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ABSTRACT

The turbulent boundary layer under a freestream velocity that varies sinusoidally in time around a zero mean is considered. The flow has a rich variety of behaviors including strong pressure gradients, inflection points, and reversal. A theory for the velocity and stress profiles at high Reynolds number is formulated. Well-resolved direct Navier-Stokes simulations are conducted over a narrow range of Reynolds numbers and the results are compared with the theoretical predictions. The flow is also computed over a wider range of Reynolds numbers using a new algebraic turbulence model: the results are compared with the direct simulations and the theory.

NOMENCLATURE

f_1, f_2, \dots unknown nondimensional functions, see Eq. (3), (4)...

$L \equiv U_0/\omega$ outer length scale

$Re \equiv U_0 \delta_l/\nu$ Reynolds number

t time

u, v, w velocity components

$u' \equiv u - U$ fluctuating velocity component

$U \equiv \langle u \rangle$ mean velocity component

U_l laminar mean velocity component, see Eq. (3)

U_0 peak freestream velocity, see Eq. (1)

U_∞ freestream velocity, see Eq. (1)

u^* peak friction velocity, see Eq. (5)

u_r friction velocity (can be negative)

$U^+ \equiv U/u_r$ wall units

x, y, z streamwise, normal, spanwise coordinates

$y^+ \equiv y|u_r|/\nu$ wall units

$\delta_l \equiv \sqrt{2\nu/\omega}$ laminar boundary-layer thickness, see Eq. (3)

δ turbulent boundary-layer thickness, see Eq. (5)

κ Karman constant

Λ_x, Λ_z periods in x and z directions

ν kinematic viscosity

$\phi \equiv \omega t$ phase angle

ϕ_0 phase shift, a function of Re , see Eq. (7)

ω frequency, see Eq. (1)

$\tau \equiv U_y - \langle u'v' \rangle$ total shear stress

$\langle \rangle$ average in x, z and/or ensemble

INTRODUCTION

The flow under consideration is the turbulent version of a classical exact solution of the Navier-Stokes equations, known as Stokes' second problem (1). The domain is the half-space over a stationary flat plate and the freestream velocity is given by

$$U_\infty(t) = U_0 \cos(\omega t). \quad (1)$$

The three parameters (peak velocity U_0 , frequency ω and kinematic viscosity ν) combine into a single nondimensional parameter: a Reynolds number Re . The laminar solution is

$$U_l(y, t) = U_\infty(t) - U_0 e^{-y/\delta_l} \cos(\omega t - y/\delta_l) \quad (2)$$

where δ_l is the laminar boundary-layer thickness.

This flow is attractive because of its rich time-dependent behavior, and because it is naturally homogeneous in the directions parallel to the plate (this is true only because the mean value of $U_\infty(t)$ is zero). This justifies imposing periodic conditions in a direct simulation and considerably improves the statistical sample. In addition, the Reynolds-averaged quantities are functions only of the normal coordinate and the time. This provides a good test case for turbulence models, in which their ability to treat unsteady and inflectional velocity profiles can be tested with little numerical effort and with high numerical accuracy. It also exhibits reversal of the velocity without the usual viscous-inviscid coupling difficulties and singularities encountered in spatially-separating flows. The fully-developed flow will most likely be close to the common turbulent boundary layer, except that the lack of entrainment will prevent the formation of a sharp laminar-turbulent interface.

The known results concern primarily the transition Reynolds number, $Re \approx 600$, and the stability of the laminar solution to small disturbances (2). Detailed experimental results are not available for validation. However the only source of error is numerical: an approximate treatment of the boundary-layer growth is not needed here as it was in Ref. 3. The numerical errors can be reliably estimated by conducting simulations with improved resolution, enlarged domains, and so on, and by using the experience gained while simulating other flows (3, 4). The agreement with well-established laws (e. g., the log law) also helps build confidence in the numerical results.

TENTATIVE THEORY OF THE FLOW

The theory is tentative in that it is based on assumptions which are plausible and consistent with current thinking, but cannot be rigorously proven. As is often the case in turbulence, only necessary conditions will be obtained. Also, the evidence supporting the theory is encouraging, but still limited. We focus on the mean velocity $U[y, t]$ and the total shear stress $\tau[y, t]$. They are linked by the momentum equation, $U_t - U_{\infty t} = \tau_y$. For clarity we use the following notation: square brackets surround the arguments of a function, while parentheses group terms in an expression. Most of the derivation can be generalized to other laws than $\cos[\omega t]$ for U_∞/U_0 .

