

Mechanochemical Synthesis of Poly(phenylene vinylenes)

The MIT Faculty has made this article openly available. *Please share* how this access benefits you. Your story matters.

Citation	Ravnsbæk, Jens B. and Timothy M. Swager. "Mechanochemical Synthesis of Poly(phenylene Vinylenes)." ACS Macro Letters 3, 4 (March 2014): 305–309 © 2014 American Chemical Society		
As Published	http://dx.doi.org/10.1021/mz500098r		
Publisher	American Chemical Society (ACS)		
Version	Author's final manuscript		
Citable link	http://hdl.handle.net/1721.1/115098		
Terms of Use	Article is made available in accordance with the publisher's policy and may be subject to US copyright law. Please refer to the publisher's site for terms of use.		



Mechanochemical Synthesis of Poly(phenylene vinylenes)

Jens B. Ravnsbæk and Timothy M. Swager*

Massachusetts Institute of Technology, Department of Chemistry, Massachusetts Avenue 77, Cambridge, MA, USA

We report a simple, rapid and solvent-free methodology for solid-state polymerizations yielding poly(phenylene vinylenes) (PPV) promoted by ball-milling. This solid-state Gilch polymerization method produces PPVs in as little as five minutes of milling. Detailed investigations of the parameter space governing the solid-state polymerization, i.e. milling time, base strength, solid-state dilution, milling frequency and size of milling balls, revealed that polymerization by ball-milling is a rapid process achieving molecular number average weights of up to 40 kDa in up to 70% yield. To explore the scope, a solid-state polymerization via the dithiocarbamate precursor route is explored.

Application of mechanical force as activation for chemical transformations i.e. mechanochemistry, is a powerful alternative to photo-, electro- or thermo-chemical activation.¹ The impact of mechanochemistry to organic synthesis is now recognized and many important organic transformations have been successfully demonstrated e.g., amide couplings,² palladium catalyzed cross-couplings³ and the Wittig reactions.⁴ Several informative reviews have been recently published covering these developments.⁵ Solid-state transformations, typically promoted by ball-milling, have several advantages over their traditional "wet-chemistry" counterparts. Firstly, the reactions can proceed in higher yields and short reaction times. Secondly, no solvents or reagent equivalent solvents are added, which significantly reduces waste generation. Despite demonstrations of mechanochemical activation in organic synthesis, the utilization for synthesis of polymers, especially conjugated polymers, is largely untapped. There have only been a handful of reports on the synthesis of conjugated polymers by mechanochemical promoted polymerizations.⁶ A critial element in polymer synthesis is the fact that mechnochemical treatments are well known to break polymers down and can be used to lower their molecular weights. As a result, investigations of mechanochemical parameters (i.e., reaction time, energy input, dilution of the monomers etc) need to be examined to determine the potential of this method in polymer synthesis. Detailed investigations of the parameter space governing solid-state polymerization provides new insight and allows further utilization of this solid-state synthesis method.

We report herein a simple, rapid and solvent-free method for the synthesis of poly(phenylene vinylene) via solid-state polymerization promoted by ball-milling, and the parameters influencing the mechanochemical promoted polymerization. Poly(phenylene vinylene)s (PPVs) have received extensive research interest since there use an electroluminescent material in the early 1990's.⁷ PPVs can be synthesized by methods including Wessling,⁸ sulfinyl,⁹ xanthate,¹⁰ dithiocarbamate,¹¹ Gilch,¹² Wittig,¹³ Heck,¹⁴ Suzuki¹⁵ couplings. The Gilch method is the preferred route to PPVs as a result of the easy obtainable monomer and straightforward reaction conditions producing conjugated polymers of high molecular weight in good to excellent yield.¹⁶ However, the Gilch method still has drawbacks. Firstly, to achieve high yields extended reaction times approaching 24 hours are typically required. Secondly, the reactive quinodimethane intermediates undergo fast polymerization and associated high molecular weight fractions often leads to gelation of the reaction mixture, which complicates purification.¹⁶ We envisioned, that these issues could be resolved by utilizing a solid-state Gilch polymerization promoted by ball milling.

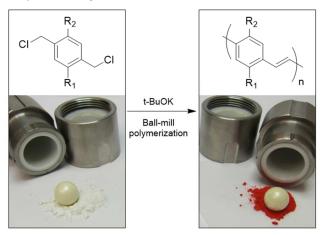


Figure 1. Solid-state Gilch polymerization promoted by ballmilling.

