**Research Article** 

# Improved biosurfactant production from *Aspergillus niger* through chemical mutagenesis: characterization and RSM optimization



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#### Abstract

Biosurfactants are surface-active natural polymers produced within several microorganisms and are secreted outside the cellular environment. They are the focus of modern researches due to their eco-friendly nature and high production capability using low-cost agro-industrial wastes. In this research, we have evaluated *Aspergillus niger (A. niger)* for its biosurfactant production potential during solid state fermentation of banana stalks powder. The native strain of *A. niger* produced 2.3 g/L of biosurfactant with 49.74 cm<sup>2</sup> oil displacement, 57% emulsification index and an emulsification activity of 1.024 ( $OD_{540}$ ). Sequential mutagenesis was induced in the native strain of *A. niger* by exposing the strain with different concentrations of ethidium bromide (EtBr), for different time periods. Significantly higher amount of biosurfactant (3.3 g/L) was obtained from the mutant strain *A. niger* M2 exposed to 50 µg/10 mL of EtBr for 60 min. The screening tests revealed the improvement in oil displacement (59.81 cm<sup>2</sup>), emulsification index (62.3%) and emulsification activity ( $OD_{540}$ , 1.262) of biosurfactant. FTIR analysis confirmed the presence of amine, amide, fatty acids and triglycerides functional groups. The maximum biosurfactant synthesizing mutant (*A. niger* M2) was further optimized using RSM under CCD. After optimization, the highest biosurfactant (5.50 g/L) was obtained at 35 °C temperature, 7 pH, 5.75 g substrate concentration and 168 h of overall incubation period. In conclusion, the cost-effective production of biosurfactant, along with novel structural and multifunctional characteristics, this study may be useful for different industrial and biotechnological applications.

**Keywords** Biosurfactant · Aspergillus niger · Mutagenesis · Structural properties · Statistical optimization · Characterization

# **1** Introduction

Surfactants are surface-active chemical substances which have gained high importance in fluid mechanics because of their ability to reduce surface tension of liquids. Most of these surface-active compounds are synthesized chemically, which are causing serious toxicological and environmental problems. Biosurfactants are biopolymers, produced by several microorganisms (bacteria and fungi), which possess hydrophobic and hydrophilic moieties. They provide the best alternative to synthetic surfactants in term of low toxicity, high biodegradability, environmentally friendly nature, and the production capability using low-cost agro-industrial raw materials "green technology" [1]. Biosurfactants comprise a large group of chemical compounds e.g. glycolipids, lipopeptides, phospholipids, lipoproteins and lipid-polysaccharide complexes [2]. They present various applications as emulsifiers, conditioners, cosmetics and food industries [3, 4].

Biosurfactants have been reported to possess excellent biomedical and therapeutic properties [5–8] and also found to be effective to tackle environmental pollution

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through bioremediation [4, 9]. They are important in food digestion and respiratory action, plant pathogenicity, paints, beverages, cosmetics and cement industries. Moreover, biosurfactants can be produced from renewable resources and commonly effective in extreme environmental conditions. Biosurfactants also have applications in laundry formulations, pesticides and herbicides, agriculture, textile, household cleaning products, detergents, petroleum and paper industries, food processing, and pharmaceutical industries. They are also important in enzyme biotechnology because of their regulatory effects and bio-stimulatory effects [10].

Surfactant display properties like foaming, emulsification, detergency and dispersion [11–13]. Microorganisms have ability to produce different kinds of surfactants, from these, high molecular weight polymers are highly efficient emulsifiers [14, 15], while low molecular weight polymers efficiently reduce interfacial and surface tension of liquids [16]. Biosurfactants can bear extreme environmental conditions e.g., wide range of pH, high salinity and temperature [17]. In previous decade, much attention has been devoted towards biosurfactants because of their exceptional functional properties. These properties allow a possible replacement of chemically synthesized surfactants for a number of industrial and biotechnological operations [18].

