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著者 Author(s)	Shigechi, Hisayori / Koh, Jun / Fujita, Yasuya / Matsumoto, Takeshi / Bito, Yohei / Ueda, Mitsuyoshi / Satoh, Eiichi / Fukuda, Hideki / Kondo, Akihiko
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Direct Production of Ethanol from Raw Corn Starch via Fermentation by Use of a Novel Surface-Engineered Yeast Strain Codisplaying Glucoamylase and α -Amylase

Hisayori Shigechi,¹ Jun Koh,¹ Yasuya Fujita,² Takeshi Matsumoto,² Yohei Bito,¹ Mitsuyoshi Ueda,³ Eiichi Satoh,⁴ Hideki Fukuda,² and Akihiko Kondo^{1*}

Department of Chemical Science and Engineering, Faculty of Engineering,¹ and Division of Molecular Science, Graduate School of Science and Technology,² Kobe University, Nada-ku, Kobe 657-8501, Department of Applied Biochemistry, Division of Applied Life Sciences, Graduate School of Agriculture, Kyoto University, Sakyo-ku, Kyoto 606-8502,³ and Department of Applied Biology and Chemistry, Tokyo University of Agriculture, Setagaya-ku, Tokyo 156-8502,⁴ Japan

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Direct and efficient production of ethanol by fermentation from raw corn starch was achieved by using the yeast *Saccharomyces cerevisiae* codisplaying *Rhizopus oryzae* glucoamylase and *Streptococcus bovis* α -amylase by using the C-terminal-half region of α -agglutinin and the flocculation functional domain of Flo1p as the respective anchor proteins. In 72-h fermentation, this strain produced 61.8 g of ethanol/liter, with 86.5% of theoretical yield from raw corn starch.

Recent years have seen the introduction of large-scale processing in the bioconversion of biomass resources, especially starchy materials, to ethanol, which is expected to find a wide range of uses, including as biofuel and as the starting material for various chemicals. However, the present process for ethanol production from starchy materials via fermentation consists of two or three steps and requires improvement if it is to realize efficient production at low cost. There are two main reasons for the present high cost: one is that, as the yeast *Saccharomyces cerevisiae* cannot utilize starchy materials, large amounts of amylolytic enzymes, namely, glucoamylase (EC 3.2.1.3) and α -amylase (EC 3.2.1.1), need to be added; the other is that the starchy materials need to be cooked at a high temperature (140 to 180°C) to obtain a high ethanol yield. To reduce the energy cost for cooking of starchy materials, previously reported noncooking and low-temperature-cooking fermentation systems (11, 12) have succeeded in reducing energy consumption by approximately 50% (11), but it is still necessary to add large amounts of amylolytic enzymes to hydrolyze the starchy materials to glucose.

Many researchers have reported on attempts to resolve this problem by using recombinant glucoamylase-expressing yeasts with the ability to ferment starch to ethanol directly (1, 3, 7, 9, 14, 16). Recombinant yeasts which coproduce glucoamylase and α -amylase have meanwhile been developed to further improve the efficiency of starch fermentation (2, 4, 6, 15, 21, 22). We also have used a cell surface engineering system based on α -agglutinin to demonstrate the advantages of yeast strains codisplaying amylolytic enzymes and have succeeded in producing ethanol from soluble and low-temperature-cooked corn starch using yeast strains which display *Rhizopus oryzae* glu-

coamylase and codisplay or secrete *Bacillus stearothermophilus* α -amylase (21, 22). These strains cannot, however, ferment raw corn starch to ethanol.

In the present study, instead of the *B. stearothermophilus* α -amylase, we therefore attempted to express α -amylase from the lactic acid bacterium *Streptococcus bovis* 148 together with *R. oryzae* glucoamylase. Extracellular α -amylase secreted from *S. bovis* 148 is known to have a strong ability to hydrolyze and be adsorbed onto raw corn starch (18, 19). For the development of a novel noncooking fermentation system, direct ethanol production from raw corn starch was investigated with yeast strains that codisplayed *R. oryzae* glucoamylase and *S. bovis* 148 α -amylase by using the C-terminal half of α -agglutinin and the flocculation functional domain of Flo1p (13, 26) as anchor proteins.

Strains and media. *Escherichia coli* NovaBlue (Novagen Inc., Madison, Wis.) was used for genetic manipulation. The *S. cerevisiae* strain used was YF207 (*MATa ura3-52 trp1 Δ 2 leu can1-100 FLO8*) (9). *E. coli* was grown in Luria-Bertani medium (10 g of tryptone, 5 g of yeast extract, and 10 g of sodium chloride/liter) containing 100 μ g of ampicillin per ml. Synthetic medium (6.7 g of yeast nitrogen base/liter without amino acids [Difco Laboratories, Detroit, Mich.] with appropriate nucleic acids and amino acids, 20 g of glucose per liter, and 20 g of Casamino Acids [Difco] per liter) was used for yeast cultivation under selective conditions (SDC medium).

