

AD-751 984

**FAST COMPUTER PROGRAM FOR NONEQUILIBRIUM
ROCKET PLUME PREDICTIONS**

R. R. Mikatarian, et al

AeroChem Research Laboratories, Incorporated

Prepared for:

Air Force Rocket Propulsion Laboratory

August 1972

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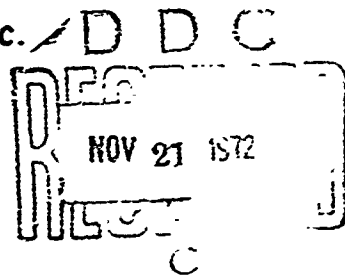
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AD 751984

A FAST COMPUTER PROGRAM FOR NONEQUILIBRIUM ROCKET PLUME PREDICTIONS

R.R. Mikotarian, C.J. Kou and H.S. Pergament

AeroChem Research Laboratories, Inc.
Princeton, N.J. 08540



August 1972

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DOCUMENT CONTROL DATA - R & D

(Security classification of title, body of abstract and indexing annotation must be entered when the report is classified)

| | | | |
|---|---|--|--|
| 1. PERFORMING ACTIVITY (Corporate authority) AeroChem Research Laboratories, Inc. P. O. Box 12 Princeton, NJ 08540 | | 2a. REPORT SECURITY CLASSIFICATION UNCLASSIFIED | |
| 2. REPORT TITLE A Fast Computer Program for Nonequilibrium Rocket Plume Predictions | | 2b. GROUP | |
| 3. DESCRIPTIVE NOTES (Type of report and inclusive dates) Final Report 15 June 1971 - 14 July 1972 | | | |
| 4. AUTHOR(S) (First name, middle initial, last name) R. R. Mikatarian, C. J. Kau, H. S. Pergament | | | |
| 5. PERIOD DATE August 1972 | 7a. TOTAL NO. OF PAGES viii + 22 / 02 | 7b. NO. OF REFS 22 | |
| 6a. CONTRACT OR GRANT NO. F04611-71-C-0064 | 7c. ORIGINATOR'S REPORT NUMBER(S) AeroChem TF-282 | | |
| 6b. PROJECT NO. | 9d. OTHER REPORT NUMBER(S) (Any other numbers that may be assigned this report) AFPRL-TR-72-94 | | |
| 7. DISTRIBUTION STATEMENT Approved for public release; distribution unlimited. | | | |
| 8. SUPPLEMENTARY NOTES | | 12. SPONSORING/MONITORING AGENCY NAME(S) Air Force Rocket Propulsion Laboratory | |

A fast computer program for predicting nonequilibrium rocket plume properties is described. The analytical model assumes parallel turbulent (or laminar) mixing between concentric chemically reacting streams and can also be used for studying chemical lasers and re-entry wakes. The equations for free shear layer mixing with nonequilibrium chemistry are solved via a mixed implicit/explicit finite difference scheme which efficiently predicts flow properties and composition, even when many chemical reactions are near equilibrium. The stability problems inherent in fully explicit finite difference schemes are shown to be eliminated, and stable integration step sizes are shown to be increased by up to 4 orders of magnitude. Computer run times for typical afterburning rocket plume calculations are shown to be decreased by more than one order of magnitude over the original (fully explicit) AeroChemaxisymmetric mixing with nonequilibrium chemistry program. Both the analysis and computer program write-up are presented, including a sample calculation and a FORTRAN listing.

UNCLASSIFIED

Security Classification

| KEY WORDS | LINK A | | LINK B | | LINK C | |
|---|--------|----|--------|----|--------|----|
| | ROLE | WT | ROLE | WT | ROLE | WT |
| Turbulent Mixing Chemically Reacting Flows Mixing/Nonequilibrium Chemistry Computer Code | | | | | | |

UNCLASSIFIED

Security Classification

A FAST COMPUTER PROGRAM
FOR NONEQUILIBRIUM ROCKET PLUME

PREDICTIONS

R. R. Mikatarian

C. J. Kau

H. S. Pergament

August 1972

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FOREWORD

This work was supported by Tri-Service (Air Force Rocket Propulsion Laboratory/Naval Weapons Center/Army Missile Command) funding and administered under Air Force Contract F04611-71-C-0064.

The authors gratefully acknowledge the many helpful discussions with Project Engineer Capt. W.J. Rothschild, Air Force Rocket Propulsion Laboratory, and the support of Mr. A.C. Victor, Naval Weapons Center and Dr. B.J. Walker, Army Missile Command.

This technical report has been reviewed and is approved.

Paul J. Daily, Col. USAF
Chief, Technology Division

This report is designated AeroChem TR-282.

ABSTRACT

A fast computer program for predicting nonequilibrium rocket plume properties is described. The analytical model assumes parallel turbulent (or laminar) mixing between concentric chemically reacting streams and can also be used for studying chemical lasers and re-entry wakes. The equations for free shear layer mixing with nonequilibrium chemistry are solved via a mixed implicit/explicit finite difference scheme which efficiently predicts flow properties and composition, even when many chemical reactions are near equilibrium. The stability problems inherent in fully explicit finite difference schemes are shown to be eliminated, and stable integration step sizes are shown to be increased by up to 4 orders of magnitude. Computer run times for typical afterburning rocket plume calculations are shown to be decreased by more than one order of magnitude over the original (fully explicit) AeroChemaxisymmetric mixing with nonequilibrium chemistry program. Both the analysis and computer program write-up are presented, including a sample calculation and a FORTRAN listing.

NOMENCLATURE

| | |
|-------------------|--|
| a | defined by Eq. (15b) |
| $a_{\frac{1}{2}}$ | defined by Eq. (33) |
| a^s | attenuation per unit length |
| A | constant in expression for k_f (see Eq. (23)) |
| $b_{\frac{1}{2}}$ | defined under Eq. (25b) |
| B | activation energy (see Eq. (23)) |
| c_p | specific heat of mixture ($\sum_i X_i c_{p_i}$) |
| c_{p_i} | specific heat of ith species |
| e | electronic charge |
| F_i | defined as X_i/W ($= Y_i/W_i$) |
| FDL | factor used for the external control of integration step size |
| g_i | Gibbs free energy of ith species at standard state (1 atm) |
| ΔG | change in standard Gibbs free energy for a reaction, $\sum_i (g_i)_{\text{products}}$ $- \sum_i (g_i)_{\text{reactants}}$ |
| h | enthalpy of mixture |
| h_i | enthalpy of ith species |
| h_{298i} | heat of formation of ith species at $T = 298 \text{ K}$ |
| k_f | forward rate coefficient |
| K | eddy viscosity coefficient (see Section VI) |
| \bar{K} | eddy viscosity coefficient for Donaldson/Gray model (see Eq. (32)) |
| K_p | equilibrium constant |
| Le | Lewis number (laminar or turbulent) |
| m_e | electron mass |
| $M_{\frac{1}{2}}$ | Mach number at half radius, defined under Eq. (32) |
| N | temperature exponent in reaction rate equation (Eq. (23)) |
| n_e | electron density |
| Q | arbitrary dependent variable (see Eqs. (13) - (15)) |

| | |
|-------------------------|---|
| Q_e | electron-neutral collision cross section |
| p | static pressure |
| Pr | Prandtl number (laminar or turbulent) |
| r | coordinate normal to jet centerline |
| r_i | inner mixing zone radius |
| r_j | jet radius |
| $r_{\frac{1}{2}}$ | defined under Eq. (28b) |
| $\bar{r}_{\frac{1}{2}}$ | defined under Eq. (27) |
| R | universal gas constant |
| T | static temperature |
| u | x component of velocity |
| v | r component of velocity |
| v_e | electron velocity |
| \dot{w}_i | molar rate of production of ith species |
| $\dot{w}^{(j)}$ | molar rate of production from jth reaction |
| W | molecular weight of mixture $(\sum_i F_i)^{-1}$ |
| W_i | molecular weight of ith species |
| x | coordinate parallel to jet centerline |
| Δx | $x_{n+1} - x_n$ |
| X_i | mole fraction of ith species |
| Y_i | mass fraction of ith species |

Greek

| | |
|--------------|--|
| α | constant for external control of eddy viscosity (see Eqs. (25) - (31)) |
| $\Delta\Psi$ | $\psi_{m+1} - \psi_m$ |
| ϵ | eddy diffusivity for turbulent flow; defined as μ/ρ |
| η | defined by Eq. (25) |
| μ | viscosity (or eddy viscosity for turbulent flow) |
| ν_e | electron-neutral collision frequency |
| ρ | density |
| σ | electrical conductivity |

Ψ stream function
 ω signal frequency

Subscripts

e evaluated at edge of mixing layer (free stream)
 e^- electrons
i ith species
j value at nozzle (jet) exit
m Ψ index in grid network
n x index in grid network
o evaluated at axis of symmetry, $r = 0$

Miscellaneous

$| |$ absolute value

$\left(\frac{\partial}{\partial \beta}\right)_\gamma$ partial derivative with respect to β ; γ being held constant

\sum_i summation over i species

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I. INTRODUCTION

The need to accurately determine electromagnetic wave/plume interactions^{1,2} has motivated the development of several programs³⁻⁶ to predict the electrical properties of turbulent rocket exhaust plumes.* Each program uses the same gas dynamic model (parallel mixing between two concentric streams), but only the AeroChem program of Mikatarian and Pergament accounts for nonequilibrium chemistry effects; the others³⁻⁵ assume local thermochemical equilibrium to prevail. Attempts to account for transverse radar attenuation data (taken with focused microwaves) under simulated altitude conditions using equilibrium chemistry programs generally fail. Indeed, it has been demonstrated by Pergament and Jensen^{7,8} that finite-rate chemical kinetics must be incorporated into rocket plume calculations to accurately predict plume temperatures, electrical properties, etc.

Conceptually the numerical solution of the equations describing axisymmetric mixing with nonequilibrium chemistry presents few difficulties. A fully explicit finite difference scheme⁴ yields an accurate solution to the problem. Unfortunately, however, on many occasions the stability requirements associated with the explicit integration scheme are found to so severely limit maximum step sizes (e. g. on the order of 10^{-5} to 10^{-10} ft) that computer solutions become economically prohibitive.† This "stiffness" in the equations,^{9,10} (which results in small step sizes) is found to be restricted to nonequilibrium flows where one or more of the chemical reactions is at or near-equilibrium, a situation typical of relatively low altitude ($< \approx 70$ kft) afterburning plumes.

In this computer program we utilize a new numerical technique to solve the partial differential equations (in finite-difference form) describing turbulent (or laminar) shear flows with nonequilibrium chemistry: Implicit differences are used in the solution of the species conservation equations‡

*References 3 and 5 are unclassified descriptions of the solution techniques used in the Naval Weapons Center and Lockheed Propulsion Company codes. Further information on these codes may be found in the classified literature.

†For frozen (non-reactive) flow the governing equations can be integrated quite rapidly using explicit differences.

‡This appears to be the first program to utilize implicit differences for free shear layers with nonequilibrium chemistry, although such schemes have been applied to one-dimensional nonequilibrium nozzle flows.^{11,12}

and explicit differences are used for the momentum and energy equations. This mixed implicit/explicit scheme eliminates the instability problems which characterize fully explicit schemes and allows integration step sizes to be increased by orders of magnitude without sacrificing accuracy. Those rocket exhaust plume predictions which could not be made with the original AeroChem program² (which uses the fully explicit scheme) because the stable step size approached 10^{-10} ft, are quite easily handled by the new program. Most importantly, for the more typical case in which average step sizes range from 10^{-4} to 10^{-2} ft, the new program reduced computer run times by at least an order of magnitude. (A detailed comparison between rocket plume calculations using the original fully explicit difference scheme and the new mixed implicit/explicit scheme is given in Appendix D.)

The gas dynamic model assumes parallel mixing between the rocket exhaust products and surrounding air (either quiescent or moving), and allows for non-uniform initial conditions at the nozzle exit plane.* Lewis and Prandtl numbers are assumed to be constant, and pressure is allowed to vary parallel to the plume axis. Turbulent transport is described via an appropriate eddy viscosity model and Sutherland's law is used to calculate the viscosity for laminar flow. The program is quite general; it allows any chemical reaction mechanism (and associated rate coefficients) to be used as long as thermodynamic data are available for all species. Thermodynamic data, taken directly from the JANNAF Tables, are input in tabular form.

This report gives the governing partial differential equations and their finite difference formulations, the various eddy viscosity models which may be input to the program, a description of the input data, the output from a sample calculation and a complete FORTRAN listing. The computer output gives detailed axial and radial distributions of velocity, temperature, density and species mole fractions. These results are used to calculate electron densities and electron-neutral collision frequencies which, in turn, are used to determine radar attenuation transverse to the plume and electrical conductivity.

Although the program was written in response to a need for fast predictions of relatively low altitude afterburning rocket plume electrical properties, it can equally well be used for applications to missile base heating and IR radiation problems.

*Thus it is possible to account for the effects of an initial boundary layer on the properties in the mixing region.

II. GOVERNING EQUATIONS

A. Conservation Equations and Boundary Conditions

The following equations describe the free-shear layer turbulent or laminar mixing of co-flowing axisymmetric streams undergoing chemical reactions. For turbulent flow all properties are interpreted to be the mean (time-averaged) values. The eddy viscosity, μ , is then described by one of the phenomenological expressions given in Section VI.

Global Continuity

$$\frac{\partial}{\partial x} (\rho u) + \frac{1}{r} \frac{\partial}{\partial r} (\rho v r) = 0 \quad (1)$$

Conservation of Species

$$\rho u \frac{\partial F_i}{\partial x} + \rho v \frac{\partial F_i}{\partial r} = \frac{1}{r} \frac{\partial}{\partial r} \left(\frac{Le}{Pr} \mu r \frac{\partial F_i}{\partial r} \right) + \dot{w}_i \quad (2)$$

Conservation of Momentum

$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial r} = - \frac{dp}{dx} + \frac{1}{r} \frac{\partial}{\partial r} \left(\mu r \frac{\partial u}{\partial r} \right) \quad (3)$$

Conservation of Energy

$$\rho c_p \left[u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial r} \right] = u \frac{dp}{dx} + \mu \left(\frac{\partial u}{\partial r} \right)^2 + \frac{1}{r} \frac{\partial}{\partial r} \left[\frac{c_p}{Pr} \mu r \frac{\partial T}{\partial r} \right] + \mu \frac{Le}{Pr} \frac{\partial T}{\partial r} \sum_i c_{p_i} \frac{\partial F_i}{\partial r} - \sum_i \dot{w}_i h_i \quad (4)$$

State

$$\rho = \frac{pW}{RT} \quad (5)$$

The conservation equations are solved subject to the following initial and boundary conditions:

$$\begin{aligned}
 x = 0: & \quad u = u(r), \quad F_1 = F_1(r), \quad T = T(r) \\
 r = 0: & \quad \frac{\partial u}{\partial r} = \frac{\partial T}{\partial r} = \frac{\partial F_1}{\partial r} = 0 \\
 r \rightarrow \infty: & \quad u \rightarrow u_e, \quad F_1 \rightarrow (F_1)_e, \quad T \rightarrow T_e
 \end{aligned} \tag{6}$$

Pressure is allowed to vary in the axial direction according to,

$$p = c_0 + c_1 x + c_2 x^2 + c_3 x^3 \tag{7}$$

where c_0 , c_1 , c_2 and c_3 are input coefficients (Card 5, Cols. 21-60).

B. Transformation to Stream Function Coordinates

It is convenient to transform the equations into a streamline coordinate system and utilize the stream function, Ψ , as the radial coordinate. The transformation from cartesian (x, r) coordinates to streamline (x, Ψ) coordinates (which automatically satisfies global continuity, Eq. (1)) is defined by:

$$\Psi \frac{\partial \Psi}{\partial r} = \rho u r \tag{8a}$$

$$\Psi \frac{\partial \Psi}{\partial x} = -\rho v r \tag{8b}$$

From Eqs. (8a) and (8b) we obtain,

$$\left(\frac{\partial}{\partial r} \right)_x = \frac{\rho u r}{\Psi} \left(\frac{\partial}{\partial \Psi} \right)_x \tag{9a}$$

$$\left(\frac{\partial}{\partial x} \right)_r = \left(\frac{\partial}{\partial x} \right)_\Psi - \frac{\rho v r}{\Psi} \left(\frac{\partial}{\partial \Psi} \right)_x \tag{9b}$$

Introducing Eqs. (9a) and (9b) into Eqs. (2), (3), and (4), gives:

Species

$$\frac{\partial F_i}{\partial x} = \frac{1}{\psi} \frac{\partial}{\partial \psi} \left[\left(\frac{\mu}{Pr} \right) \frac{\mu \rho u r^2}{\psi} \frac{\partial F_i}{\partial \psi} \right] + \frac{\dot{w}_i}{\rho} \quad (10a)$$

and, on the axis of symmetry, $r = \psi = 0$

$$\frac{\partial F_i}{\partial x} = 2\mu \left(\frac{\mu}{Pr} \right) \frac{\partial^2 F_i}{\partial \psi^2} + \frac{\dot{w}_i}{\rho} \quad (10b)$$

Momentum

$$\frac{\partial u}{\partial x} = -\frac{1}{\rho u} \frac{d\rho}{dx} + \frac{1}{\psi} \frac{\partial}{\partial \psi} \left[\frac{\mu \rho u r^2}{\psi} \frac{\partial u}{\partial \psi} \right] \quad (11a)$$

and, on the axis of symmetry, $r = \psi = 0$

$$\frac{\partial u}{\partial x} = -\frac{1}{\rho u} \frac{d\rho}{dx} + 2\mu \frac{\partial^2 u}{\partial \psi^2} \quad (11b)$$

Energy

$$c_p \frac{\partial T}{\partial x} = \frac{1}{\rho} \frac{dp}{dx} - \frac{1}{\rho u} \sum_i h_i \dot{w}_i + \frac{1}{\psi} \frac{\partial}{\partial \psi} \left[\frac{c_p}{Pr} \frac{\mu \rho u r^2}{\psi} \frac{\partial T}{\partial \psi} \right] + \quad (12a)$$

$$\frac{\mu \rho u r^2}{\psi^2} \left[\left(\frac{\partial u}{\partial \psi} \right)^2 + \frac{Le}{Pr} \frac{\partial T}{\partial \psi} \sum_i c_{p_i} \frac{\partial F_i}{\partial \psi} \right]$$

and, on the axis of symmetry, $r = \psi = 0$

$$c_p \frac{\partial T}{\partial x} = \frac{1}{\rho} \frac{dp}{dx} + 2\mu \left(\frac{c_p}{Pr} \right) \frac{\partial^2 T}{\partial \psi^2} - \frac{1}{\rho u} \sum_i h_i \dot{w}_i \quad (12b)$$

C. Finite-Difference Formulation

The governing set of parabolic partial differential equations, (Eqs. (10), (11) and (12)), are first rewritten in finite difference form and then solved using a forward marching technique. The chemistry terms, \dot{w}_i , in the species continuity equations are evaluated via implicit-differences; the diffusion terms in the species continuity equations and the complete energy and momentum equations are evaluated via explicit-differences. The following finite-difference formulations¹³ are used:

$$\left(\frac{\partial Q}{\partial x}\right)_{n+1, m} = \frac{Q_{n+1, m} - Q_{n, m}}{\Delta x} \quad (13)$$

$$\left(\frac{\partial Q}{\partial \bar{y}}\right)_{n, m} = \frac{Q_{n, m+1} - Q_{n, m-1}}{2\Delta \bar{y}} \quad (14a)$$

$$\left[\frac{\partial}{\partial \bar{y}} \left(a \frac{\partial Q}{\partial \bar{y}} \right)\right]_{n, m} = \frac{a_{n, m+\frac{1}{2}} [Q_{n, m+1} - Q_{n, m}]}{(\Delta \bar{y})^2} \quad (14b)$$

$$- \frac{a_{n, m-\frac{1}{2}} [Q_{n, m} - Q_{n, m-1}]}{(\Delta \bar{y})^2}$$

where

$$a_{n, m \pm \frac{1}{2}} = \frac{a_{n, m} \pm a_{n, m \pm 1}}{2} \quad (15a)$$

and

$$a = \frac{\mu p u^2}{\Psi} \quad (15b)$$

The difference equations that result from applying Eqs. (13), (14) and (15) to Eqs. (10), (11) and (12) are:

Species

$$\begin{aligned}
 (F_i)_{n+1,m} - (\bar{x}_i)_{n+1,m} \Delta x / (\rho u)_{n,m} \\
 = \frac{\Delta x}{m(\Delta \bar{\psi})^3} \left\{ \left(\frac{Le}{Pr^2} \right)_{n,m+\frac{1}{2}} \left[(F_i)_{n,m+1} - (F_i)_{n,m} \right] \right. \\
 \left. + \left(\frac{Le}{Pr^2} \right)_{n,m-\frac{1}{2}} \left[(F_i)_{n,m-1} - (F_i)_{n,m} \right] \right\} \\
 + (F_i)_{n,m}
 \end{aligned} \tag{16a}$$

and, on the axis of symmetry ($m = 0$),

$$\begin{aligned}
 (F_i)_{n+1,0} - (\bar{x}_i)_{n+1,0} \Delta x / (\rho u)_{n,0} \\
 = \frac{\Delta x}{(\Delta \bar{\psi})^2} \left(\frac{Le}{Pr} \right)_{n,0} \left[(F_i)_{n,1} - (F_i)_{n,0} \right] \\
 + (F_i)_{n,0}
 \end{aligned} \tag{16b}$$

Momentum

$$\begin{aligned}
 u_{n+1,m} = \frac{\Delta x}{m(\Delta \bar{\psi})^3} \left\{ a_{n,m+\frac{1}{2}} \left[u_{n,m+1} - u_{n,m} \right] \right. \\
 \left. + a_{n,m-\frac{1}{2}} \left[u_{n,m-1} - u_{n,m} \right] \right\} - \frac{\Delta x}{(\rho u)_{n,m}} \left(\frac{dp}{dx} \right)_{n+1} + u_{n,m}
 \end{aligned} \tag{17a}$$

and, on the axis of symmetry, $m = 0$

$$u_{n+1,0} = -\frac{\Delta x}{(\rho c_p)_{n,0}} \left(\frac{dp}{dx} \right)_{n+1} + \frac{h_{i,n,0} \Delta x}{(\Delta \Psi)^2} [u_{n,1} - u_{n,0}] + u_{n,0} \quad (17b)$$