The identification and optimization of fermentation parameters that influence the surfactant yield represent the major points for the development of cost-effective procedures [19]. There are several different factors controlling the microbial biosurfactant production during fermentation which are needed to be maintained within a specific range. It will allow maximum microbial multiplication, which ultimately leads to higher biosurfactant production. In this regard, several physical and nutritional parameters are needed to be optimized for enhance biosurfactant yield. The yield of biosurfactant highly depends upon the availability of carbon and nitrogen sources and other limiting nutrients [20]. Factors influencing biosurfactant production have extensively been investigated particularly for *Pseudomonas* spp. [21, 22], *Candida* spp. [23–25], Rhodococcus spp. [26, 27] There is a dirt of information related to biosurfactant production from bacterial spp. and the optimization of several nutritional and physical parameters influencing the overall yield [28–30].

Microbial biosurfactant production can only be maximized if fermentation parameters are maintained at the optimal growth conditions of microbe. For this purpose, one of the most appropriate approach could be response surface optimization. RSM is a combination of statistical and mathematical tool that is frequently being used in fermentation biotechnology for optimization of fermentation parameters [31–33]. RSM is a statistical design experimental process in which several factors are varied simultaneously. In fact, the relationship between the independent variables and the response variable is usually unknown in an experiment. Therefore, the initial step is to approximate the response variable through analyzing the independent variables.

This study was designed to investigate *A. niger* for its ability to synthesize biosurfactant. The native fungal strain was mutated using different concentrations of EtBr for different time periods. The lyophilized biosurfactant from both native and mutant strain was structurally characterized using FT-IR spectroscopy. The maximum biosurfactant producer mutant strain (*A. niger* M2) was further optimized using RSM under CCD. An insight of primary characteristics of fungal biosurfactant have also been provided in this article.

# 2 Materials and methods

# 2.1 Materials

Banana stalks were obtained from Botanical Garden of University of Agriculture, Faisalabad (UAF), Pakistan. After pretreatment, stalks were chopped and placed in the incubator (LabTech LDO-150 N) at 50 °C for 48 h. The dried substrate was ground into fine powder and stored in an airtight jar at 25 °C temperature. All other chemicals/materials used in this study were obtained from distributors of international companies (Merck KGaA, USA and Sigma Aldrich, Germany).

# 2.2 Fungal strain

Purified culture of a black rot fungus (*A. niger*) was collected from Industrial Biotechnology Laboratory of UAF, Pakistan. Culture was streaked on a freshly prepared PDA slants of pH 6.5 and incubated at 35 °C temperature for 6–8 days. Fungal spore suspension was prepared by transferring the culture to Vogel's minimal media [34]. Media was added with glucose (2%) as carbon source and placed in shaking incubator at 160 *rev*/min and 37 °C temperature.

# 2.3 Chemical mutagenesis

Ethidium bromide (EtBr) was used for the induction of mutation in *A. niger*. For this purpose, mutagen stock solution was prepared by the addition of EtBr 500  $\mu$ g/10 mL of distilled water. Solutions of different concentrations i.e. 50, 100, 150 and 200  $\mu$ g/10 mL were prepared from EtBr stock. Serial dilutions of vegetative cells of fungal inoculum were formed and pellets were suspended in EtBr solution for different time periods of 30, 60 and 90 min. The

fungal suspension was centrifuged, and the pellets were washed thrice with saline solution [composition (g/L) of NaCl (8.9) and yeast extract (1.0) in ddH<sub>2</sub>O]. Agar media containing triton X-100 was used for the development of genetically modified colonies [35]. The final screening of mutant colonies was achieved by using 2-deoxy-D-glucose as metabolic inhibitor that was used for the isolation of mutant strains [36]. The inocula were prepared from native as well as selected mutant strain and preserved at refrigerator temperature (4 °C).

