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EXPERIMENTAL EVALUATION OF PREMIXING - PREVAPORIZING FUEL INJECTION CONCEPTS FOR A GAS TURBINE CATALYTIC COMBUSTOR

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Work performed as part of a joint effort with ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION Division of Transportation Energy Conservation Heat Engine Highway Vehicle Systems Program Under Interagency Agreement EC-77-A-31-1011

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ABSTRACT

Experiments were performed to evolve and evaluate a premixing-prevaporizing fuel system to be used with a catalytic combustor for possible application in an automotive gas turbine. Spatial fuel distribution and degree of vaporization were measured using Jet A fuel. Three types of airblast injectors, an air-assist nozzle and a simplex pressure atomizer were tested. Air swirlers with vane angles up to 30° were used to improve the spatial fuel distribution. The work was done in a 12-cm (4.75-in,) diameter tubular rig. Test conditions were: a pressure of 0.3 and 0.5 MPa (3 and 5 atm), inlet air temperatures up to 800 K (980° F), velocity of 20 m/see (66 ft/sec) and fuel-uir ratios of 0.01 and 0.025. Uniform sputial fuel distributions that were within ±10 percent of the mean were obtained. Complete vaporization of the fuel was achieved with airblast configurations at inlet air temperatures of 550 K (530°F) and higher. The total pressure loss was less than 0.5 percent for configurations without air swirlers and less than 1 percent for configurations with a 30° vanc angle air swirler.

NOMENCLATURE

NORMANDENIE				
E	degree of vaporization $\approx \frac{(f/a)_V}{(f/a)_V + (f/a)_Z}$			
£/u	fuel-air ratio			
(f/a) _{mean}	fuel-air ratio determined by inlet fuel flow divided by inlet sirflow			
P _{in}	inlet pressure			
Tin	inlet air temperature			
v	probe velocity at inlet			
v _R	reference velocity, velocity based on inlet pressure, inlet temperature, and the area of the 12-cm (4.75-in.) diameter duct			
w_	fuel flow through probe			
w _a	airflow through the probe at isokinetic velocity			
wi	airflow through the probe			

Subscripts:

isq	isokinetie
Ł	liquid
p	probe
v	vapor

INTRODUCTION

The use of combustors with lean premixedprevaporized fuel-air mixtures has been shown to have the potential to keep NO, levels low (1). Since NO, is exponentially dependent on flame temperature, the use of a catalytic reaction has the potential to reduce NOx levels even further by being able to completely react the fuel at temperatures below the flammability limit. Catalysis evaluation work being done at Lewis as described in references 2 to 4 has utilized vaporized propone. This paper describes the effort to develop a liquid fuel preparation system to be used with the catalytic combustor. 1 Uniform fuel distribution and complete vaporization are necessary for catalytic combustors since the substrates are currently limited to temperatures below 1800 K (2780° F), thus rich zones or liquid drops burning off the substrate could damage it. The development of such a fuel system would also have application to premixed-prevaporized combustors using homogeneous combustion.

Data on drop size from various types of fuel injectors and data on single dioplet vaporization rates are plentiful. But only limited data has been published on spatial fuel distribution and vaporization rates of sprays. Such information is necessary for the development of a premixing-prevaporizing system for a gas turbine combustor. Using a multiple-orifice contrastream injector, vaporization rates of JP-5 sprays were measured in reference 5 and using a simple orifice contrastream injector, vaporization rates of isooctane sprays were measured in reference 6. In reference 7 the spatial fuer distribution and degree of vaporization were measured from simplex pressure atomizers using isooctane and No. 2 fuel oil as the fuel.

In this study spatial fuel distribution and vaporization data were taken with two types of airblast injectors, a simplex pressure atomizer and a

¹Work sponsored by Division of Transportation Energy Conservation, ERDA.

Sonicore fuel injector. Air swirlers with vane angles up to 30° were used to improve the spatial fuel distribution. Test conditions were: inlet air pressure, 0.3 and 0.5 MPa (3 and 5 atm); reference velocity, 20 m/sec (66 ft/sec); fuel-air ratios of 0.01 and 0.025; and a.r inlet temperatures from 450 K (350° F) to 806 K (980° F). The fuel was Jet A.

APPARATUS AND PROCEDURE

Test Rig

Figure 1 is a schematic of the test rig. The airflow rate was measured with a square-edged orifice. The air was heated up to 800 K (980° F) in a nonvitiating preheater. The fuel flow was measured by two turbine flowmeters in series. A temperature and pressure measurement was taken upstream of the fuel injector. The duet diameter was 10.2 cm (4.0 in.) apstream of the injector and 12 cm (4.75 in.) downstream. A 7.6-cm (3.0-in.) diameter inlet section was inserted upstream of the injector to increase the air velocity which improves fuel atomization. A diffuser was then inserted downstream of the injector.