Construction of plasmids for display of α -amylase from *S. bovis*. Figure 1 shows the expression plasmids used for C-terminal immobilization based on the C-terminal half of α -agglutinin and for N-terminal immobilization based on the flocculation functional domain of Flo1p of *S. bovis* α -amylase. The gene encoding the mature region of α -amylase was amplified by PCR (primers 5'-GGATCCTGCAGATGAACAAGTGTC AA-3' and 5'-CTCGAGTTTTAGCCCATCTTTATTAT-3') with *S. bovis* 148 genomic DNA as the template and inserted

* Corresponding author. Mailing address: Department of Chemical Science and Engineering, Faculty of Engineering, Kobe University, 1-1 Rokkodaicho, Nada-ku, Kobe 6547-8501, Japan. Phone: 81-78-803-6196. Fax: 81-78-803-6196. E-mail: kondo@cx.kobe-u.ac.jp.

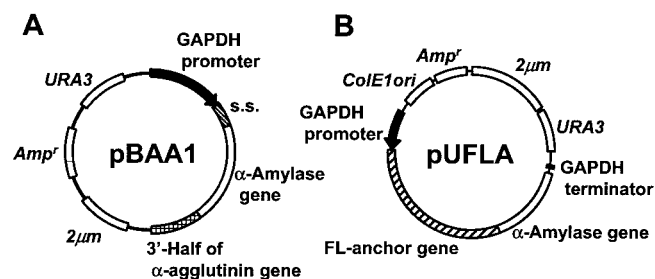


FIG. 1. Expression plasmids for cell surface display of *S. bovis* α -amylase. (A) Plasmid pBAA1 for C-terminal immobilization using the α -agglutinin-based surface display system; (B) plasmid pUFLA for N-terminal immobilization using the Flo1p-based surface display system. s.s., secretion signal sequence of *R. oryzae* glucoamylase gene.

into the BamHI-SalI site of plasmid pQE31 (Qiagen, Valencia, Calif.) to give plasmid pQE31::amyA.

The multicopy plasmid pBAA1 (Fig. 1A) for cell surface display of α -amylase using a surface display system based on α -agglutinin was constructed as follows: the mature region of α -amylase was prepared by PCR (primers 5'-ACGGCCGCGGGGATGAACAAGTGTCAATGAAAGATGGT-3' and 5'-CTGCCTCGAGGGTTTTAGCCCATCTTTATTATAGTTTCC-3') with plasmid pQE31::amyA as the template and inserted into the SacII-XhoI site of plasmid pCAS1 (20) to give plasmid pCAS1::amyA. Next, a 2.2-kb DNA fragment containing the secretion signal sequence of the *R. oryzae* glucoamylase gene and the mature region of the α -amylase gene was prepared by PCR (primers 5'-AATACTCGAGATGCAACTGTCAATTTGCCATTGAAAGT-3' and 5'-CTGCCTCGAGGGTTTTAGCCCATCTTTATTATAGTTTCC-3') with plasmid pCAS1::amyA as the template and inserted into the XhoI site of the cell surface expression plasmid pUGP12 (21). The resulting plasmid was designated pBAA1.

The multicopy plasmid pUFLA (Fig. 1B) for cell surface display of α -amylase using a surface display system based on the flocculation functional domain of Flo1p was constructed as follows: the gene encoding the mature region of α -amylase was amplified by PCR (primers 5'-CGTTAGATCTGATGAACAAGTGTCAATGAAAGATGGTACG-3' and 5'-ATAACTCGAGTTATTTAGCCCATCTTTATTATAGTTTCC-3') with plasmid pQE31::amyA as the template and inserted into the BglII-XhoI site of plasmid pWIFL (13) to give plasmid pWIFLA. The fusion gene encoding amino acids 1 to 1447 of Flo1p (FL anchor) and the mature region of α -amylase was prepared by PCR (primers 5'-ACATGGATCCATGACAATGCCTCATCGCTATATGTTTTTG-3' and 5'-ATAACTCGAGTTATTTAGCCCATCTTTATTATAGTTTCC-3') with plasmid pWIFLA as the template. This fragment was digested with BamHI and XhoI and inserted into the BamHI-SalI site of plasmid pUGP3 (24). The resulting plasmid was designated pUFLA.

Plasmid pGA11 for cell surface display of *R. oryzae* glucoamylase was constructed previously (14). The plasmids were transformed into *S. cerevisiae* YF207 by the lithium acetate method using the YEASTMAKER transformation system (Clontech Laboratories, Inc., Palo Alto, Calif.).