#### 2.4 Development and recovery of biosurfactant

The solid-state fermentation was carried out using banana stalk powder (5 g) as substrate moistened with 5 mL of fungal growth suspension prepared by mixing g/L of NaNO<sub>3</sub> (3.0), MgSO<sub>4</sub>.7H<sub>2</sub>O (0.5), KH<sub>2</sub>PO<sub>4</sub> (1.0), yeast extract (1.0) and peptone (3.0) with a pH 7.0. The media was sterilized by autoclaving for 20 min at 121 °C temperature. Fermentation medium was added with 2 mL of A. niger inoculum containing 10<sup>7</sup> spores/mL and incubated at 37 °C for 6-8 days. All the experiments were conducted in triplicate. Media was centrifuged for 20 min at 5600 rev/min to get cell-free supernatant. Cell-free supernatant was acidified with 6 N HCl to get a final pH of 2.0 and was kept in refrigerator temperature (4 °C) for the precipitation of lipids and proteins [1]. The pallets were harvested by centrifugation for 15 min at 10,000 rev/min and pH was adjusted to normal by the addition of sufficient amount of distilled water. The extracted pallets were lyophilized for the quantification of biosurfactant.

# 2.5 Screening of biosurfactant

#### 2.5.1 Oil displacement

Oil displacement was performed using the method adopted from Morikawa et al. [37] with little modifications. Briefly, distilled water (40 mL) was poured in a glass petri plate of 90 mm diameter. Cottonseed oil (8.0 mL) was poured on the water surface to form a thin layer. Cellfree supernatant containing biosurfactant (3 mL) was gently poured at the center of petri plate. The area (cm<sup>2</sup>) of displaced oil layer was measured for determination of biosurfactant.

# 2.5.2 Emulsification index

Emulsification index ( $E_{24}$ ) was determined by the method of Alvarez et al. [38]. Briefly, the cell free supernatant was added in the cottonseed oil with 3:2 (biosurfactant: oil) ratio. The mixture was gently vortexed, and the height (cm) of emulsion layer and total height of solution was calculated after 24 h. The emulsification index was calculated by using the equation.

Emulsification index(
$$E_{24}$$
) =  $\frac{Hight of emulsion layer (cm)}{Total hight of solution (cm)} \times 100$ 

## 2.5.3 Emulsification activity assay

The determination of emulsification assay was performed by the method described by Patel and Desai, [39]. Briefly, a solution of Tris-Mg was prepared by the addition of Tris-HCl (20 mM) and MgSO<sub>4</sub> (10 mM) with a final pH of 8.0. Tris-Mg solution (7.5 mL) was added in a test tube and added with 0.5 mL of cell-free supernatant (biosurfactant) and 0.1 mL of kerosene oil. The tubes were gently vortexed and allowed to stand for 60 min. Absorbance was recorded at 540 nm using UV/visible spectrophotometer (Dynamica Scientific, HALO DB-20). Patel and Desai (1997) described the emulsification activity as the measured optical density of a sample. The activity was calculated by using the following relationship:

Emulsification activity(OD<sub>540</sub>) =  $^{A}/_{I}$ 

here 'A' is absorbance and 'L' is optical pass length.

# 2.6 Structural characterization of biosurfactant

#### 2.6.1 Fourier transform infrared spectroscopy (FT-IR)

Biosurfactant obtained from native as well as mutant strains of *A. niger* was analyzed using FT-IR (Bruker Alpha FTIR, Germany) for the detection of major functional groups. The lyophilized biosurfactant samples (0.5 mg) were placed directly under the infrared beam and spectrum was recorded at 500 – 4000 nm wavelength for detailed structural analysis.

# 2.7 Optimization of biosurfactant production

Optimization is a technique used to get the best possible results with maximum achievable performance and costeffectiveness under certain limitations. The biosurfactant production from mutant *A. niger* was optimized using response surface methodology (RSM) under central composite design (CCD). RSM is a combination of statistical and mathematical techniques used to analyze the effect of dependent variables on one or more independent variables (response). Four parameters i.e., temperature (X1), pH (X2), incubation time (X3) and substrate concentration (X4) were optimized using four-factors, six-level CCD requiring 30 runs with six central points and  $\alpha$  0.5. The biosurfactant was harvested by acid-precipitation followed by centrifugation at 10,000 *rev*/min for 15 min. The extracted biosurfactant was freeze-dried and weighted for quantification. The RSM model was designed using Design Expert software v11.1.0.1.

