Directed percolation phase transition to sustained turbulence in Couette flow

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Turbulence is one of the most frequently encountered nonequilibrium phenomena in nature, yet characterizing the transition that gives rise to turbulence in basic shear flows has remained an elusive task. Although, in recent studies, critical points marking the onset of sustained turbulence¹⁻³ have been determined for several such flows, the physical nature of the transition could not be fully explained. In extensive experimental and computational studies we show for the example of Couette flow that the onset of turbulence is a second-order phase transition and falls into the directed percolation universality class. Consequently, the complex laminar-turbulent patterns distinctive for the onset of turbulence in shear flows^{4,5} result from short-range interactions of turbulent domains and are characterized by universal critical exponents. More generally, our study demonstrates that even high-dimensional systems far from equilibrium such as turbulence exhibit universality at onset and that here the collective dynamics obeys simple rules.

In basic shear flows (pipe, channel, Couette and boundary laver flows) the onset of turbulence is characterized by the sudden occurrence of chaotic domains⁴ that coexist and compete with laminar motion, resulting in irregular continually changing flow patterns (Fig. 1). In this first manifestation, turbulence is sustained, yet intrinsically patchy, and the state of space-filling fully turbulent motion typical for larger Reynolds numbers is not yet stable⁶. The earliest attempts to explain the initial appearance of turbulence were largely concerned with the linear stability of the laminar flow⁷⁻¹⁰, and later studies took the potential of perturbations to exhibit transient growth^{11,12} into account. More recently, much progress has been made regarding the microscopic flow structures (building blocks) underlying the chaotic motion¹³⁻¹⁸; however, these advances have provided limited insights into the macroscopic transition process. Analogous to phase transitions in thermodynamics it may be expected that the nature of the transition is instead determined by large-scale correlations which do not depend on the details of the microscopic interactions but rather on their collective behaviour. Such concepts are well established for phase transitions in equilibrium statistical mechanics; turbulence, on the other hand, is dissipative and hence not in equilibrium. Although, generally, non-equilibrium systems are much more abundant, there is surprisingly little experimental confirmation of predicted universal characteristics¹⁹⁻²¹.

Possible analogies between the onset of turbulence and certain classes of non-equilibrium phase transitions, more specifically the so-called directed percolation (DP) universality class, were first pointed out 30 years ago by Pomeau²². A simple realization of DP is bond percolation. Here, an active state can spread by

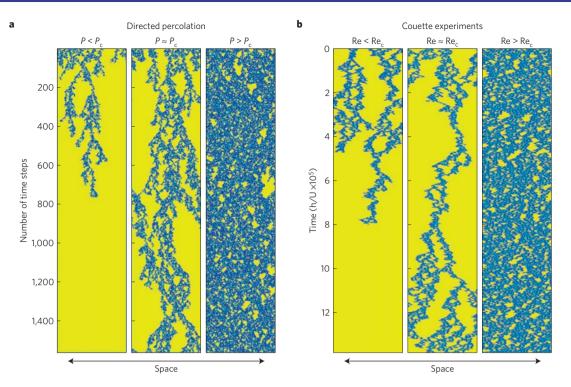
means of connected bonds on a fixed grid with a probability P, and proliferation can take place only by nearest-neighbour interaction. Similarly, the spreading of turbulence in shear flows is a contact process: owing to the linear stability of the laminar state, turbulence cannot arise spontaneously, but only through interaction with domains that are already turbulent. Percolation is governed solely by the probability P and, analogously, the transition to sustained turbulence, and the likelihood of turbulence to spread, is governed by a single parameter—in this case the Reynolds number, Re = Uh/v, where U is half the wall speed difference, h half the gap between the walls and ν the kinematic viscosity. In DP there is an exact critical point, $P = P_{c}$, below which the system will always return to the passive state (Fig. 1a, left panel), whereas at $P = P_c$ (Fig. 1a, mid panel) a continuous phase transition occurs and for $P > P_c$ (Fig. 1a, right panel) the fraction of active states is strictly greater than zero (in the thermodynamic limit). There are certain requirements that need to be fulfilled for DP, such as the absence of long-range interactions, the absence of additional symmetries or conservation laws, and the existence of a unique absorbing state (the laminar state in Couette flow qualifies as an absorbing state owing to its linear stability). Indeed, it has been conjectured that these are not only necessary but also sufficient criteria for DP (refs 23,24). More generally, the DP universality class is believed to play a central role for non-equilibrium phenomena, ranging from transport in porous media to the spreading of epidemics or forest fires¹⁹. However, so far only a single experimental verification for the rather specific case of liquid crystal electro-convection²⁵ has been possible.

