

New Insight into Partial Denitrification (PD)-based Anammox Process and Potential Engineering Application: A Review

Fahmi Bahtiar¹, Xingxing Zhang¹, Yuguang Wang¹, Chaochao Wang¹, Yunkang Xia¹, Peng Wu^{1,2,3}, Lezhong Xu^{1,2,3,*}

¹School of Environmental Science and Engineering, Suzhou University of Science and Technology, Suzhou, China

²National and Local Joint Engineering Laboratory of Municipal Sewage Resource Utilization Technology, Suzhou, China

³Jiangsu Collaborative Innovation Center of Technology and Material of Water Treatment, Suzhou, China

Email address:

kgre505@163.com (Lezhong Xu)

*Corresponding author

To cite this article:

Fahmi Bahtiar, Xingxing Zhang, Yuguang Wang, Chaochao Wang, Yunkang Xia, Peng Wu, Lezhong Xu. New Insight into Partial Denitrification (PD)-based Anammox Process and Potential Engineering Application: A Review. *Journal of Health and Environmental Research*. Vol. 6, No. 3, 2020, pp. 79-86. doi: 10.11648/j.jher.20200603.15

Received: July 16, 2020; **Accepted:** July 29, 2020; **Published:** August 4, 2020

Abstract: Recently reported partial denitrification (PD, $\text{NO}_3^- \text{-N} \rightarrow \text{NO}_2^- \text{-N}$) has attracted extensive attention as a novel promising alternative for anaerobic ammonium oxidation (anammox)-based process. Flexible and stable nitrite ($\text{NO}_2^- \text{-N}$) supply via PD provides substantial electron acceptors for sustainable and economic anammox wastewater treatment with simple control and minimal cost. However, our understanding of researches on PD-based anammox processes applied in biological wastewater treatment is still limited. Given obviously advantages for PD-based anammox (PDA) coupling process held and countless researches have been developed, the major objective of this study was to review the latest advances of which, key influencing factors, principled characteristics and economical analyses. Comprehensive knowledge of PDA engineering application prospects were also helpful to deepen our understanding of its practices, i.e., advanced nitrogen removal from tertiary municipal sewage, post-anammox treatment of nitrogen-rich wastewater and simultaneous nitrogen removal from domestic and nitrate ($\text{NO}_3^- \text{-N}$) contained wastewater. Ultimately, future researches trend of PDA was prospected to enlarge its application into full-scale wastewater treatment. In summary, PD-based anammox process held obvious advantages in actual wastewater treatment through efficiently ammonia and nitrate removal, providing a new insight into retrofitting current wastewater treatment plants. Additionally, more attention should be paid to exploring the complicated metabolic network of different types of bacteria in the PD and anammox integration system.

Keywords: Partial Denitrification (PD), Anammox, Biological Nitrogen Removal, Coupling Process, Engineering Application

1. Introduction

Conventional biological nitrification-denitrification process has been widely developed in current municipal wastewater treatment plants (MWTPs), in which aerobic nitrifying bacteria converted ammonium ($\text{NH}_4^+ \text{-N}$) into nitrate ($\text{NO}_3^- \text{-N}$) with oxygen (O_2) as electron acceptor, followed by anoxic denitrifying bacteria would conduct denitrification to reduce $\text{NO}_3^- \text{-N}$ to nitrogen gas under sufficient organic

condition [1, 2]. However, large amount of aeration investment and chemical addition resulted in energy-intensive process, which was far away from future-oriented novel concept MWTPs in China. Anaerobic ammonium oxidation (anammox) process has attracted extensive attention as an energy-efficient and environmental-friendly strategy to retrofit existing plants, because of its obvious advantages such as 60% lack in oxygen demand, 100% decrease in organic carbon requirement and less/no N_2O (global warming

potential of 310) emission [3, 4]. In this technology, the ratio of $\text{NH}_4^+\text{-N}$ to $\text{NO}_2^-\text{-N}$ about 1:1.30 is needed for anammox, whereas the latter substrate was rarely discovered in the real wastewater [5]. This means $\text{NO}_2^-\text{-N}$ production process is indispensable for anammox engineering practices.

