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# Numerical and experimental analysis of shallow turbulent flow over complex roughness beds

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1	Numerical and Experimental Analysis of Shallow Turbulent Flow over
2	Complex Roughness Beds
3	Yong Zhang, State Key Laboratory of Hydroscience and Engineering, Tsinghua University,
4	Beijing 100084, China
5	Email: <u>zhang.yong.sichuan@163.com</u>
6	
7	Matteo Rubinato, Faculty of Engineering, Environment & Computing, School of Energy,
8	Construction and Environment, Coventry University, Coventry, CV1 5FB, UK
9	Email: matteo.rubinato@coventry.ac.uk ORCiD orcid.org/0000-0002-8446-4448
10	
11	Ehsan Kazemi, Department of Civil and Structural Engineering, The University of Sheffield,
12	Sheffield S1 3JD, UK
13	Email: <u>e.kazemi@sheffield.ac.uk</u> , ORCiD: orcid.org/0000-0002-1780-1846
14	
15	Jaan H. Pu, Faculty of Engineering and Informatics, University of Bradford, Bradford, BD7
16	IDP, UK
17	Email: <u>J.H.Pu1@bradford.ac.uk</u> ORCiD: orcid.org/0000-0002-3944-8801
18	
19	Yuefei Huang, State Key Laboratory of Hydroscience and Engineering, Tsinghua University,
20	Beijing 100084, China
21	Email: <u>yuefeihuang@tsinghua.edu.cn</u>
22	
23	Pengzhi Lin, State Key Laboratory of Hydraulics and Mountain River Engineering, Sichuan
24	University, Chengdu 610065, China
25	Email: <u>cvelinpz@scu.edu.cn</u> (corresponding author)
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27	ABSTRACT
28	A set of shallow-water equations (SWEs) based on a $\hat{k} - \hat{\varepsilon}$ Reynold stress model is established
29	to simulate the turbulent flows over a complex roughness bed. The fundamental equations are

- 30 discretized by the second-order finite-difference method (FDM), in which spatial and temporal
- 31 discretization are conducted by staggered-grid and leap-frog schemes, respectively. The
- 32 turbulent model in this study stems from the standard  $\hat{k} \hat{\varepsilon}$  model, but is enhanced by replacing
- 33 the conventional vertical production with a more rigorous and precise generation derived from
- 34 the energy spectrum and turbulence scales. To verify its effectiveness, the model is applied to

compute the turbulence in complex flow surroundings (including a rough bed) in an abrupt bend and in a natural waterway. The comparison of the model results against experimental data and other numerical results shows the robustness and accuracy of the present model in describing hydrodynamic characteristics, especially turbulence features on the complex roughness bottom.

40

*Keywords*: Energy spectrum, Roughness bed, SWE model, Shallow flows, Turbulent flows

41

#### 42 1 Introduction

43 Large and small turbulent swirling flows are often clearly observable when dealing with 44 hydraulic structures in rivers and coastal areas and they are a key factor that influence the 45 frequency and magnitude of natural processes such as the sediment transport, mixing of 46 pollutants and/or riverbed deformation. Therefore, to better manage the rivers and design 47 reliable hydraulic structures, it is fundamental to understand these features and facilitate their 48 predictions. However, certain external factors (e.g. various and inconsistent boundary 49 conditions) make the characterizations of turbulent flows very challenging. To the author's 50 knowledge, there is not yet a fully accurate, time-convenient, or general numerical model to 51 completely replicate the turbulent flows and their impacts over a natural roughness bed. Despite 52 that, effective simulations of the turbulent flow for some specific scenarios have been made due 53 to the rapid progress on the numerical modeling techniques and the computing powers.

54

55 The nature of turbulence is fundamentally three-dimensional (3D). Historically, 3D approaches 56 on the turbulence modeling mainly included the Direct Numerical Simulation (DNS), Large-57 Eddy Simulation (LES), and Reynolds-Averaged Navier-Stokes (RANS) modeling [1-4]. 58 Along the rivers and coastal regions, the flow domain is quite complex and spacious, and hence 59 to characterize the flow structures it would be excessively time-consuming to apply any of these 60 three approaches, which would require a large number of grid nodes in order to provide the 61 accurate results [5]. The two-dimensional (2D) Shallow Water Equations (SWE) coupled with 62 the benchmark turbulence closure model is much faster and enables the interpretation of 63 turbulent characteristics using a smaller vertical length scale (z) as compared with the two 64 horizontal ones (x and y) in those regions [6-9]. Furthermore, to obtain more accurate and 65 repeatable results, it is also critical to select the appropriate coefficients in these turbulence 66 closure equations.

68 2D shallow-turbulence flow models have been extensively developed over the last decades. 69 Most of the available ones are based on the Boussinesq approximations. For example, the depth-70 averaged eddy viscosity model suggests that eddy viscosity is the simple product of the bed 71 shear velocity and water depth [10] and the depth-averaged mixing length model accounts for 72 the influence of vertical turbulence [11]. Rastogi and Rodi [12] established the 2D standard depth-averaged  $\hat{k} - \hat{\varepsilon}$  turbulence model based on the 3D version described by Launder and 73 Spalding [13]. To widen the range of practical applications, some coefficients in the model 74 developed by Rastogi and Rodi were modified and new  $\hat{k} - \hat{\varepsilon}$  models were introduced, as 75 presented in the other studies [14-18]. The standard  $\hat{k} - \hat{\varepsilon}$  model has been demonstrated to 76 provide satisfactory results after numerous comparisons with the measured data [11,14] and it 77 78 is also relatively simple to use and very fast. Despite this, more progresses have been made in 79 this field and recently, Cea et al. [11] established a depth-averaged algebraic stress turbulence 80 model (DASM) to solve a single transport equation for each Reynolds stress without requiring 81 an isotropic assumption.

82

83 For the shallow turbulent flows on a roughness bed, the vertical velocity gradient distribution 84 is the main source of turbulence. The accuracy of its depth-averaged process directly determines the numerical performance of the aforementioned  $\hat{k} - \hat{\varepsilon}$  models. To date there is still area for 85 improvement due to the fact that preliminary results of the standard  $\hat{k} - \hat{\varepsilon}$  model only partially 86 agree with the experimental data [12]. According to Rastogi and Rodi [12], this may be related 87 88 to the bottom shear stress, via the friction velocity, under the assumption of similarity in the 89 vertical velocity profiles. The depth-averaging process is a consideration only of the 90 macroscopic effects of the bottom roughness on the turbulent generations. In the classic 91 "cascade" theory of energy introduced by Richardson [19], the turbulent motion is a process of 92 energy transfer among various scales including not only the macroscale, but also various 93 microscales [2, 20, 21]. The contribution of these features should be rigorously and precisely 94 replicated within turbulent closure models.

95

96 The turbulent structure of various scales based on the framework of energy cascade can be 97 divided into the energy-containing, inertial, and dissipative regions, respectively. The kinetic 98 energy, produced in the energy-containing region, is considered to be transferred by inertial 99 forces to smaller scales until the energy is typically dissipated by the molecular viscosity [2]. 100 The energy spectrum in the inertial region has a universal statistical form, i.e. the Kolmogorov 101 -5/3 spectrum [22], and can be applied to larger or smaller wave numbers as the Reynolds 102 number increases [8]. Nezu and Nakagawa [20] analogized the energy transfer processes to open-channel flows and divided the whole water depth into the three regions: wall,
 intermediate, and free-surface zones. A universal log-law in the intermediate region was
 verified by the extensive experimental and numerical results and they confirmed this can be
 applied to a wider range of bed roughness and Reynolds numbers.

107

108 Taking into considerations all of these previous works and the new insights that have been provided, this study aims to improve the performance of the standard  $\hat{k} - \hat{\varepsilon}$  model to 109 110 characterise the generation of turbulent conditions at various scales over complex roughness 111 beds. The numerical SWE model utilised in this work includes a second-order leap-frog finite-112 difference method (FDM) and it is built into a staggered-grid system. This model was initially 113 developed by Cho [23] to calculate the evolution of the long waves and was further extended 114 by Lin [24] to simulate the turbulent structures within an experimental zone. Lately this 115 turbulence model has been widely used to compute the complex flows induced by irregular 116 geometries and the results obtained have proven that it is a robust numerical technique [25-27]. 117 In the present study, we emphasized the improvement of the model for application to the 118 complex roughness beds.

119

120 The paper is organized as follows: Section 2 presents the description of the mathematical and 121 numerical shallow turbulence model considered for this study, clarifying various assumptions 122 and hypothesis: the governing equations are presented in *Section 2.1*, then the vertical turbulent 123 production is formulated in Section 2.2 by incorporating the energy transfer information 124 between various scales into  $P_{kV}$  and  $P_{\varepsilon V}$  based on the two universal semi-theoretical formulas 125 of Kolmogorov -5/3 scaling law and log-law. Section 3 includes the validation of the numerical 126 model against the experimental data collected on a flume, where varying roughness on the bed 127 was tested with a complex sharp bend. Finally, to further demonstrate the potentials of the 128 model, its performance was more vigorously examined in the transport of moraine along the 129 Yangtze River under dry seasons, and the results are explained in Section 4. Section 5 provides 130 a brief summary and concluding remarks of the whole study.

131 2 Numerical Model

#### 132 2.1 Governing equations

133 This section presents the governing equations and the boundary conditions utilised in this study.

#### 134 2.1.1 Shallow-water equations

135 The time-dependent SWEs are the fundamental hydrodynamic equations described in this

section. By integrating the Reynolds Averaged Navier-Stokes (RANS) equations along the
entire water depth and assuming the vertical flow to be nearly-uniform and pressure
distributions to be hydrostatic, the SWEs can be given as follows [25-27]:

139 
$$\frac{\partial H}{\partial t} + \frac{\partial P}{\partial x} + \frac{\partial Q}{\partial y} = 0$$
(1a)

140

$$\frac{\partial P}{\partial t} + \frac{\partial}{\partial x} \left(\frac{P^2}{H}\right) + \frac{\partial}{\partial y} \left(\frac{PQ}{H}\right) + gH \frac{\partial \eta}{\partial x} = \frac{1}{\rho} \frac{\partial (HT_{xx})}{\partial x} + \frac{1}{\rho} \frac{\partial (HT_{yx})}{\partial y} - \frac{f}{8H^2} \sqrt{P^2 + Q^2} P - \frac{2}{3} \frac{\partial (H\hat{k})}{\partial x}$$
(1b)

141 
$$\frac{\partial Q}{\partial t} + \frac{\partial}{\partial x} \left(\frac{PQ}{H}\right) + \frac{\partial}{\partial y} \left(\frac{Q^2}{H}\right) + gH \frac{\partial \eta}{\partial y} = \frac{1}{\rho} \frac{\partial \left(HT_{xy}\right)}{\partial x} + \frac{1}{\rho} \frac{\partial \left(HT_{yy}\right)}{\partial y} - \frac{f}{8H^2} \sqrt{P^2 + Q^2}Q - \frac{2}{3} \frac{\partial \left(H\hat{k}\right)}{\partial y} (1c)$$

142 where 
$$H(=\eta - z_b)$$
 is the water depth, in which  $\eta$  and  $z_b$  are the free surface and bed elevation

143 respectively (Fig. 1); P(=HU) and Q(=HV) are components of unit volume flux, in which

144 
$$U\left(=\frac{1}{H}\int_{z_b}^{\eta} \langle u \rangle dz\right)$$
 and  $V\left(=\frac{1}{H}\int_{z_b}^{\eta} \langle v \rangle dz\right)$  are the depth-averaged velocities in x and y directions.