Determination of enzyme activities. Glucoamylase and α -amylase activities of yeast strains were determined by using

TABLE 1. Glucoamylase and α -amylase activities of yeast strains carrying different plasmids

Strain	Activity (U/g [wet wt] of cells) ^a	
	Glucoamylase	α -Amylase
YF207	ND	ND
YF207/pGA11	42.5	ND
YF207/pBAA1	ND	2.52
YF207/pUFLA	ND	90.1
YF207/pGA11/pBAA1	45.9	2.38
YF207/pGA11/pUFLA	57.0	114

^a Values are averages of three independent experiments. ND, not detected.

the saccharifying-ability assay kit and α -amylase assay kit (Kikkoman Corp., Chiba, Japan), respectively, with 4-nitrophenyl β -maltoside and 2-chloro-4-nitrophenyl 6⁵-azide-6⁵-deoxy- β -maltopentaoside as the substrates. After aerobic cultivation of yeast in SDC medium at 30°C for 60 h, cells were collected by centrifugation for 10 min at 8,000 \times g, resuspended in distilled water, and used for enzyme assays.

Experiments on ethanol production via fermentation. Yeast strains were aerobically grown in SDC medium at 30°C for 60 h and harvested by centrifugation for 10 min at 8,000 \times g. The cell pellet was used to inoculate YPS medium, which was prepared by adding raw corn starch (Wako Pure Chemical Industries, Ltd., Osaka, Japan) to sterile YP medium (10 g of yeast extract, 20 g of polypepton, and 0.5 g of potassium disulfite/liter). Ethanol production via fermentation was carried out in 100-ml closed bottles equipped with a bubbling CO₂ outlet and containing 50 ml of YPS medium. All fermentations were performed at 30°C with mild agitation at 100 rpm. Potassium disulfite as an antiseptic was added to the YPS medium to prevent contamination with harmful microorganisms. The initial cell density was adjusted to 10 to 100 g [wet weight] of cells per liter. The wet weight of cells was determined by measuring the weight of the cell pellet, which was collected by centrifugation at 8,000 \times g for 10 min and careful removal of the supernatant. The dry weight of cells corresponds to 0.15 times the wet weight of cells.

Total sugar and glucose concentrations were measured using the phenol-sulfuric acid method (5) as the glucose equivalent and the Glucose CII test (Wako), respectively. Ethanol concentration was measured by gas chromatography (model GC-8A fitted with a flame-ionization detector; Shimadzu, Kyoto, Japan) using a glass column (3.2 mm by 2.0 m) packed with Thermo-3000 (Shimadzu).

Activities of surface-displayed glucoamylase and α -amylase. To confirm the coproduction of glucoamylase and α -amylase, their activities were determined (Table 1). The glucoamylase activities of yeast strains YF207/pGA11, YF207/pGA11/pBAA1, and YF207/pGA11/pUFLA harboring the plasmid pGA11 for surface display were 42.5, 42.3, and 57.0 U/g [wet weight] of cells, respectively; no activity was detected in strains YF207/pBAA1 and YF207/pUFLA. α -Amylase activity, meanwhile, was high in strains YF207/pUFLA and YF207/pGA11/pUFLA, which display α -amylase using Flo1p as an anchor (90.1 and 114 U/g [wet weight] of cells), but approximately 40 times lower in strains YF207/pBAA1 and YF207/pGA11/pBAA1, which display α -amylase using α -agglutinin as an an-

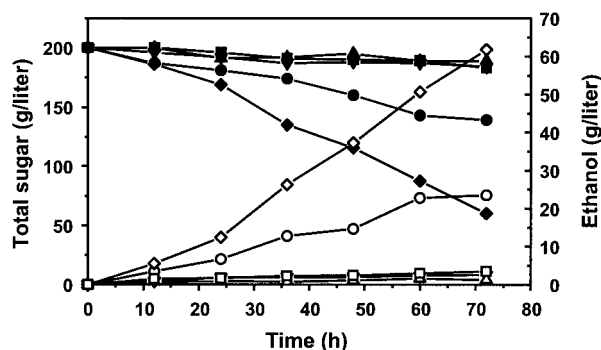


FIG. 2. Time course of direct ethanol production via fermentation from raw corn starch, which corresponds to 200 g of total sugar as the sole carbon source/liter using 100 g [wet weight] of cells of yeast strains *S. cerevisiae* YF207/pGA11 (squares), YF207/pBAA1 (triangles), YF207/pUFLA (inverted triangles), YF207/pGA11/pBAA1 (circles), and YF207/pGA11/pUFLA (diamonds) per liter. Open and closed symbols show ethanol and total sugar concentrations, respectively. Data are averages from three independent experiments.

chor (2.52 and 2.38 U/g [wet weight] of cells). It has been reported that several α -amylases have raw-starch-digesting and raw-starch-binding abilities and that the starch binding domain is located in the C-terminal region (8, 10, 17, 23, 25). Immobilization on the cell surface at the N terminus using Flo1p allows α -amylase to be efficiently adsorbed onto, and to degrade, raw corn starch. No glucoamylase or α -amylase activity was detected in the culture supernatant of any of the strains.