Define the phase ϕ and the length scale L . Dimensional analysis shows that U and τ must have the following form:

$$U[y, t] - U_\infty[t] = U_0 f_1 \left[\frac{y}{L}, \phi, Re \right] \quad (3a)$$

$$\tau[y, t] = U_0^2 f_2 \left[\frac{y}{L}, \phi, Re \right] \quad (3b)$$

for some nondimensional functions f_1 and f_2 . Recall that the averages are taken over x and z with sufficiently large domains and by phase-averaging. The momentum equation and boundary condition become

$$\frac{\partial f_1}{\partial \phi} = \frac{\partial f_2}{\partial (y/L)}, \quad f_1[0, \phi, Re] = -\frac{U_\infty}{U_0}[\phi]. \quad (4)$$

So far no approximations have been made. The functions f_1 and f_2 are functions of three variables; the objective is to separate the dependence on Re from the other two as much as possible.

Outer region

The Reynolds-number-similarity hypothesis (5) asserts that, away from the wall, the gross features of the turbulence (at least U and τ , which do not depend strongly on the small-scale motion) can be independent of the Reynolds number provided that proper velocity- and length scales u^* and δ (different from U_0 and L) are chosen to normalize them. In the outer region we replace Eq. (3) by

$$U[y, t] - U_\infty[t] = u^* f_3 \left[\frac{y}{\delta}, \phi, Re \right], \quad (5a)$$

$$\tau[y, t] = u^{*2} f_4 \left[\frac{y}{\delta}, \phi, Re \right]. \quad (5b)$$

This equation is just as general as Eq. (3), since u^*/U_0 and δ/L are functions of Re , but f_3 and f_4 are now of order 1, as is the range of y/δ over which most of their variation occurs. We can define u^* as $\sqrt{\tau_{max}}$ where τ_{max} is the peak value of the shear stress at the wall during the cycle. For δ there is no such obvious, quantitative definition (especially since the flow does not have a sharp laminar-turbulent interface). Since the time scale is $1/\omega$, δ must be proportional to u^*/ω . We can use this to define δ . We are free to choose the value of the ratio, and we choose 1. Therefore:

$$\delta \equiv \frac{u^*}{\omega}. \quad (6)$$

Thus δ is proportional to the thickness of the turbulent region, but not equal to it. Because of Eq. (6), f_3 and f_4 satisfy an equation analogous to Eq. (4(a)), simply replacing L with δ .

We now introduce the major assumption: the only dependence of f_3 and f_4 on Re is a phase shift $\phi_0[Re]$ (as we shall see, the theory is too limited if we assume that f_3 and f_4 do not depend on Re at all). The idea behind this assumption is that at different Reynolds numbers $U - U_\infty$ and τ (scaled with u^* and δ) may have the same behavior, but not at exactly the same phase relative to U_∞ . The assumption is expressed as follows:

$$f_3 \left[\frac{y}{\delta}, \phi, Re \right] = f_3 \left[\frac{y}{\delta}, \phi + \phi_0[Re] \right], \quad (7a)$$

$$f_4 \left[\frac{y}{\delta}, \phi, Re \right] = f_4 \left[\frac{y}{\delta}, \phi + \phi_0[Re] \right]. \quad (7b)$$

Note that f_3 and f_4 are functions of only two variables. On the other hand we have introduced three new functions of Re : u^*/U_0 , δ/L and ϕ_0 (but recall that the first two are related by Eq. (6)).

Inner region

Here we apply the usual arguments. The variation of τ with y is neglected, so $\tau[y, t] \approx \tau[0, t]$, and the momentum equation is not considered. Define $u_\tau \equiv \sqrt{\tau[0, t]}$ where the square root is taken to have the sign of the argument. The velocity U is assumed to follow the law of the wall:

$$U = u_\tau f_\tau \left[\frac{y|u_\tau|}{\nu} \right]. \quad (8)$$

Clearly when the wall shear stress reverses ($\tau[0, t]$ vanishes), this assumption breaks down. The theory will not apply near the phase of reversal, but this may not have much effect on the rest of the cycle.

Overlap argument

In the overlap region both Eq. (7a) and Eq. (8) are assumed to be valid and we obtain

$$\frac{U_0}{u^*} \frac{U_\infty}{U_0}[\phi] + f_3 \left[\frac{y}{\delta}, \phi + \phi_0 \right] = \frac{u_\tau}{u^*}[\phi + \phi_0] f_\tau \left[\frac{y|u_\tau|}{\nu} \frac{u^* \delta}{\nu} \right]. \quad (9)$$

To exploit the overlap argument we can, for instance, vary Re in Eq. (9) while holding y/δ and $\phi + \phi_0$ fixed. We obtain

$$\frac{U_\infty}{U_0} \frac{d}{dRe} \left(\frac{U_0}{u^*} \right) - \frac{U_0}{u^*} \frac{d}{d\phi} \left(\frac{U_\infty}{U_0} \right) \frac{d\phi_0}{dRe} = \frac{u_\tau}{u^*} \frac{df_\tau}{d(\log[y^+])} \frac{d(\log[u^* \delta / \nu])}{dRe}. \quad (10)$$

The only term that depends on y is the last one, which contains $df_\tau/d(\log[y^+])$. Therefore this quantity must be a constant, e.g., $1/\kappa$; again the overlap argument predicts a log layer ($f_\tau = \log[y^+]/\kappa + C$).

