

Heat Transfer in a Micropolar Fluid over a Stretching Sheet with Newtonian Heating

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Abstract

This article looks at the steady flow of Micropolar fluid over a stretching surface with heat transfer in the presence of Newtonian heating. The relevant partial differential equations have been reduced to ordinary differential equations. The reduced ordinary differential equation system has been numerically solved by Runge-Kutta-Fehlberg fourth-fifth order method. Influence of different involved parameters on dimensionless velocity, microrotation and temperature is examined. An excellent agreement is found between the present and previous limiting results.

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Introduction

Understanding the flow of non-Newtonian fluids is a problem of great interest of researchers and practical importance. There are several natural and industrial applications of such fluids, for instance volcanic lava, molten polymers, drilling mud, oils, certain paints, poly crystal melts, fluid suspensions, cosmetic and food products and many others. The flow dynamics of non-Newtonian fluids can be described by non-linear relationships between the shear stress and shear rate. Further these fluids have shear dependent viscosity. In literature there exist many mathematical models with different constitutive equations involving different set of empirical parameters. The micropolar fluid model is adequate for exocitic lubricants, animal blood, liquid crystals with rigid molecules, certain biological fluids and colloidal or suspensions solutions. The micromotion of fluid elements, spin inertia and the effects of the couple stresses are very important in micropolar fluids [1,2]. The fluid motion of the micropolar fluid is characterized by the concentration laws of mass, momentum and constitutive relationships describing the effect of couple stress, spin-inertia and micromotion. Hence the flow equation of micropolar fluid involves a micro-rotation vector in addition to classical velocity vector. In micropolar fluids, rigid particles in a small volume element can rotate about the centroid of the volume element. The micropolar fluids in fact can predict behavior at microscale and rotation is independently explained by a micro-rotation vector. More interesting aspects of the theory and application of micropolar fluids can be found in the books of Eringen [3] and Lukazewicz [4] and in some studies of Peddieson and McNitt [5] Willson [6] Siddheshwar and Pranesh [7,8], Siddheshwar and Manjunath [9].

During the past few decades, several researchers have concentrated on the boundary layer flows over a continuously stretching surface. This is because of their in several processes including

thermal and moisture treatments of materials in metallurgy, in the manufacture of glass sheets, in textile industries in polymer processing of chemical engineering plants. Further the stretching flow with heat transfer is quite important in polymer extrusion, cable coating etc. The boundary layer flow of a viscous fluid over a stretching sheet was initially studied by Crane [10], then followed by many investigators for the effect of heat transfer, rotation, MHD, suction/injection, non-Newtonian fluids, chemical reaction etc. It is well known that in many industrial processes, heat transfer is an integral part of the flow mechanism. Now there is an abundant literature available on the flow induced by a stretching sheet with heat transfer [11–20]. Heat transfer characteristics are dependent on the thermal boundary conditions. In general, there are four common heating processes representing the wall-to-ambient temperature distribution, prescribed surface heat flux distribution, and conjugate conditions, where heat transfer through a bounding surface of finite thickness and finite heat capacity is specified. The interface temperature is not known a priori but depends on the intrinsic properties of the system, namely, the thermal conductivities of the fluid and solid. In Newtonian heating, the rate of heat transfer from the bounding surface with a finite heating capacity is proportional to the local temperature surface which is usually termed as conjugate convective flow (see Merkin [21], Lesnic et al. [22], Chaudhary and Jain [23], Salleh et al. [24], Makinde [25]). Salleh et al. [24] numerically investigated the boundary layer flow of viscous fluid over a stretched surface in the regime of Newtonian heating. Numerical solution of the differential system is obtained by Keller box method. Desseaux and Kelson [26] investigated the flow of a micropolar fluid over a stretching sheet. In another attempt, Kelson and Desseaux [27] have investigated the effects of surface conditions on the flow of a micropolar fluid over a stretching sheet. The presented the closed form solution using the perturbation method and made a comparison between the analytical solution

with numerical solution obtained by shooting method with fourth-order-Runge-Kutta algorithm. Bhargava et al. [28] studied mixed convection flow of a Micropolar fluid over a porous stretching sheet by implementing finite element method. The stagnation point flow of a micropolar fluid over a stretching surface has been discussed by Nazar et al. [29]. The steady MHD mixed convection flow towards a vertical stretching surface immersed in an incompressible micropolar fluid was investigated by Ishak et al. [30].