145 respectively; g is gravitational acceleration;  $\rho$  is fluid density;  $\hat{k}\left(=\frac{1}{H}\int_{z_b}^{\eta}kdz\right)$  is the depth-

146 averaged turbulent energy;  $T_{xx}$ ,  $T_{yy}$ ,  $T_{yx}$ , and  $T_{xy}$  are the depth-averaged effective stresses 147 expressed as follows [25-26]:

148 
$$T_{xx} = 2\rho \frac{\nu + \hat{\nu}_t}{H} \frac{\partial P}{\partial x}$$
(2a)

149 
$$T_{yy} = 2\rho \frac{\nu + \hat{\nu}_t}{H} \frac{\partial Q}{\partial y}$$
(2b)

150 
$$T_{yx} = T_{xy} = \rho \frac{\nu + \hat{\nu}_t}{H} \left( \frac{\partial P}{\partial y} + \frac{\partial Q}{\partial x} \right)$$
(2c)

151 where  $\nu$  and  $\hat{\nu}_t$  are the kinematic viscosity and the depth-averaged turbulent viscosity, 152 respectively, as defined in Eq. (4).

153

*f* in Eq. (1) is the bed friction factor defined according to parameters for the smooth and rough
beds previously obtained [26, 28], such as Chézy-Manning's and Altsul's formula:

156 
$$f = \frac{8gm^2}{H^{1/3}}$$
 (3a)

157 
$$f = 0.1 \left( 1.46 \frac{k_s}{R} + \frac{100}{\text{Re}} \right)^{1/4}$$
 (3)

158 b)

159 where *m* is Manning's roughness coefficient;  $k_s$  is bed roughness height, which in this study 160 it is considered to be the median diameter of the bed material; *R* is the hydraulic radius (the 161 water depth, in this study); and *Re* is the Reynolds number.

# 162 2.1.2 Depth-averaged $\hat{k} - \hat{\varepsilon}$ closure equations

163 The depth-averaged velocity field in Eq. (1) can be solved when  $\hat{v}_t$  is determined. The 164 specification of  $\hat{v}_t$  is assumed to be mathematically analogous to the turbulent viscosity  $v_t$  in 165 the standard  $k - \varepsilon$  model [25], and can be expressed as follows:

166 
$$\hat{v}_t = C_\mu \frac{\hat{k}^2}{\hat{\varepsilon}}$$
(4)

167 The transport equations  $\hat{k}$  and  $\hat{\varepsilon}$  can be then introduced, respectively, as follows:

$$\frac{\partial \left(H\hat{k}\right)}{\partial t} + \frac{\partial \left(P\hat{k}\right)}{\partial x} + \frac{\partial \left(Q\hat{k}\right)}{\partial y} = H\hat{v}_{t}\left[2\left(\frac{\partial U}{\partial x}\right)^{2} + 2\left(\frac{\partial V}{\partial y}\right)^{2} + \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x}\right)^{2}\right] + P_{kV} + \frac{\partial}{\partial x}\left[\left(\nu + \frac{\hat{v}_{t}}{\sigma_{k}}\right)\frac{\partial \left(H\hat{k}\right)}{\partial x}\right] + \frac{\partial}{\partial y}\left[\left(\nu + \frac{\hat{v}_{t}}{\sigma_{k}}\right)\frac{\partial \left(H\hat{k}\right)}{\partial y}\right] - H\hat{\varepsilon}$$
(5a)

$$\frac{\partial(H\hat{\varepsilon})}{\partial t} + \frac{\partial(P\hat{\varepsilon})}{\partial x} + \frac{\partial(Q\hat{\varepsilon})}{\partial y} = C_{\varepsilon^{1}}\frac{\hat{\varepsilon}}{\hat{k}}H\hat{v}_{t}\left[2\left(\frac{\partial U}{\partial x}\right)^{2} + 2\left(\frac{\partial V}{\partial y}\right)^{2} + \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x}\right)^{2}\right] + P_{\varepsilon^{V}} + \frac{\partial}{\partial x}\left[\left(v + \frac{\hat{v}_{t}}{\sigma_{\varepsilon}}\right)\frac{\partial(H\hat{\varepsilon})}{\partial x}\right] + \frac{\partial}{\partial y}\left[\left(v + \frac{\hat{v}_{t}}{\sigma_{\varepsilon}}\right)\frac{\partial(H\hat{\varepsilon})}{\partial y}\right] - C_{\varepsilon^{2}}H\frac{\hat{\varepsilon}^{2}}{\hat{k}}$$
(5b)

170 where 
$$C_{\mu}, \sigma_{k}, \sigma_{\varepsilon}, C_{1\varepsilon}$$
 and  $C_{2\varepsilon}$  are the empirical constants and their values, as recommended by

171 Launder and Spalding [13], are

172 
$$C_{\mu} = 0.09, \sigma_{k} = 1.0, \sigma_{\varepsilon} = 1.3, C_{1\varepsilon} = 1.44, C_{2\varepsilon} = 1.92$$
 (6)

173 and, as suggested in [8], [12] and [13],

174 
$$P_{kV} = \frac{n^2 g}{H^{\frac{1}{3}}} \left( U^2 + V^2 \right)^{\frac{3}{2}}$$
(7a)

175 
$$P_{\varepsilon V} = \frac{C_2 C_{\mu} n^{\frac{5}{2}} g^{\frac{5}{4}} \left( U^2 + V^2 \right)^2}{H^{\frac{17}{12}}}$$
(7b)

#### 177 **2.2 Vertical turbulent production** $P_{kV}$ and $P_{\varepsilon V}$

178  $P_{kV}$  and  $P_{eV}$  in Eq. (5) are the components generated by turbulence and can be defined as the 179 tensor product of the horizontal Reynolds stress and vertical velocity gradient, respectively. In 180 the context of homogeneous, open-channel turbulence, they represent all the turbulent energy 181 produced. The corresponding expressions to calculate their magnitude were deduced by Rastogi 182 and Rodi [12], although their derivations seemed to have overgeneralized the generation of 183 vertical turbulent features.

184

According to the theory of cascade energy, which has been proven and validated against 185 186 extensive experimental studies, the turbulent motion is a one-way energy transfer process from 187 large scale eddies to smaller ones [2]. The theory can also be applied to the transfer of energy 188 from the bottom of the river to the free surface [20]. To rigorously and precisely quantify the 189 energy transfer across various scales, this study presents an additional model that estimates the 190 generation of vertical turbulent features in a different manner, considering the interaction 191 between points at different levels and the total energy spectrum. Bottom roughness elements 192 markedly affect the amount of turbulence. Turbulence tends to be isotropy as the bed roughness 193 and Reynolds numbers increase [2, 20,29]. Cea et al. [11] found a similar degree of accuracy between the  $\hat{k} - \hat{\varepsilon}$  model, which is based on the concise isotropic hypothesis, and the DASM 194 195 model, which includes complex model structures considering anisotropy. Based on this assumption, below are listed the steps selected to deduce the expressions of  $P_{kV}$  and  $P_{\varepsilon V}$ . 196

#### 197 2.2.1 Mean velocity profiles

For a uniform and fully-developed turbulent flow in a wide open channel, the Reynolds equation in the *z*-direction (as derived from the Navier-Stokes equations) is reduced to:

$$200 \qquad \rho v \frac{d\langle u \rangle}{dz} - \rho \langle u'w' \rangle = \rho u_*^2 \left(1 - \frac{z}{H}\right) \tag{8}$$

201 where  $\rho v d\langle u \rangle / dz$  is the viscous stress;  $-\rho \langle u'w' \rangle$  is the Reynolds stress;  $u_* \left( = \sqrt{\tau_b / \rho} \right)$  is the 202 friction velocity, in which  $\tau_b$  is the bed shear stress at z = 0.

203

By considering the Prandtl's mixing-length hypothesis, v can be expressed as the product of a velocity scale  $u^*$  and a length scale  $l_m$ , in which  $u^*$  is specified as  $u^* = |\langle u'w' \rangle|^{1/2}$ . From Eq. (8), 206 the following equation could be obtained:

207 
$$\frac{d\langle u \rangle^{+}}{dz^{+}} = \frac{2\tau/\tau_{b}}{1 + \sqrt{1 + (4\tau/\tau_{b})(l_{m}^{+})^{2}}}$$
(9)

where  $\langle u \rangle^+ = \langle u \rangle / u_*$  and  $z^+ = zu_* / v_k$  are the dimensionless velocity and z-coordinate normalized by the viscous length  $\delta_v = v_k / u_*$ , respectively;  $l_m^+ = l_m u_* / v_k$  is the dimensionless mixing-length. If appropriate specification of  $l_m^+$  over the whole depth can be obtained, Eq. (9) can be easily integrated to yield the distribution of  $\langle u \rangle$ .

212

In various regions from z=0 to  $z=\eta$ , the effect of  $\rho v d\langle u \rangle/dz$  and  $-\rho \langle u'w' \rangle$  on the velocity distribution is different. According to their contribution to the turbulent structure, the vertical turbulence fields of  $\langle u \rangle$  are divided into two regions: the inner region and the outer region [20]. It is assumed that the viscous effect dominates the inner region (in general, z/H < (0.15-0.2)), so the length scale can be denoted by  $\delta_v$ . The component  $\tau/\tau_w$  tends towards unity and  $l_m^+$  can be specified as  $l_m^+ = \kappa z^+$  in this region, so the solution to Eq. (9) (the "log-law"), can be obtained as follows:

$$220 \qquad \left\langle u \right\rangle^{+} = \frac{1}{\kappa} \ln z^{+} + A \tag{10}$$

where  $\kappa = 0.40 - 0.43$  and B = 5.2 are the empirical constants [2, 30].