To probe the possibilities of solid-state Gilch polymerization and to investigate the parameter space of the solid-state mechanochemical polymerization, we selected poly(2methoxy-5-2'-ethylhexyloxy phenylene vinylene) (MEH-PPV) as a model system.¹⁷ MEH-PPV is among the most widely studied PPVs, owing to the excellent solubility in most organic solvents. The required monomer for the synthesis of MEH-PPV via Gilch polymerization is readily synthesized in multigram scale via a two steps procedure.¹⁸

In our initial attempt at solid-state Gilch polymerization promoted by ball-milling the MEH-PPV monomer and three equivalents of potassium tert-butoxide were added to a 10 mL zirconium oxide milling jar along with a 10 mm diameter zirconium oxide ball. The solid reaction mixture was subjected to vibrational ball-milling in a Retsch® mixer-mill 400 at 30 Hz for 30 minutes. After ball-milling, quenching was achieved by adding acidified methanol (5 mL) to the milling jars and subjecting the slurry to 15 seconds of ball-milling to ensure complete quenching of the polymerization reaction. This direct quenching procedure eliminates any continued polymerization that may occur during work-up, allowing us to probe exclusively the degree of polymerization taking place during ballmilling. The red slurry was poured onto a filter and washed thoroughly with water and methanol. The obtained red powder (see Figure 1) was subsequently dissolved in chloroform, precipitated from methanol and subjected to GPC analysis using a polystyrene standard. This confirmed that ball-milling yielded a polymeric material, i.e. a number average molecular mass (M_n) of 35 kDa was obtained for the product. The usage of zirconium oxide milling jars was chosen as the ceramic properties allows for the important direct quenching procedure as opposed to use of stainless steel milling jars, which are not inert towards the acidic quenching conditions.

The success of our initial experiment with solid-state Gilch polymerization prompted a series of questions: What is the effect of milling time on polymer size, polydispersity and yield? Does the solid-state nature of the polymerization alter the base requirements? How does solid-state dilution of the monomer in base effect the polymer size, polydispersity and yield? What is the required energy input for successful polymerization? To answer these questions we initiated an investigation into the parameter space governing the solid-state dilution, milling frequency and size of the milling balls. All experiments described in the following were repeated either two or four times, and presented results (yields, polydispersity index (PDI) and M_n) are reported as averaged values.

First, we conducted a series of solid-state polymerizations with varying milling time. The isolated yield, along with molecular weight and polydispersities estimated by GPC using a polystyrene standard are shown in Figure 2. The solid-state Gilch polymerization promoted by ball-milling is rapidly occurring, i.e. after just five minutes, polymers with M_n of 35 kDa is obtained in >50% yield (Figure 2A). A significant improvement in isolated yield as a function of ball milling time is observed, however the main improvement occurs at short milling times, i.e. one to five minutes with isolated yields increasing from 22 to 50%. After ten minutes of ball milling the isolated yield reaches 63% with only a minor improvement upon extended milling times e.g. 67% at 30 minutes. It should be noted, that during the purification process precipitation of small amounts of insoluble polymeric material were discarded. The insoluble material may originate from crosslinking of the polymer chains during the radical polymerization at very high concentrations. Surprisingly, only minor correlation between milling time and the molecular weight is observed, with M_n rapidly reaching a plateau of ~40 kDa (Figure 2B). The isolated polymers show a broad molecular weight distribution with polydispersity ranging from 3.8 to 4.5 with no significant improvement with increased milling time.

To gain further insight into the observed upper limit of $M_n \sim$ 40 kDa for the isolated polymers, a MEH-PPV with a $M_n \sim$ 150 kDa prepared by standard solution based methods¹⁶ was subjected to ball milling and samples were taken at specific milling times i.e., 5, 10, 15, 20, 25 and 30 minutes. The samples were analyzed by GPC and the data are depicted in Figure 2C. The M_n of the solid-state polymerization from Figure 2B are shown in 2C for comparison. We observe a rapid degradation of MEH-PPV as a function of milling time, i.e. after 15 minutes of ball-

