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Exploration of low-cost agro-industrial waste substrate for cellulase and xylanase production using *Aspergillus heteromorphus*

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Abstract

The current study was executed to explore the nutritive potential of low-cost agro-industrial waste substrates including anaerobically treated distillery spent wash (ADSW) and rice straw (RS) for enzyme production (cellulase and xylanase). The statistical model, Box–Behnken Design (BBD), was utilized to optimize the enzyme production through *Aspergillus heteromorphus* under liquid state bioconversion on examining the interactive interaction between substrate (ADSW), co-substrate (RS), temperature and initial pH. The BBD results revealed that the optimum levels of different factors for enzymes production were 6% ADSW, 3% RS, pH 5 and temperature 32.5 °C. The highest exoglucanase, xylanase and endoglucanase enzyme activities under optimum conditions were 6.3 IU/mL, 11.6 IU/mL and 8.1 IU/mL, respectively. The results confined that the agro-industrial waste substrate could be a cost-effective and eco-friendly alternative to produce value-added products like enzymes.

Keywords Enzyme · Rice straw · Distillery spent wash · Overlay contour plots · BBD

Introduction

The management of agro-industrial waste is very important as it poses a serious threat to the environment. A large amount of agro-industrial waste like rice straw, wheat straw, rice husk, bagasse, industrial effluents, sludge, etc., are produced annually, which create problem associated with disposal of these solid and liquid waste. The management of by-products is an augmented approach to achieve low carbon dioxide emissions (Weber and Stadlbauer 2017). The agricultural residues left after harvesting are either burned on-site (which creates air pollution and affects soil quality) or stored in the form of heaps in the field. Therefore, management of the agricultural waste is becoming one of the serious issues nowaday. However, solid

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waste can be utilized as a potential source for the production of a variety of value-added industrially useful products including enzyme, chemicals, biofuel and animal feed (Mohana et al. 2008; Mathioudakis et al. 2017). The industrial effluent like distillery spent wash produced from ethanol manufacturers generates a large volume of high strength wastewater that poses a serious threat to the water quality of surrounding area. India being the second largest producer of alcohol, contribute to huge amount of spent wash through distilleries (Mohana et al. 2009). Around 400 distillery units are operated in India, which produce around 3800 million L of alcohol (MOEFCC, India). On an average, each distillery produces 8-15 L of spent wash for generation of each liter of alcohol, depending upon raw material used, quality of raw material and process (Saha et al. 2005). Considering its polluting nature, distilleries are counted as one of the 17 most polluting "Red Category" industries (Krishnamoorthy et al. 2017). The wastewater generated in form of spent wash is enriched with high quantity of dissolved organic and inorganic content. Proper handling and disposal of the wastewater is required to avoid any damage to the environment. Therefore, environment regulation authorities are much concerned and enacted strict norms and regulate proper discharge of industrial effluents into the environment (Mohana et al. 2009). The discharge of untreated or partially treated ADSW into the environment may cause serious health



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and ecotoxicological threats (Chowdhary et al. 2018). Several approaches are widely utilized for the treatment of distillery wastewater including physical, chemical and biological, but anaerobic treatment is widely accepted practice (Pettigrew et al. 2015). Though, anaerobically treated effluent cannot be discharge directly into the environment due to enriched proportion of organic matter in form of biochemical oxygen demand (BOD) and chemical oxygen demand (COD) (Nandy et al. 2002). The anaerobically treated wastewater contains micro-(potassium, sodium, nitrogen, phosphorus) and macro-(Ca, Cu, Mn, and Zn) nutrients, which can be utilized to meet the requirement of crops through irrigation fields and production of value-added products like enzyme, biosurfactant, polyunsaturated fatty (Mohana et al. 2008; Chapla et al. 2010; Singh et al. 2010).