Energy

$$\begin{aligned} T_{n+1,m} &= \frac{\Delta x}{(\rho c_p)_{n,m}} \left(\frac{dp}{dx} \right)_{n+1} + \frac{\Delta x}{4m(\Delta \Psi)^3} \left(\frac{\mu}{Pr} \right)_{n,m} (u_{n,m+1} - u_{n,m-1})^2 \\ &+ \frac{\Delta x}{m(\Delta \Psi)^3 (c_p)_{n,m}} \left\{ \left(\frac{c_p}{Pr^2} \right)_{n,m+\frac{1}{2}} (T_{n,m+1} - T_{n,m}) \right. \\ &+ \left. \left(\frac{c_p}{Pr^2} \right)_{n,m-\frac{1}{2}} (T_{n,m-1} - T_{n,m}) + \frac{1}{4} \left(\frac{L_2}{Pr^2} \right)_{n,m-1} \sum_i (c_{p,i})_{n,m} \right. \\ &\left. (F_{i,n,m+1} - F_{i,n,m-1}) [T_{n,m+1} - T_{n,m-1}] \right\} \\ &+ T_{n,m} - \frac{1}{(\rho u)_{n,m}} \sum_i (h_i \dot{w}_i)_{n,m} \quad (18a) \end{aligned}$$

and, on the axis of symmetry, $m = 0$

$$\begin{aligned} T_{n+1,0} &= \frac{\Delta x}{(\rho c_p)_{n,0}} \left(\frac{dp}{dx} \right)_{n+1} + \frac{4\Delta x}{(\Delta \Psi)^2} \left(\frac{\mu}{Pr} \right)_{n,0} [T_{n,1} - T_{n,0}] \\ &+ T_{n,0} - \frac{1}{(\rho u)_{n,0}} \sum_i (h_i \dot{w}_i)_{n,0} \quad (18b) \end{aligned}$$

The species mole fractions at station $n+1, m$ are determined from the species conservation equations by linearizing the chemistry terms* (i. e. $(\dot{w}_i)_{n+1, m}$) and inverting the resulting matrix. The linearizations involving species F_i and F_j (for a two-body reaction) or F_i, F_j and F_k (for a three-body reaction) at station $n+1$ (all variables are known at station n), are given by

$$\begin{aligned} (F_i F_j)_{n+1} &= (F_i F_j)_n + F_{jn} [(F_i)_{n+1} - (F_i)_n] + F_{in} [(F_j)_{n+1} - (F_j)_n] \\ &= - \underline{(F_i F_j)_n} + \underline{(F_j)_n} (F_i)_{n+1} + \underline{(F_i)_n} (F_j)_{n+1} \end{aligned} \quad (19)$$

$$\begin{aligned} (F_i F_j F_k)_{n+1} &= - \underline{2(F_i F_j F_k)_n} + \underline{(F_j F_k)_n} (F_i)_{n+1} + \underline{(F_i F_k)_n} (F_j)_{n+1} \\ &\quad + \underline{(F_i F_j)_n} (F_k)_{n+1} \end{aligned} \quad (20)$$

The terms underscored by a single line contribute to the elements of the coefficient matrix, while the terms underscored by a double line contribute to the known column matrix on the right hand side of the matrix equation for the linearized system. Thus the matrix equation takes the form (for N species),

$$\begin{bmatrix} a_{11} & a_{12} & a_{13} & & a_{1N} \\ & a_{21} & & & \\ & & & & \\ & & & & \\ & & & & a_{NN} \\ a_{N1} & & & & \end{bmatrix} \begin{bmatrix} F_1 \\ F_2 \\ \\ \\ F_N \end{bmatrix} = \begin{bmatrix} Q_1 \\ Q_2 \\ \\ \\ Q_N \end{bmatrix} \quad (21)$$

*The chemistry term does not make the energy equation "stiff"; thus when solving for temperature the chemistry term is treated explicitly.

III. SOLUTION OF FINITE DIFFERENCE EQUATIONS

A. Integration Step Size

An exact stability relationship governing the maximum allowable integration step size, $(\Delta x)_{\max}$ cannot be obtained due to the nonlinearity of the governing equations. Instead the step-size requirement to satisfy stability can only be estimated. Following Von Neuman¹⁴ a limit is placed on $(\Delta x)_{\max}$ such that all dependent variables (u , T , F_i) always remain equal to or greater than zero. Thus the maximum step size at each radial grid point ($m \neq 0$) as established from the species conservation equation* is estimated to be

$$(\Delta x)_{\max} = \frac{m (\Delta \Psi)^2}{\left[\frac{Le}{Pr^2} \right]_{n, m+\frac{1}{2}} + \left[\frac{Le}{Pr^2} \right]_{n, m-\frac{1}{2}}} FDL \quad (22a)$$

i

and on the axis, ($m = 0$),

$$(\Delta x)_{\max} = \frac{(\Delta \Psi)^2 Pr}{4 Le} FDL \quad (22b)$$

The actual integration step size, Δx , is taken to be $\frac{1}{3}$ of the smallest value of $(\Delta x)_{\max}$ as computed from Eqs. (22a) and (22b). This fraction ($\frac{1}{3}$) was selected on the basis of many trial calculations. Since Eqs. (22a) and (22b) are only approximate an additional factor, FDL, has been incorporated into the program in order to maintain external control (Card 5, Cols. 11-20) on Δx in case smaller step sizes are required to maintain stability of the solution. In addition, the step size can never exceed the input print increment (Card 4, Cols. 21-30).

Should the computed species mole fraction at any radial point become negative (typically, because the chemistry is "fast", and one or more reactions are near-equilibrium), the step size is repeatedly halved until either the species mole fraction becomes positive or the step size becomes less than

* Applying the same criteria to the momentum and energy equations usually results in larger values of $(\Delta x)_{\max}$

some minimum step size.* In the latter case, the program terminates. After the species mole fraction becomes positive, the next value of Δx is again computed from $\frac{1}{3}(\Delta x)_{\max}$. Thus the step size is never determined from the value of Δx needed to satisfy stability for the previous step. This is a somewhat unique approach to specifying Δx for the solution to finite difference equations, and can save substantial computer time. It was adopted because, typical rocket plume calculations show that, when using the mixed implicit/explicit difference scheme, the chemistry only influences stable step sizes in a small region of the flow. Once the program integrates through this region step sizes of $\frac{1}{3}(\Delta x)_{\max}$ usually suffice.

B. Edge of Mixing Layer

An additional radial mesh point (at free stream conditions) is added whenever the "next-to-the-last" radial point value of temperature or velocity, differs from the corresponding free stream value by more than a specified percentage of the free stream value. One percent has been selected for velocity and five percent for temperature.

C. Halving the Mesh

The number of grid points cannot be allowed to expand without bounds because of the limited storage capacity of the computer. Therefore, the number of points is halved either when the mesh increases to twice its original size (Card 2, Cols. 1-5) or the number of points exceeds 26. The computer prints all output at the station at which halving occurs.

*The minimum step size is an input number (Card 5, Cols 1-10).

IV. CHEMICAL REACTION RATE EQUATIONS

Ten possible reaction types are included in the program:

Reaction Type

| | | | |
|------|-----------|---|-----------|
| (1) | A + B | = | C + D |
| (2) | A + B + M | = | C + M |
| (3) | A + B | = | C + D + E |
| (4) | A + B | = | C |
| (5) | A + M | = | C + D + M |
| (6) | A + B | → | C + D |
| (7) | A + B + M | → | C + M |
| (8) | A + B | → | C + D + E |
| (9) | A + B | → | C |
| (10) | A + M | → | C + D + M |

Reaction types (6)-(10) correspond to reaction types (1)-(5), but proceed in the forward direction only. In Reactions (2), (5), (7) and (10), M is an arbitrary third body. In this program, all species are assumed to have equal third body efficiencies; thus, in evaluating $\dot{w}^{(j)}$, $F_M = (W)^{-1}$. The net rates of production for all reactions are written below, in the form, $\dot{w}^{(j)} = RP^{(j)} - RM^{(j)}$.*

$$\begin{aligned}
 (1) \quad \dot{w}^{(j)} &= k_f \rho^2 F_A F_B - \frac{k_f \rho^2 F_C F_D}{K_p} \\
 (2) \quad \dot{w}^{(j)} &= \frac{k_f \rho^3 F_A F_B}{W} - \frac{k_f \rho^2 F_C}{K_p W R T} \\
 (3) \quad \dot{w}^{(j)} &= k_f \rho^2 F_A F_B - \frac{k_f \rho^3 F_C F_D F_E R T}{K_p} \\
 (4) \quad \dot{w}^{(j)} &= k_f \rho^2 F_A F_B - \frac{k_f \rho^3 F_C}{K_p R T} \\
 (5) \quad \dot{w}^{(j)} &= \frac{k_f \rho^2 F_A}{W} - \frac{k_f \rho^3 F_C F_D R T}{K_p W}
 \end{aligned}$$

* The symbols RP and RM are used on the computer output.

$$(6) \quad \dot{w}^{(j)} = k_f \rho^2 F_A F_B$$

$$(7) \quad \dot{w}^{(j)} = \frac{k_f \rho^3 F_A F_B}{W}$$

$$(8) \quad \dot{w}^{(j)} = k_f \rho^2 F_A F_B$$

$$(9) \quad \dot{w}^{(j)} = k_f \rho^2 F_A F_B$$

$$(10) \quad \dot{w}^{(j)} = \frac{k_f \rho^2 F_A}{W}$$

To reduce round-off and truncation errors $RP^{(j)}$ and $RM^{(j)}$ are computed separately for each reaction. All contributions to the molar rate of production of a given species are then computed and added algebraically to form \dot{w}_i .

The forward rate coefficient, k_f , is expressed in the form,

$$k_f = AT^{-N} \exp(B/RT) \quad (23)$$

and K_p is determined from,

$$\ln K_p = -\Delta G/RT \quad (24)$$

The rate coefficients are divided into seven types:

Rate Coefficient Type*

- | | |
|-----|----------------------------|
| (1) | $k_f = A$ |
| (2) | $k_f = AT^{-1}$ |
| (3) | $k_f = AT^{-2}$ |
| (4) | $k_f = AT^{-\frac{1}{2}}$ |
| (5) | $k_f = A \exp(B/RT)$ |
| (6) | $k_f = AT^{-1} \exp(B/RT)$ |
| (7) | $k_f = AT^{-\frac{3}{2}}$ |

*Rate coefficient data for typical rocket plume reactions may be found, e. g., in Ref. 15.

V. THERMODYNAMIC DATA

The thermodynamic properties (specific heat, Gibbs free energy and enthalpy) for each species are taken directly from the JANNAF Thermochemical Tables,¹⁶ and input to the program as c_{P_i} , $-\left(\frac{g_i - h_{298i}}{T}\right)$ and $(h_i - h_{298})$ in tabular form as a function of temperature (Card 11). Linear interpolation is used to define thermodynamic properties at the local temperature.

VI. TRANSPORT PROPERTIES

A. Turbulent Eddy Viscosity Models

The following eddy viscosity models¹⁷⁻²⁰ are incorporated into the program:

Model 1 (Ferri)¹⁷

Initial region, *

$$\mu = \rho \epsilon = \alpha 0.00137 \times |\rho_o u_o - \rho_e u_e| \quad (25a)$$

Developed region,

$$\mu = \rho \epsilon = \alpha K b_{\frac{1}{2}} |\rho_o u_o - \rho_e u_e| \quad (25b)$$

where $b_{\frac{1}{2}}$ is the value of r where $\rho u = (\rho_o u_o + \rho_e u_e)/2$ and K is the eddy viscosity coefficient, usually taken to be 0.025.†

*Defined as region upstream of axial position where $(u_o - u_e)/(u_j - u_e) = 0.95$.

†Most of the models contain a numerical coefficient K which must be determined empirically. The value $K = 0.025$, taken from Schlichting,¹⁸ has been incorporated directly into the program. This can be changed by the program input data via an appropriate value for the additional constant, α , Eqs. (25-31) (Card 4, Cols. 61-70).

Model 2 (Ting/Libby)¹⁹

$$\mu = \rho \epsilon = \alpha K \bar{r}_{\frac{1}{2}} |u_o - u_e| \rho \left(\frac{\rho_o}{\rho}\right)^2 \left(\frac{\eta}{r}\right)^2 \quad (26)$$

where

$$\eta^2 = 2 \int_0^r (\rho_o/\rho) r' dr' \quad (27)$$

and $\bar{r}_{\frac{1}{2}}$ is the value of η where $u = (u_o + u_e)/2$

Model 3

Initial region,

$$\mu = \rho \epsilon = \alpha 0.00137 \times \rho_o |u_o - u_e| \quad (28a)$$

Developed region,

$$\mu = \alpha K r_{\frac{1}{2}} \rho_o |u_o - u_e| \quad (28b)$$

where $r_{\frac{1}{2}}$ is the value of r where $u = (u_o - u_e)/2$

Model 4

Initial region,

$$\mu = \rho \epsilon = \alpha 0.00137 \times \rho_e |u_o - u_e| \quad (29a)$$

Developed region,

$$\mu = \rho \epsilon = \alpha K r_{\frac{1}{2}} \rho_e |u_o - u_e| \quad (29b)$$

Model 5* (Ting/Libby)¹⁹

Initial region,

$$\mu = \rho \epsilon = \alpha 0.00137 \times |u_j - u_e| \rho \left(\frac{r_j}{r}\right)^2 \quad (30)$$

Developed region,

$$\mu = \rho \epsilon = \alpha K \bar{r}_{\frac{1}{2}} |u_0 - u_e| \rho \left(\frac{r_0}{r}\right)^2 \left(\frac{r_1}{r}\right)^2 \quad (26)$$

Model 6 (Donaldson/Gray)²⁰

Initial region,

$$\mu = \rho \epsilon = \alpha \bar{K} (r_{\frac{1}{2}} - r_1) \rho |u_0 - u_e|/2 \quad (31a)$$

$$\text{For } M_{\frac{1}{2}} \leq 1.2 \quad \bar{K} = 0.0468 + M_{\frac{1}{2}} \left[-0.0460 M_{\frac{1}{2}} + 0.0256 M_{\frac{1}{2}}^2 \right]$$

$$M_{\frac{1}{2}} > 1.2 \quad \bar{K} = 0.0248 \quad (32)$$

where $M_{\frac{1}{2}}$ is the value of the Mach number where $u = (u_0 + u_e)/2$ (i.e., the half radius). The speed of sound at the half radius, $a_{\frac{1}{2}}$ is expressed by,

$$a_{\frac{1}{2}} = \left[\frac{c_p}{c_p - (R/W_{\frac{1}{2}})} \frac{RT_{\frac{1}{2}}}{W_{\frac{1}{2}}} \right]^{\frac{1}{2}} \quad (33)$$

where $W_{\frac{1}{2}}$ and $T_{\frac{1}{2}}$ are evaluated at the half radius. In Eq. (31a), r_1 is the inner mixing zone radius and is defined as the value of r where $(u - u_e)/(u_j - u_e) = 0.95$.

Developed region,

$$\mu = \rho \epsilon = \alpha \bar{K} r_{\frac{1}{2}} \rho |u_0 - u_e|/2 \quad (31b)$$

*In the program, the specification of Model 5 means that Eq. (30) will be used in the initial region and Model 2 (Eq. 26) will be used in the developed region. This is important for re-starting a problem in the developed region for which Model 5 was selected to run from $x = 0$. In this case, Model 2 must be specified on Card 2, Cois. 11-15.

B. Laminar Flow

Sutherland's Law²¹ is used to describe the viscosity as a function of temperature.

$$\mu = 9.8 \times 10^{-7} T^{3/2} / (T + 111) \quad \text{lb}_{\text{m}}/\text{ft-sec} \quad (34)$$

VII. PLUME ELECTRICAL PROPERTIES

Electron density, electron-neutral collision frequency, unit radar attenuation and electrical conductivity are computed at all radial points for each axial print-out station.

A. Electron Density

$$n_e = 0.733 (10^{22}) X_e - p T^{-1} \quad \text{mi}^{-1} \quad (35)$$

where p is in atm and T in degrees K.

B. Collision Frequency

$$\nu_e = 4.57 (10^{27}) p T^{-\frac{1}{2}} \sum X_i Q_{ei} \quad \text{sec}^{-1} \quad (36)$$

where p is in atm, T in degrees K and Q_{ei} in cm^2 . The electron-neutral collision cross sections²² used in the calculations and given in the following table are those which characterize typical solid propellant exhaust plumes. If other species contribute to the value of ν_e , the program must be modified.

| Species | Q_{ei} , cm ² |
|------------------|---|
| CO | $2.03 (10^{-23}) v_e^{\dagger} + 2.46 (10^{-16})$ |
| CO ₂ | $4.7 (10^{-23}) v_e^{-1}$ |
| H ₂ O | $5.9 v_e^{-2}$ |
| HCl | $1.85 v_e^{-2}$ |
| N ₂ | $3.29 (10^{-23}) v_e$ |
| H ₂ | $1.45 (10^{-23}) v_e + 8.7 (10^{-16})$ |

$$\dagger v_e = 6.21 (10^5) T^{\frac{1}{2}} \text{ cm/sec}$$

C. Transverse Radar Attenuation

$$a' = 1.17 \frac{n_e / v_e}{[1 + (\omega / v_e)^2]} \quad \text{db/in} \quad (37)$$

where n_e is in ml⁻¹, v_e in sec⁻¹ and ω is rad/sec.* The program then computes transverse (normal to the axis) radar attenuation along a "line-of-site" (i. e. radar beam "spot size" much smaller than the electrical plume diameter) from,

$$A = 2 \int_0^{\infty} a' dr \quad \text{db} \quad (38)$$

where r is in inches.

D. Electrical Conductivity

$$\sigma = 2.54(10^4) \frac{e^2 n_e}{v_e m_e} \text{ mho/in} \quad (39)$$

where e is 1.6×10^{-19} coulomb and m_e is 9.1×10^{-31} kg.

*Attenuation calculations can be made for a maximum of six signal frequencies.

VIII. PROGRAM OPERATION

A. Machine

The program, as listed in Appendix A, must be run on a CDC computer since a library routine named **SECOND** (called in subroutine **TICK**) is used to sense elapsed time from the start of execution. This routine enables the continuing solution cards to be punched when the execution time exceeds the time input on Card 2, Cols. 36-40--if punch options 2 or 3 are selected (Card 2, Cols. 31-35). The program may be run on a different machine by removing the subroutine and replacing it with the dummy routine shown below:

```
SUBROUTINE TICK (JJJ)
  IJJ = 0
  RETURN
END
```

When this is done the maximum execution time input on Card 2, Cols. 36-40 will not trigger the punch option.

Input and output are on the standard tape units (i. e. 5 for READ, 6 for WRITE and 7 for PUNCH).

B. Sense Switch Control

1. Sense Switch 1 - When Sense Switch 1 is on, the current values of x , T_0 , and $n_{e,0}$ are printed on-line.
2. Sense Switch 3 - When Sense Switch 3 is on, the case is terminated and all output is printed at the current axial station.

C. Program Optimization

It is recommended that the program be compiled using the highest level of optimization. On the CDC 6600 this corresponds to the **FAST OBJECT CODE MODE**.

IX. PROGRAM INPUT DATA

The input data cards are explained below. A listing of the computer program, a sample input data sheet and a sample output are given in Appendices A, B and C, respectively.

| <u>Card No.</u> | <u>Columns</u> | <u>Description</u> | <u>Format</u> |
|-----------------|----------------|--|---------------|
| 1 | 1-72 | Run identification | 12A6 |
| 2 | 1-5 | Initial number of grid points* in ψ coordinate (26 maximum) | 15 |
| | 6-16 | Number of species (24 maximum) | 15 |
| | 11-15 | Viscosity option key If -1: Laminar (Eq. 34) 0: $\mu = \text{constant}$ 1: Model 1 (Eq. 25) 2: Model 2 (Eq. 26) 3: Model 3 (Eq. 28) 4: Model 4 (Eq. 29) 5: Model 5 (Eqs. 26 and 30) 6: Model 6 (Eq. 31) | 15 |
| | 16-20 | Number of reactions (40 maximum) | 15 |
| | 21-25 | \dot{w}_i output option If 0: \dot{w}_i for each species is not output 1: \dot{w}_i for each species is output at all radial points whose temperature is greater than the kinetics cut-off temperature (Card 6, Cols. 61-70) | 15 |

*Recommended number, 13

| <u>Card No.</u> | <u>Columns</u> | <u>Description</u> | <u>Format</u> |
|-----------------|------------------------------|---|---------------|
| 2 | 26-30 | RP, RM output option If 0: RP, RM for each reaction is not output 1: RP, RM for each reaction is output at all radial points whose temperature is greater than the kinetics cut-off temperature (Card 6, Cols. 61-70) | I5 |
| | 31-35 | Card punch option If 0: No cards punched 1: Cards with radial distributions of electron density and collision frequency at all printout stations are punched 2: Cards for continuing a given solution are punched 3: Both the above sets of cards are punched | I5 |
| | 36-40 | Maximum computer execution time (min) (If card punch option 1, 2 or 3 is selected, cards will be punched after this amount of computer time)* | I5 |
| | 41-45 | Pressure option If 0: Pressure is a constant 1: Pressure is a function of axial distance | I5 |
| 3 | 1-10 . . . 51-60 | Signal frequencies (MHz) - 6 maximum - for which transverse attenuation calculations will be made (see Section VII). Leave blank if no attenuation calculations desired | E10.3 |

*In practice if this option is selected, the calculations will terminate at an execution time 30 seconds less than this value.

| Card No. | Columns | Description | Format |
|----------|---------|--|--|
| 4 | 1-10 | Initial value of x (ft) | E10.3 |
| | 11-20 | Final value of x (ft) | E10.3 |
| | 21-30 | Print increment (ft) | E10.3 |
| | 31-40 | Lewis number | E10.3 |
| | 41-50 | Prandtl number | E10.3 |
| | 51-60 | Nozzle (jet) radius (ft) | E10.3 |
| | 61-70 | α , factor used to vary eddy viscosity* (see Section VI) | E10.3 |
| 5 | 1-10 | Δx_{\min} , Minimum integration step size (ft)† | E10.3 |
| | 11-20 | FDL, diffusion step size factor‡ | E10.3 |
| | 21-30 | c_0 (atm) | E10.3 |
| | 31-40 | c_1 (atm/ft) | E10.3 |
| | 41-50 | c_2 (atm/ft ²) | Pressure Coefficients (see Section II) E10.3 |
| | 51-60 | c_3 (atm/ft ³) | E10.3 |
| 6 | 1-10 | Pressure at initial value of x(atm) | E10.3 |
| | 11-20 | Temperature at jet centerline (K) | E10.3 |
| | 21-30 | Temperature at edge of jet (K) (free stream value) | E10.3 |

*Set $\alpha = 1.0$ if no changes to eddy viscosity coefficient are desired.

