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1 **Minimizing acetate formation in *E. coli* fermentations**

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17 **Keywords:** acetate reduction, *Escherichia coli*, metabolic engineering

18 **Abstract**

19 *Escherichia coli* remains the best established production organisms in industrial
20 biotechnology. However, during aerobic fermentation runs at high growth rates, considerable
21 amounts of acetate are accumulated as by-product. This by-product has negative effects on
22 growth and protein production. Over the last 20 years, substantial research efforts have been
23 spent to reduce acetate accumulation during aerobic growth of *E. coli* on glucose. From the
24 onset it was clear that this quest should not be a simple nor uncomplicated one. Simple
25 deletion of the acetate pathway, reduced the acetate accumulation, but instead other by-
26 products were formed. This minireview gives a clear outline of these research efforts and the
27 outcome of them, including bioprocess level approaches and genetic approaches. Recently,
28 the latter seems to have some promising results.

29

30 **1 Introduction**

31 *Escherichia coli* was the first and is still one of the most commonly used production
32 organisms in industrial biotechnology. Aerobic high cell density cultures of *E. coli* are most
33 frequently used to arrive at high biomass yields and high metabolite/protein concentrations.
34 Normally, glucose is fed as a carbon source in these high cell density fed-batch cultures.
35 Glucose is a cheap and simple molecule which enters the glycolysis (flow from glucose to
36 acetyl CoA) and the central metabolism through a minimum of steps. Furthermore, in a
37 medium with several carbon sources, glucose is first preferred one as a result of catabolite
38 repression. The glycolyse is the trunk routes of intermediary sugar metabolism in enteric
39 bacteria, which canalize 72% of the carbon supply. However, during aerobic fermentation
40 runs at high growth rates, considerable amounts of acetate are accumulated, as described by

41 Akkeson et al. (1999) [1] and references therein. In addition to a loss of carbon and therefore
42 an economic sink, acetate is also detrimental to recombinant protein production and inhibits
43 cell growth [2]. For more information about overcoming acetate in *E. coli* recombinant
44 protein fermentations see reference [3].

45 Formation of acetate in *E. coli* cultures under fully aerobic conditions can be caused by two
46 phenomena. On the one hand, a (local) lack of dissolved oxygen activates the fermentation
47 pathways, causing acetate excretion. This is referred to as mixed-acid fermentation. On the
48 other hand, this acetate excretion is also due to a metabolic overflow mechanism, caused by
49 an imbalance between the rapid uptake of glucose and its conversion into biomass and
50 products, diverting acetyl-CoA from the TCA-cycle towards acetate [1].

51
52 The two major aerobically active acetate producing pathways in *E. coli* are pyruvate oxidase
53 (*poxB*) and acetate kinase/phosphotransacetylase (*ackA-pta*). Two enzymes comprise the
54 *ackA-pta* pathway: phosphotransacetylase [EC 2.3.1.8] reversibly converts acetyl-CoA and
55 inorganic phosphate to acetyl phosphate and CoA, and acetate kinase [EC 2.7.2.1] reversibly
56 converts acetyl phosphate and ADP into acetate and ATP [4]. The two genes include one
57 operon [5] and are considered to be important for balanced carbon flux within the cell during
58 exponential growth both, aerobically and anaerobically [6, 7]. *E. coli* uses the *ackA-pta*
59 pathway as an ATP production source under anaerobic and even aerobic conditions [7].

60 The second enzyme, pyruvate oxidase [EC 1.2.2.2], is a peripheral membrane protein that
61 converts pyruvate, ubiquinone and H₂O to acetate, ubiquinol and CO₂. It has been reported to
62 be a nonessential aerobic enzyme active in the early stationary phase [8, 9]. However, more
63 recent studies has shown that pyruvate oxidase plays an important role in the aerobic growth
64 efficiency of *E. coli* [10], perhaps to preserve the pool of free CoA-SH. Dittrich et al. (2005)
65 [2] confirm that the *poxB* pathway is more active during the late exponential and stationary

66 phases, whereas the *ackA-pta* pathway is more active in the exponential stage of the cell
67 growth. They also report that the two acetate producing pathways are affected by culture
68 conditions such as pH. Acidic environments repress the *ackA-pta* pathway, but activate the
69 *poxB* pathway. In addition, acetate itself has a strong negative effect on the two pathways.

70

71 Acetate formation has several disadvantages:

- 72 • acetate concentrations above ca. 1 g/l are damaging for both the biomass production
73 and the production of recombinant proteins [11]
- 74 • besides the inhibition on recombinant protein production, acetate has a negative effect
75 on the stability of intracellular proteins [12]
- 76 • organic acids already show negative effects at concentrations much lower than those
77 for mineral acids. The non-dissociated form of acetate can move freely through the
78 cell membrane and thus accumulates in the medium. A part of this extracellular, non-
79 dissociated form will re-enter the cell and dissociate due to the higher internal pH.
80 Acetate thus acts as a proton conductor and the process causes a reduction in proton
81 motive force [13]
- 82 • accumulation of acetate in the medium will acidify the medium. When the pH is below
83 5.0, cell lysis will appear due to the irreversible denaturation of proteins and DNA
84 [14].