The agro-industrial waste can be used for the production of commercially important products like enzyme due to their nutritional potential. Enzymes like cellulase and xylanase have industrial importance and widely used in various industries including textile, pulp and paper, laundry and detergent, wine and brewery, food processing, agricultural industries and bio-ethanol production (Mohana et al. 2008; Kuhad et al. 2011). The cost of these enzymes is a big issue faced by these industries, and efforts are going on to reduce the cost by strain improvement, better fermentation and recovery system and utilization of easily available low-cost substrates (Xu et al. 2005; Ahamed and Vermette 2008). Enzymes like cellulase and xylanase play a very significant role in lignocellulosic biomass to biofuel conversion process. Therefore, production of cellulase and xylanase enzymes from underrated biomass rice straw and industrial effluent anaerobically treated distillery spent wash can be economically beneficial in various industries. In the previous study (Singh et al. 2010), comparison of ADSW and mineral media for laccase production was studied and found that ADSW gives better results than mineral media. Media components, and their concentration, substrate, fungal species and process parameters play a very important role in maximizing cellulase enzyme production (Hu et al. 2018; Sreena and Sebastian 2018). Therefore, aim of the present study was to explore the feasibility and optimization of ADSW and rice straw substrates for enzyme production. Box-Behnken Design (BBD) of response surface methodology (RSM) was exploited further to assess the interactive effects of substrates (ADSW and RS) and other parameters (initial pH and temperature) on production of beneficial enzyme by fungi A. heteromorphus.

Materials and methods

Substrate, fungal culture and inoculum preparation

Anaerobically treated distillery spent wash (ADSW) and rice straw (RS) (Singh et al. 2010) were used as a substrate



and co-substrate, respectively, for enzyme (cellulase and xylanase) production. Fungal strain *Aspergillus heteromorphus* (MTCC 8625) was maintained on potato dextrose agar (PDA) plates for spore production. The fungal strain was cultured on PDA slant for 07 days and incubated at constant temperature condition of 32 °C. After a week of incubation, sterilize distilled water was added to the slant and spore suspension was made by scraping of surface gently with sterilized glass rod. The spore concentration in aqueous suspensions was determined using a hemocytometer.

Experimental procedure for cellulase and xylanase production

Rice straw (1-5% (w/v)) was added to 50 mL of 2-10% (w/v) anaerobically treated distillery spent wash (ADSW) in 250 mL Erlenmeyer flask as per design matrix of Box–Behnken Design (BBD) (Table 1). pH of the mixture was maintained from a range of 4.0–6.0 by adding 1 N HCl or 1 N NaOH. The sample was sterilized in autoclave at temperature 121 °C and pressure condition at 15 psi for 30 min. After sterilization samples were inoculated with fungal spore inocula of 1.8×10^8 /mL. The samples were incubated at temperature varied from 30 °C to 35 °C in incubator shaker at agitation speeds of 125 RPM for enzyme production. Samples were collected after 05 days of fermentation to analyze the enzymatic activities.

Box–Behnken design for optimization of the parameters for cellulase production

Microbial growth and activities are deeply affected by nutrients and process parameters. Moreover, the nutritional and non-nutritional parameters play an important role in enzyme production by microbes. Therefore, in the present study, 04 important parameters including substrate concentration (Anaerobically treated Distilleries Spent Wash (ADSW), 2–10%) (A); co-substrate concentration (Rice Straw (RS), 1-5%) (B); initial pH 4.0-6.0(C) and temperature 30-35 °C (D) were chosen as the independent variables for production of cellulase and xylanase enzyme as dependent response (Table 1). Box-Behnken Design (BBD) of Response Surface Methodology (Box and Wilson 1951) was used to study the optimum conditions for enzyme production and to explore the interactive effect of 04 independent factors on enzyme production. In Box-Behnken Design, each variable was studied at 03 levels; therefore, a total of 27 experiments were designed by the software for the current study. Overall second-order polynomial mathematical relationship was used to express enzyme activity (Y_1) a function of independent variables as follows:

 Table 1
 Experimental design in terms of coded factors and results of the Box–Behnken model

Sr. no.	Sub. conc. (%w/v)	Co-sub. conc. (%w/v)	pН	Temp. (°C)	X	Y	Z
1	-1	- 1	0	0	2.5	7.5	7.3
2	1	-1	0	0	2.1	7.2	7.1
3	-1	1	0	0	3.2	7.6	7.9
4	1	1	0	0	3.2	8	8.1
5	0	0	- 1	-1	3.3	7.8	7.9
6	0	0	1	-1	3.0	8.1	7.9
7	0	0	- 1	1	3.4	8.5	8.5
8	0	0	1	1	3.6	8.6	8.5
9	-1	0	0	-1	2.5	7.7	7.4
10	1	0	0	-1	2.6	7.9	8.1
11	- 1	0	0	1	2.9	8.1	8.3
12	1	0	0	1	2.4	7.8	8
13	0	-1	-1	0	2.7	7.6	7.7
14	0	1	-1	0	3.6	8.4	8.3
15	0	-1	1	0	2.9	7.9	7.5
16	0	1	1	0	3.8	8.1	8.3
17	- 1	0	- 1	0	1.8	6.6	6.7
18	1	0	-1	0	1.6	6.8	6.8
19	- 1	0	1	0	1.8	6.8	6.7
20	1	0	1	0	2.1	6.8	6.8
21	0	-1	0	-1	3.8	8.9	8.7
22	0	1	0	-1	4.9	9.5	9
23	0	-1	0	1	4.3	9.1	9.3
24	0	1	0	1	5.3	9.8	7.3
25	0	0	0	0	6.3	11.5	7.1
26	0	0	0	0	6.5	11.5	7.9
27	0	0	0	0	6.3	11.6	8.1
28	-1	-1	0	0	6.2	10.9	8
29	1	-1	0	0	6.1	11.4	7.8

X = Cellulase/exoglucanase enzyme activity (IU/mL) by A. heteromorphus

Y = Xylanase enzyme activity (IU/mL) by A. heteromorphus

Z=CMCase/endoglucanase enzyme activity (IU/mL) by A. heteromorphus

$$Y_{1} = b_{0} + b_{1}A + b_{2}B + b_{3}C + b_{4}D + b_{11}A^{2} + b_{22}B^{2} + b_{33}C^{2} + b_{44}D^{2} + b_{12}AB + b_{13}AC + b_{14}AD + b_{23}BC + b_{24}BD + b_{34}CD$$
(1)

where Y_1 is the predicted response; b_0 is the intercept; b_1 , b_2 , b_3 , b_4 are linear coefficients; b_{11} , b_{22} , b_{33} , b_{44} are squared coefficients; b_{12} , b_{13} , b_{14} , b_{23} , b_{24} , b_{34} are interaction coefficients with independent variables, A (substrate concentration), B (co- substrate concentration), C (pH) and D(temperature). The results of the experimental design were analyzed and interpreted using Minitab (trial version 15.0) and "Design Expert" software (trial version 8.1.1, Stat-Ease, Inc., Minneapolis, USA).

Enzyme extraction and analytical analysis

The microcosm containing the substrate and co-substrate under defined incubation condition as per design order was recovered after 05 days and homogenize for further processing of the samples. The homogenate from each flask was filtered through muslin cloth, and the filtrate was centrifuged in refrigerated centrifuge at 4 °C on 7200 RPM for 20 min. The supernatant was further used to analyze enzyme activities. Filter paper activity (exoglucanse) and endoglucanase (CMCase) activity were determined following the Ghose's method as suggested in the literature (Ghose 1987). The xylanase activity was determined by using oat spelt xylan as substrate (Singh and Bishnoi 2013). The reduced sugars released were analyzed using the DNS assay (Miller 1959). Cellulose, hemicellulose



and lignin content were estimated by the method of Goering and Van Soest (1970).

