the genes homologous to *alkK* in *P. oleovorans* (*alkK<sub>po</sub>*) (26) were also analyzed by qRT-PCR (Table 5). Transcription levels of most of the genes were upregulated during growth in medium with low N concentrations. Based on

TABLE 4 Expression levels of genes involved in PHA biosynthesis pathways in *P. putida* KT2440 cells grown on low N MS medium and those grown on high N MS medium

Locus name	Gene symbol	Putative identification	Induction <sup>a</sup> (n-fold)
PP5003	<i>phaC1</i>	Poly(3-hydroxyalkanoate) polymerase 1	2.6 ± 0.5
PP5004	<i>phaZ</i>	Poly(3-hydroxyalkanoate) depolymerase	4.5 ± 0.8
PP5005	<i>phaC2</i>	Poly(3-hydroxyalkanoate) polymerase 2	4.3 ± 0.5
PP4552	<i>phaJ1</i>	(R)-specific enoyl-CoA hydratase 1	1.1 ± 0.2
PP0580	<i>phaJ3</i>	(R)-specific enoyl-CoA hydratase 2	0.9 ± 0.2
PP4817	<i>phaJ4</i>	(R)-specific enoyl-CoA hydratase 3	3.8 ± 1.3
PP1048	<i>phaG</i>	3-Hydroxyacyl-ACP thioesterase	220 ± 31

<sup>a</sup> Induction is defined as the ratio of expression level of genes in cells grown on low N MS medium versus that in cells grown on high N MS medium.

the transcription levels and the hypothesis that a CoA ligation step is necessary for PHA production from unrelated carbon sources, this result showed that multiple enzymes might be involved in this reaction. Among the *P. putida* homologs to the AlkK protein from *P. oleovorans*, the gene encoding the putative medium-chain-fatty-acid CoA ligase (the PP0763 gene), which shares 36% identity and 54% similarity to AlkK<sub>po</sub>, showed the highest transcription level; therefore, it was hypothesized to play an important role in the production of (R)-3-hydroxyacyl-CoA for PHA production from unrelated carbon sources.

**MCL-PHA production in recombinant *E. coli* strains.** Previous studies demonstrated that *phaG* is important for PHA biosynthesis from unrelated carbon sources in pseudomonads (18). However, based on *phaG* expression experiments in *E. coli*, *phaG* alone is unable to provide 3-hydroxyacyl-CoA substrates for PHA production from unrelated carbon sources (18, 30). In order to investigate if the gene encoding the putative medium-chain-fatty-acid CoA ligase (the PP0763 gene) was involved in PHA biosynthesis from unrelated carbon sources, the *phaG* and PP0763 genes were amplified by PCR from *P. putida* KT2440 and inserted into the expression vector pTrc99A to construct the plasmid pTrcGK. For construction of the control plasmids, *phaG* and the PP0763 gene were also cloned into pTrc99A separately to make the plasmids pTrcG and pTrcK.

The *P. putida* PP0763 gene encoding the AlkK-like protein and *phaG* genes encoding the synthetic pathway to produce MCL-PHA precursors were coexpressed from pTrcKG with pBBRSTQK (Table 1) carrying the PHA synthase gene *phaC1*(STQK)<sub>ps</sub> in *E. coli* to assess their ability to produce MCL-PHA from non-fatty acid carbon sources. The initial strain used for PHA production

TABLE 5 Expression levels of genes encoding acyl-CoA ligase homologs in *P. putida* KT2440 cells growing on low N MS medium and on high N MS medium