222

It is assumed that the viscous contribution in the outer region (generally, 
$$z/H \ge (0.15-0.2)$$
) to  
the turbulent structure is negligible, and that  $l_m^+$  no longer depends on  $\delta_v$ . It is challenging to  
solve Eq. (9) because there is no universal representation of  $l_m^+$ . The wake law provided by  
Coles [31], is typically used to extend the log-law to the outer region. The profile of  $\langle u \rangle$  in this  
region can be approximated as follows:

228 
$$\langle u \rangle^+ = \frac{1}{\kappa} \ln z^+ + A + \frac{2\Pi}{\kappa} \sin^2 \left( \frac{\pi z}{2H} \right)$$
 (11)

where  $\Pi$  is Coles's wake-strength parameter.  $\Pi$  has been investigated in various studies where its value has been suggested to be around 0.08-0.20.  $\Pi$  also shows no distinct value for flows with different bed roughness conditions [32]. Considering the comparisons made by Pope [2] and Nezu and Nakagawa [20], the profile of  $\langle u \rangle$  can be effectively approximated by Eq. (11) over the whole depth except in a small region near the bed. In the core region of closed-bed flow (e.g.,  $z^+ < 26$ ),  $l_m^+$  is strongly affected by the Reynolds number and bed roughness, so  $\langle u \rangle$  is likely to remain the complex profile. In this study, we considered the distribution of  $\langle u \rangle$ in this region to be determined by using Eq. (11).

#### 237 2.2.2 Depth-averaged vertical production

Based on Kolmogorov's scaling theory outlined at [22], the dissipation rate  $\varepsilon$  could be related to  $\|u'\|$  by using the macroscale of turbulence described in [20, 21] as follows:

$$\mathcal{E} = K \frac{\|u'\|^3}{L_x} \tag{12}$$

where  $K = [2/(\pi C')]^{3/2} (L_x k_0)^{5/2}$  is a turbulent coefficient which is greatly influenced by the Reynolds number, C' is a universal Kolmogorov constant,  $L_x$  is the longitudinal integral macroscale,  $k_0$  is macroscale of turbulence. Nakagawa et al. [33] suggested that  $||u'||/u_*$  can be approximated as the power function of z/H:

245 
$$\frac{\|u'\|}{u_*} = \left[\frac{B_N}{\kappa K} \left(1 - \frac{z}{H}\right)\right]^{1/3} \left(\frac{z}{H}\right)^{-1/6}$$
(13)

Further, under an assumption of isotropy, Nezu and Nakagawa [20] found that the correlation coefficients of turbulence intensities are nearly constant as long as  $z^+$  is sufficiently large. This can be approximately represented by:

249 
$$||w'|| / ||u'|| = C_1, ||v'|| / ||u'|| = C_2$$
 (14)

- 250 where  $C_1$  and  $C_2$  are empirical constants.
- 251

For stationary and homogeneous turbulence, the turbulent production  $P_k \left(= -\langle u'w' \rangle \partial \langle u \rangle / \partial z \right)$  is balanced approximately by the sum of the turbulent diffusion  $D_k \left(= (d/dz) \left[ (v/\sigma_k) (dk/dz) \right] \right)$ and dissipation  $\varepsilon$  independently of the molecular diffusion. In the inertial subrange, energy transfer is the only significant process; there is no energy production or dissipation. Thus,  $P_k \approx \varepsilon$ . The dynamic equilibrium of turbulent energy can then be expressed as follows:

$$257 \qquad v \frac{dk}{dz} = \text{const.} \tag{15}$$

258 in which  $v(=C_{\mu}k^2/\epsilon)$  is the turbulent viscosity. Substituting Eq. (12) into v (where  $L_x$  is of 259 the same order as H) and making use of Eq. (14) (where u' is of the order of  $u_*$ ) yields the 260 following approximation of v:

$$261 \qquad v \approx \frac{1}{k} H u_*^3 \tag{16}$$

Substituting Eq. (16) into Eq. (15) with the integral from 0 to z yields the distribution of k:

$$263 \qquad \frac{k}{u_*^2} = D \exp\left(-2C_k \frac{z}{H}\right) \tag{17}$$

where *D* and  $C_k$  are the constants. Applying Eqs. (14) and (17) provides the profiles of u', v', and w':

$$266 \qquad \frac{\|u'\|}{u_*} = D_u \exp\left(-C_k \frac{z}{H}\right) \tag{18a}$$

267 
$$\frac{\|v'\|}{u_*} = D_v \exp\left(-C_k \frac{z}{H}\right)$$
(18b)

$$268 \qquad \frac{\|w'\|}{u_*} = D_w \exp\left(-C_k \frac{z}{H}\right) \tag{18c}$$

where  $D_u$ ,  $D_v$ ,  $D_w$ , and  $C_k$  are the empirical constants; their values are 2.30, 1.27, 1.63, and 1.0, respectively [20].

271

By closely examining the turbulence intensities presented by Nezu and Nakagawa [20], we found close agreement between Eq. (18) results and the experimental values throughout the whole depth apart from a thin layer near the bed. Surprisingly, any deviation between them gradually decreased as Re and  $k_s^+$  ( $=k_s u_*/v_k$ ) increased. To some extent, Eq. (18) is successful in displaying the vertical distribution of turbulence intensity. Integrating Eq. (18) with the given empirical constants allows the depth-averaged turbulent energy  $\hat{k}$  to be obtained:  $\hat{k} = 2.07 u_*^2$  (19)

279 The constant used in Eq. (19) has been found by combining  $D_u$ ,  $D_v$ , and  $D_w$  at Eqs. (18a) – (18c), 280 suggested in Nezu and Nakagawa [20]. The formulation of k is described in Eq. (37). According 281 to the theory of cascade energy, at the end of the sequence of processes, the dissipation of 282 turbulent energy is accomplished primarily by molecular viscosity. In other words, the energy 283 of open-channel flows is predominantly dissipated in the free surface region. Observed  $\varepsilon$ 284 values in this region are less accurate due to the constraints of free-surface fluctuations. In the 285 comparison made by Nakagawa et al. [33], it is very difficult to obtain a universal formula for 286  $\varepsilon$ . In this study, we used v as a replacement for  $\varepsilon$  to determine  $P_{kV}$  and  $P_{\delta V}$ .

288 
$$\nu = \frac{\kappa (1 - z/H) H u_*}{(H/z) + \pi \Pi \sin(\pi z/H)}$$
(20)

Eq. (20) is found from substituting Coles' law at Eq. (11) into Eq. (8). By integrating Eq. (20) from the bed to free surface, we obtained the depth-averaged turbulent viscosity  $\hat{v}_t$  as follows:  $\hat{v}_t = 0.06Hu_*$  (21)

The constant in Eq. (21) comes from depth-averaging Eq. (20) from bed to free-surface, using described values of  $\kappa$  and  $\Pi$  in section 2.2.1. In stationary and homogeneous flows,  $P_{kV}$  and  $P_{eV}$  in the  $\hat{k} - \hat{\varepsilon}$  transport equations are balanced only by their dissipation terms  $\hat{e}H$  and  $C_{2\varepsilon} \hat{\varepsilon}^2 H/\hat{k}$ , respectively.  $P_{kV}$  and  $P_{eV}$  can be obtained by rearranging Eq. (5) and combining Eqs. (4), (19) and (21):

297 
$$P_{kV} = 71.42 C_{\mu} u_*^{3}$$
 (22a)

298 
$$P_{\varepsilon V} = 2464.16 C_{\mu}^{2} C_{2\varepsilon} \frac{u_{*}^{4}}{H}$$
 (22b)

where  $u_* = \sqrt{f(U^2 + V^2)/8}$ . These Eqs. (22a) and (22b) have been derived from the standard  $\hat{k} - \hat{\varepsilon}$  formulations of  $P_{kV}$  and  $P_{eV}$  terms as showing at Eqs. (7a) and (7b).

301

#### 302 2.3 Numerical implementation

In this study, we discretized the fundamental equations using the explicit leap-frog FDM which has second-order accuracy in both time and space [25-26]. As plotted in Fig. 2, all of the vectors (P, Q, U, and V) were evaluated at the faces of the grid; all of the scalars  $(H, \eta, z_b, \hat{k}, \text{and } \hat{\epsilon})$ were defined at the center of the grid. The defined location of the normal stresses (e.g.,  $T_{xx}$  and  $T_{yy}$ ) is the same as the scalar; the shear stresses (e.g.,  $T_{xy}$  and  $T_{yx}$ ) were calculated as shown in the right-top corner of the grid.