Recently, the high $\text{NO}_2^-\text{-N}$ producing from $\text{NO}_3^-\text{-N}$ reduction was observed in partial denitrification (PD, $\text{NO}_3^-\text{-N} \rightarrow \text{NO}_2^-\text{-N}$) process and over 80% nitrate-to-nitrite transformation ratio (NTR) was obtained [6, 7], indicating a more stable alternative to providing substrate for anammox bacteria compared with current extensively studied partial nitrification technology [8]. Cao et al. firstly enriched $\text{NO}_2^-\text{-N}$ accumulation sludge using sludge fermentation liquid as external organics and a robust high nitrite of 20.91 ± 0.52 mg/L was obtained in a 108-day operation [6]. Du et al. proposed a novel two-stage PD and anammox process in two isolated sequencing batch reactors (SBRs), where anammox-SBR nitrate effluent was fed into post PD-SBR to operate $\text{NO}_3^-\text{-N}$ reduction process with $\text{NO}_2^-\text{-N}$ as final product, and then $\text{NO}_2^-\text{-N}$ backflow to anammox-SBR for the purpose of advanced nitrogen removal [9]. Moreover, a single-reactor (i.e., upflow anaerobic sludge blanket, UASB) for simultaneous PDA was also developed, a 225-days operation demonstrated that the relatively low total nitrogen (TN) effluent concentration of 6.56 mg/L achieved even in a cold temperature (17.5°C). These experimental results provided a new insight on the nitrogen removal when combined with economical and sustainable anammox process, thus gave a summary and discussion on the current status of researches and future perspectives of PDA seemed necessary [8]. Our view was shifted to this promising coupling process and considerable novel outcomes were noticed, including influencing factors, principled characteristics, and economical analyses to elucidate this significant cost-effective method. This would lessen our knowledge gap for PDA latest researches.

Increasing interest focused on combining PD with anammox for treating $\text{NH}_4^+\text{-N}$ and $\text{NO}_3^-\text{-N}$ contained wastewater, and numerous lab-scale actual wastewater treatment by PDA has been reported, i.e., domestic and nitrate contained wastewater (simulated industrial nitrate wastewater) [10-12], tertiary/secondary municipal sewage [13-16], high strength anammox-based wastewater [9, 17-20]. Nevertheless, there has been limited literature to show us comprehensive knowledge of PDA potential application, which might accelerate the popularization of PDA process. Last but not least, future trends for applications in extensive wastewater treatment and the issues that merit further study were pointed out to quickly establish a full-scale PDA process.

2. Characteristics of PDA Coupling Process

As we all known, the key reason for efficient nitrogen removal via PDA process was the coexistence of diverse microbial flora, owing to PD biomass known as classical

heterotrophic bacteria along with intense proliferation growth might lead to autotrophic anammox bacteria possibly inhibited. Notably, maintaining dominant anammox nitrogen removal pathway was essential, since researchers have reported that anammox contributed more than 95% nitrogen removal in PDA [11]. On the other hand, PD occurred ahead of anammox was a prerequisite due to $\text{NO}_2^-\text{-N}$ -electron acceptor supply must be warranted for anammox microbes [1]. Additional, denitrifying bacteria would compete for $\text{NO}_2^-\text{-N}$ with anammox and destroy the effluent quality once the latter activity was suppressed [21, 22]. Overall, how to balance the activity among the PD and anammox biomass was of importance to gaining satisfactory nitrogen removal. Here we showed that critical factors influenced the PDA coupling process and principled characteristics of it, moreover, economical analyses were conducted to highlight the predominant advantages.

