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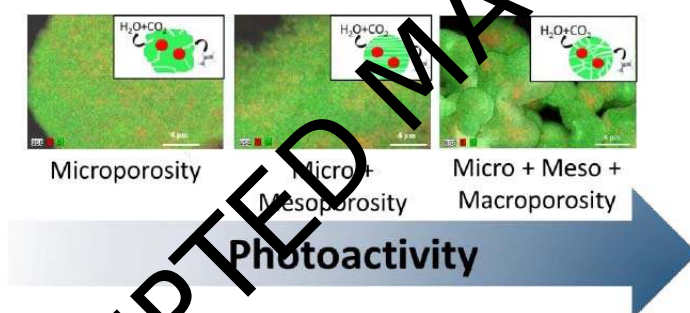
# Facile encapsulation of P25 (TiO<sub>2</sub>) in spherical silica with hierarchical porosity with enhanced photocatalytic properties for gas-phase propene oxidation

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## Graphical Abstract



## Highlights

- We present a facile encapsulation method of P25 in different SiO<sub>2</sub> materials.
- The synergetic effect between silica and TiO<sub>2</sub> favours photoactivity of P25.
- Tuning the porous texture of the SiO<sub>2</sub> matrix is key for optimizing performance.
- A hierarchical SiO<sub>2</sub> matrix provides TiO<sub>2</sub> with the best photoactivity

## Abstract

In this work, we have performed the encapsulation of a reference TiO<sub>2</sub> material (P25) in spherical silica with hierarchical porosity using a sol-gel methodology. The same P25 material has been encapsulated within a “classical” MCM-41 mesoporous silica and a precipitated silica. The materials synthesized in this work were characterized by ICP-OES, SEM, TEM, EDX, XRD, UV–VIS, TG, and nitrogen adsorption. It has been observed that the P25 samples encapsulated in silica present improved CO<sub>2</sub> production rates per mol of P25 in the photooxidation of propene, compared to P25 alone as well as the physical mixture of the two components. Moreover, the sample with a low content of P25 encapsulated in silica with hierarchical porosity presents the highest CO<sub>2</sub> production rates per mol of P25 with respect to the other P25/silica samples, due to a better accessibility of the titania phase and improved illumination of the active phase. Furthermore, the hierarchical porosity of the silica shell material favours mass transport and an increased concentration of reagents by adsorption near the titania phase. This improvement in photocatalytic activity is obtained by following a simple and reproducible synthesis methodology that employs an established silica preparation protocol. Thus, the choice of a silica with an adequate porosity for this application is proven to be a promising advancement in the development of efficient photocatalysts.

**Keywords:** TiO<sub>2</sub>, SiO<sub>2</sub>, Composites, Photocatalytic activity and Propene

## 1. Introduction

One of the most extensively researched photocatalysts over the past decades up to date is titanium dioxide (TiO<sub>2</sub>), due to its unique properties including high photocatalytic efficiency, physical and chemical stability, and relatively low cost and toxicity [1-3].

Moreover, this semiconductor is an important industrial product in many applications such as inorganic pigment, photocatalysis, sunscreen and energy storage, among others [4-10]. An interesting commercially available TiO<sub>2</sub> powder is P25 (EVONIK), which consists approximately of 80% anatase and 20% rutile titanium dioxide [11]. This commercial TiO<sub>2</sub> is widely used as photocatalyst in photochemical reactions due to its high activity both in aqueous phase and in gas phase [12]. In many cases P25 is used as benchmark material to compare the potential of different photocatalysts in both mediums [13,14].

Many factors influence the photocatalytic properties of TiO<sub>2</sub>, such as particle size, morphology, exposed lattice planes, and crystalline phase [9,15,16]. Despite the fine-tuning through which P25 has already undergone, this material presents low surface area (it is essentially a non-porous material) and low concentration of active surface groups, such as hydroxyl groups, as main drawbacks [17].

In the last years, many efforts have been made to increase the porosity of TiO<sub>2</sub> by synthesis of new nanoporous TiO<sub>2</sub> materials [18-20]. Many works have also focused on the fabrication of Ti/Adsorbent composites or supported TiO<sub>2</sub> on the surface of adsorbents to improve the aforementioned factors, with the aim of enhancing the photocatalytic activity of TiO<sub>2</sub>. The most interesting materials used as adsorbents in these composites are carbon materials, zeolites, mesoporous materials, and polymers, among others [17,21-23].

TiO<sub>2</sub>/SiO<sub>2</sub> materials have attracted a great deal of attention due to the advantages of SiO<sub>2</sub> as support or as component of composites, due to its tunable surface area and pore size, as well as interconnectivity of the pore network facilitating mass transport, high surface acidity (presence of Ti-O-Si) species, abundant surface hydroxyl groups and transparency in a wide wavelength range in the UV/Vis region [17,24].

Some studies have pointed out that the photocatalytic activity of TiO<sub>2</sub>/SiO<sub>2</sub> composites is worse than that of the pure TiO<sub>2</sub> due to a blocking effect exerted by the silica on the active phase. For example, K. J. Nakamura et al showed a decreased rate of photocatalytic degradation of methylene blue when using TiO<sub>2</sub> encapsulated in SiO<sub>2</sub> [25]. Another report by M. Nussbaum et al demonstrated that as the thickness of the SiO<sub>2</sub> shell (measured in SiO<sub>2</sub> layers prepared by chemisorption-oxidation cycles according to the authors) around the TiO<sub>2</sub> photocatalyst decreased the activity of the active phase [26].

On the other hand, many studies show that the presence of SiO<sub>2</sub> with TiO<sub>2</sub> particles is not deleterious. In fact, several reports point out that silica favours the photoactivity of TiO<sub>2</sub> [27-30]. In the last years, many efforts have been made to synthesize a nanostructured photocatalyst with enhanced absorption and molecular-sieving properties, with tunable conformations, as well as improved mass transfer in order to optimize the activity of the photocatalyst. In this aspect, S. Wang et al synthesised Core(TiO<sub>2</sub>)@shell(SiO<sub>2</sub>) nanoparticles, with a void interlayer [31]. Another approach was carried out by Y. Kurihara et al where they developed yolk-shell nanostructured photocatalysts, consisting of TiO<sub>2</sub> nanoparticles in the core of spherical hollow silica shells [32]. Also, Y. Chen et al synthesised TiO<sub>2</sub>/SiO<sub>2</sub> and TiO<sub>2</sub>/ZrO<sub>2</sub> nanocomposites with hierarchical macro/mesopores [29]. In all cases the authors intended the preparation of well-defined porous textures of their composites in order to favour mass transport and the selective concentration of reagents on the photoactive surface so as to optimize the photocatalytic activity. Some authors used this type of composites for the selective degradation of molecules due to the textural properties that silica brings forth to the composite [31,33].

Considering the extensive background, this work approach consists of a facile and reproducible synthesis of TiO<sub>2</sub>/SiO<sub>2</sub> composites through the encapsulation of commercial P25 in silica materials with markedly different porous textures (combining micro, meso, and macro-porosity in the best case scenario) in order to improve the photocatalytic activity by enhancing the adsorption characteristics of the composites (see [Scheme 1](#)). In this respect, the use of a silica shell displaying hierarchical porosity favours the aspects commented previously. Also, this work studies the effect of the percentage of P25 encapsulated in the silica with hierarchical porous texture in order to test the illumination efficiency and optimize the photocatalytic activity. This type of study, has not been undertaken through this approach to the best of our knowledge.