The reason $\phi_0(Re)$ was introduced is not apparent. Consider the variation of the various terms in Eq. (10) as a function of ϕ . If ϕ_0 were independent of Re , the second term would be 0. Then during the cycle, u_τ/u^* (the third term) would be proportional to U_∞/U_0 (first term), so that the wall shear stress would have to have the same phase as the freestream velocity, which is physically not correct. The variable- ϕ_0 model allows the deceleration to enter through $d(U_\infty/U_0)/d\phi$ (second term) and make the wall stress "lead" the freestream velocity and reverse earlier (if $d\phi_0/dRe < 0$).

Dependence on ϕ and ϕ_0

We conclude the analysis by exploiting the dependence of Eq. (10) on ϕ and ϕ_0 . Using Eq. (1) we see that the left-hand-side is proportional to $\cos(\phi + \phi_1)$ with ϕ_1 defined by $\tan[\phi_1] \equiv d\phi_0/d(\log[u^*/U_0])$. The right-hand-side is proportional to u_τ/u^* which is a function of $\phi + \phi_0$. Therefore $\phi_1 - \phi_0$ is a constant. Since ϕ_0 is meaningful only up to an additive constant (see Eq. (7)), we can choose the constant so that $\phi_0 = \phi_1$. Consequently $\tan[\phi_0] = d\phi_0/d(\log[u^*/U_0])$, which integrates to

$$\sin[\phi_0] = A \frac{u^*}{U_0} \quad (11)$$

where A is a constant. Also, u^* was defined so that the peak value of u_τ/u^* is 1. Therefore

$$\frac{u_\tau}{u^*} = \cos[\phi + \phi_0]. \quad (12)$$

Finally, rearranging Eq. (10) and using Eq. (6) to eliminate δ ,

$$-\left(\frac{A\kappa}{2 \sin[\phi_0]} + \cos[\phi_0] \right) \frac{d\phi_0}{\sin[\phi_0]} = \frac{dRe}{Re}. \quad (13)$$

This integrates to

$$\frac{\kappa U_0}{2 u^*} \cos[\phi_0] + \log \left[\frac{U_0}{u^*} \right] = \log[Re] - B \quad (14)$$

where B is a constant. It turns out that ϕ_0 is small, of the order of 0.15 radians, so that $\cos[\phi_0] \approx 0.99$. If it is replaced by 1, Eq. (14) involves only u^*/U_0 and Re .

Equations (11), (12), and (14) provide strong predictions that can be checked against sufficiently accurate simulations. Such a check will also provide the values of A and B . The theory predicts that as $Re \rightarrow \infty$, u^*/U_0 , δ/L , and ϕ_0 all tend to 0, although slowly (roughly like $1/\log(Re)$, as in other flows). Also note that the nondimensional shear-stress gradient $d\tau^+/dy^+$ is of order $(U_0/u^*)^2/Re^2$; it also tends to zero as $Re \rightarrow \infty$ so that the "almost-constant-stress" assumption for the inner region becomes more and more valid.

The known limitations of the theory are that it applies only at sufficiently high Reynolds number and that it does not apply near the phase of reversal of the wall shear stress. This failure near reversal is obvious since Eq. (12) predicts that τ has a double zero when it reverses, which is counterintuitive and is not indicated by the simulation results. It may be possible to extend the theory to cover the reversal region by matching asymptotic expansions, but this has not yet been achieved.

DIRECT-SIMULATION RESULTS

The numerical method used to solve the time-dependent, three-dimensional, incompressible Navier-Stokes equations is described in detail in Ref. 6. It is fully spectral in space and second-order-accurate in time. The method was further tested by solving the linear stability equations for the laminar solution using Floquet theory (in that case the time integration used a fourth-order-accurate, implicit, reversible scheme). The results obtained by Hall (7) with a very different method were reproduced, which shows that the spectral basis functions that are used are well adapted to the flow. The results indicate linear stability at all of the Reynolds numbers and wave numbers that were investigated (up to $Re = 2000$). For the turbulent simulations, the boundary condition (Eq. 1) is most simply enforced by solving for the difference between the flow and the laminar flow U_l ; this difference satisfies homogeneous boundary conditions at $y = 0$ and $y \rightarrow \infty$.

The periods are $\Lambda_x = 0.12L$ and $\Lambda_z = 0.06L$ (about $60\delta_l$ and $30\delta_l$). The resolution is as follows. In the y -direction there are 10 collocation points within about 10 wall units of the wall. In the x - and z -directions the spacing is about 20 and 7 wall units, respectively. Random numbers are used as initial disturbances in order to break any symmetries in the flow field. Their amplitude has to be large enough; otherwise the flow remains laminar (recall that it is linearly stable). The initial transient takes about one cycle and is not included in the phase averages. The parity under the transformation $\phi \rightarrow \phi + \pi$ is used to double the sample (averages are of course taken over x and z as well).