2.1. Key Influencing Factors

2.1.1. Carbon Sources

PD organisms was considered easily exploit small molecule organics to conduct denitrification process [23, 24]. The type of carbon source can significantly influence the $\text{NO}_2^-\text{-N}$ accumulation performance. It could be attributed by diverse organics affected the selection and enrichment of $\text{NO}_2^-\text{-N}$ -accumulating bacteria [24], and the discrepancy of $\text{NO}_3^-\text{-N}$ and $\text{NO}_2^-\text{-N}$ reduction rates would also emerge [7, 25]. Previous literatures have evidenced that simple micromolecule organic materials could easily harvest $\text{NO}_2^-\text{-N}$ accumulating organisms compared with complex carbon source. For instance, ethanol [26], methanol [23], acetate [27], even the biodegradable organics in urban sewage were exploited as denitrifiers electronic donors. However, easily biodegradable organics were rarely detected in current practical wastewater, i.e., municipal wastewater, sludge digestion solution and manufacturing wastewater. Therefore, external carbon sources were frequently added into PDA reactor to support $\text{NO}_2^-\text{-N}$ production when applied in actual wastewater. Du et al. conducted two sludge nitrification and PDA reactor to treat real municipal sewage and artificial nitrate wastewater with sodium acetate solution as external organics, achieving as low as 5 mg/L TN effluent despite frequent temperature fluctuations ($16.3\sim 25.7^\circ\text{C}$) [10]. In addition, Ji et al. successfully coupled in-situ fermentation with PDA in a single reactor for advanced nitrogen removal from domestic and nitrate-containing wastewater, and the slowly biodegradable organics could be hydrolyzed and acidized to volatile fatty acids (VFAs) via fermentation, thus in-situ carbon source generated for further $\text{NO}_3^-\text{-N}$ reduction without external addition [11]. This provided new insight into practical application of PDA in a cost-effective and environmental-friendly way.

Endogenous partial denitrification (EPD) driven by denitrifying glycogen accumulating organisms (DGAOs) provided another alternative to produce $\text{NO}_2^-\text{-N}$ in mainstream anammox-based systems [28]. Previous researches

demonstrated that DGAOs played an important role in nitrogen removal by sufficiently utilizing the organic carbon in raw wastewater to form intracellular poly-hydroxyalkanoates (PHAs) and then use them to conduct denitrification, and a high NTR of 88.7% obtained even as reactor temperature was decreased from 25°C to 13.5°C [29]. It could be concluded that EPD system has the potential to provide stable NO_2^- -N for mainstream anammox though exposed to low temperature. A novel SNPR process was established which based on anammox, endogenous partial-denitrification and denitrifying dephosphatation to treat mainstream wastewater and excellent removal performance was achieved. Anammox pathway was proved to contribute 82.9% of the overall nitrogen removal because of the stable NO_2^- -N production from NO_3^- -N via EPD [30]. This indicated that the novel SNPR process has promising prospect to obtain advanced nitrogen and phosphorus removal in the mainstream of wastewater treatment plants.

2.1.2. COD/ NO_3^- -N

Limited COD/ NO_3^- -N means low level COD or sufficient NO_3^- -N in raw wastewater, which was critical factor for terminating NO_3^- -N reduction only to NO_2^- -N. The ratio of COD/ NO_3^- -N largely determined the denitrification process and controlled the reduction rate of NO_3^- -N [26]. Widely reported appropriate COD/ NO_3^- -N ratio for PD process ranged from 2.0~3.5, of which high NTR performance and anammox bacteria suitable influent substrate (NH_4^+ -N/ NO_2^- -N=1.30) could be available [8, 22, 31]. However, chemoautotrophic anammox bacteria directly converted NH_4^+ -N and NO_2^- -N into nitrogen gas without carbon source addition and organics played a negative role in this process [32]. On the other hand, when the influent contains suitable organics, the nitrogen removal efficiency can be enhanced by denitrification. It was reported that the nitrogen removal efficiency of the anammox process was improved at a COD/N ratio of 0.8 [33]. The effect of COD/N ratio on completely autotrophic nitrogen removal over nitrite (CANON) process was also investigated, the high COD/N ratio performed suppression on the bioactivity and biodiversity of both AOB (ammonia-oxidizing bacteria) and anammox bacteria, the suppressing threshold of COD/N ratio 1.7 was favorable for nitrogen removal [34, 35]. Thus, pretreatment of high strength organics wastewater should be performed to alleviate excess COD cause completely denitrification and avoid organic toxicity for anammox bacteria.