The materials studied in this work will be tested in the elimination of propene since this type of composites (TiO<sub>2</sub>/SiO<sub>2</sub>) can improve the photooxidation of VOCs as reported in the literature [17,21]. Moreover, these compounds are known to be very harmful to the environment and human health [34,35]. In particular, this work deals with the removal of propene at low concentration because this molecule might be taken as a representative example of low molecular weight VOCs [36]. These results are compared to the benchmark P25 and other related materials [37,38], in order to study the effect of the porous texture of the silica on the photocatalytic performance.

## 2. Experimental section

### 2.1 Materials

Titanium Tetramethyl orthosilicate (TMOS, 99%, Sigma-Aldrich), Tetraethyl orthosilicate (TEOS, 99%, Sigma-Aldrich), glacial acetic acid (HAc, 99%, Sigma-Aldrich), Pluronic F-127 (F-127, Sigma-Aldrich), Cetyltrimethylammonium

bromide ionized (Sigma-Aldrich), urea (99%, Merck), ammonium hydroxide (NH<sub>4</sub>OH, 30%, Panreac), absolute ethanol (EtOH, 99.8%, Fisher Scientific), TiO<sub>2</sub> (P25, Rutile: Anatase/85:15, 99.9%, 20nm, Degussa) and deionized water were used in the present work. All reactants were used as received, without further purification. The ultrasonic probe equipment SONOPULS HD 2200 (BANDELIN electronic GmbH & Co. KG) was used to disperse the P25 powder in water.

## 2.2 Preparation of P25 (TiO<sub>2</sub>) encapsulated in silica with hierarchical porosity.

Commercial TiO<sub>2</sub> (Evonik P25) was encapsulated in spherical silica with hierarchical porosity following a straightforward sol-gel synthesis adapted from previous reports [39].

As an illustrative example, the synthesis of the P25 encapsulated hierarchical silica done to obtain a nominal loading of 20 wt.% TiO<sub>2</sub> was performed as follows: 0.32 g of P25 were dispersed in 10.1 g of water using an ultrasound probe (Banelin SONOPULS HD 2200) with a power of 660 W operating at 50% power for 5 min. In order to prepare the composite material, the P25 dispersion in water was mixed with 0.9 g of urea, 0.81 g of F-127 and 5.8 µl of glacial HCl. This solution was stirred for 80 min. The solution was cooled at 0 °C and 1 g of TMOS were added dropwise under vigorous stirring. The resulting solution was kept under stirring for 40 min at 0 °C. The solution was rapidly transferred to a 40 mL autoclave and heated at 40 °C for 20 h to promote gel formation. The temperature was later increased to 120 °C with a dwelling time of 6 hours to promote the decomposition of urea to generate the mesoporosity. The resulting encapsulated P25 was calcined at 500 °C for 6 h with a heating rate of 1 °C/min in order to remove the templates and any leftover reagents used in the synthesis.

In this work, the amount of P25 in the synthesis was changed to obtain composites with a nominal TiO<sub>2</sub> loading of 10 and 40 wt.% (0.16 g and 0.64 g, respectively). All samples were calcined as described above. The nomenclature of these samples is P25\_10/SiO<sub>2</sub>, P25\_20/SiO<sub>2</sub> and P25\_40/SiO<sub>2</sub> for the samples containing 10, 20, and 40 wt.% of nominal P25 loading, respectively.

### 2.3 Preparation of P25 (TiO<sub>2</sub>) in a precipitated silica (M001) and a mesoporous silica (MCM-41)

For comparison purposes, two more composites of P25 encapsulated (20 wt.% nominal loading) with precipitated silica [37] and a mesoporous silica (MCM-41 type) [38] were also prepared. We used the same methodology as that employed to encapsulate the P25 in hierarchical silica.

The synthesis of the P25 encapsulated in a precipitated silica was performed as follows: 0.4 g of P25 were dispersed in 20 g of water with an ultrasound probe (Bandelin SONOPULS HD 2200) with a power of 660 W output operating at 30% power for 5 min. In order to prepare the composite material, the P25 dispersion in water was mixed with 4 ml of NH<sub>4</sub>OH, 25 g of EtOH to favour the precipitation of the silica, 70 g of water and 8 ml of TEOS, at 380 rpm for 1 h. The mixture was filtered and dried overnight at 303 K. The resulting encapsulated P25 was calcined at 500 °C for 6 h with a heating rate of 1 °C/ min in order to remove the templates and any leftover reagents used in the synthesis. This sample was named P25/M001.

The synthesis of the P25 encapsulated in mesoporous silica was performed as follows: 0.4 g of P25 were dispersed in 20 g of water with an ultrasound probe (Bandelin SONOPULS HD 2200) with a power of 660 W operating at 30% power for 5 min. The composite material was prepared by dissolving 2 g of the templating agent



(cetyltrimethylammonium bromide) in 76 g of deionized water. The mixture was stirred and heated gently until a clear solution was obtained. This mixture was added to the P25 dispersion in water, together with 4 ml of NH<sub>4</sub>OH and 8 ml of TEOS. The resulting mixture was stirred at 380 rpm for 1 h. The suspension was filtered and dried overnight at 323 K. The resulting encapsulated P25 was calcined as described above. This sample was labelled as P25/MCM-41.

#### 2.4 Samples Characterization

The percentages of TiO<sub>2</sub> and SiO<sub>2</sub> present in the samples were analyzed by inductively coupled plasma emission spectroscopy (ICP-OES), in a Perkin-Elmer Optima 4300 system. Dissolution of the samples was carried out by treating them with HF at room temperature.

Thermogravimetric analysis was done in a thermobalance (SDT 2960 instrument, TA). In these analyses, the sample was heated up at 900 °C in air (heating rate of 5 °C min<sup>-1</sup>). X-ray diffraction (XRD) analysis was carried out in a SEIFERT 2002 equipment. Cu K $\alpha$  (1.54 Å) radiation was used. The scanning velocity was 2 °/min, and diffraction patterns were recorded in the angular 2 $\theta$  range of 6–80 °.

The UV-VIS/DR spectroscopy analysis was performed in an UV-Visible spectrophotometer (Jasco V-670), with an integrating sphere accessory and powder sample holder. BaSO<sub>4</sub> was used as the standard reference and the reflectance signal was calibrated with a Spectralon standard (Labsphere SRS-99-010, 99% reflectance). The absorption edge wavelength was estimated from the intercept at zero absorbance of the high slope portion of each individual spectrum in the range 200–800 nm (absorbance method). Then, the band gap can be calculated [40] as:

$$E_g = \frac{1239.8}{\lambda}$$

where  $E_g$  is the band gap energy (eV) and  $\lambda$  is the edge wavelength (nm).

Nitrogen adsorption–desorption isotherms were performed in an Autosorb-6B apparatus from Quantachrome [37]. Prior to analysis all samples were degassed at 250 °C for 4 h. BET surface area ( $S_{\text{BET}}$ ) and total micropore volume ( $V_{\text{N}_2}$ ) were determined by applying the Brunauer–Emmett–Teller (BET) equation, and the Dubinin–Raduskevich equation to the N<sub>2</sub> adsorption data obtained at –196 °C, respectively. Total pore volumes were determined by nitrogen adsorption volume at a relative pressure of 0.95. Mesopore size distributions for all the samples were obtained applying the Barrett-Joyner-Halenda (BJH) equation to the N<sub>2</sub> desorption branch data from the adsorption isotherms at –196 °C, using the software provided by Quantachrome [41].