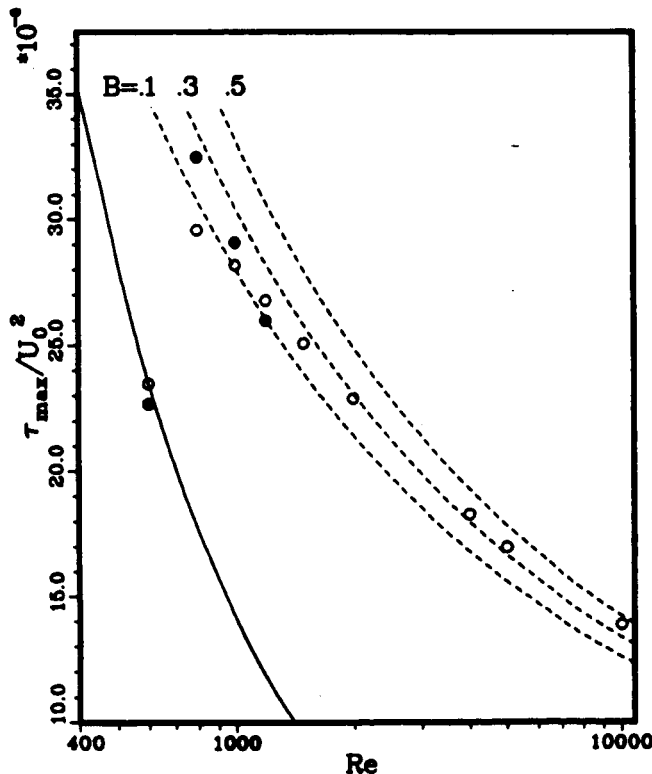


Fig. 1. Peak wall shear stress vs. Reynolds number. — laminar flow; --- Eq. (14); ● direct simulations; ○ turbulence model.

Figure 1 shows τ_{max}/U_0^2 as a function of Re . The laminar solution and the curves corresponding to several values of B in Eq. (14) are shown. Direct simulations were conducted at $Re = 600, 800, 1000, \text{ and } 1200$. The trend from 800 to 1200 is steeper than predicted by the theory. The range of Reynolds number is too narrow for one to conclude whether the theory is invalidated by the results, or whether the disagreement is simply a low-Reynolds-number effect. The results obtained with the turbulence model are included in the figure, but will be discussed later.

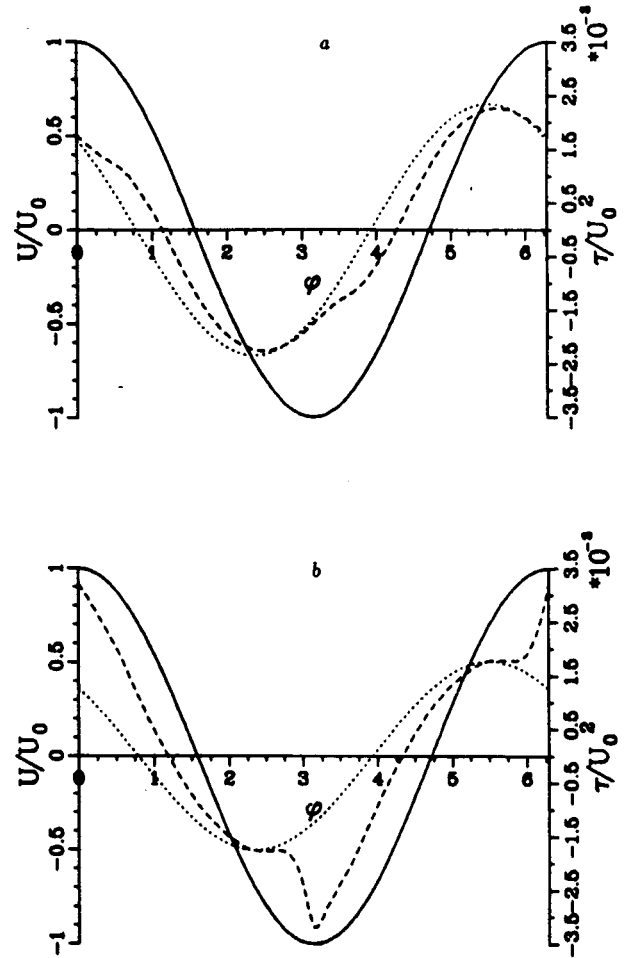


Fig. 2. Freestream velocity and wall shear stress vs. phase angle. — U_∞/U_0 ; ··· τ in laminar flow; --- τ in turbulent flow. a) $Re = 600$; b) $Re = 800$.