#### 309 2.3.1 Continuity equation

310 According to the spatial staggered grid system and the temporal leap-frog scheme, the 311 continuity equation is explicitly discretized as follows:

312 
$$H_{i,j}^{n+1/2} = H_{i,j}^{n-1/2} - \frac{\Delta t}{\Delta x_i} \left( P_{i+1/2,j}^n - P_{i-1/2,j}^n \right) - \frac{\Delta t}{\Delta y_j} \left( Q_{i,j+1/2}^n - Q_{i,j-1/2}^n \right)$$
(23)

#### 313 2.3.2 Momentum equations

314 Without loss of generality, only the discretized form of x-momentum equation is presented here 315 in detail:

$$P_{i+l/2,j}^{n+1} = \frac{1 - \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2}}{1 + \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2}} P_{i+l/2,j}^{n} \\ - \frac{\Delta t}{1 + \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2}} \left\{ \left[ \frac{\partial}{\partial x} \left( \frac{P^{2}}{H} \right) \right]_{i+l/2,j}^{n} + \left[ \frac{\partial}{\partial y} \left( \frac{PQ}{H} \right) \right]_{i+l/2,j}^{n} \right\} \right]^{n} \\ - \frac{g\Delta t}{\left\{ 1 + \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2} \right\} \Delta x_{i+l/2}} H_{i+l/2,j}^{n+l/2} \left\{ 1 + \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2} \right\} \Delta x_{i+l/2}} + \frac{\Delta t/\rho}{1 + \frac{f\Delta t}{16(H_{i+l/2,j}^{n})^{2}} \left[ \left( P_{i+l/2,j}^{n} \right)^{2} + \left( Q_{i+l/2,j}^{n} \right)^{2} \right]^{1/2}} \left[ \frac{\partial(HT_{xx})}{\partial x} + \frac{\partial(HT_{yx})}{\partial y} \right]_{i+l/2,j}^{n} \right]^{n}$$

where the convection terms are respectively discretized as follows by applying the upwindscheme:

319 
$$\left[\frac{\partial}{\partial x}\left(\frac{P^{2}}{H}\right)\right]_{i+1/2,j}^{n} = \begin{cases} \frac{\left(\frac{P_{i+1/2,j}^{n}}{H_{i+1/2,j}^{n}} - \frac{\left(\frac{P_{i-1/2,j}^{n}}{H_{i-1/2,j}^{n}}\right)^{2}}{\Delta x_{i}} & \text{if } P_{i+1/2,j}^{n} > 0 \\ \frac{\left(\frac{P_{i+3/2,j}^{n}}{L_{i+3/2,j}^{n}} - \frac{\left(\frac{P_{i-1/2,j}^{n}}{H_{i-1/2,j}^{n}}\right)^{2}}{\Delta x_{i} + \Delta x_{i+1}} & \text{if } P_{i+1/2,j}^{n} = 0 \\ \frac{\left(\frac{P_{i+3/2,j}^{n}}{L_{i+3/2,j}^{n}} - \frac{\left(\frac{P_{i+1/2,j}^{n}}{H_{i+1/2,j}^{n}}\right)^{2}}{\Delta x_{i+1}} & \text{if } P_{i+1/2,j}^{n} < 0 \end{cases}$$
(25a)

$$320 \qquad \left[\frac{\partial}{\partial y}\left(\frac{PQ}{H}\right)\right]_{i+1/2,j}^{n} = \begin{cases} \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j}^{n}}{H_{i+1/2,j}^{n}} - \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j-1}^{n}}{H_{i+1/2,j-1}^{n}} & \text{if } Q_{i+1/2,j}^{n} > 0 \\ \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j+1}^{n}}{H_{i+1/2,j+1}^{n}} - \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j-1}^{n}}{H_{i+1/2,j-1}^{n}} & \text{if } Q_{i+1/2,j}^{n} = 0 \\ \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j+1}^{n}}{H_{i+1/2,j+1}^{n}} - \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j}^{n}}{H_{i+1/2,j}^{n}} & \text{if } Q_{i+1/2,j}^{n} = 0 \\ \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j+1}^{n}}{H_{i+1/2,j+1}^{n}} - \frac{\left(\frac{PQ}{P}\right)_{i+1/2,j}^{n}}{H_{i+1/2,j}^{n}} & \text{if } Q_{i+1/2,j}^{n} < 0 \end{cases}$$

$$(25b)$$

### 321 2.3.3 Turbulent transport equations

316

322 The  $\hat{\varepsilon}$  – and  $\hat{k}$  – equations are respectively discretized by applying a semi-implicit scheme:

323 
$$\hat{\varepsilon}_{i,j}^{n+1/2} = \frac{\frac{(H\hat{\varepsilon})_{i,j}^{n-1/2}}{\Delta t} - F\hat{\varepsilon}X - F\hat{\varepsilon}Y + VIS\hat{\varepsilon}X + VIS\hat{\varepsilon}Y + C_{1\varepsilon}\frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{\hat{k}_{i,j}^{n-1/2}}(P_h)_{i,j}^{n+1/2} + (P_{\varepsilon V})_{i,j}^{n+1/2}}{\frac{H_{i,j}^{n+1/2}}{\Delta t} + C_{2\varepsilon}\frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{\hat{k}_{i,j}^{n-1/2}}H_{i,j}^{n-1/2}}$$
(26a)

324 
$$\hat{k}_{i,j}^{n+1/2} = \frac{\frac{(H\hat{k})_{i,j}^{n-1/2}}{\Delta t} - F\hat{k}X - F\hat{k}Y + VIS\hat{k}X + VIS\hat{k}Y + (P_h)_{i,j}^{n+1/2} + (P_{kV})_{i,j}^{n+1/2}}{\frac{H_{i,j}^{n+1/2}}{\Delta t} + C_{\mu}\frac{\hat{\varepsilon}_{i,j}^{n-1/2}}{(\hat{V}_i)_{i,j}^{n-1/2}}H_{i,j}^{n-1/2}}$$
(26b)

326 Similarly, the upwind scheme can be used to discretize the convective term  $F\hat{\epsilon}X$  (the 327 differences of  $F\hat{\epsilon}Y$ ,  $F\hat{k}X$ , and  $F\hat{k}Y$  are similar to  $F\hat{\epsilon}X$ ) as follows:

$$328 \qquad \left[F\hat{\varepsilon}X\right]_{i,j}^{n-1/2} = \left[\frac{\partial(P\hat{\varepsilon})}{\partial x}\right]_{i,j}^{n-1/2} = \begin{cases} \frac{P_{i,j}^{n-1/2}\hat{\varepsilon}_{i,j}^{n-1/2} - P_{i-1,j}^{n-1/2}\hat{\varepsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2}} & \text{if} \quad P_{i,j}^{n-1/2} > 0\\ \frac{P_{i+1,j}^{n-1/2}\hat{\varepsilon}_{i+1,j}^{n-1/2} - P_{i-1,j}^{n-1/2}\hat{\varepsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2}} & \text{if} \quad P_{i,j}^{n-1/2} = 0\\ \frac{P_{i+1,j}^{n-1/2}\hat{\varepsilon}_{i+1,j}^{n-1/2} - P_{i,j}^{n-1/2}\hat{\varepsilon}_{i,j}^{n-1/2}}{\Delta x_{i+1/2}} & \text{if} \quad P_{i,j}^{n-1/2} < 0 \end{cases}$$

$$(27)$$

329

330 The central difference method was applied to discretize the diffusion term  $VIS\hat{\epsilon}X$  (the 331 difference forms of  $VIS\hat{\epsilon}Y$ ,  $VIS\hat{k}X$ , and  $VIS\hat{k}Y$  are analogous to  $VIS\hat{\epsilon}X$ ) as follows:

$$332 \qquad VIS \hat{\epsilon} X = \frac{1}{\Delta x_{i}} \left\{ \left[ \left( \mathbf{v}_{k} + \frac{\hat{\mathbf{v}}_{t}}{\sigma_{\epsilon}} \right) \frac{\partial \left(H\hat{\epsilon}\right)}{\partial x} \right]_{i+1/2,j}^{n-1/2} - \left[ \left( \mathbf{v}_{k} + \frac{\hat{\mathbf{v}}_{t}}{\sigma_{\epsilon}} \right) \frac{\partial \left(H\hat{\epsilon}\right)}{\partial x} \right]_{i-1/2,j}^{n-1/2} \right\} = \frac{1}{\Delta x_{i}} \left[ \left( \mathbf{v}_{k} + \frac{\left(\hat{\mathbf{v}}_{t}\right)_{i+1/2,j}^{n-1/2}}{\sigma_{\epsilon}} \right) \frac{H_{i+1/2,j}^{n-1/2} \hat{\epsilon}_{i+1,j}^{n-1/2} - H_{i,j}^{n-1/2} \hat{\epsilon}_{i,j}^{n-1/2}}{\Delta x_{i+1/2}} - \left( \mathbf{v}_{k} + \frac{\left(\hat{\mathbf{v}}_{t}\right)_{i-1/2,j}^{n-1/2}}{\sigma_{\epsilon}} \right) \frac{H_{i,j}^{n-1/2} \hat{\epsilon}_{i-1,j}^{n-1/2}}{\Delta x_{i-1/2}} \right]$$
(28)

# 333 The horizontal velocity-gradient production term $P_h$ can be discretized as:

334 
$$(P_{h})_{i,j}^{n+1/2} = H_{i,j}^{n+1/2} (\hat{v}_{i})_{i,j}^{n-1/2} \begin{bmatrix} 2 \left( \frac{U_{i+1/2,j}^{n+1/2} - U_{i-1/2,j}^{n+1/2}}{\Delta x_{i}} \right)^{2} + 2 \left( \frac{V_{i,j+1/2}^{n+1/2} - V_{i,j-1/2}^{n+1/2}}{\Delta y_{j}} \right)^{2} + \left( \frac{V_{i+1/2,j}^{n+1/2} - V_{i-1/2,j}^{n+1/2}}{\Delta x_{i}} + \frac{U_{i,j+1/2}^{n+1/2} - U_{i,j-1/2}^{n+1/2}}{\Delta y_{j}} \right)^{2} \end{bmatrix}$$
(29)

According to the expression of Eq. (22b), the vertical velocity-gradient production term  $P_{ev}$ 

336 (the difference form of  $P_{kV}$  is the same as  $P_{kV}$ ) can be discretized as:

337 
$$(P_{\varepsilon V})_{i,j}^{n+1/2} = 2464.16 C_{\mu}^{2} C_{2\varepsilon} \frac{\left\{ \frac{f}{8} \left[ \left( U_{i,j}^{n+1/2} \right)^{2} + \left( V_{i,j}^{n+1/2} \right)^{2} \right] \right\}^{2}}{H_{i,j}^{n+1/2}}$$
(30)

#### 338 2.4 Boundary conditions

To perform the staggered-grid difference method, ghost cells are typically imposed around the outmost computational domain. The boundary of all scalar variables, e.g.,  $\eta^B$ ,  $\hat{k}^B$ , and  $\hat{\varepsilon}^B$ (where the superscript *B* denotes the boundary) is set at the center of the ghost grid; the boundary of all vector variables, e.g.,  $P^B$  and  $Q^B$ , is located at the center of the adjacent surface between the ghost cell and the outermost computational grid [27]. The boundary conditions selected for this study mainly include open boundaries and no-slip boundaries.