To the best of authors' knowledge, the flow of micropolar fluid over a stretching sheet with heat transfer in the presence of Newtonian heating has not been addressed so far. The resulting problems are solved numerically and solutions obtained are compared with the existing results. It is found that the present results are in a very good agreement. Variations of several pertinent physical parameters are also analyzed in detail by plotting graphs.

Basic Equations

We consider the steady boundary layer flow of an incompressible Micropolar fluid induced by a stretching surface. The sheet is stretched with a velocity $u_w(x) = cx$ (where c is a real number). The heat transfer in the presence of Newtonian heating is considered. The governing equations of the boundary layer flow in the present study are

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \left(v + \frac{\kappa}{\rho} \right) \frac{\partial^2 u}{\partial y^2} + \frac{\kappa}{\rho} \frac{\partial N}{\partial y}, \quad (2)$$

$$u \frac{\partial N}{\partial x} + v \frac{\partial N}{\partial y} = \frac{\gamma^*}{\rho j} \frac{\partial^2 N}{\partial y^2} - \frac{\kappa}{\rho j} \left(2N + \frac{\partial u}{\partial y} \right), \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2}, \quad (4)$$

where u and v are the velocity components parallel to the x - and y -axes, respectively, ρ the fluid density, ν the kinematic viscosity, T is temperature, N the microrotation or angular velocity, c_p the specific heat, k the thermal conductivity of the fluid, $j = (\nu/c)$ is microinertia per unit mass, $\gamma^* = (\mu + \kappa/2)j$ and κ are the spin gradient viscosity and vortex viscosity, respectively. Here $\kappa = 0$ corresponds to situation of viscous fluid and the boundary parameter n varies in the range $0 \leq n \leq 1$. Here $n = 0$ corresponds to the situation when microelements at the stretching sheet are unable to rotate and denotes weak concentrations of the microelements at sheet. The case $n = 1/2$ corresponds to the vanishing of anti-symmetric part of the stress tensor and it shows weak concentration of microelements and the case $n = 1$ is for turbulent boundary layer flows.

The boundary conditions of the present problem are [24]

$$u = u_w(x) = cx, v = 0, N = -n \frac{\partial u}{\partial y}, \frac{\partial T}{\partial y} = h_s T \quad (\text{NH}) \quad \text{at } y = 0,$$

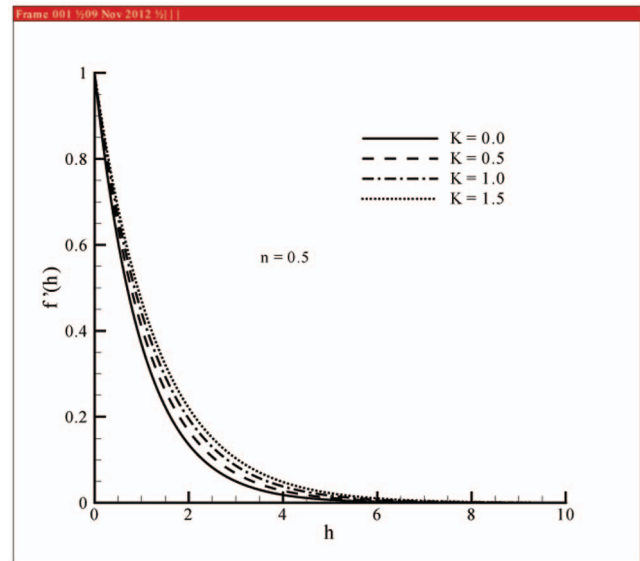


Figure 1. Influence of K on velocity profile $f'(\eta)$ when $n=0.5$.
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$$u = 0, N \rightarrow 0, T = T_\infty \quad \text{as } y \rightarrow \infty. \quad (5)$$

Here h_s is heat transfer coefficient and T_∞ is the ambient temperature. In terms of similarity variables, we write

$$u = cx f'(\eta), v = -\sqrt{cx} f(\eta), N = (c/\nu)^{1/2} cx g(\eta), \eta = y \sqrt{\frac{c}{\nu}},$$