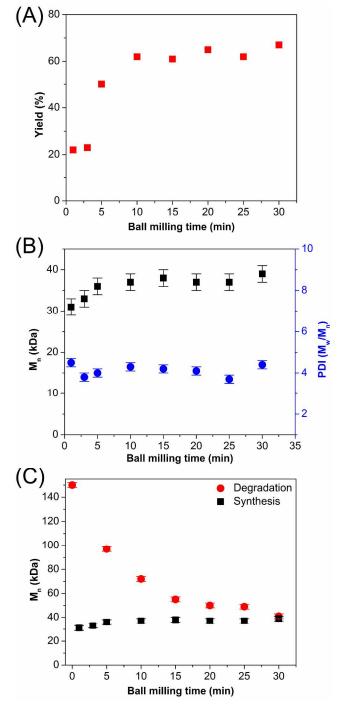


Figure 2. The effect of varying milling time on isolated yield, molecular number average weight (M_n) and polydispersity (PDI). A) Isolated yield as function of milling time. B) M_n and PDI as function of milling time. C) M_n as function of milling time for synthesis (black squares) of solid-state prepared MEH-PPV and degradation (red circles) of solution-prepared MEH-PPV.

milling the M_n is only 1/3 of the starting value. The results further show that the majority of degradation takes place within the first 15 min of milling after which M_n levels of to a plateau at ~40 kDa. We hypothesize, based on this observation, that when the M_n of the PPVs exceed 40 kDa the polymer chain can accumulate sufficient energy for chain scission, i.e. degradation occurs. The correlation between the M_n for the degradation and the synthesis suggests that two processes occur during ball-mill promoted polymerization, i.e. a construc1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

16

17

18

19

20

21

22

23

24

25

26

27

28

29

30

31

32

33

34

35

36

37

38

39 40

41 42 43

44

45

46 47

48

49

50

51

52

53

54

55

56

57

58

59 60 tive and destructive process. For polymer chain sizes of $M_n <$ 40 kDa the constructive process is dominant, while the destructive pathway becomes the dominant pathway for large polymer chains. A similar trend has been reported for the mechanochemical synthesis/degradation of styrene/polystyrene.¹⁹ It should be noted that once chain scission has occurred, the polymer chain loses its ability to reinitiate polymer growth. This is supported by the lack of improvement in PDI as a function of milling time. In the characterization of the MEH-PPVs obtained from our mechanochemical method, we observe no significant differences between solid-state prepared and solution-prepared polymers by FT-IR, ¹H NMR and the polymer have similar degradation temperatures as evaluated by thermo gravimetric analysis (see supplementary information).

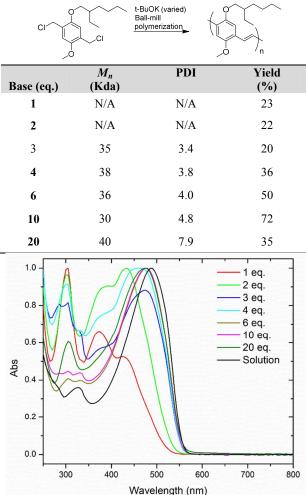


Figure 3. Effects of varying the equivalents of tBuOK illustrated by GPC analysis (top) and UV-Vis data (bottom).

The solid-state nature of this method results in very high concentrations of monomers compared to solution-based reactions, i.e. in the solid-state mixture approximately $\frac{1}{4}$ of the total volume is monomer. Addition of additional base effectively constitutes a dilution of the monomer. To investigate the effect of solid-state dilution, we conducted a series of polymerizations with varying amounts of base ranging from one to twenty equivalents. The results from this series of experiments are depicted in Figure 3. In a typical Gilch polymerization carried out in solution three to four equivalents of *t*-

BuOK are added to initiate effective polymerization. We observe a similar requirement for the solid-state Gilch polymerization, i.e. no polymerization is observed when adding only one or two molar equivalents of t-BuOK, and only small molecule products are isolated. Addition of >3 equivalents of base results in polymerization. Interestingly, the yield of the polymerization increases significantly with increasing amount of base, i.e. only 20% yield is obtained at three equivalents base, while a very satisfying 72% isolated yield is obtained at 10 equivalents of base. Further dilution, as illustrated by 20 molar equivalents of base, has a severe impact on the isolated yield and only 35 % is obtained in this case. We speculate that the beneficial effect up to around 10 equivalents is due to minimization of crosslinking by dilution and that increased dilution beyond this point results in less efficient polymerization. Again, no significant effect on M_n is observed as function of equivalent base added. We analyzed the samples from this series of experiments by UV-Vis spectroscopy (see Figure 3, bottom). This further confirms that the number of base equivalents affects the polymerization. For low molar equivalents i.e. one or two equivalents we observe absorption peaks at high energy corresponding to short conjugated systems. As we increase the molar equivalents of base the main absorption peak shifts towards the characteristic major absorption peak of MEH-PPV, as illustrated by comparison to a solution-prepared MEH-PPV. This trend can even be observed by simple inspection of the visual colors of the crude polymers (see SI). Furthermore, as Balemo et al. have reported effective ylide formation in the solid-state promoted by ball-milling utilizing milder bases than the corresponding solution-based reaction, we tested K₂CO₃, KOH and t-BuOK as bases for our solidstate Gilch polymerization. Unfortunately, no polymerization was observed for the milder bases, K₂CO₃ and KOH under the tested conditions.

