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# Environment-friendly magnetic Fe–Ce–W catalyst for the selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>: influence of citric acid content on its activity–structure relationship†

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The influence of the citric acid content on the structural and redox properties of a magnetic iron–cerium–tungsten mixed oxide catalyst prepared through a microwave-assisted citric acid sol–gel method is investigated *via* TG–DTG–DSC, XRD, N<sub>2</sub> adsorption–desorption, XPS, H<sub>2</sub>-TPR and NH<sub>3</sub>-TPD. Additionally, the NH<sub>3</sub>-SCR activity of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts are also studied. The results indicate that an increase in citric acid content strengthens the sol–gel reaction between citric acid and metal ions and promotes the formation of the γ-Fe<sub>2</sub>O<sub>3</sub> crystallite not α-Fe<sub>2</sub>O<sub>3</sub>. Meanwhile, it decreases the BET surface area and pore volume of the catalyst. Furthermore, the surface concentration of iron species on the catalyst is enhanced when the molar ratio of citric acid/(Fe + Ce + W) increases from 0.25 to 1.0, but its surface absorbed oxygen and total oxygen concentration decrease. The magnetic FeCeW-0.5 catalyst shows the best reducibility at temperatures below 790 °C. The increase in the citric acid content inhibits the formation of acid sites in the catalyst, thus the magnetic FeCeW-0.25 catalyst possesses the most Lewis acid sites and Brønsted acid sites among the catalysts. The enhancement in citric acid content is beneficial to improve the SCR reaction rates normalized by the surface area of the catalyst. This catalyst exhibits high anti-SO<sub>2</sub> and H<sub>2</sub>O poisoning, and the molar ratio of citric acid/(Fe + Ce + W) affects the adsorption of NO<sub>x</sub> species on its surface.

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## 1. Introduction

Nitrogen oxide (NO<sub>x</sub>) emitted from the combustion of fossil fuel in coal-fired power plants or automobile engines is a typical environmental pollutant, which causes serious problems to the environment and human health, such as acid rain, photochemical smog, pulmonary edema and tissue hypoxia.<sup>1–6</sup> Therefore, many technologies have been developed to reduce the emission of NO<sub>x</sub> from coal-fired power plants.<sup>7–9</sup> Compared with other de-nitrogen technologies, the selective catalytic reduction of NO<sub>x</sub> by NH<sub>3</sub> (NH<sub>3</sub>-SCR) has drawn increasing attention due to its high efficiency.<sup>7</sup> V<sub>2</sub>O<sub>5</sub>–WO<sub>3</sub>(MoO<sub>3</sub>)/TiO<sub>2</sub> is widely used as an NH<sub>3</sub>-SCR catalyst due to its high NO<sub>x</sub> conversion and high anti-SO<sub>2</sub> poisoning. However, it has some limitations, such as a relatively narrow temperature window

and the toxicity of vanadium species. Therefore, it is necessary to develop novel non-vanadium catalysts with high deNO<sub>x</sub> performances to replace the commercial V<sub>2</sub>O<sub>5</sub>–WO<sub>3</sub>(MoO<sub>3</sub>)/TiO<sub>2</sub> catalyst.<sup>10–16</sup>

Due to their relatively high NH<sub>3</sub>-SCR activity, low cost and non-toxicity, iron-based catalysts have been receiving significant attention by many researchers.<sup>17–25</sup> Cerium or/and tungsten are widely used additives to optimize the NH<sub>3</sub>-SCR activity of iron-based catalysts owing to the high oxygen storage capacity and high redox ability of the Ce species by shifting between Ce<sup>4+</sup> and Ce<sup>3+</sup>, and the high surface acidity and excellent thermal stability of W species.<sup>26–30</sup> In our previous research, a novel magnetic iron–cerium–tungsten mixed oxide catalyst was proposed through a microwave-assisted citric acid sol–gel method with both Ce and W as additives, and the synergistic promotional effect of Ce and W on the NH<sub>3</sub>-SCR activity of iron oxide was also investigated.<sup>15,16</sup> Meanwhile, many researches have indicated that the amount of citric acid plays an important role in the sol–gel reaction between citric acid and metal ions, thereby influencing the structural and redox properties of the powder obtained by the citric acid sol–gel method.<sup>31–35</sup> However, these properties are usually thought to be the important factors in the NH<sub>3</sub>-SCR activity of iron-based mixed oxide catalysts.<sup>16,17</sup>

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Therefore, herein, to reveal the effect of the physical structure of magnetic iron–cerium–tungsten mixed oxide catalysts on their  $\text{NH}_3$ -SCR activity, three types of catalysts are obtained by changing the content of citric acid, where the molar ratios of citric acid/(Fe + Ce + W) are 0.25, 0.5 and 1.0. Thermogravimetric analysis (TG–DTG–DSC), X-ray diffraction (XRD),  $\text{N}_2$  adsorption–desorption, X-ray photoelectron spectroscopy (XPS), temperature-programmed reduction ( $\text{H}_2$ -TPR) and temperature-programmed desorption ( $\text{NH}_3$ -TPD) are used to characterize the physical structural properties of the catalysts. The influence of the citric acid/(Fe + Ce + W) molar ratio on the  $\text{NH}_3$ -SCR mechanism over the catalyst at 200 °C is obtained using *in situ* diffuse reflection infrared Fourier transform spectroscopy (*in situ* DRIFTS).

## 2. Material and methods

### 2.1 Catalyst preparation and activity test

The magnetic iron–cerium–tungsten mixed oxide catalyst was prepared through a microwave-assisted citric acid sol–gel method according to ref. 15 and 16.  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ ,  $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ ,  $(\text{NH}_4)_6\text{H}_2\text{W}_{12}\text{O}_{40} \cdot n\text{H}_2\text{O}$  were used as the precursors and citric acid as the complexing agent. The precursors were successively dissolved in 10 mL water to obtain a mixed solution by controlling the molar ratio of Fe/Ce/W to 85 : 10 : 5. The mixed solution was then stirred for about 10 min at ambient temperature to ensure all the precursors were completely dissolved. A certain amount of citric acid (2.9472, 5.8944 and 11.7888 g) was added to this mixed solution according to the citric acid/(Fe + Ce + W) molar ratio of 0.25, 0.5 and 1.0, respectively. After stirring for about 10 min, the mixed solution was placed in a household microwave oven (EG8MEA6-NR, 2.45 GHz, 800 W) irradiated for 10 min at 36.4% power (microwave irradiation 8 s, 14 s suspended for a cycle with full power), and a pale red dry gel was obtained. The dry gel was calcined at 500 °C for 5 h under an air atmosphere (at a heating rate of 5 °C  $\text{min}^{-1}$ ), and then it was crushed and sieved to 40–60 mesh for the  $\text{NH}_3$ -SCR activity tests. The catalyst was denoted as FeCeW-*m*, where *m* represents the molar ratio of citric acid/(Fe + Ce + W). For example, FeCeW-0.5 contained the molar ratio of citric acid/(Fe + Ce + W) of 0.5. Meanwhile, it should be mentioned that there existed a weak spreading combustion phenomenon for the FeCeW-1.0 sol–gel during microwave irradiation.

The selective catalytic reduction of  $\text{NO}_x$  with  $\text{NH}_3$  was carried out in a fixed-bed continuous flow quartz reactor at atmospheric pressure.<sup>15,16</sup> The concentration of the reactants was controlled as follows: 1000 ppm  $\text{NO}$ , 1000 ppm  $\text{NH}_3$ , 3 vol%  $\text{O}_2$ , 100 ppm  $\text{SO}_2$  (when used), 5 vol%  $\text{H}_2\text{O}$  (when used) and balance  $\text{N}_2$ . The volume of sample used in each experiment was 2 mL (0.512 g for FeCeW-0.25, 1.049 g for FeCeW-0.5 and 0.989 g for FeCeW-1.0) with a gas hourly space velocity (GHSV) of 60 000  $\text{h}^{-1}$ . The downstream concentrations of  $\text{NO}$  and  $\text{NO}_2$  at the inlet and outlet of the reactor were measured using a flue gas analyzer (Model 60i, Thermo Fisher Scientific Co. Ltd, USA).  $\text{NO}$  conversion ( $X_{\text{NO}_x}$ ) was calculated as follows:  $X_{\text{NO}_x} = (1 - [\text{NO}_x]_{\text{out}}/[\text{NO}_x]_{\text{in}}) \times 100\%$  with  $[\text{NO}_x] = [\text{NO}] + [\text{NO}_2]$ . The different bulk densities of the magnetic

FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts might be mainly attributed to the influence of the citric acid/(Fe + Ce + Ti) molar ratio on the sol reaction between citric acid and the ions, and the burning characteristic of the formed sol–gel during the calcination process. Citric acid is the burning fuel in addition the complexing agent, and the nitrate ion is the oxidizer for the spreading combustion during the calcination process. The enhancement of the citric acid/(Fe + Ce + W) molar ratio improved both the sol reaction among the reactants and the formation of  $\text{NO}_2$  due to the decomposition of nitric acid during the process of microwave irradiation (a type of brown gas was formed). In addition, a high molar ratio of citric acid/(Fe + Ce + W) might cause the agglomeration of the sol–gel particles.<sup>37</sup>

### 2.2 Catalyst characterization

The thermal decomposition properties of the citric acid crystallite and the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) sol–gels were determined on a thermal gravimetric analyzer (Netzsch, STA449 F3) under an air atmosphere. In addition, the physicochemical properties and the  $\text{NH}_3$ -SCR mechanism of the samples were also characterized *via* XRD,  $\text{N}_2$  adsorption–desorption, XPS,  $\text{H}_2$ -TPR,  $\text{NH}_3$ -TPD and *in situ* DRIFTS according to ref. 15, 16 and 38. The detailed information is listed in the ESI.†

## 3. Results and discussion

### 3.1 TG–DTG–DSC

Thermo-gravimetric analysis is an important characterization method for investigating the relationship between catalyst weight and temperature or differential thermal analysis. The TG–DTG–DSC curves of the FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) sol–gels were measured after microwave irradiation, and the thermal decomposition property of the citric acid crystallite was also studied for comparison (Fig. 1, Fig. S1 and S2†).