# **3 Results**

# 3.1 Screening for best biosurfactant producer strain

Biosurfactant produced by native strain of *A. niger* (2.3 g/L) showed 49.74 cm<sup>2</sup> oil displacement area, 57% emulsification index and 1.024 emulsification activity. The wild fungal strain was mutated with EtBr to determine the consequence of mutagenesis on total biosurfactant yield. Table 1 summarizes the data obtained after sequential

mutagenesis in A. niger using different concentrations and exposure time to mutagen (EtBr). Maximum biosurfactant yield (3.3 g/L) was attained from A. niger M2 specie exposed to 50 µg/10 mL EtBr for 60 min. In addition, screening tests revealed an emulsification index of 62.30% and emulsification activity of 1.262 (OD<sub>540</sub>) with oil displacement area of 59.81 cm<sup>2</sup>. All the mutants produced significant amount of biosurfactant ranging from 1.5 – 3.3 g/L depending upon mutagen concentration and exposure time (Fig. 1a). Figure 1b provides a representation of emulsification index  $(E_{24})$  from different mutant strains of A. niger. The emulsification and oil displacements conformed the biosurfactant production, and the dry weight estimation after lyophilization made the selection easier for maximum producing mutant colonies (A. niger M2) which was subjected to RSM optimization.

Table 1Screening of A.niger mutants for theirbiosurfactant productionpotential depending upontotal biomass, oil displacementarea, emulsification index andemulsification activity

EtBr conc. (µg/10 mL)	Mutant strain ID	Exposure time (min.)	Displace- ment area (cm <sup>2</sup> )	Emulsifica- tion index % (E <sub>24</sub> )	Emulsification activity (OD <sub>540</sub> )	Biosur- factant yield (g/L)
50	M1	30	47.76±3.44	57.63±2.30	1.024±0.01	2.9±0.20
	M2	60	$59.81 \pm 4.20$	$62.30 \pm 2.41$	$1.262 \pm 0.00$	$3.3 \pm 0.21$
	M3	90	$52.78 \pm 4.01$	$59.95 \pm 1.80$	$1.175 \pm 0.01$	$3.0 \pm 0.18$
100	M4	30	$30.18 \pm 3.32$	$42.45 \pm 2.81$	$0.820 \pm 0.03$	$2.1 \pm 0.28$
	M5	60	$37.37 \pm 3.41$	$47.50 \pm 2.73$	$0.963 \pm 0.02$	$2.6 \pm 0.30$
	M6	90	$35.24 \pm 3.00$	$47.23 \pm 2.89$	$0.894 \pm 0.01$	$2.7 \pm 0.27$
150	M7	30	$25.50 \pm 2.91$	$39.60 \pm 2.31$	$0.679 \pm 0.00$	$1.6 \pm 0.10$
	M8	60	$24.62 \pm 3.31$	$38.24 \pm 2.40$	$0.652 \pm 0.01$	$1.5 \pm 0.13$
	M9	90	$32.96 \pm 4.29$	$43.04 \pm 2.44$	$0.740 \pm 0.00$	$1.7 \pm 0.11$
200	M10	30	$40.69 \pm 4.10$	$49.90 \pm 7.20$	$0.826 \pm 0.00$	$1.9 \pm 0.51$
	M11	60	44.39±6.21	$63.45 \pm 7.61$	$1.260 \pm 0.02$	$3.0 \pm 0.39$
	M12	90	$42.99 \pm 4.02$	$61.20 \pm 6.91$	$1.187 \pm 0.00$	$2.4 \pm 0.42$

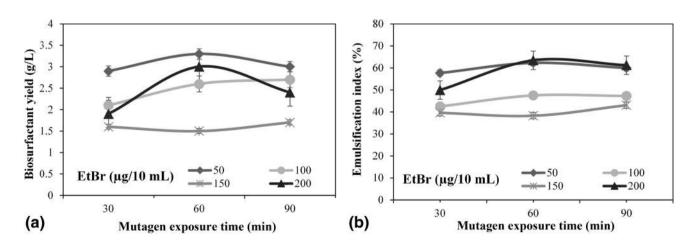


Fig. 1 Representation of **a** Biosurfactant yield **b** Emulsification index (E<sub>24</sub>) of biosurfactant produced from *A*. *niger* after exposure to different concentrations of EtBr for different time periods