Locus name	Gene symbol	Putative identification	Induction (n-fold)
PP0763		Medium-chain-fatty-acid CoA ligase	10.5 ± 1.0
PP3553		AMP-binding domain protein	3.2 ± 1.8
PP2795		AMP-binding domain protein	6.1 ± 0.2
PP3458		Long-chain-fatty-acid CoA ligase, putative	2.1 ± 1.3
PP2038		Long-chain-fatty-acid CoA ligase, putative	2.6 ± 0.6
PP4063		Long-chain-fatty-acid CoA ligase, putative	0.9 ± 0.2
PP4549	<i>fadD</i>	Long-chain-fatty-acid CoA ligase	1.5 ± 0.03
PP4550	<i>fadD2</i>	Long-chain-fatty-acid CoA ligase	1.3 ± 0.1
PP4487	<i>acsA</i>	Acetyl-CoA synthetase	0.6 ± 0.02
PP2213	<i>fadDx</i>	Acyl-CoA ligase	1.8 ± 0.2
PP2351		Acetyl-CoA synthetase, putative	1.2 ± 0.1
PP4702	<i>acsB</i>	Acetyl-CoA synthetase	1.3 ± 0.5
PP3071		Acetoacetyl-CoA synthetase, putative	4.2 ± 0.7
PP2709		Long-chain-fatty-acid CoA ligase, putative	3.3 ± 0.5

TABLE 6 PHA production in recombinant *E. coli* strains<sup>a</sup>

Relevant plasmids <sup>b</sup>	CDW (g liter <sup>-1</sup> )	PHA produced (mg liter <sup>-1</sup> )	% PHA	Composition (mol%)			
				3HHx	3HO	3HD	3HDD
<i>E. coli</i> BL21(DE3)							
pTrcG, pBBRSTQK	1.2 ± 0.1	3.1 ± 0.7	0.2 ± 0.05	ND	ND	100	ND
pTrcK, pBBRSTQK	0.8 ± 0.1	ND	ND	ND	ND	ND	ND
pTrcGK, pBBRSTQK	1.7 ± 0.1	69 ± 21	4.1 ± 1.3	3.3 ± 0.4	51.0 ± 1.1	44.3 ± 1.6	1.4 ± 0.3
<i>E. coli</i> LS5218							
pTrcGK, pBBRSTQK	3.4 ± 0.2	392 ± 61	11.6 ± 1.3	1.3 ± 0.1	39.2 ± 0.8	56.9 ± 0.8	2.6 ± 0.1
<i>E. coli</i> LS11							
pTrcGK, pBBRSTQK	1.7 ± 0.1	123 ± 30	7.2 ± 1.5	N.D.	32.9 ± 0.9	65.1 ± 2.0	2.0 ± 0.1

<sup>a</sup> CDW, cell dry weight; 3HHx, 3-hydroxyhexanoate; 3HO, 3-hydroxyoctanoate; 3HD, 3-hydroxydecanoate; 3HDD, 3-hydroxydodecanoate; ND, not determined.

<sup>b</sup> The cells were grown on LB medium with 100 µg ml<sup>-1</sup> ampicillin and 50 µg ml<sup>-1</sup> kanamycin. IPTG was added to a final concentration of 1 mM at 5 h, and 20 g liter<sup>-1</sup> glucose was added at 8 h.

was *E. coli* BL21(DE3). This strain was chosen because it has been used in previous studies for overproducing recombinant proteins, ethanol, and other biomolecules (29). The results of this coexpression are shown in Table 6. PHA was accumulated to ~4% cell dry weight in recombinant *E. coli* BL21(DE3) harboring the plasmids pTrcGK and pBBRSTQK. The major repeating units in the PHA polymers produced were 3-hydroxyoctanoate (3HO) (~51 mol%) and 3HD (~44 mol%), which was slightly different in composition compared to PHA polymer produced in the wild-type *P. putida* strain (Table 3). A recombinant *E. coli* BL21(DE3) strain containing plasmid pTrcK (PP0763) and pBBRSTQK was examined as a negative control and failed to produce any polymer, while another control strain harboring pTrcG (*phaG<sub>pp</sub>*) and pBBRSTQK produced trace amounts of 3HD (~0.2% per cell dry weight) based on GC. In addition to the PP0763 gene, another open reading frame encoding an AlkK<sub>po</sub> homolog, the PP2795 gene, which was transcribed at the second highest level (~6-fold) among genes encoding AlkK homologs in cells grown under PHA-producing conditions (Table 5), was also coexpressed with *phaG<sub>pp</sub>* and *phaC1*(STQK)<sub>ps</sub> in *E. coli*. However, unlike the PP0763 gene, no detectable MCL-PHAs were produced in the recombinant cells. Therefore, the PP2795 gene is unlikely to be involved in PHA biosynthesis.