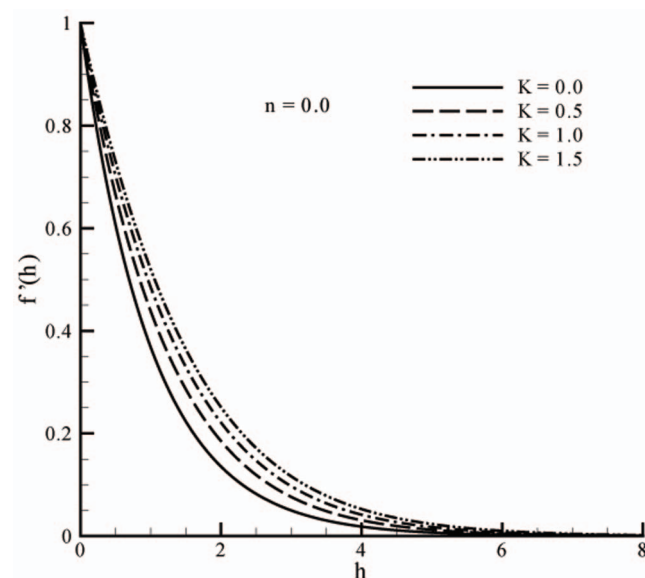


Figure 2. Influence of K on velocity profile $f'(\eta)$ when $n=0.0$.
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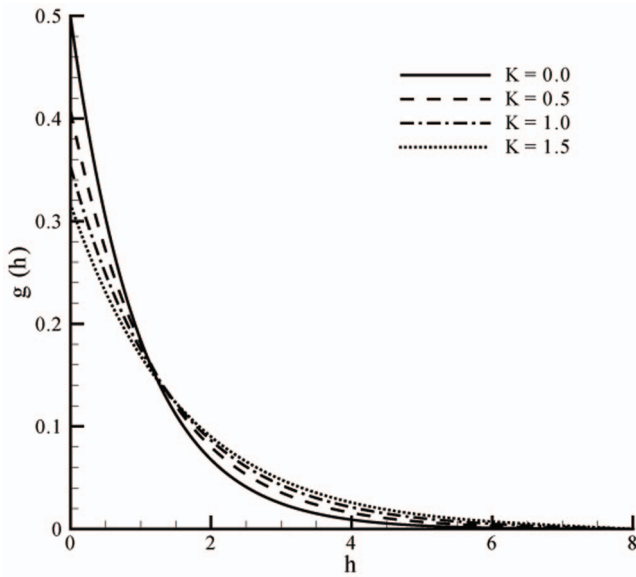


Figure 3. Influence of K on microrotation profile $g(\eta)$ when $n=0.5$.
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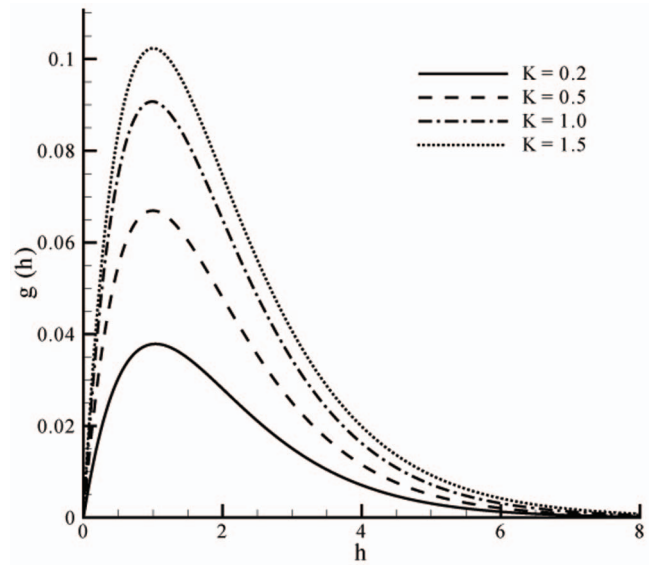


Figure 4. Influence of K on microrotation profile $g(\eta)$ when $n=0.0$.
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$$\theta(\eta) = \frac{T - T_\infty}{T_\infty} (\text{NH}), \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty} (\text{CWT}), \quad (6)$$

$$\theta(\eta) = \left(\frac{k}{q_w}\right) (T - T_\infty) \sqrt{\frac{c}{v}} (\text{CHF}).$$