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#### 3.2 Fermentation for biosurfactant production

Biosurfactant production was monitored after 168 h of fermentation. The maximum biosurfactant production (3.3 g/L) was attained from *A. niger* M2 spp. with highest emulsification index of 62.30%. The extraction of biosurfactant was performed using acid-precipitation. Biosurfactant is generally soluble at basic or neutral pH (i.e. 7). By decreasing the pH, biosurfactant start to precipitate and increase the turbidity of the solution. This effect was determined by gradually decreasing the pH using 6 N HCl and taking the absorbance at 600 nm at UV/vis spectrophotometer (Dynamica Scientific, HALO DB-20). The maximum biosurfactant precipitation was achieved at pH 2. Further decrease in pH did not resulted any significant change (Fig. 2).

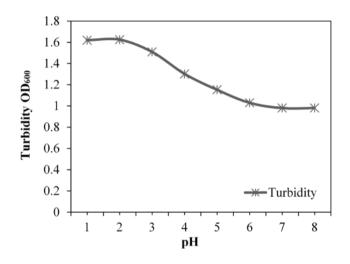


Fig. 2 Representation of biosurfactant precipitation (increase in turbidity of solution) at acidic range of  $\ensuremath{\mathsf{pH}}$ 

# 3.3 Major functional groups: FTIR

Spectrum of biosurfactant produced from native *A. niger* (Fig. 3, orange line) showed a broad peak at 3366 cm<sup>-1</sup> which shows asymmetric stretching of N–H bonds of secondry amides of proteins. A peak at 2890 cm<sup>-1</sup> shows strong stretching of C–H bonds of alkane alkene and alkynes. A intense peak at 1655 cm<sup>-1</sup> indicate C=O, C–N stretching and N–H bending of protein amides. A short peak at 1710 cm<sup>-1</sup> shows the presnece of C=O stretching of carboxylic acid, aldehyde and keton functional groups. A peak at 1500 cm<sup>-1</sup> indicate the presence of C=C bond of aromatic skeloton and peak at 1571 cm<sup>-1</sup> shows N–H bonds of amines group. Peek at 1220 cm<sup>-1</sup> indicate the presence of P=O bond of phosphodiester group of nuclic acid and phospholipids.

Biosurfactant from mutant strain *A. niger* M2 has been presented in Fig. 3 (blue line), which shows a broad peak at 3349 cm<sup>-1</sup> which shows weak N–H stretching of primary and secondary amines and amides. Successive vibrations between 2000 and 2500 cm<sup>-1</sup> indicates the presence of N–H, C–H bonds of alkane alkene and alkynes. A peak at 1710 cm<sup>-1</sup> show plane stretching of C=O bond which indicate the presence of ester, lipid and triglycerides functional group. A peak at 1551 cm<sup>-1</sup> indicates the presence of N–H bending which is coupled with C–N bond stretching of amide functional group. Peaks at 1456, 1435 and 1400 cm<sup>-1</sup> indicate the presence of CH<sub>3</sub> asymmetric vibration, C–H bending and CH<sub>3</sub> symmetric vibrations of protein respectively. A broad peak at 1051 cm<sup>-1</sup> shows C-O stretch of COH tyrosine protein. Peek at 702 cm<sup>-1</sup>

#### 3.4 Optimization of biosurfactant

The biosurfactant yield from *A. niger* M2 was further optimized in SSF using statistical tools (RSM). 4-level, 6-factors CCD was used which required 30 experiments and

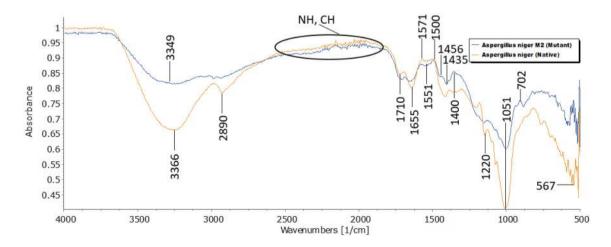


Fig. 3 FT-IR spectra of lyophilized biosurfactant produced by native and mutant strains of A. niger

the response (g/L of biosurfactant yield) was determined. Total biosurfactant yield was in the range of 2.8–5.5 g/L depending upon fermentation conditions provided. The lowest yield was obtained at 35 °C temperature, 5.5 pH, 4.5 g substrate concentration and incubation of 168 h. The maximum biosurfactant yield (5.5 g/L) was obtained at 35 °C temperature, 7 pH, 5.57 g substrate concentration and an overall incubation period of 168 h. The model was analyzed using Design-Expert software and the 3D response surface graphs were constructed.