Table 1. Effects of frequency (top table) and size of the milling balls (bottom table).

Frequency (Hz)	M _n (Kda)	PDI	Yield (%)
<10	-	-	-
15	Inhomogeneous	Inhomogeneous	-
20	28	8.2	28
25	24	4.4	45
30	39	4.4	67
Ball Size (mm)	Mn (Kda)	PDI	Yield (%)
1.5 (68 pcs)	-	-	-
5 (10 pcs)	Inhomogeneous	Inhomogeneous	*
10 (1 pcs)	39	4.4	67

*The obtained samples were inhomogeneous as a result of incomplete mixing as a result M_n , PDI and yield was not determined.

Lastly, we investigated the requirements on the energy input for effective polymerization. This was achieved by changing the vibrational milling frequency as well as the size of the milling balls. In our investigations of the effect of ball milling frequency (number of impacts between ball and vial wall per second), we conducted solid-state polymerizations at 5, 10, 15,

20, 25 and 30 Hz (see Table 1). At low frequencies, i.e. 5 and 10 Hz, no significant polymerization occurs, while increasing the frequency to 15 Hz results in inhomogeneous polymerization arising from insufficient mixing. Higher frequencies result in successful polymerization with improved M_n and isolated yields as we increase the frequency from 20 Hz to 30 Hz, the upper frequency limit of the instrument. These results suggest that solid-state polymerization promoted by ball milling requires a certain amount of energy to promote monomer activation as well as effective mixing. We speculated that utilizing milling balls with a smaller diameter would improve polymerization due to improved mixing. To test this hypothesis we conducted a series of polymerizations with varying sizes of milling ball i.e. diameters of 1.5, 5 and 10 mm. For these experiments, we kept the total mass of added milling balls constant, to ensure approximately the same overall energy input in each polymerization. The results are summarized in bottom part of Table 1. We observed no polymerization with the smallest diameter milling balls (1.5 mm) and only inhomogeneous pockets of polymerization are observed for milling balls with diameter of 5 mm. These results suggest that solid-state Gilch polymerization via vibrational ball-milling requires a threshold impact-energy in addition to efficient mixing, i.e. the most important contribution to successful polymerization stems from impact energy and in our system milling balls of 15 mm diameter are required to ensure sufficient energy to effectively initiate and promote polymerization. Here, it should be noted milling jars did not appear to heat up (determined by touch) during these short milling experiments. To confirm that successful solid-state polymerization is not a result of impact heating, we subjected a solid mixture of monomer and t-BuOK to heat in an oil bath. We observed that polymerization does occur when the sample is subjected to prolonged heating (1 hour) at 100 °C. However, the polymerization results in heavy cross-linking and soluble polymer was only isolated in 10% yield. This emphasizes the importance of simultaneously inducing high impact energy and efficient mixing in order to achieve successful solid-state polymerization.

1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

16

17

18

19

20

21

22

23

24

25

26

27

28

29

30

31

32

33

34

35

36

37

38

39

40

41

42

43

44

45

46

47

48

49

50

51

52

53

54

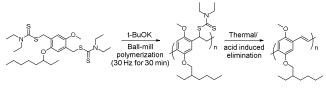
55

56

57

58

59 60



Scheme 1. The dithiocarbamate route promoted by ball-milling.