2.1.3. pH

The high pH was considered as an effective strategy to accumulate NO_2^- -N in the development of denitrification process [24, 36]. The reduction of NO_3^- -N to N_2 in denitrification is a consecutive four-step enzymatic reaction, which was related to the electronic reception, transmission and consumption [8]. High pH would reduce the rate of carbon oxidation in denitrification process, and further intensified the electronic competition between denitrifying enzymes [37]. Long-term or short-term effect of high pH on NO_2^- -N

accumulation rate (NAR) were investigated [24, 36], and as high as 57% NAR achieved during 420-day operation under pH of 9.0 [36]. Similarly, anammox communities had high activities in alkaline environment and pH of 7.5~8.5 was prior to anammox bacterial proliferation [38]. In general, high alkalinity conditions were not usually found in actual wastewater. It is of noted that, denitrification process consumed hydrogen ions and generated hydrogen peroxide, thus pH of the system significantly increased. The phenomenon was termed as denitrification self-alkalization [39, 40]. Previous study reported that the self-alkalization of denitrifying automatic circulation (DAC) reactor resulted in a large increase of pH up to 9.20 and caused a tremendous accumulation of NO_2^- -N up to 451.1 ± 49.0 mgN/L at NO_3^- -N loading rate (NLR) of 55 kgN/(m³·d) [39]. For this reason, the alkaline micro-environment was easy to form whether in a two-stage or single-stage PDA system, and there was no need to increase the influent pH with chemicals addition. This further confirmed the feasibility of coupling PD with anammox to treat NH_4^+ -N and NO_3^- -N containing wastewater.

2.1.4. Sludge Morphology

Flocs, granular aggregates and biofilms were the common life forms of microbe. Resisting adverse environments and facilitating the exchange of products and signal between bacteria were attractive features in granules and biofilms [41]. At present, granule-based PD sludge became a hot topic of researchers, high-loading or low-loading rate were used to explore the granulation of PD sludge, granulation mechanism and superior NTR performance were obtained [42-44]. Nevertheless, there has been broad gaps for us to understand the NO_2^- -N accumulation performance via biofilm-based PD process. More efforts should be taken to enrich PD biofilm carriers, which would be significant to provide stable electron acceptors for anammox bacteria. The current study described the start-up of PDA process with mature PD and anammox flocculent or granule mixture sludge as inoculum [12, 13], also DENitrifying AMmonium OXidation (DEAMOX) biomass [45, 46]. Furthermore, Zhang et al. firstly established a novel biofilm DEAMOX system in a sequencing biofilm batch reactor (SBBR) for actual wastewater treatment, after 240 days of operation, TN removal efficiency maintained at 93.0% with biofilm growth [47]. High anammox activity was obtained in biofilms implied that mature biofilms formed on carriers and the anammox bacteria were sufficient enriched in DEAMOX-SBBR system [47].

2.2. Principled Characteristics

Two- and single-stage reactors were the common form of PDA process. The separation technology was the two independent process in which NO_2^- -N generation and nitrogen removal with PD microorganisms and anammox bacteria as the absolute dominant community, effectively avoiding the microbe competition on NO_2^- -N substrate and living space. In this fashion, the carbon source was fully utilized by denitrifiers to significantly reduce the organic matter into the

post-anammox reactor. For example, municipal sewage and industrial nitrate wastewater firstly entered the PD reactor, and NO_3^- -N reduction easily occurred by utilizing biotic carbon source in raw wastewater. However, because of the low molecule carbon source content, it was necessary to invest external electron donor to achieve appropriate anammox reaction of NO_2^- -N/ NH_4^+ -N=1.32. Subsequently, the effluent was recycled to PD reactor for deep-level nutrient removal [9, 27]. Cao et al. established an innovative two-stage PDA process was applied to remove the nitrate nitrogen (20-40 mg N/L) from municipal secondary effluent, with raw wastewater providing organic matters for denitrifiers, the final effluent TN and COD concentration were as low as 4.0 mg N/L and 30.1 mg/L [13]. Du et al. optimized the feeding ratio between the two type wastewaters and external carbon dosage to obtain satisfactory effluent nitrogen concentration even though high-strength nitrate wastewater introduced (1000 mg N/L), the excellent removal efficiency of NO_3^- -N and NH_4^+ -N achieved 95.8% and 92.8%, respectively [27].