Results and discussion

Box-Behnken Design (BBD) was used to study the linear, quadratic and interactive effects of independent variables considered for the current study on cellulase and xylanase enzyme production by A. heteromorphus. The polynomial equation, describing the cellulase and xylanase enzyme production by A. heteromorphus as a simultaneous function of the ADSW (A), RS (B), initial pH (C) and temperature (D), is shown in Eqs. (2-4).

$$X = +6.16 - 0.067 * A + 0.47 * B + 0.092 * C + 0.15 * D$$

- 2.66 * A² - 0.92 * B² - 2.02 * C² - 0.96 * D²
+ 0.10 * A * B + 0.13 * A * C - 0.17 * A * D
+ 0.000 * B * C - 0.075 * B * D + 0.10 * C * D
(2)

$$Y = +11.38 + 0.017 * A + 0.27 * B + 0.050 * C + 0.17 * D$$

- 2.55 * A² - 1.20 * B² - 2.15 * C² - 0.93 * D²
+ 0.18 * A * B - 0.050 * A * C - 0.13 * A * D
- 0.15 * B * C + 0.025 * B * D - 0.050 * C * D
(3)

$$Z = +7.78 + 0.050 * A + 0.11 * B - 0.017 * C + 0.075 * D$$

- 0.58 * A² + 0.33 * B² - 0.28 * C² + 0.64 * D²
+ 0.10 * A * B + 0.000 * A * C - 0.25 * A * D
+ 0.050 * B * C - 0.058 * B * D + 0.000 * C * D
(4)

where X, Y and Z are observed response as cellulase enzyme activity (IU/mL), xylanase enzyme activity (IU/mL) and endoglucanase or CMCase enzyme activity (IU/mL), respectively. The coefficient of determination (R^2) was used to check the fitness of the model. The closer value of the R^2 to 1 showed a good fit between the predicted response and experimental values. The coefficient of determination R^2 for the above-predicted Eqs. (2), (3) and (4) was 99.27%, 99.16% and 72.8%, respectively. The estimated regression coefficient (R^2) and corresponding p value for the cellulase and xylanase enzyme activities are shown in Table 2. The results revealed that the coefficient for the quadratic effects of ADSW, RS, initial pH, and temperature was highly significant for all responses.

As shown in Table 1, cellulase enzyme activity varied from 1.6 to 6.5 IU/mL, whereas xylanase and endoglucanase enzyme activities showed variations from 6.6 to 11.6 IU/ mL and 6.7-8.1 IU/mL, respectively, under variable conditions, as prescribed in BBD design order. Overlaid contour plots Fig. 1a-f showed interactive effect of the studied variables-pH, temperature, RS conc. and ADSW conc. on enzyme production as dependent variable. Multiple contour plots are overlaid over one another in a single graph, and the white area in these overlaid contour plots will shows the range of two variables where the criteria for all response variables are satisfied. These plots are used to find the bestoperating conditions for maximizing the response. Figure 1a showed the interactive effect of rice straw (RS) and ADSW concentration on enzyme activities (exoglucanase, xylanase and endoglucanase), and as per the white portion of overlay contour plots highest enzyme activities observed at middle value of both variables. Exoglucanase and xyalanse

Table 2 Estimated regression coefficient and corresponding	Source	Cellulase		
<i>p</i> value for cellulase, xylanase		Coff	<i>p</i> -value	
and CMCase production by A. heteromorphus	Constant	6.16	0.00	
	Α	-0.067	0.233	
	В	0.47	0.00	
	С	0.092	0.108	
	D	0.15	0.014	
	A^2	-2.66	0.00	
	B^2	-0.92	0.00	
	C^2	-2.02	0.00	
	D^2	-0.96	0.00	