At $Re = 600$, the peak wall stress is close to the laminar value, but the flow is not laminar. Figure 2(a) compares the turbulent wall stress to the laminar solution; they differ significantly during the deceleration phase. Reversal occurs much later in the turbulent flow. The average power consumption per unit area, normalized by U_0^3 , is about 0.98×10^{-3} in the turbulent flow compared with 0.83×10^{-3} in the laminar flow. The flow is clearly not laminar, but is also far from being well-developed turbulence. The velocity profile never displays a log layer and the anisotropy of the Reynolds-stress tensor is abnormal. Monkewitz and Bunter (8) visually observed finite-amplitude disturbances, also near the phase of reversal, starting between $Re = 554$ and 647 .

Between Reynolds number 600 and 800 a second transition occurs. Figure 2(b) shows that the wall stress is now high dur-

ing the high-freestream-velocity phase. It now has a sharp peak with a value much larger than in the laminar flow, and the power consumption is 86% larger than in laminar flow. Strong turbulence develops around $\phi = 2.8$; a log layer forms in the velocity profile near $\phi = 0$ and is maintained well into the deceleration phase, around $\phi = 0.7$. Reversal now occurs near $\phi = 1.25$. The results at $Re = 1000$ are similar, but the peak in the wall stress is much wider. Turbulence during the peak-velocity phase was observed in experiments by Merkli and Thomann (9) but their Reynolds number was much lower, about 300. See also Hino, Sawamoto and Takasu's experiments in a pipe (10).

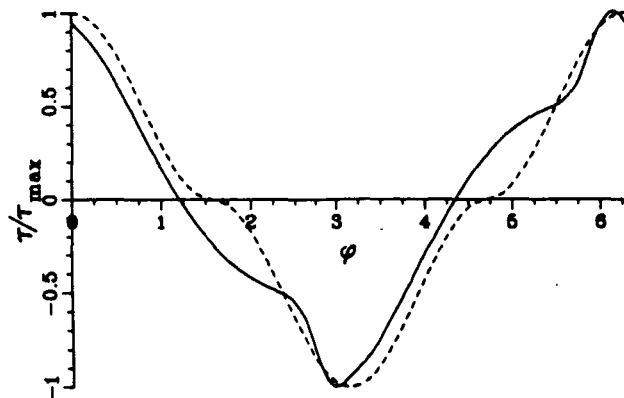


Fig. 3. Wall shear stress vs. phase angle. $Re = 1000$.
— τ/τ_{max} ; --- $\cos(\phi)|\cos(\phi)|$.

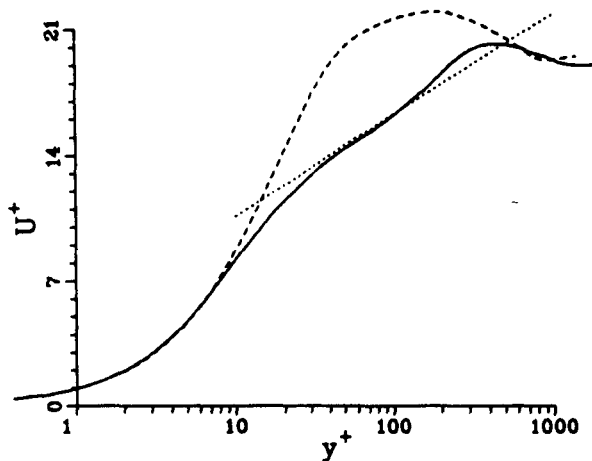


Fig. 4. Mean velocity vs. distance from the wall. $Re = 1000$.
— $\phi = 0$; --- $\phi = 2.44$; ... $\log[y^+]/0.41 + 5$.

The agreement with Eq. (12) is tested in Fig. 3. One expects τ/τ_{max} to have the same shape as $\cos(\phi)|\cos(\phi)|$, only shifted to the left. This is observed only for ϕ between about -0.3 and 1. This is also the range of phases in which a log layer is observed. Figure 4 shows a log layer at $\phi = 0$, but not at $\phi = 2.44$. The profile at $\phi = 2.44$ is laminar-like: $U^+[y^+]$ is far above the usual log layer. During the acceleration phase, the favorable pressure gradient delays the development of the turbulence considerably. Transition does not occur until the pressure gradient falls below about 0.02, in wall units based on the current wall shear stress, even though the near-wall layer is subjected to strong disturbances from the turbulence remaining farther from the wall. Thus one can attribute the lack of agreement with Eq. (12) during that phase to low-Reynolds-number effects. This lack of agreement and the narrow

range of Reynolds numbers make an accurate check of Eq. (11) impossible; one can just note that the value of A is of the order of 3.