†Recommended value, 1×10^{-10} ft.

‡Set FDL = 1.0 if maximum integration step size criterion discussed in Section III is to be used.

| Card No. | Column | Description | Format |
|----------|--------|--|--------|
| 6 | 31-40 | Velocity at jet centerline (ft/sec) | E10.3 |
| | 41-50 | Velocity at edge of jet (ft/sec) (free stream value) | E10.3 |
| | 51-60 | $\Delta \Psi, \left(\frac{\text{ftm}}{32.2} \text{sec}^{-1}\right)^{\frac{1}{2}}$ | E10.3 |
| | | If $\Delta \Psi = 0$ (or blank) the program computes $\Delta \Psi$ assuming velocity, temperature and species mole fractions are constant at initial station | |
| | | If $\Delta \Psi$ is specified, cards 7.1 to 9.13 are read next. If $\Delta \Psi$ is not specified, card 10.1 is the next card read with cards 7.1 through 9.13 being omitted | |
| | 61-70 | Kinetics cut-off temperature (kinetics are frozen at temperatures below this value*) | E10.3 |

NOTE: For the purpose of illustration it is assumed that there are 13 initial grid points in the Ψ coordinate.

| | | | |
|-----|-------|---|-------|
| 7.1 | 1-10 | T(1), Temperature (K) at jet centerline, $r = 0$ | E10.3 |
| | 61-70 | T(7) | |
| 7.2 | 1-10 | T(8) | E10.3 |
| | 51-60 | T(13), Temperature (K) in free stream | |
| 8.1 | 1-10 | u(1), Velocity (ft/sec) at jet centerline, $r = 0$ | E10.3 |
| | 61-70 | u(7) | |
| 8.2 | 1-10 | u(8) | E10.3 |
| | 51-60 | u(13) | |

*If blank or zero, 400 K is used.

| <u>Card No.</u> | <u>Column</u> | <u>Description</u> | <u>Format</u> |
|-----------------|---------------|--------------------|---------------|
|-----------------|---------------|--------------------|---------------|

NOTE: For the purpose of illustration it is assumed that there are 8 species

| | | | |
|--------|-------|---|-------|
| 9.1.1 | 1-10 | Mole fraction of 1st species at jet center-line, $r = 0$ | E10.3 |
| | ⋮ | | |
| | 61-70 | Mole fraction of 7th species at jet center-line, $r = 0$ | E10.3 |
| 9.1.2 | 1-10 | Mole fraction of 8th species at jet center-line, $r = 0$ | E10.3 |
| 9.2.1 | 1-10 | Mole fraction of 1st species at next grid point | E10.3 |
| | ⋮ | | |
| | 61-70 | Mole fraction of 7th species at next grid point | |
| 9.2.2 | 1-10 | Mole fraction of 8th species of next grid point | E10.3 |
| 9.13.1 | 1-10 | Mole fraction of 1st species at 13 grid point (free stream) | E10.3 |
| | ⋮ | | |
| | 61-70 | Mole fraction of 7th species at 13th grid point (free stream) | |
| 9.13.2 | 1-10 | Mole fraction of 8th species at 13th grid point (free stream) | E10.3 |

NOTE: Card Type 10 is not required if Card Types 7, 8 and 9 are input.

| | | | |
|--------|-------|--|-------|
| 10.1.1 | 1-10 | Mole fraction of 1st species at jet center-line, $r = 0$ | E10.3 |
| | ⋮ | | |
| | 61-70 | Mole fraction of 7th species at jet center-line, $r = 0$ | |
| 10.1.2 | 1-10 | Mole fraction of 8th species at jet center-line, $r = 0$ | |

| Card No. | Column | Description | Format |
|----------|--------|---|--------|
| 10 2.1 | 1-10 | Mole fraction of 1st species in free stream | E10.3 |
| | 61-70 | Mole fraction of 7th species in free stream | |
| 10.2.2 | 1-10 | Mole fraction of 8th species in free stream | |

NOTE: The following cards contain the thermodynamic data. * The first card contains the species name, molecular weight and heat of formation. The second and remaining cards contain the temperature and corresponding specific heat, free energy and enthalpy for that species. Two temperatures and corresponding thermodynamic data are placed on each card. The input table can contain up to a maximum of 30 temperature points. The data are input exactly as presented in the JANNAF tables.¹⁶

| Card No. | Column | Description | Format |
|----------|--------|--|--------|
| 11.1.1 | 1- 6 | Name of first species | A6 |
| | 7-16 | Molecular weight | E10.3 |
| | 17-26 | Heat of formation, h_{298_i} (kcal/mole) | E10.3 |
| 11.1.2 | 1-10 | First temperature point (K) | E10.3 |
| | 11-20 | c_{p_i} (cal/mole-K) | E10.3 |
| | 21-30 | $-\left(\frac{g_i - h_{298_i}}{T}\right)$ (cal/mole K) | E10.3 |
| | 31-40 | $h_i - h_{298_i}$ (kcal/mole) | E10.3 |
| | 41-50 | Second temperature point (K) | E10.3 |
| | 51-60 | c_{p_i} (cal/mole-K) | E10.3 |
| | 61-70 | $-\left(\frac{g_i - h_{298_i}}{T}\right)$ (cal/mole-K) | E10.3 |

*The order of the species must be identical to the order on Card Types 9 or 10.

| <u>Card No.</u> | <u>Column</u> | <u>Description</u> | <u>Format</u> |
|-----------------|---------------|-------------------------------|---------------|
| 11.1.2 | 71-80 | $h_i - h_{298_i}$ (kcal/mole) | E10.3 |
| 11.1.3 | : | Third temperature point | |
| | : | | |
| 11.2.1 | : | Name of second species | |
| | : | | |

NOTE: The chemical reaction mechanism for a particular problem is input on the last set of cards, one card for each reaction. (See Section IV.) No particular order is required.

| | | | |
|------|-------|---|------|
| 12.1 | 1-6 | Species A | A6 |
| | 7 | + sign | |
| | 8-13 | Species B (or M) | A6 |
| | 14 | + sign | |
| | 15-20 | Blank or M | 6x |
| | 21 | = sign | |
| | 22-27 | Species C | A6 |
| | 28 | + sign (if needed) | |
| | 29-34 | Species D (or M) | A6 |
| | 35 | + sign (if needed) | |
| 12.1 | 36-41 | Species E (or M) | A6 |
| | 42-48 | Blank | |
| | 49-50 | Reaction type, 1 to 10 (see Section IV) | I2 |
| | 51 | Rate coefficient type, 1 to 7 (see Section IV) | II |
| | 52-59 | A, Pre-exponential factor cm-molecule-sec units | E8.2 |
| | 60-63 | N, Temperature exponent | F4.1 |
| | 64-72 | B, Activation energy cal/mole | F9.1 |
| 12.2 | : | Next Reaction | |
| | : | | |
| | : | | |

X. PROGRAM OUTPUT

A. Description

Sample output sheets for the input data given in Appendix B are shown in Appendix C. The first page contains the key program input parameters, initial distributions of velocity, temperature and species mole fractions and the chemical reaction mechanism and rate coefficients. The succeeding pages contain printouts at axial stations corresponding to the print increment (Card 4, Cols. 21-30). Following the listing of electrical properties (last page of output), the integration step size and corresponding axial position are given for each integration step up to the next print station.

B. Units

A mixed system of units appears on the program output for ease in making additional calculations and for program check-out.

| | |
|----------------------------|--|
| COLLISION FREQUENCY | electron-neutral collision frequency, sec^{-1} . |
| DELTA X | integration step size, ft |
| DENSITY | g/cm^3 |
| ELECTRICAL CONDUCTIVITY | mho/in |
| ELECTRON DENSITY | ml^{-1} |
| ENTHALPY | mixture static enthalpy, cal/g |
| HALF RADIUS/R | nondimensional radial distance to point where $u = (u_o + u_e)/2$, ft (viscosity option 6 only) |
| INNER MIXING ZONE RADIUS/R | nondimensional radial distance to point where $(u-u_e)/(u_i - u_e) = 0.95$, (viscosity option 6 only) |
| MACH NO. | Mach number |
| MACH NUMBER AT HALF RADIUS | Mach number at point where $u = (u_o + u_e)/2$ (viscosity option 6 only) |
| MINIMUM STEP SIZE | $(\Delta x)_{\text{min}}$, ft |

| | |
|---|---|
| MIXING RATE COEFFICIENT | defined by Eq. (31a) or Eq. (31b) (viscosity option 6 only) |
| MOLE FRACTIONS | species mole fractions |
| NET RATE OF PRODUCTION (W-DOT/RHO*U) | $\dot{w}_i/\rho u$, mole/g-ft |
| PRESS | pressure, atm |
| PSI | stream function, $\left[\frac{\text{lbm}}{32.2} \text{ sec}^{-1}\right]^{\frac{1}{2}}$ |
| PT | radial grid point number |
| R | nozzle radius |
| REACTION J | refers to reactions listed on first page of output |
| RM | negative molar rate of production for jth reaction (see Section IV), mole/ ml-sec |
| RP | positive molar rate of production for jth reaction (see Section IV), mole/ ml-sec |
| SIGN. FREQ. | signal frequency for attenuation calculations, mHz |
| TEMPERATURE | K |
| TRANSVERSE ATTENUATION | db |
| UNIT ATTENUATION | db/in |
| VELOCITY | axial velocity, ft/sec |
| VISCOSITY | μ , lbm/ft-sec |
| X | axial distance, ft |
| X/R | nondimensional axial distance |
| Y/R | nondimensional radial distance from axis |

C. Card Output

1. Continuing Solution - Due to the large amount of input data required to continue a solution (after being terminated at a given value of x) the program will punch all input except the thermodynamic data and chemical reaction mechanism if this option is selected (Card 2, Cols. 31-35). However, a new final value of x (Card 4, Cols. 11-20) must be input manually if the problem was initially terminated by reaching the old maximum distance. Cards will also be produced if maximum time (Card 2, Cols. 36-40) is exceeded, by using the proper option.

2. Electron Density and Collision Frequency - The complete radial distribution of electron density and collision frequency at all printout stations will be punched if this option is selected (Card 2, Cols. 31-35).