85 The level of acetate produced during aerobic fermentations is depending on the *E. coli* strain,
86 the growth conditions, the actual glucose concentration in the medium and the overall
87 composition of the fermentation medium. For more detailed information about why, when and
88 how bacterial cells excrete acetate, see reference [15].

89

90 Researchers have tried a wide variety of strategies to reduce acetate accumulation in high cell
91 density fed-batch *E. coli* fermentations. These strategies are situated at two levels: the
92 bioprocess level and the genetic level.

93

94 **2 Bioprocess level approaches to minimize acetate formation**

95 These methods mostly intervene in the medium composition and/or the cultivation conditions.

96 The fermentation run can be optimized by controlling a range of parameters such as
97 temperature, agitation regime, volume, foaming, dissolved oxygen tension (DOT), pH, optical
98 density, (limiting) substrate concentration, etc.

99

100 A culture of *E. coli* will generate acetate when the cells surpass a threshold specific rate of
101 glucose consumption, regardless of the availability of oxygen to the culture [3]. In the
102 literature, several specific fermentation strategies are mentioned to reduce acetate production
103 [1, 16-20]. levels were developed. These methods are based on mathematical models that
104 describe growth patterns and the expected demand for nutrients. These strategies include
105 various glucose feeding approaches [21-27], limitations of growth rate by substrate-limited
106 fed batch schemes [16, 18, 26, 28-30] and utilization of alternative feeds such as glycerol [26,
107 31], mannose [32] or fructose [33]. For example, reduced acetate and an increase in protein
108 yield have been reported when fructose was used as carbon source instead of glucose [33].
109 Also supplementing the medium has proven to be positive on reducing acetate [34]. Recently,
110 the combination of glucose pulses with an amino-acid containing feed stream has been
111 demonstrated to be successful to minimize acetate production [35]. Another approach to hold
112 the growth rate below the threshold for acetate production, is the pH-stat, where a nutrient
113 feed is activated when the pH increases and variants, where the culture is dosed with more
114 nutrient than necessary. However a fundamental drawback of the pH-stat is that it detects
115 starvation rather than the acetate threshold directly [3]. In general, a consequence of limiting
116 the growth rate is that biomass is generated at a slower rate than the cells are capable of
117 achieving.

118

119 Instead of lowering the growth rate, the produced acetate can be removed from the culture
120 during the fermentation process to reduce the inhibitory effects of acetate. In literature, the
121 use of a dialyse-fermentors is reported to remove acetate from the culture [36, 37]. Dialysis is
122 defined as the separation of solute molecules by their unequal diffusion through a semi-
123 permeable membrane based on a concentration gradient. Recently, another method to remove
124 acetate from the fermentor was reported via the use of macroporous ion-exchange resins [38].
125 However, methods to remove acetate from the culture tend to remove also nutrients. In
126 addition, this strategy do not deal with the fact that carbon is diverted to a by-product and thus
127 the economic sink.

128

129 Although, these methods are extensively used in the industry, they are not the best solutions
130 because they undermine the maximum growth and production capacity. Therefore, we will
131 emphasize genetic approaches to minimize acetate formation.

132

133 **3 Genetic approaches to minimize acetate formation**

134 Several strategies which intervene with acetate formation on the genetic level have also been
135 reported. These strategies are based on the alteration of the central metabolism of *E. coli* (see
136 figure 1, table 1). First, the effect of alterations in the glucose uptake mechanism and in the
137 TCA cycle will be discussed. The pathway from glycolysis to the TCA cycle is very
138 important because of the many reactions which play a role in the pyruvate branch point. From
139 this branch point, the carbon flux can be directed to acetate production via the genes coding
140 for acetate kinase (*ackA*), phosphotransacetylase (*pta*), acetyl-CoA synthase (*acs*) and
141 pyruvate oxidase (*poxB*). The flux can also be directed to the TCA-cycle (citrate synthase,
142 *gltA*) where the glyoxylate bypass plays an important regulation control (isocitrate lyase,

143 *ackA*; malate synthase, *aceB* and isocitrate dehydrogenase; *icd*). In a final paragraph, the
144 influence of alterations in coenzyme pools on the acetate metabolism will be discussed.

145

146 Since *E. coli* is a facultative anaerobic strain, part of the glucose (even under aerobic
147 conditions) will be catabolized via fermentation (consuming no oxygen). Besides a lower
148 energy yield per mol glucose obtained by anaerobic fermentation, this causes a faster
149 utilization of glucose by the cells, as compared with aerobic respiration. [39]. Because of the
150 occurrence of reactions which run normally anaerobically in aerobic conditions, some
151 enzymes which are active under anaerobic growth conditions will be discussed. Strictly
152 anaerobic culture strategies and strategies based on involvement of non-*E. coli* pathways (e.g.
153 *pyc* pathway) will not be discussed.