Based on the recently results, there was a positive correlation between anammox and denitrification bacteria activity, and the synergism of which microbes greatly improved the system TN removal performance [32, 48, 49]. Li et al. found that the transformation of anoxic area of municipal sewage plant into MBBR enhanced the loss of nitrogen in the system, and took samples for metagenome sequencing and mass balance analysis [14]. It was proved that the up-regulation of nitrate reductase gene in anoxic carrier biofilm improved the NTR performance, promoted the growth of anammox in the mainstream process, which greatly enhanced the denitrification in the continuous flow of domestic sewage treatment [14]. A single-stage reactor was based on the in-situ reduction of NO_3^- -N by denitrifying bacteria and supplied NO_2^- -N to anammox to directly remove NH_4^+ -N and NO_2^- -N simultaneously. Anammox biomass can utilize a small amount of carbon source and NO_3^- -N under anaerobic condition, which made it show resistant to high C/N ratio wastewater.

2.3. Economical Analyses

PD-based anammox technology held great economical advantages in terms of oxygen consumption, carbon demand, biomass production as well as CO_2 production. No oxygen was consumed (100% savings), 1.14 g COD was required (80.0% savings), and 0.44 g MLVSS was produced (64.8% fewer) in the PD-Anammox process compared with conventional nitrification/denitrification process, demonstrating the PD-Anammox process was economically favorable [13]. Cao et al. compared the PDA and PNA aeration depletion in a 100000 m^3/d full-scale wastewater treatment plant, the calculated results showed that 23760 kg oxygen would be consumed in the integrated PDA process, which was 4.3% lower than that of the PNA process (24780 kg) [50]. The reason for this was that a portion of the influent organic matter was diverted to the PDA reactor for denitrification rather than being oxidized in the pretreatment stage, which reduced the

overall oxygen consumption. Therefore, the integrated PDA process was comparable with the PNA process in terms of aeration requirements and organic matter recovery as biogas.

As for retrofitting currently conventional denitrifying biofilter (DNBF) to a novel economically attractive denitrification/anammox biofilter (DABF) for nitrate removal from secondary effluent [15, 51, 52], Ma et al. found that organic carbon source consumption and backwash sludge production in the DABF were significantly reduced by 63% and 70% compared with DNBF, respectively [51]. Outstanding economical advantages such as saving 7.9% of aeration consumption, 56.8% of carbon source cost, 20.2% of sludge production, and 28.1% of CO_2 emission were elucidated in a A/A/O wastewater treatment plant with post-DABF process [15]. PDA biofilter was confirmed to be a feasible process to advanced wastewater treatment, which could save aeration consumption and carbon source addition, and reduce sludge production.

3. Recent Advances in PDA Coupling Process

3.1. Advanced Nitrogen Removal from Tertiary Municipal Sewage

High nitrate concentration in the final effluent of wastewater treatment plants (WWTPs), could not meet the increasing stringent discharge limits and challenged energy-autarky or even energy-positive WWTPs in future. Denitrification was usually developed in the NO_3^- -N reduction process of secondary effluent. But too much organic materials addition and excess waste sludge seriously deviated from the sustainable development goal of economic and environmental. Previous study has showed that two-stage PDA process could support the secondary effluent treatment, the NO_3^- -N wastewater was firstly fed to PD reactor to produce NO_2^- -N along with the low carbon/nitrogen ratio (C/N) municipal sewage, then the effluent from PD was pumped to the anammox reactor for further nitrogen removal, the excellent removal efficiency of NH_4^+ -N, NO_3^- -N and COD were 95.2%, 97.9% and 81.6%, respectively [13]. Additionally, DNBF was thought to be a feasible strategy for further NO_3^- -N reduction, whereas abundant carbon source addition and frequent backwash operation was involved due to relatively high sludge yield [15, 51, 52]. For this reason, DABF was constructed for removing NO_3^- -N from secondary effluent with carbon source in raw wastewater as electronic donor, nitrogen balance analysis revealed that 93% of N_2 produced in DABF was via anammox, DABF biofilm reduced NO_2^- -N using NH_4^+ -N as the electron donor, and accumulated NO_2^- -N during denitrification, thus providing NO_2^- -N for the anammox bacteria [51]. More than 80% TN removal was available with the average effluent TN concentration was 7.82 mg/L, indicated the promising PDA biofilter technology once in practical application.