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APPENDIX A

A FAST COMPUTER PROGRAM FOR NONEQUILIBRIUM
ROCKET PLUME PREDICTIONS

Fortran Listing


```

97 READ(5,100) MPSI,NS,ITURB,OH,IOU1,IOU2,(PURCH,ITIME,IPDESS,HT
98 MAIN (5,111) (FREQA(I), I=1,6)
99 DO 113 I=1,6
100 IF (FREQA(I)) 117, 114, 111
101 CONTINUE
102 I=7
103 NFREQA = I-1
104 NPSI=MPSI-I
105 PFAC (5,1000)X,XMAX,PRNT,XI,I(1),SIGMA(I),R,J,XK2
106 OX=0,1,RJ
107 INPUT MINIMUK STPFSIZE LIMIT (DXMIN)
108 PFAC(5,1000) DXMIN,FOL, PC(I),PCIP,PC(J),PC(K)
109 READ (5,1000)P,T(I),T(MPSI),U(I),U(MPSI),DELPSI,TKINET
110 IF (TKINET.EQ.0.0) TKINET = 400.0
111 TIME VALUE OF 30 SECONDS IS TO ALLOW FOR COMPILC TIME
112 LIMIT = 60*TIME-30
113 DIFFY = 0
114 CALL TICKS(I,SECT)
115 IF ((I,SECT)-60*TIME).GT.0.66400) IDIFFY = 0.6600-ISECT
116 UNIT = U(I)
117 I=77 = 2
118 USUR01 = 0.0
119 TURBULENCE MODELS
120 IF (ITURB - 3) 8600,9010,9010
121 IF (ITURB - 1) 9011,9010,9011
122 USUR01 = 0.95 * (U(I)-U(MPSI)) * U(MPSI)
123 9011 CONTINUE
124 IF (DELPSI) 3011,7012,3011
125 READ (5,1000)(ALPHA(J,I),J=1,NS)
126 PFAC (5,1000)(ALPHA(J,MPSI),J=1,NS)
127 MMD=MPSI-2
128 DO 4001 I=1,MMD
129 T(I)=T(I)
130 U(I)=U(I)
131 DO 4001 J=1,NS
132 ALPHA(J,I)=ALPHA(J,I)
133 DO 4002 J=1,NS
134 ALPHA(J,MPSI)=ALPHA(J,MPSI)
135 GO TO 3015
136 3011 READ (5,1000)(T(I),I=1,MPSI)
137 READ (5,1000)(U(I),I=1,MPSI)
138 DO 7 I=1,MPSI
139 7 READ (5,1000)(ALPHA(J,I),J=1,NS)
140 NEW THERMO DATA INPUT IN JANNAF TABLE FORM
141 3015 DO 1991 I=1,NS
142 READ(5,222) ATD(I),WHOLE(I),MF(I)
143 DO 10 I=1, NI,2
144 READ(5,102) TTR(I), CPT8(I,IT),GTR(I,IT),HT8(I,IT)
145 ATTE(IT,1) = CPT8(I,IT), GTR(I,IT),HT8(I,IT,1)
146 GTR(I,IT) = -GTR(I,IT),HT8(I,IT) *MF(I) *1000.
147 GTR(I,IT,1) = -GTR(I,IT,1),HT8(I,IT) *MF(I)*1000.
148 HT8(I,IT)=HT8(I,IT),MF(I)*1000.
149 HT8(I,IT,1)=HT8(I,IT,1),MF(I)*1000.
150 CONTINUE
151 IF (4*TMOLE(I)-1.0) 1972,1991,1991

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PROGRAM

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1072 IECC=1
1091 CONTINUE
DO 301 J = 1,6
DO 301 I = 1,NS
IF(AID(I).EQ.XAME(J)) ISAVE(J) = 1
301 CONTINUE
DO 1992 I=1,NR
READ (5,444)(71D(J),J=1,5),IRR(I),IRT(I),PC(I,K),K=1,3)
DD 1993 J=1,5
IRR(I,J)=0
DO 1993 L=1,NS
IF(71D(J)-AID(L)) 1993,1994,1993
1994 IRR(I,J)=L
1995 CONTINUE
1992 CONTINUE
DO 912 I=1,MPSI
WTVP=0.0
DO 632 J=1,NS
WTVP=WTVP+ALPHA(J,1)*WTHOLE(J)
DO 633 J=1,NS
633 ALPHA(J,1)=ALPHA(J,1)/WTVP
912 CONTINUE
IF(DELPSI) 903,3041,903
3041 DIM=0.0
DO 5001 J=1,NS
5001 DIM=DIM+ALPHA(J,1)
XMD=MOD-1
DELPSI=SORT(P*U(1)/42.285/T(1)/DIM)*RJ/XMD
903 DO 20 I=1,29
XI=I-1
PSI(I)=XI*DELPSI
XLE(I)=XLE(I)
20 SIGMA(I)=SIGMA(I)
DO 90 I=MPSI,29
RT(I)=T(MPSI)
T(I)=T(MPSI)
DO 90 J=1,NS
ALPHA(J,1)=ALPHA(J,MPSI)
90 ALPHA(J,1)=ALPHA(J,MPSI)
RU(I)=U(MPSI)
90 U(I)=U(MPSI)
CALL INOUT
PPUNCH = P
P=2117.0*P
PPDX=0.0
C PRESSURE OPTION, IF IPRESS=0, PRESSURE
C IS CONSTANT AND = TO P, IF IPRESS = 1, COEFFICIENTS CALLED
C PC(1),PC(2),PC(3),PC(4) ARE INPUT.
C EQUATION USED IS P = PC(1) + PC(2)*X + PC(3)*X*X + PC(4)*X*X*X
2 IF (IPRESS) 821,822,821
821 P=(PC(1)+X*(PC(2)+X*(PC(3)+X*PC(4))))*2117.0
PPDX=(PC(2)+X*(2.0*PC(3)+X*3.0*PC(4)))*2117.0
822 DO 31 I=1,MPSI
WTMIX(I)=0.0

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225 GO TO 8016
    A015 00200 = .0248*KK2
    8016 IF (U(1)-USUB01)*U(1)-U(MPS1)) A020.8020.8000
    A020 IF (USUB01-9000.0) A021.8021.8900
    8021 USUR01 = 10000.0
    WRITE (6,9900) X
    GO TO 8900
C
230 MODEL 6 BEFORE MIXING ZONE REACHES AXIS
    8900 009 = 0.95*(U(1)-U(MPS1)) + U(MPS1)
    DD 8802 I = 2.MPS1
    IF ((009-U(1))*(009-U(1-1)) 8804.8804.8804
    CONTINUE
    8804 00200 = Y(1-1)*Y(1)-Y(1-1))*(009-U(1-1))/U(1)-U(1-1)
    DO 8810 I = 1,MPS1
    8810 XWU(I) = 0010*RHO(I)
    GO TO 98
C
235 MODEL 6 AFTER MIXING ZONE REACHES AXIS
    8900 0011 = 00400*008*(00100-00200)
    DO 8910 I = 1,MPS1
    8910 XWU(I) = 0011*RHO(I)
    00200 = 0.0
    GO TO 98
240 9800 1077 = 9
    USUR01 = 0.0
    WRITE (6,9900) X
    9801 LL = ITURB + 1077
C
245 EDDY VISCOSITY MODEL 5
    GO TO (51,59,8666,78,8667,8668,9003,91.99,65,78,26.33,78),LL
C
250 MODEL 1 BEFORE MIXING ZONE REACHES AXIS
    8666 XWU(1) = 0.0137*(X+1.0E-05)*ABS(RHO(1))*U(1)-RHO(MPS1)*U(MPS1)
    GO TO 37
C
255 MODEL 3 BEFORE MIXING ZONE REACHES AXIS
    8667 XWU(1) = 0.00137*(X+1.0E-05)*RHO(1)*ANS(U(1))-U(MPS1)
    GO TO 37
C
260 MODEL 4 BEFORE MIXING ZONE REACHES AXIS
    8668 XWU(1) = 0.00137*(X+1.0E-05)*RHO(MPS1)*ANS(U(1))-U(MPS1)
    GO TO 37
C
265 91 DO 92 I=1,MPS1
    92 XWU(I) = 3.05E-8*(I)*.5/(I(1)+11.0)
    45 DUM = .5*(RHO(1)*U(1)+RHO(MPS1)*U(MPS1))
    I=MPS1-J+1
    IF (RHO(1)*U(1)-DUM) 52,52.51
C
270 MODEL 1 AFTER MIXING ZONE REACHES AXIS
    51 2*(Y(1)-Y(1-1))*U(1)-DUM)/(RHO(1)*U(1)-RHO(1-1))*U(1+1)
    XWU(1) = XK2*Z*ABS(RHO(1))*U(1)-RHO(MPS1)*U(MPS1)*0.025
    GO TO 37
    98 DO 39 I=1,MPS1
    39 XWU(I) = XK2*0.025
    GO TO 98

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280 7R RD=(U(1)+UMPSI)/2.0
    DO 47 I=2,MPSI
    IF ((RD-U(I))* (RD-U(I-1))) 4R,4R,47
47 CONTINUE
4R PHALVE=ETA(I-1)*(ETA(I)-ETA(I-1))*(RD-U(I-1))/(U(I)-U(I-1))
DUMMY=XK2*RHALVE*ABS(U(I)-UMPSI)*0.025
XHU(I)=DUMMY*RHO(I)
C 79 XHU(I)=DUMMY*(PHO(I)*ETA(I)/Y(I))*2/RHO(I)
GO TO 98
C MODEL 2 BEFORE MIXING ZONE REACHES AXIS
26 RD=(U(1)+UMPSI)/2.0
DO 27 I=2,MPSI
IF ((RD-U(I))* (RD-U(I-1))) 2R,2R,27
27 CONTINUE
2R PHALVE=Y(I-1)*(Y(I)-Y(I-1))*(RD-U(I-1))/(U(I)-U(I-1))
C MODEL 3 AFTER MIXING ZONE REACHES AXIS
XHU(I)=XK2*RHALVE*RHO(I)*ABS(U(I)-UMPSI)*0.025
DO 29 I=1,MPSI
29 XHU(I)=XHU(I)
GO TO 98
33 RD=(U(1)+UMPSI)/2.0
DO 34 I=2,MPSI
IF ((RD-U(I))* (RD-U(I-1))) 35,35,34
34 CONTINUE
35 PHALVE=Y(I-1)*(Y(I)-Y(I-1))*(RD-U(I-1))/(U(I)-U(I-1))
C MODEL 4 AFTER MIXING ZONE REACHES AXIS
XHU(I)=XK2*RHALVE*RHO(I)*ABS(U(I)-UMPSI)*0.025
37 DO 36 I=1,MPSI
36 XHU(I)=XHU(I)
GO TO 98
C MODEL 5 BEFORE MIXING ZONE REACHES AXIS
9003 XHU(I) = 0.00137*(2+1.0E-05)*ABS(UNIT-U(MPSI))*RHO(I)
DO 9004 I = 2,MPSI
XHU(I)=0.00137*(Y+1.0E-05)*ABS(UNIT-U(MPSI))*(RHO(I))*2/RHO(I)
9004 CONTINUE
9R A(I)=0.0
C CALCULATE A
DO 44 I=2,MPSI
44 A(I)=XHU(I)*RHO(I)*U(I)*Y(I)*Y(I)/PSI(I)
DO 899 L=1,MPSI
8RT=1.986*Y(L)
800TT=8RT*(L)
TX=I(L)
CALL TKEY(TX ,TTR,ITKEY,SDT,HDT,ANT)
IF (ITKEY.FD.0) GO TO 9
DO 855 I=1,MNS
G(I)=0.0
WH(I)=0.0
OX(I,L)=0.0
DO 872 J=1,MNS
CM(I,J,L)=0.0
872 CALL LIPLN(ITKEY,I, G1R,SDI,HDI,AX)

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G(I)=AX
CONTINUE
855 REACTION CALCULATION
C REACTION KINETICS CONTINUE DOWN TO 400 DEGREES K
C UNLESS KINET IS SET TO A VALUE OTHER THAN 400. K
C PFACIION KINETIC FOR ALL REACTIONS CONTINUE DOWN TO TKINET
IF(T(L)-TKINET) 3256,3256,3259
CONTINUE
3259 DO 862 I=1,NR
      RP(I,L)=0.0
      RK(I,L)=0.0
      KK = IRT(I)
C HFACIION CONSTANT TYPE
      GO TO (841,842,843,844,845,846,847),KK
841 RATE=RC(I,1)*AV
      GO TO 849
842 RATE=RC(I,1)/T(L)*AV
      GO TO 849
843 RATE=RC(I,1)/T(L)/T(L)*AV
      GO TO 849
844 RATE=RC(I,1)/ROOTI*AV
      GO TO 849
845 RATE=RC(I,1)*EXP(RC(I,3)/RRT)*AV
      GO TO 849
846 RATE=RC(I,1)*EXP(RC(I,3)/RRT)/T(L)*AV
      GO TO 849
847 RATE=RC(I,1)/T(L)/ROOTI*AV
      GO TO 849
849 CONTINUE
      K=IRRT(I)
C TYPE OF REACTION
      GO TO(864,865,866,870,871,834,835,836,837,838)*K
870 J1=IRRT(I,1)
      J2=IRRT(I,2)
      J3=IRRT(I,3)
      E = (G(J1)+G(J2)-G(J3))/RRT
      IF(ARS(E).LT.80.0) GO TO 700
      IF(E.LT.0.0) E = EXP(-80.0)
      IF(E.GT.0.0) E = EXP(80.0)
      GO TO 701
      E = EXP(E)
700 CONTINUE
      CRP=RATE*RHOUT(L)
      RP(I,L)=CRP*RHOUT(L)*ALPHA(J1,L)*ALPHA(J2,L)
      RP(I,L)=CRP*ALPHA(J3,L)/E/R/T(L)
      DO 771 J=1,3
      SIGN=1.0
      IF (J.GT.2) SIGN=-1.0
      IRON= IRRP(I,J)
      CH(IRON,J1,L) = CM(IRON,J1,L) + SIGN*RP(I,L)/ALPHA(J1,L)
      CH(IRON,J2,L) = CM(IRON,J2,L) + SIGN*RP(I,L)/ALPHA(J2,L)
      CH(IRON,J3,L) = CM(IRON,J3,L) - SIGN*RM(I,L)/ALPHA(J3,L)
771 OX(IRON,L) = OX(IRON,L) + SIGN*RP(I,L)
      GO TO 868
871 J1=IRRT(I,1)
      J2=25

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445 707 CONTINUE
      CRP=RATE*RHOUT(L)*RHOUT(L)*WTMIX(L)*AV
      RP(I,L)=CRP*RHOUT(L)*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=CRP*ALPHA(J3,L)/(E*RR(I))
      DO 774 J=1,3
      SIGN=1.0
      IF (J.GT.2) SIGN=-1.0
      IP0W= IRRR(I,J)
      CM(IP0W,J1,L)= CM(IP0W,J1,L) *SIGN*RP(I,L)/ALPHA(J1,L)
      CM(IP0W,J2,L)= CM(IP0W,J2,L) *SIGN*RP(I,L)/ALPHA(J2,L)
      CM(IP0W,J3,L)= CM(IP0W,J3,L) -SIGN*RM(I,L)/ALPHA(J3,L)
      774 OX(IP0W,L)= OX(IP0W,L) + SIGN*(RP(I,L) )
      GO TO 868
      866 J1=IRRR(I,1)
      J2=IRRR(I,2)
      J3=IRRR(I,3)
      J4=IRRR(I,4)
      J5=IRRR(I,5)
      E = (G(J1)+G(J2)-G(J3)-G(J4)-G(J5))/RRR
      IF (ABS(E).LT.80.0) GO TO 708
      IF (E.LT.0.0) E=EXP(-80.0)
      IF (E.GT.0.0) E = EXP(80.0)
      GO TO 709
      E = EXP(E)
      708 CONTINUE
      CRP=RATE*RHOUT(L)*RHOUT(L)
      RM(I,L)=CRP*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=CRP*ALPHA(J3,L)*ALPHA(J4,L)*ALPHA(J5,L)*RHOUT(L)*RR(I,L)/E
      DO 775 J=1, 5
      SIGN=1.0
      IF (J.GT.2) SIGN=-1.0
      IP0W= IRRR(I,J)
      CM(IP0W,J1,L)= CM(IP0W,J1,L) *SIGN*RP(I,L)/ALPHA(J1,L)
      CM(IP0W,J2,L)= CM(IP0W,J2,L) *SIGN*RP(I,L)/ALPHA(J2,L)
      CM(IP0W,J3,L)= CM(IP0W,J3,L) -SIGN*RM(I,L)/ALPHA(J3,L)
      CM(IP0W,J4,L)= CM(IP0W,J4,L) -SIGN*RM(I,L)/ALPHA(J4,L)
      CM(IP0W,J5,L)= CM(IP0W,J5,L) -SIGN*RM(I,L)/ALPHA(J5,L)
      775 OX(IP0W,L)= OX(IP0W,L) + SIGN*(RP(I,L)-? *RM(I,L))
      GO TO 861
      837 J1=IRRR(I,1)
      J2=IRRR(I,2)
      J3=IRRR(I,3)
      CRP=RATE*RHOUT(L)
      RM(I,L)=CRP*RHOUT(L)*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=0.0
      DO 776 J=1, 3
      SIGN=1.0
      IF (J.GT.2) SIGN=-1.0
      IP0W= IRRR(I,J)
      CM(IP0W,J1,L)= CM(IP0W,J1,L) *SIGN*RP(I,L)/ALPHA(J1,L)
      CM(IP0W,J2,L)= CM(IP0W,J2,L) *SIGN*RP(I,L)/ALPHA(J2,L)
      OX(IP0W,L)= OX(IP0W,L) + SIGN* RP(I,L)
      GO TO 869
      838 J1=IRRR(I,1)
      J2=25

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PROGRAM MAIN

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500 J3=IPRR(I,3)
      J4=IRRR(I,4)
      CR=RATE*RHOOUT(L)*RHOOUT(L)*WTMIX(L)
      RP(I,L)=CR*ALPHA(J1,L)
      RM(I,L)=0.0
      DO 777 J=1, 4
        SIGN=1.0
        IF (J.GT.2) SIGN=-1.0
        IROW= IRRR(I,J)
        IF (J.EQ.2) IROW=25
        777 CM(IROW,J1,L)= CM(IROW,J1,L) +SIGN*CR
           GO TO 867
834 J1=IRRR(I,1)
      J2=IRRR(I,2)
      J3=IRRR(I,3)
      J4=IRRR(I,4)
      CR=RATE*RHOOUT(L)*RHOOUT(L)
      RP(I,L)=CR*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=0.0
      DO 778 J=1, 4
        SIGN=1.0
        IF (J.GT.2) SIGN=-1.0
        IROW= IRRR(I,J)
        CM(IROW,J1,L)= CM(IROW,J1,L) +SIGN*RP(I,L)/ALPHA(J1,L)
        CM(IROW,J2,L)= CM(IROW,J2,L) +SIGN*RP(I,L)/ALPHA(J2,L)
        778 OX(IROW,L)= OX(IROW,L) + SIGN* RP(I,L)
           GO TO 867
835 J1=IRRR(I,1)
      J2=IRRR(I,2)
      J3=IRRR(I,3)
      CR=RATE*RHOOUT(L)*RHOOUT(L)*WTMIX(L)*AV
      RP(I,L)=CR*RHOOUT(L)*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=0.0
      DO 779 J=1, 3
        SIGN=1.0
        IF (J.GT.2) SIGN=-1.0
        IROW= IRRR(I,J)
        CM(IROW,J1,L)= CM(IROW,J1,L) +SIGN*RP(I,L)/ALPHA(J1,L)
        CM(IROW,J2,L)= CM(IROW,J2,L) +SIGN*RP(I,L)/ALPHA(J2,L)
        779 OX(IROW,L)= OX(IROW,L) + SIGN* RP(I,L)
           GO TO 868
836 J1=IRRR(I,1)
      J2=IRRR(I,2)
      J3=IRRR(I,3)
      J4=IRRR(I,4)
      J5=IRRR(I,5)
      CR=RATE*RHOOUT(L)*RHOOUT(L)
      RP(I,L)=CR*ALPHA(J1,L)*ALPHA(J2,L)
      RM(I,L)=0.0
      DO 780 J=1, 5
        SIGN=1.0
        IF (J.GT.2) SIGN=-1.0
        IROW= IRRR(I,J)
        CM(IROW,J1,L)= CM(IROW,J1,L) +SIGN*RP(I,L)/ALPHA(J1,L)
        CM(IROW,J2,L)= CM(IROW,J2,L) +SIGN*RP(I,L)/ALPHA(J2,L)

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PROGRAM      MAIN
555          780 OX(IRON,L)= OX(IRON,L)+ SIGN* RP(I,I)
              CALCULATE WOOT
              MAIN
556          861 WP(JS)=WP(JS)+PP(I,L)
              MAIN
557          WW(JS)=WW(JS)+WP(I,L)
              MAIN
558          WP(J4)=WP(J4)+RP(I,L)
              MAIN
559          WP(J3)=WP(J3)+RP(I,L)
              MAIN
560          WW(J3)=WW(J3)+RM(I,L)
              MAIN
561          WP(J2)=WP(J2)+RP(I,L)
              MAIN
562          WP(J1)=WP(J1)+RM(I,L)
              MAIN
563          WW(J1)=WW(J1)+RP(I,L)
              MAIN
564          CONTINUE
              MAIN
565          3P56 DO R97 J=L,NS
              DO R97 J=L,NS
              MAIN
566          997 WOOT(J,L)=(WP(J)-WW(J))/RHOOOT(L)/U(L)
              MAIN
567          999 CONTINUE
              MAIN
568          IOUT=IOUT+1
              MAIN
569          CALL SWITCH(1,K000FX)
              MAIN
570          GO TO(62,63)*K000FX
              MAIN
571          EOUT=RH0(1)*ALPHA(IECC,1)*J10RE23
              MAIN
572          PRINT 61,X,T(1),U(1),EOUT,IOUT
              MAIN
573          61 FORMAT(3H0X=1PE15.7,3H T=1PE15.7,3H U=1PE15.7,6H E/CC=1PE15.7,7H S
              MAIN
574          )TPFS=15)
              MAIN
575          63 IF(IFINIS) 64,69,64
              MAIN
576          54 CALL SWITCH(3,K000FX)
              MAIN
577          GO TO(66,65)*K000FX
              MAIN
578          65 IF(X-XMAX) 67,66,66
              MAIN
579          67 IF(PRNT-PCNT) 69,69,68
              MAIN
580          68 CONTINUE
              MAIN
581          GO TO 5
              MAIN
582          66 IFINIS=2
              MAIN
583          69 CALL OUTPUT
              MAIN
584          PCNT=0.0
              MAIN
585          IF(IFINIS-1) 5,5,6
              MAIN
586          C      CHECK DIFFUSION STEP SIZE
              MAIN
587          5 XD=DELPSI*DELPSI*SIGMA(1)/XWU(1)/XLE(1)/12.0 *FDL
              MAIN
588          DO 511 I=2,NPSI
              MAIN
589          DUMMY=A(I+1)+ACL-1)+A(I)+A(I)
              MAIN
590          DUMMY=PSI(1)*DELPSI*DELPSI*SIGMA(1)/XLF(1)/DUMMY/1.5*FDL
              MAIN
591          XD=AMINI(XD,DUMMY)
              MAIN
592          DX=AMINI(DX,XD)
              MAIN
593          DO 101 I=2,NPSI
              MAIN
594          FX1=PSI(1)*DELPSI**2/DY
              MAIN
595          EX1=.5*(A(I)+A(I+1))
              MAIN
596          FX12=.5*(A(I)+A(I+1))
              MAIN
597          C      INTEGRATE MOMENTUM EQUATION
              MAIN
598          PH(I)=(EX11*(U(I+1)-U(I))+FX12*(U(I+1)-U(I)))/EX1+U(I)
              MAIN
599          PH(I)=PU(I)-DX*DPX/RH0(1)/U(I)
              MAIN
600          F*3=0.0
              MAIN
601          F*4=0.0
              MAIN
602          DO 21 J=1,NS
              MAIN
603          F*3=EX3+H(J,1)*WDOT(J,1)
              MAIN
604          F*4=EX4+CP(J,1)*(ALPHA(J,I+1)-ALPHA(J,I-1))
              MAIN
605          EX2=EX1+CPHAR(1)
              MAIN

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607     EX5=XLE(I)*A(I)/SIGMA(I)
608     EX6=.5*(EX5+XLE(I-1)*A(I-1)/SIGMA(I-1))
609     EX7=.5*(EX5+XLE(I-1)*A(I-1)/SIGMA(I-1))
610     EX8=CPBAR(I)*A(I)/SIGMA(I)
611     EX9=.5*(EX8+CPBAR(I-1)*A(I-1)/SIGMA(I-1))
612     EX10=.5*(EX8+CPBAR(I-1)*A(I-1)/SIGMA(I-1))
613     EX14=EX4*EX5/4.0
614     INTEGRATE ENERGY EQUATION
615     R(I)= (U(I+1)-U(I-1))*2*A(I)/EX2/4.0+DX*DPDX/RHO(I)/CPBAR(I)+T(I)
616     I*(EX9+EX14)*T(I+1)+(EX10-EX14)*T(I-1)-(EX9+EX10)*T(I)/EX2-EX3*DX
617     /CPBAR(I)
618     RHOUIX=DX/(RHOUIT(I)*U(I))
619     INTEGRATE SPECIES EQUATIONS
620     DO 41 J=1,NS
621     I(J)= (EX6*(ALPHA(J,I+1)-ALPHA(J,I))+EX7*(ALPHA(J,I-1)-ALPHA
622     I(J,I)))/EX1+ALPHA(J,I)* OX(J,I)*RHOUIX
623     DO 781 N=1,NS
624     DO 781 M=1,NS
625     CM(M,N)= CM(M,N,1)*RHOUIX
626     IF (M.EQ.N) CM(M,N)=CM(M,N) *1.0
627     781 CONTINUE
628     CALL SLDP(OX1,CM1,NS)
629     FORMAT (1H, 2I5)
630     DO 782 J=1, NS
631     RALPHA(J,I)= OX1(J)
632     101 CONTINUE
633     WRITE(6,786) DX,X
634     FORMAT(1H, 1P2E12.5)
635     EX3=4.0*XNU(I)*DX/DELPSI/DELPSI
636     RHOUIX=DX/(RHOUIT(I)*U(I))
637     COMPUTE U AT CENTER LINE
638     R(I)=EX3*(U(2)-U(1))+I(I)-DX*DPDX/RHO(I)/U(I)
639     FX4=0.0
640     DO 200 J=1,NS
641     EX4=EX4+H(U,J)*WDOT(J,I)
642     RALPHA(J,MPSI)=ALPHA(J,MPSI)
643     200 OX1(J) =EX3*XL(I)*(ALPHA(J,2)-ALPHA(J,1))/SIGMA(I)+ALPHA(J,I)
644     I+ OX(J,I)*RHOUIX
645     DO 783 N=1,NS
646     DO 783 M=1,NS
647     CM(M,N)= CM(M,N,1)*RHOUIX
648     IF (M.EQ.N) CM(M,N)=CM(M,N) *1.0
649     783 CONTINUE
650     CALL SLDP(OX1,CM1,NS)
651     DO 784 J=1, NS
652     COMPUTE SPECIES AT CENTER LINE
653     RALPHA(J,I)= OX1(J)
654     CALCULATE TEMP. AT CENTER LINE
655     PT(I)=EX3*(T(2)-T(1))/SIGMA(I)+T(I)+DX*DPDX/RHO(I)/CPBAR(I)
656     I-FX4*DX/CPBAR(I)
657     PT(MPSI)=T(MPSI)
658     IF (IEDGE) 230,231,230
659     COMPUTE TEMP. AND U AT EDGE
660     PH(MPSI)=U(MPSI)-DX*DPDX/RHO(MPSI)/U(MPSI)
661     PT(MPSI)=T(MPSI)+DX*DPDX/RHO(MPSI)/CPBAR(MPSI)

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PROGRAM MAIN

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DC 210 I=MPSI,29
RU(I)=RU(MPSI)
U(I)=RU(MPSI)
PT(I)=RT(MPSI)
210 T(I)=RT(MPSI)
231 CONTINUE
1 IFNIS=1
921 SAVEX=X
-----
DO 941 I=1,29
SAVEU(I)=U(I)
SAVET(I)=T(I)
DO 940 J=1,NS
SAVEA(J,I)=ALPHA(J,I)
940 CONTINUE
941 CONTINUE
MINIT = 13
MHALF = 25
NTEST=MPSI-1
DO 967 I=1,NTEST
CHECK_NEGATIVE_MOLE_FRACTION.
C
965 DO 967 J=1,NS
IF (RALPHA(J,I)) 995,967,967
967 CONTINUE
X=X+DX
PCNT=PCNT+DX
DX=XD
DO 925 I=1,29
DO 926 J=1,NS
926 ALPHA(J,I)=RALPHA(J,I)
T(I)=RT(I)
925 U(I)=RU(I)
GO TO 999
995 IF (DX.LT.DXMIN) GO TO 8000
981 DX=SAVEDX/2.0
X=SAVEX
DO 985 I=1,29
DO 982 J=1,NS
982 ALPHA(J,I)=SAVEA(J,I)
T(I)=SAVET(I)
985 U(I)=SAVEU(I)
GO TO 2
C
IF MPSI .GE. 26 .MPSI IS HALVED
999 IF (MPSI-MHALF) 1001,1500,1500
1001 IF (ABS(U(MPSI)-U(MPSI-1))/U(MPSI)) .GT. 0.101, 1011,1011,1004
1011 IF (ABS(T(MPSI)-T(MPSI-1))/T(MPSI)) .GT. 0.050, 1002,1002,1004
1002 CONTINUE
GO TO 2000
1004 MPSI=MPSI-1
MPSI=MPSI-1
DO 1101 I=MPSI,29
SAVEU(I)=U(MPSI)
SAVET(I)=T(MPSI)
U(I)=U(MPSI)
SAVET(I)=T(MPSI)
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T(I)=T(NPSI)
PT(I)=T(NPSI)
DO 1102 J=1,NS
SAVEA(J,I)=ALPHA(J,NPSI)
ALPHA(J,I)=ALPHA(J,NPSI)
1102 RALPHA(J,I)=ALPHA(J,NPSI)
1101 CONTINUE
GO TO 2000
1500 .IFINIS=0
ORLPSI=DELPSI*DFLPSI
DO 1600 I=1,MINIT
DO 1650 J=1,NS
1650 ALPHA(J,I)=ALPHA(J,2*I-1)
T(I)=T(2*I-1)
1600 U(I)=U(2*I-1)
NPSI=MINIT
NPSI=NPSI-1
DO 1700 I=MINIT,29
DO 1750 J=1,NS
ALPHA(J,I)=ALPHA(J,NPSI)
1750 RALPHA(J,I)=ALPHA(J,NPSI)
T(I)=T(NPSI)
RT(I)=T(NPSI)
U(I)=U(NPSI)
1700 RU(I)=U(NPSI)
DO 1800 I=2,29
1800 PSI(I)=PSI(I-1)*DELPSI
ITER=0
ISTEP=0
GO TO 2000
8000 WRITE (6,8001)
8001 FORMAT(68HNEGATIVE PARAMETER - NOT CORRECTED BY REPEATED HALVING
10F,STEP SIZE)
.IFINIS=2
GO TO 69
2000 CONTINUE
CALL TICK(ISECS)
TELAPS = ISECS-ISECST
IF(TELAPS.LT.0) TELAPS = IDIFFT + ISECS
IF(TELAPS.GE.ILIMIT) GO TO 6
GO TO 2
100 FORMAT(14I5)
102 FORMAT(8F10.4)
111 FORMAT (7(IPE10.3))
222 FORMAT (A6.7E10.3)
333 FORMAT (12A6)
444 FORMAT (A6.1X,A6.8X,A6.1X,A6.7X,I2,I1,E8.2,F4.1,F9.1)
666 FORMAT (10I5)
1000 FORMAT (7E10.3)
9900 FORMAT (39H1 MIXING REGION INTERSECTS AXIS AT X = IPE15.7)
IF(IPUNCH.EQ.0.OR.IPUNCH.EQ.?) GO TO 9
PUNCH333,(TITLE(I),I=1,12)
PUNCH 666,MPSI,NS,ITURR,NR,IOUT1,IOUT2,IPUNCH,ITIME,IPRESSANT
PUNCH 555,FREQA(1),FREQA(2),FREQA(3),FREQA(4),FREQA(5),FREQA(6)

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PROGRAM MAIN

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PUNCH 555,X,XHAX,PRNT,XLE(1),SIGHA(1),RJ,XK2
PUNCH 555,DXMIN,FIL,PC(1),PC(2),PC(3),PC(4)
PUNCH 555,PPUNCH,T(1),TIMPSI,U(1),UMPSI,DELPSI,TKINET
PUNCH 555,(T(I),I=1,MPSI)
PUNCH 555,(U(I),I=1,MPSI)
ON H I = 1,MPSI
PUNCH 555,(RALPHA(J,I),J=1,NS)
R CONTINUE
9 CONTINUE
END

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SUBROUTINE OUTPUT
DIMENSION A(30),RHO(30),Y(30),T(30),PSI(30),RT(30),SUM(30),AR(25),
JHSTAT(30),H(25,30),ALPHA(25,30),RALPHA(25,30),CP(25,30),SIGMA(30),
WFM0(F(25),CPRAP(30),C(25,9),AID(25),ETA(30),RATIO(30),
3RU(30),U(30),T1E(12),XLE(30),XMU(30)
4RC(40,3),IRRR(40,5),WR(25),WM(25),WDT(25,30),SAVET(30),SAVEU(30),
5 IRR(40),ERED(30),SAVEA(25,30),
6 ECC(30),HOUT(30),YOUT(30),RHOUT(30),XHUOUT(30),XLT(30),
7T4(30),TFDG(30),IRT(40),REL(40,30),RM(40,30),
DIMENSION ISAVE(6),FREQA(6),ALOC(50,6),ATT(6),YATT(50)
COMMON A , AR , Y , H , HSTAT , H , PSI , RT ,
COMMON SUM , ALPHA , RALPHA ,
COMMON CP , SIGMA , WFM0LE , C ,
COMMON AID , ETA , RATIO , RU , U , TITLE
COMMON XLE , XHU , G , WFMIX , WDT ,
COMMON SAVEU , SAVET , WM , WP , RC , X , XMAX
COMMON SAVEA , PC , X
COMMON PRNT , DXMIN , DX , FDL , DELPSI , RJ
COMMON XK2 , P , ZID , FREQ , ECC , DPDX
COMMON YOUT , HOUT , RHOUT , IRRP , IRR , IFINIS
COMMON IPAGE , MPSI , BY , NS , NR , LEDGE
COMMON ITURB , IPRESS , NP5I , ITES , ITR , IECC
COMMON IPT , XHUOUT , XLT , T4 , TFDG , IOUT
COMMON IOUT1 , IOUT2 , RP , RM , ISAVE , IPUNCH
COMMON TRINET,NFREQA,ALOC,FREQA,00100,00200,00300,00400
DATA ZC02/6HC0 /
DATA ZH20/6HR20 /
RTG=1.0E30
DO 5 I=1, NS
IF (AID(I),EQ,ZC0 ) IC0=I
IF (AID(I),EQ,ZC02) IC02=I
IF (AID(I),EQ,ZH20)...IRZ0=I
6 CONTINUE
531 DO 532 I=1,MPSI
532 ECC(I)=RHO(I)*ALPHA(IECC,I)*3.108E23
539 DO 10 I=1,MPSI
YOUT(I)=Y(I)/PJ
XHUOUT(I)=XHU(I)*32.174
HOUT(I)=HSTAT(I)/45055.31
SUM(I)=0.0
DO 10 J=1,NS
10 SUM(I)=SUM(I)+ALPHA(J,I)*WFM0LE(J)
UD=.05*U(I)+.95*U(MPSI)
DO A3 I=2,MPSI
IF ((U(I)-UD)*(U(I-1)-UD)) > .84,84.83
A3 CONTINUE
A4 VP=(Y(I)-Y(I-1))*(UD-U(I-1))/(U(I)-U(I-1))+Y(I-1)
TC=.05*T(I)+.95*T(MPSI)
DO A5 I=2,MPSI
IF ((T(I)-TC)*(T(I-1)-TC)) > .86,86.85
A5 CONTINUE
A6 TP=(Y(I)-Y(I-1))*(TD-T(I-1))/(T(I)-T(I-1))+Y(I-1)
TP=TR/RJ

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110 OUTPUT
111 OUTPUT

VP=VR/PJ
DO 87 J=1,NS
  AR(J)=0
  AD=.05*ALPHA(J,1)*.95*ALPHA(J,MPSI)
  IP(ALPHA(J,MPSI)) 91,92,91
  91 DO 88 I=1,MPSI
    IF(ALPHA(J,I)-AD) 88,88,89
  88 CONTINUE
  89 AR(J)=Y(I-1)+Y(I)*(1-1)/(ALPHA(J,I)-ALPHA(J,I-1))
  AR(J)=AR(J)/RJ
  60 TO 87
  92 DO 93 I=1,MPSI
    IF(ALPHA(J,I)-AD) 94,93,93
  93 CONTINUE
  94 DO 94 TO 89
  87 CONTINUE
  PCNT=0.0
  IPAGE=IPAGE+1
  WRITE (6,201)X,(TITLE(I),I)=1,12),IPAGE
  WRITE (6,102)
  XQJ=X/RJ
  POUT=P/2117.0
  DPOUT=DPDX/2117.0
  WRITE(6,103) XQJ,DX,POUT
  IF (ITURB-6) 8600,8500,8600
  8500 WRITE (6,8555)
  00101=00100/RJ
  00201=00200/RJ
  WRITE (6,8556) 00101,00201,00300,00400
  8556 FORMAT(1H0.8X,4HHALF,21X,12HINFR MIXING,17X,11HMACH NUMBER,16X,11
    *MIXING RATE/7X,10HRADIUS/R ,16X,15HZONE RADIUS/P ,14X,14HAT HAL
    *F RADIUS,14X,11HCOEFFICIENT)
  855A FORMAT (4X,1PE14.6,1P3E28.6)
  8600 WRITE (6,107)
  DO 73 I=1,MPSI
    WRITE (6,509)
    SSI= 89517.501*WTHIX(I)
    SS2= CPBAR(I)/(CPBAR(I)-SS1)
    SS=SQRT(SS2*SS1)*T(I)
    XMACH= U(I)/SS
    IF(IECC) 71,72,71
    71 WRITE (6,207)I,YOUT(I),U(I),T(I),RHOUT(I),XMACH, HOUT(I), XMUOUT(
      11),FCC(I),PSI(I),I
    60 TO 73
    72 WRITE (6,307)I,YOUT(I),U(I),T(I),RHOUT(I),XMACH, HOUT(I), XMUOUT(
      11),PSI(I),I
    73 CONTINUE
    DO 581 I=1,MPSI
    DO 581 J=1,NS
    581 RALPHA(J,I)=ALPHA(J,I)/WTHIX(I)
    DO 564 KK=1,1RPT
    11=1+(KK-1)*7
    1P=7*(KK-1)*7