Introducing above Eqs. (6) into Eqs. (1)–(5) one has

$$(1 + K)f''' + ff'' - (f')^2 + Kg' = 0, \quad (7)$$

$$\left(1 + \frac{K}{2}\right)g'' + fg' - f'g - 2Kg - Kf'' = 0, \quad (8)$$

$$\theta'' + \text{Pr}f\theta' = 0, \quad (9)$$

$$f(0) = 0, f'(0) = 1, f'(\infty) = 0, g(0) = -nf''(0), g(\infty) = 0 \quad (10)$$

$$\theta'(\eta) = -\gamma[1 + \theta(\eta)] (\text{NH}) \text{ at } \eta = 0 \quad \theta = 0 \text{ at } \eta \rightarrow \infty,$$

$$\theta(\eta) = 1 (\text{CWT}) \text{ at } \eta = 0 \quad \theta(\eta) = 0 \text{ as } \eta \rightarrow \infty,$$

$$\theta'(\eta) = -1 (\text{CHF}) \text{ at } \eta = 0 \quad \theta(\eta) = 0 \text{ as } \eta \rightarrow \infty, \quad (11)$$

where Pr is the Prandtl number, γ is the conjugate parameter for Newtonian heating and micropolar parameter K . These quantities are given by

$$\text{Pr} = \frac{\mu c_p}{k}, \quad \gamma = h_s \sqrt{\frac{v}{c}}, K = \frac{\kappa}{\mu} \quad (12)$$

The skin friction coefficient C_f and local Nusselt number Nu_x are

$$C_{fx} = \frac{\tau_w}{\rho u_w^2}, \quad Nu_x = \frac{xq_w}{(T_w - T_\infty)}, \quad (13)$$

in which the wall skin friction τ_w and the heat transfer q_w from the plate can be expressed as follows:

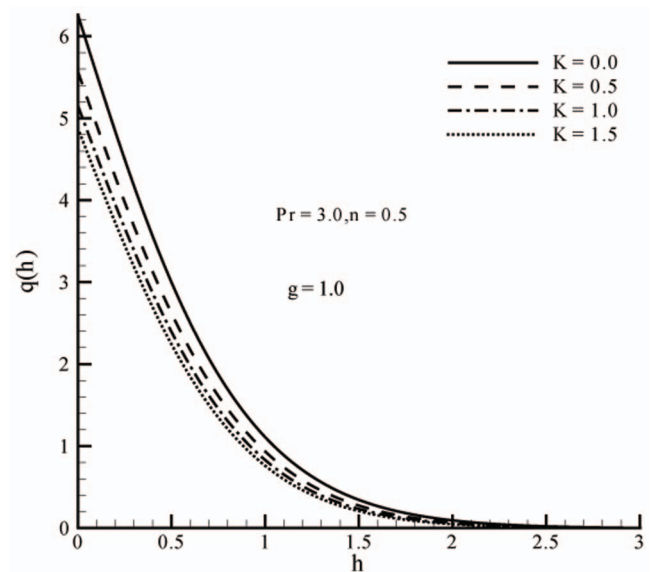


Figure 5. Influence of K on temperature profile $\theta(\eta)$ when $n=0.5$.
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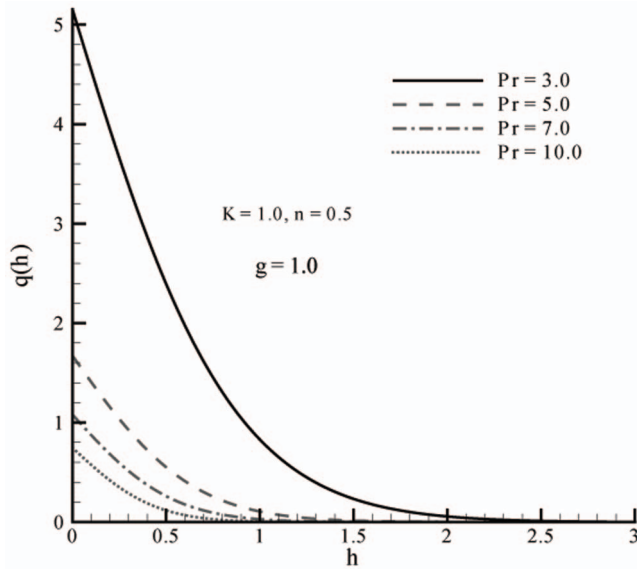