Transmission electron microscopy (TEM) images were taken using JEOL JEM-2010 equipment. Field-emission scanning electron microscope (FE-SEM) images were taken using a ZEISS, Merlin VP Compact, this equipment has incorporated a microanalysis system by Energy Dispersive X-ray spectroscopy (EDX), BRUKER Quantax 400 for performing elemental mapping of Si and Ti species present in the samples.

## 2.5 Catalytic Tests

The photocatalytic performance of the different materials was studied using an experimental system designed in our laboratory. The system consists of a vertical quartz reactor where the photocatalyst bed is placed on a quartz wool bed. The reactor is 50 mm in height, its diameter is 20 mm and the quartz wool support height is around 10 mm. A UV lamp is placed parallel to the quartz reactor, at a distance around 1 cm. The UV lamp radiation peak appears at 365 nm. The commercial reference of this lamp is TL 8W/05 FAM (Philips, 1W). Finally, the coupled quartz reactor lamp is surrounded by a cylinder covered with aluminum foil. A scheme of this system is depicted elsewhere [36].

The photocatalysts synthesised in this work were used for the oxidation of propene at 100 ppmv in air at room temperature under flow conditions. The calibrated gas cylinder was supplied by Carbueros Metálicos, S.A.

The flow rate of the propene-containing stream was 30 (STP) ml/min after purging the reactor with helium.

The weight of photocatalyst used in these experiments was 0.11 g. However, in order to study the illumination efficiency and any possible inter-particle mass transfer issues, tests at different flow rates of propene were done in which the flow of propene and the mass of P25 were both changed in order to keep the space velocity constant ( $V_{sp} = \text{flow (ml/min)} / \text{mass of photocatalyst (g)}$ ) at a value of 257 ml/g·min. The ratio was 10 ml min<sup>-1</sup>/0.0367 g, 20 ml min<sup>-1</sup>/0.0735, 30 ml min<sup>-1</sup>/0.11 g and 40 ml min<sup>-1</sup>/0.147 g. This was done in order to properly compare the samples prepared in this study. In addition, the sample P25\_40/SiO<sub>2</sub> was measured with the same  $V_{sp}$  (257 ml/g·min) with respect to the amount of P25. Additionally, blank tests were performed under the same experimental conditions as the catalytic tests but in absence of the photocatalysts, resulting in non detectable catalytic activity.

To better study the combined effect between the silica and the P25, the reactor was filled with both silica and P25 as separate powders in a configuration in which the silica with hierarchical porosity was either on top or under the titania. The resulting samples were named SiO<sub>2</sub>/P25 and P25/SiO<sub>2</sub> respectively. Furthermore, a physical mixture of P25 and silica (containing the appropriate amount of P25) was also prepared with the same purpose, the nomenclature of this sample is PM.

The propene-containing stream was passed through the photocatalyst bed until the propene concentration was stable (after about 3 h). The lamp is then switched on and kept working until a constant propene signal is achieved, that is, steady state conditions

(usually after 3 h) and, afterwards the outlet gas is continuously analyzed by mass spectrometry (Balzers, Thermostar GSD 301 01).

Propene conversion was calculated using the following expression:

$$\text{Propene conversion (\%)} = \frac{C_{\text{initial C}_3\text{H}_6} - C_{\text{steady state C}_3\text{H}_6}}{C_{\text{initial C}_3\text{H}_6}} \times 100$$

where  $C_{\text{initial C}_3\text{H}_6}$  is the initial propene concentration, 100 ppmv and  $C_{\text{steady state C}_3\text{H}_6}$  is the propene concentration at steady state conditions in the outlet gas when the UV light is switched on. Moreover the CO<sub>2</sub> production rate was calculated per mol of P25, taken as the active phase, using the following expression (with the aim to normalize the results with the amount of P25):

$$\text{CO}_2 \text{ production rate} = \frac{q_{\text{gen}}}{n}$$

where  $q_{\text{gen}}$  is the molar flow rate of CO<sub>2</sub> generated (moles CO<sub>2</sub>/s) and  $n$  is the moles of catalyst (moles of P25).

### 3. Results and Discussion

#### 3.1 P25/SiO<sub>2</sub> Sample Characterization

In this section, the results on the characterization for the P25 samples encapsulated in spherical silica with hierarchical porosity (SiO<sub>2</sub>) are presented, emphasizing the effect of the P25 loading in the composites.

The results obtained by ICP-OES show the discrepancies between the nominal and real loadings analysed by ICP-OES in the samples (Table 1). The sample with 10 wt.% nominal loading of TiO<sub>2</sub>, results in a 3.8 wt.% loading by ICP-OES analysis. The other samples encapsulated in hierarchical silica present the same trend as showed in Table 1. As a result of the analysis of ICP-OES, the samples P25\_10/SiO<sub>2</sub>, P25\_20/SiO<sub>2</sub>, P25\_40/SiO<sub>2</sub> show a content of 3.8, 8.14 and 15.9 wt% of P25; these values will be

used in the calculations in order to obtain reliable figures. The discrepancies between the nominal loading of TiO<sub>2</sub> and the results obtained for the ICP-OES technique may be due to a fraction of the P25 solid present in the dispersion which was not transferred to the reaction medium. In this aspect, we observed the presence of a significant amount of P25 solid adhered to the walls and in the bottom of the vessel where the dispersion was prepared after transferring this suspension.

The XRD pattern of the P25/SiO<sub>2</sub> samples with different P25 loading are showed in [Figure 1 \(a\)](#). In all cases, the particles of P25 encapsulated in silica have the same crystalline phases as the benchmark P25 (rutile and anatase) after calcination at 500 °C, indicating the presence of P25 in all composites (P25\_10/SiO<sub>2</sub>, P25\_20/SiO<sub>2</sub> and P25\_40/SiO<sub>2</sub>) without any further modification. An elbow in the XRD pattern of all composites due to the presence of amorphous silica is also observed, as showed in the pattern for the naked SiO<sub>2</sub> sample [\[39\]](#). TG analyses show a small weight loss of approximately 2 wt% in all samples (see [Figure 1\(b\)](#)). This suggests that all organic matter and any leftover reagents present in the synthesis were eliminated in the calcination step. The low weight percentage losses observed might be due to adsorbed water or the possible decomposition reactions of hydroxyl groups at higher temperatures [\[16\]](#).

The UV-vis spectra obtained for the P25/SiO<sub>2</sub> with different P25 loading samples are showed in [Figure 2](#). All hybrid photocatalysts with different loading of P25 show a

similar absorption band edge at 400 nm. This fact indicated that the loading of P25 in the composite does not modify the absorption range and the band gap of the P25. However the composites show a small discrepancy in the absorbance range and in the band gap with respect to the naked P25 (Figure 2) indicating that the presence of the silica can slightly modify the band gap of P25 from 3.2 to 3.3 eV.

The porous texture of the synthesized samples was investigated by N<sub>2</sub> adsorption measurements as showed in Figure 3. The N<sub>2</sub> physisorption isotherm of P25 shows a typical type-II isotherm, indicative of a non-porous solid. However, the sample does present a hysteresis in the high relative pressure range due to interparticle adsorbate condensation. The SiO<sub>2</sub> prepared in our research group is a combination of type I and IV isotherms, typical of mesoporous materials with a certain degree of microporosity. This silica has hierarchical porosity, presenting micro, meso and macro-porosity [39]. As expected, the composites obtained in this work present similar isotherms to that of the pure hierarchical SiO<sub>2</sub> material, with a noticeable decrease in the adsorption uptake at low relative pressures and the hysteresis loop as the P25 loading increases.