Source	Cellulase		Xylanase		CMCase		
	Coff	<i>p</i> -value	Coff	<i>p</i> -value	Coff	<i>p</i> -value	
Constant	6.16	0.00	11.38	< 0.0	7.78	0.03	
Α	-0.067	0.233	0.01	0.77	0.05	0.73	
В	0.47	0.00	0.26	0.00	0.10	0.46	
С	0.092	0.108	0.05	0.39	-0.01	0.90	
D	0.15	0.014	0.16	0.01	0.075	0.61	
A^2	-2.66	0.00	-2.55	< 0.00	-0.57	0.01	
B^2	-0.92	0.00	-1.20	< 0.00	0.33	0.11	
C^2	-2.02	0.00	-2.15	< 0.00	-0.27	0.17	
D^2	-0.96	0.00	-0.92	< 0.00	0.63	0.006	
AB	0.10	0.298	0.17	0.09	0.1	0.69	
AC	0.13	0.198	-0.05	0.61	0	1.00	
AD	-0.17	0.079	-0.12	0.22	-0.25	0.33	
BC	0.00	1.0	-0.15	0.14	0.05	0.84	
BD	-0.075	0.43	0.02	0.80	-0.57	0.03	
CD	0.10	0.298	-0.05	0.61	0	1.00	
Lack of fit		0.054		0.94		0.29	





Fig. 1 Overlaid contour plot for the effects of **a** ADSW (% v/v) and RS (% w/v), **b** pH and ADSW (% v/v), **c** pH and RS (%w/v), **d** pH and temperature (°C), **e** temperature (°C) and ADSW (% v/v), **f** RS (%w/v) and temperature (°C), on enzyme production by *A. heteromorphus*

activities share the same optimum range of ADSW conc. for maximum enzyme activity, but different optimum range of rice straw concentration as 3.5% for exoglucanase and 3.0% for xylanase activity. Highest endoglucanase activity was observed at 6.3% ADSW conc. and 4.7% rice straw conc., slightly higher than the middle value of studied variables.

Figure 1b shows the interactive effect of pH and ADSW conc. on enzyme activities. The white portion of Fig. 1b shows that maximum enzyme activities were observed at middle value of both ADSW conc. and pH, i.e., 4–8% of ADSW and 4.5–5.5 of pH.



The concentration of substrate exhibits linear behavior with the enzymes activities up to the middle tested level; however, the substrate concentration at higher level (10%) affects adversely the cellulase, xylanase and endogluconase production by A. heteromorphus. The antagonistic relationship of ADSW at higher concentration with the enzyme production by A. heteromorphus might be because of toxicity caused by higher ADSW concentration to the microbes, which adversely affects the culture growth and enzyme activity. The distillery effluent is enriched in organic content (BOD, COD, TOC) along with various macro- and micro-nutrient including total nitrogen, calcium, potassium, phosphates, phenolic compounds, sulfates and other solids which help in microbial growth (Singh et al. 2010). Chapla et al. (2010) studied the xylanase enzyme production by A. foetidus MTCC 4898 on utilizing ADSW and wheat bran as substrate and co-substrate, respectively. Further, it was claimed that A. foetidus exhibited higher yield of xylanase enzyme production and specific activity with ADSW when compared to MS media and tap water. Acharya et al. (2010) studied cellulase enzyme production by fungus A. ellipticus using ADSW and revealed that the fungi flourished very well and support enzyme production, even in soaring concentrations of distillery effluent.