Two sample collecting probes, 90° apart, were located 35.6 cm (14.0 in.) downstream of the fuel injector to sample the fuel-air mixture. The fuel-air ratio was determined by passing the mixture sample over a cutalyst heated in an oven to 1030 K (1400° and then analyzing the products of combustion for carbon monoxide, carbon dioxide and unburned hydrocarbons. Carbon monoxide and carbon dioxide concentrations were measured on Beckman mondispersive infrared analyzers and unburned hydrocarbon concentrations were measured on a Beckman Flame Ionization Detector. The amount of unburned hydrocarbons and carbon monoxide measured was negligible because mixture ratius were always very lean. A temperature and pressure measurement was also taken at the 35.6-cm (14.0-in.) downstream station. The fuel-air mixture was enriched with hydrogen and burned downstream of the sampling probes. Water was injected to cool the exhaust products and a back pressure valve was used to control the rig pressure.

Injectors

Five fuel injectors were evaluated. They were a multiple-jet contrastream injector, a multiple-jet cross-stream injector, a splash-groove injector, a simplex pressure atomizer, and an air-assist atomizer. The first three types of injectors are airblast atomizers; that is, they rely on the relative velocity between fuel and air for atomization. The simplex pressure atomizer relies on fuel pressure for atomization. The air assist was a Hartman whistle-type that depends on a high velocity external airstream for atomization.

Multiple-jet injector. Two multiple-jet injectors are shown in figures 2 and 3. Figure 2 shows an injector where the fuel was injected contrastream from eight orifices. The diameter of the orifices was 0.25 mm (0.016 in.) in diameter and the radial location could be varied. The multiple-jet crossstream injector is shown in figure 3. Twenty-eight orifices of 0.37 mm (0.015 in.) diameter were located so that each of the 28 orifices injects fuel into a space of approximately equal area. Larger diameters were used since the penetration was not important and the 0.25-mm (0.010-in.) diameter orifices would plug due to carbon buildup.

Splush-groove fuel injector. This injector was developed by Ingebo (8) and is shown in figure 4. A sketch showing the principal features of the injector is shown in figure 4(a). Fuel is injected through orifices into three grooved portions of the nezzle. The fuel splashes over the lips of each of the three grooves and is atomized by the airflow. Configurations used with the splash-groove injector consisted of 10.2 cm (4 in.) (fig. 4(b)) and 7.6 cm (3 in.) (fig. 4(c)) inlets, and the use of air swirlers (fig. 4(d)).

Simplex pressure atomizer. The simplex nozzle used was a Monarch 0,013 m³/hr (3.5 gal/hr), hollow cone apray, with a 70° cone angle. Configurations terted consisted of 10.2 cm (4 in.) inlet (fig. 5(a)), 7.6 cm (3 in.) inlet (fig. 5(b)), insertion of air swirlers upstream (fig. 5(c)) and apraying the fuel contrastream (fig. 5(d)) as compared to the previous configurations in which the fuel was aprayed costream. The air swirler was located upstream of the nozzle so that when the fuel was sprayed contrastream there would not be liquid fuel impinging on the swirler.

Sonicore nezzle. The air-assist nozzle was a Hartman whistle-type that is produced commercially by Sonic Development Corporation. The particular nozzle used was a Sonicore P/N 125 M-A. This nozzle (see fig. 6) uses an external air supply which provides a high velocity airstream for atomizing. As the air-stream implages upon the resonator cap, it produces strong local shock waves in the space between the nozzle and cap. Fuel is pumped or sucked into the airstream and the result is a cone-shaped spray pattern of finely atomized droplets. The external air-stream had a supply pressure of 0.55 MPa (5.5 atm). Configurations tested consisted of a 7.6-cm (3.0-in.) inlet with and without the use of air swirlers.

Data Analysis

The sample collecting probes were used to determine the spatial fuel distribution and the degree of vaporization.

Spatial fuel distribution. The spatial fuel distribution was found by traversing the sample probe across the diameter of the duct. The fuel-air ratio was sampled isokinetically (at seven points) across the diameter of the duct with each probe. The fuel-air ratio in the plot is normalized using the fuel-air ratio determined from the inlet fuel flow divided by the inlet airflow.