3.2. Post-anammox Treatment of Nitrogen-Rich Wastewater

The developed industrial activities produced a large amount of industrial ammonia-rich wastewater, i.e., glutamate wastewater, pharmaceutical wastewater, piggery wastewater, landfill leachate, etc. Nowadays, PN-based anammox technology provided a sustainable and environmental way for such wastewater treatment without carbon source addition. However, it is difficult to achieve high standard effluent via PNA process because excessive NO_3^- -N produced as an inherent issue. For this reason, an economical process for enhancing nitrogen removal from post-anammox NO_3^- -N-rich technology which combined PD and anammox could be established for advanced nitrogen removal. Wang et al. introduced mature leachate PNA effluent to one-stage PDA-SBR, under the concentration of influent NH_4^+ -N and NO_3^- -N of 47.5 mg/L and 93.7 mg/L on average, TN removal efficiency of 84.8% was obtained with the effluent TN less than 20 mg/L [18]. The ORP and pH could potentially be used as control parameters to maintain the stability of combined process [18]. Similarly, by applying the strategy of PNA coupled with PDA, NH_4^+ -N and TN removal efficiencies of over 95% were achieved during leachate treatment. In addition, providing an electron donor for PD of NO_3^- -N using diluted leachate is feasible for producing NO_2^- -N for subsequent anammox [20]. Overall, PD in cooperation with anammox is a reliable and economic strategy for post-anammox NO_3^- -N-rich treatment with lower carbon requirements, and can help meet the stringent environmental guidelines for TN removal.

3.3. Simultaneous Nitrogen Removal from Domestic and Nitrate-Contained Wastewater

It is well noted that, industrial nitrate wastewater is mainly distributed in the industrial park, so the establishment of MWTPs with PDA as the core treatment process in the park has bright application prospects, which could achieve simultaneous nitrogen removal from domestic sewage and industrial nitrate wastewater. The lab-scale PDA has been verified for high nitrate and municipal wastewater treatment process, in which NO_3^- -N (1000 mg/L) wastewater and municipal sewage (COD 182.5 mg/L, NH_4^+ -N 58.3 mg/L) were simultaneously introduced to the PD reactor for NO_2^- -N accumulation, and the NH_4^+ -N, NO_2^- -N in effluent of PD were removed in subsequent anammox reactor. A satisfactory nitrogen removal was achieved by optimizing the volume ratios of influent NO_3^- -N and municipal sewage, as well as the external organic matter dosage, indicated that PDA offered an economically and technically attractive approach in the high NO_3^- -N wastewater treatment. Recently studies introduced low-strength nitrate wastewater and domestic wastewater into one-stage PDA reactor, excellent effluent quality was obtained with < 5 mg/L of total nitrogen (TN) despite frequent temperature fluctuations (25.7-16.3°C) [10]. Metagenomic revealed that the abundances of cytoplasmic nitrate reductase (58706 hits) and periplasmic nitrate reductase (70540 hits)

were much higher than copper nitrite reductase (16436 hits) and cytochrome cd1 nitrite reductase (14264 hits), potentially contributing to the occurrence of PD [11].

4. Future Trends of the PDA Coupling Process

PD-based anammox wastewater system has been successfully applied into actual domestic sewage [10, 11], landfill leachate [53], and simulated industrial nitrate-contained wastewater, yet many hazardous materials in nitrate-contained wastewater were all neglected. The heavy metals, such as chromium, nickel, copper, zinc, etc., had strong cytotoxic and cell lysis effects, also fluoride, which had evident inhibition of enzyme activity [50]. None researches depicted the potential toxic effects of such substances in raw nitrate wastewater on PD, which was warranted to be investigated in future work.

From the micromolecule perspective, there are still knowledge gaps on the inter and intra-relationships between the various groups of bacteria in the mixed PDA culture [8]. The new molecular tools, such as metagenomic and metatranscriptomic have provided new insights into the complex nitrogen metabolic pathways of the involved bacteria [54]. Wang et al. applied metagenomic and metatranscriptomic approaches to gain comprehensive and deep understanding of the nitrogen metabolic pathways in a lab-scale single PDA bioreactor, NO_3^- -N reduction process was found to be mainly related to the activation of the *napA/B/C* genes instead of *narG/H* genes, the nitrogen metabolic network was also established to improve our knowledge of the nitrogen metabolic mechanisms [54]. Notably, the specific roles of each species of denitrifying and anammox bacteria should be elucidated to shed a new light for engineering application of PDA technology.