The carbon source supplied to microorganisms is also crucial for enzyme production; therefore, the selection of carbon source is very important. The interaction between RS conc. and pH on all enzyme activities is shown in Fig. 1c. In this case, pH 5.0 was optimum for all enzyme activities, but optimum range of RS conc. varied as 3.4% for exoglucanase activity, 3.0% for xylanase activity and 4.7% for endoglucanase activity. Different types of carbon substrates like rice straw, wheat straw, rice husk, wheat bran, water hyacinth, sugarcane bagasse, saw dust were studied for enzyme production depending upon the need, availability, accessible surface area, particle size and physical properties of the substrate, considering their crucial role in solid state fermentation (Archana and Sayyanarayana 1997; Chapla et al. 2010). In the present study, rice straw was used as a carbon source for enzyme (cellulase, xylanase and endoglucanase) production, considering their biochemical composition, containing 38% cellulose, hemicellulose 26% and 7% lignin content. Lignocellulosic biomass is an underutilized source of biomass on planet earth, which can be used as substrate for enzyme production. Lignocellulosic biomass provides surface as well as carbon source required for microbial growth. Kulkarni et al. (1999) reported that both xylanase and cellulase enzymes were produced when cellulose and hemicellulose were used together as carbon source. Cellulase and xylanase both are inducible enzymes, and the presence of cellulose and xylan in media acted as good inducers for enzyme production (Aro et al. 2001; Nair et al. 2008).



The effect of initial pH on enzyme activities shows that as the pH increases cellulase and xylanase activities increase but up to mid-level only, further increase in pH decreases enzyme activity as shown in Table 1. The overlay contour plot of interactions between pH and temperature affecting enzyme activities is shown by Fig. 1d. Figure 1d shows that highest enzyme activities observed at middle level of pH (5.0) and temperature (32.5 °C) except for endoglucanase activity where optimum temperature was 34 °C. The initial pH of the medium is very important and critical parameter as it affects the microbial morphology, growth of mycelia, enzymatic processes and transport of various components across the cell membrane (Kapoor et al. 2008), pellet formation and coagulation of spores (Galbraith and Smith 1969). Most suitable pH range is 4.5–5.5 for the growth of most of the fungal species and their metabolites; the reason might be the suitability of extracellular enzymes at this pH, and change in this pH range may leads to denaturation of enzymes (Latifian et al. 2007). Cellulase production is affected by pH in many ways like pelleted morphology, hydrogen ion effect and stability (Kalra and Sandhu 1986). Dispersed morphology found to be associated with increased cellulase production, while pelleted morphology decrease cellulase enzyme production which might be due to hindered internal gas-liquid mass transfer (Papagianni 2004). Both these morphologies are pH dependent, and higher pH leads to pelleted morphology. Matkar et al. (2013) studied cellulase enzyme production under submerged fermentation by A. sydowii and obtained maximum enzyme activity at pH 5.5. Aggarwal et al. (2017) also found highest cellulase production by A. nigerBK01 at pH 5.5. Shrivastava et al. (1984) found maximum enzyme activity by A. wentii Pt 2804 over a pH range of 4.5–5.5 but declined sharply beyond 5.5. Ncube et al. (2012) used Jatropha curcas seed cake for cellulase enzyme production by A. niger and found optimum pH 5.0 for maximum cellulase activity. Jecu (2000) studied endoglucanase enzyme production by A. niger 38 using a combination of wheat straw and wheat bran as substrate and found that maximum enzyme activity was found at initial pH range 4.5–5.5.

Incubation temperature plays an important role in the production of enzymes and metabolic activities of a microorganism. The enzyme is a secondary metabolite, and its yield is greatly affected by the incubation temperature (Kumar et al. 2016). So, the optimum temperature is very important for enzyme production because both higher and lower temperature than the optimum value affects the process. The lower temperature affects the transport of nutrients and at higher temperature more energy is spent by the microorganism for maintaining the process (Pirt 1975). In the present study, optimization of temperature and its interaction with other variables were studied. Figure 1e showed interaction between ADSW conc. and temperature on enzyme activities,
 Table 3
 Comparative study of enzyme activities under submerged fermentation from Aspergillus strains grown on different carbon source