The response surface model significance and fitness were analyzed by the determination of ANOVA variant for quadratic model and each individual factor was tested using F-values and p-values. ANOVA for RSM quadratic model for biosurfactant production under optimized conditions has been represented in Table 2. The high model F value (2.743) showed that the model is significant. The lack of fit value was insignificant indicating the model appropriateness. These results showed the quality and the fitness of the RSM and its capability to predict the response within the range of variables used. RSM model suggested the quadratic equation for the total biosurfactant yield which can be expressed as follows: where X1, X2, X3 and X4 are the codded values of the relating factors temperature, pH, incubation time and substrate concentration.

Temperature and pH are the great influencer of biosurfactant production during fermentation. The optimum production occurs in the specific range where the microorganism is most active. In case of Aspergillus strains, the optimum growth temperature lies between 30 and 40 °C and a pH ranging from 6 to 7. This indicates the high temperature and pH dependency of biosurfactant production process. In this study, maximum biosurfactant production was obtained at pH 7 and 35 °C temperature. Figure 4a presents the effect of temperature and pH on biosurfactant yield at fixed value of substrate concentration and fermentation time. Since the optimum pH for Aspergillus strains is 6.5-7, the production was drastically reduced at end points of pH variable. Temperature was also the critical parameter that have been controlled in bioprocess. Strain A. niger M2 showed maximum activity at 30-40 °C temperature with maximum biosurfactant production at 35 °C (Fig. 4a).

Incubation time was found to be one of the most influencer of biosurfactant production. Biosurfactant

Biosurfactant yield 
$$(g/L) = 2.05 + 0.0784(X1) + 0.0166(X2) + 0.0157(X3)$$
  
+ 0.0353(X4) + 0.0441(X1 × X2) + 0.0206(X1 × X2))

+ 
$$0.0212(X1 \times X4) - 0.0027(X2 \times X3) + 0.0234(X2 \times X4)$$

$$-0.0134(X3 \times X4) + 0.3274(X1^{2}) - 0.5901(X2^{2})$$

$$-0.9827(X3^2) + 1.09(X4^2)$$

Table 2Analysis of variance(ANOVA) for response surfacemodel for the development ofbiosurfactant by A. niger M2

Source	Sum of squares	df	Mean square	F value	<i>p</i> value	
Model	22.15	14	1.58	36.29	0.000	Significant
A-temperature	0.116	1	0.117	2.68	0.002	
В-рН	0.136	1	0.136	3.13	0.007	
C-incubation time	0.434	1	0.434	9.96	0.006	
D-substrate concentration	0.012	1	0.013	0.294	0.005	
AB	1.95	1	1.95	44.63	< 0.000	
AC	0.230	1	0.231	5.29	0.036	
AD	0.024	1	0.024	0.551	0.009	
BC	0.176	1	0.176	4.05	0.002	
BD	0.000	1	0.001	0.009	0.925	
CD	0.144	1	0.144	3.31	0.088	
A <sup>2</sup>	0.176	1	0.176	4.04	0.062	
B <sup>2</sup>	0.469	1	0.470	10.77	0.005	
C <sup>2</sup>	0.030	1	0.031	0.702	0.415	
D <sup>2</sup>	0.073	1	0.074	1.69	0.213	
Residual	0.654	15	0.044			
Lack of fit	0.588	10	0.059	4.46	0.0562	Not significant
Pure error	0.065	5	0.014			
Cor total	22.80	29				

X3)