Concerning the textural properties showed in Table 2, the BET surface area and  $V_{total}$  0.95 decreases with increasing P25 loading, as commented in the previous paragraph. However, the textural parameters cannot help in distinguishing whether the P25 is encapsulated or not in the SiO<sub>2</sub>. Comparing the  $S_{BET}$  (obtained from the isotherms) and  $T_{S_{BET}}$  (obtained theoretically assuming that the composite is a physical mixture), the samples with lower quantities of P25 (P25<sub>10</sub>/SiO<sub>2</sub> and P25<sub>20</sub>/SiO<sub>2</sub>) show a discrepancy of only 7 % between  $S_{BET}$  and  $T_{S_{BET}}$ . Nevertheless, the samples with the highest loading of P25 (P25<sub>40</sub>/SiO<sub>2</sub>) shows a much higher discrepancy (45 %) between  $S_{BET}$  and  $T_{S_{BET}}$ . This difference indicates that high TiO<sub>2</sub> loadings severely affect the final morphology of the obtained composite, resulting not only in a

modification of the porous texture, but also in the shaping of the final SiO<sub>2</sub>/TiO<sub>2</sub> sample (vide infra). In this sense, it appears that high concentrations of suspended TiO<sub>2</sub> powder prevents the spinodal decomposition of the SiO<sub>2</sub>-rich phase, resulting in a composite with an irregular morphology. As a result, the mixing law fails to apply for this sample. TEM images are showed in Figure 4. The TiO<sub>2</sub> crystals are encased in the hierarchical silica matrix (Figure 4(a)). Moreover, the SiO<sub>2</sub> is clearly surrounding the P25 particles in the sample P25\_20/SiO<sub>2</sub>, which corroborates the encapsulation of the TiO<sub>2</sub> inside the SiO<sub>2</sub> matrix. Figure 4 b shows the presence of P25 in the sample P25\_20/SiO<sub>2</sub> as the particle shows the lattice fringes and interplanar distances characteristic of both anatase and rutile present in P25 particles.

SEM images show that the samples with low P25 loadings (3.8 % and 8.14 wt.% ) (Figure 5 (a) and (b)) have a spherical morphology typical for this silica (Figure 5 (d)) [39]. No particles with irregular morphology (representative of P25 NPs, Figure 5 (e)) are observed for these samples, which indicates the encapsulation of P25 inside the SiO<sub>2</sub> matrix, as already pointed at by the TEM images. However the sample with the highest P25 loading (P25\_40/SiO<sub>2</sub>) presents both spherical and irregular particles (Figure 5 (c)), in agreement with the comments made from the adsorption isotherms results.

EDX mapping images are presented in Figures 6(a), (b) and (c). Sample P25\_10/SiO<sub>2</sub> contains Ti in the composites indicating that P25 is probably inside the SiO<sub>2</sub> shell, owing to the composite presenting a spherical structure as observed in the SEM images (Figure 6 (a)). This is a clear indication that the spinodal decomposition process is not

largely affected by the presence of the TiO<sub>2</sub> powder. For sample P25\_20/SiO<sub>2</sub> a similar observation can be made although the presence of Ti is more noticeable as showed in Figure 6(b), allowing us to conclude that in both composites the P25 particles are encapsulated within the SiO<sub>2</sub> matrix. Nevertheless, the sample with the highest TiO<sub>2</sub> loading (sample P25\_40/SiO<sub>2</sub>, Figure 6(c)), presents a morphology distinct from spherical, which shows that the spinodal decomposition is modified in the presence of large concentrations of photocatalyst. In turn, this encapsulated TiO<sub>2</sub> sample shows a significantly different morphology from the other two samples as corroborated by the SEM images and the textural parameters of these composites, in which the mixing law does not apply. In order to better compare the results towards an understanding of the encapsulation phenomenon Figures 7 (a) and (b) show EDS images mapping of sample P25\_20/SiO<sub>2</sub> and a physical mixture in which the two phases are clearly and completely separated, with no observable encapsulation.

### 3.2 P25/M001 and P25/MCM-41 Samples Characterization

In this section, the results on the characterization of the P25 samples encapsulated inside precipitated silica (M001) and a mesoporous silica (MCM-41) with a nominal TiO<sub>2</sub> content of 20% are discussed. These results are compared with P25 encapsulated in spherical hierarchical silica (P25\_20/SiO<sub>2</sub>) to better put the results in perspective.

The results obtained by ICP-OES (Table 3) show discrepancies between the samples encapsulated in different silicas where all samples have a 20 wt.% nominal of P25. The sample with P25/M001 presents the lowest TiO<sub>2</sub> loading (3.2 wt.%). The other samples P25/MCM-41 and P25\_20/SiO<sub>2</sub> present a similar TiO<sub>2</sub> loading, 6.8 wt.% and 8.1 wt.%, respectively, being the sample with the P25 encapsulated in hierarchical silica the one



with the highest loading. These values will be used in the calculations in order to obtain reliable figures.

The XRD pattern for the P25 encapsulated in different silica samples (M001, MCM-41 and SiO<sub>2</sub>) are showed in Figure 8. The particles of P25 encapsulated in the different silicas present the same crystalline phases as the benchmark P25 (rutile and anatase) after calcination at 500 °C, indicating the presence of P25 in the composites without any further modification as indicated previously in Figure 1 (a) for the composite (P25\_20/SiO<sub>2</sub>). In these composites with different silicas (P25/M001, P25/MCM-41 and P25/SiO<sub>2</sub>) an elbow in each of the XRD patterns was also observed, indicating the presence of the different silicas (M001, MCM-41 and SiO<sub>2</sub>) in each composite used in this study.

The UV–vis spectra obtained for the P25 encapsulated with different silica (M001, MCM-41 and SiO<sub>2</sub>) are showed in Figure 9. All hybrid photocatalysts with different silica samples present a similar absorption band edge at 400 nm and band gap. These values indicate that the use of different silica (M001, MCM-41 and SiO<sub>2</sub>) does not modify the light absorption of the P25 encapsulated.

The N<sub>2</sub> adsorption measurements at 77 K are showed in Figure 10. The N<sub>2</sub> physisorption isotherm of sample M001 shows a type-II isotherm, indicative of a non-porous material, with some porosity arising from a small hysteresis in the high relative pressure range due to interparticle condensation. However, the composite P25/M001 presents a combination of type I and type IV isotherms. This fact is remarkable since this composite with P25 (non-porous material) has higher N<sub>2</sub> adsorption capacity with respect to the naked M001, indicating the appearance of additional porosity when the composite is formed probably due to interparticle spacings with sizes in the below-

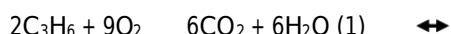
nanometer region. The silica MCM-41 shows a combination of types I and IV isotherms, typical of mesoporous materials with a certain degree of microporosity as it has been reported in the literature [37]. As expected, the composites obtained with this silica present similar isotherms to that of the pure MCM-41, with a noticeable decrease in the adsorption uptake at low pressures and the hysteresis loop due the presence of a non-porous material (P25).

The textural properties obtained from the adsorption isotherms are showed in Table 4. The BET surface area and  $V_{\text{total}}$  0.95 decrease with the incorporation of P25 except in the case of the P25/M001 sample where these values increase. The samples with MCM-41 present the highest surface area and total pore volume.