<u>Vuporization data</u>. The degree of vaporization was determined by the spillover technique (5). This technique consists of varying the velocity through the probe above and below the isokinetic velocity and determining the degree of vaporization by the change in fuel-air ratio through the probe. The following analysis was used (see NOMENCLATURE):

$$\left(\frac{f}{a}\right)_{D} = \left(\frac{f}{a}\right)_{\frac{1}{2}} + \left(\frac{f}{a}\right)_{V} = \frac{w_{\frac{1}{2}}}{w_{\frac{1}{2}}} + \frac{w_{\frac{1}{2}}}{w_{\frac{1}{2}}} = \frac{w_{\frac{1}{2}}}{w_{\frac{1}{2}}} + \frac{w_{\frac{1}{2}}}{w_{\frac{1}{2}}} + \frac{w_{\frac{1}{2}}}{w_{\frac{1}{2}}}$$
(1)

if the degree of vaporization is uniform in the vicinity of the probe, then the vapor fuel-air ratio through the probe does not vary with velocity through the probe; that is

$$\frac{\mathbf{w}_{\mathbf{v}}}{\mathbf{w}_{\mathbf{a}}^{T}} = \text{constant} = \left(\frac{\mathbf{f}}{\mathbf{a}}\right)_{\mathbf{f} \in \mathbf{A}} \cdot \mathbf{f} \tag{2}$$

w; is assumed to be constant; that is, the atreamlines of the liquid drops do not change with velocity through the probe

$$\frac{\mathbf{w}_f}{\mathbf{w}_a} = \left(\frac{\mathbf{f}}{a}\right)_{1,1,1,0} = (1 - \mathbf{E}) \left(\frac{\mathbf{f}}{a}\right)_{1,1,0} = \text{constant}$$
 (3)

$$\left(\frac{t}{a}\right)_{p} = (1 + E) \left(\frac{t}{a}\right)_{t \in O} \left(\frac{w_{a}}{w_{a}^{t}}\right) + E\left(\frac{t}{a}\right)_{t \in O}$$
 (4)

in terms of velocity

$$\frac{\mathbf{v}_{a}}{\mathbf{v}_{a}^{*}} = \frac{\mathbf{v}_{Iso}}{\mathbf{v}_{p}}, \ \mathbf{v}_{Iso} = \mathbf{v}_{R} \tag{5}$$

$$\frac{(1/a)_{p}}{(1/a)_{180}} = (1 - E) \left(\frac{v_{180}}{v_{p}} \right) + E$$
 (6)

The fuel-air ratio through the probe was normalized by the fuel-air ratio determined by the inlet fuel flow divided by the inlet airflow.

$$\frac{(f/a)_{p}/(f/a)_{mean}}{(f/a)_{180}/(f/a)_{mean}} \circ (1 - E) \left(\frac{v_{180}}{v_{p}}\right) + E \tag{7}$$

$$E = \left[\frac{(t/a)_p/(t/a)_{mean}}{(t/a)_{tso}/(t/a)_{mean}} - \frac{v_{tso}}{v_p} \right] / \left(1 - \frac{v_{tso}}{v_p} \right)$$
 (8)

Figure 7 is a typical plot. The degree of vaporization is 0.84; that is, 84 percent of the fuel has vaporized.

RESULTS AND DISCUSSION

The spatial fuel distribution, degree of vaporization, and pressure drop data will be discussed for the injector configurations tested. Data was taken at the following test conditions: inlet air temperature, 600 K (620° F), inlet air pressure, 0.3 and 0.5 MPa (3 and 5 atm); reference velocity, 20 m/sec (66 ft/sec); and fuel-air ratios of 0.010 and 0.025. If a satisfactory spatial fuel distribution was obtained, the inlet temperature was raised to 800 K (980° F) (facility maximum) with the other conditions the same. Lower inlet temperatures were used to obtain vaporization data.

Spatial Fuel Distribution

Multiple-jet injectors. The spatial fuel distribution obtained with the multiple-jet contrastream fuel injector (fig. 2) is shown in figure 8. With the radial injection 1.9 cm from the wall (68 percent of the radius) the profile was center p-aked. Moving the radial injection point to 1.3 cm from wall (78 percent of the radius) improved the distribution significantly. Decreasing the distance from the wall to 0.95 cm (84 percent of the radius) only slightly improved the distribution. At the radial injection distance of 1.3 and 0.95 cm the fuel distribution is within ±20 percent of the average.

In figure 9 the spatial fuel distribution obtained with the multiple-jet cross-stream fuel injector (fig. 3) is presented. Nearly uniform distribution was obtained, local values of fuel-air ratio were within ±10 percent of the average value.