345

Open boundary conditions are applied mainly to inflow and outflow. For the tests conducted, subcritical flow is the most frequent, hence the boundary conditions assumed include a specific flow rate assigned at the upstream boundary location; in addition, uniform water depth is applied as the downstream boundary condition. The inflow boundary condition can be expressed as follows:

351 
$$\eta_1^{B} = \eta_2^{B}, P_{3/2}^{B} = P_{5/2}^{B}, Q_1^{B} = Q_2^{B}, \hat{k}_1^{B} = \hat{k}_2^{B} \text{ and } \hat{\varepsilon}_1^{B} = \hat{\varepsilon}_2^{B}$$
 (31a)

352 The outflow boundary condition can be expressed follows:

353 
$$\eta_n^{\rm B} = \eta_{n-1}^{\rm B}, P_{n-1/2}^{\rm B} = P_{n-3/2}^{\rm B}, Q_n^{\rm B} = Q_{n-1}^{\rm B}, \hat{k}_n^{\rm B} = \hat{k}_{n-1}^{\rm B} \text{ and } \hat{\varepsilon}_n^{\rm B} = \hat{\varepsilon}_{n-1}^{\rm B}$$
 (31b)

No-slip boundary conditions are applied on the side where there is the solid-wall. The flux on the solid boundary is zero, i.e.,  $P_{l+1/2}^{B} = Q_{l+1/2}^{B} = 0$ , where the subscript l+1/2 denotes the adjacent surface between the water and solid-wall cells and l denotes the corresponding center of the wall cell. The boundary conditions for  $\hat{k}$  and  $\hat{\varepsilon}$  at the location l are also necessary.

According to the boundary-layer theory, if the distance *s* between *l* and l+1/2 is sufficiently small, the shear stress and the turbulent production at *l* can be balanced approximately with the wall shear stress and the dissipation at l+1/2, respectively [13]. The depth-averaged statistic characteristics in the small region near the wall are assumed to be analogous to the turbulent features in the core region near the bed. In other words, per Eqs. (8), (11), and (15),  $\hat{\varepsilon}_l^{\rm B}$  can be expressed approximately as follows:

365 
$$\hat{\varepsilon}_{l}^{B} = u_{W*}^{2} \frac{dU'}{dy'} = \frac{u_{W*}^{3}}{\kappa s}$$
(32a)

where dU'/dy' is the depth-averaged velocity gradient in normal coordinates near the solid wall. Based on the specifications of  $\hat{v}_t$  and Eq. (4),  $(\hat{v}_t)_l^{\rm B}$  can be expressed as  $(\hat{v}_t)_l^{\rm B} = \kappa s u_{\rm W*}$ ;  $\hat{k}_l^{\rm B}$  can be written as follows:

369 
$$\hat{k}_{l}^{\rm B} = \frac{u_{\rm W*}^{2}}{\sqrt{C_{\mu}}}$$
 (32b)

370  $u_{W*}$  must satisfy the following equation [24]:

371 
$$\frac{U'}{u_{W^*}} = \begin{cases} \frac{1}{\kappa} \ln\left(\frac{Eu_{W^*}y'}{v_k}\right) & \text{for hydraulically smooth wall} \\ \frac{1}{\kappa} \ln\left(\frac{30y'}{k_s}\right) & \text{for hydraulically rough wall} \end{cases}$$
(33)

where E = 0.9 is the constant; U' is treated as a depth-averaged shear velocity at *l*; both *s* and y' are approximated by half of the normal space step at *l*.

375 To secure stable numerical results, the Courant-Friedrichs-Lewy (CFL) number  $C_r$  was 376 considered as the stability criterion within the proposed model and to enable its incorporation, 377 the following double stability conditions were imposed for  $C_r$  as suggested by the literature 378 [24]:

379 
$$\operatorname{Cr}_{\mathrm{flow}} = \Delta t \max\left\{ \max\left[ \left( \frac{|P|/H + \sqrt{gH}}{\Delta x} \right)_{i,j} \right], \max\left[ \left( \frac{|Q|/H + \sqrt{gH}}{\Delta y} \right)_{i,j} \right] \right\} \le 1$$
(34a)

380 
$$\operatorname{Cr}_{\operatorname{turbulence}} = \Delta t \max\left\{ \max\left[ \left( \frac{2(\hat{v}_{t} + v_{k})}{(\Delta x)^{2}} \right)_{i,j} \right], \max\left[ \left( \frac{2(\hat{v}_{t} + v_{k})}{(\Delta y)^{2}} \right)_{i,j} \right] \right\} \le 1$$
(34b)

381 where  $\Delta t$  is set as the minimum of the  $\Delta t$  values calculated by using Eqs. (34a) and (34b).

#### **382 3 Model Validations**

To validate the model previously described to quantify complex turbulence, its performance has been verified against experimental turbulent flows obtained under various circumstances: 1) a uniform gravel bed, 2) a 90° bend, and 3) a suddenly expanding section. Numerical results were then compared against measured datasets as well as the calculated values from the standard  $\hat{k} - \hat{\varepsilon}$  model and other numerical schemes. To distinguish among the different models' results, "*PF*" and "*RRF*" are used to represent the model constructed by the proposed formula and by Rastogi and Rodi's formula, respectively.

#### 390 3.1 Turbulent flow in a straight channel with gravel bed

To verify the accuracy of the proposed model in replicating bed roughness and Reynolds number effects on the formation of turbulent features, a series of experiments on open-channel flows over rough beds conducted by Wang et al [38], were used for comparison. The experiments were conducted in a straight flat glass flume 13.5 m long, 0.60 m wide, and 0.60 deep [38]. The roughness elements on the bottom of the flume were composed of gravel with median diameter  $d_{50}$  ranging from 2 to 40 mm. Throughout all measurements, the simultaneous high-frequency velocities in the middle of the flume were obtained with an acoustic Doppler

398 399 velocimeter (ADV).

400 According to the ensemble averages terms used in this study, velocity samples were gathered 401 to determine the mean flows and turbulent fields in the system. The mean velocities in x-, y-, 402 and z-directions were estimated as follows [24]:

403 
$$\overline{u} = \frac{1}{N} \sum_{i=1}^{N} u_i, \, \overline{v} = \frac{1}{N} \sum_{i=1}^{N} v_i, \, \overline{w} = \frac{1}{N} \sum_{i=1}^{N} w_i$$
 (35)

404 where N is the number of samples. The root-mean-square (marked as r.m.s) values of the 405 velocity fluctuations are defined by the sample standard deviation:

406 
$$\text{r.m.s. } u' = \sqrt{\frac{\sum_{i=1}^{N} u_i^2 - N\overline{u}^2}{N-1}}, \text{r.m.s. } v' = \sqrt{\frac{\sum_{i=1}^{N} v_i^2 - N\overline{v}^2}{N-1}}, \text{r.m.s. } w' = \sqrt{\frac{\sum_{i=1}^{N} w_i^2 - N\overline{w}^2}{N-1}}$$
 (36)

407 The turbulent kinetic energy k can be calculated from the above definitions as follows:

408 
$$k = \frac{1}{2} \left[ (r.m.s. u')^2 + (r.m.s. v')^2 + (r.m.s. w')^2 \right]$$
(37)

409

410 The corresponding depth-averaged  $\hat{k}$  can be obtained by depth-averaging the vertical profiles. 411 The depth-averaged data calculated from vertical measured regions was taken to represent the 412 entire depth at the corresponding horizontal coordinate due to the operation constraints of the 413 ADV. The deviations between the depth-averaged velocities obtained by this method and those 414 calculated by the logarithm profile in whole depth are around 5% [24].

415

The calculating dimensions in the numerical experiments were  $4.0 \text{ m} \times 0.6 \text{ m} \times 0.6 \text{ m}$ , which are consistent with the turbulent regime used by Wang et al. [38]. The roughness heights of the glass wall and the gravel bed were set to  $k_s = 0.02 \text{ mm}$  and  $k_s = d_{50}$ , respectively [39].  $k_s$  is the same in the glass bed as the wall. A uniform grid size  $\Delta x = \Delta y = 0.02 \text{ m}$  and time step of 0.002 s were used in the computation. Eleven typical cases of different gravel  $d_{50}$  and Reynolds numbers (Table 1) were analyzed. Considering the weight balance between the boundary conditions and fully turbulent development in regards to the effects of the turbulent structure in 423 the numerical flume, the inflow unit volume flux and outflow water depth were set to  $H_0U_0$  and 424  $H_0$ , respectively.

425

426 According to the measurement results,  $\hat{k}$  was strongly dependent on the flow conditions when 427  $k_s$  was constant and it increased as Re increased. It is demanding to make any definite 428 conclusion regarding the effects of  $k_s$  on  $\hat{k}$ , however, because it is too difficult to keep Re or 429 Fr neatly constant in any experiment. The ADV operation limitations and geometrical 430 inhomogeneity over the gravel bed were likely to be responsible for this phenomenon.

431

432 The numerical results of the models derived from different expressions of  $P_{kV}$  and  $P_{kV}$  are also presented in Table 1. The PF values deviate slightly from the measured data, but there is 433 434 reasonable agreement between them for the given ranges of  $k_s$  and Re. The RRF results 435 contained larger error than PF considering the whole range of results. The average of the error for all the test cases C1 to C11, for the PF and RRF models are, respectively, 49.67 and 436 437 108.45%. With low bed roughness,  $k_s < 5 \text{ mm}$ , both sets of results deviate gradually from the 438 experimental values as  $k_{e}$  decreases. This behaviour can be attributed to the anisotropic 439 tendency under which turbulent energy is redistributed over a smooth bed more slowly than 440 over a rough one, which may be enhanced as roughness size decreases. Overall, the results 441 show that the proposed model can effectively simulate turbulent flows over most of the gravel 442 bed.

#### 443 **3.2 Turbulence of open-channel flow in a** 90° bend

444 Furthermore, the performance of numerical models PF and RRF and other models presented by Cea et al. [11] was compared against turbulent flows in open channel with a 90° bend based 445 446 on the experimental conditions described by Bonillo [40]. The experimental setup was identical 447 to that described by Cea et al. [11], as shown in Fig. 3. The flow domain was made of two 448 straight flat sections linked by a 90° bend. The length and width of the first section were 4.835 449 m and 0.86 m, respectively; those of the second section were 4.43 m and 0.72 m, respectively. 450 The bed of Segment 1 is 0.013 m higher than the bottom of Segment 2. The bottom and two 451 sidewalls of the open channel are made of smooth concrete.

452

For calculation convenience and comparability among similar models, the flow region was discretized using a uniform grid of  $\Delta x = \Delta y = 0.02$ m. The Manning's coefficient of the bed surface selected was the same as Cea et al.'s [11] 0.016 s/m<sup>1/3</sup>. The roughness height of the 456 sidewall surface was assumed to be  $k_s = 0.001 \text{m}$  [39]. The time step was fixed to  $\Delta t = 0.005 \text{ s}$  to maintain numerical stability. The resulting  $\hat{k}$  values at three different cross sections are shown 457 458 in Fig. 4. The values calculated by two classical turbulence models [11], the KE model and 459 RSM model, are also included. Cea et al. [11] also developed a finite volume model to solve 2D 460 SWEs, in which two famous turbulence models were used for comparison. The KE model is 461 based on the assumption of isotropic eddy viscosity to solve the Reynolds stresses, while the 462 RSM model directly solves each Reynolds stress without any restrictive hypothesis. Though 463 the KE model equations are very similar to those of the RRF model, the location of H in the 464 diffusion term and the value of  $\sigma_{c}$  in the former differ from those of the latter.