The plasmids pTrcGK and pBBRSTQK were also transformed into *E. coli* LS5218 [*fadR601 atoC2*(con)], which allowed for constitutive expression of enzymes involved in utilization of fatty acids (6). PHA content increased to 11.6% per cell dry weight, and the cell dry weight was also about 2-fold higher than that of the recombinant BL21(DE3) strain. The PHA production reached ~400 mg liter<sup>-1</sup>, which was ~4-fold higher than that of wild-type *Pseudomonas putida* KT2440 (109 mg liter<sup>-1</sup>). The composition of PHAs was 1.3% 3-hydroxyhexanoate (3HHx), 32.9% 3HO, 56.9% 3HD, and 2.6% 3-hydroxydodecanoate (3HDD), which was similar to that of wild-type *Pseudomonas putida* KT2440 (Table 3). Prior to the current study, MCL-PHA production from unrelated carbon sources had been problematic due to the difficulty of drawing PHA precursors from fatty acid biosynthesis. In a previous study, MCL-PHAs were produced at 2.3% per cell dry weight in the presence of gluconate and overexpression of *E. coli* thioesterase I (8). By adding the fatty acid biosynthesis inhibitor triclosan into the medium, another study claimed that coexpression of *phaC1* and *phaG<sub>pp</sub>*

led to accumulation of 2 to 3% PHA per cell dry weight in recombinant *E. coli* (19). However, since the PHA content was measured only by GC, the 3HD detected in that study might have been extracellular 3-hydroxydecanoic acids rather than PHA polymers, based on a previous study (30) and our current study.

Since  $\beta$ -oxidation was constitutively expressed in *E. coli* LS5218, the higher MCL-PHA production in *E. coli* LS5218 than in *E. coli* BL21(DE3) might be due to MCL-PHA substrates contributed from intermediates of  $\beta$ -oxidation. In order to exclude the possibility that the PHA production was derived from fatty acid  $\beta$ -oxidation, the *fadE* gene encoding an acyl-CoA dehydrogenase was inactivated in *E. coli* 5218 to produce the mutant strain *E. coli* LS11. This strain was unable to grow on fatty acids as the sole carbon sources (data not shown). The two plasmids pTrcGK and pBBRSTQK were also coexpressed in *E. coli* LS11, and the PHA yield was 7.2% per cell dry weight, which was still higher than that from *E. coli* BL21(DE3). The PHA composition was similar to that of recombinant *E. coli* LS5218. This result suggested that the PHA production in recombinant *E. coli* strains was derived mainly from fatty acid biosynthesis. The higher production in *E. coli* LS5218 is likely due to better transportation of the free 3-hydroxy fatty acids generated by PhaG back into the cells to make PHAs.

For further confirmation, the PHA polymer produced by recombinant *E. coli* LS5218 was purified and analyzed by <sup>1</sup>H and <sup>13</sup>C NMR spectroscopy (Fig. 3). The chemical shifts for the <sup>1</sup>H NMR were assigned based on NMR spectroscopy performed in the study by Huijberts et al. (5), and the chemical shifts for <sup>13</sup>C NMR spectroscopy were assigned based on the study by Matsusaki et al. (13). The results confirmed that MCL-PHAs were produced and the major repeating units were 3HD and 3HO. The ratios of 3HHx and 3HDD were too low to be detected by <sup>13</sup>C NMR.