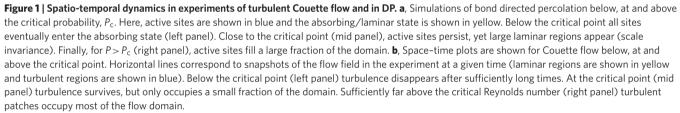
Regarding a possible connection between turbulence and DP, analogies have been discussed in a variety of studies considering model systems^{26–30}. However, in the only detailed experimental study, a discontinuous first-order transition was reported, disagreeing with the continuous DP type transition scenario. These experiments were carried out for Couette flow, where a fluid is sheared between two moving walls^{31,32}. Equally, simulations of the same flow^{33,34} reported a non-universal first-order transition.

More recently, however, in an investigation of pipe flow¹ the critical point for the onset of sustained turbulence could be determined and it was shown that the time and length scales relevant close to the critical point are much longer than expected— and, in particular, also much larger than those considered in refs 31–34. In the case of pipe flow these excessively long timescales make it virtually impossible to determine the nature of the transition. An analogous study was performed for Couette flow² in a slender (spanwise) but long (streamwise) domain, and here the relevant timescales (that is, characteristic decay and spreading times of turbulent stripes) close to the critical point are three orders of magnitude smaller than in pipes. Resolving these scales

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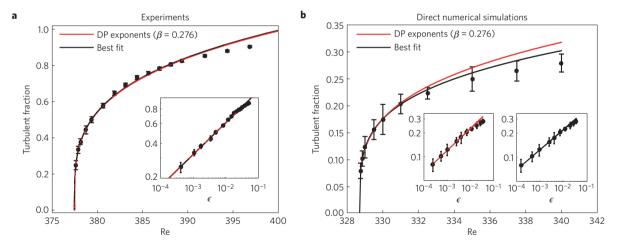


Figure 2 | Scaling of the turbulent function Equilibrium turbulent fraction as a function of Re: experiments (**a**) and direct numerical simulations (DNS) (**b**). The turbulent fraction (TF), that is, the percentage of the flow that is turbulent, is the order parameter of the transition to sustained turbulence. As the critical point (Re_c \approx 328.7 in simulations and Re_c \approx 377.5 in experiments) is surpassed, TF increases continuously, and close to the critical point it follows a power law. In experiments the best fit results in an exponent of $\beta \sim 0.28$ (black curve in **a**), whereas in simulations we obtain an exponent of $\beta \sim 0.25$ (black curve in **b**). These values are close to the universal DP exponent (0.276) and fits with a fixed exponent of 0.276 are shown in red. In the numerical simulations, domain sizes were increased when approaching the critical point. For Re < 329, simulations were carried out in domains 1920*h* wide (using 12,288 Fourier modes). For 329 < Re < 334, a domain size of 960*h* (6,144 Fourier modes) was chosen, and for Re > 334 a domain size of 480*h* (3,072 Fourier modes) was chosen. 48 Fourier modes were used in the stripe direction and 32 grid points in the wall-normal direction for all runs. Errors bars represent the standard deviation.