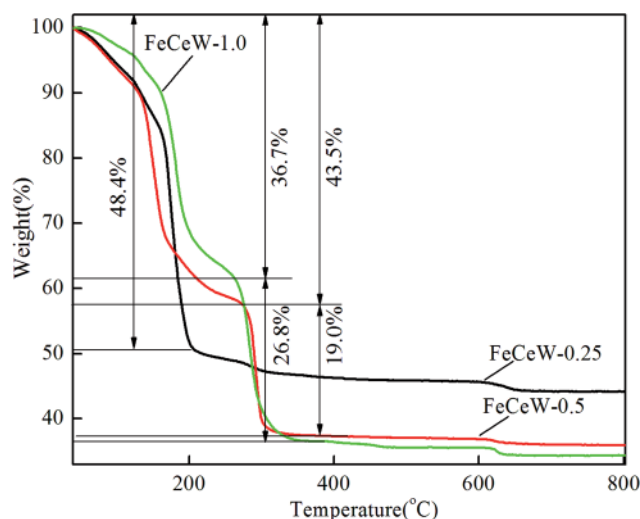


Fig. 1 TG curves of the magnetic FeCeW catalyst sol–gels.



From Fig. S1,† two obvious weight loss peaks are observed in the TG curve of the citric acid crystallite. The low-temperature weight loss peak is assigned to its rapid decomposition with about 84.9% weight loss, and the high-temperature weight loss peak is attributed to the slow oxidation of the residual carbon after its rapid decomposition. Different from the TG curve of the citric acid crystallite, three weight loss peaks appear for the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalyst sol-gels after microwave irradiation (Fig. 1). The temperature of the first weight loss peak for the FeCeW-0.25 sol-gel is lower than that of the citric acid crystallite, which is mainly attributed to the introduction of nitrate ions from iron or/and the cerium precursors. Meanwhile, the decomposition of nitric acid gradually improved during the process of microwave irradiation due to the enhancement of the sol-gel reaction between citric acid and metal ions when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0. Similar to the thermal decomposition properties of the citric acid crystallite, the FeCeW-0.25 sol-gel almost completely decomposed at the first weight loss peak, although its starting decomposition temperature decreased due to the introduction of nitrate ions. Meanwhile, a second peak with a larger weight loss is observed for the FeCeW-0.5 and FeCeW-1.0 sol-gels, and the FeCeW-1.0 sol-gel showed a larger weight loss than the FeCeW-0.5 sol-gel. This indicates that the sol-gel reaction between citric acid and metal ions becomes stronger when the molar ratio of citric acid/(Fe + Ce + W) is increased from 0.25 to 1.0. The DSC curves also show the presence of two exothermic peaks for the FeCeW-*m* (*m* = 0.5 and 1.0) sol-gels compared to one exothermic peak for the FeCeW-0.25 sol-gel (Fig. S2†). Meanwhile, the first exothermic peak of the FeCeW-1.0 sol-gel almost disappeared and was smaller than that of the FeCeW-0.5 sol-gel. This is mainly attributed to the occurrence of a weak spreading combustion phenomenon for the FeCeW-1.0 sol-gel during the microwave irradiation process. Therefore, it can be concluded that the citric acid content plays an important role in the sol-gel process between citric acid and Fe/Ce/W ions, and the complex reaction between them is fully completed with the molar ratio of citric acid/(Fe + Ce + W) increasing from 0.25 to 1.0. Thus, it influences the structural properties and NH<sub>3</sub>-SCR activity of the magnetic iron-cerium-tungsten mixed oxide catalysts prepared through the microwave-assisted citric acid sol-gel method.

### 3.2 Structure and redox properties

**3.2.1 XRD.** The XRD patterns of the FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts are shown in Fig. 2. The XRD pattern of FeCeW-0.25 contains diffraction peaks attributed to both  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>(#33-0664) and  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>(#39-1346) according to the Joint Committee of Powder Diffraction Standards (JCPDS), and no crystallite of cerium or/and tungsten species are observed. However, the intensity of the diffraction peaks attributed to  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>(#33-0664) gradually became weaker with an increase in the molar ratio of citric acid/(Fe + Ce + W) from 0.25 to 1.0, and the intensity of the diffraction peaks attributed to  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>(#39-1346) initially became weak and then increased. In addition, no crystallite of cerium or/and tungsten species were also detected

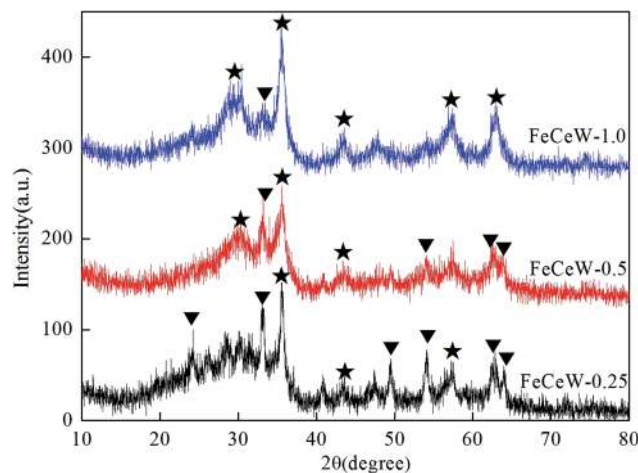


Fig. 2 XRD spectra of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts (▼  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> (#33-0664) and ★  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> (#39-1346)).

for both the FeCeW-0.5 and FeCeW-1.0 catalysts. These results indicate that iron oxide is the main crystallite of the magnetic iron-cerium-tungsten mixed oxide catalyst prepared through the microwave-assisted citric acid sol-gel method, and Ce or W species probably existed in the crystallite phase with a small particle size or amorphous phase (such as Ce-W solid solution without long-range order) in the catalyst. The amount of citric acid affected the sol-gel reaction between citric acid and metal ions, which is in accordance with the TG results in Fig. 1. The sol-gel reaction between citric acid and metal ions (especially Fe<sup>3+</sup>) is incomplete at the citric acid/(Fe + Ce + W) molar ratio of 0.25, which caused larger  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystallites to be formed in the catalyst due to the decomposition of Fe(NO<sub>3</sub>)<sub>3</sub>. The enhancement in the citric acid content improved the sol-gel reaction between citric acid and metal ions and depressed the formation of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystallite, thereby enhancing the formation of  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>. A small amount of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystallite formed in the FeCeW-1.0 catalyst due to the oxidation of  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> to  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> during the annealing process at 400 °C.

**3.2.2 N<sub>2</sub> adsorption-desorption.** The pore structure of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts was characterized *via* N<sub>2</sub> adsorption-desorption and the results are shown in Fig. 3 and Table 1. Hysteresis loops appear in the N<sub>2</sub> adsorption-desorption curves of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts, as shown in Fig. 3(A), which indicate that the magnetic iron-cerium-tungsten mixed oxide catalysts possess abundant mesoporous structures. Meanwhile, the hysteresis loop closing point (*P*/*P*<sub>0</sub>) of the catalyst at a low relative pressure gradually shifted to the right when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0, and the hysteresis loop closing point (*P*/*P*<sub>0</sub>) at a high relative pressure initially decreased and then increased. This indicates that the citric acid content has an inhibition effect on the formation of micropores and mesopores in the magnetic iron-cerium-tungsten mixed oxide catalyst. The pore size distribution of the catalysts also demonstrate that the enhancement in citric acid content resulted in the top



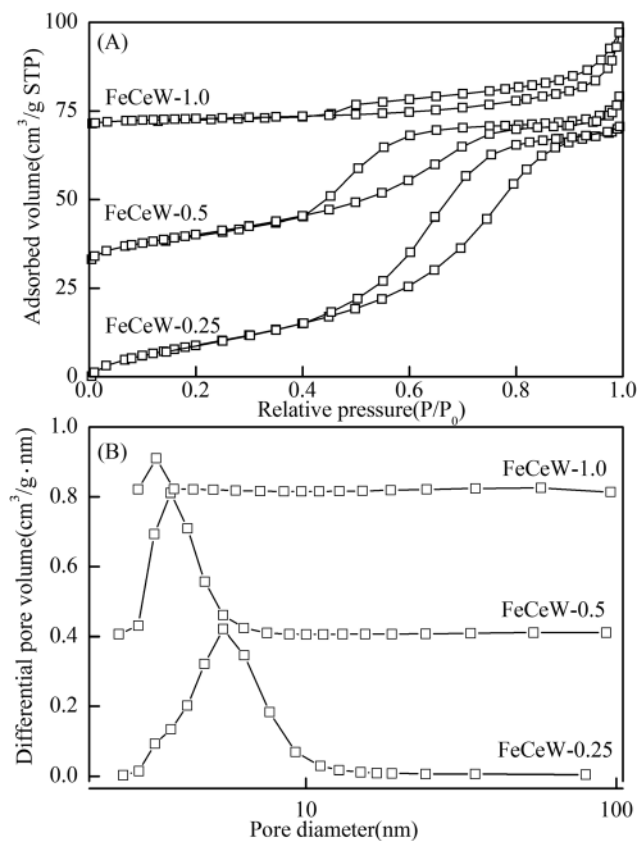


Fig. 3  $N_2$  adsorption-desorption of the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts (A)  $N_2$  adsorption-desorption isotherms and (B) pore size distributions.

position of the pore size distribution curve shifting to left and led to a decrease in the BET surface area and pore volume of the magnetic catalyst (as shown in Fig. 3(B), S3† and Table 1).