The successful solid-state Gilch polymerization results in broad PDIs ranging from 3.5-4.5. In solution-based polymerization of PPVs, the broad PDIs associated with the Gilch polymerization can be avoided by utilizing a precursor route, such as sulfinyl,⁹ xanthate,¹⁰ and dithiocarbamate.¹¹ We were interested in investigating if the improved characteristics of the precursor strategies would translate to our solid-state polymerization methodology. To this end we converted the Gilch monomer to the corresponding dithiocarbamate monomer in one simple step (see SI) and subjected this monomer and 10 eq. tBuOK to our optimized solid-state polymerization conditions i.e. 30 min at 30 Hz. In solution-based dithiocarbamate polymerizations a precursor polymer is first isolated and subsequently converted to the final conjugated PPV by thermal or acid elimination. This strategy typically requires the use of very strong lithium bases, such as LHMDS to produce the desired precursor polymer.¹¹ Much to our delight, we

observe that a polymeric product can be obtained by utilizing milder base, here tBuOK, under ball-mill promoted polymerization. The obtained polymers are of comparable molecular weight to MEH-PPV obtained by solid-state Gilch polymerization, namely M_n of 35 KDa. Moreover, this solid-state method provided a precursor polymer with a relatively low PDI of 1.4 in 54% isolated yield. The presence of the diethyl-thiocarbamate moiety was confirmed by ¹H-NMR (see supplementary information). Furthermore, thermal elimination was observed at 180 °C during thermo gravimetric analysis, which is in good agreement with temperatures for thermal elimination of such PPV-precursor polymers reported in literature¹¹.

In summary, we demonstrated successful solid-state polymerizations mechanochemically promoted by ballmilling. This method offers a rapid, simple and solvent-free synthetic route to PPVs. Detailed investigations of parameters affecting the solid-state polymerization revealed that polymers with molecular weights up to 40 kDa is produced in as little as five minutes. The isolated yield of the solid-state polymerization is affected by both milling time and more importantly by solid-state dilution, with a 44% improvement in yield by increasing the amount of base from six to ten equivalents. An upper limitation for the molecular weight of the polymers, ~40 kDa, were observed and ascribed to a competing mechanochemical constructive and destructive processes. Furthemore, solid-state dithiocarbamate precursor route resulted in polymers with a PDI of 1.4 constituting a significant improvement over the solid-state Gilch polymerization. The solid-state nature of this methodology could allow for direct synthesis of PPVs from monomers that are incompatible with solutionbased reaction conditions for the Gilch polymerization. Furthermore, we envision that this methodology will find utility in the fabrication of composite materials in which one component has poor solubility in organic solvents.

ASSOCIATED CONTENT

Supporting Information. Synthetic details, NMR, UV-Vis, GPC and related details. This material is available free of charge via the Internet at http://pubs.acs.org.

AUTHOR INFORMATION

Corresponding Author

*Email: tswager@mit.edu.

Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

Funding Sources

This work was supported by the US Air Force Office of Scientific Research.

Notes

Authors declare no conflicts of interest.

ACKNOWLEDGMENT

This work has been funded by US Air Force, Office of Scientific Research. JBR gratefully thanks the Danish council for independent research for funding. The authors thanks Jonathan G. Weis for fruitful discussions and John Goods for assistance with TGA.

1

2

3

4

5

6

7

8

9

ABBREVIATIONS

 M_n , number average molecular mass; PDI, polydispersity index; GPC, Gel Permeation chromatography.

REFERENCES

- James, S. L.; Adams, C. J.; Bolm, C.; Braga, D.; Collier, P.; Friščić, T.; Grepioni, F.; Harris, K. D. M.; Hyett, G.; Jones, W.; Krebs, A.; Mack, J.; Maini, L.; Orpen, A. G.; Parkin, I. P.; Shearouse, W. G.; Steed, J. W.; Waddell, D. C.; *Chem. Soc. Rev.*, **2012**, *41*, 413-447; Ralph, K.; Hardacre, C.; James, S. L.; *Chem. Soc. Rev.*, **2013**, *42*, 7701-7718; Zhu, S. -E.; Li, F.; Wang, G. -W.; *Chem. Soc. Rev.*,
- 10 2013, 42, 7535-7570; May, P. A.; Moore, J. S.; Chem. Soc. Rev., 11 2013, 42, 7497-7506.
- 12 2) Declerck, V.; Nun, P.; Martinez, J.; Lamaty, F.; *Angew. Chem., Int.* 13 *Ed.*, 2009, 48, 9318-9321.
- 2010, 12, 985-991; Tullberg, E.; Peters, D.; Frejd, T.; J. Organomet.
 Chem., 2004, 689, 3778-3781.
 4) Balema, V. P.; Wiench, J. W.; Pruski, M.; Pecharsky, V. K.; Chem.
- 4) Balema, V. P.; Wiench, J. W.; Pruski, M.; Pecharsky, V. K.; *Chem. Commun.*, 2002, 724-725.; Balema, V. P.; Wiench, J. W.; Pruski, M.;
 Pecharsky, V. K.; *J. Am. Chem. Soc.*, 2002, *124*, 6244-6245.
- 19 Pecharsky, V. K.; J. Am. Chem. Soc., 2002, 124, 6244-62 5) Wang, G. -W. Chem. Soc. Rev., 2013, 42, 7668-7700.
- a) Walig, G. W. Chem. Boc. Rev., 2010, 42, Vol. 71, 72, 100 (1997).
 b) Walig, J.; Moore, J. A.; Acquaye, J. H.; Kaner, R. B.; Macromole-cules, 2005, 37, 317-321. Mamimim X. Matsidik, R. Obulda, A.
- *cules*, 2005, *37*, 317-321; Mamtimim, X.; Matsidik, R.; Obulda, A.;
 Sidik, S.; Nurulla, I.; *Fiber Polym.*, 2013, *14*, 1066-1072; Murakami,
- S.; Tabata, M.; Sohma, J.; Hatano, M.; *J. Appl. Polym. Sci.*, 1984, 29, 3445-3455; Posudievsky, O. Y.; Goncharuka, O. A.; Pokhodenko, V.
- 24 D.; Synthetic Met., 2010, 160, 47-51; Posudievsky, O. Y.; Goncharuka, O. A.; Barille, R.; Pokhodenko, V. D.; Synthetic Met., 2010, 160, 462-467.
 27