Many studies have identified that PDA could achieve advanced nitrogen removal, where anammox by-products NO_3^- -N could be reused by denitrification process to producing NO_2^- -N, this is also the unique advantages of PDA process compared with other biological nitrogen removal technology [11, 55]. However, phosphate as normal nutrient in real wastewater seemed unacceptable for PDA process, and novel technology for synchronous advanced nitrogen and phosphorus removal should be established. Considering this, we proposed an innovative simultaneous partial denitrification, anammox and denitrifying phosphorus removal (SPADPR) in a continuous flow reactor, since DPR was a promising opportunity for phosphorus removal with minimal waste sludge and minor carbon demand. The schematic diagram of SPADPR-ABR reactor exploited was shown in Figure 1. In this process, three anaerobic baffled reactor (ABR) chambers were operated as DPR area (termed as DPR-ABR), where the first chamber used as anaerobic P-release zone and other two compartments functioned as anoxic P-absorption with NO_3^- -N/ NO_2^- -N as electron acceptors. Continuous stirred tank reactor (CSTR) reactor was used to conduct PDA process,

termed as PDA-CSTR. In detail, $\text{NH}_4^+\text{-N}$, $\text{PO}_4^{3-}\text{-P}$ and COD contained wastewater (i.e., domestic sewage) was directly introduced into A1-DPR chamber to achieve phosphorus releasing under anaerobic condition, artificial nitrate wastewater was pumped into A2 chamber and implemented P-removal in the subsequent compartment (A2-3). Finally, the residual $\text{NO}_3^-\text{-N}$, $\text{NH}_4^+\text{-N}$, and little COD entered PDA reactor

to carry out advanced nitrogen removal via coordination of PD and anammox process. Overall, significantly synchronous nitrogen and phosphorus removal achieved without any aeration demand and external carbon source, thus a novel cost-effective and highly-efficient nutrient removal method was successfully established.

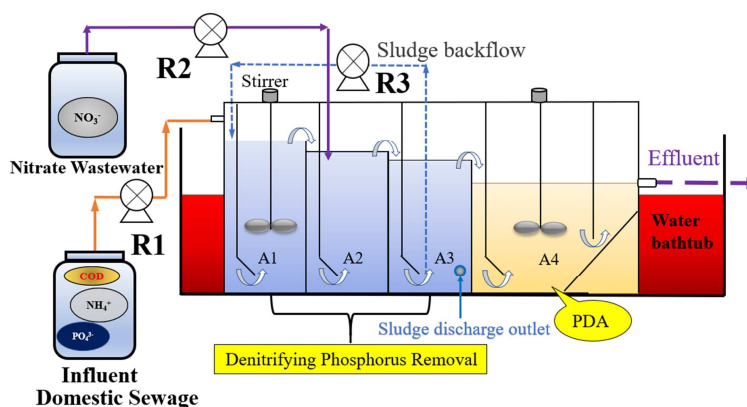


Figure 1. Schematic diagram of SPADPR-ABR reactor.

5. Conclusion

The PD-based anammox process offers a promising solution to $\text{NH}_4^+\text{-N}$ and $\text{NO}_3^-\text{-N}$ containing wastewater in a cost-effective and environmental-sustainable way. The highly-efficient nitrogen removal could be achieved and maintain a relatively stable despite exposed to long-term low temperature condition. The coupling system holds significant advantages in dealing with low/high strength wastewater by two- or single-stage integrations, such as 50% reduction in aeration energy consumption, 80% decrease in carbon source demand, and lower greenhouse (N_2O) as well as biomass production. Numerous lab-scale PDA process for actual wastewater treatment has been well developed for advanced nitrogen removal but practical engineering application still be lacking. More efforts are recommended on the controllable strategies for engineering practices and the penetrating understanding of microbial mechanism and metabolic pathway for the multispecies nitrogen transformation process.

Acknowledgements

This work was financially supported by Natural Science Foundation of China (51578353 and 51808367); Funding Project of Jiangsu Natural Science Research (BK20160356); Research Foundation of Suzhou University of Science and Technology (XKZ2018002).

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