TEM images show the possible encapsulation of P25 inside the different silicas. (Figure 11). SEM images show the morphology of the samples P25/M001, P25/MCM-41 and P25\_20/SiO<sub>2</sub> (Figure 12 (a-c)). The samples P25/M001 and P25/MCM-41 present an irregular morphology, a feature common for both precipitated silica and P25. EDX mapping images are presented in Fig. 12(d), (e) and (f). All samples present Ti in the composites indicating that P25 is inside the different silicas as observed for sample P25\_20/SiO<sub>2</sub>.

### 3.3 Photocatalytic Activity

The photocatalytic activity of the materials prepared in this work was evaluated by studying the mineralization of propene in the gas phase at low concentration (100 ppmv in air) to CO<sub>2</sub> at room temperature, following the global reaction showed in Equation 1[36].



It must be noted that in this study the mechanism of total photooxidation of VOCs was not studied since it has been extensively studied and reported in the literature [36,42]. Given that the samples used in this study do not differ significantly from those studies, it is safe to assume that the mechanism should be identical to that previously reported.

The results of the effect of different P25 loadings in the photocatalytic activity of the samples with the hierarchically porosity silica are showed in Figure 13 (a). The naked P25 presents the best value of propene conversion with respect to the composites where the P25 was encapsulated in the spherical hierarchical silica (SiO<sub>2</sub>). In the case of the composites, as the concentration of P25 (active phase) is increased propene conversion increases. Nevertheless the samples with 8.1 wt.% and 15.9 wt.% P25 loading present approximately the same propene conversion. This might be due to sample P25<sub>40</sub>/SiO<sub>2</sub> presenting a different morphology with respect to the other composites and this factor affects the activity of the composite (Figure 13 (a)). When the results of the photocatalytic activity are normalized per mol of active phase (P25) (CO<sub>2</sub> production rate) expressed as moles CO<sub>2</sub>/(moles P25 X s), P25 has the lowest photoactivity compared to the composites due to the silica favouring the activity per mol of P25 as showed in the literature [21]. With respect to CO<sub>2</sub> production rate, the composites show a decrease in the conversion of propene upon increasing the percentage of P25 in the composite which might be due to the change in porous texture and morphology of the silica or to another important factor such as the better illumination efficiency [43] of particles of P25 when the composites have lower percentages of active phase as explained later. Moreover in this section we evaluated the durability of the samples in specific the P25<sub>10</sub>/SiO<sub>2</sub> as reference sample. The conditions used in this test have been described in the Catalytic Test section but running the propene abatement tests continuously for 14 hours. In this sample the propene conversion was stable after 14 h

of reaction (the initial and final propene conversion values were kept at 14%). In this sense, this sample (P25\_10/SiO<sub>2</sub>) was also recycled three times. For this purpose the sample was cycled in the photooxidation of propene as described in the Catalytic Test for three cycles (the conversion values for the three consecutive cycles was 14%). The performance of the sample did not show a noticeable change in the propene conversion value at the end of each cycle.

In order to deepen into the synergy between silica and P25 upon encapsulation in these materials as described in literature [21,23,29], the sample showing the highest TiO<sub>2</sub> loading (P25\_40/SiO<sub>2</sub>), is compared in propene mineralization with composites in different configurations (PM, SiO<sub>2</sub>/P25 and P25/SiO<sub>2</sub>) as described in the Catalytic Tests section. As showed above (Figure 13 (b)), the naked P25 presents the best propene conversion value with respect to the other samples, due to the composites having a significantly lower amount of P25. In the composites and the mixtures (SiO<sub>2</sub> and TiO<sub>2</sub>), the sample with the P25 encapsulated has better propene conversion than the other samples. This result indicates a synergetic effect between the encapsulated P25 and the SiO<sub>2</sub>; it seems that hierarchical silica favours mass transport and increases the concentration of reagents near the P25 particles.

Interestingly, P25 has the lowest photocatalytic activity when expressed as rate of CO<sub>2</sub> formation per moles of P25, compared to the composites (Figure 13(b)) even when the P25 sample is not encapsulated. In the case of the composites, the encapsulation of P25 (Figure 13(a)) improved the activity per mol of P25. This is observed in the conversion of propene for the P25\_xx/SiO<sub>2</sub> samples, which hints at a synergy between the P25 encapsulated inside the hierarchical silica. In this respect, the coexistence of a hierarchical porosity which favours mass transfer of reagents and products, the possibility of this same porosity acting as an adsorbent for reagents, and the intimate

contact between the SiO<sub>2</sub> and TiO<sub>2</sub> phase results in an improved performance of the encapsulated samples compared with all its physically mixed counterparts (Figure 13(b)).

From our results showed in Table 2 and Figure 14, it would appear that there is a correlation between the BET surface area in the composites and their CO<sub>2</sub> production rate in the propene mineralization reaction. With this in mind, from the values showed in Table 4, the TiO<sub>2</sub> sample encapsulated in MCM-41 (SiO<sub>2</sub>) should outperform all samples. This material should better concentrate the reagents favouring their oxidation by the TiO<sub>2</sub> phase, as explained in the literature [21,25,29]. In order to probe into this effect in the activity of encapsulated P25, the CO<sub>2</sub> production rates for the samples with silica having different textural parameters ( $S_{\text{BET}}$ ) and morphologies are showed in Figure 14. Interestingly, the composite with hierarchical silica presents the highest CO<sub>2</sub> production rate, despite having poorer textural parameters. It is also observed that the sample encapsulated in mesoporous silica shows better photooxidation of propene than that in microporous silica. This result evidences the importance of using a silica not only with large surface area but also with hierarchical porosity for optimizing the mass transport in addition to an increased concentration of reagents due to the hierarchical porosity interconnected which allows all the adsorbed propene to arrive at the active phase (P25) even comparing these samples with others showing a BET surface area four times larger which lack this hierarchical structure as showed in Scheme 1. In the MCM-41 sample, the porous structure (tubular non-interconnected mesopores) does not guarantee a good access to the active phase via the mesopores, since many of them may not be connected with the P25 particles. On the other hand, in the silica with hierarchical porosity (SiO<sub>2</sub>) the interconnected porosity allows a much higher

accessibility to the active sites, favouring the oxidation of propene on P25, as showed in [Scheme 1](#).

With the purpose of studying the possible effect of the better illumination efficiency in the encapsulated P25 particles as discussed before, the conversion of propene was also obtained by varying the propene flow and the mass of P25 ([Figure 15](#)) keeping the space velocity ( $V_{sp}$ ) constant with the purpose of comparing the naked P25 samples with different mass as described in the Catalytic Test section. These catalytic tests are usually done to detect diffusional limitations. The results show an increase in propene conversion as the flow of reagents and mass of catalysts are decreased. This is markedly different from the expected results for classic catalysis, where the conversion remains constant until it decreases due to diffusional problems [44]. This result indicates some contribution of the photonic efficiency [43]. When the weight of the sample (in this case only P25) is decreased (and consequently the particles bed size), the propene conversion increases due to a better illumination of the particles. This factor could partially explain the increased photocatalytic activity of the composites compared to P25 as showed in [Figure 13\(b\)](#). In fact, the results of the comparison of the samples P25 (0.11 g of naked P25) and P25\_40/SiO<sub>2</sub> (0.69 g of composite), which represents the worst case scenario in illumination efficiency for the encapsulated P25 particles, performed at the same  $V_{sp}$  with respect to the amount of P25 (adding in both cases 0.11 g of P25 in the reactor), indicate a double effect: one arising from the better illumination of the TiO<sub>2</sub> particles because the P25 particles are kept within a UV-transparent shell in the composite; this effect combines with the presence of hierarchical porosity that enhances the conversion of propene as showed [Figure 14](#). These results indicated the difficulty in separating the significant effect brought forth by the porosity of the silica shell (as showed in [Figure](#)

14) and the contribution of the improved illumination efficiency in the photocatalyst (as showed in Figure 15).