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The mixing length was reduced from 39.4 cm (15.5 in.) to 25 cm (9.9 in.) and the fuel distribution abtained is plotted in figure 9(b). The distribution was not as uniform us that obtained using the longer length but still within 415 percent of the average.

Eplash-greave fuel injector. The spatial fuel distribution for the splash-greave fuel injector is shown in figure 10. The profile obtained using the 12-cm (4.75-in.) inlet diameter was very fuel rich in the center. Reducing the inlet diameter to 7.6 cm (3.0 in.) survived the profile significantly. The profile became nearly uniform, within ±10 percent, when a 15° vane angle air swirler was added. Increasing the vane angle to 30° also resulted in fuel-air distributions within ±10 percent of the average value (see fig. 10(b)).

Simplex pressure atomizer. The spatial fuel distribution for the giaplex pressure atomizer is shown in tigure 11. The penetration of the fuel into the airstream was small since the fuel distribution was center peaked at the Conditions tested and when an air swirler was not used. In contrast with the splash-graove results, the distribution was approximately the same with a 10.2 cm (4.0 in.) and 7.6 cm (3.0 in.) inlet. At the lower inlet air temperature of 450 K (3500 F), the penetration was even less. The increase in air density with temperature seems to have a greater effect on penetration than the increased pressure drop across the nozzle (feel pressure drop increases because the sirflow has to increase to maintain the same velocity at the lower inlet air temperature and thus fuel flow has to increase to maintain the same fuel-sir ratio).

Adding a 30° vane angle air swirler resulted in a more uniform profile (see fig. 11(a)). The distribution was within ±15 percent of the average except there remained one quadrant in which the fuel-air ratio was high at the wall. This effect was more pronounced when a 15° vane angle air swirler was used. As the swirler was rotated the location of this rich zone would rotate. Only the fuel tube was uncyamotrical and there may have been some interaction between the swirler and fuel tube.

Spraying the fuel upstream or contrastream the profile was nearly uniform (within ±10 percent of the average) using a swirler with 30° vane angles (see fig. 11(b)). The profile was still center peaked with the use of a 10° vane angle air swirler. The rich zone which was present when the fuel was sprayed costream was not present with upstream injection.

Senicore fuel injector. The Sonicore fuel Injector also had a center peaked fuel profile (see fig. 12) with the configuration (fig. 6) tested without an air swirler. With the addition of a 9° vane angle air swirler, the profile improved but was not symmetrical. Since the only thing that was not symmetrical was the fuel tube and air-assist tube, there must have been interaction between the tubes and the swirler. The profile improved when the swirler blade angle was increased to 12° and the fuel-air distribution was within ±10 percent of the average when a 30° vane angle air swirler was used.

The mixing length was decreased from 35.6 cm (14.0 tm.) to 24 cm (9.5 im.) and the results are presented in figure 12(b). The fael-air distribution was within ±15 percent of the average with a 24-cm mixing length.

Vaportantion Data

The degree of vaporization was determined with the opillover technique. The measurements were taken in the center of the duct and the injectors were tested without air swirlers.

The degree of vaporization as a function of inlet air temperature is shown in figure 13 for the multiple-jet cross-stress injector, the optach-groave injector, the Sonicore nozzle, and the simplex nozzle. The multiple-jet cross-stress and splash-groave injectors gave the highest percent vaporizated fuel, followed by the Sonicore and then the simplex nozzle. At an inlet air temperature of 500 K (340° F) the percent of fuel vaporized was 95 for the multiple-jet cross-stress injector, 94 for the splash-groave, 87 for the Sonicore, and 61 for the simplex nozzle.

Calculation of the mean drop size for the varieus injectors should indicate the relative rates of fuel vaporization. Drop size calculations were made for the following inlet conditions: reference voluctty of 20 m/see (66 tt/sec), pressure of 0.5 MPa (5 atm), inlot air temperature of 500 K (440° F), and fuel-air ratio of 0.01. For the airblast injectors (multiple-jet cross-stream and aplush-groove) . the Sauter mean drop size was calculated using the correlations of Nuklyama-Tananawa (as given in ref. 9) to be 69 pm and from Lorenzette and Lofebvre (10) to be 71 µm. For the aimplex pressure atomizer the Sauter mean drop size was calculated to be between 60 and 100 pm using the correlations given in reference 10. Using the correlation given in referonce 11 for a simplex pressure atomizer the Sauter mean drop size come out to be 74 am. Data from the manufacturer indicates the drop size of the Soulcore nozzle to be less than 20 and.