- 7) Grimsdale, A. C.; Chan, K. L.; Martin, R. E.; Jokisz, P. G.; Holmes, A. B.; *Chem. Rev.*, **2009**, *109*, 897-1091.
- 8) Wessling, R. A.; Zimmerman, R. G.; US Pat., 3401152, 1968; Wessling, R. A.; J. Polym. Sci., Polym. Symp., 1985, 72, 55-66.
- 9) Louwet, F.; Vanderzande, D.; Adriaensens, P.; Gelan, J.; Synth. *Met.*, **1992**, *52*, 125-130; Louwet, F.; Vanderzande, D.; Gelan, J.; Mullens, J.; *Macromolecules*, **1995**, *28*, 1330-1331.
- 10) Son, S.; Dodabalapur, A.; Lovinger, A. J.; Ganlvin, M. E.; Science, 1995, 269, 376-378.
- 11) Henckens, A.; Duyssens, I.; Lutsen, L.; Vanderzande, D.; Cleij, T. J.; *Polymer*, **2006**, *47*, 123-131.
- 12) Gilch, H. G.; Wheelwright, W. L.; J. Polym. Sci., Part A-1, 1966, 4, 1337-1349.
- 13) McDonald, R. N.; Campbell, T. W.; *J. Am. Chem. Soc.*, **1960**, *82*, 4669-4671; Yang, Z.; Hu, B.; Karasz, F. E.; *Macromolecules*, **1995**, *28*, 6151-6154.
- 14) Klingelhöfer, S.; Schellenberg, C.; Pommerehne, J.; Bässler, H.; Greiner, A.; Heitz, W.; *Macromol. Chem. Phys.*, **1997**, *198*, 1511-1530; Bao, Z.; Chen, Y.; Cai, R.; Yu, L.; *Macromolecules*, **1993**, *26*, 5281-5286.
- 15) Koch, F.; Heitz, W.; Macromol. Chem. Phys., 1997, 198, 1531-1544.
- 16) Junkers, T.; Vandenbergh, J.; Adriaensens, P.; Lutsen, L.; Vanderzande, D.; *Polym. Chem.*, **2012**, *3*, 275-285.
- 17) Wudl, F.; Allemand, P. M.; Srdanov, G.; Ni, Z.; McBrranch, D. J.; ACS Symp. Ser., **1991**, 455, 683
- 18) Anderson, N.; Bagge, W.; Webber, C.; Zarras, P.; Davis, M. C.; *Synth. Comm.*, **2008**, *38*, 3903-3908.
- 19) Hasegawa, M.; Kimata, M.; Kobayashi, S.-I.; *J. Appl. Polym. Sci.*, **2001**, *82*, 2849-2855.

ACS Macro Letters

Authors are required to submit a graphic entry for the Table of Contents (TOC) that, in conjunction with the manuscript title, should give the reader a representative idea of one of the following: A key structure, reaction, equation, concept, or theorem, etc., that is discussed in the manuscript. Consult the journal's Instructions for Authors for TOC graphic specifications.