**Production of free 3-hydroxy fatty acids in recombinant *E. coli* expressing the *phaG* gene.** PhaG was previously identified as an (R)-3-hydroxyacyl-ACP-CoA transferase based on the ability of the partially purified enzyme to convert 3-hydroxydecanoyl-CoA to 3-hydroxydecanoyl-ACP in the presence of ACP (18). However, there was no PHA produced when the *phaG* and PHA synthase genes were heterogeneously expressed in recombinant *E. coli* (12, 18). On the other hand, overexpression of the *phaG* gene in *E. coli* led to the extracellular production of 3-hydroxydecanoic acid as demonstrated in the current study

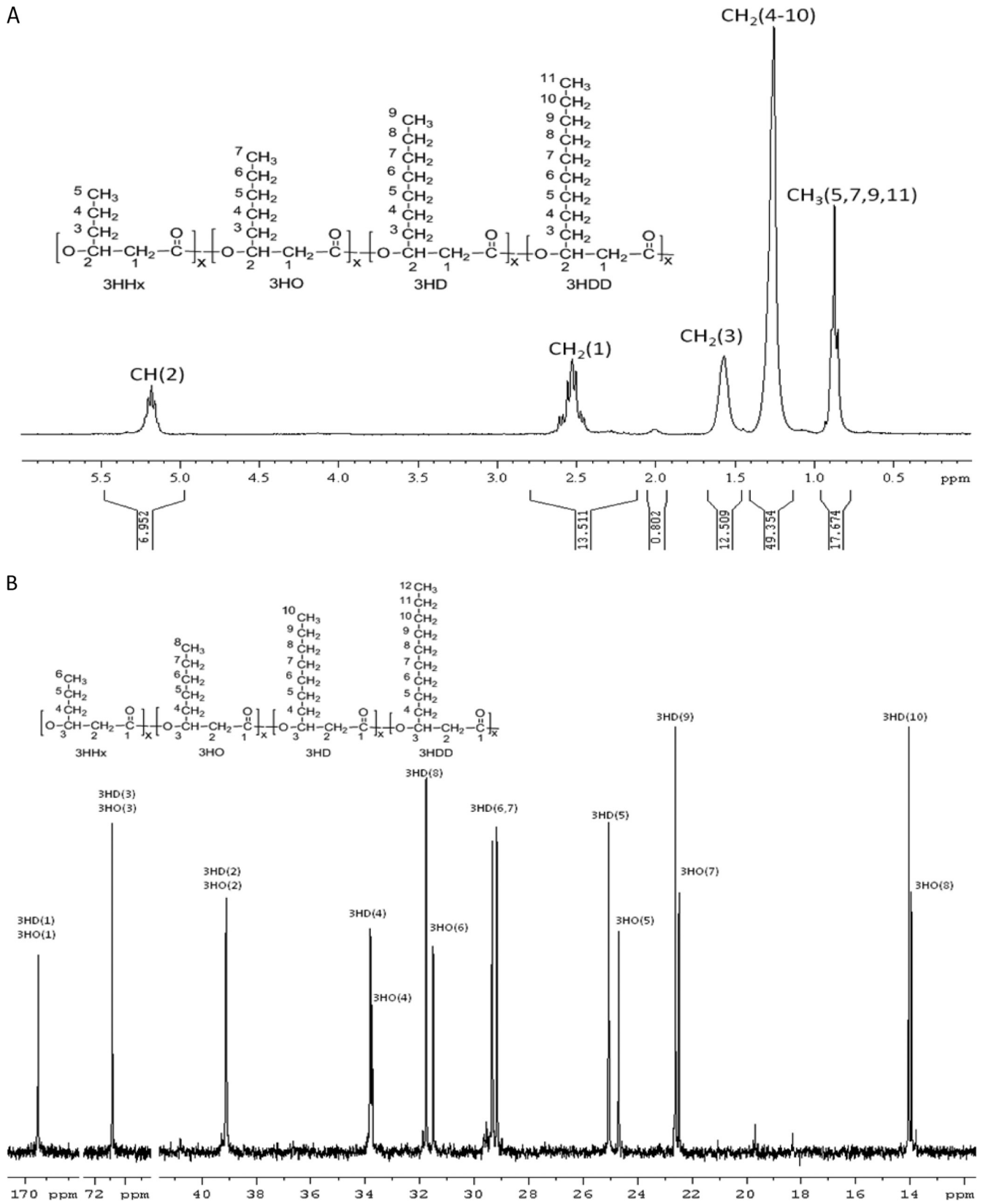


FIG 3 NMR spectrum of polymers isolated from *E. coli* LS5218 harboring the pTrcGK and pBBRSTQK plasmids grown in the presence of glucose. (A)  $^1\text{H}$  NMR spectrum. Protons in the polymers are numbered and assigned to the peaks in the spectrum. (B)  $^{13}\text{C}$  NMR spectrum. Carbon atoms in polymers are numbered and assigned to peaks in the spectrum.



and a previous study (30). These results suggest that PhaG functions as a 3-hydroxyacyl-ACP thioesterase to remove the ACP from the 3-hydroxyacyl-ACP to form free 3-hydroxy fatty acids rather than as an (*R*)-3-hydroxyacyl-ACP-CoA transferase.

In order to further verify that PhaG is a 3-hydroxy-acyl-ACP thioesterase rather than a 3-hydroxyacyl-ACP-CoA transacylase, recombinant *E. coli* LS5218 harboring pTrcG (expressing only the *phaG* gene) was grown under the same conditions as those described in Table 6. Results indicate that expression of *phaG* alone led to the production of  $\sim 1.6$  g liter<sup>-1</sup> free 3-hydroxy fatty acids consisting of 45% 3-hydroxyoctanoate and 55% 3-hydroxydecanoate as detected in the supernatant and no detectable PHAs in the cells. This result is consistent with previous research showing (30).

In order to demonstrate that the substrates for PHA synthesis were most likely derived from the fatty acid biosynthesis pathway and to further prove that PhaG is a 3-hydroxy-acyl-ACP thioesterase, *E. coli* LS5218 harboring pTrcG and pBBRSTQK was also grown on MS medium using glycerol as the sole carbon source. *E. coli* LS5218 harboring