sufficiently close to the critical point resulted in scale-invariant flow patterns, which in contrast to the aforementioned studies³¹⁻³⁴ is a signature of a continuous, second-order transition. In the following

we report detailed experiments and extensive direct numerical simulations (DNS) for Couette flow and show that the transition to turbulence is a non-equilibrium phase transition, falling into

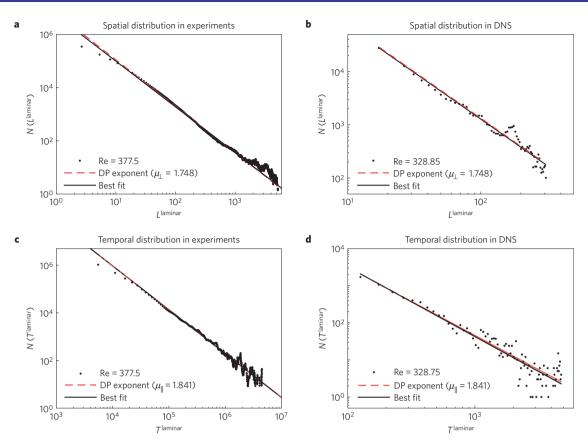


Figure 3 | **Distribution of laminar gaps in space and time.** The critical exponents governing the spatial and temporal correlations are determined by analysing long runs close to the critical point. Here the distributions of the laminar gaps interspersing turbulent sites are scale invariant and follow universal power laws (empty interval exponents). **a,b**, Distribution of laminar gaps (L^{laminar}) in space from experiments (Re = 377.5) (**a**) and from direct numerical simulations (DNS) (Re = 328.85) (**b**). The slopes correspond to the so-called spatial empty interval exponent, and the best fit to the experimental data results in a value of -1.72, whereas in simulations we obtain -1.75. The universal value of DP is $\mu_{\perp} = 1.748$, where $N(L) \sim L^{-\mu_{\perp}}$. **c,d**, The empty interval exponent governing the gap duration (T^{laminar}) in the time direction is shown for experiments (**c**), giving a slope of -1.84, and for DNS (**d**), where the slope is -1.85. The universal exponent for DP is $\mu_{\parallel} = 1.84$, with $N(T) \sim T^{-\mu_{\parallel}}$ and is hence in excellent agreement.

the DP universality class. Experiments are carried out in a circular Couette geometry, where the fluid is held in the gap between two concentric cylinders. An advantage of this geometry is the periodic boundary condition in the streamwise (azimuthal) direction, which in contrast to pipes and channels allows unlimited observation times. In addition to very long observation times, measurements require very large aspect ratios, as the relevant length scales are expected to diverge at the critical point. The azimuthal aspect ratio (circumference/gap) is maximized by making the radius ratio $\eta = r_i/r_o$ as near to unity as possible. Hence the main experimental difficulty is to keep a high relative precision of the very narrow gap (and hence Reynolds number) needed to achieve a large azimuthal aspect ratio. In our experiment, $\eta = 0.998$, which is very close to the planar Couette case ($\eta = 1$) and yields an azimuthal aspect ratio of \sim 5,500 (see Supplementary Information for details). In the axial direction the fluid is confined by a top and a bottom end-wall (attached to the inner cylinder) and the axial aspect ratio (cylinder height/h) is 16. To ensure a constant Reynolds number \pm 0.25 over the long observation times, viscosity changes of the working fluid had to be minimized and hence its temperature controlled. This was achieved by circulating fluid of constant (to within ± 0.02 K) temperature around the outside of the outer cylinder and on the inside of the inner cylinder. As working fluid, a low-viscosity (1cSt at 20 °C) silicone oil was chosen, which has an approximately five times smaller viscosity change with temperature in comparison to water. The current experimental set-up is a modification of a previous apparatus³⁵ (details of the present modifications are

given in the Supplementary Methods). The DNS of Couette flow was performed with the hybrid code nsCouette³⁶ and a domain of $1,920 \times 10 \times 2$ (where the small dimension corresponds to the radial gap width) was chosen. Turbulent stripes in Couette flow are not perpendicular to the main flow (that is, azimuthal) direction. To maximize the number of stripes that can be contained in the simulated volume, we tilted the domain (by 24°) so that the long direction of the box is perpendicular to the turbulent stripes. In simulations and experiments, the elongation of the domain is essential, as it determines the number of turbulent stripes that can be accommodated. In analogy to DP, the number of stripes corresponds to the number of sites. As the distances between active sites in DP diverge when the critical point is approached, so do the laminar gaps increase between stripes in Couette flow (see Fig. 1b).