Figure 6. Influence of Pr on temperature profile $\theta(\eta)$ when $n=0.5$.
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$$\tau_w = \left[(\mu + \kappa) \frac{\partial u}{\partial y} + \kappa N \right]_{y=0},$$

$$q_w = -\alpha \left(\frac{\partial T}{\partial y} \right)_{y=0}. \quad (14)$$

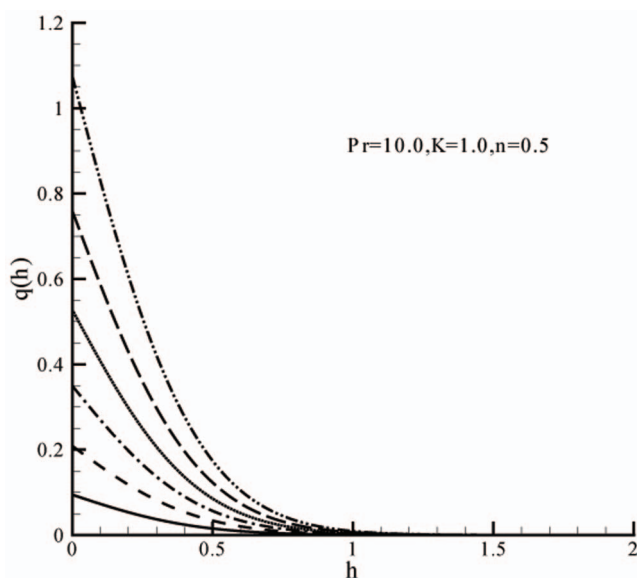


Figure 7. Influence of γ on temperature profile $\theta(\eta)$ when $n=0.5$.
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Table 1. Comparison of $(Re_x)^{1/2} Nu_x$ for different values of Pr when $K=0$ for CHF case.

Pr	$\mathcal{A}(0)$ (CHF)	
	[24]	Present
0.72	2.15902	2.15916
1	1.71816	1.71828 1.71816
3	0.85819	0.85817
5	0.63773	0.63770
7	0.52759	0.52755
10	0.43327	0.43322
100	0.12877	0.12851

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Now using Eqs. (6) and (14) into Eq. (13) we have

$$Re_x^{1/2} C_{fx} = [1 + (1-n)K] f''(0),$$

$$Nu/Re_x^{1/2} = \gamma \left[1 + \frac{1}{\theta(0)} \right] \text{(For NH)},$$

$$Nu/Re_x^{1/2} = -\theta'(0) \text{(For CWT)},$$

$$Nu/Re_x^{1/2} = \frac{1}{\theta(0)} \text{(For CWT)}. \quad (15)$$

where $Re_x = (cx^2/\nu)$ is the local Reynolds number.

Results and Discussion

This section the effects of different parameters on the velocity, microrotation and temperature profiles (Fig. 1, 2, 3, 4, 5, and 6). Skin friction coefficient and the local Nusselt number are also Computed (see Tables 1, 2, 3, and 4). To authenticate our numerical solution a comparison is given in Tables 1, 2, 3, and 4 with already existing results in literature and both solutions are found in good harmony. The results for viscous fluid can be

Table 2. Comparison of $(Re_x)^{1/2} Nu_x$ for different values of Pr when $K=0$ for CWT case.

Pr	$-\theta(0)$ (CWT)	
	[24]	Present
0.72	0.46317	0.46360
1	0.58202	0.58198
3	1.16525	1.16522
5	1.56805	1.56806
7	1.89540	1.89548
10	2.30800	2.30821
100	7.76565	7.76249

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Table 3. Comparison of $\theta(0)$ and $-\theta'(0)$ for different values of Pr when $K=0$ and $\gamma=1$ for NH case.