Considering the results obtained in this study in terms of characterization of samples and their performance in the photocatalytic oxidation of propene at low concentrations, the most promising outlook seems to be the following: (1) this work presents a facile encapsulation of P25 in different SiO<sub>2</sub> materials through a simple and reproducible sol-gel method, providing a synergetic effect between the P25 and the silica; (2) the increase in TiO<sub>2</sub> loading decreases the activity of the P25/SiO<sub>2</sub> samples, due to the change in the morphology of the composites (TiO<sub>2</sub>-40/SiO<sub>2</sub>) and the importance of the illumination efficiency of the active phase; (3) the synergetic effect between the silica and P25 takes place upon encapsulation due to an intimate contact of the P25 with the silica which acts as adsorbent for the propene molecules and this favours photoactivity; (4) The election of a suitable (i.e. interconnected) porous texture of the silica matrix allows the improved photoactivity of the photocatalyst per mol of P25.

With the results discussed above, the encapsulation of P25 (TiO<sub>2</sub>) in spherical silica with hierarchical porosity, which can be prepared by a simple, reproducible, and cost-effective sol-gel method displays a remarkable photocatalytic activity with respect to the benchmark P25 and the P25 encapsulated in a standard precipitated silica (M001) or mesoporous silica (MCM41). This approach opens the door to synthetic encapsulation strategies [25] with high performance in photoactivity of elimination of VOCs at low concentration using an adequate silica without using convoluted or advanced synthesis methods [32,45].

#### 4. Conclusions

In this study, a facile encapsulation of P25 (TiO<sub>2</sub>) in different silica materials (spherical silica with hierarchical porosity, mesoporous silica and precipitated silica) was performed from a modification of an established methodology. The sample P25\_10/SiO<sub>2</sub> presents the best improvement of CO<sub>2</sub> production rate per mol of P25, because the increase in the loading of P25 causes a modification in the morphology and porosity of the composite and a diminished illumination efficiency affecting photocatalytic activity. Apart from the synergetic effect between the silica and P25, encapsulation provides an added bonus due to an intimate contact of the P25 with the silica what favours photoactivity. Another important factor is the selection of a correct porous network for the silica matrix. This fact, allows to synthesize new materials with an improved mass transfer and catalytic efficiency for the abatement of contaminants at low concentrations in gas phase.

#### **Acknowledgements**

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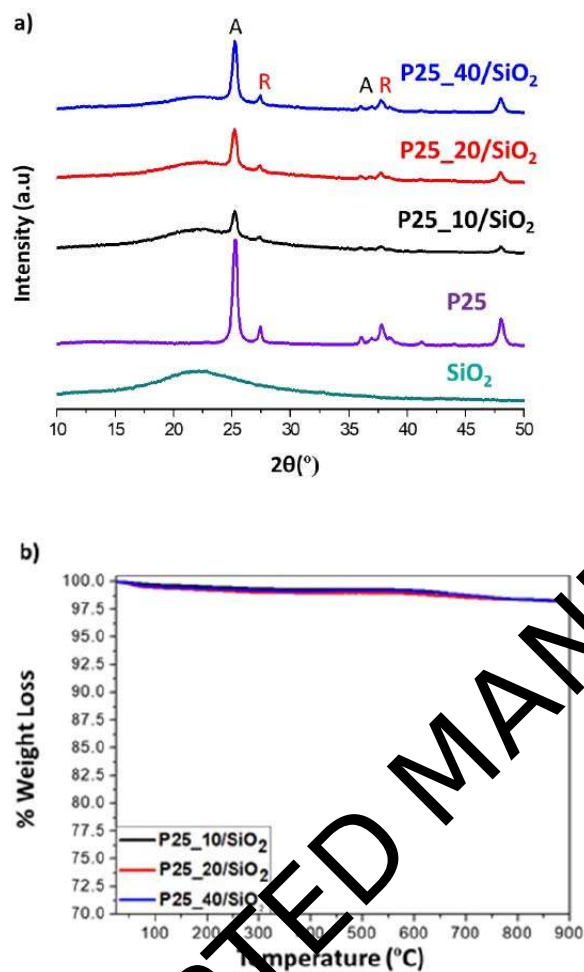


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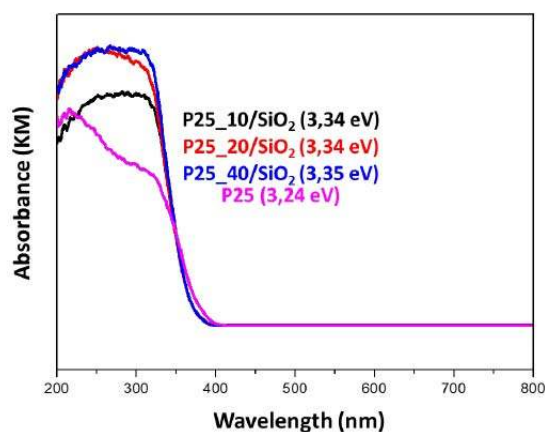
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**Figure 1.** (a) XRD patterns of all composites prepared with hierarchical porosity silica.

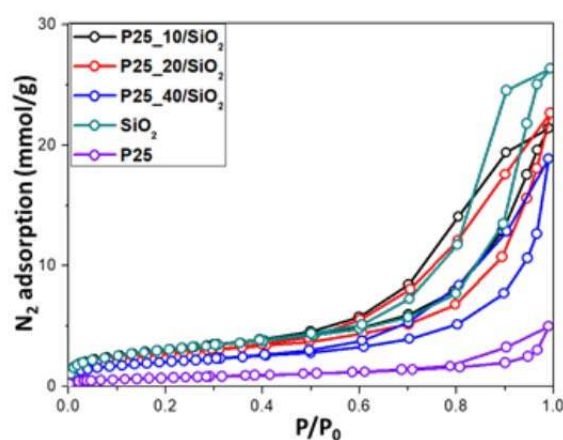
The data for the SiO<sub>2</sub> and P25 are showed for comparison. Key: A = anatase; R = rutile

(b) TG curves of the P25 encapsulated with hierarchical porosity silica.



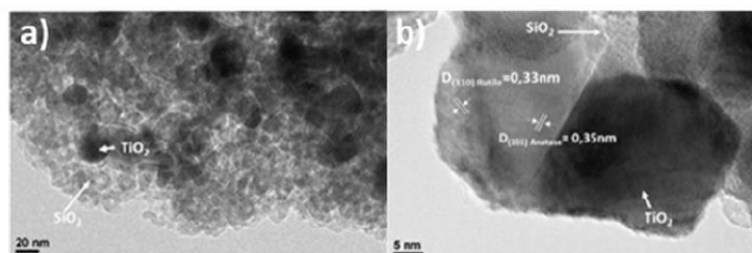
**Figure 2.** UV-VIS absorption spectra and band gap value ( $E_g$ ) of the P25/SiO<sub>2</sub> with different P25 loading samples. The data for the benchmark material P25 are showed for comparison.