```

```

112 WRITE (6,201)X,(I11LL(I),I=1,IP1),IPAGE
113 WRITE (6,400)
114 WRITE (6,108)(A10(J),J=11,12)
115 DO 41 I=1,NP51
116 A1 WRITE (6,208)I,YOUT(I),(RALPHA(J),J=11,12),I
117 IF(IOUT)564,564,74
118 74 WRITE (6,420)
119 WRITE (6,421)(A10(J),J=11,12)
120 DO 82 I=1,NP51
121 IF(I(I)-TKIN(I)) 564,564,R2
122 82 WRITE (6,422)I,(WDOI(J),J=11,12),I
123 564 CONTINUE
124 IF(I(OUT2))567,567,75
125 75 IP1=(NR*9)/10
126 N=0
127 NNR=NR-1
128 DO 565 NK=1,IP1
129 LI=0
130 N=1
131 WRITE (6,201)X,(TITLE(I),I=1,12),IPAGE
132 I1=1*(N-1)*5
133 I2=5*(N-1)*5
134 NNN1=11
135 NNN2=11*1
136 NNN3=11*2
137 NNN4=11*3
138 NNN5=12
139 WRITE (6,209)
140 WRITE (6,431)NNN1,NNN2,NNN3,NNN4,NNN5
141 DO 63 I=1,NP51
142 WRITE (6,432)
143 IF(I(I)-TKIN(I)) 566,566,63
144 63 WRITE (6,433)I,YOUT(I),(RP(J),J=11,12),I
145 64 IF(NNR/5*N)565,565,64
146 64 IF(LL)565,66,565
147 65 N=1
148 LL=1
149 GO TO 65
150 565 CONTINUE
151 567 CONTINUE
152 I=(IPUNCH.FO.0.OP,IPUNCH.EO.2) GO TO 568
153 C-*** COMPUTE AND OUTPUT THE COLLISION FREQUENCY
154 569 IF (NFREQA) 1065, 1065, 1065
155 1045 WRITE (6,600)
156 WRITE (6,601)
157 GO TO 1066
158 CONTINUE
159 1065 CONTINUE
160 WRITE (6,600)
161 WRITE (6,601)
162 WRITE (6,1013) (FREQA(J), J=1,NFREQA)
163 WRITE (6,1068)
164 DO 502 I=1,NP51
165 F1 = 1.0/SQRT(I)
166 F2 = 1.0/F1

```

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```

170 FT3 = 1.0/1(I)
    FT4 = 1(I)*0.75
    SUMS = 0.0
    DO 603 I = 1,6
      IF (ISAVE(IDX).EQ.0) GO TO 603
      K = ISAVE(IDX)
      IFRM = ALPHA(K,I)
      GO TO (604,605,606,607,608,614),IDX
604 Q = (1.29E-17)*FT2 + 2.46E-16
605 O = (0.758E-13)*FT1
606 O = (1.53E-11)*FT3
607 Q = (9.0E-18)*FT2 + 8.9E-16
608 Q = 3.29E-23*6.21E5*FT2
609 GO TO 609
614 Q = 1.85*(6.21)**(-2)*(1.0E-10)*FT3
609 SUMS = SUMS + O*TERM
607 CONTINUE
XNEU = (4.57E27)*SUMS*POUT*FT1
ECON = 0.07157* ECC(I)/XNEU
IF (NFREQA) 1000, 1001, 1000
1000 CATT = 1.17
      GO 1003 J = 1,NFREQA
      ALOC1 = 1. + (6.283*6.283*FREQA(J)*FREQA(J))*1.0E12/(XNEU*XNEU)
1003 ALOC(I,J) = CATT*ECC(I)/XNEU*ALOC1
      GO TO 1008
1001 WRITE(6,610) I, YOUT(I),XNEU,ECON
      GO TO 1010
1008 WRITE(6,610) I, YOUT(I),XNEU,ECON,(ALOC(I,J),J=1,NFREQA)
1010 IF (IPUNCH.EQ.0.OR.IPUNCH.EQ.2) GO TO 602
      RPT = YOUT(I)
      PFCO = ALPHA(ICO,I)*POUT
      PFCO2 = ALPHA(ICO2,I)*POUT
      PPH2O = ALPHA(IP2O,I)*POUT
      WRITE(7,780) RPT,ECC(I),XNEU,T(I),PPCO,PPCO2,PPR20
602 CONTINUE
1009 DO 1004 J = 1,NFREQA
      IF (NFREQA) 1009, 1015, 1009
      DO 1005 I = 1, NPSI
1005 YATT(I) = 24.0*YALOC(I,J)
      CALL GRATE(ATT(J),YATT,YOUT,NPSI)
1004 CONTINUE
      WRITE (6,1014) (ATT(J),J=1,NFREQA)
1015 CONTINUE
102 FORMAT(1H0,8X,3HX/R,
      1FFET,4X,10HPRESS(ATM)).
103 FORMAT(4X,186E16.6)
107 FORMAT(4H0 PT,5X,3HY/R, 6X,9HVELOCITY,6X,11HTEMPERATURE,5X,7HDENSI
      1TY, 6X,8HMACH NO., 8X,8HENTHALPY,5X,9HVISCOISITY,5X,*ELECTRON*
      2, 8X,3HPSI,6X,2HPT )
109 FORMAT(3H0PT,3X,5H Y/R, 7(3X,46,4X),1X,3H PT)
201 FORMAT(1H1,//////3H X=1PE15.75H FEET,8X,12A6,8X,4HPAGE16)

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170 OUTPUT 167
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SUBROUTINE INOUT
  WTIX(MPSI)=0.0
  DO 1920 J=1,NS
    WTIX(J)=WTIX(J)+ALPHA(J,1)
  1930 WTIX(MPSI)=WTIX(MPSI)+ALPHA(J,MPSI)
  DO 1919 J=1,NS
    ALPHA(J,1)=ALPHA(J,1)/WTIX(J)
  1919 ALPHA(J,MPSI)=ALPHA(J,MPSI)/WTIX(MPSI)
    WRITE (6,120)
  DO 159 I=1,NR
    L=IPR(I)
    GO TO(131,132,133,134,135,136,137,138,139,140),L
  131 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    J4=IRRR(I,4)
    WRITE (6,121)I,AID(J1),AID(J2),AID(J3),AID(J4),(RC(I,J),J=1,3)
    GO TO 159
  132 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    WRITE (6,122)I,AID(J1),AID(J2),AID(J3),(RC(I,J),J=1,3)
    GO TO 159
  133 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    J4=IRRR(I,4)
    J5=IRRR(I,5)
    WRITE (6,123)I,AID(J1),AID(J2),AID(J3),AID(J4),AID(J5),(RC(I,J),J=
    1,5)
    GO TO 159
  134 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    WRITE (6,124)I,AID(J1),AID(J2),AID(J3),(RC(I,J),J=1,3)
    GO TO 159
  135 J1=IRRR(I,1)
    J2=IRRR(I,3)
    J3=IRRR(I,4)
    WRITE (6,125)I,AID(J1),AID(J2),AID(J3),(RC(I,J),J=1,3)
    GO TO 159
  136 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    J4=IRRR(I,4)
    WRITE (6,126)I,AID(J1),AID(J2),AID(J3),AID(J4),(RC(I,J),J=1,3)
    GO TO 159
  137 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)
    WRITE (6,127)I,AID(J1),AID(J2),AID(J3),(RC(I,J),J=1,3)
    GO TO 159
  138 J1=IRRR(I,1)
    J2=IRRR(I,2)
    J3=IRRR(I,3)

```

SUBROUTINE INOUT

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115      J4=IRRR(I,4)
        J5=IRRR(I,5)
        WRITE (6,128)I,AID(J1),AID(J2),AID(J3),AID(J4),AID(J5),(RC(LA,J),J=
116      11,3)
        GO TO 159
117      J1=IRRR(I,1)
        J2=IRRR(I,2)
        J3=IRRR(I,3)
        WRITE (6,129)I,AID(J1),AID(J2),AID(J3),(RC(LA,J),J=1,3)
120      GO TO 159
121      J1=IRRR(I,1)
        J2=IRRR(I,2)
        J3=IRRR(I,3)
        WRITE (6,130)I,AID(J1),AID(J2),AID(J3),(RC(I,J),J=1,3)
122      CONTINUE
123      159 CONTINUE
124      120 FOPMAT(1H0,19X,26HREACTIONS REING CONSIDERED,6X,19HXR=A*EXP(B/RT)/
125      11*8N,7X,1HA,8X,1HN,9X,1HB,7X,* (MOLECUF-ML-SEC UNITS)*
126      121 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,2H* ,A6,18X,1PE9,3,2X,0PF4,1,2X
127      1A,F10,1)
128      122 FOPMAT(19,9X,A6,2H* ,A6,3H* ,M,5X,2H* ,A6,3H* ,M,23X,1PE9,3,2X,0PF4,
129      11,2X,F10,1)
130      123 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,2H* ,A6,10X,1PE9,3,2X,0
131      1PF4,1,2X,F10,1)
132      124 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,26X,1PE9,3,2X,0PF4,1,2X,F10,1)
133      125 FOPMAT(19,9X,A6,3H* ,M,13X,2H* ,A6,2H* ,A6,3H* ,M,15X,1PE9,3,2X,0PF4
134      1A,2X,F10,1)
135      126 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,26X,1PE9,3,2X,0PF4,1,2X,
136      1F10,1,3X,16HONE WAY REACTION)
137      127 FOPMAT(19,9X,A6,2H* ,A6,3H* ,M,5X,2H* ,A6,3H* ,M,23X,1PE9,3,2X,0PF4,
138      11,2X,F10,1,3X,16HONE WAY REACTION)
139      128 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,2H* ,A6,2H* ,A6,10X,1PE9,3,2X,0
140      1PF4,1,2X,F10,1,3X,16HONE WAY REACTION)
141      129 FOPMAT(19,9X,A6,2H* ,A6,8X,2H* ,A6,26X,1PE9,3,2X,0PF4,1,2X,
142      1F10,1,3X,16HONE WAY REACTION)
143      130 FOPMAT(19,9X,A6,2H* ,A6,3H* ,M,13X,2H* ,A6,2H* ,A6,3H* ,M,15X,1PE9,3,2X,0PF4
144      1A,2X,F10,1,3X,16HONE WAY REACTION)
145      131 FOPMAT(19,9X,A6,2H* ,A6,3H* ,M,13X,2H* ,A6,2H* ,A6,3H* ,M,15X,1PE9,3,2X,0PF4
146      1A,2X,F10,1,3X,16HONE WAY REACTION)
147      132 FOPMAT(1H1,37X,46HAEROCHEM RESEARCH LABORATORIES PRINCETON (A,J)
148      1901 FOPMAT(125X,*A FAST COMPUTER PROGRAM FOR NONEQUILIBRIUM ROCKET PLUM
149      1902 IE PREDICTIONS*)
150      133 FOPMAT(1H0,24X,12A6)
151      134 FOPMAT(1H0,22X,19HPRESSURE(INITIAL)=1PE15,7,12H ATMOSPHERES)
152      135 FOPMAT(1H0,22X,20HPRESSURE(CONSTANT)=1PE15,7,12H ATMOSPHERES)
153      136 FOPMAT(123X,24HTEMPERATURE( DEG. KELVIN),3X,1PE15,7,4X,1PE15,7)
154      137 FOPMAT(123X,24HVELOCITY (FEET/SECOND),3X,1PE15,7,4X,1PE15,7)
155      138 FOPMAT(1H0,22X,14HNOZZLE RADIUS=1PE15,7,5H FEET)
156      139 FOPMAT(1,0,22X,23HEMIC NUMBER(CONSTANT)=1PE15,7,5X,25HPRANDTL NUM
157      140 IRR(CONSTANT)=1PF15,7)
158      141 FOPMAT(1H0,54X,3HJET,16X,4HEEDGE)
159      142 FOPMAT(23X,13HMOLE FRACTION,3X,A6,5X,1PE15,7,4X,1PF15,7)
160      143 FOPMAT(1H0,22X,40HMINMAP VISCOSITY MODEL (SUTHERLANDS LAW))
161      144 FOPMAT(1H0,22X,29HCONSTANT VISCOSITY MODEL MU=1PE15,7)
162      145 FOPMAT(1H0,22X,27HFERRI VISCOSITY MODEL K=1PE15,7)
163      146 FOPMAT(1H0,22X,31HTTING-LIBBY VISCOSITY MODEL K=1PF15,7)
164      147 FOPMAT(1H0,22X,14HX INITIAL (FEET)=1PE15,7,12X,14HX FINAL (FEET)=IPE
165      115,7)

```

SUBROUTINE INOUT

CDC 6600 FTN V3.0-P312 OPT=2 08/07/72 12.54.49.

PAGE

4

```

1967 FORMAT(1H0.22X.16HPRINT INCREMENT=1PE15.7.12X.18HMINIMUM STEP SIZE INOUT 167
1=1PE15.7) INOUT 168
9951 FORMAT(1H0.22X.69HTING-LIBBY VISCOSITY MODEL AFTER MIXING REGION I INOUT 169
INTERSECTS X AXIS N=1PE15.7) INOUT 170
RETURN INOUT 171
END INOUT 172

```

170

SUBROUTINE GRATE

```
SUBROUTINE GRATE (ANSWER, Y, X, N)
DIMENSION X(30), Y(50)
SUM = 0.0
INTER = N-1
I1 = 1
I2 = 2
DO 1 I = 1, INTER
SUM = SUM + (X(I2) - X(I1)) * (Y(I2) + Y(I1))
I1 = I1 + 1
I2 = I2 + 1
1 CONTINUE
ANSWER = 0.5 * SUM
RETURN
END
```

CDC 6600 FTN V3.0-P312 OP1=2 08/07/72 12.54.49.

PAGE 1

GRATE 2
GRATE 3
GRATE 4
GRATE 5
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GRATE 10
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GRATE 12
GRATE 13
GRATE 14
GRATE 15

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SUBROUTINE TICK

SUBROUTINE TICK(JJJJ)
CALL SECONDTIME
JJJ=TIME
RETURN
END

CDC 6600 FTU VJ.6-P312 OPT=2

08/07/72 12.54.49.

PAGE

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TICK
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TICK

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5      SUBROUTINE SLOP(X,A,N)
      THIS PROGRAM FINDS THE SOLUTIONS TO A SET OF N SIMULTANEOUS LINEAR
      EQUATIONS BY USING THE GAUSS-GORDAN REDUCTION ALGORITHM WITH THE
      DIAGONAL PIVOT STRATEGY
      DIMENSION A(25,25),X(25)
      DO 9 K=1,N
      IF (ABS(A(K,K)) .GT. 1.E-10) GO TO 5
      WRITE (6,101)
      GO TO 99
10     5 KPI= K+1
      DO 6 J= KPI, N
      A(K,J)= A(K,J)/A(K,K)
      X(K)= X(K)/A(K,K)
      A(K,K)= 1.0
      DO 9 I=1,N
      IF (I.CO.K .OR. A(I,K).EQ.0.) GO TO 9
      DO 8 J=KPI,N
      A(I,J)= A(I,J)- A(I,K)*A(K,J)
      X(I)= X(I)- A(I,K)*X(K)
      A(I,K)=0.
      9 CONTINUE
      99 CONTINUE
101  FORMAT ( * ERROR--- SMALL PIVOT *)
      RETURN
      END
25

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SURROUTINE TKFY

CDC 6600 F1N V3.0-P312 OPT=2 08/07/72 12.54.49.