154

155 3.1 The phosphoenolpyruvate (PEP):carbohydrate phosphotransferase systems (PTSs)

156 The phosphoenolpyruvate (PEP):carbohydrate phosphotransferase systems, which are both
157 transport and sensing systems, are an example of group translocation enzymes. PTS (figure 2)
158 is involved in the transport and the phosphorylation of a large number of carbohydrates (PTS
159 carbohydrates), in the movement of cells towards these carbon sources (chemotaxis), and in
160 the regulation of a number of metabolic pathways. The PTS catalyzes the following overall
161 process:

162



164

165 Carbohydrate phosphorylation is coupled to carbohydrate translocation across the cytoplasmic
166 membrane, the energy for these processes being provided by the glycolytic intermediate PEP.

167 PTS consists of three kinds of proteins: enzyme I and histidine protein (HPr), which

168 participate in the phosphorylation of all PTS carbohydrates and thus have been called the
169 general PTS proteins, and enzyme II, which is carbohydrate specific.

170 Chou *et al.* (1994)[40], tried to reduce the acetate excretion by knocking out the *ptsG* gene,
171 coding for the glucose specific enzyme II of PTS [EC 2.7.1.69]. This method did not totally
172 prevent the uptake of glucose, but its uptake rate was reduced. Consequently, the flux through
173 the glycolysis was decreased, causing a reduced acetyl-CoA accumulation. Chou *et al.* (1994)
174 [40] observed no acetate excretion in cultures of this mutant. Similar results were found by
175 [41-43]. Moreover, Han *et al.* (2004)[41] found an increase in biomass and recombinant
176 protein production as result of knocking out *ptsG*. Another way to intervene in the PTS is to
177 influence the regulation of *ptsG*. It was found that the regulator ArcA binds to the promoter of
178 *ptsG*. Deletion of the *arcA* gene caused about a 2-fold increase in the *ptsG* expression.
179 Overexpression of *arcA* significantly decreased glucose consumption and hence decreased the
180 acetate accumulation [44]. Knocking out *ptsG* and overexpressing *arcA*, however, are a
181 genetic variant of limiting the glucose feed rate. Moreover, mutation of a PTS gene causes an
182 efficiency reduction in the energy metabolism [17].

183 However, recently it is been reported that the deletion of the ArcA gene in combination with
184 the overexpression of a heterologous NADH oxidase increased the glycolytic flux and
185 reduced acetate production [45, 46].

186

187 3.2 Pyruvate branch point

188 Many strategies of metabolic engineering are focussing on the enzymes around the pyruvate
189 branch point since the intracellular level of pyruvate has an immediate influence on acetate
190 excretion. Pyruvate is the substrate or end product of many reactions and thus an interesting
191 target for manipulation. The enzymes of the main reactions around pyruvate are: pyruvate

192 kinase (*pyk*), pyruvate dehydrogenase (*pdh*), pyruvate formate lyase (*pfl*), lactate
193 dehydrogenase (*ldh*), PEP-carboxylase (*ppc*) and PEP-carboxykinase (*pck*).

194 Lowering the pyruvate pool has been many times described in the literature as a way to
195 reduce acetate production [47, 48].

196 *Pyruvate kinase (pyk)*

197 Pyruvate kinase [PYK, EC 2.7.1.40] is one of the key enzymes of glycolysis. It catalyzes the
198 conversion of PEP into pyruvate and simultaneously converts ADP to ATP:

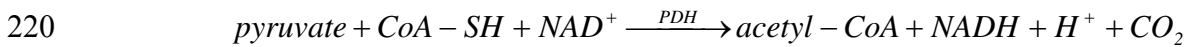


200 In almost each cell type, the flux through this reaction controls the global flux through the
201 glycolysis. There are two isoenzymes of pyruvate kinase, encoded by *pyk-I* (or *pyk-F*) and
202 *pyk-II* (or *pyk-A*). The enzyme PYK-F is activated by fructose-1,6-bisphosphate while PYK-A
203 is activated by intermediary products of the pentose phosphate pathway, such as ribose-5-
204 phosphate [49].

205 Inactivation of one or both pyruvate kinase isoenzymes has already been tried several times to
206 reduce acetate production [50-52]. Several studies have reported that the glycolysis was down
207 regulated in *E. coli pykF* mutants under aerobic conditions [50, 53]. It was found that the flux
208 through phosphoenol pyruvate carboxylase and malic enzyme were up-regulated in the *pykF*⁻
209 mutant as compared with the wild type, and acetate formation was significantly reduced in the
210 mutant. Inactivation of one *pyk*-enzyme caused a slight decrease of the maximum growth rate.