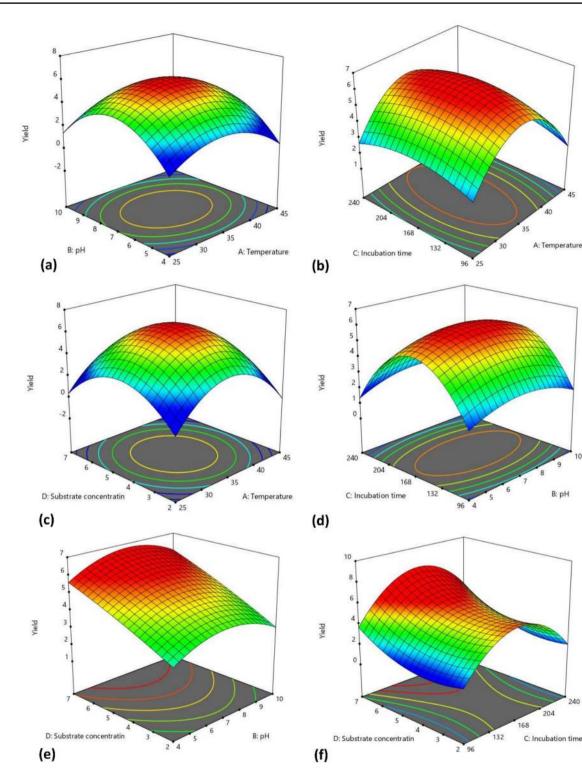


Fig. 4 Response surface three-dimensional (3D) plots showing interaction between a temperature versus pH b temperature versus incubation time c temperature versus substrate concentration

production was maximum after 168 h of incubation in SSF of banana stalks powder. The production was equally decreased at higher or lower values of incubation time d pH versus incubation time e pH versus substrate concentration f incubation time versus substrate concentration

than 168 h. Figure 4b shows the interaction between temperature and incubation time by keeping other factors constant. Any deviation from 168 h of incubation leads to

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the decline in biosurfactant production from *A. niger* M2. The strains showed maximum production after 168 h in the exponential growth phase of the specie.

The joint effect of temperature and substrate concentration has been represented in Fig. 4c by keeping pH and incubation time constant. The biosurfactant yield was maximum at 4–5 g of substrate and the yield was equally decreased at upper and lower level of factor. The maximum biosurfactant production was achieved at 5.75 g of substrate concentration where the factor was at + 1 level of the design. Figure 4d shows the joint effect of pH and incubation time on biosurfactant production by keeping other factors constant. Maximum biosurfactant production was obtained at pH 6 to 7 and 168 h of incubation in SSF. The production was equally declined at higher and lower level of these factors, but the pH was less influencing the production as compared with incubation time.

The effect of pH versus substrate concentration has been displayed in Fig. 4e by keeping constant values of temperature and incubation time. In the figure, substrate concentration positively influenced the biosurfactant production, means the yield was increased by increase in substrate concentration, whereas, at pH 6 to 7, yield was optimum which gradually decreased by moving towards extreme points, but the reduction was generally lower. Figure 4f shows the interaction between incubation period and substrate concentration by keeping temperature and pH constant. Highest yield was obtained at 6 to 7 g substrate concentration and incubation period of 168 h.

# 4 Discussion

The production of microbial surfactants has gained high importance from previous decade, especially due to their potential applications in biomedical and industrial biotechnological sectors. Oil displacement, Emulsification activity and emulsification index has been used for the estimation of biosurfactant [32, 38–40]. Therefore, using such strategy, biosurfactant production from A. niger was screened after random mutagenesis for the selection of highest biosurfactant producer mutant strain. Furthermore, quantification using dry weight estimation made the selection more convenient. Biosurfactant production from fungal species have extensively been described from Aspergillus spp. [41–44] using various synthetic and biobased substrates, but herein, mutant A. niger (M2) produce significantly higher amount of biosurfactant (3.3 g/L) as compared with previous studies using native A. niger strain. The mutant (A. niger M2) exhibited high emulsification index and oil displacement as compared to native strain (Table 1).