**3.2.3  $H_2$ -TPR.** To investigate the effect of the citric acid content on the reducibility of the catalyst,  $H_2$ -TPR experiments were conducted using the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts and the results are shown in Fig. 4. From Fig. 4, six  $H_2$  consumption peaks are observed for the magnetic FeCeW-0.25 catalyst. Among them, the two low temperature peaks in the range of 200–400 °C are attributed to the reduction of  $Fe_2O_3$  to  $Fe_3O_4$ , and the other four peaks in the range of 400–1000 °C are assigned to the further reduction from  $Fe_3O_4$  to FeO/partial  $Fe^0$  and the reduction of the Ce species based on the weaker reducibility of the  $WO_x$  species.<sup>36</sup> In contrast, only four  $H_2$

consumption peaks are observed for the magnetic FeCeW-0.5 and FeCeW-1.0 catalysts. The enhancement in the citric acid content caused the low-temperature  $H_2$  consumption curve of the catalyst to shift to a higher temperature. The reduction peaks of the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts were de-convoluted into twelve sub-bands for the optimum combination of Gaussian bands with correlation coefficients ( $r^2$ ) above 0.998. Additionally, the first five sub-bands at low temperature are attributed to the reduction of surface adsorbed oxygen and lattice oxygen during the reduction of  $Fe^{3+}$  to  $Fe^{2+}$ .<sup>16</sup> The enhancement in the citric acid/(Fe + Ce + W) molar ratio caused these five sub-bands to gradually shift to the right. This indicates that the enhancement in citric acid content decreased the low-temperature reduction of surface adsorbed oxygen during the reduction of  $Fe^{3+}$  to  $Fe^{2+}$ . Meanwhile, the magnetic FeCeW-0.5 catalyst showed the most  $H_2$  consumption at a reduction temperature below 790 °C as shown in Fig. 4(B). This indicates that the enhancement in citric acid content depressed the formation of iron oxide crystallite, especially  $\alpha$ - $Fe_2O_3$ , thereby reducing the  $H_2$  consumption attributed to the reduction of  $Fe_2O_3$  to  $Fe_3O_4$  below 400 °C. In addition, it might improve the total concentration of amorphous iron and cerium species on the surface of the catalyst. Also, the formation of  $\gamma$ - $Fe_2O_3$  crystallite decreased the  $H_2$  consumption at temperatures below 790 °C when the molar ratio of citric acid/(Fe + Ce + W) was further increased from 0.5 to 1.0.

**3.2.4 XPS.** XPS is widely used to investigate the redox properties of catalysts. Fig. 5 and Table 2 show the surface atomic concentrations and valence states of the Fe, Ce, W and O elements in the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts. According to Fig. 5(A) and Table 2, there two types of oxygen exist for all the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts, lattice oxygen located at a low binding energy (529.2 eV) and adsorbed oxygen ( $O^-$  and  $O^{2-}$ , denoted as  $O_a$ ) located at a high binding energy (531.1 eV). Meanwhile, the enhancement in citric acid content reduced the surface adsorbed oxygen concentration in the catalyst, and the ratio of surface  $O_a/(O_a + O_b)$  decreased from 49.6% to 45.7% when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0. According to the previous research,<sup>15,16</sup> the binding energies of Fe  $2p_{3/2}$  (located at about 711.5 eV) and Fe  $2p_{1/2}$  (located at about 723.9 eV) together with the Fe  $2p_{3/2}$  satellite peak (717.9–718.1 eV) are attributed to  $Fe^{3+}$  in the iron species (Fig. 5(B)). The results in Fig. 5(C) and (D) demonstrate the existence of the  $Ce^{3+}$ ,  $Ce^{4+}$  and  $W^{6+}$  valence states for the cerium

Table 1 The pore structure properties of the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts and the SCR reaction rates normalized by the catalyst surface area

Sample	$S_{BET}^a$ ( $m^2 g^{-1}$ )	Pore volume <sup>b</sup> ( $cm^3 g^{-1}$ )	Pore diameter <sup>c</sup> (nm)	$R_s^d \times 10^9$ ( $mol (s^{-1} m^{-2})$ )		
				150 °C	175 °C	200 °C
FeCeW-0.25	66.30	0.127	5.6	0.93	2.77	8.64
FeCeW-0.5	53.34	0.086	4.5	2.55	7.07	21.3
FeCeW-1.0	10.10	0.042	9.1	4.73	19.23	65.7

<sup>a</sup> BET surface area. <sup>b</sup> BJH desorption pore volume. <sup>c</sup> BJH desorption pore diameter. <sup>d</sup> SCR reaction rates normalized by the catalyst surface area.



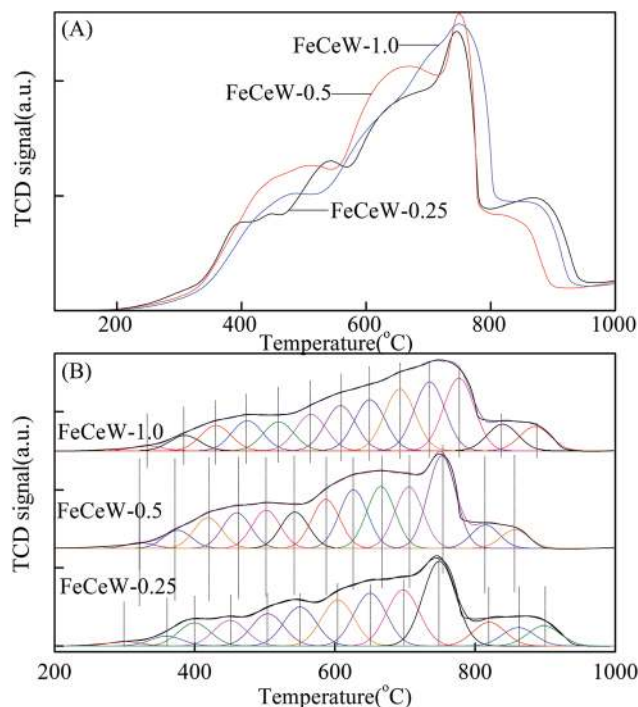


Fig. 4  $\text{H}_2$ -TPR spectra of the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts.

and tungsten elements on the surface of the catalyst. As shown in Table 2, the enhancement in the citric acid content improved the surface concentration of iron element (both  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$ ) for the magnetic catalyst, although it decreased both the absorbed oxygen and the total oxygen concentrations. Meanwhile, the surface concentrations of both Ce and W initially increased and then decreased when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0. Therefore, the amount of citric acid used in the sol-gel process plays an important role in the surface atomic concentrations and valence states of the elements in the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts.

**3.2.5  $\text{NH}_3$ -TPD.** Fig. 6 shows the  $\text{NH}_3$  desorption spectra on the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts. A large desorption peak corresponding to the  $\text{NH}_3$  reductive agent is observed for all the samples in the tested temperature range. Previous research showed that this desorption peak for iron oxide or iron-tungsten mixed oxide catalysts can be fitted into three peaks, which are attributed to the weak acid sites (weakly bonded  $\text{NH}_3$ ), medium acid sites (Lewis acid sites and Brønsted acid sites) and strong acid sites (Lewis acid sites) from low temperature to high temperature in the temperature range of  $100$ – $500$  °C.<sup>39–41</sup> Therefore, the enhancement in the citric acid content decreases the quantity of acid sites in the catalyst, especially the weak acid sites and medium acid sites. Thus, the magnetic FeCeW-0.25 catalyst shows the most surface acid sites.