211 This indicates that the other *pyk*-enzyme can compensate for the supply of the pyruvate pool,
212 together with the PTS. Inactivation of both *pyk*-enzymes causes a major decrease in the
213 growth rate and the acetate production [51]. Emmerling *et al.* (2002) [50] reported that
214 relatively more oxaloacetate is derived from PEP and more pyruvate from malate in
215 comparison with the wild type. This mechanism is probably activated to compensate to some
216 extent for the pyruvate kinase knock-out.

217 *Pyruvate dehydrogenase (pdh), expressed under aerobic culture conditions, in E. coli*
218 Pyruvate dehydrogenase [PDH, EC 1.2.4.1] complex catalyzes the conversion of pyruvate
219 into acetyl-CoA with the formation of one molecule CO₂.



221 A too large pool of acetyl-CoA contributes to a large extent to the overflow of acetate.
222 Elmansi & Holms (1989) [54] tried to reduce the acetate excretion by decreasing the flux
223 from pyruvate to acetyl-CoA. This was achieved by adding 3-bromopyruvate, an inhibitor
224 which directly acts on the active domain of pyruvate dehydrogenase. They reported no acetate
225 production at all. However, there was still lactate produced and a decrease of the growth rate
226 with respect to the wild type was observed.

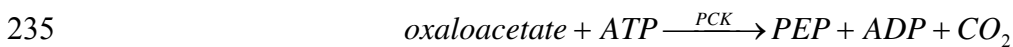
227 *PEP carboxylase (ppc) and PEP carboxykinase (pck)*

228 PEP carboxylase [PPC, EC 4.1.1.31] converts PEP into oxaloacetate and is referred as PPC
229 shunt by Noronha et al (2000) [55]:



231 This reaction is activated by acetyl-CoA, guanosinetriphosphate and fructose-1,6-biphosphate,
232 and inhibited by aspartate and malate [56].

233 PEP-carboxykinase [PCK, EC 4.1.1.49] catalyzes the reverse reaction with consumption of 1
234 molecule ATP:



236 PCK is inhibited by high levels of PEP and nucleotides [56]. The purpose of PCK is to
237 maintain the PEP:oxaloacetate ratio and stabilize the pool of intermediate products of the
238 Krebs cycle. The net reaction of the cycle formed by both reactions consumes one molecule
239 of ATP. In *E. coli* wild type strains, this futile cycle is strongly regulated. Inactivation of the
240 *pck* gene causes a decrease of PEP carboxylation and a stimulation of the glyoxylate cycle.
241 Yang et al. (2003) [57] reported that *pck* deletion mutants are able to grow on high
242 concentrations of glucose without acetate production.

243 Chao & Liao (1994) [58] decided that overexpression of both enzymes gives an increased
244 activation of the futile cycle with a higher production of fermentative products as a
245 consequence. The double overexpression was also responsible for less growth and a higher
246 consumption of glucose and oxygen. All these are consequences of the leakage of energy via
247 the futile cycle.

248 Simple overexpression of the *pck* causes a slight increase in acetate production [59]. On the
249 other hand, overexpression of *ppc* can completely eliminate acetate production [59, 60].
250 According to Chao & Liao (1993) [59], overexpression of *ppc* decreases the glucose
251 consumption rate and organic acid excretion, while growth and respiration rate remain
252 unchanged. Farmer (1997) [17] described the effect of overexpressing PPC in *E. coli* VJS632
253 aerobic cultures and conclude that the final acetate concentration is reduced by 60%. A
254 reduction of 60% of the acetate excretion by overexpression of PPC was also obtained for *E.*
255 *coli* ML308 by Holms (1996) [61]. Knocking out *ppc* has a negative effect on the overall cell
256 metabolism: growth rate is impaired and the excretion of undesirable metabolites increases
257 [60, 62, 63].

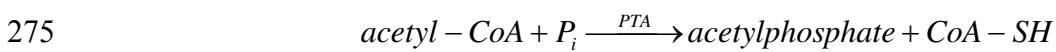
258 Noronha et al. (2000) [55] showed that the TCA cycle/PPC shunt flux ratio is differing
259 between a low acetate producer, *E. coli* BL21 and a high acetate producer, JM109. The PPC
260 shunt is active in BL21 and inactive in JM109. This was confirmed by Yang et al. (2003)
261 [57]. In contrast to the wild type, *ppc* overexpression mutants show more activity of the
262 glyoxylate bypass [57] making a higher flux through the Krebs cycle possible. This means
263 that the ratio PPC bypass:Krebscycle will decrease strongly. According to Yang et al (2003)
264 [57], this ratio is very important for the production of acetate.

265 It is generally accepted that PPC activity strongly regulates the PCK activity. In the wild type,
266 PPC is more active than PCK, firstly, to compensate for the activity of PCK and secondly, to
267 supply the Krebs cycle with sufficient intermediates. Inactivation of *pck* leads immediately to

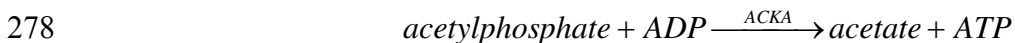
268 a decrease in PPC activity, since compensation of PCK is no longer needed [57].
269 Overexpression of *pck* deregulates this system, causing an increase of the acetate production.