Ethanol production from raw corn starch. Each of the recombinant yeast strains was used in direct ethanol production via fermentation from raw corn starch. The raw corn starch, which corresponds to 200 g of total sugar/liter, was used as the sole carbon source. As shown in Fig. 2, strain YF207/pGA11, displaying only glucoamylase, and strains YF207/pBAA1 and YF207/pUFLA, displaying only α -amylase, produced almost no ethanol, while soluble sugar accumulated in the fermentation medium of strain YF207/pUFLA due to degradation of corn starch to oligosaccharides by the surface-displayed α -amylase. Although strain YF207/pGA11/pBAA1, codisplaying glucoamylase and α -amylase via α -agglutinin, did produce ethanol from the raw corn starch, the ethanol yield was low (23.5 g/liter) after 72 h of fermentation. On the other hand, the yeast strain codisplaying glucoamylase and α -amylase using α -agglutinin and Flo1p (YF207/pGA11/pUFLA) was able to produce ethanol directly from raw corn starch without addition of commercial enzymes. The concentration of raw corn starch decreased drastically during fermentation, as the ethanol concentration increased to 61.8 g/liter after 72 h of fermentation. A reduction in the particle size and the number of corn starch granules during fermentation was also observed by microscopy (data not shown). The yield in terms of grams of ethanol produced per gram of sugar consumed was 0.44 g/g, which corresponds to 86.5% of theoretical yield (0.51 g of glucose consumed/g). No glucose was detected in the fermentation medium. The yeast strain YF207/pGA11/pUFLA maintained almost the same glucoamylase and α -amylase activities during fermentation. This result suggests that degradation of raw corn starch by α -amylase plays a very important role and that the putative starch binding domain at the C terminus of α -amylase

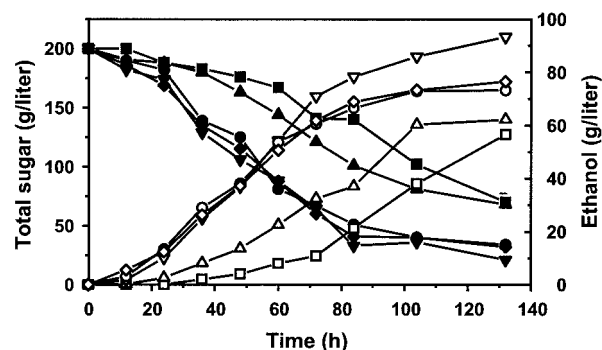


FIG. 3. Effect of initial YF207/pGA11/pUFLA cell density on non-cooking fermentation from raw corn starch, which correspond to 200 g of total sugar, as the sole carbon source, per liter. Symbols represent initial cell densities of 10 (squares), 25 (triangles), 50 (inverted triangles), 75 (circles), and 100 (diamonds) g [wet weight] of cells per liter. Open and closed symbols show ethanol and total sugar concentrations, respectively. Data are averages from two or three independent experiments.

acts on raw corn starch in the yeast strain used (YF207/pGA11/pUFLA), which codisplays glucoamylase and α -amylase using α -agglutinin and Flo1p as anchors.

Effect of initial cell density. To reduce the number of yeast cells used for direct ethanol production via fermentation, the effect of initial cell density was examined with yeast strain YF207/pGA11/pUFLA and raw corn starch. Direct fermentation was carried out in the range of 10 to 100 g [wet weight] of cells per liter. As shown in Fig. 3, in fermentations using 50, 75, and 100 g of cells/liter, ethanol productivity was almost the same, but it was higher than with 10 and 25 g of cells/liter. Specifically, with 50 g of cells/liter, the maximum ethanol concentration increased gradually and reached 93.3 g/liter in the 132-h fermentation.

Conclusions. We succeeded in producing ethanol directly from raw corn starch using yeast strain YF207/pGA11/pUFLA, which codisplays *R. oryzae* glucoamylase and *S. bovis* α -amylase, using α -agglutinin and Flo1p with no time lag in the decrease in corn starch. In sequential reactions of α -amylase and glucoamylase codisplayed on the cell surface, raw corn starch was hydrolyzed to glucose. The noncooking fermentation system using a cell surface-engineered yeast strain thus promises to be very effective in reducing the production costs of ethanol.

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