465

466 As shown in Fig. 4, the PF results are very close to the experimental data in both the left sidewall area  $(0 \le x \le 4.955)$  and right sidewall region  $(5.195 \le x \le 5.555)$ , where B is the width of the 467 468 channel. There are varying degrees of deviation in the numerical curves of the other three 469 models. In short, the flow features in both regions can be captured adequately by the PF model. 470 In the intermediate region (4.955  $\leq x \leq$  5.195), none of the numerical curves matched the 471 measured data. This may be because the basic assumption of the shallow water equations is 472 difficult to satisfy in the strong shear and bend zone, which includes intense 3D turbulence. The 473 proposed model yielded accurate results overall despite some data scattering in the shear region.

#### 474 3.3 Turbulent characteristics in an expanding section

An additional experiment was conducted to determine whether the proposed model can 475 476 simulate the turbulent flows on an expanding channel [24]. The experiment was carried out in 477 a flat expanding flume at the Hydraulic Engineering Laboratory at National University of 478 Singapore. The length, width, and depth of the flume are respectively 15 m, 0.6 m, and 0.6 m. 479 As shown in Fig. 5, the widths of the channel upstream and downstream of x = 0 are 0.3 m and 480 0.6 m, respectively. The steady flows were strictly controlled by two pumps and a tail gate during the experiment; boundary conditions were the discharge at upstream (0.024 m<sup>3</sup>/s) and 481 482 the flow depth at downstream (0.015 m), respectively. 137 regular points of the intersection 483 were set between the longitudinal coordinates x = -0.10, 0.25, 0.50, 0.75, 1.00, 1.25, 1.50, 1.75, 1484 2.00, 2.25, 2.50, 2.75, and 3.00 m and the lateral coordinates y = 0.05, 0.10, 0.15, 0.20, 0.25, 0.2485 0.30, 0.35, 0.40, 0.45, 0.50, and 0.55 m to observe velocity profiles and further inspect 486 turbulence changes.

The three-dimensional flow velocities were measured with a SonTek/YSI 16-MHz MicroADV with the sampling rate of 50Hz and the outputs of SNR and correlation factor from the

490 instrument were monitored following procedure already published in literature [24]. Similar to 491 the process in Section 3.1, the depth-averaged data  $(U, V, \hat{k}, \text{ and } \hat{\varepsilon})$  were further obtained.

492

493 We used identical numerical settings and discretization as Lin [24] to simulate turbulent flows 494 in this study. The computational analysis was performed in a rectangular region of 9.0 m × 0.6 m and differentiated by a 180x30 uniform grid with increments of  $\Delta x = 0.05$  m 495 496 and  $\Delta y = 0.02$  m; the length and width of the narrow channel upstream were 2.0 m and 0.3 m, 497 respectively. The upstream and downstream boundary conditions were unit volume flux of  $0.08 \text{ m}^2/\text{s}$  and water depth of 0.15 m, respectively. The Manning coefficient of the bed was 498  $m = 0.01 \text{ s/m}^{1/3}$  and the sidewall was considered to be smooth. The time step used was 499 500  $\Delta t = 0.001 \,\mathrm{s}\,.$ 

501

502 The computed longitudinal velocities at different transverse sections were non-dimensionalized 503 by the approach velocity  $U_0$  and compared against the experimental results as shown in Fig. 6. 504 In the upstream region without extension, i.e.,  $X_a=-0.1$  m, the U-velocity distribution was highly uniform. The sudden expansion in the profile of the sidewall induces strong non-uniformity to 505 506 the velocity profiles, which was clearly observable per the flow separation and wake region in 507 the detached flow. A recirculation zone (i.e.,  $0 \le x/B \le 8$ ), which was generated mainly due 508 to the stagnant effect of the right sidewall of the building and the southern boundary of the 509 channel, could also be clearly seen. In the downstream section, the longitudinal velocities 510 gradually tended towards uniformity. By contrast, the maximum forward and backward 511 velocities for both methods closely matched experimental data after the change in channel width, 512 especially in the circulation region.

513

514 Similar to the U-velocity profiles, the non-dimensional transversal velocities calculated by the 515 two models are shown in Fig. 7. In the main flow region (the area between y = 0.3 and 0.6 m), 516 the computed results agree fairly well with experimental data. A steep velocity gradient 517 occurred downstream of the building due to the strongly deflected flow. In the circulation zone 518 (from y = 0.0 to 0.3 m), the velocity changes computed via *RRF* method do not agree very well 519 with the experimental data. The proposed method agrees slightly better with the experimental 520 data but still underestimates the actual velocity by an average of about 50%. In that region, the 521 distribution of horizontal velocities is quite skewed over the full depth. The improved 522 turbulence model does not sufficiently offset the defect of the hydrodynamic assumption in the 523 deflected zone.

Figure 8 shows a comparison among computed  $\hat{k}/U_0^2$  values and experimental data. The 525 526 proposed method vielded close agreement in the transverse section located  $X_a$ =-0.1 m upstream 527 of the abrupt extension, in which the statistical turbulence features are similar to the turbulent 528 characteristics in the open-channel uniform flow. The RRF results, by contrast, overestimated by about 10%. At the upper-right corner of the building, where the flow separation began, 529 530 sizable boundary irregularities were a source of turbulent energy in the horizontal direction. 531 The horizontal bursts of turbulent activity propagated downstream and expanded on both sides, forcing the  $\hat{k}$  values towards uniformity. Despite some scattering in the circulation zone, *PF* 532 yielded slightly more accurate results than RRF overall. 533

534

535 The dimensionless profiles of turbulent dissipation  $\hat{\varepsilon}$  calculated by the two models were compared against experiment data as shown in Fig. 9. In the main area and circulation zone, 536 537 the PF results were a better fit to the data than the RRF results. In the transitional region between 538 them, especially near the corner of the building, high levels of energy dissipation were produced 539 due to large-scale eddies and a steep velocity gradient. The proposed method better reflected 540 this phenomenon than the RRF, but still overestimated it by around 80%. The difference is 541 mainly attributable to experimental error due to ADV operation limitations and partly by the 542 strong 3D flow structure in corresponding regions. These results altogether indicate that PF can 543 better describe the hydraulic and turbulent structure in the abrupt expanding channel than *RRF*.

#### 544 4 Turbulent Flows near Two Groins in a Natural Waterway

To further investigate the performance of the model developed and illustrate its engineering application, it was used to compute complex turbulent flows and the correspondent navigation conditions in natural waterways and waterways after the construction of two buildings.

#### 548 4.1 Site description and numerical setup

549 The Yangliu moraine is located in a relatively straight gorge on the upper reach of the Yangtze 550 River, approximately 1017.8 km upstream of Yichang City, a prefecture-level city in Hubei 551 Province, China. The length and width of the moraine are respectively 1800 m and 400 m, as 552 shown in Fig. 10. The top level of the moraine near the mid-channel, where the highest point is 553 5 m above the designed water level, is higher than the shoreline. To this effect, the unique bed 554 structure forms a concave basin. The water level in the river must be at least 1 m higher than 555 the designed level to satisfy the necessary flow conditions. Under the restriction of the moraine, 556 the main channel was squeezed to only 250 m in width. Another upstream moraine section of 557 the main reach, the Huangjia moraine, is affected by a shorter lateral flow area with 300 m. A

transitional shallow zone (width 500 m) was formed between the two moraines.

559

The transitional region, in which the flow is relatively slow, has a flat and straight geometric bed. There is no erosion of river bed material along the ship route during the dry seasons due to hydrodynamic limitations, hence there is only a small water depth for navigation during this period. The minimum depths were recorded in 1993 and 2006, 2.3 m and 2.5 m, respectively. Under these hydraulic conditions, it is very challenging to satisfy the class III navigation conditions necessary for free travel of ships with dimensions 560 m × 50 m × 2.7 m.

566

To guarantee class III navigational standards throughout the entire year, the local waterway bureau constructed two groins on the left side of the shallow region in 2008 (Fig. 10). Groin 1 was built at the upstream reach with a  $60^{\circ}$  angle between its axis and the main stream for smooth flow transition. Groin 2 was constructed at the downstream end with a corresponding angle of  $75^{\circ}$ . The length of the two groins are respectively 281 m and 313 m; both of their hook heads are 87 m.

573

The local waterway bureau measured the bed topography of the reach, the water surface elevation on the shipping route, and the flow velocity in three streamlines on January  $15^{\text{th}}$ , 2010, to investigate the effects of the two groins on the waterway (Fig. 10) and the consequent riverbed erosion. For this specific date, the total discharge recorded at the upstream section was  $3120 \text{ m}^3$ /s and the average water level at the downstream section was 253.44 m, values derived by a nearby hydrological station and a water gauge, respectively.

580

According to the geological analysis conducted to characterise the properties of the soil in the two boreholes (N1 and N2, as shown in Fig. 10), the bed materials of the transitional shoal region are mainly composed of boulders, sand-cobbles, and brick red sandstones. The mixture of boulders and sand-cobbles typically forms a covering layer 2.3 m thick above the base layer composed by sandstones. The maximum boulder particle-size is 0.9 m and the mass percentage of sand-cobble with 0.03-0.2 m diameter is about 65%. The sieving results at N1 and N2 indicate that  $d_{50}$  in the reach is approximately 0.04 m.

588

589 The river section that was simulated within the model developed to verify its applicability is 590 1964 m long and 924 m wide, based on the topographic features of Yangliu and Huangjia 591 moraines (Fig. 10). The region that was computed was discretized by applying a uniform 592 Cartesian grid size with dimensions  $\Delta x = \Delta y = 4$  m. The median particle size of the bed material was set at  $d_{50} = 0.04$  m and the time step was set at  $\Delta t = 0.002$  s. A flow rate of 3120 m<sup>3</sup>/s and an averaged water surface elevation of 253.44 m were respectively assigned to the inflow and outflow boundaries according to the simplified methods presented by Zhang [41].