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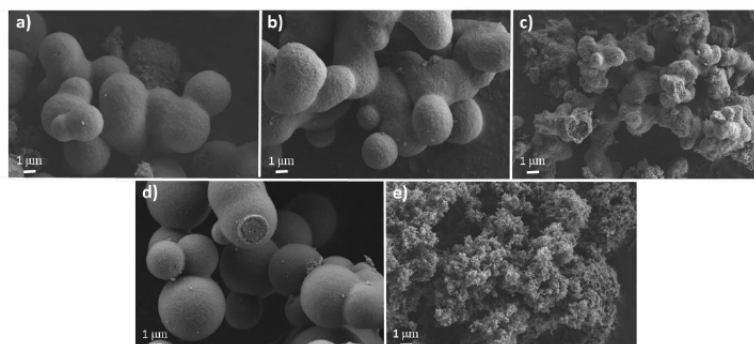


**Figure 3.** N<sub>2</sub> isotherms at 77 K for the different composites with hierarchical porosity silica samples. The adsorption isotherm of SiO<sub>2</sub> and P25 is also shown for comparison purposes.

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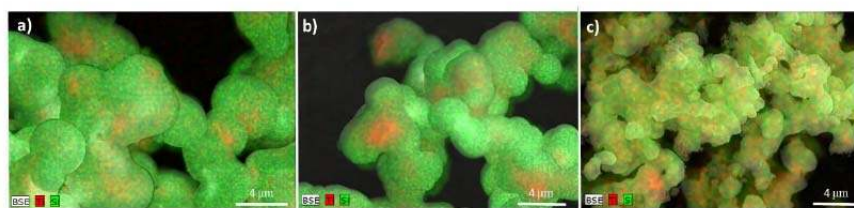


**Figure 4.** TEM images of a representative sample prepared in this study. (a) P25\_20/SiO<sub>2</sub>, (b) Magnification of P25 NPs (sample P25\_20/SiO<sub>2</sub>)

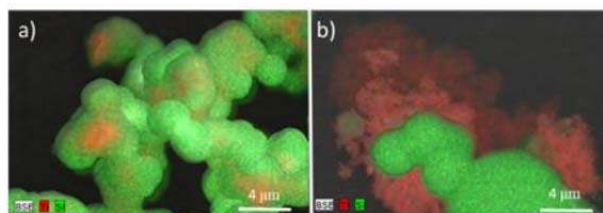


**Figure 5.** SEM of the samples with hierarchical porosity silica: (a) P25\_10/SiO<sub>2</sub>, (b) P25\_20/SiO<sub>2</sub>, (c) P25\_40/SiO<sub>2</sub>. The SEM images of SiO<sub>2</sub> (d) and P25 (e) are also showed for comparison purposes.



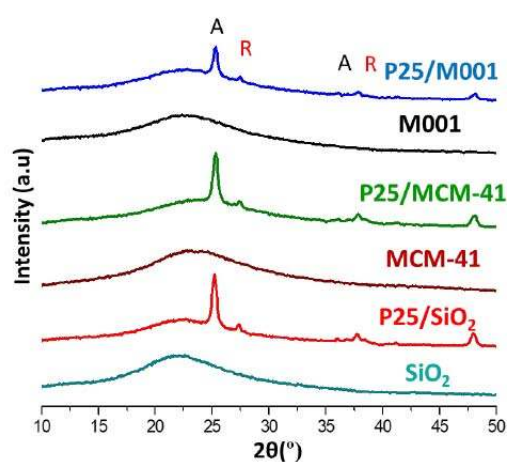


**Figure 6.** EDX images mapping of the samples (a) P25\_10/SiO<sub>2</sub>, (b) P25\_20/SiO<sub>2</sub>, (c) P25\_40/SiO<sub>2</sub>.

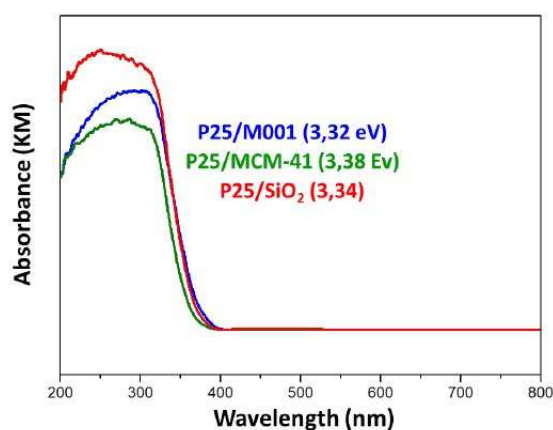


**Figure 7.** EDX images mapping of the composite and the physical mixture with the same percentage of P25 (a) P25\_20/SiO<sub>2</sub> (composite), (b) PM (Physical mixture).

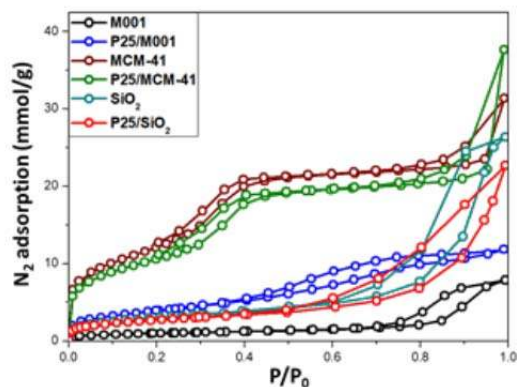
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**Figure 8.** XRD patterns of the composites with different silica. The data for the different silica used in this work are showed for comparison Key: A = anatase; R = rutile

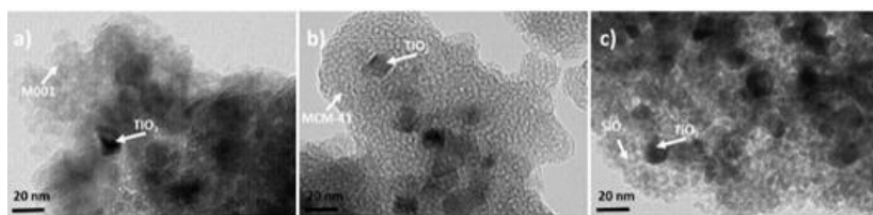


**Figure 9.** UV-VIS absorption spectra and the band gap (Eq) of the P25/SiO<sub>2</sub> with different silica samples.



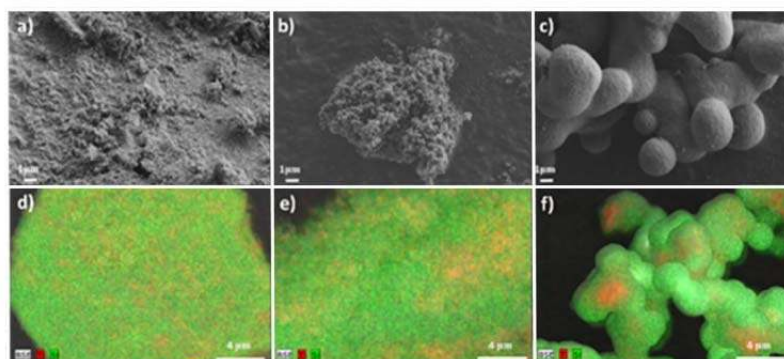
**Figure 10.** N<sub>2</sub> isotherms at 77 K for the samples prepared in this study: P25/M001, P25/MCM-41, and P25<sub>20</sub>/SiO<sub>2</sub>. The adsorption isotherms of the pure silicas are also showed for comparison purposes.