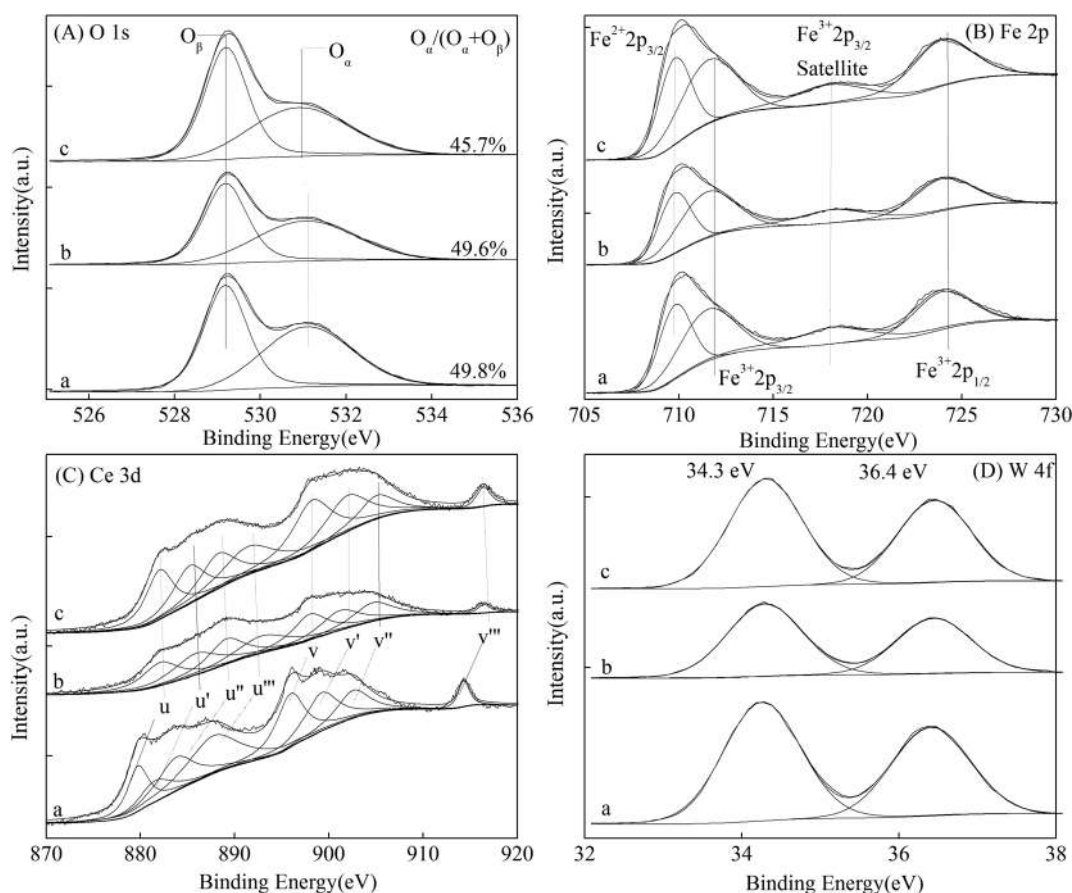


Fig. 5 XPS spectra of the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts ((A) O 1s, (B) Fe 2p, (C) Ce 3d, and (D) W 4f).



Table 2 XPS results for the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts

Sample	Surface atomic concentration (%)							
	Fe <sup>2+</sup>	Fe <sup>3+</sup>	Fe <sub>total</sub>	Ce	W	O <sub>α</sub>	O <sub>β</sub>	O <sub>total</sub>
FeCeW-0.25	4.41	12.38	16.79	6.52	1.64	37.66	37.39	75.05
FeCeW-0.5	4.67	13.86	18.53	5.96	1.33	36.78	37.40	74.18
FeCeW-1.0	5.00	14.69	19.69	7.10	1.40	32.84	38.97	71.81

### 3.3 Catalytic performance

**3.3.1 NH<sub>3</sub>-SCR activity.** The NO<sub>x</sub> conversion over the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts is shown in Fig. 7(A). According to the results in Fig. 7(A), the NH<sub>3</sub>-SCR activity of the catalyst first increased and then decreased when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0, and FeCeW-0.5 showed the best NH<sub>3</sub>-SCR activity in the reaction temperature window under the same GHSV. It should be mentioned that the quantity of FeCeW-0.25, FeCeW-0.5 and FeCeW-1.0 used in the test was 0.512, 1.049 and 0.989 g in 2 mL with a GHSV of 60 000 h<sup>-1</sup>, respectively. Fig. 7(B) shows the calculated NO<sub>x</sub> conversion per gram of magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalyst at 150–225 °C in one hour. The NO<sub>x</sub> conversion at 150–225 °C per gram catalyst also decreased as follows: FeCeW-0.5 > FeCeW-1.0 > FeCeW-0.25. Therefore, the citric acid content unquestionably influenced the NH<sub>3</sub>-SCR activity of the magnetic iron-cerium-tungsten mixed oxide catalyst prepared through the microwave-assisted citric acid sol-gel method.

The results in Fig. 1 demonstrate that the enhancement in citric acid content strengthened the sol-gel reaction between citric acid and metal ions, and the sol-gel reaction between them was fully completed when the molar ratio of citric acid/(Fe + Ce + W) was increased from 0.25 to 1.0. This depressed the formation of α-Fe<sub>2</sub>O<sub>3</sub> crystallite and caused the average pore

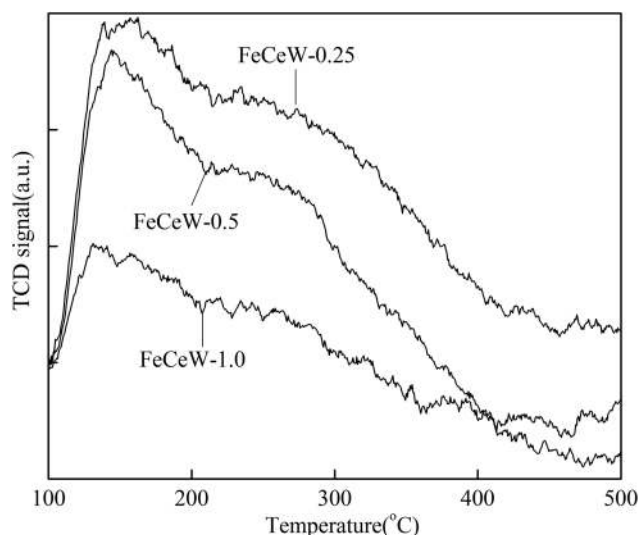


Fig. 6 NH<sub>3</sub>-TPD spectra of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts.

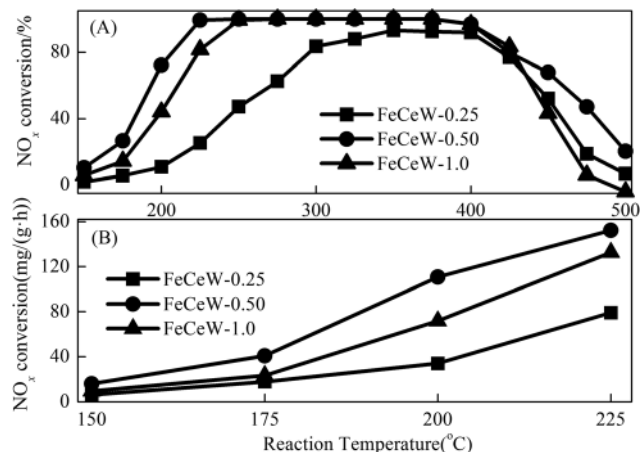
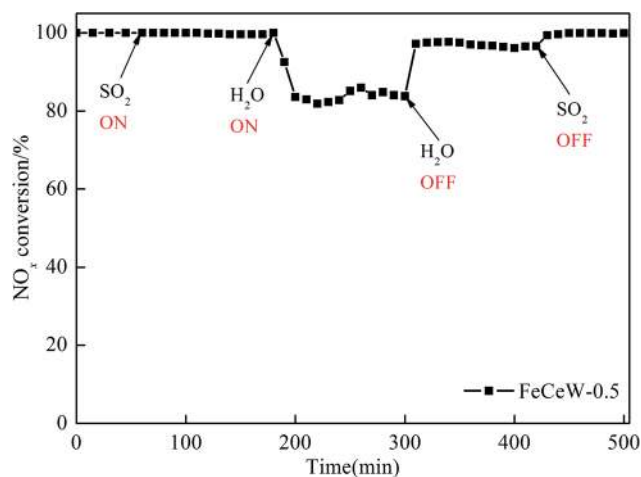


Fig. 7 NH<sub>3</sub>-SCR activity of the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts. Reaction conditions: [NO] = [NH<sub>3</sub>] = 1000 ppm, [O<sub>2</sub>] = 3.0 vol% and 2 mL of catalyst with gas hourly space velocity (GHSV) = 60 000 h<sup>-1</sup>.

size of the catalyst to become bigger (Fig. 2 and 3, respectively), thereby decreasing its BET surface area and pore volume (Table 1). In addition, the enhancement of the citric acid/(Fe + Ce + W) molar ratio from 0.5 to 1.0 promoted the formation of the γ-Fe<sub>2</sub>O<sub>3</sub> crystallite, and magnetic FeCeW-1.0 shows the smallest BET surface area and pore volume among the catalysts. Furthermore, the SCR reaction rates normalized by the catalyst surface area over the magnetic FeCeW-1.0 catalyst was the fastest among the catalysts, as shown in Table 1. Therefore, it might be concluded that the formation of metal species crystallite is an important factor in the NH<sub>3</sub>-SCR activity of the magnetic iron-cerium-tungsten mixed oxide catalyst, and the formation of γ-Fe<sub>2</sub>O<sub>3</sub> crystallite under a higher molar ratio of citric acid/(Fe + Ce + W) might be beneficial to NO<sub>x</sub> conversion over the unit area of catalyst. The H<sub>2</sub>-TPR results also demonstrate that the citric acid content affects the formation of metal species crystallite in the catalyst, and the magnetic FeCeW-0.5 catalyst shows the highest H<sub>2</sub> consumption at the temperature range of 400–790 °C due to the formation of amorphous iron and cerium species on its surface. Meanwhile, the enhancement in the citric acid/(Fe + Ce + W) molar ratio improved the surface concentration of Fe element, and decreased the surface concentrations of both the absorbed oxygen (O<sub>α</sub>) and total oxygen (O<sub>α</sub> + O<sub>β</sub>), as shown in Fig. 5 and Table 2. Li<sup>42</sup> *et al.* reported that the presence and quantity of Fe<sup>2+</sup> are important to create charge imbalance, vacancies, interactions and unsaturated chemical bonds on the surface of catalysts, which are beneficial to promote their NH<sub>3</sub>-SCR activity. Compared with lattice oxygen (O<sub>β</sub>), absorbed oxygen (O<sub>α</sub>) is often thought to be more reactive in oxidizing NO to NO<sub>2</sub> due to its higher mobility, and a higher O<sub>α</sub>/(O<sub>α</sub> + O<sub>β</sub>) ratio can facilitate a fast SCR reaction owing to the higher oxidation of NO to NO<sub>2</sub> in the NH<sub>3</sub>-SCR reaction at low temperature.<sup>43,44</sup> Interestingly, the low-temperature NO<sub>x</sub> conversion (150–225 °C) at 60 000 h<sup>-1</sup> over the magnetic FeCeW-*m* (*m* = 0.25, 0.5 and 1.0) catalysts decreased as follows: FeCeW-0.5 > FeCeW-1.0 > FeCeW-0.25.