270 3.3 Phosphotransacetylase (*pta*) and acetate kinase (*ackA*)

271 Phosphotransacetylase [PTA, EC 2.3.1.8] and acetate kinase [ACKA, EC 2.7.2.1] are the
272 enzymes that accomplish the production of acetate from acetyl-CoA. Phosphotransacetylase
273 catalyzes the conversion of acetyl-CoA to acetylphosphate with production of CoA-SH.
274 Phosphotransacetylase is activated by pyruvate and inhibited by $\text{NADH} + \text{H}^+$ [64]



276 Acetate kinase uses the product formed by phosphotransacetylase as substrate; this is the last
277 step of the acetate pathway.



279 Both reactions are reversible. As such, the cell can convert acetate to acetyl-CoA and
280 subsequently use it for biosynthesis reactions.

281

282 Mutations in both *pta* and *ackA* have frequently been investigated [2, 11, 54, 65]. All data
283 report a strong reduction of acetate production, when *ackA* and/or *pta* are eliminated. This is
284 at the expense of the growth rate and is accompanied by an increase in the production of other
285 fermentation products such as lactate and formate. Though lactate and formate are less toxic
286 to the cells, they are still disadvantageous for cell growth.

287

288 3.4 Acetyl-CoA synthetase (*acs*)

289 When glucose is used in high cell density cultures, acetate is produced and excreted in the
290 medium. Acetyl-CoA synthetase [ACS, EC 6.2.1.1] can use the re-absorbed acetate and

291 convert it to acetyl-CoA via a two step reaction scheme. These reactions are irreversible and
292 thus they are only responsible for acetate consumption and not for acetate production.



294 The enzyme has a strong affinity for acetate (Km of 200µM), which allows it to function at
295 low acetate concentrations, but it is inhibited by glucose [66, 67]. On the other hand, the
296 reversible *ackA-pta* pathway can assimilate acetate only at high acetate concentrations [15].

297

298 Contiero *et al.* (2000) [11] investigated the effect of the deletion of *acs* on the growth on
299 glucose at high cell densities in fed-batch fermentations. No clear conclusion could be drawn
300 from their research. It only indicated that acetyl-CoA plays a key role in accomplishing high
301 cell densities and has no or few importance during normal growth.

302 The overexpression of *acs* in *E. coli* resulted in a significant reduction in acetate formation
303 during glucose metabolism. It also enhanced the assimilation of acetate when used as the sole
304 carbon source. These characteristics guarantee *acs* overexpression as a positive approach to
305 coping with acetate in *E. coli* fermentations [68].

306

307 3.5 Pyruvate oxidase (*poxB*)

308 Pyruvate oxidase [POXB, EC 1.2.2.2] catalyses the oxidative carboxylation of pyruvate to
309 acetate and CO₂ [69]. This ‘non-essential’ enzyme is a part of the respiratory chain.

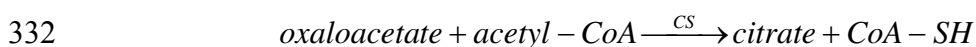


311 An elevated intracellular concentration of pyruvate activates this enzyme, suggesting that
312 POXB regulates the flux partitioning of pyruvate, presumable to reduce the carbon flux
313 towards acetyl-CoA in order to maintain the intracellular pool of CoA for other metabolic
314 functions [10]. Abdel-Hamid *et al.* (2001) [10] investigated the function of *poxB* in *E. coli* by

315 knock-out mutants. Inactivation of *poxB* results in a decrease of 24% of the carbon converted
316 into biomass. The amount of carbon necessary for energy production increased with 23%.
317 They concluded that puruvate oxidase is essential for a good functioning of the overall
318 metabolism. They advised not to use *poxB* as target to decrease acetate production. However,
319 Causey et al. (2004), have reported the beneficial effect of *poxB*⁻ mutation on pyruvate
320 production and cell growth. The relationship between POXB and acetate formation has been
321 studied. Vemuri et al. (2005) [70] studied the physiological response of *Escherichia coli*
322 central metabolism to the expression of heterologous pyruvate carboxylase (PYC) in the
323 presence or absence of pyruvate oxidase. The presence of PYC activity in *E. coli* substantially
324 increases the cell yield from glucose, particularly for a *poxB* mutant, biomass which appears
325 to be derived directly or indirectly from acetate [70]. Recently, a *poxB* knockout strain (and
326 also knockouts in *ldhA* and *pflB* genes) demonstrated significantly reduced acetate formation
327 when the strain was subjected to oscillatory oxygenation [71].