The vaporization data, however, implies that the airblast configurations had the smallest initial drop sizes. A possible explanation is that the correlations for the airblast injectors were developed for atmospheric air pressure and at 0.5 MPa (8 atm) the drop size may be much smaller. The drop sizes of the Senicore nozzle may have been smaller than the airblast injectors and still had lower vaporization rates. This is because the air for the air-assist was at ambient conditions and thus the drops were initially surrounded by air at a much lower temperature.

Vaporization data was taken at pressure levels of 0.3 and 0.5 MPa (3 and 5 atm). In figure 14 the degree of vaporization using the multiple-jet cross-stream injector is plotted against inlet air temperature for the two pressures. The vaporization rates are higher at the higher pressure. At an inlet air temperature of 450 K there was about 7 percent ware fuel vaporized at the higher pressure. Evidently, at these conditions, the effect of higher heat transfer rates at the higher pressure is greater than the higher partial pressures needed for vaporization.

Pressure Drop

At a reference velocity of 20 m/sec, an inlet air temperature of 600 to 800 K and an inlet pressure of 0.5 MPa (5 atm), the pressure drop from the injector to the sample probes was less than 0.5 percent of the inlet total pressure for the injectors tested without swirlers. With a 30° air swirler the pres-

oure drep was approximately I percent. For an automative application it is desired to keep the combuster total pressure loss below I percent. A 2 percent pressure loss for the entalytic section seems inspractical (3), so a 1 percent pressure drop for the fuel injector would be acceptable.

CONCLUDING REMARKS

Uniform spatial fool distribution and a high degree of Vaporization with acceptable total pressure loss were obtained at the conditions tested. At an air inict temperature of 800 K, coal flame reactions were observed. Advanced automative gas turbine eyeles call for much higher combustor inict temperatures and thus dwell time may have to be reduced to prevent autoignition of the fuel. For a catalytic combustor uniform velocity profiles would also be necessary. Velocity measurements were not made in this study. Nonuniform velocity profiles would be very likely to occur with configurations using air swirlers, capacially as the vaporizor length is shortened.

Summary of Results

Several fuel injectors were tested for spatial fuel-air distribution, degree of fuel vaporized, and total pressure drop. The multiple-jet cross-atream fuel injector with 28 distributed fuel injection locations and a mixing length of 39.4 cm (15.5 in.) gave the heat results. Fuel-air spatial distributions that were within ±10 percent of the mean were obtained, 100 percent of the fuel was vaporiz 1 at an inlet air temperature of 600 K (620° F), and the pressure was less than 0.5 percent. A multiple-jet contrastress fuel injector with eight fuel injection locations and a mixer length of 39.4 cm (15.5 in.) had spatial fuel-air distributions within ±20 percent of the mean.

With the splash-groove, Sonicore and simples fuel injectors the fuel was injected from the center of the duct and center peaked proffles were obtained. The use of air swirlers improved the mixing so that fuel-air opatial distributions that were within ±10 percent of the mean were obtained. The a r ... lengths were 33 cm (13.0 in.) for the aplash gr * cm (14.0 in.) for the Sonfcore and 33.7 cm (13.23 in.) for the cimplex. The use of air swirlers is not desired for a cutolytic combustor, however, since nonuniform velocity profiles result, especially as the wixer length is decreased. The use of a 300 want angle air swirler also increased the pressure drop irom 0.5 to 1.0 percent. Of these injectors the splash. groove gave the best vaporization regults (100 percent of the fuel vaporized at an inlet air temperature of 600 K (620° F)) and the simplex the poorest (80 percent at 600 K. The Sonicore vaporization results (96 percent at 600 K) would have been better if the air for the air-assist would have been preheated rather than at ambient temperature.

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Figure L. - Rig schematic. (Dimensions in cm (in.)

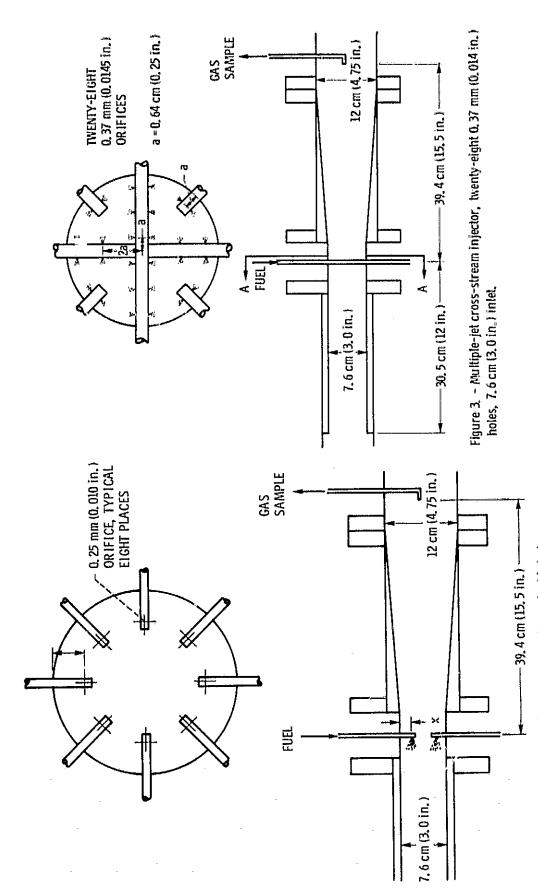


Figure 2 - Multiple-jet contra-stream fuel injector.