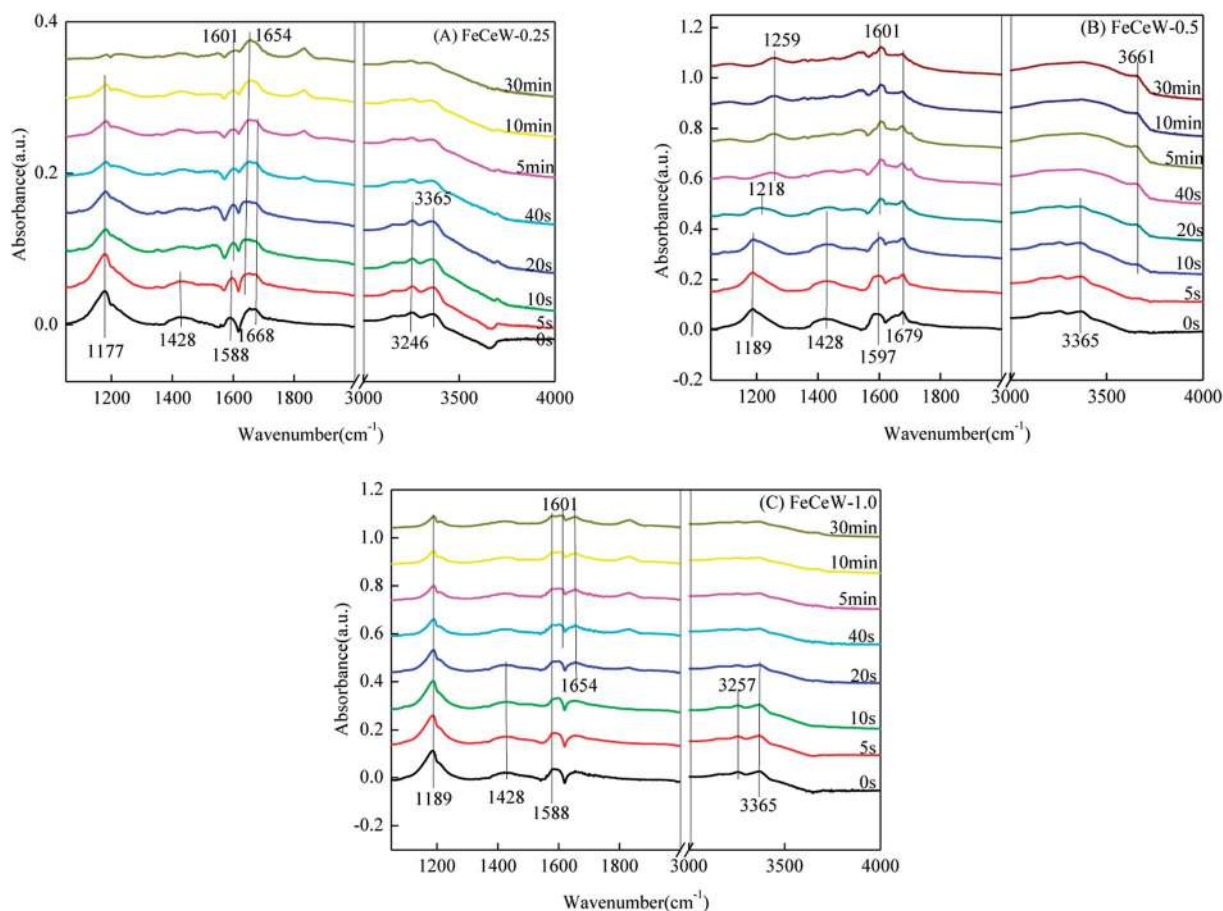


**Fig. 8** Influence of  $\text{SO}_2$  and  $\text{H}_2\text{O}$  on  $\text{NO}_x$  conversion in the  $\text{NH}_3$ -SCR reaction over the magnetic FeCeW-0.5 catalyst. Reaction conditions:  $[\text{NO}] = [\text{NH}_3] = 1000$  ppm,  $[\text{SO}_2] = 100$  ppm,  $[\text{O}_2] = 3.0$  vol%,  $[\text{H}_2\text{O}] = 5$  vol% and 2 mL of catalyst with gas hourly space velocity (GHSV) =  $60\,000\text{ h}^{-1}$ .

Therefore, the concentration of absorbed oxygen ( $\text{O}_a$ ) might not play a primary role in the low-temperature  $\text{NO}_x$  conversion by the catalyst. The enhancement in acid sites is known as an important factor in the  $\text{NH}_3$ -SCR activity of catalysts, and is

usually thought to be beneficial to promote their  $\text{NO}_x$  conversion. However, the quantity of both Lewis acid sites and Brønsted acid sites in the catalyst decreased when the molar ratio of citric acid/(Fe + Ce + W) increased from 0.25 to 1.0 (Fig. 6), although FeCeW-0.25 showed the worst  $\text{NH}_3$ -SCR activity and the lowest SCR reaction rates normalized by the catalyst surface area.

**3.3.2 Influence of  $\text{SO}_2$  and  $\text{H}_2\text{O}$ .** Due to the inhibition of  $\text{SO}_2$  and  $\text{H}_2\text{O}$  on the  $\text{NH}_3$ -SCR activity of the catalyst, FeCeW-0.5 was chosen to investigate the influence of  $\text{SO}_2$  or/and  $\text{H}_2\text{O}$ , and the results are shown in Fig. 8. When 100 ppm  $\text{SO}_2$  was introduced, the  $\text{NO}_x$  conversion over the magnetic FeCeW-0.5 catalyst showed almost no decrease. Meanwhile, when 5 vol%  $\text{H}_2\text{O}$  was also introduced for 20 min, the  $\text{NO}_x$  conversion decreased rapidly to 83%, which remained almost unchanged with the further introduction of  $\text{H}_2\text{O}$ . After shutting off the  $\text{H}_2\text{O}$ , the  $\text{NO}_x$  conversion increased obviously and was maintained at approximately 97.5%. When  $\text{SO}_2$  was also turned off from the gas flue, the  $\text{NO}_x$  conversion recovered to nearly 100% of the initial value. Therefore, the magnetic FeCeW-0.5 catalyst shows high anti- $\text{SO}_2$  poisoning at  $300\text{ }^\circ\text{C}$ , and the influence of  $\text{SO}_2$  and  $\text{H}_2\text{O}$  on its  $\text{NH}_3$ -SCR activity might be attributed to the competitive adsorption of  $\text{H}_2\text{O}$  and  $\text{NH}_3$  on its surface, not the formation of  $\text{NH}_4\text{HSO}_4$ , which deposits on the surface of the catalyst and then blocks its partial active sites.



**Fig. 9** *In situ* DRIFTS of the reaction between nitrogen oxides and pre-adsorbed  $\text{NH}_3$  species over the FeCeW-0.25, FeCeW-0.5 and FeCeW-1.0 catalysts at  $200\text{ }^\circ\text{C}$ .