328 3.6 Citrate synthase (*gltA*)

329 Citrate synthase [CS, EC 2.3.1.1] is the first enzyme of the Krebs cycle. It delivers acetyl-
330 CoA in the cycle via binding with oxaloacetate. During this reaction one molecule of citrate is
331 formed.



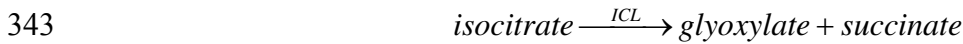
333 Citrate synthase is inhibited by α -ketoglutarate and activated by $\text{NADH} + \text{H}^+$ [56]

334 This reaction is often indicated as the rate limiting step of the Krebs cycle. Overexpression of
335 *gltA* showed a decrease of acetate production but no real elimination of it [60]. Knocking out
336 *gltA* caused a strong increase of the acetate production, accompanied by an increase in
337 formate and pyruvate excretion [72].

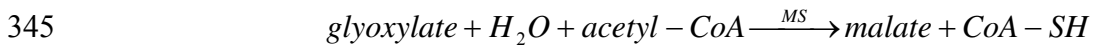
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339 3.7 Isocitrate lyase (*aceA*), malate synthase (*aceB*) and isocitrate dehydrogenase (*icd*)

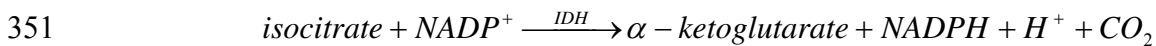
340 Isocitrate lyase [ICL, EC 4.1.3.1] and malate synthase [MS, EC 2.3.3.9] catalyse the reactions
341 of the glyoxylate bypass. Isocitrate lyase converts isocitrate in one molecule succinate and
342 one molecule glyoxylate.



344 Malate synthase convert glyoxylate and acetyl-CoA into one molecule malate.



346 Besides their role in the Krebs cycle, oxaloacetate and α -ketoglutarate are also used for
347 further biosyntheses. This can cause an exhaustion of the Krebs cycle intermediates, because
348 of the continuous need for those essential intermediates. The glyoxylate bypass has as goal to
349 provide the Krebs cycle with additional oxaloacetate. The switch over from the Krebs cycle to
350 the glyoxylate bypass occurs at the isocitrate dehydrogenase [IDH, EC 1.1.1.42] step.



352 Isocitrate dehydrogenase has more affinity for isocitrate than isocitrate lyase. This regulation
353 takes place by reversible phosphorylation of isocitrate dehydrogenase under the influence of
354 the intracellular oxaloacetate level. At high levels of oxaloacetate, isocitrate dehydrogenase is
355 phosphorylated; this phosphorylated form of isocitrate dehydrogenase is not active and as a
356 result, the glyoxylate shunt is activated [57].

357

358 Aoshima et al. (2003) [73] found that knocking out isocitrate dehydrogenase results in an
359 increase of citrate. El-Mansi *et al.* (1994) [74] tried to delete the glyoxylate shunt by
360 overexpression of isocitrate dehydrogenase. Because of this, the flux through isocitrate lyase
361 decreased, but the intracellular pool of isocitrate became exhausted; they concluded that
362 isocitrate dehydrogenase is not the rate limiting step in the Krebs cycle. Farmer and Liao
363 (1997) [17] stimulated the flux through the glyoxylate shunt by inactivation of the *fadR*

364 operon. This operon negatively controls the expression of isocitrate lyase and malate
365 synthase. Acetate production decreased with 13% by stimulating the glyoxylate shunt.

366

367 Yang et al. (2003) [57] concluded that the glyoxylate bypass is of big importance in the
368 regulation of the ratio PPC-shunt/Krebs cycle. A high ratio should give a higher acetate
369 production. When the oxaloacetate concentration in the cell is too low, the balance between
370 the glycolyse and the Krebs cycle is deregulated, causing acetate production. It has also been
371 observed that the glyoxylate shunt is active in a low acetate producer, while it is inactive in a
372 high acetate producer [55].

373

374 3.8 Alterations in the coenzyme pools

375 Most current metabolic engineering studies have focused on enzyme levels and on the effect of
376 amplification, addition, or deletion of a particular pathway.

377 When enzyme levels are not limiting, the availability and occurrence of coenzymes can
378 become limiting. It is conceivable that in coenzyme-dependent production systems, coenzyme
379 availability and the proportion of coenzyme in the active form may play an important role in
380 dictating the overall process yield. Hence, the manipulation of these coenzyme levels may be
381 crucial in order to further increase production [75-78].

382 $NADH+H^+/NAD^+$

383 NAD^+ plays a significant role in primary metabolism. It is a coenzyme of more than 300
384 redox reactions. By using this coenzyme, the cell can maintain its redox state in balance.