#### 596 4.2 Results and performance

597 Figure 11 shows the comparisons between observed and simulated water levels along the ship 598 route. The average discrepancy between observed data and PF results is 0.124 m, while the 599 discrepancy between observed data and RRF results is 0.127 m. Although PF slightly 600 outperforms RRF, especially in the transition section, both have discrepancies from the 601 measured data. This is mainly due to the uniform roughness coefficient that was imposed in the 602 whole river, which does not replicate accurately the natural variety of roughness along the 603 system. In fact, the bed material is uneven in both longitudinal and transverse directions and 604 the bed structure is irregular in such a natural channel hence the bed resistance status could not 605 be characterised by a uniform median size as assumed in this study. Therefore, there is huge 606 potential to greatly improve the results if  $d_{50}$  was obtained at each specific site for the 607 numerical calculations.

608

609 The flow velocity along three different streamlines was computed and compared against the 610 measured values as shown in Fig. 12. Overall, the calculated curves agree well with the 611 experimental data except in the transition region of Streamline 2, where the maximum absolute 612 deviation was about 0.3 m/s. Similar to the measured water surface elevations, the surveyed points of Streamline 2 were mainly distributed on the route. The  $d_{50}$  in the transitional area 613 was generally underestimated. Although there were no significant differences between the two 614 615 numerical results at most points, PF was more accurate than RRF near the two groins (the groins are approximately at x = 900 and x = 1200 m, PF model is more accurate between  $x \sim 800-1300$ 616 m). Because the turbulence parameters were not measured, we only depict the numerical  $\hat{k}$  at 617 618 two cross sections symbolically to reflect the relevant turbulence characteristics (Fig. 13). The 619 two sections, A-A and B-B (displayed as dash lines in Fig. 10 and their results presented in Fig. 620 13), are located downstream of the two groins where the longitudinal distance to the root of the 621 groin is approximately equal to the length of the corresponding groin (Fig. 10). As shown in Fig. 13, the numerical values of *RRF* are about 2 times the *PF* results in the mainstream area 622 623 and approximately 1.5 times *PF*'s in the circulation zone behind the groin. Furthermore, for 624 each method, the numerical values at B-B were larger than those at A-A. 625

To further explore the navigation scenario discussed above, we calculated the water depth by the proposed model as shown in Fig. 14. In the transitional region of a straight waterway, the water depth was at least 3.5 m and the width of the water surface was greater than 80 m. To this effect, the river would satisfy category III navigation conditions during the dry season. Our results altogether showed that flow behavior in a natural river can indeed be captured with a reasonable accuracy by the proposed method.

#### 632 **5** Conclusions

This study focused on developing a second-order numerical scheme of spatial staggered-grid difference and temporal leap-frog discretization for simulating the turbulent flows on a complex roughness bed. The model is based on the 2D SWE model and the  $\hat{k} - \hat{\varepsilon}$  turbulent closure model. The depth-averaged vertical turbulent generation from the universal notions of the Kolmogorov -5/3 spectrum and the log-law was derived and used as a substitute for the vertical velocity gradient term of the standard  $\hat{k} - \hat{\varepsilon}$  model. The proposed  $\hat{k} - \hat{\varepsilon}$  model reflects the vertical turbulent production of various scales more robustly than the standard model.

640

Extensive comparisons were conducted against complex turbulent flows between the proposed model, standard  $\hat{k} - \hat{\varepsilon}$  model, and measurement data. The proposed method effectively captured the experimental hydrodynamic features, especially the turbulence characteristics, and improved the simulation accuracy over the standard  $\hat{k} - \hat{\varepsilon}$  model. The proposed model also showed better global performance than other 2D shallow numerical schemes.

646

Furthermore, the turbulent flows over the roughness bed in a natural river were simulated and analyzed. Results showed that the depth-averaged turbulent energy increases as Reynolds number increases when the roughness height is constant. Additionally, the numerical results for Yangliu moraines reach showed that the river navigation conditions are satisfied after constructing the two groins under the flow conditions we considered.

652

653 3D simulations will even more adequately disclose the fundamental physics of flows. In this 654 present model application, a large flow domain (Yangliu moraines reach) was considered hence 655 fully 3D computations would have not been very cost-effective. By using the proposed 2D 656 Shallow Water Equations with improved turbulence modelling techniques, it was possible to 657 achieve reasonably engineering accuracy but with a much lower CPU cost. Despite that, 658 considering that 3D analysis would provide a more accurate predictive tool for the flow 659 problems and promote a deeper understanding of the physics of the fluid motion, future work 660 will target the development of an enhanced quasi-three-dimensional shallow flow solver.

- 662 Per the large amplitude and gradient of turbulent energy near the structures, local scouring may
- occur in rainy seasons and gradually alter the bottom configuration, affecting the stability of
- the groins. To safeguard the regulation buildings, an effective sediment transportation model is
- 665 necessary to investigate the bed deformation and future research should incorporate more cases
- to replicate accurately a variety of scenarios to achieve a universal model that can be reliable
- 667 for each situation.

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#### 676 Notation

677	f	= bed friction factor (-)
678	g	= gravitational acceleration (ms <sup>-2</sup> )
679	Н	= water depth (m)
680	k	= turbulent energy $(m^2s^{-2})$
681	$\hat{k}$	= depth-averaged turbulent energy $(m^2s^{-2})$
682	$k_s$	= equivalent sand roughness (m)
683	$l_m$	= length scale of turbulent flow (m)
684	т	= Manning's roughness coefficient (sm <sup>-1/3</sup> )
685	<i>P</i> , <i>Q</i>	= unit volume flux in x - and y -directions, respectively $(m^2s^{-1})$
686	R	= hydraulic radius (m)
687	Re	= Reynolds number (-)
688	$T_{xx}, T_{yy}$	= depth-averaged normal stress in $x$ - and $y$ -directions, respectively (Pa)
689	$T_{yx}, T_{xy}$	= depth-averaged shear stress in $x$ - and $y$ -directions, respectively (Pa)
690	u <sup>*</sup>	= velocity scale of turbulent flow (ms <sup>-1</sup> )
691	<i>u</i> <sub>*</sub>	= friction velocity (ms <sup>-1</sup> )
692	U, V, W	= depth-averaged velocity in $x$ -, $y$ - and $z$ -directions, respectively (ms <sup>-1</sup> )

693	<i>u</i> , <i>v</i> , <i>w</i>	= instantaneous velocity in $x$ -, $y$ - and $z$ -directions, respectively (ms <sup>-1</sup> )
694	$\overline{u}, \overline{v}, \overline{w}$	= ensemble-averaged velocity in $x$ -, $y$ - and $z$ -directions, respectively (ms <sup>-1</sup> )
695	<i>u'</i> , <i>v'</i> , <i>w'</i>	= fluctuating velocity in $x$ -, $y$ - and $z$ -directions, respectively (ms <sup>-1</sup> )
696	$\langle u  angle, \langle v  angle, \langle w  angle$	$v\rangle$ = mean velocity in x-, y - and z -directions, respectively (ms <sup>-1</sup> )
697	$\ u'\ , \ v'\ , \ w$	= turbulence intensity in x-, y - and z -directions, respectively (ms <sup>-1</sup> )
698	<i>x</i> , <i>y</i> , <i>z</i>	= streamwise, spanwise, and vertical coordinates, respectively (-)
699	$Z_b$	= bed elevation (m)
700	ε	= turbulent dissipation $(m^2s^{-3})$
701	$\hat{\mathcal{E}}$	= depth-averaged turbulent dissipation $(m^2s^{-3})$
702	η	= free surface elevation (m)
703	ν	= turbulent viscosity $(m^2s^{-1})$
704	$\mathbf{v}_k$	= kinematic viscosity $(m^2s^{-1})$
705	$\hat{v}_t$	= depth-averaged turbulent viscosity $(m^2s^{-1})$
706	ρ	= fluid density (kgm <sup>-3</sup> )
707	τ	= total shear stress (Pa)
708	$ au_b$	= bed shear stress (Pa)
709		

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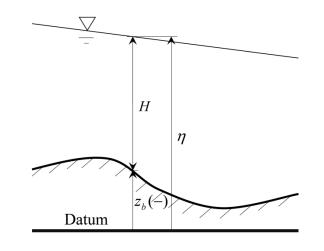
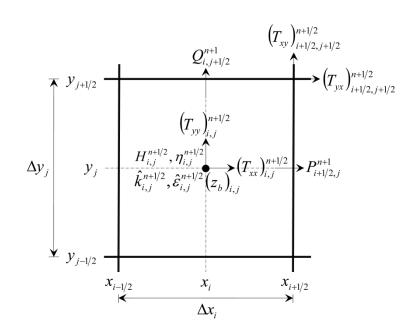
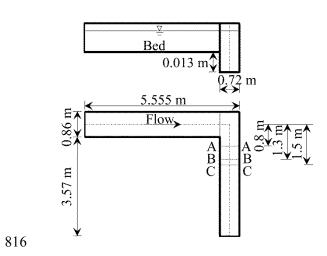


Figure 1 - Scheme illustrating an example of irregular bed elevation and free surface waterdepth.



812 Figure 2 - Scheme of staggered grid which includes the locations of the variables considered in813 a single cell.



817 Figure 3 – Scheme of the experimental channel with a 90° bend: front view (top) and top view

- 818 (bottom).
- 819

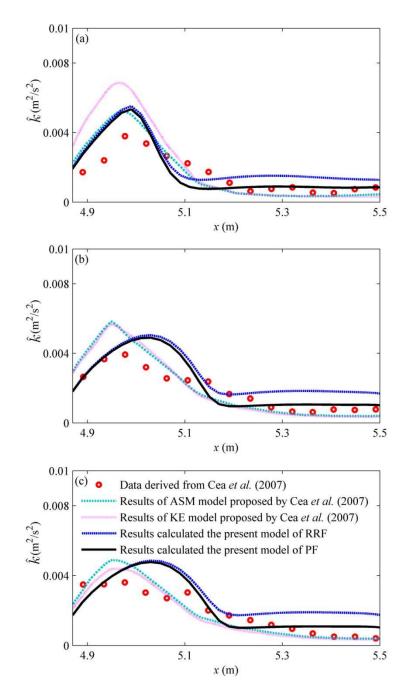
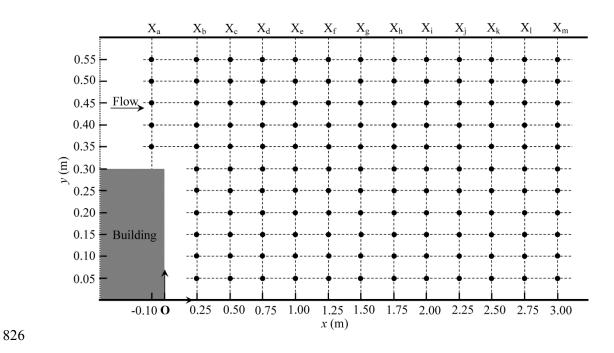


Figure 4 – Comparison of turbulent kinetic energy measured experimentally and calculated
numerically at three sections (a) A-A, (b) B-B and (c) C-C.