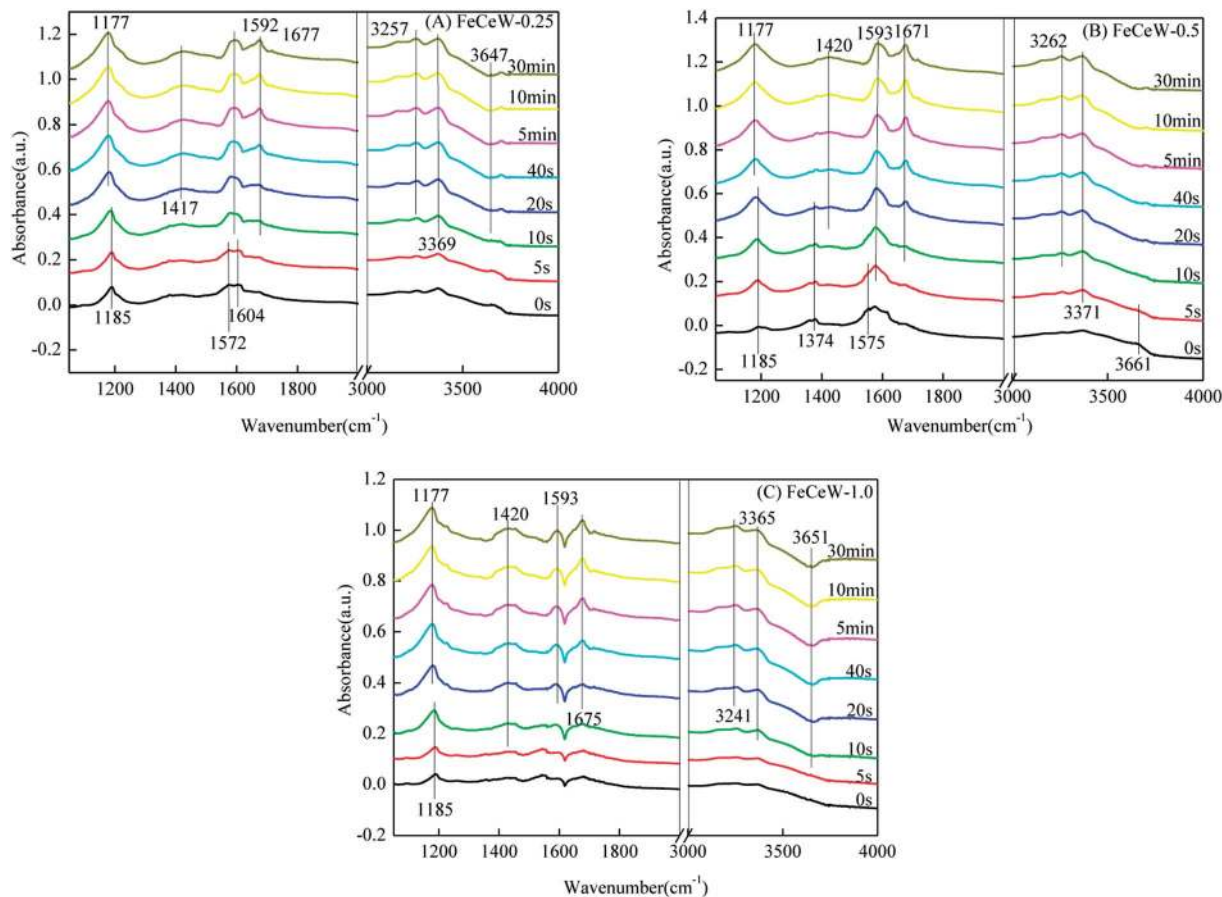


Fig. 10 *In situ* DRIFTS of the reaction between  $\text{NH}_3$  and pre-adsorbed nitrogen oxides species over the FeCeW-0.25, FeCeW-0.5 and FeCeW-1.0 catalysts at 200 °C.

### 3.4 *In situ* DRIFTS

**3.4.1 Reactivity of adsorbed  $\text{NH}_3$  species.** The *in situ* DRIFTS spectra for the reaction between  $\text{NO} + \text{O}_2$  and pre-adsorbed  $\text{NH}_3$  species over the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts at 200 °C are shown in Fig. 9. As illustrated in Fig. 9(A), FeCeW-0.25 shows several bands in the range of 1000–1700  $\text{cm}^{-1}$  and 3000–4000  $\text{cm}^{-1}$  after  $\text{NH}_3$  adsorption and  $\text{N}_2$  purge at 200 °C. The bands located at 1177 and 1588  $\text{cm}^{-1}$  are ascribed to coordinated  $\text{NH}_3$  on the Lewis acid sites. The bands at 1428 and 1668  $\text{cm}^{-1}$  are attributed to ionic  $\text{NH}_4^+$  bound to the Brønsted acid sites.<sup>45,46</sup> The two peaks at 3246 and 3365  $\text{cm}^{-1}$  correspond to the N–H stretching modes of coordinated  $\text{NH}_3$  on the Lewis acid sites.<sup>39,47,48</sup> After the introduction of  $\text{NO} + \text{O}_2$  for 20 s, the intensity of the bands at 1428 and 1588  $\text{cm}^{-1}$  ascribed to ionic  $\text{NH}_4^+$  and coordinated  $\text{NH}_3$  disappeared, and the bands located at 1177 and 1668  $\text{cm}^{-1}$  attributed to coordinated  $\text{NH}_3$  and ionic  $\text{NH}_4^+$  also showed an obvious decrease, respectively. Meanwhile, a band at 1601  $\text{cm}^{-1}$  corresponding to the bridging nitrate appeared. Therefore, both the ionic  $\text{NH}_4^+$  and coordinated  $\text{NH}_3$  could react with  $\text{NO} + \text{O}_2$  over FeCeW-0.25 at 200 °C, which follows an E–R mechanism. Similar to the adsorption of  $\text{NH}_3$  species over FeCeW-0.25 at 200 °C, both reactive coordinated  $\text{NH}_3$  and ionic  $\text{NH}_4^+$  adsorbed on FeCeW-0.5 and FeCeW-1.0 existed after  $\text{NH}_3$  adsorption and

$\text{N}_2$  purge, which could react with the  $\text{NO} + \text{O}_2$  gas, respectively. After the introduction of  $\text{NO} + \text{O}_2$  for 20 s, a band corresponding to bridging nitrate appeared over them. Meanwhile, mono-dentate nitrate (1218 and 1259  $\text{cm}^{-1}$ ) and  $-\text{NO}_2$  formed by the reaction between  $-\text{OH}$  and  $\text{NO}_x$  (3661  $\text{cm}^{-1}$ ) also appeared on FeCeW-0.5. Therefore, the molar ratio of citric acid/(Fe + Ce + W) exhibited almost no effect on the reaction between nitrogen oxides and pre-adsorbed  $\text{NH}_3$  species over the catalysts, and the adsorbed ionic  $\text{NH}_4^+$  and coordinated  $\text{NH}_3$  could react with the  $\text{NO} + \text{O}_2$  gas over the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts at 200 °C.

**3.4.2 Reactivity of adsorbed  $\text{NO}_x$  species.** The *in situ* DRIFTS spectra of the reaction between  $\text{NH}_3$  and pre-adsorbed nitrogen oxides species over the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts at 200 °C are shown in Fig. 10. After  $\text{NO} + \text{O}_2$  adsorption and  $\text{N}_2$  purge, a band at 1185  $\text{cm}^{-1}$  corresponding to the bridging nitrate appeared for all the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts, and a bidentate nitrate peak located at about 1575  $\text{cm}^{-1}$  also appeared over FeCeW-0.25 and FeCeW-0.5. In addition, M- $\text{NO}_2$  nitro compounds (1374  $\text{cm}^{-1}$ ) and  $-\text{NO}_2$  formed by the reaction between  $-\text{OH}$  and  $\text{NO}_x$  (3661  $\text{cm}^{-1}$ ) were detected over FeCeW-0.5.<sup>39,45,46</sup> Meanwhile, the bands belonging to nitrate species disappeared and some bands ascribed to ionic  $\text{NH}_4^+$ , coordinated  $\text{NH}_3$  and N–H





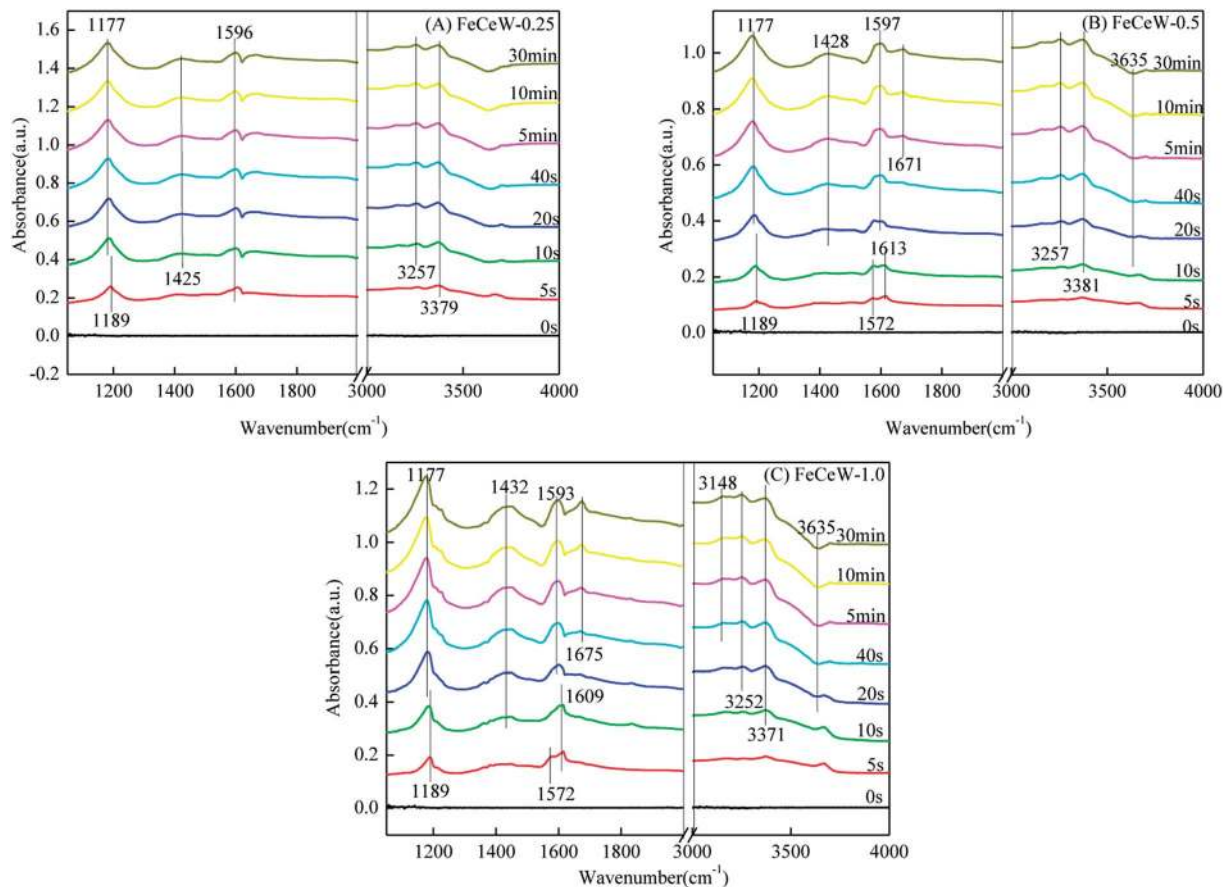


Fig. 11 *In situ* DRIFTS of  $\text{NH}_3 + \text{NO} + \text{O}_2$  over the FeCeW-0.25, FeCeW-0.5 and FeCeW-1.0 catalysts at 200 °C.

stretching modes appeared over the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts after the reintroduction of  $\text{NH}_3$  for 20 s. Therefore, the adsorbed nitrate species over the magnetic catalyst could react with  $\text{NH}_3$  to generate  $\text{N}_2$  and  $\text{H}_2\text{O}$ .