385 NAD^+ and $NADH+H^+$ play a major role in catabolism. To catabolize glucose into precursors,
386 NAD^+ is used as coenzyme and converted to $NADH+H^+$. In anabolism, $NADP^+$ and
387 $NADPH+H^+$ occur more frequently, but with a similar function. The cell regenerates the
388 produced $NADH+H^+$ into NAD^+ by the reduction of oxygen (under aerobic conditions), or via

389 another oxidising product or via fermentation. It is also generally known that the ratio
390 $\text{NADH}+\text{H}^+/\text{NAD}^+$ regulates the expression of certain genes, such as *adhE*, coding for alcohol
391 dehydrogenase [EC 1.1.1.1], and the activity of certain enzymes, such as the enzymes of the
392 pyruvate dehydrogenase complex [75].

393 Berrios-Rivera et al. (2002) [75] investigated mainly alterations in the ratio
394 $\text{NADH}+\text{H}^+/\text{NAD}^+$. Under aerobic conditions, formate was added to activate pathways that
395 normally do not function. The results were depending on whether the formate dehydrogenase
396 was endogenous or not (originating from *Candida boidinii*). Adding formate to the strain with
397 the cell-own formate dehydrogenase under aerobic conditions resulted in a large increase in
398 the acetate production compared to the strain with the heterologous enzyme, were a small
399 increase of the acetate production was observed [75].

400 Acetate overflow at high glucose consumption rates is believed to result from an enzymatic
401 limitation in the TCA cycle causing excess carbon from glycolysis to be shunted acetate or
402 from a saturation of the respiratory pathways used to reoxidize NADH [46]. Since the
403 glycolysis and TCA cycle generate NADH while acetate formation does not, saturation of
404 NADH oxidation at high glucose consumption rates could cause the cell to form acetate in
405 order to modulate the redox balance [45]. Recently a strong link was demonstrated between
406 redox ratio (in vivo molar concentration ratio NADH/NAD) and acetate overflow metabolism
407 in *E. coli* [45]. The authors revealed that the initiation of acetate overflow metabolism
408 occurred above a critical NADH/NAD ratio of 0.06. In addition, the acetate production could
409 be delayed by the expression of the heterologous NADH oxidase. Expression of the
410 heterologous NADH oxidase coupled with the deletion of the regulatory *arcA* gene in *E. coli*,
411 increased the glycolytic flux and reduced acetate production [46]. The presence of the
412 heterologous NADH oxidase or the absence of ArcA reduced acetate about 50% and
413 increased the recombinant protein production by 10-20%. The presence of the heterologous

414 NADH oxidase in the *arcA* knock-out strain eliminated acetate production entirely in batch
415 fermentations and resulted in a 120% increase in the recombinant protein production.

416 *Coenzyme A (CoA-SH)*

417 A second important type of coenzymes is coenzyme A and its derivatives (acetyl-CoA,
418 succinyl-CoA,...). Acetyl-CoA is an essential intermediate in many energy yielding
419 processes. More than 100 different reactions of the central metabolism depend on this
420 substrate. It is the main source of activity of the Krebs cycle [78].

421 The intracellular pool contains mainly short chain CoA-thioesters such as acetyl-CoA and
422 succinyl-CoA. CoA A-thioesters of long chain fatty acids form the intermediates of the β -
423 oxidation route and in the production of phospholipids. Besides the major role of CoA-SH in
424 these pathways, it has a substantial regulatory effect. CoA-SH inhibits or activates reactions
425 of the central metabolism and of the fatty acid biosynthesis [79].

426 The ratio acetyl-CoA/free acetyl-CoA is constant in *E. coli* cells grown on glucose. This ratio
427 might regulate certain enzymes of the central metabolism [56].

428 San et al. (2002) [78] investigated the production and availability of CoA-SH by means of the
429 biosynthesis of isoamylacetate. This pathway does not occur in *E. coli* wild type cells. Acetyl-
430 CoA is used as substrate for the production of isoamylacetate and thus manipulation of the
431 CoA-SH pool influences the production of isoamyl acetate. Pantothenate kinase is the rate
432 limiting step in the CoA-SH production. This enzyme is inhibited by CoA-SH and acetyl-
433 CoA. San et al. (2002) [78] observed small differences in the central metabolism when *coaA*
434 is overexpressed. Acetate and ethanol concentration increased hardly with respect to the
435 isoamyl acetate level, which increased 3 times.

436 3.9 Alteration in ATP level

437 Metabolic control theory postulates that flux control can be shared by many enzymes in a
438 pathway and that control could also reside outside the pathway, for instance, in the process
439 that consumes the ATP generated in the glycolysis (ATP demand). Koebmann et al. (2002)
440 [80] investigated whether ATP consumption by cellular processes determines the steady-state
441 flux through glycolysis, by increasing the current ATP consumption rate. Therefore, they
442 introduced an ATP-consuming process that does not interfere with other aspects of
443 metabolism. The added ATP activity resulted in up to 70% increase in the rate of glycolysis
444 and they estimate that major control (>75%) resides outside the glycolysis, i.e., in enzymes
445 that consume ATP.