PAGE 1

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SURROUTINE TKFY(IT,ITB,ITKEY,SOT,HOT,NT)
DIMENSION ITB(30)
NTI=NT-1
DO 10 IT=1,NTI
  DT= ITB(IT+1)-ITB(IT)
  SOT=(1-ITB(IT))/DT
  HOT=(ITB( IT+1)-1) /DT
  IF ((SOT*HOT).GE.0.0) GO TO 11
10 CONTINUE
  WRITE(6,100) T,I
  ITKPY=0
100 FORMAT(1H * * TEMPERATURE OUT OF RANGE *,E14.5,15)
  11 ITKEY=IT
  RETURN
END

```

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TKFY 2
TKFY 3
TKFY 4
TKFY 5
TKFY 6
TKFY 7
TKFY 8
TKFY 9
TKFY 10
TKFY 11
TKFY 12
TKFY 13
TKFY 14
TKFY 15
TKFY 16
TKFY 17

```

SUBROUTINE IIPIN

CDC 6606 FIN V3.0-P317 01-1-2 08/07/77 12.56.49. PAGE 1

SUBROUTINE LIPLN (ITREY,I,ATR,SDI,MOT,AX)
DIMENSION ATR(25,30)
AX= ATR(I,ITREY)*MOT+ ATR(I,ITREY,I)*SDI
RETURN
END

LIPLN 2
LIPLN 3
LIPLN 4
LIPLN 5
LIPLN 6

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APPENDIX B

SAMPLE INPUT DATA SHEET

IBM

FORTRAN Coding Form

A FAST COMPUTER PROGRAM FOR
NONEQUILIBRIUM ROCKET PLUME PREDICTIONS

| CARD | SAMPLE TEST CASE | | | | | | | | | | PARAMETER | | | | | | | | | | |
|--------|-------------------------------|-----|-------|------|------|-----|-------|----|------|------|-----------|------|------|------|-----|------|--|-----|------|-----|--|
| 1 | | | | | | | | | | | | | | | | | | | | | |
| 2 | 13 | 17 | 6 | 19 | 1 | 1 | 0 | 60 | 0 | 22 | | | | | | | | | | | |
| 3 | 9.57 | +03 | | | | | | | | | | | | | | | | | | | |
| 4 | 0.0 | | 10.0 | | 1.0 | | 1.0 | | 1.0 | | | 0.25 | | 1.0 | | 1.0 | | | | | |
| 5 | 1.0 | | -10 | 2.0 | | | | | | | | | | | | | | | | | |
| 6 | 0.1 | | 2000. | | 300. | | 7480. | | 100. | | | | | 600. | | | | | | | |
| 7 | CARD TYPES 7, 8 AND 9 OMITTED | | | | | | | | | | | | | | | | | | | | |
| 8 | | | | | | | | | | | | | | | | | | | | | |
| 9 | | | | | | | | | | | | | | | | | | | | | |
| 10.1 | 3.27 | | -08 | 5.36 | | -03 | 5.04 | | -02 | 5.96 | | -06 | 5.36 | | -07 | 8.14 | | -02 | 2.85 | -01 | |
| 10.12 | 2.35 | | -01 | 1.76 | | -01 | 2.68 | | -03 | 5.16 | | -07 | 1.29 | | -08 | 6.06 | | -05 | 1.19 | -03 | |
| 10.13 | 1.19 | | -04 | 3.40 | | -02 | 1.27 | | -01 | | | | | | | | | | | | |
| 10.2.1 | 0.0 | | | 0.0 | | | 0.0 | | | 0.0 | | 0.0 | | | 0.0 | | | | | 0.0 | |
| 10.2.2 | 0.0 | | | 0.0 | | | 0.0 | | | 0.0 | | 0.0 | | | 0.0 | | | | | 0.0 | |
| 10.2.3 | 2.1 | | -01 | 0.0 | | | 7.9 | | -01 | | | | | | | | | | | | |

IBM

FORTHAN Coding Form

CORBAN CLAIMS

THEMODYNAMIC DATA CARDS IN THE FOLLOWING ORDER: K, H, HCL, KCL, K⁺, H₂, H₂O, CO, CO₂, CL₂, CL, F₂, O, OH, O₂, Al₂O₃, N₂

| Code | Species | 39.1 | 21.31 | Value | Value | Value | Value | Value | Value | Value | Value |
|---------|---------|-------|--------|--------|-------|-------|--------|-------|-------|--------|--------|
| 11.1.1 | K | | | | | | | | | | |
| 11.1.2 | | 4.968 | 42.714 | -0.984 | 200. | 4.968 | 39.751 | 4.968 | 4.968 | 39.751 | -0.488 |
| 11.1.3 | | 4.968 | 38.492 | 0.506 | 600. | 4.968 | 39.272 | 4.968 | 4.968 | 39.272 | 1.500 |
| 11.1.4 | | 4.968 | 40.084 | 2.493 | 1000. | 4.968 | 40.822 | 4.968 | 4.968 | 40.822 | 3.487 |
| 11.1.5 | | 4.968 | 41.481 | 4.481 | 1400. | 4.968 | 42.070 | 4.970 | 4.970 | 42.070 | 5.474 |
| 11.1.6 | | 4.975 | 42.602 | 6.469 | 1800. | 4.975 | 43.084 | 4.988 | 4.988 | 43.084 | 7.465 |
| 11.1.7 | | 5.013 | 43.526 | 8.465 | 2200. | 5.013 | 43.932 | 5.057 | 5.057 | 43.932 | 9.471 |
| 11.1.8 | | 5.122 | 44.310 | 10.489 | 2600. | 5.122 | 44.662 | 5.213 | 5.213 | 44.662 | 11.522 |
| 11.1.9 | | 5.334 | 44.993 | 12.576 | 3000. | 5.334 | 45.305 | 5.489 | 5.489 | 45.305 | 13.658 |
| 11.1.10 | | 5.685 | 45.601 | 14.775 | 3400. | 5.685 | 45.883 | 5.932 | 5.932 | 45.883 | 15.935 |
| 11.1.11 | | 6.242 | 46.153 | 17.152 | 3800. | 6.242 | 46.412 | 6.630 | 6.630 | 46.412 | 18.438 |
| 11.1.12 | | 7.111 | 46.664 | 19.810 | 4200. | 7.111 | 46.908 | 7.701 | 7.701 | 46.908 | 21.289 |

11.2.1 2ND SPECIES (H)

11.2.1 18TH SPECIES (N₂)

11.1.2

IBM

CHEMICAL REACTION CARDS:

| | | | | | |
|----------------|------------|--------------|----------|------------|------------|
| 12.1 KCL | + H | = K | + HCL | 15 3.0E-11 | 4072. |
| 12.2 ϕ | + ϕ | + M | + M | 22 1.0E-29 | 1.0 |
| 12.3 H | + H | + M | + M | 22 1.0E-29 | 1.0 |
| 12.4 ϕ | + H | + M | + M | 22 1.0E-29 | 1.0 |
| 12.5 H | + ϕ H | + M | + M | 22 1.0E-28 | 1.0 |
| 12.6 C ψ | + ϕ | + M | + M | 26 5.0E-29 | 1.0 -4000. |
| 12.7 ϕ H | + ϕ H | + ϕ | + ϕ | 15 1.0E-11 | -1000. |
| 12.8 ϕ H | + H2 | + H2 ϕ | + H | 15 4.0E-11 | -5500. |
| 12.9 ϕ | + H2 | + ϕ H | + H | 15 3.0E-11 | -8200. |
| 12.10 H | + ϕ 2 | + ϕ H | + ϕ | 15 3.0E-10 | -16500. |
| 12.11 C ϕ | + ϕ H | + C ϕ 2 | + H | 15 5.0E-13 | -600. |

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IBM

FORTRAN Coding Form

B-4

FORTRAN STATEMENT

| FORTRAN STATEMENT | OPERATOR | OPERAND | OPERATOR | OPERAND | OPERATOR | OPERAND | OPERATOR | OPERAND | OPERATOR | OPERAND |
|-------------------|----------|---------|----------|---------|----------|---------|----------|---------|----------|---------|
| 1212 H | +HCL | | =CCL | | +H2 | | | 15 | 8.0E-11 | -4622. |
| 1213 HCL | +ΦH | | =H2Φ | | +CCL | | | 15 | 7.2E-12 | -3250. |
| 1214 ΦH | +CCL | | =HCL | | +Φ | | | 15 | 3.0E-11 | -5000. |
| 1215 H | +CCL | +M | =HCL | | +M | | | 22 | 3.0E-29 | |
| 1216 K+ | +E- | +M | =K | | +M | | | 27 | 2.0E-22 | 1.5 |
| 1217 K+ | +CCL- | | =K | | +CCL | | | 14 | 1.0E-08 | 0.5 |
| 1218 CIL | +E- | +M | =CCL- | | +M | | | 21 | 3.0E-30 | |
| 1219 H | +CCL- | | =HCL | | +E- | | | 15 | 1.7E-12 | -6210. |

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APPENDIX C

SAMPLE OUTPUT

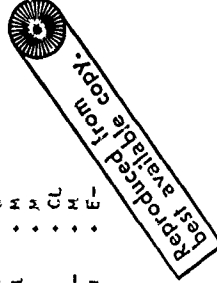
AEROCHEM RESEARCH LABORATORIES PRINCETON N.J.
A FAST COMPUTER PROGRAM FOR NONEQUILIBRIUM ROCKET PLUME PREDICTIONS

SAMPLE TEST CASE (R777?)

PRESSURE(CONSTANT) = 1.0000000F-01 ATMOSPHERES
 NOZZLE RADIUS = 2.5000000F-01 FEET
 LEWIS NUMBER(CONSTANT) = 1.00000000E+00 PRANDTL NUMER(CONSTANT) = 1.0000000F+00
 X INITIAL(FEET) = 0. X FINAL(FEET) = 1.0000000E+01
 PRINT INCREMENT = 1.0000000F+00 MINIMUM STEP SIZE = 1.0000000E-10
 DONALDSON/GRAY VISCOSITY MODEL

| | | | |
|---------------------------|---------------|------|---------------|
| TEMPERATURE(DEG. KELVIN) | 2.0000000E+03 | EDGE | 3.0000000E+02 |
| VISCOITY (FEET/SEC-POISE) | 7.4800000E+03 | | 1.0000000E+02 |
| MOLE FRACTION H | 3.2784627F-0A | | 0. |
| MOLE FRACTION HCL | 5.3647026E-01 | | 0. |
| MOLE FRACTION KCL | 5.0467965E-02 | | 0. |
| MOLE FRACTION K+ | 5.960A140F-0A | | 0. |
| MOLE FRACTION H2 | 5.3647026E-07 | | 0. |
| MOLE FRACTION H2O | 8.1464558E-02 | | 0. |
| MOLE FRACTION CO | 2.8512545E-01 | | 0. |
| MOLE FRACTION CO2 | 2.3544450E-01 | | 0. |
| MOLE FRACTION CL | 1.7683338E-01 | | 0. |
| MOLE FRACTION CL- | 2.6823513F-03 | | 0. |
| MOLE FRACTION E- | 5.1659988F-07 | | 0. |
| MOLE FRACTION OH | 1.2914247F-0A | | 0. |
| MOLE FRACTION OH- | 6.0601159E-05 | | 0. |
| MOLE FRACTION O2 | 1.1921228E-07 | | 0. |
| MOLE FRACTION AL2O3 | 1.1921228E-04 | | 2.1000000E-01 |
| MOLE FRACTION N2 | 3.4075652F-02 | | 0. |
| | 1.2716243E-01 | | 7.9000000E-01 |

| REACTIONS BEING CONSIDERED | | KP=EXP(P/RT)/T**N | | (MOLECULE-ML-SEC UNITS) | |
|----------------------------|---|-------------------|-----|-------------------------|----------|
| KCI | H | K | HCL | A | B |
| 1 | + | = | + | 3.000E-11 | -0.0 |
| 2 | + | = | + | 1.000E-29 | -0.0 |
| 3 | + | = | + | 1.000E-29 | -0.0 |
| 4 | + | = | + | 1.000E-29 | -0.0 |
| 5 | + | = | + | 1.000E-29 | -0.0 |
| 6 | + | = | + | 5.000E-29 | -4000.0 |
| 7 | + | = | + | 1.000E-11 | -1000.0 |
| 8 | + | = | + | 4.000E-11 | -5500.0 |
| 9 | + | = | + | 3.000E-11 | -6200.0 |
| 10 | + | = | + | 3.000E-10 | -16500.0 |
| 11 | + | = | + | 5.000E-13 | -600.0 |
| 12 | + | = | + | 8.400E-11 | -4622.0 |
| 13 | + | = | + | 7.200E-12 | -3250.0 |
| 14 | + | = | + | 3.000E-11 | -5000.0 |
| 15 | + | = | + | 3.000E-29 | -0.0 |
| 16 | + | = | + | 2.000E-22 | -0.0 |
| 17 | + | = | + | 1.000E-08 | -0.0 |
| 18 | + | = | + | 3.000E-30 | -0.0 |
| 19 | + | = | + | 1.700E-12 | -6210.0 |



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SAMPLE TEST CASE (8/7/7?)

| PT | X/R | FFFT | DELTA X FEET | PRESS(ATM) | INNER MIXING ZONE RADIUS/R | MACH NO. | ENTHALPY CAL/GM | VELOCITY FEET/SEC | TEMPERATURE K | DENSITY GW/CC | MACH NO. | MIXING RATE COEFFICIENT | ELECTRON DENSITY (1/ML) | PSI | PT |
|----|--------|--------------|--------------|--------------|----------------------------|--------------|-----------------|-------------------|---------------|---------------|--------------|-------------------------|-------------------------|--------------|----|
| 0. | 0. | 0. | 2.500000F-02 | 1.000000F-01 | 1.019000F+00 | 1.775436E+00 | | | | | | 2.480000F-02 | | | |
| 1 | 0.0000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 0. | 1 |
| 2 | .1000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 1.259332E-02 | 2 |
| 3 | .2000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 2.514665E-02 | 3 |
| 4 | .3000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 3.777997E-02 | 4 |
| 5 | .4000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 5.037330E-02 | 5 |
| 6 | .5000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 6.296662E-02 | 6 |
| 7 | .6000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 7.555994E-02 | 7 |
| 8 | .7000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 8.815327E-02 | 8 |
| 9 | .8000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 1.007466E-01 | 9 |
| 10 | .9000 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+03 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 1.133399E-01 | 10 |
| 11 | 1.0000 | 7.480000F+02 | 2.000000E+03 | 1.748625E-05 | 1.748625E+03 | 2.723236E+00 | -1.239554E+03 | 7.480000F+02 | 2.000000E+03 | 1.748625E-05 | 2.723236E+00 | 4.474016E-03 | 4.746058E+09 | 1.259332E-01 | 11 |
| 12 | 1.3982 | 1.000000F+02 | 3.000000E+02 | 1.172305E-04 | 1.172305E+02 | 8.770271E-02 | 5.116059E-01 | 1.000000F+02 | 3.000000E+02 | 1.172305E-04 | 8.770271E-02 | 2.999450E-02 | 0. | 1.385286E-01 | 12 |
| 13 | 2.2874 | 1.000000F+02 | 3.000000E+02 | 1.172305E-04 | 1.172305E+02 | 8.770271E-02 | 5.116059E-01 | 1.000000F+02 | 3.000000E+02 | 1.172305E-04 | 8.770271E-02 | 2.999450E-02 | 0. | 1.511199E-01 | 13 |

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SAMPLE TEST CASE (U/777)

FEET

Y/R

| PT | Y/R | K | FEET | H | HCl | HCL | FGL | K* | H2 | H2O | PT |
|----|---------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|----|
| 1 | 0.0000 | 3.27844E-08 | 0.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 1 |
| 2 | .10000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 2 |
| 3 | .20000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 3 |
| 4 | .30000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 4 |
| 5 | .40000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 5 |
| 6 | .50000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 6 |
| 7 | .60000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 7 |
| 8 | .70000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 8 |
| 9 | .80000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 9 |
| 10 | .90000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 10 |
| 11 | 1.00000 | 3.27844E-08 | 9.76470E-03 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.06480E-02 | 5.36470E-07 | 8.14646E-02 | 2.85125E-01 | 11 |
| 12 | 1.10000 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 12 |
| 13 | 2.28737 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 13 |

MOLF FRACTIONS

NET RATE OF PRODUCTION (W-00T/RHOEU)

| PT | Y/R | K | FEET | H | HCl | HCL | FGL | K* | H2 | H2O | PT |
|----|---------|-------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|--------------|----|
| 1 | 0.0000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 1 |
| 2 | .10000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 2 |
| 3 | .20000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 3 |
| 4 | .30000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 4 |
| 5 | .40000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 5 |
| 6 | .50000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 6 |
| 7 | .60000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 7 |
| 8 | .70000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 8 |
| 9 | .80000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 9 |
| 10 | .90000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 10 |
| 11 | 1.00000 | 3.69220E-04 | -1.09439E-04 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -3.69223E-06 | -6.69310E-11 | -4.73642E-08 | -1.11832E-03 | 11 |

SAMPLE TEST CASE (8/7/72)

| PT | Y/R | CO | FFET | CO2 | CI | CL | E | OM | PT |
|----|---------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| 1 | 0.0000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 0.06012E-05 | 1.19212E-03 |
| 2 | .10000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 3 | .20000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 4 | .40000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 5 | .60000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 6 | .80000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 7 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 8 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 9 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 10 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 11 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 12 | 1.00000 | 2.35445E-01 | 1.76033E-01 | 1.76033E-01 | 2.48235E-03 | 5.16600E-07 | 1.29142E-0A | 6.06012E-05 | 1.19212E-03 |
| 13 | 2.28737 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |

MOLE FRACTIONS

NET RATE OF PRODUCTION (M-DOT/RHO*U)

| PT | Y/R | CO | CO2 | CI | CL | E | OM | PT |
|----|---------|-------------|--------------|--------------|--------------|--------------|--------------|-------------|
| 1 | 0.0000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 2 | .10000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 3 | .20000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 4 | .40000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 5 | .60000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 6 | .80000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 7 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 8 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 9 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 10 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 11 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 12 | 1.00000 | 1.02762E-04 | -1.02762E-04 | -1.10779E-03 | -3.59762E-12 | -6.33334E-11 | -8.46927E-06 | 1.23469E-03 |
| 13 | 2.28737 | 0. | 0. | 0. | 0. | 0. | 0. | 0. |

SAMPLE TEST CASE (8/7/76)

MOLE FRACTIONS

| PT | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 |
|----|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| WT | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 |
| PC | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 |
| MC | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 |
| MP | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| AP | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| AT | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |

NET RATE OF PRODUCTION (M-DOT/PHO-U)

| PT | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 |
|----|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| WT | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 |
| PC | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 | 1.27162E-01 |
| MC | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 | 3.40757E-02 |
| MP | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| AP | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |
| AT | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 0. |

REACTION RATES (MOLE/ML-SEC)

| WT | Y/H | REACTION 1 PP | RM | REACTION 2 PP | RM | REACTION 3 PP | RM | REACTION 4 PP | RM | REACTION 5 PP | RM | PT |
|----|------------|------------------|------------|------------------|------------|------------------|------------|------------------|------------|------------------|------------|----|
| 1 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 1 |
| 2 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 2 |
| 3 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 3 |
| 4 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 4 |
| 5 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 5 |
| 6 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 6 |
| 7 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 7 |
| 8 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 8 |
| 9 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 9 |
| 10 | 1.0000F-01 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 10 |
| 11 | 1.0000F-00 | 5.9858F-07 | 1.1564E-07 | 1.5003F-12 | 2.1309E-13 | 1.1828E-08 | 8.7195E-10 | 1.3361E-10 | 9.4971E-12 | 2.6288E-08 | 2.9804E-09 | 11 |

REACTION RATES (MOLE/ML-SEC)

| WT | Y/H | REACTION 6 PP | RM | REACTION 7 PP | RM | REACTION 8 PP | RM | REACTION 9 PP | RM | REACTION 10 PP | RM | PT |
|----|------------|------------------|------------|------------------|------------|------------------|------------|------------------|------------|-------------------|------------|----|
| 1 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 1 |
| 2 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 2 |
| 3 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 3 |
| 4 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 4 |
| 5 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 5 |
| 6 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 6 |
| 7 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 7 |
| 8 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 8 |
| 9 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 9 |
| 10 | 1.0000F-01 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 10 |
| 11 | 1.0000F-00 | 1.0711E-08 | 1.1404E-09 | 2.4730F-06 | 3.9452E-06 | 2.1772E-04 | 3.3490E-04 | 4.2064E-06 | 4.0558E-06 | 6.7424E-07 | 3.3818E-07 | 11 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/M | REACTION 11 RM | REACTION 12 RM | REACTION 13 RM | REACTION 14 RM | REACTION 15 RM | PT |
|----|------------|-------------------|-------------------|-------------------|-------------------|-------------------|----|
| 1 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 1 |
| 2 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 2 |
| 3 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 3 |
| 4 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 4 |
| 5 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 5 |
| 6 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 6 |
| 7 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 7 |
| 8 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 8 |
| 9 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 9 |
| 10 | 1.0000F-01 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 10 |
| 11 | 1.0000F-00 | 2.7000E-05 | 4.0459E-05 | 1.6657E-03 | 1.7828E-03 | 4.2780E-05 | 11 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/M | REACTION 16 RM | REACTION 17 RM | REACTION 18 RM | REACTION 19 RM | REACTION 20 RM | PT |
|----|------------|-------------------|-------------------|-------------------|-------------------|-------------------|----|
| 1 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 1 |
| 2 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 2 |
| 3 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 3 |
| 4 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 4 |
| 5 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 5 |
| 6 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 6 |
| 7 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 7 |
| 8 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 8 |
| 9 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 9 |
| 10 | 1.0000F-01 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 10 |
| 11 | 1.0000F-00 | 1.2774E-12 | 6.3496E-12 | 8.5421E-12 | 5.9077E-13 | 2.2084E-10 | 11 |

UNIT ATTENUATION (DB/IN)

CURTAIN ELECTRICAL CONDUCTIVITY (MMH./IN)

PT YRS

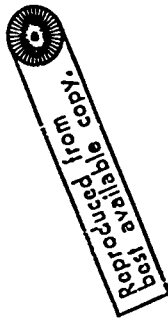
SIGMA FREQ. (MEGACYC) = 0.7500E+09

| | | | | |
|----|-------|------------|------------|------------|
| 1 | 0.000 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 2 | .100 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 3 | .200 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 4 | .300 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 5 | .400 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 6 | .500 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 7 | .600 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 8 | .700 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 9 | .800 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 10 | .900 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 11 | 1.000 | 3.6402E+10 | 1.1017E-02 | 3.6402E-02 |
| 12 | 1.398 | 7.3762E+09 | 0. | 0. |

TRANSMISSION

ATTENUATION (DB) = 2.6139E-01

- 2.5000E-02 0.
- 1.9000E-01 2.5000E-02
- 2.2755E-01 2.1500E-01
- 1.7717E-01 3.6263E-01
- 8.8585E-02 4.2639E-01
- 1.7717E-01 5.3126E-01
- 1.2758E-01 7.0239E-01
- 1.0042E-01 8.3597E-01
- 9.8887E-02 9.3641E-01



SAMPLE TEST CASE (8/7/72)