Pr	$\theta(0)$ (NH)		$-\theta'(0)$ (NH)	
	[24]	Present	[24]	Present
3	6.02577	6.05168	7.02577	7.05168
5	1.76594	1.76039	2.76594	2.76039
7	1.13511	1.11682	2.13511	2.11682
10	0.76531	0.76452	1.76531	1.76452
100	0.16115	0.14781	1.16115	1.14780

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obtained when $K=0$. Figs. 1 and 2 represent the velocity profiles for various values of vortex viscosity parameter K when $n=0.5$ and $n=0.0$ respectively. It is seen that results here are similar in both cases but change in Fig. 1 is slightly smaller when compared with Fig. 2. From Figs. 3 and 4 we can also observed that the microrotation profile for $n=0$ is different than $n=0.5$. Fig. 5 displays the effects of vortex viscosity parameter K on temperature profiles θ . It is obvious that the increasing values of K decreases temperature θ . Fig. 6 depicts the effects of conjugate parameter γ for Newtonian heating. For $\gamma=0$, an insulated wall is present and constant surface temperature can be recovered when $\gamma \rightarrow \infty$. It is found that temperature increases with an increase in γ . It is also noticed that the thickness of thermal boundary layer increases with an increase in γ . Further Eq. (9) has no meaningful solution for a very small Prandtl number, i.e. $\text{Pr} (< 1)$. This is obvious in the sense that for $\text{Pr} (< 1)$ Eq. (9) reduces to $\theta''(\eta)=0$ which has the solution $\theta(\eta)=A\eta+B$ (where A and B are the constants). The boundary conditions are not satisfied by this θ . (see [24]). Fig. 7 examine the effects of Prandtl number on the temperature. An increase in Prandtl number Pr decrease the temperature θ . Note that $\text{Pr} < 1$ corresponds to the flows for which momentum diffusivity is less than the thermal diffusivity. An increase in the weaker thermal diffusivity therefore results in a thinner thermal boundary layer. The solution for Newtonian fluid ($K=0$) reduces to that derived by Salleh et al. [24]. To authenticate our present numerical solution by Runge-Kutta-Fehlberg fourth-fifth order method with the exact solution and numerical solution obtained by Keller-box method a comparison is given in Tables 1, 2, 3, and 4 with already existing results in [24]. All the solutions are found in good harmony. In Table 1, values of local Nusselt number are compared with [24] for the case of constant wall temperature (CWT). From this table we observed that the results obtained by Runge-Kutta-Fehlberg fourth-fifth order method are very closed to exact solution as compared to Keller-box method. From Table 2, it is found that the values of local Nusselt number are

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Table 4. Values of Skin-friction coefficient $(Re_x)^{1/2}C_f$ for different values of K and n .

K\n	0.0		0.5	
	[24]	Present	[24]	Present
0.0	-1.000000	-1.000000	-1.000000	-1.000000
1.0	-1.367872	-1.367872	-1.224741	-1.224741
2.0	-1.621225	-1.621225	-1.414218	-1.414218
4.0	-2.004133	-2.004133	-1.732052	-1.732052

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comparable with the results obtained by [24]. Table 3, presents the $\theta(0)$ and $-\theta'(0)$ for various values of Pr when $\gamma=1$. On comparison with Tables 1 and 2 for the cases of CHF and CWT, the trend for NH case is found similar to the CHF case but different from the CWT case. It is also observed that for Newtonian case both $\theta(0)$ and $-\theta'(0)$ decreases as Pr increases. From Table 4 it is noticed that the magnitude of skin friction coefficient increases for large values of K .

Conclusions

The present study describes the boundary layer flow of Micropolar fluid with Newtonian heating. The main observations of this study are:

- Velocity and momentum boundary layer thickness are increasing functions of vortex viscosity parameter K .
- Microrotation profile has a parabolic distribution when $n=0$.
- The effect of vortex viscosity parameter K on velocity and temperature are quite opposite.
- Temperature and thermal boundary layer thickness are decreasing functions of vortex viscosity parameter K .
- An increase in the value of Prandtl number Pr reduces the temperature and thermal boundary layer thickness.
- The present results in a limiting case ($K=0$) are found in excellent agreement with those of Salleh et al. [24].
- An appreciable increase in the magnitude of $\theta(0)$ is shown for large values of Pr and γ .
- The temperature profiles are also increased by increasing γ .

Author Contributions

Conceived and designed the experiments: MQ IK SS. Performed the experiments: MQ IK SS. Analyzed the data: MQ IK SS. Contributed reagents/materials/analysis tools: MQ IK SS. Wrote the paper: MQ IK SS.

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