446

447 **4 Conclusion and perspectives**

448 Over the last 20 years, substantial research efforts have been spent to reduce acetate
449 accumulation during aerobic growth of *E. coli* on glucose. From the onset it was clear that this
450 quest should not be simple. Simple deletion of the acetate pathway, reduced the acetate
451 accumulation, but instead other by-products were formed. From the current state of the
452 literature, we can conclude that reduction of acetate requires a multigene action. In particular,
453 one has to pay attention to the regulation of futile cycles, anapleurotic pathways, coenzyme
454 levels, acetate producing pathways and ATP consuming pathways. The expression of the
455 heterologous NADH oxidase in an *arcA* knock-out strain seems promising. However, the
456 intuitive prediction of the manipulation consequences of several genes is difficult. In most
457 cases the construction of a producer strain did not turn out to be as straightforward as was
458 initially anticipated. Indeed, in complex metabolic networks, it is often a difficult task to ad
459 hoc predict the impact, both qualitatively and quantitatively, of a genetic intervention [81].
460 Moreover, as the focus in metabolic engineering is shifting from massive overexpression and

461 inactivation of genes towards the fine tuning of gene expression [82-90], the need for a
462 reliable, quantitative predictor, i.e. a model, is rapidly growing. The use of metabolic flux
463 analysis is vital here. Metabolic models allow a better prediction of genetic interventions and
464 can help to predict the construction of the ideal *E. coli* phenotype.

465

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734 **Figure legends**

735 **Figure 1. The central metabolism of *Escherichia coli***

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737 **Figure 2. PTS-system and regulation**

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739 **Tables**740 **Table 1. Influence of genetic approaches to minimize acetate formation. Abbreviations: KO: knock-out; OE: overexpression**

pathway	gene	protein	KO/OE	result	reference
PTS	<i>ptsG</i>	glucose specific enzyme II	KO	glycolyse flux ↓, no acetate excretion	[40]
				energy metabolism ↓	[17]
				acetate ↓	[43]
				growth rate ↓, flux to TCA cycle ↑	[42]
				acetate ↓, recombinant protein ↑, biomass ↑	[41]
	<i>arcA</i>	regulator <i>ptsG</i>	KO	<i>ptsG</i> ↑	[44]

			OE	glucose consumption ↓ acetate accumulation ↓	[44]
			KO <i>ptsG</i> , <i>pykF</i> and <i>pykA</i>	acetate ↓	[43, 91]
Glycolyse	<i>pfk</i>	phosphofructokinase	OE	ethanol ↓, lactate and acetate ↑	[92]
Pyruvate branchpoint	<i>pyk</i>	pyruvate kinase	KO	KO_1: growth rate and acetate ↓	[50]
				KO_2: growth rate and acetate ↓↓	[51]
			KO <i>PykF</i>		[53]
	<i>pdh</i>	pyruvate dehydrogenase	Inhibition PDH	no acetate production, growth rate ↓, lactate ↑	[93]
	<i>pfl</i>	pyruvate formate lyase	KO	lactate ↑, small ↓ flux acetyl CoA to acetate	[94-96]
	<i>ldh</i>	lactate dehydrogenase	OE	acetate ↓	[97]
			KO <i>pfl</i> and <i>ldh</i>	acetate and lactate ↓, malate ↑	[98]

	<i>ppc</i>	PEP carboxylase	KO	acetate ↓, growth rate ↓, glyoxylate shunt ↑, glycolysis and PPpw ↓	[60, 62, 63]
			OE	no/↓ acetate , growth yield ↑,	[17, 59-61]
	<i>pck</i>	PEP carboxykinase	KO	PEP carboxylation ↓, glyoxylate ↑, no acetate on high glucose	[57]
			OE	acetate ↑	[59]
			OE <i>ppc</i> and <i>pck</i>	fermentative products ↑, growth yield ↓	[58]
			OE <i>ppc</i> or <i>pck</i>	PPC bypass: Krebscycle ↓↓	[55, 57]
	<i>ackA</i>	acetate kinase	KO <i>ackA</i> or <i>pta</i>	acetate ↓↓, growth rate ↓, formate and lactate ↑	[2, 11, 54, 97, 99]
	<i>pta</i>	phosphotransacetylase			
	<i>acs</i>	acetyl-CoA synthetase	KO	no clear conclusions	[11]

			OE	acetate ↓↓	[68]
	<i>poxB</i>	pyruvate oxidase	KO	C-yield ↓↓	[10]
	<i>gltA</i>	citrate synthase	KO	acetate ↑↑, pyruvate and formate ↑	[72]
			OE	acetate ↓	[60]
	<i>aceA</i>	isocitrate lyase	stimulation shunt	acetate ↓	[17]
	<i>aceB</i>	malate synthase			
	<i>icd</i>	isocitrate dehydrogenase	KO	accumulation citrate	[73]
			OE	no rate limiting step Krebs	[74]

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