pTrcGK and pBBRSTQK grown under the same conditions was used as a control. The concentration of free fatty acids was measured in the supernatant. The *E. coli* strain harboring pTrcG and pBBRSTQK produced about 30 mg liter<sup>-1</sup> 3-hydroxy fatty acids, comprised of 3-hydroxydecanoic acid (58%) and 3-hydroxyoctanoic acid (42%) in the supernatant. These results indicate that PhaG functions as a 3-hydroxyacyl-ACP thioesterase rather than a 3-hydroxyacyl-ACP-CoA transferase.

Meanwhile, the control strain did not produce any detectable 3-hydroxy fatty acids in the supernatant but produced PHA polymers in the cell. The *E. coli* strain harboring pTrcG and pBBRSTQK produced about 0.9 mg liter<sup>-1</sup> PHAs as detected by GC, while the strain harboring pTrcGK and pBBRSTQK produced about 25 mg liter<sup>-1</sup> PHAs. This result was consistent with the PHA production data described in Table 6. Since glycerol was the only carbon source for these experiments, this result further proved that PP0763 is essential to establish a link to PHA production from non-fatty acid carbon sources in recombinant *E. coli*.

**Conclusions.** Our study demonstrates for the first time that MCL-PHA polymers could be successfully synthesized from the non-fatty acid carbon sources glucose and glycerol in recombinant *E. coli*, with production levels as high as 400 mg liter<sup>-1</sup> and 11.6% per cell dry weight. This study has identified and characterized a novel pathway to make MCL-PHAs from non-fatty acid carbon sources. Glucose can be derived from cellulosic feedstocks, and glycerol is a by-product of biodiesel production. It is expected that the cost of these feedstocks will decrease as the technologies for their production mature. Due to the ubiquity of fatty acid biosynthesis in organisms and because the biosynthetic pathway developed by our study derives 3-hydroxyacyl-CoA substrates from fatty acid biosynthetic pathways, it offers great flexibility in carbon source utilization for MCL-PHA production. This could have great potential to expand the number of inexpensive carbon sources to be used for the production of MCL-PHA polymers.

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