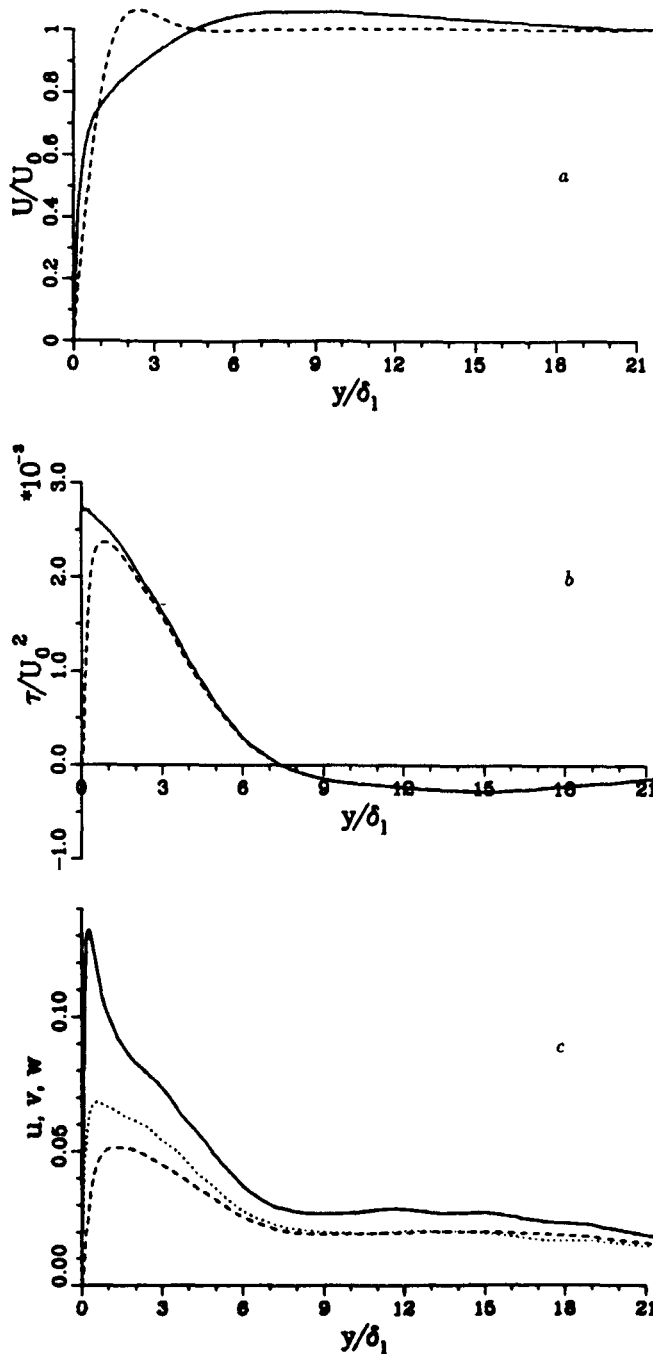


Fig. 5. Profiles in $Re = 1000$ flow, $\phi = 0$. a) Velocity U/U_0 ; — turbulent, --- laminar. b) Shear stress τ/U_0^2 ; — total stress, --- Reynolds stress. c) turbulence intensities u'/U_0 , etc.: — u' , --- v' , ... w' .

Other aspects of the flow will now be described using the $Re = 1000$ case, for which the best sample (four half-cycles) happens to be available. Figure 5 shows at $\phi = 0$ the mean velocity, the shear stress, and the turbulence intensity in each component. The near-wall behavior is very similar to that of the usual boundary layers, but away from the wall the shear stress crosses 0 and returns to it only slowly, and the intensities have very long "tails". They extend far beyond the region with significant mean shear U_y . This is caused by the lack of entrainment. Notice also how a local

minimum in the turbulence intensity, a zero crossing of the shear stress, and a zero crossing of the mean shear U_y , all coincide near $y/\delta_l = 8$. As a rule, the zero crossings of the stress and the shear tend to follow each other. Since they imply that the turbulent-energy production is 0, they explain the minimum in the energy.

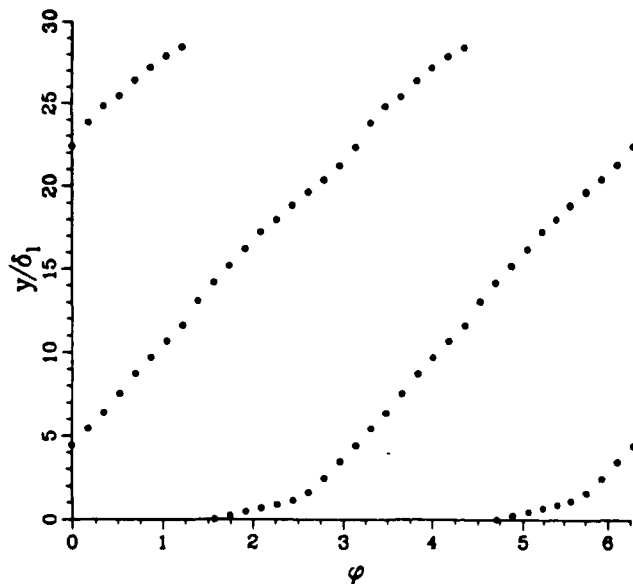


Fig. 6. Zero crossings of $U - U_\infty$ vs. phase angle. $Re = 1000$.