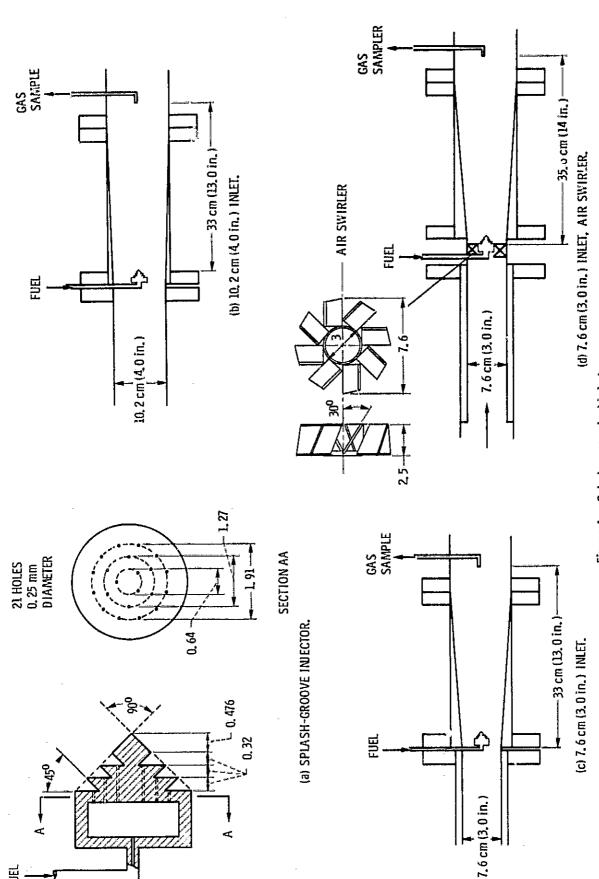


Figure 4. - Splash-groove fuel injector.

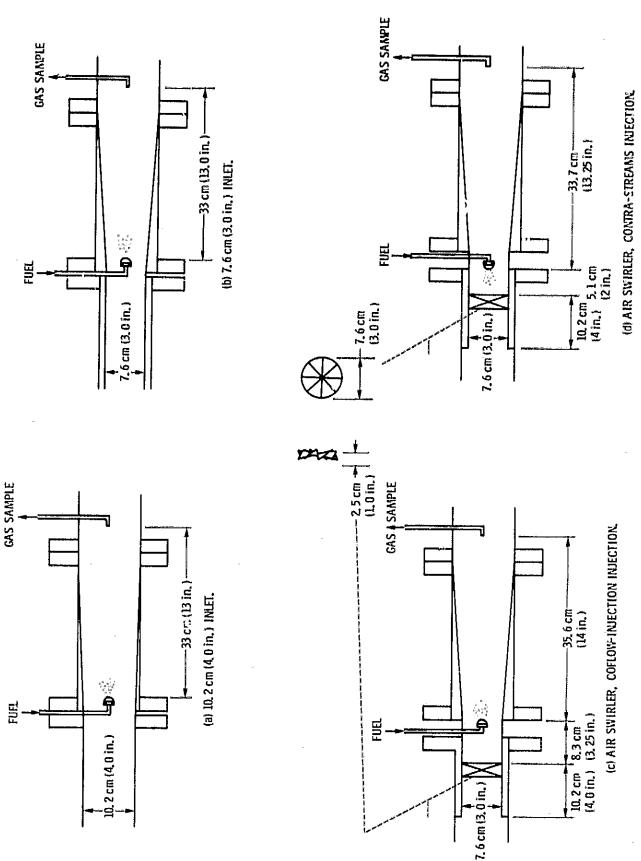


Figure 5. - Simplex pressure atomizer configurations.