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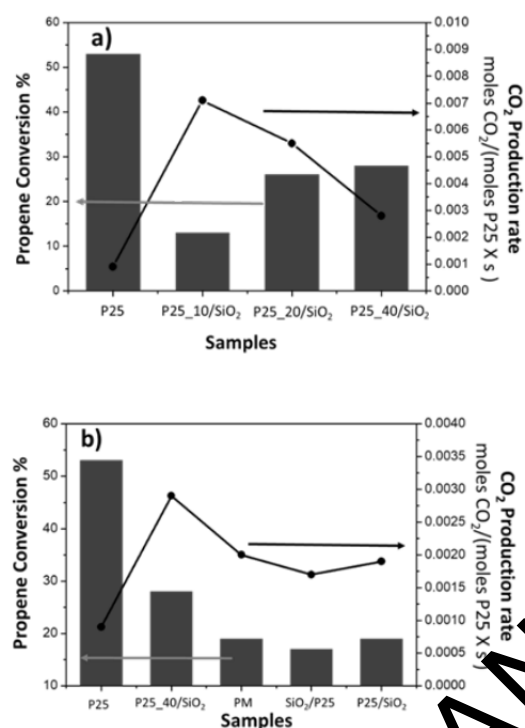


**Figure 11.** TEM of the composite prepared in this study: (a) P25/M001, (b) P25/MCM-41, (c) P25\_20/SiO<sub>2</sub>.

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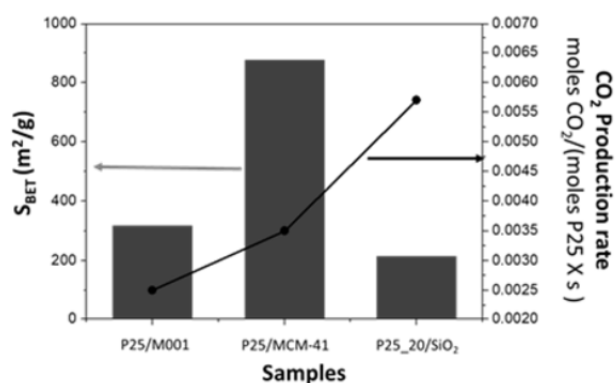


**Figure 12.** SEM of the samples with different silica: (a) P25/M001, (b) P25/MCM-41, (c) P25\_20/SiO<sub>2</sub>. Figures 12(d-f) present the EDX images mapping (d) P25/M001, (e) P25\_20/MCM-41, (f) P25\_20/SiO<sub>2</sub>.

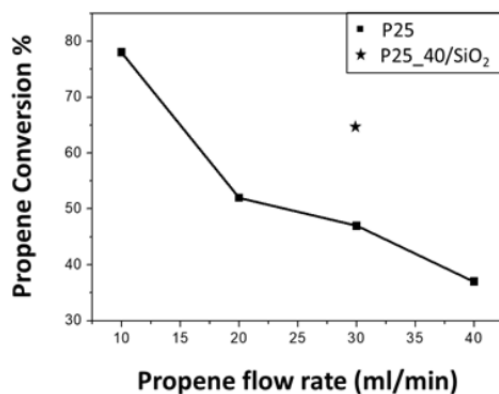


**Figure 13.** Comparison of propene conversion and CO<sub>2</sub> production rates for samples with spherical hierarchical porous silica and P25 for comparison purposes: (a) Photooxidation varying the percentage of P25 in the samples, (b) Comparison of the composite P25<sub>40</sub>/SiO<sub>2</sub> with samples where the same amount of P25 is not encapsulated.

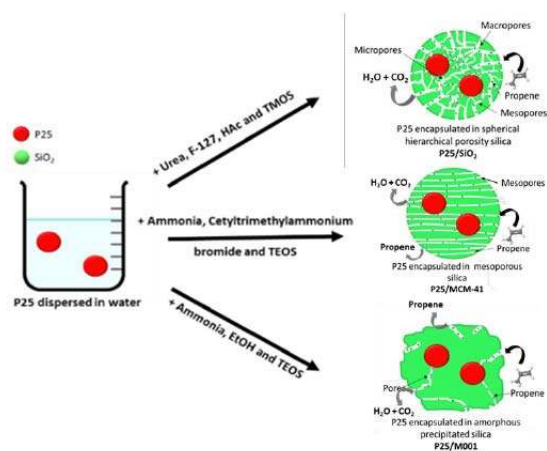




**Figure 14.** Comparison of CO<sub>2</sub> production rates of samples of P25 encapsulated in different silica and its textural parameters ( $S_{BET}$ ).



**Figure 15.** Comparison of propene conversion with different flow rates (the mass of the samples is described in Experimental section) maintaining a constant space velocity of 257 ml·g<sup>-1</sup>·min<sup>-1</sup> (See Experimental section). The sample P25<sub>40</sub>/SiO<sub>2</sub> with the same mass of P25 (0.11g) and space velocity is included for comparison purposes.



**Scheme 1.** Schematic representation of the synthetic procedure followed for the preparation of silica samples with different porous textures.

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**Table 1.** Percentage of titania of the sample prepared in this study.

Samples	% TiO <sub>2</sub> Nominal	% TiO <sub>2</sub> ICP-OES
P25_10/SiO <sub>2</sub>	10	3.8±0.9
P25_20/SiO <sub>2</sub>	20	8.1±0.2
P25_40/SiO <sub>2</sub>	40	15.9±0.3

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**Table 2.** Textural properties of the samples prepared in this study. The data for SiO<sub>2</sub> and P25 are showed for comparison purposes.

Samples	$S_{\text{BET}}$ (m <sup>2</sup> /g)	* $T_{\text{S}_{\text{BET}}}$ (m <sup>2</sup> /g)	$V_{\text{total},0.95}$ (cm <sup>3</sup> /g)	$V_{\text{N}_2\text{DR}}$ (cm <sup>3</sup> /g)	Mean pore size (nm)
SiO <sub>2</sub>	244	-	0.86	0.10	6.2
P25_10/SiO <sub>2</sub>	235	252	0.61	0.10	7.9
P25_20/SiO <sub>2</sub>	215	230	0.57	0.09	7.9
P25_40/SiO <sub>2</sub>	145	219	0.38	0.07	6.2
P25	54	-	0.18	0.02	7.6

\* $T_{\text{S}_{\text{BET}}}$  represents the theoretical  $S_{\text{BET}}$  of the composites synthesised in this work (considering the composites as a physical mixture). This value was calculated by the following expression:  $T_{\text{S}_{\text{BET}}} = (S_{\text{BET}} (\text{Mesoporous silica}) \cdot (\text{SiO}_2 \text{ present in the composites (ICP-ES)}) + (S_{\text{BET}} (\text{P25}) \cdot \text{P25 present in the composites (ICP-ES)})$

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**Table 3.** Percentage of titania of the sample with different silica samples.

Samples	% TiO <sub>2</sub> ICP-OES
P25/M001	3.2±0.1
P25/MCM41	6.8±0.9
P25_20/SiO <sub>2</sub>	8.1±0.2

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**Table 4.** Textural properties of the samples prepared in this study derived from the analysis of the N<sub>2</sub> adsorption isotherms. The data for SiO<sub>2</sub> and P25 are showed for comparison purposes.

Samples	S <sub>BET</sub> (m <sup>2</sup> /g)	V <sub>total,0.95</sub> (cm <sup>3</sup> /g)	V <sub>N<sub>2</sub>DR</sub> (cm <sup>3</sup> /g)	Mean pore size (nm)
M001	77	0.25	0.033	6.2
MCM-41	973	0.82	0.39	2.9
SiO <sub>2</sub>	244	0.86	0.10	6.2
P25/M001	317	0.39	0.17	3.1
P25/MCM-41	875	0.77	0.34	3.1
P25 <sub>20</sub> /SiO <sub>2</sub>	215	0.57	0.09	7.9
P25	54	0.18	0.02	7.6