Experiments and numerical simulations followed the same procedure. First, a turbulent flow was initiated at slightly larger Re (typically Re = 400 in simulations and Re = 625 in experiments). Note that in the experiments the fluid is confined between top and bottom end-walls and, as a consequence, turbulence is observed only at higher Re than in the simulations (where periodic boundary conditions are applied). Once a turbulent flow was established, Re was reduced (quench experiments) to a value close to the critical point. The flow was then left to evolve and, after initial transients decayed, the percentage of the domain that is in turbulent motion (that is, the turbulent fraction TF) was measured and averaged over long times. TF here plays the role of the order parameter and is zero below and non-zero above the critical point (see Fig. 1b). Depending

on whether the transition is of first or second order, TF should vary either discontinuously or continuously as the critical point is passed.

In the experiments, for each Re, the turbulent fraction was averaged over at least 10^5 advective time units (tU h⁻¹) and the regime 375 < Re < 400 was investigated. As shown in Fig. 2, with decreasing Re, TF decreases continuously. The given system size allowed measurements only for turbulent fractions $> \sim 15\%$. For smaller values, fluctuations were as large as the typical number of stripes. As expected at a second-order transition, the variation of TF follows a power law, $TF \sim \varepsilon^{\beta}$ (where $\varepsilon = (\text{Re-Re}_{c})/\text{Re}_{c}$ and Re_{c} is the critical point). The exponent is very close to the universal value for directed percolation in 1+1 dimensions (the best fit results in $\beta = 0.28 \pm 0.03$, whereas the universal value for DP is 0.276). Likewise, in the simulations, a power law is observed and the measured exponent, $\beta = 0.25 \pm 0.04$, is again close to the universal one. Although in principle an investigation of finite-size scaling, that is, the variation of the scaling relations with system size, would allow one to overcome the above restrictions, such studies pose a considerable challenge in experiments, and cannot be carried out with the present set-up.

Apart from the scaling of the order parameter, two additional critical exponents are needed; we here chose the so-called empty interval exponents, μ_{\perp} and μ_{\parallel} , which describe the distribution of laminar/empty gaps at the critical point in space and time. The spatial exponent is determined from the slope of the distribution of laminar gap sizes at Reynolds numbers closest to the critical point (Fig. 3a,b). For the experiments $\mu_{\perp} = 1.72 \pm 0.05$, whereas for the simulations $\mu_{\perp} = 1.75 \pm 0.02$. These values are in very good agreement with the universal critical exponent in DP ($\mu_{\perp} = 1.748$).

In analogy, the temporal empty interval exponent is determined from the distribution of laminar time intervals (Fig. 3c,d). Close to critical these should follow a power law with a slope μ_{\parallel} . The best fit to the experimental data yielded $\mu_{\parallel} = 1.84 \pm 0.02$, whereas in the DNS study $\mu_{\parallel} = 1.85 \pm 0.02$ was obtained. These are in excellent agreement with the critical exponent of DP ($\mu_{\parallel} = 1.84$). A summary of the measured and expected exponents is given in Table 1. Hence, exponents from experiments as well as from computer simulations indicate a second-order phase transition, and the obtained values are in very good agreement with the DP universality class in 1+1D.