X# 1.0353036E+00 FEET

X/R 4.141214E+00 PRESS(A)M 1.000000E-01

HALF RADIUS/R 1.094830E+00 INNER MIXING ZONE RADIUS/R 8.188491E-01

MACH NUMBER AT HALF RADIUS 1.509756E+00

MIXING RATE COEFFICIENT 2.440000E-02

| PT | Y/R | VELOCITY FEET/SEC | TEMPERATURE K | DENSITY GM/CC | MACH NO. | ENTHALPY CAL/GM | VISCOSITY LB/FT/SEC | ELECTRON DENSITY (1/ML) | PST | PT |
|----|--------|-------------------|---------------|---------------|--------------|-----------------|---------------------|-------------------------|--------------|----|
| 1 | 0.0000 | 7.440000E+07 | 1.995371E+03 | 1.752709E-05 | 2.726315E+00 | -1.241199E+03 | 6.907386E-03 | 4.619272E+09 | 0. | 1 |
| 2 | 0.0999 | 7.480000E+07 | 1.995371E+03 | 1.752709E-05 | 2.726315E+00 | -1.241199E+03 | 6.907386E-03 | 4.619308E+09 | 1.259332E-02 | 2 |
| 3 | 0.1998 | 7.480000E+07 | 1.995371E+03 | 1.752709E-05 | 2.726315E+00 | -1.241199E+03 | 6.907386E-03 | 4.619308E+09 | 2.518665E-02 | 3 |
| 4 | 0.2997 | 7.480000E+07 | 1.995371E+03 | 1.752709E-05 | 2.726315E+00 | -1.241199E+03 | 6.907386E-03 | 4.619308E+09 | 3.777937E-02 | 4 |
| 5 | 0.3995 | 7.470000E+07 | 1.995371E+03 | 1.752709E-05 | 2.726315E+00 | -1.241197E+03 | 6.907386E-03 | 4.619449E+09 | 5.037330E-02 | 5 |
| 6 | 0.4994 | 7.470000E+07 | 1.995355E+03 | 1.752724E-05 | 2.726206E+00 | -1.241133E+03 | 6.907445E-03 | 4.623511E+09 | 6.266664E-02 | 6 |
| 7 | 0.5993 | 7.475274E+07 | 1.995171E+03 | 1.752892E-05 | 2.726874E+00 | -1.240205E+03 | 6.908108E-03 | 4.684099E+09 | 7.555994E-02 | 7 |
| 8 | 0.6992 | 7.476271E+07 | 1.993991E+03 | 1.753991E-05 | 2.711384E+00 | -1.232162E+03 | 6.912437E-03 | 4.991374E+09 | 8.815327E-02 | 8 |
| 9 | 0.8007 | 7.234264E+07 | 1.989946E+03 | 1.759384E-05 | 2.638795E+00 | -1.188220E+03 | 6.929752E-03 | 7.384200E+09 | 1.007466E-01 | 9 |
| 10 | 0.9073 | 6.510506E+07 | 1.969091E+03 | 1.777888E-05 | 2.381637E+00 | -1.031756E+03 | 7.006222E-03 | 1.317522E+10 | 1.133399E-01 | 10 |
| 11 | 1.0310 | 4.749100E+07 | 1.827804E+03 | 1.910581E-05 | 1.788797E+00 | -6.769682E+02 | 7.582964E-03 | 1.777640E+10 | 1.259332E-01 | 11 |
| 12 | 1.1845 | 2.300324E+07 | 1.828757E+03 | 2.728697E-05 | 1.014664E+00 | -2.773312E+02 | 1.075373E-02 | 8.495933E+09 | 1.395266E-01 | 12 |
| 13 | 1.4189 | 9.051555E+06 | 7.399447E+02 | 6.751716E-05 | 5.149041E-01 | -9.124333E+01 | 1.872640E-02 | 1.356855E+09 | 1.511199E-01 | 13 |
| 14 | 1.7194 | 3.594702E+06 | 4.491325E+02 | 7.829308E-05 | 2.581546E-01 | -2.799443E+01 | 3.085512E-02 | 9.238785E+08 | 1.637132E-01 | 14 |
| 15 | 2.1306 | 1.650484E+06 | 3.378280E+02 | 1.040989E-04 | 1.372803E-01 | -6.838738E+00 | 4.102512E-02 | 3.756923E+08 | 1.763065E-01 | 15 |
| 16 | 2.6833 | 1.124715E+06 | 3.071575E+02 | 1.144977E-04 | 9.766948E-02 | -9.203940E-01 | 4.512328E-02 | 5.995028E+07 | 1.888999E-01 | 16 |
| 17 | 3.4222 | 1.019125E+06 | 3.000000E+02 | 1.168176E-04 | 8.922549E-02 | 2.905605E-01 | 4.603759E-02 | 7.862719E+06 | 2.014932E-01 | 17 |
| 18 | 3.7438 | 1.000000E+06 | 3.000000E+02 | 1.172305E-04 | 8.770271E-02 | 5.116059E-01 | 4.620029E-02 | 0. | 2.140865E-01 | 18 |
| 19 | 4.1521 | 1.000000E+06 | 3.000000E+02 | 1.173055E-04 | 8.770271E-02 | 5.116059E-01 | 4.620029E-02 | 0. | 2.266798E-01 | 19 |

ALB 1.0353076E+00 FFFY

NAME:IF TEST CASE (8/7/77)

PAGE 2

MOLF FRACTIONS

| PT | Y/R | K | M | HCL | KCL | K* | H2 | H2O | PT |
|----|---------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|----|
| 1 | 0.00000 | 1.56850E-07 | 5.08545E-03 | 5.07715E-02 | 5.83414E-06 | 5.39184E-07 | R.18652E-02 | 2.84461E-01 | 1 |
| 2 | 0.04988 | 1.55830E-07 | 5.06555E-03 | 5.07715E-02 | 5.83414E-06 | 5.39184E-07 | 8.18652E-02 | 2.84461E-01 | 2 |
| 3 | 1.19977 | 1.56480E-07 | 5.08545E-03 | 5.07715E-02 | 5.83414E-06 | 5.39184E-07 | 8.18652E-02 | 2.84461E-01 | 3 |
| 4 | 2.09965 | 1.56850E-07 | 5.08545E-03 | 5.07715E-02 | 5.83414E-06 | 5.39184E-07 | 8.18652E-02 | 2.84461E-01 | 4 |
| 5 | 7.99957 | 1.55830E-07 | 5.06555E-03 | 5.07715E-02 | 5.83414E-06 | 5.39184E-07 | 8.18652E-02 | 2.84461E-01 | 5 |
| 6 | 6.49942 | 1.57035E-07 | 5.09133E-03 | 5.07663E-02 | 5.83368E-06 | 5.39173E-07 | 8.18515E-02 | 2.84457E-01 | 6 |
| 7 | 5.49933 | 1.54724E-07 | 5.06823E-03 | 5.06823E-02 | 5.82725E-06 | 5.39012E-07 | 8.16546E-02 | 2.84390E-01 | 7 |
| 8 | 4.99941 | 1.42950E-07 | 5.01020E-03 | 5.00578E-02 | 5.77194E-06 | 5.37857E-07 | 8.00444E-02 | 2.83800E-01 | 8 |
| 9 | 4.00070 | 2.49167E-07 | 8.49315E-03 | 8.47447E-02 | 8.48223E-06 | 5.32834E-07 | 7.29236E-02 | 2.80084E-01 | 9 |
| 10 | 3.00764 | 5.91270E-07 | 1.74647E-02 | 3.65999E-02 | 4.07455E-06 | 5.14889E-07 | 5.03226E-02 | 2.61745E-01 | 10 |
| 11 | 1.03100 | 8.27781E-07 | 1.88406E-02 | 2.90126E-02 | 2.86265E-06 | 4.29543E-07 | 2.80040E-02 | 2.00135E-01 | 11 |
| 12 | 1.19652 | 7.49133E-07 | 1.11811E-02 | 4.73179E-03 | 9.68287E-07 | 1.90289E-07 | 6.19245E-03 | 1.01865E-01 | 12 |
| 13 | 1.41890 | 7.18545E-07 | 7.41545E-03 | 2.63547E-07 | 6.41387E-08 | 6.41387E-08 | 3.72846E-03 | 3.62870E-02 | 13 |
| 14 | 1.71845 | 8.74338E-08 | 8.45438E-04 | 1.17403E-03 | 1.23100E-07 | 1.95991E-08 | 1.65992E-03 | 1.11777E-02 | 14 |
| 15 | 2.11355 | 1.47919E-08 | 1.51974E-04 | 7.71461E-04 | 4.34433E-08 | 4.87975E-09 | 5.34077E-04 | 2.73869E-03 | 15 |
| 16 | 2.48327 | 1.66824E-09 | 1.44231E-05 | 7.98425E-05 | 9.08033E-09 | 9.26440E-10 | 1.23035E-04 | 5.07776E-04 | 16 |
| 17 | 3.28216 | 1.07638E-10 | 1.28541E-06 | 1.28541E-05 | 1.45620E-09 | 1.39690E-10 | 2.06919E-05 | 7.49219E-05 | 17 |
| 18 | 3.76375 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 18 |
| 19 | 4.25210 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 19 |

NET RATE OF PRODUCTION (W-DOT/RHOSHU)

| PT | K | M | HCL | KCL | K* | H2 | H2O | PT |
|----|---------------|--------------|--------------|--------------|--------------|--------------|--------------|----|
| 1 | -6.64882E-11 | -5.32473E-07 | 4.21535E-07 | -2.28450E-11 | 8.93332E-11 | 5.84653E-06 | -5.74394E-06 | 1 |
| 2 | -6.64882E-11 | -5.32473E-07 | 4.21535E-07 | -2.28450E-11 | 8.93332E-11 | 5.84653E-06 | -5.74394E-06 | 2 |
| 3 | -5.64482E-11 | -5.32473E-07 | 4.21535E-07 | -2.28450E-11 | 8.93332E-11 | 5.84653E-06 | -5.74394E-06 | 3 |
| 4 | -6.64482E-11 | -5.32473E-07 | 4.21535E-07 | -2.28450E-11 | 8.93332E-11 | 5.84653E-06 | -5.74394E-06 | 4 |
| 5 | -6.51044E-11 | -5.25848E-07 | 4.17983E-07 | -2.42414E-11 | 8.93498E-11 | 5.83853E-06 | -5.73621E-06 | 5 |
| 6 | -3.43229E-11 | -3.73239E-07 | 3.77805E-07 | -5.14925E-11 | 6.98247E-11 | 5.65207E-06 | -3.67145E-06 | 6 |
| 7 | 2.13294E-10 | 1.39225E-06 | -6.54468E-07 | -3.10310E-10 | 9.70143E-11 | 3.45840E-06 | -1.65711E-05 | 7 |
| 8 | 1.99602E-09 | 1.47767E-05 | -1.13768E-05 | -2.14072E-09 | 1.64700E-10 | -1.37331E-05 | 1.16571E-05 | 8 |
| 9 | 1.74543E-08 | 1.44271E-04 | -9.81153E-05 | -1.41163E-08 | 6.62017E-10 | -1.46223E-04 | 1.22852E-04 | 9 |
| 10 | 4.42172E-08 | 5.04251E-04 | -3.69425E-04 | -4.75418E-08 | 3.37462E-09 | -6.62950E-04 | 4.42510E-04 | 10 |
| 11 | 8.19316E-08 | 7.77689E-04 | -4.37972E-04 | -8.93179E-08 | 7.38658E-09 | -8.44388E-04 | 5.77806E-04 | 11 |
| 12 | -3.45774E-07 | -4.12008E-04 | -2.82496E-04 | 3.43164E-07 | 2.61200E-09 | -5.51770E-04 | 4.59941E-04 | 12 |
| 13 | -1.712601E-04 | 8.85255E-05 | -1.84459E-05 | 1.32608E-06 | -6.69097E-11 | -5.19879E-05 | 3.83775E-05 | 13 |

Reproduced from best available copy.

SAMPLE TEST CASE (8/7/72)

XY 1.035070E+00 FEET

MOLE FRACTIONS

| PT | Y/R | CO | CO2 | CI | CL | E- | O | OH | OT |
|----|---------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|----|
| 1 | 0.0000 | 2.75311E-01 | 1.76973E-01 | 2.77974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 1 |
| 2 | 0.0998 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 2 |
| 3 | 0.1497 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 3 |
| 4 | 0.2485 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 4 |
| 5 | 0.3983 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 5 |
| 6 | 0.4982 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 6 |
| 7 | 0.5982 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 7 |
| 8 | 0.6981 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 8 |
| 9 | 0.7979 | 2.35311E-01 | 1.76973E-01 | 2.37974E-03 | 5.20233E-07 | 1.19973E-08 | 7.89347E-05 | 1.70718E-03 | 9 |
| 10 | 0.8976 | 1.95304E-01 | 1.63158E-01 | 9.62337E-03 | 4.73545E-07 | 3.52964E-08 | 2.74125E-03 | 8.84767E-03 | 10 |
| 11 | 0.9310 | 1.24695E-01 | 1.10421E-01 | 1.75220E-02 | 7.80943E-07 | 4.41914E-08 | 9.70302E-03 | 1.28187E-02 | 11 |
| 12 | 1.1945 | 5.93039E-02 | 6.41834E-02 | 9.78882E-03 | 1.79322E-07 | 1.68830E-08 | 7.76412E-03 | 3.25615E-03 | 12 |
| 13 | 1.4188 | 2.29510E-02 | 2.22697E-02 | 3.15918E-03 | 6.20897E-08 | 1.35957E-09 | 1.08184E-03 | 1.52159E-04 | 13 |
| 14 | 1.7185 | 7.76035E-03 | 6.76917E-03 | 6.97186E-04 | 1.87894E-08 | 5.64541E-10 | 2.70964E-04 | 1.11769E-04 | 14 |
| 15 | 2.1384 | 2.04985E-03 | 1.65776E-03 | 1.06440E-04 | 4.64453E-09 | 1.72677E-10 | 5.03626E-05 | 3.67502E-05 | 15 |
| 16 | 2.6837 | 6.01088E-04 | 7.10788E-04 | 1.18801E-05 | 8.89337E-10 | 2.50529E-11 | 3.95033E-06 | 4.26322E-06 | 16 |
| 17 | 3.2421 | 6.12012E-04 | 6.43519E-05 | 1.01155E-06 | 1.34655E-10 | 3.22056E-12 | 9.24333E-08 | 3.17798E-07 | 17 |
| 18 | 3.76315 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 18 |
| 19 | 4.25210 | 0. | 0. | 0. | 0. | 0. | 0. | 0. | 19 |

NET RATE OF PRODUCTION (W-DOT/RHO*U)

| PT | Y/R | CO | CO2 | CI | CL | E- | O | OH | OT |
|----|--------------|-------------|-------------|--------------|-------------|--------------|--------------|--------------|----|
| 1 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 1 |
| 2 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 2 |
| 3 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 3 |
| 4 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 4 |
| 5 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 5 |
| 6 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 6 |
| 7 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 7 |
| 8 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 8 |
| 9 | -5.43544E-04 | 5.43544E-04 | 5.43544E-04 | -4.21406E-07 | 9.39150E-11 | -4.58176E-12 | -2.46775E-08 | -9.42413E-08 | 9 |
| 10 | -4.49022E-04 | 4.49022E-04 | 4.49022E-04 | 3.44971E-04 | 1.96681E-09 | 1.36381E-09 | 5.23358E-05 | 2.86054E-04 | 10 |
| 11 | -1.22850E-04 | 1.22850E-04 | 1.22850E-04 | 4.78056E-04 | 5.15755E-09 | 2.22902E-09 | 5.11271E-04 | 1.93455E-04 | 11 |
| 12 | -6.26208E-04 | 6.26208E-04 | 6.26208E-04 | 2.42150E-04 | 2.29516E-09 | 3.16833E-10 | 1.10596E-03 | 8.78162E-04 | 12 |
| 13 | -4.42731E-04 | 4.42731E-04 | 4.42731E-04 | 1.75196E-05 | 2.30802E-10 | -2.97712E-10 | -8.95360E-05 | -4.24589E-05 | 13 |

SAMPLE TEST CASE (R/7/72)

1.03540JAE*00 FFFY

MOLF FRACTIONS

| PI | Y/R | OP | AI 203 | NP | MOLF FRACTIONS | PT |
|----|----------|-------------|-------------|-------------|----------------|----|
| 1 | 0.00000 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 1 |
| 2 | 0.0988 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 2 |
| 3 | 1.18409 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 3 |
| 4 | 2.16818 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 4 |
| 5 | 3.15227 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 5 |
| 6 | 4.13636 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 6 |
| 7 | 5.12045 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 7 |
| 8 | 6.10454 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 8 |
| 9 | 7.08863 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 9 |
| 10 | 8.07272 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 10 |
| 11 | 9.05681 | 1.18409F-04 | 3.40762E-02 | 1.27164E-01 | 0.0 | 11 |
| 12 | 1.01100 | 4.72881E-02 | 2.14991E-02 | 7.72252E-01 | 0.0 | 12 |
| 13 | 1.114452 | 1.28105E-01 | 1.02065E-02 | 5.91999E-01 | 0.0 | 13 |
| 14 | 1.21790 | 1.82563E-01 | 3.73759E-03 | 7.17579E-01 | 0.0 | 14 |
| 15 | 1.32135 | 2.01611E-01 | 1.20090E-03 | 7.66679E-01 | 0.0 | 15 |
| 16 | 1.42480 | 2.07954E-01 | 3.06417E-04 | 7.84042E-01 | 0.0 | 16 |
| 17 | 1.52825 | 2.09424E-01 | 4.88366E-05 | 7.88856E-01 | 0.0 | 17 |
| 18 | 1.63170 | 2.09944E-01 | 6.88949E-06 | 7.89827E-01 | 0.0 | 18 |
| 19 | 1.73515 | 2.10000E-01 | 0.0 | 7.90000E-01 | 0.0 | 19 |

NET RATE OF PRODUCTION (W-DOT/RHSCU)

| PI | Y/R | OP | AI 203 | NP | NET RATE OF PRODUCTION (W-DOT/RHSCU) | PT |
|----|-------------|-----|--------|-----|--------------------------------------|----|
| 1 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 1 |
| 2 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 2 |
| 3 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 3 |
| 4 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 4 |
| 5 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 5 |
| 6 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 6 |
| 7 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 7 |
| 8 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 8 |
| 9 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 9 |
| 10 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 10 |
| 11 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 11 |
| 12 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 12 |
| 13 | 1.37115F-0A | 0.0 | 0.0 | 0.0 | 0.0 | 13 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/R | REACTION 1 RP | RM | REACTION 2 RP | RM | REACTION 3 RP | RM | REACTION 4 MP | RM | REACTION 5 RP | RM | PT |
|----|-----|------------------|------------|------------------|------------|------------------|------------|------------------|------------|------------------|------------|----|
| 1 | 0. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 1 |
| 2 | 0. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 2 |
| 3 | 1. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 3 |
| 4 | 2. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 4 |
| 5 | 3. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 5 |
| 6 | 4. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 6 |
| 7 | 5. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 7 |
| 8 | 6. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 8 |
| 9 | 7. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 9 |
| 10 | 8. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 10 |
| 11 | 9. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 11 |
| 12 | 10. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 12 |
| 13 | 11. | 5.5927E-07 | 5.5927E-07 | 2.5846E-12 | 1.9949E-13 | 1.0728E-08 | 8.3019E-10 | 1.6651E-11 | 1.2902E-11 | 3.6013E-08 | 2.7928E-09 | 13 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/R | REACTION 6 RP | RM | REACTION 7 RP | RM | REACTION 8 RP | RM | REACTION 9 RP | RM | REACTION 10 RP | RM | PT |
|----|-----|------------------|------------|------------------|------------|------------------|------------|------------------|------------|-------------------|------------|----|
| 1 | 0. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 1 |
| 2 | 0. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 2 |
| 3 | 1. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 3 |
| 4 | 2. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 4 |
| 5 | 3. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 5 |
| 6 | 4. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 6 |
| 7 | 5. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 7 |
| 8 | 6. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 8 |
| 9 | 7. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 9 |
| 10 | 8. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 10 |
| 11 | 9. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 11 |
| 12 | 10. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 12 |
| 13 | 11. | 1.4040E-08 | 1.0668E-09 | 5.0921E-06 | 5.0966E-06 | 3.1377E-04 | 3.1443E-04 | 5.5050E-06 | 5.5119E-06 | 6.3167E-07 | 6.3346E-07 | 13 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/H | REACTION 11 | REACTION 12 | REACTION 13 | REACTION 14 | REACTION 15 | PT |
|----|-----|-------------|-------------|-------------|-------------|-------------|----|
| | | RP | RP | RP | RP | RP | |
| 1 | 0 | 3.4821F-05 | 1.5916F-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 1 |
| 2 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 2 |
| 3 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 3 |
| 4 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 4 |
| 5 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 5 |
| 6 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 6 |
| 7 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 7 |
| 8 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 8 |
| 9 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 9 |
| 10 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 10 |
| 11 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 11 |
| 12 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 12 |
| 13 | 0 | 3.8059E-05 | 1.5915E-03 | 6.1800E-05 | 7.7607E-06 | 1.5060E-08 | 13 |

REACTION RATES (MOLE/ML-SEC)

| PT | Y/H | REACTION 16 | REACTION 17 | REACTION 18 | REACTION 19 | REACTION 20 | PT |
|----|-----|-------------|-------------|-------------|-------------|-------------|----|
| | | RP | RP | RP | RP | RP | |
| 1 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 1 |
| 2 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 2 |
| 3 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 3 |
| 4 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 4 |
| 5 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 5 |
| 6 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 6 |
| 7 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 7 |
| 8 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 8 |
| 9 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 9 |
| 10 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 10 |
| 11 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 11 |
| 12 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 12 |
| 13 | 0 | 1.2014F-12 | 1.4121F-11 | 7.0894E-12 | 2.1103E-10 | 0. | 13 |

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UNIT ATTENUATION (DB/IN)

ELECTRICAL CONDUCTIVITY (MMHO/IN)

CONDUCTION FREQUENCY (1/SEC)

SIG. FREQ. (MEGACYC) = 0.7500E+02

| PT | Y/W | CONDUCTION FREQUENCY (1/SEC) | ELECTRICAL CONDUCTIVITY (MMHO/IN) | UNIT ATTENUATION (DB/IN) |
|----|-------|------------------------------|-----------------------------------|--------------------------|
| 1 | 0.000 | 7.000E+10 | 1.0241E-02 | 3.3930E-01 |
| 2 | .100 | 7.000E+10 | 1.0241E-02 | 3.3930E-01 |
| 3 | .200 | 7.000E+10 | 1.0241E-02 | 3.3930E-02 |
| 4 | .300 | 7.000E+10 | 1.0241E-02 | 3.3930E-02 |
| 5 | .400 | 7.000E+10 | 1.0241E-02 | 3.3930E-02 |
| 6 | .499 | 7.000E+10 | 1.0251E-02 | 3.3962E-02 |
| 7 | .699 | 7.000E+10 | 1.0399E-02 | 3.4424E-02 |
| 8 | .901 | 7.000E+10 | 1.1588E-02 | 3.8240E-02 |
| 9 | .907 | 7.000E+10 | 1.7334E-02 | 5.6254E-02 |
| 10 | 1.031 | 7.000E+10 | 3.2465E-02 | 9.7411E-02 |
| 11 | 1.145 | 7.000E+10 | 4.9231E-02 | 1.21E-01 |
| 12 | 1.419 | 7.000E+10 | 2.5773E-02 | 5.4470E-02 |
| 13 | 1.719 | 7.000E+10 | 4.6375E-02 | 7.4316E-01 |
| 14 | 2.147 | 7.000E+10 | 4.0595E-02 | 4.3419E-01 |
| 15 | 2.643 | 7.000E+10 | 2.5026E-02 | 1.2279E-02 |
| 16 | 3.242 | 7.000E+10 | 5.2965E-04 | 1.4841E-04 |
| 17 | 3.764 | 7.000E+10 | 7.5163E-05 | 1.4043E-05 |
| 18 | | | 0. | 0. |

TRANSMISSION

ATTENUATION (DB) = 4.5217E-01

A.7792E-02 1.03530E+00
 A.74182E-02 1.11903E+00

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APPENDIX D

COMPARISON BETWEEN MIXED IMPLICIT/EXPLICIT
AND FULLY EXPLICIT FINITE DIFFERENCE SCHEMES

APPENDIX D

Comparisons between rocket exhaust plume calculations obtained using the present program (mixed implicit/explicit scheme) and the original AeroChem program⁶ (explicit scheme) have been made in order to (i) demonstrate that both schemes yield identical results and (ii) determine the difference in computer run times between the two schemes. The case investigated is a typical solid propellant exhaust containing potassium as the dominant alkali metal impurity. (Typical input data for such a propellant are given in Appendix B.) The programs were run on a CDC 6600 computer. Comparisons between centerline and radial distributions, velocity, temperature and species mole fractions computed via the mixed implicit/explicit and explicit schemes are shown in Figs. D1-D4. The notation $k_1/100$ means that the rate coefficients for $K + HCl \rightarrow KCl + H$ (which is very near equilibrium, even at a pressure of 0.1 atm) was arbitrarily reduced by a factor of 100. This was necessary in order to run the original (explicit) AeroChem program⁶ without excessive computer time. Figures D1-D4 show that the two schemes do, in fact, give identical results and we are therefore confident that the new program properly calculates exhaust plume properties.