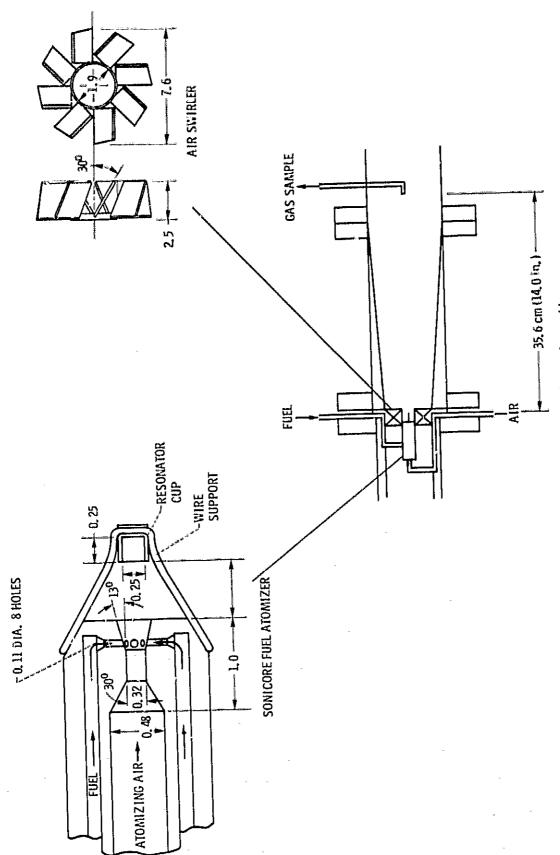


Figure 6. - Sonicore fuel atomizer and assembly.

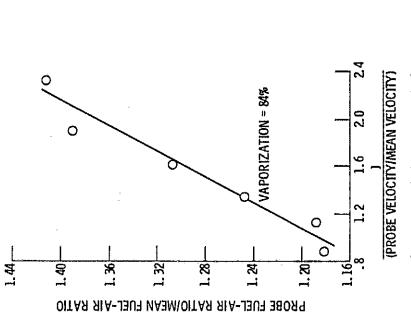
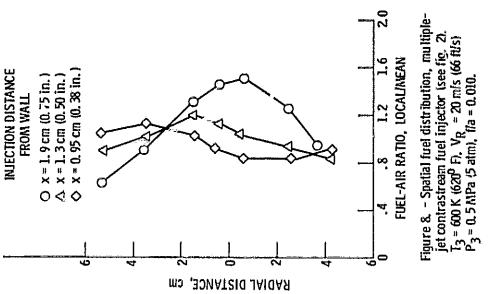


Figure 7. - Typical plot used to obtain degree of vaporization. Multiplejet cross-stream injector, 29.5 cm vaporization length, $T_{in} = 444 \text{ K}$ (339⁹ F), $V_{R} = 20 \text{ m/s}$ (66 ft/s), $P_{in} = 0.5 \text{ MPa}$ (5 atm), $f_{Iamean} = 0.010$.



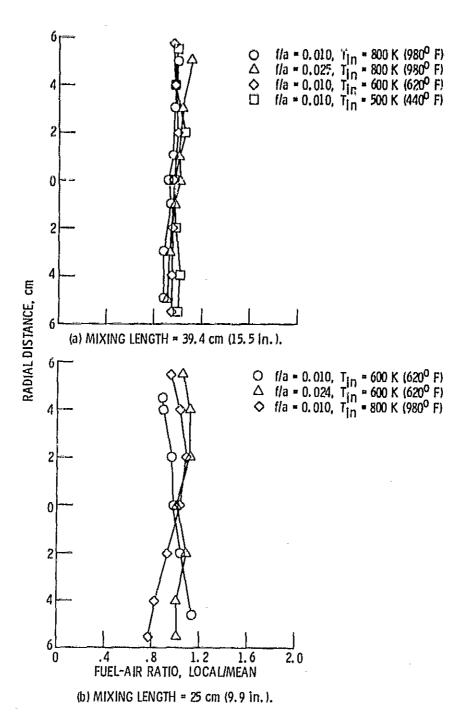
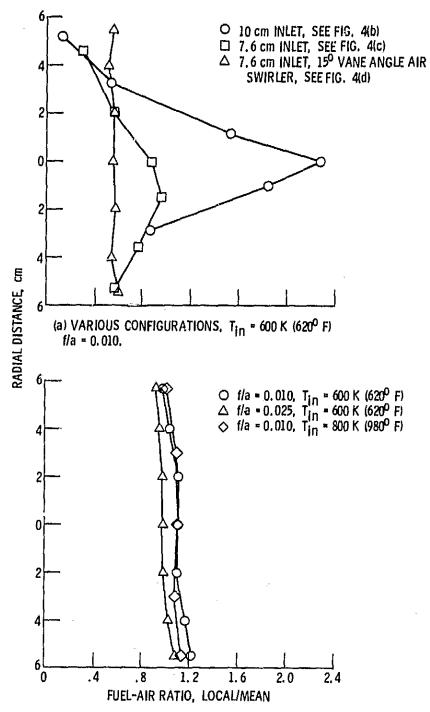
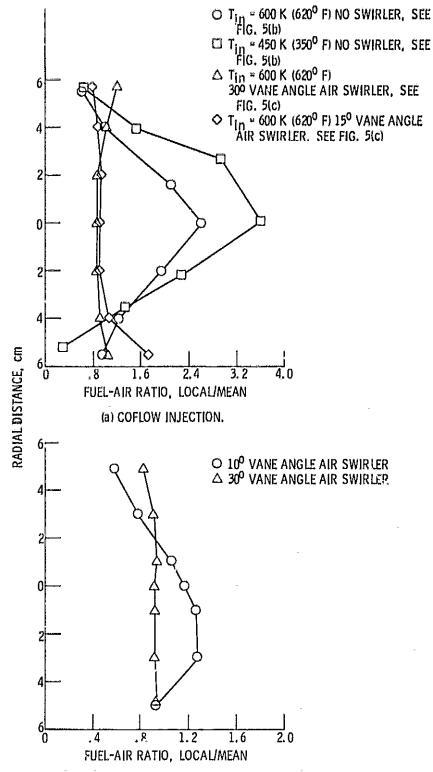