**3.4.3  $\text{NH}_3 + \text{NO} + \text{O}_2$  co-adsorption ability.** Fig. 11 shows the *in situ* DRIFT spectra of  $\text{NH}_3 + \text{NO} + \text{O}_2$  over the magnetic FeCeW- $m$  ( $m = 0.25, 0.5$  and  $1.0$ ) catalysts at 200 °C. Bands ascribed to coordinated  $\text{NH}_3$ , ionic  $\text{NH}_4^+$  and N-H stretching modes of coordinated  $\text{NH}_3$  appeared over FeCeW-0.25, and their intensity became stronger with an increase in the  $\text{NH}_3 + \text{NO} + \text{O}_2$  introduction time. However, the bands at about 1572 and 1609  $\text{cm}^{-1}$  ascribed to bidentate nitrate and bridging nitrate appeared over the magnetic FeCeW-0.5 and FeCeW-1.0 catalysts when  $\text{NH}_3 + \text{NO} + \text{O}_2$  were introduced into the reaction tank, although they quickly vanished. Similar to FeCeW-0.25, the intensity of coordinated  $\text{NH}_3$ , ionic  $\text{NH}_4^+$  and N-H stretching modes of coordinated  $\text{NH}_3$  over the magnetic FeCeW-0.5 and FeCeW-1.0 catalysts became stronger when  $\text{NH}_3 + \text{NO} + \text{O}_2$  were further introduced into the reaction tank. Therefore, it can be concluded that the main reaction was between the adsorbed  $\text{NH}_3$  species and gaseous  $\text{NO} + \text{O}_2$  over FeCeW-0.25 at 200 °C, which follows an Eley-Rideal (E-R) mechanism. Meanwhile, a reaction between the adsorbed  $\text{NH}_3$  species with gaseous  $\text{NO} + \text{O}_2$  or the adsorbed  $\text{NO}_x$  species may occur over FeCeW-0.5 and FeCeW-1.0 at 200 °C, which obeys both the Eley-Rideal (E-R) and Langmuir-Hinshelwood (L-H) mechanisms.

## 4. Conclusions

The influence of citric acid content on the  $\text{NH}_3$ -SCR activity, structure and redox properties of a magnetic iron-cerium-tungsten mixed oxide catalyst prepared through the microwave-assisted citric acid sol-gel method was investigated. The enhancement in citric acid/(Fe + Ce + W) molar ratio is beneficial to the formation of  $\gamma\text{-Fe}_2\text{O}_3$  crystallite and promotion of the SCR reaction rates normalized by the surface area of the magnetic catalyst, although this decreased its BET surface area and pore volume. The concentrations of both  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$  on the surface of the catalyst were enhanced when the molar ratio of citric acid/(Fe + Ce + W) increased from 0.25 to 1.0, but it decreased the concentration of adsorbed oxygen and total oxygen. Also, the magnetic FeCeW-0.5 catalyst showed the best reducibility at temperatures below 790 °C. Simultaneously, the enhanced citric acid content inhibited the formation of acid sites in the magnetic iron-cerium-tungsten mixed oxide catalyst, and FeCeW-0.25 showed the most Lewis acid sites and Brønsted acid sites among the catalysts. The molar ratio of citric acid/(Fe + Ce + W) exhibited almost no effect on the adsorption of  $\text{NH}_3$  species over the catalyst. Meanwhile, it affected the adsorption of  $\text{NO}_x$  species. The main reaction occurs between the adsorbed  $\text{NH}_3$  species and gaseous  $\text{NO} + \text{O}_2$  over FeCeW-0.25 at 200 °C, which follows an E-R mechanism. Meanwhile, both E-R and L-H mechanisms exist over FeCeW-0.5 and FeCeW-1.0 at 200 °C.



## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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## References

- L. B. Duan, Y. Q. Duan, C. S. Zhao and J. W. Anthony, NO emission during co-firing coal and biomass in an oxy-fuel circulate in fluidized bed combustor, *Fuel*, 2015, **150**, 8–13.
- D. Husain, Chemistry of Atmospheres: An Introduction to the Chemistry of Atmospheres of Earth, the Planets and their Satellites By R. P. Wayne, *J. Photochem. Photobiol.*, A, 1992, **63**(2), 253–254.
- L. B. Duan, Z. X. Jiang, X. P. Chen and C. S. Zhao, Investigation on water vapor effect on direct sulfation during wet-recycle oxy-coal combustion, *Appl. Energy*, 2013, **108**, 121–127.
- L. B. Duan, D. Y. Liu, X. P. Chen and C. S. Zhao, Fly ash recirculation by bottom feeding on a circulating fluidized bed boiler co-burning sludge and coal, *Appl. Energy*, 2012, **95**, 295–299.
- R. Kurose, H. Makino and A. Suzuki, Numerical analysis of pulverized coal combustion characteristics using advanced low-NO<sub>x</sub> burner, *Fuel*, 2004, **83**, 693–703.
- S. J. Zhao, L. Wang, Y. Wang and X. Li, Hierarchically porous LaFeO<sub>3</sub> perovskite prepared from the pomelo peel bio-template for catalytic oxidation of NO, *J. Phys. Chem. Solids*, 2018, **116**, 43–49.
- Y. Y. Wang, H. Y. Fang, D. Zhou, H. C. Han and J. Chen, Characterization of nitrous oxide and nitric oxide emissions from a full-scale biological aerated filter for secondary nitrification, *Chem. Eng. J.*, 2016, **299**, 304–313.
- K. Zhao, W. L. Han, G. X. Lu, J. Y. Lu, Z. C. Tang and X. P. Zhen, Promotion of redox and stability features of doped Ce–W–Ti for NH<sub>3</sub>-SCR reaction over a wide temperature range, *Appl. Surf. Sci.*, 2016, **379**, 316–322.
- M. Kong, Q. C. Liu, X. Q. Wang, S. Ren, J. Yang, D. Zhao, W. C. Xi and L. Yao, Performance impact and poisoning mechanism of arsenic over commercial V<sub>2</sub>O<sub>5</sub>-WO<sub>3</sub>/TiO<sub>2</sub> SCR catalyst, *Catal. Commun.*, 2015, **72**, 121–126.
- L. Qiu, Y. Wang, D. D. Pang, F. Ouyang and C. L. Zhang, SO<sub>4</sub><sup>2-</sup>-Mn-Co-Ce supported on TiO<sub>2</sub>/SiO<sub>2</sub> with high sulfur durability for low-temperature SCR of NO with NH<sub>3</sub>, *Catal. Commun.*, 2016, **78**, 22–25.
- S. Lai, D. Meng, W. Zhan, Y. Guo and Y. Guo, The promotional role of Ce in Cu/ZSM-5 and *in situ* surface reaction for selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>, *RSC Adv.*, 2015, **5**(110), 90235–90244.
- Q. Xu, R. Su, L. Cao, Y. Li and C. Yang, Facile preparation of high-performance Fe-doped Ce-Mn/TiO<sub>2</sub> catalysts for the low-temperature selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>, *RSC Adv.*, 2017, **7**(77), 48785–48792.
- P. Lu, H. Li, H. Liu, Y. Chen and Z. Zhang, Influence of tungsten on the NH<sub>3</sub>-SCR activity of MnWO<sub>x</sub>/TiO<sub>2</sub>, *RSC Adv.*, 2017, **7**(32), 19771–19779.
- C. Liu, G. Gao, J. W. Shi, C. He, G. D. Li, N. Bai and C. M. Niu, MnO<sub>x</sub>-CeO<sub>2</sub> shell-in-shell microspheres for NH<sub>3</sub>-SCR de-NO<sub>x</sub> at low temperature, *Catal. Commun.*, 2016, **86**, 36–40.
- Z. B. Xiong, B. Peng, F. Zhou, C. Wu and W. Lu, Magnetic iron-cerium-tungsten mixed oxide pellets prepared through citric acid sol-gel process assisted by microwave irradiation for selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>, *Powder Technol.*, 2017, **319**, 19–25.
- Z. B. Xiong, J. Liu, F. Zhou, D. Y. Liu and W. Lu, Selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub> over iron-cerium-tungsten mixed oxide catalyst prepared by different methods, *Appl. Surf. Sci.*, 2017, **406**, 218–225.
- F. D. Liu, H. He, C. B. Zhang, Z. C. Feng, L. R. Zheng, Y. N. Xie and T. D. Hu, Selective catalytic reduction of NO with NH<sub>3</sub> over iron titanate catalyst: catalytic performance and characterization, *Appl. Catal., B*, 2010, **96**, 408–420.
- Y. Xin, N. N. Zhang, Q. Li, Z. L. Zhang, X. M. Gao, L. R. Zheng, Y. W. Zeng and J. A. Anderson, Selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub> over short-range ordered W–O–Fe structures with high thermal stability, *Appl. Catal., B*, 2018, **229**, 81–87.
- G. H. Yao, F. Wang, X. B. Wang and K. T. Gui, Magnetic field effects on selective catalytic reduction of NO by NH<sub>3</sub> over Fe<sub>2</sub>O<sub>3</sub> catalyst in a magnetically fluidized bed, *Energy*, 2010, **35**, 2295–2300.
- J. Grzybek, B. Gil, W. J. Roth, M. Skozej, A. Kowalczyk and L. Chmielarz, Characterization of Co and Fe-MCM-56 catalysts for NH<sub>3</sub>-SCR and N<sub>2</sub>O decomposition: an *in situ* FTIR study, *Spectrochim. Acta A*, 2018, **196**, 281–288.
- Z. B. Xie, F. Wang, J. S. Liang, Z. S. Wang, N. Hui and Y. Ding, Enhanced catalytic efficiency of FeMnTiO<sub>x</sub> SCR catalysts through adding tourmaline nanopowders during the one-step sol-gel process, *Mater. Lett.*, 2018, **217**, 60–63.
- C. Z. Shao, X. F. Liu, D. M. Meng, Q. Xu, Y. Guo, W. Z. Zhan, L. Wang and G. Z. Lu, Catalytic performance of Co-Fe mixed oxide for NH<sub>3</sub>-SCR reaction and the promotional role of cobalt, *RSC Adv.*, 2016, **70**, 66169–66179.
- J. Liu, L. Kang, P. Maitarad, J. P. Zhang, L. Y. Shi and D. S. Zhang, Mn-Fe bi-metal oxides *in situ* created on metal wire mesh as monolith catalysts for selective catalytic reduction of NO with NH<sub>3</sub>, *RSC Adv.*, 2017, **7**, 40444–40451.
- Z. B. Xiong, C. Wu, Q. Hu, Y. Z. Wang, J. Jin, C. M. Lu and D. X. Guo, Promotional effect of microwave hydrothermal treatment on the low-temperature NH<sub>3</sub>-SCR activity over iron-based catalyst, *Chem. Eng. J.*, 2016, **286**, 459–466.
- Z. B. Xiong, Q. Hu, D. Y. Liu, C. Wu, F. Zhou, Y. Z. Wang, J. Jin and C. M. Lu, Influence of partial substitution of iron oxide by titanium oxide on the structure and activity of