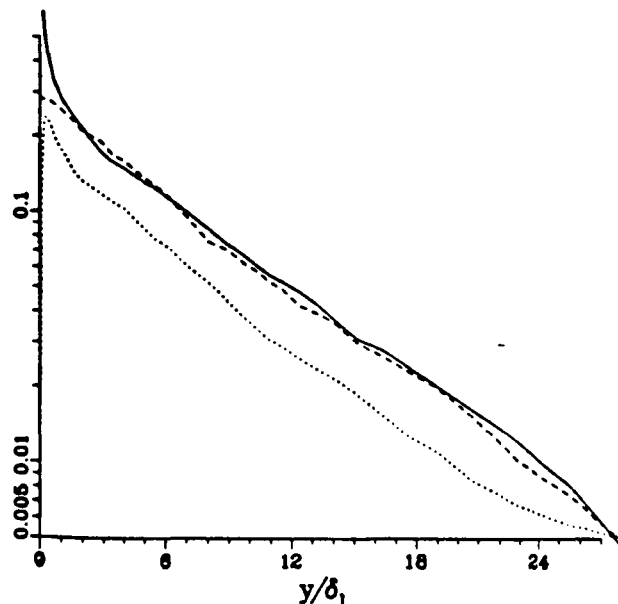


Fig. 7. Peak value of various quantities over a cycle, vs. y . $Re = 1000$. — $(U - U_\infty)$; - - - $100 \times \tau$; ··· $10 \times (u'^2 + v'^2 + w'^2)$. Normalized by U_0 .

The results further show that the structure of the turbulence (for instance the anisotropy of the Reynolds-stress tensor) at different values of y/δ is quite similar. The zero crossings of the stress τ , of the mean shear U_y , and of the deviation from freestream $U - U_\infty$ all propagate away from the wall at roughly constant velocity, except close to the wall. Figure 6 shows that the $U = U_\infty$ point starts from the wall at $\phi = \pi/2$ with a slope of 1 (the laminar value), and that near $\phi = 2.5$ its velocity abruptly increases to about 6. The peak values of τ , the turbulent energy, and $U - U_\infty$ over a cycle also decay exponentially as functions of y/δ (Fig. 7). The decay rate is about 7 times smaller than in laminar flow. Thus there is a strong analogy with the laminar

flow (Eq. 2); the “eddy viscosity” would be uniform at about 40 times the molecular viscosity (at $Re = 1000$).

These findings were somewhat surprising. It was expected that the propagation velocity of the waves would scale with the local velocity scale, and therefore decrease rapidly away from the wall. For the peak values of $U - U_\infty$ and τ , an algebraic decay seemed more likely. Note that a constant viscosity scale and an exponential decay of the velocity scale imply an exponential growth of the length scale. On the other hand, it was found that in the Reynolds-stress budgets, the role of the various terms did change with y : near the wall the usual terms dominate but away from it, the turbulent-diffusion term becomes much stronger. Thus the similarity is not complete. Even so, the behavior in Figs. 6 and 7 ought to be explained.

To further document the behavior of the turbulence the $k - \epsilon$ model was applied to the flow. The high-Reynolds number version of the model was used with standard values for the constants ($C_\mu = 0.09$, $C_{\epsilon 1} = 1.45$, $C_{\epsilon 2} = 1.9$, $\sigma_k = 1$, $\sigma_\epsilon = 1.3$) (11). Only the region $y > 2\delta_l$ was considered: boundary conditions for U , k and ϵ at $y = 2\delta_l$ were taken from the direct simulations ($Re = 1000$). Thus near-wall corrections were not needed. For large y trivial conditions were used ($U = U_\infty$, $k = \epsilon = 0$). The $k - \epsilon$ results were in very good agreement with the direct simulations, including the uniformity of the eddy viscosity. The agreement was further improved by a slight adjustment of C_μ , to 0.085. The direct-simulation results also suggested lower values for σ_k , around 0.8, but such values did not alter the results noticeably. This exercise shows that, excluding the wall region, the oscillating boundary layer is within the reach of the high-Reynolds-number $k - \epsilon$ model. Thus, near-wall corrections to the model could be tested with confidence that the outer region is treated properly.

ALGEBRAIC-TURBULENCE-MODEL RESULTS

The eddy-viscosity model used in this paper is algebraic in the sense that the eddy viscosity in a given profile is a specified function. However, one of the parameters depends on the phase angle (in other problems it could depend on time or on the streamwise coordinate) and is determined from solution of an ordinary differential equation. The development of the model follows the procedure originated by Johnson and King (12), but differs in detail. The structure parameter is used to convert the turbulent-energy equation to an equation for τ , which is integrated over the profile to obtain an ordinary differential equation. Models of this type can exhibit transition and relaminarization properties in contrast to conventional algebraic models. A complete description will be given elsewhere.