827 Figure 5 - Plan view of flume with an expanding section and the observed points.

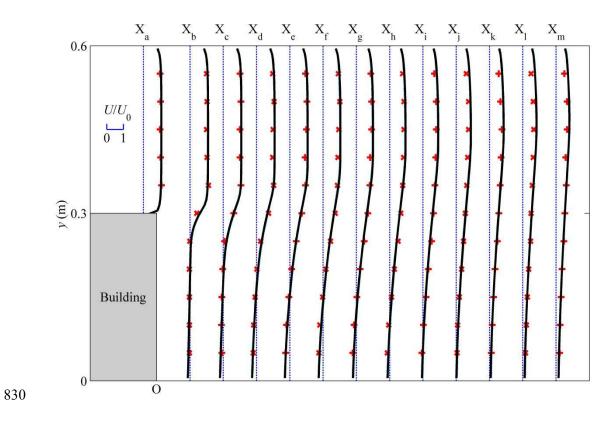


Figure 6 - Comparisons of non-dimensionalized *U* between numerical results and experimental
data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
results).

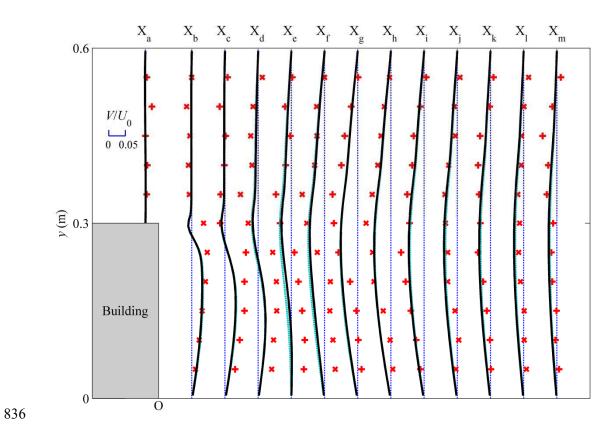


Figure 7 - Comparisons of non-dimensionalized V between numerical results and experimental
data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's
results).

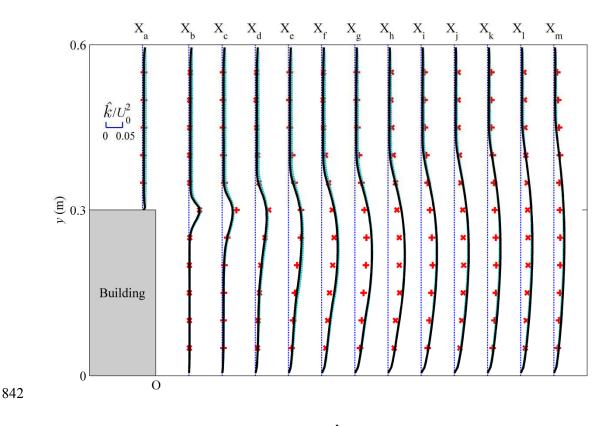
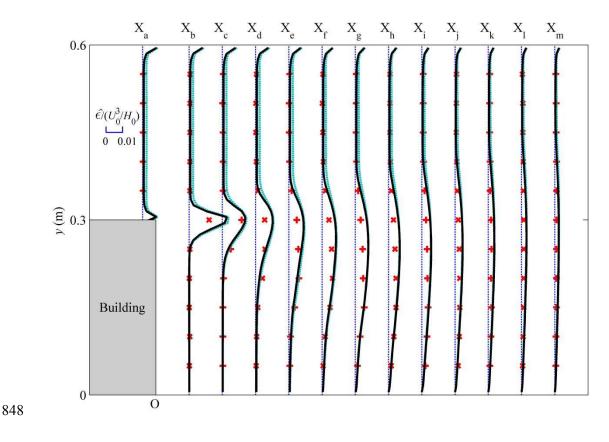


Figure 8 - Comparisons of non-dimensionalized  $\hat{k}$  between numerical results and experimental data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's results).



849Figure 9 - Comparisons of non-dimensionalized  $\hat{\varepsilon}$  between numerical results and experimental850data (Red crosses: experimental data; Dashed green line: RRF's results; Solid black line: PF's851results).

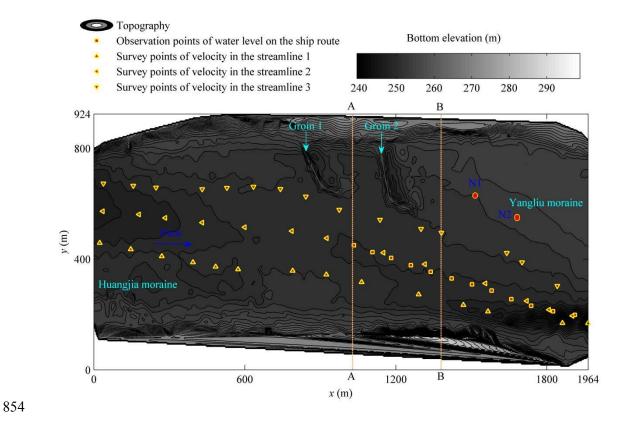


Figure 10 - Bed topography of Yangliu moraine reach and location of observation points.

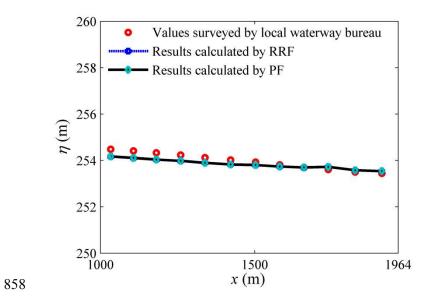


Figure 11 - Water level comparison between observed data and computed results on the shiproute.

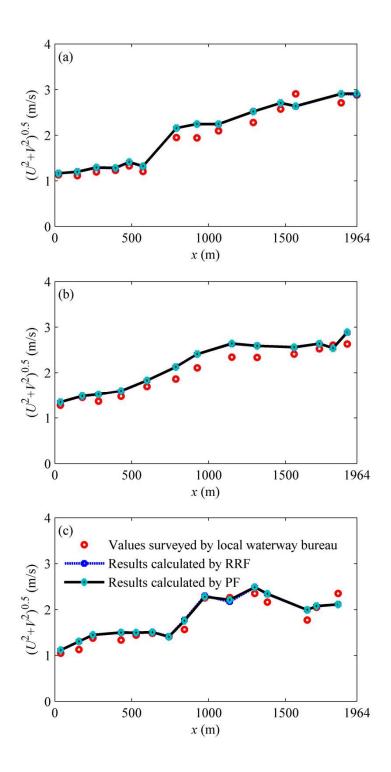


Figure 12 - Flow velocity comparison between measured values and calculated results in the
three streamlines: (a) streamline 1, (b) streamline 2 and (c) streamline 3.

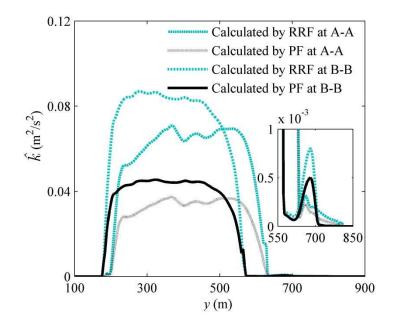


Figure 13 - Comparisons of the numerical results between PF and RRF at the sections of A-Aand B-B behind the two groins.

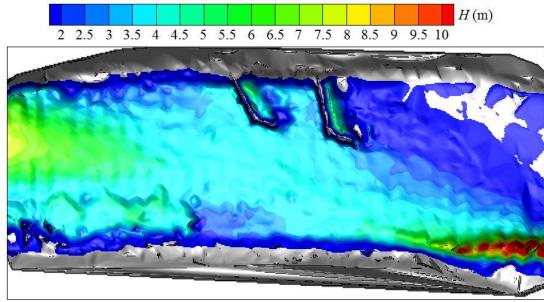


Figure 14 - Water depth calculated by the proposed model.

Case	k <sub>s</sub>	H	$U_{0}$	Re	Fr	$\hat{k}$ acquired	$\hat{k}$ simulated by PF		$\hat{k}$ simulated by RRF	
						from	Results	Relative	Results	Relative
	mm	cm	cm/s			measurements	$(\times 10^{-3}) \text{ m}^2/\text{s}^2$	Absolute	$(\times 10^{-3}) \text{ m}^2/\text{s}^2$	Absolute
						$(\times 10^{-3}) \text{ m}^2/\text{s}^2$		Error %		Error %
C1	0.02	50.2	34.0	170,680	0.15	2.83	0.33	88.3	0.77	72.8
C2	2	42.0	36.2	152,040	0.18	2.36	0.70	70.3	1.40	40.7
C3	5	24.8	65.3	161,944	0.42	3.41	3.20	6.2	5.83	71.0
C4	10	19.6	46.3	90,748	0.33	1.85	2.04	10.3	3.51	89.7
C5	10	30.7	57.8	177,446	0.33	3.81	2.84	25.5	5.02	31.8
C6	10	19.4	101.0	195,940	0.73	5.27	8.48	60.9	14.69	178.7
C7	20	31.8	42.7	135,786	0.24	2.35	1.84	21.7	3.12	32.8
C8	20	28.1	63.5	178,435	0.38	2.45	4.14	69.0	6.96	184.1
C9	40	28.8	35.4	101,952	0.21	0.89	1.55	74.2	2.49	179.8
C10	40	29.5	62.5	184,375	0.37	3.24	4.70	45.1	7.60	134.6
C11	40	17.5	110.5	193,375	0.84	7.22	12.63	74.9	20.00	177.0

Table 1. Hydraulic data collected with the experiments and numerically calculated.

878  $k_s$ : gravel median diameter  $d_{50}$ , H and  $U_0$ : average vertical distance from gravel bed to

879 water surface and bulk free-stream velocity in the middle section of the experimental flume,

880 respectively.