Despite having several commercially attractive characteristics compared with synthetic surfactants, the production of commercial scale biosurfactants from microbial origin has not been realized because of their high production cost and significantly low yield. There are two basic strategies that are being adopted by the biotechnologists for economical biosurfactant production, which corresponds, the use of low-cost waste materials to reduce the overall substrate cost and the efficient bioprocesses, including optimized fermentation parameters involving multiple physical and nutritional factors [45]. The selection of appropriate substrate is a crucial step in the production of biosurfactant, as the substrate account for overall 10-30% cost of the experiment [45, 46]. Therefore, in this context, herein, a cost-effective process was developed for the production of biosurfactant using agro-industrial raw-material (banana stalks powder) with waste-to-value approach. The production of significant amount of biosurfactant using banana stalks waste revealed the compatibility of the medium. Hence, the reported medium composition was selected for the next experiments.

The biosurfactant production during logarithmic growth phase and stationary phase of microorganisms have already been studied from various fungal species e.g., A. ustus [42], A. niger [43, 44], A. flavus [43, 46], A. versicolor [47], and Piper hispidum [48], and various factors influencing the total biosurfactant yield during fermentation have broadly been studied in previous few decades [42, 49–54]. From these, several studies have reported classical methods for optimization purpose by placing one factor as constant and modifying another one. In this research, we have applied a proper tool (RSM) for the optimization of different factors that influence biosurfactant production from A. niger M2 during fermentation. One of the advantages of this mutant (A. niger M2) is the highest amount of biosurfactant production with maximum emulsification activity, which make it capable for several industrial applications such as microbially enhanced oil recovery [30, 38].

After optimization using RSM-CCD, maximum biosurfactant production (5.5 g/L) was attained which was 2.5-folds higher than the biomass obtained from native strain and about 1.7-folds higher than the mutant strain (*A. niger* M2). These results clearly suggest a significantly higher amount of biosurfactant as compared with previous studies. The central composite design (CCD) during RSM enabled us to investigate different fermentation parameters that support biosurfactant overproduction. A close association was observed between R<sup>2</sup> (0.820) and predicted R<sup>2</sup> (0.794), which reflected the compatibility and suitability of methodology to optimize biosurfactant production. The maximum yield was obtained at 35 °C temperature, 7 pH, 5.75 g substrate concentration and 168 h of overall fermentation period. Any change (increase of decrease) in one of these parameters may cause decrease in biosurfactant production. The biosurfactant yield (5.5 g/L) from *A. niger* M2 is the highest reported yield from *Aspergillus* species in solid state fermentation.

In addition, the use of banana stalks waste as a substrate in SSF for biosurfactant production by A. niger is novel. The production cost would be significantly reduced via experimental design described in this study using optimized fermentation conditions. The insights of fungal surfactants and their significant characteristics have also been studied in this research. The stability of biosurfactant obtained from A. niger M2 over a wide temperature range indicates its activity at extreme environmental conditions, which is an amazing feature for its potential use in biomedical and industrial biotechnological sectors including microbial enhanced oil recovery and bioremediation [9, 12]. In conclusion, we have successfully improved the biosurfactant production about 1.5-folds after random chemical mutagenesis of A. niger using banana stalks powder as low-cost substrate following waste-to-value idea (from 2.3 to 3.3 g/L).

# 5 Conclusion

In this study, biosurfactant production was successfully enhanced about 1.5-folds after EtBr mutagenesis of A. niger using agro-industrial waste (banana stalks powder) as low-cost substrate. Optimization of fermentation parameters was performed using statistical approach (RSM-CCD) to maximize the yield. After optimization, maximum biosurfactant yield (5.5 g/L) was attained, which was significantly higher from both native as well as mutant strains (before optimization) i.e., 2.5-folds and 1.7-folds respectively. In conclusion, the biosurfactants produced from A. niger were a kind of surface-active substances, having potential applications in biomedical and industrial biotechnological sectors including enhanced oil recovery and bioremediation. To the best of our knowledge, this the first study reporting mutagenesis of A. niger for improved biosurfactant production and process optimization using cost-effective agro-industrial waste as substrate.

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#### **Compliance with ethical standards**

**Conflict of interest** The authors declared that they have no conflict of interest.

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