The peak wall stress obtained with the model between $Re = 800$ and 10,000 was shown in Fig. 1. Where the direct-simulation and turbulence-model results overlap, the agreement is acceptable. In that range both sets of results disagree with Eq. (14) since they do not follow a $B = \text{constant}$ curve. When Re exceeds about 4,000, the agreement between the model and Eq. (14) is seen to improve. This suggests that the discrepancy for Re of the order of 1000 is indeed due to low-Reynolds-number effects, for which the theory is not expected to account. The value of B would then be between 0.3 and 0.5. On the other hand the Reynolds-number-similarity hypothesis and the law-of-the-wall hypothesis, which are central to the theory, are also “built into” the turbulence model. In that sense, the model does not provide a truly independent check of the theory. It is still very useful in assessing the low-Reynolds-number effects, which the direct simulations will be unable to do in the near future because of their excessive cost. Note also that the model predicted relaminarization, between $Re = 800$ and 600.

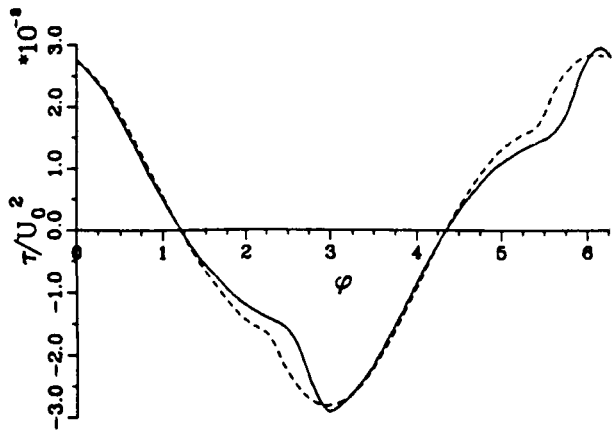


Fig. 8. Wall shear stress vs. phase angle. $Re = 1000$. — direct simulation; - - - turbulence model.

Figure 8 compares the evolution of the wall stress at $Re = 1000$, computed by direct simulation and with the model. The agreement is very good; the model even predicts the quiescent phase around $\phi = 2$ and the surge after $\phi = 2.5$ (although the surge occurs slightly earlier with the model). The agreement away from the wall (velocity profiles, etc.) is also good. Finally, Fig. 9 shows τ/τ_{max} versus ϕ at $Re = 10,000$. The curve follows Eq. (12) well for a much longer part of the cycle than at $Re = 1000$ (roughly, from $\phi = -1$ to $\phi = 1$). The phase shift ϕ_0 is also smaller. The predictions of the model are quite consistent with the theory.

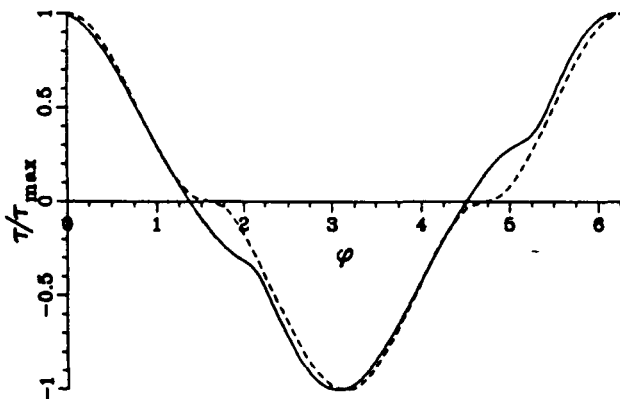


Fig. 9. Wall shear stress vs. phase angle. $Re = 10,000$. — τ/τ_{max} ; - - - $|\cos(\phi)|\cos(\phi)$.

CONCLUSIONS

The oscillating boundary layer displays a complex behavior, both as a function of phase angle and of Reynolds number. Although it is believed to be linearly stable, it exhibits a first transition to a "pre-turbulent" state just below a Reynolds number of 600. A second transition, between 600 and 800, allows it to generate well-developed turbulence during at least part of the cycle. During that part of the cycle, it contains a log layer and agrees with other aspects of a high-Reynolds-number theory that was also presented. Thus the theory is confirmed to some extent by the direct-simulation results. These results even suggest that the theory could be simplified further, which does not seem to be justified by traditional arguments but is also supported by predictions of the $k - \epsilon$ model. A new algebraic turbulence model, designed and calibrated on the present flow, yielded satisfactory agreement with the direct simulations and with the theory in spite of the complexity of the flow.

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16. Abstract The turbulent boundary layer driven by a freestream velocity that varies sinusoidally in time around a zero mean is considered. The flow has a rich behavior including strong pressure gradients, inflection points, and reversal. A theory for the velocity and stress profiles at high Reynolds number is formulated. Well-resolved direct Navier-Stokes simulations are conducted over a narrow range of Reynolds numbers, and the results are compared with the theoretical predictions. The flow is also computed over a wider range of Reynolds numbers using a new algebraic turbulence model; the results are compared with the direct simulations and the theory.			
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