Figure 9. - Spatial fuel distribution, multiple-jet cross-stream injector (see fig. 3). V_R = 20 m/s (66 ft/s), P_{in} = 0.5 MPa (5 atm).



(b) 7.6 cm INLET, $30^{\rm O}$ VANE ANGLE AIR SWIRLER, SEE FIG. 4(d).

Figure 10. - Spatial fuel distribution, splash-groove ruel injector.



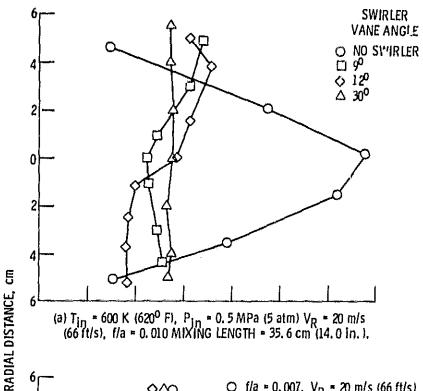
(b) CONTRASTREAM INJECTION (SEE FIG. 5(d)) T_{1n} = 600 K (620° F).

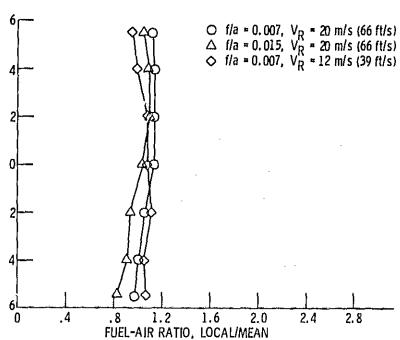
Figure 11. - Spatial fuel distribution, simplex pressure atomizer.

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(b) MIXING LENGTH = 24 cm (9.5 in.) T_{in} = 800 K (980° F), P_{in} = 0.3 MPa (3 atm), 30° vane angle air swirler.

Figure 12. - Spatial fuel distribution, sonicore fuel nozzle, see fig. 6.

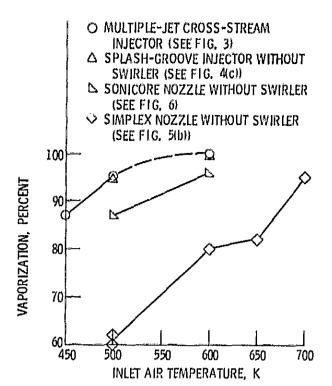


Figure 13. - Effect of inlet air temperature on degree of vaporization for various fuel injectors. Vaporization length nominally 36 cm, V_R = 20 m/s (66 ft/s), P_{in} = 0.5 MPa (5 atm), f/a = 0.010.

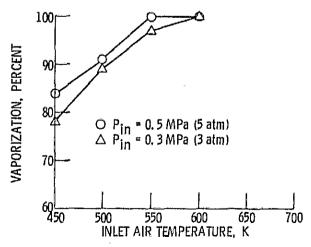


Figure 14. - Effect of inlet air temperature on degree of vaporization for the multiple-jet cross-stream injector at 0.3 MPa (3 atm) and 0.5 MPa (5 atm). Vaporization length = 29.3 cm, $V_R = 20 \text{ m/s}$, f/a = 0.010.