In addition, a further prediction from DP regarding the time evolution of the order parameter (in our case TF(t)) could be tested for the experimental data. Starting from a fully occupied system, DP predicts that on quenching the control parameter to different values in the vicinity of the critical point, all time-series TF(t) should collapse to a single curve (on a simple rescaling). As shown in Supplementary Fig. 2, the data sets indeed collapse as predicted, providing further evidence that onset of sustained turbulence in Couette flow falls into the DP framework. In principle, the collapse experiments provide an independent way of determining the critical point, and allowed us to confirm that the critical Re is within \pm 0.5 of the value determined above (Fig. 2a). However, the relatively large scatter of the data unfortunately prohibits a more accurate estimate.

Despite numerous studies, the nature of the onset of turbulence in shear flows had remained unresolved since the nineteenth century. In early studies (for example, by Kelvin, Rayleigh, Lorentz and Heisenberg³⁷) attempts were limited to linear stability analysis, which cannot explain the sub-critical transition scenario common to these flows. Although concepts from statistical physics have been discussed in this context for 30 years, earlier studies underestimated the spatial and temporal scales relevant for the transition process. We speculate that the onset of sustained turbulence in pipe and other shear flows will equally fall into the DP universality class. In situations where turbulence can spread in two directions (such studies would require Couette or channel experiments with lengths and widths comparable to the domain length used in the present

Table 1 | Comparison between the critical exponents measured in Couette experiments, Couette simulations and the exponents of the DP universality class.

Critical exponents	μ_{\perp}	μ_{\parallel}	β
Couette simulations	1.75 ± 0.02	1.85 ± 0.02	0.25 ± 0.04
Couette experiments	1.72 ± 0.05	1.84 ± 0.02	0.28 ± 0.03
DP	1.748	1.84	0.276

(Note that the empty interval exponents are directly related to the more commonly used spatial and temporal correlation exponents $\nu_{\perp}, \nu_{\parallel}$ by $\mu_{\perp/\parallel}\!=\!2\!-\!\beta/\nu_{\perp/\parallel}$.) Error estimates correspond to 95% confidence intervals.

study) the exponents are likely to change to DP in 2+1 dimensions (see also ref. 38), although discontinuous transitions cannot be ruled out at this stage. Demonstrating that models from non-equilibrium statistical mechanics can explain phenomena as complex as the onset of turbulence, and that universal critical exponents can be explicitly measured, should inspire further research exploring universality far from equilibrium.

Received 15 October 2015; accepted 25 January 2016; published online 15 February 2016

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Acknowledgements

We thank P. Maier for providing valuable ideas and supporting us in the technical aspects. Discussions with D. Barkley, Y. Duguet, B. Eckhart, N. Goldenfeld, P. Manneville and K. Takeuchi are gratefully acknowledged. We acknowledge the Deutsche Forschungsgemeinschaft (Project No. FOR 1182), and the European Research Council under the European Union's Seventh Framework Programme (FP/2007-2013)/ERC Grant Agreement 306589 for financial support. L.S. and B.H. acknowledge research funding by Deutsche Forschungsgemeinschaft (DFG) under Grant No. SFB 963/1 (project A8). Numerical simulations were performed thanks to the CPU time allocations of JUROPA in Juelich Supercomputing Center (project HGU17) and of the Max Planck Computing and Data Facility (Garching, Germany). Excellent technical support from M. Ramp on the hybrid code nsCouette is appreciated.

Author contributions

G.L., K.A. and B.H. designed the experiment. K.A. and S.V.J. performed preliminary experiments. G.L. performed final experiments. B.H. supervised the experimental work. L.S. and M.A. designed and performed the computer simulations of the Navier–Stokes equations. M.A. and B.H. supervised the computer simulations. G.L., L.S., K.A., S.V.J., M.A. and B.H. wrote the paper.

Additional information

Supplementary information is available in the online version of the paper. Reprints and permissions information is available online at www.nature.com/reprints. Correspondence and requests for materials should be addressed to B.H.

Competing financial interests

The authors declare no competing financial interests.