Organism	Substrate	Enzyme activities			References	
		FPase	CMCase	Xylanase		
Aspergillus nidulans ATCC62041	Delignified bagasse	0.26 U/ml	3.0 U/ml	_	Bagga et al. (1987)	
Aspergillus niger SBS6	Wheat bran	_	1.76 IU/ml	35.0 IU/ml	Nair et al. (2008)	
Aspergillus niger SBS47	Wheat bran	_	2.0 IU/ml	32.0 IU/ml	Nair et al. (2008)	
Aspergillus terreus	Oil palm empty fruit bunch	2.29 U/ml	50.33 U/ml	_	Shahriarinour et al. (2011)	
Aspergillus flavus SBS65	Wheat bran	_	-	6.0 IU/ml	Nair et al. (2008)	
Aspergillus fumigatus (CWSF-7)	Treated grass biomass	0.9 IU/ml	1.9 IU/ml	_	Mohapatra et al. (2018)	
Aspergillus sydowi	Sugarcane bagasse	1.33 IU/ml	1.32 IU/ml)	_	Matkar et al. (2013)	
Aspergillus heteromorphus	Rice straw	6.3 IU/ml	11.6 IU/ml	8.1 IU/ml	This work	

FPase filter paper activity, CMCase carboxymethylcellulase activity

and maximum enzyme activities were observed with 6% ADSW concentration. While in case of temperature optima, highest exoglucanase and xylanase activities were observed at 32.5 °C, while 34 °C for endoglucanase activity. Figure 1f depicted the interaction between RS conc. and temperature, and their effect on enzyme activities. In this overlay contour plot, optimum RS conc. was 3.0% for all enzyme activities. In case of temperature, similar trend is observed as in Fig. 1e in all enzyme activities. Any increase in temperature beyond optimum range had a drastic adverse effect on the enzyme production. Jecu (2000) also observed that temperature above 34 °C leads to decrease in biosynthesis of enzyme by A. niger, might be due to temperature deactivation. Gilna and Khaleel (2011) studied cellulase enzyme production by fungus A. fumigates and found 32 °C as optimum temperature for cellulase production. The higher temperature causes cell death due to alteration in the cell membrane composition and stimulate protein catabolism (Bansal et al. 2012).

Table 3 showed the comparative studies of enzyme activities obtained in present study by fungus A. heteromorphus with other Aspergillus strains using lignocellulosic biomass as substrate. There are many reports available which shows that different pH, temperatures and substrates for maximum cellulase and xylanase production using Aspergillus sp. suggesting that the optimum range of these parameters for enzyme production depends on the strain variation of the microorganism (Murao et al. 1988; Lu et al. 2003; Gautam et al. 2011). The crude on-site produced from the present study can be used for hydrolysis of lignocellulosic biomass. Acharya et al. (2010) used partially purified enzymes produced by Aspergillus ellipticus using anaerobically treated distillery spent wash and wheat straw as substrate for saccharification of wheat straw, wheat bran, rice straw, corn cobs and crystalline cellulose. Deswal et al. (2011) studied the saccharification of wheat straw by crude enzymes produced by Fomitopsis sp. RCK2010 and found reducing sugars production of 214.1 mg/g of the substrate. Kumar et al. (2016) studied saccharification of pearl millet stover by crude on-site produced enzymes and found reducing sugar concentration of 546.91 mg/g of substrate. The utilization of crude enzymes or partially purified enzymes in lieu of purified enzymes may reduce the cost of saccharification process.

Conclusions

In this study, anaerobically treated distillery spent wash and rice straw which were used as substrate and co-substrate, respectively, for enzyme (cellulase, exogluacanse and xylanase) production by *A. heteromorphus*. The optimum process conditions for maximum enzyme production under liquid state bioconversion were successfully determined by statistical method Box–Behnken design. The optimum conditions, for highest enzyme activities, as obtained from second order polynomial model, were the substrate 6% (v/v), co-substrate concentration of 3% (w/v), temperature 32.5 °C, pH 5. Further investigations will be required to explore the nutritive potential of anaerobically treated distillery spent wash and underrated natural resource rice straw for enzymes-cellulase and xylanase production, so that the developed process can be used at industry level.

Compliance with ethical standards

Conflict of interest The authors declare that there is no conflict of interest regarding the publication of this article.

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