The principal advantage of the mixed implicit/explicit scheme over the explicit scheme is that stable integration step sizes are much larger. This is clearly demonstrated via the (typical) step size comparison shown in Fig. D5. Thus even though the computational time for each integration step in the present program is about 4 times greater than in the original AeroChem program (primarily because of the matrix inversion subroutine in the present program) the much larger step sizes still give considerable reductions in computer run time.

Table D-I shows a comparison between computer run times for the present and original programs for a typical solid propellant plume at sea level and at 50 kft. For this case, the original AeroChem program cannot be used (in a practical sense) to compute plume properties--primarily because the reaction $K + HCl \rightarrow KCl + H$ is very nearly in equilibrium--resulting in stable integration step sizes of less than about 10^{-8} ft. Thus we record an (essentially) infinite computer run time in Table D-I. However this case can be run using a modified version of the original AeroChem program⁶ which keeps the reaction $K + HCl \rightarrow KCl + H$ identically in equilibrium. Run times are noted to be 30 min and 17 min for the sea level and 50 kft cases, respectively. Using the present program reduces these run times to 2.5 and 2.2 min--a very considerable reduction. If, in addition the program is compiled with the 6600 optimized compiler, the run time then is reduced to 1 min for the 50 kft case.

Additional comparisons (made at AFRPL while demonstrating the present program), between the original and present AeroChem programs for other low altitude plumes also showed reductions in computer run times by factors of from 10 to 30.

TABLE D-1

CDC 6600 COMPUTER RUN TIME, MINUTES10 ft plume; $r_j = 0.25$ ft

| | <u>Sea Level</u> | <u>50 kft</u> |
|--|------------------|---------------|
| Original AeroChem (Explicit) Program ⁶ | ∞ | ∞ |
| Original AeroChem (Explicit-modified to put Program ⁶ K + HCl = KCl + H in equilibrium) | 30 | 17 |
| Present Program (Mixed Implicit/Explicit) | 2.5 | 2.2 |
| Present Program (Mixed Implicit/Explicit using CDC 6600 Optimized Compiler) | | 1.0 |

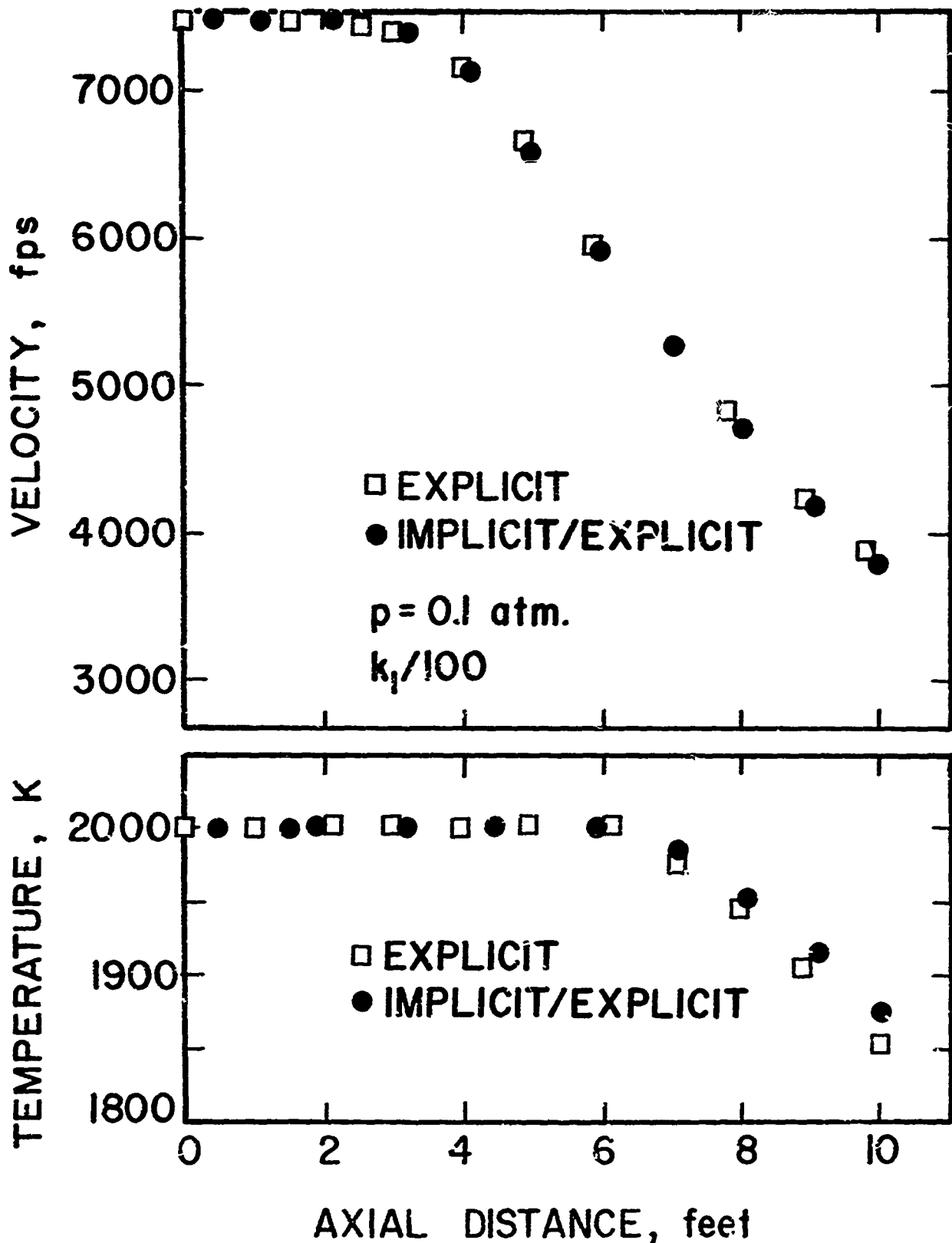


FIG. D1 COMPARISONS BETWEEN CENTERLINE DISTRIBUTIONS OF VELOCITY AND TEMPERATURE COMPUTED FROM MIXED IMPLICIT/EXPLICIT AND EXPLICIT DIFFERENCE TECHNIQUES

$$r_j = 0.25 \text{ ft}$$

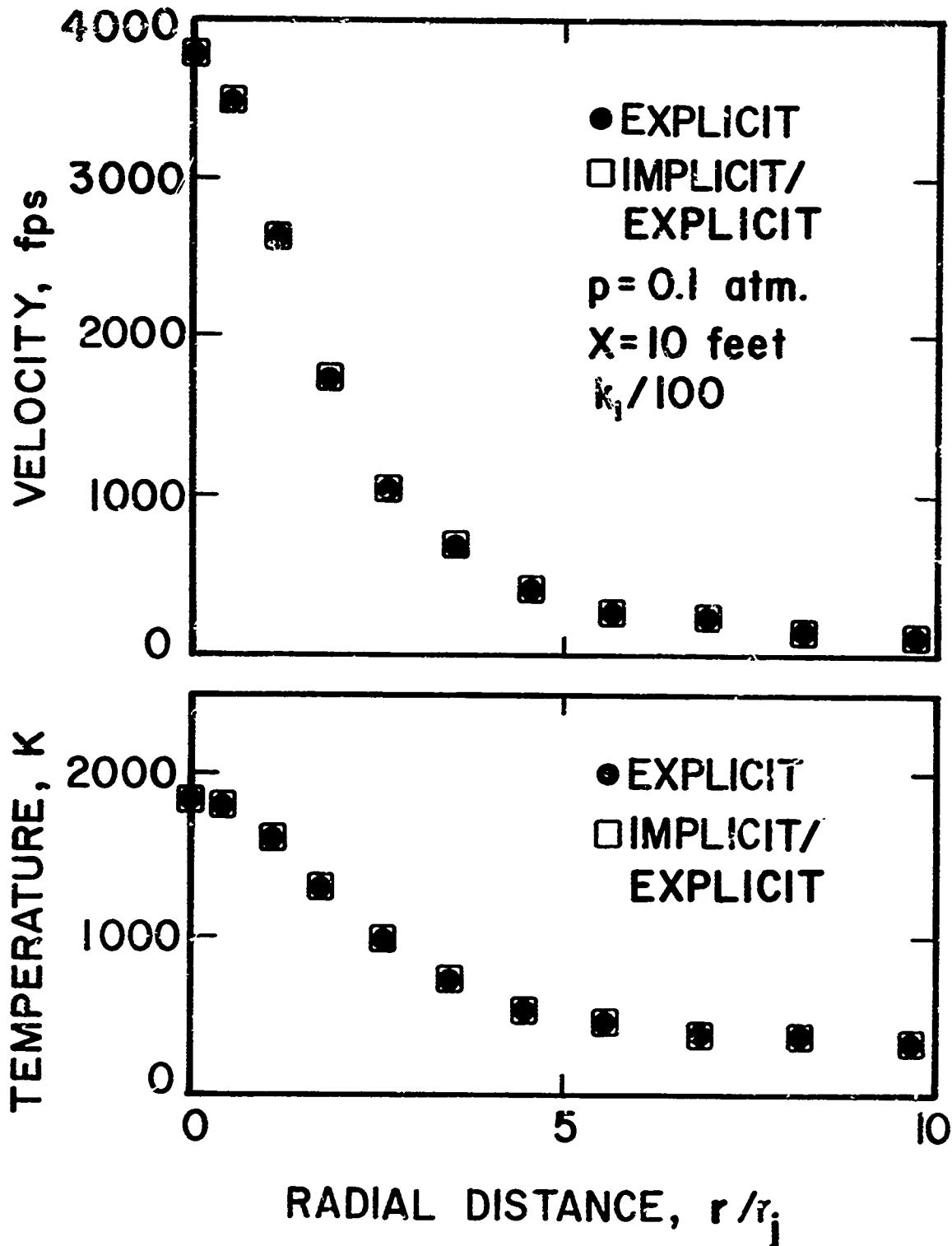


FIG. D2 COMPARISONS BETWEEN RADIAL DISTRIBUTIONS
 OF VELOCITY AND TEMPERATURE COMPUTED
 FROM MIXED IMPLICIT/EXPLICIT AND EXPLICIT
 DIFFERENCE TECHNIQUES

$$r_j = 0.25 \text{ ft}$$

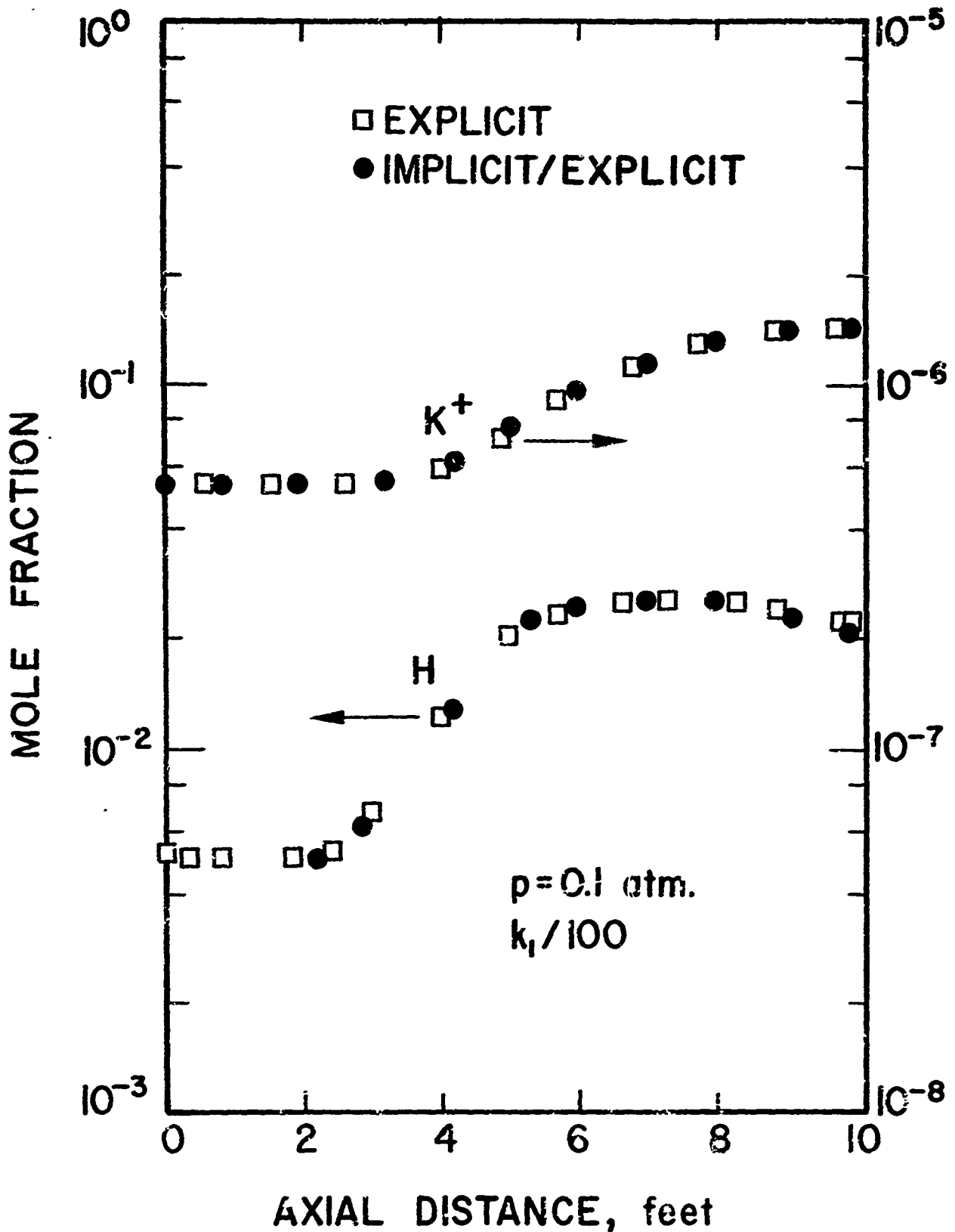


FIG. D3 COMPARISONS BETWEEN CENTERLINE DISTRIBUTIONS OF X_{K^+} AND X_H COMPUTED FROM MIXED IMPLICIT/EXPLICIT AND EXPLICIT DIFFERENCE TECHNIQUES

$$r_j = 0.25 \text{ ft}$$

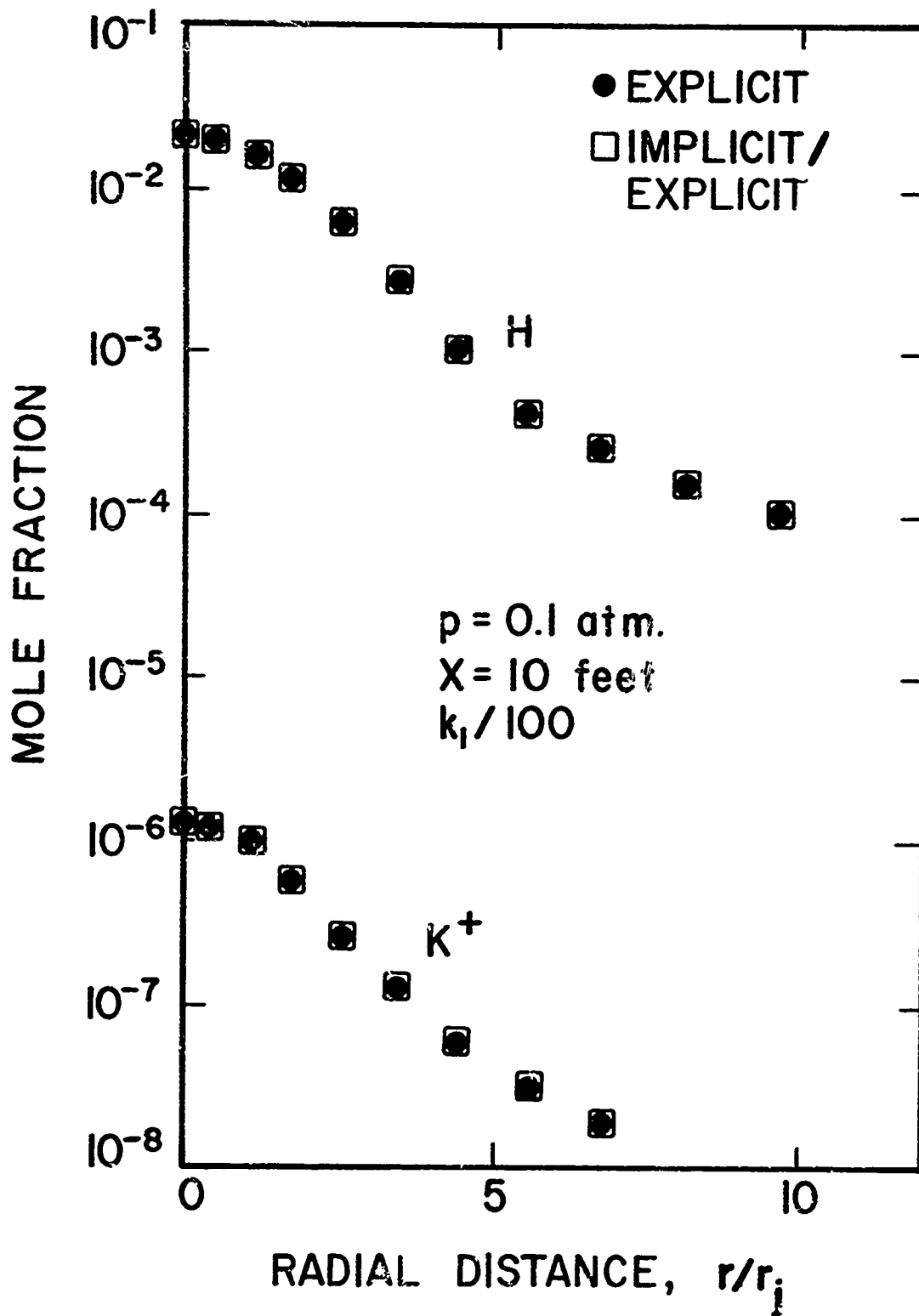


FIG. D4 COMPARISONS BETWEEN RADIAL DISTRIBUTIONS OF X_{K^+} AND X_H COMPUTED FROM MIXED IMPLICIT/EXPLICIT AND EXPLICIT DIFFERENCE TECHNIQUES

$$r_j = 0.25 \text{ ft}$$

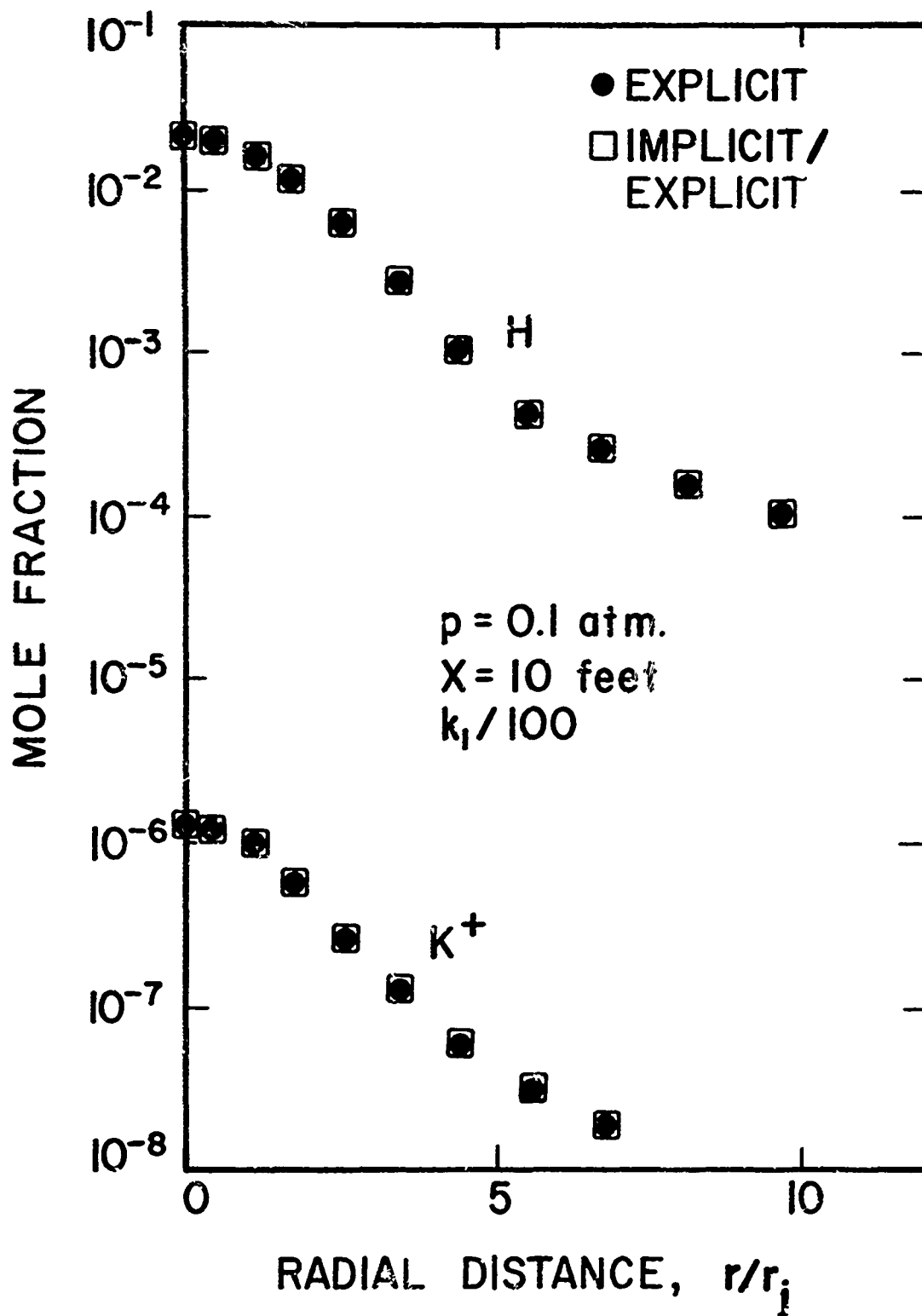


FIG. D4 COMPARISONS BETWEEN RADIAL DISTRIBUTIONS OF X_{K^+} AND X_H COMPUTED FROM MIXED IMPLICIT/EXPLICIT AND EXPLICIT DIFFERENCE TECHNIQUES

$$r_j = 0.25 \text{ ft}$$