- iron-cerium mixed oxide catalyst for selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>, *Fuel*, 2016, **165**, 432–439.
- 26 K. Zhao, W. L. Han, Z. C. Tang, J. Y. Lu and X. Hu, High-Efficiency Environmental-Friendly Fe–W–Ti Catalyst for Selective Catalytic Reduction of NO with NH<sub>3</sub>: The Structure-Activity Relationship, *Catal. Surv. Asia*, 2018, **22**, 20–30.
- 27 A. Stahl, Z. Wang, T. Schwaemmle, J. Ke and X. B. Li, Novel Fe–W–Ce Mixed Oxide for the Selective Catalytic Reduction of NO<sub>x</sub> with NH<sub>3</sub> at Low Temperatures, *Catalysis*, 2017, **7**(2), 1–12.
- 28 H. Wang, Z. P. Qu, S. C. Dong, H. B. Xie and C. Tang, Superior Performance of Fe<sub>1-x</sub>W<sub>x</sub>O<sub>delta</sub> for the Selective Catalytic Reduction of NO<sub>x</sub> with NH<sub>3</sub>: Interaction between Fe and W, *Environ. Sci. Technol.*, 2016, **50**(24), 13511–13519.
- 29 Y. Sun, Y. Guo, W. Su and Y. J. Wei, Low-Temperature Selective Catalytic Reduction of NO with NH<sub>3</sub> over Fe–Ce–O<sub>x</sub> Catalysts, *Trans. Tianjin Univ.*, 2017, **23**(1), 35–42.
- 30 X. B. Wang, L. Zhang, S. G. Wu, W. X. Zou, S. H. Yu, Y. Shao and L. Dong, Promotional Effect of Ce on Iron-Based Catalysts for Selective Catalytic Reduction of NO with NH<sub>3</sub>, *Catalysts*, 2016, **6**(8), 1–15.
- 31 A. Mali and A. Ataie, Influence of the metal nitrates to citric acid molar ratio on the combustion process and phase constitution of barium hexaferrite particles prepared by sol-gel combustion method, *Ceram. Int.*, 2004, **30**, 1979–1983.
- 32 W. D. Yang, Y. H. Chang and S. H. Huang, Influence of molar ratio of citric acid to metal ions on preparation of La<sub>0.67</sub>Sr<sub>0.33</sub>MnO<sub>3</sub> materials *via* polymerizable complex process, *J. Eur. Ceram. Soc.*, 2005, **25**, 3611–3618.
- 33 C. Cannas, A. Musinu, D. Peddis and G. Piccaluga, New synthesis of ferrite-silica nanocomposites by a sol-gel auto-combustion, *J. Nanopart. Res.*, 2004, **6**, 223–232.
- 34 R. Ran, X. D. Wu and D. A. Weng, Effect of complexing species in a sol-gel synthesis on the physicochemical properties of La<sub>0.7</sub>Sr<sub>0.3</sub>Mn<sub>0.7</sub>Cu<sub>0.3</sub>O<sub>3</sub> + λ catalyst, *J. Alloys Compd.*, 2006, **414**(1–2), 169–174.
- 35 Z. X. Yue, W. Y. Guo, J. Zhou, Z. L. Gui and L. T. Li, Synthesis of nanocrystalline ferrites by sol-gel combustion process: the influence of pH value of solution, *J. Magn. Magn. Mater.*, 2004, **270**, 216–223.
- 36 F. D. Liu, H. He, C. B. Zhang, Z. C. Feng, L. R. Zheng, Y. N. Xie and T. D. Hu, Selective catalytic reduction of NO with NH<sub>3</sub> over iron titanate catalyst: catalytic performance and characterization, *Appl. Catal., B*, 2010, **96**, 408–420.
- 37 Z. X. Yue, J. Zhou, H. G. Zhang, Z. L. Gui and L. T. Li, Auto-combustion behavior of nitrate-citrate gels and synthesis of ferrite nano-particles, *J. Chin. Ceram. Soc.*, 1999, **27**(4), 466–470.
- 38 F. Zhou, Z. B. Xiong, W. Lu, J. Jin and X. C. Ding, Microwave-pyrolysis assisted preparation of magnetic iron-titanium mixed oxide catalyst for Selective catalytic reduction of NO<sub>x</sub> with NH<sub>3</sub>, *Clean: Soil, Air, Water*, 2017, **45**(11), 1–9.
- 39 Y. K. Yu, J. S. Chen, J. X. Wang and Y. T. Chen, Performances of CuSO<sub>4</sub>/TiO<sub>2</sub> catalysts in selective catalytic reduction of NO<sub>x</sub> by NH<sub>3</sub>, *Chin. J. Catal.*, 2016, **37**, 281–287.
- 40 M. P. Ruggeri, A. Grossale, I. Nova, E. Tronconi, H. Jirglova and Z. Sobalik, FTIR *in situ* mechanistic study of the NH<sub>3</sub>–NO/NO<sub>2</sub> “Fast SCR” reaction over a commercial Fe-ZSM-5 catalyst, *Catal. Today*, 2012, **184**(1), 107–114.
- 41 G. Busca, L. Lietti, G. Ramis and F. Berti, Chemical and mechanistic aspects of the selective catalytic reduction of NO<sub>x</sub> by ammonia over oxide catalysts: a review, *Appl. Catal., B*, 1998, **18**, 1–36.
- 42 X. Li, J. H. Li, Y. Peng, T. Zhang, S. Liu and J. M. Hao, Selective catalytic reduction of NO with NH<sub>3</sub> over novel iron-tungsten mixed oxide catalyst in a broad temperature range, *Catal. Sci. Technol.*, 2015, **5**, 4556–4564.
- 43 F. He, Y. G. Wei, H. B. Li and H. Wang, Synthesis Gas Generation by Chemical-Looping Reforming using Ce-Based Oxygen Carriers Modified with Fe, Cu, and Mn oxides, *Energy Fuels*, 2009, **23**, 2095–2102.
- 44 H. He, H. X. Dai and C. T. Au, Defective structure, oxygen mobility, oxygen storage capacity, and redox properties of RE-based (RE = Ce, Pr) solid solutions, *Catal. Today*, 2004, **90**, 245–254.
- 45 M. P. Ruggeri, A. Grossale, I. Nova, E. Tronconi, H. Jirglova and Z. Sobalik, FTIR *in situ* mechanistic study of the NH<sub>3</sub>–NO/NO<sub>2</sub> “Fast SCR” reaction over a commercial Fe-ZSM-5 catalyst, *Catal. Today*, 2012, **184**(1), 107–114.
- 46 Z. M. Liu, Y. Yi, J. H. Li, S. I. Woo, B. Y. Wang, X. Z. Cao and Z. X. Li, A superior catalyst with dual redox cycles for the selective reduction of NO<sub>x</sub> by ammonia, *Chem. Commun.*, 2013, **70**, 726–7728.
- 47 Y. Q. Zeng, S. L. Zhang, Y. N. Wang and Q. Zhong, CeO<sub>2</sub> supported on reduced TiO<sub>2</sub> for selective catalytic reduction of NO by NH<sub>3</sub>, *J. Colloid Interface Sci.*, 2017, **496**, 487–495.
- 48 J. Liu, X. Y. Li, Q. D. Zhao, J. Ke, H. N. Xiao, X. J. Lv, S. M. Liu, M. Tadé and S. B. Wang, Mechanistic investigation of the enhanced NH<sub>3</sub>-SCR on cobalt-decorated Ce–Ti mixed oxide: *In situ* FTIR analysis for structure-activity correlation, *Appl. Catal., B*, 2017, **200**, 297–308.

