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## Open-path Fourier transform infrared studies of large-scale laboratory biomass fires

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**Abstract.** A series of nine large-scale, open fires was conducted in the Intermountain Fire Sciences Laboratory (IFSL) controlled-environment combustion facility. The fuels were pure pine needles or sagebrush or mixed fuels simulating forest-floor, ground fires; crown fires; broadcast burns; and slash pile burns. Mid-infrared spectra of the smoke were recorded throughout each fire by open path Fourier transform infrared (FTIR) spectroscopy at  $0.12\text{ cm}^{-1}$  resolution over a 3 m cross-stack pathlength and analyzed to provide pseudocontinuous, simultaneous concentrations of up to 16 compounds. Simultaneous measurements were made of fuel mass loss, stack gas temperature, and total mass flow up the stack. The products detected are classified by the type of process that dominates in producing them. Carbon dioxide is the dominant emission of (and primarily produced by) flaming combustion, from which we also measure nitric oxide, nitrogen dioxide, sulfur dioxide, and most of the water vapor from combustion and fuel moisture. Carbon monoxide is the dominant emission formed primarily by smoldering combustion from which we also measure carbon dioxide, methane, ammonia, and ethane. A significant fraction of the total emissions is unoxidized pyrolysis products; examples are methanol, formaldehyde, acetic and formic acid, ethene (ethylene), ethyne (acetylene), and hydrogen cyanide. Relatively few previous data exist for many of these compounds and they are likely to have an important but as yet poorly understood role in plume chemistry. Large differences in emissions occur from different fire and fuel types, and the observed temporal behavior of the emissions is found to depend strongly on the fuel bed and product type.

### Introduction

Biomass burning injects significant amounts of trace gases and particles into the regional and global atmosphere [Crutzen and Andreae, 1990]. Quantification of representative emissions from fires is difficult, and different configurations of analysis techniques and sampling platforms have been utilized. Aircraft can probe a large area of well-mixed, integrated emissions, investigate secondary chemistry, and provide details on transport [Andreae *et al.*, 1988a, b]. However, airborne sampling is expensive; it is difficult to monitor a single fire continuously from beginning to end; and specific knowledge of the fuels and fire types are difficult to correlate with measurements. Ground-based measurements provide the opportunity for more detail on the fire and fuels [Delmas *et al.*, 1991] but may tend to incorrectly estimate the emissions in the convection column above the fire [Andreae *et al.*, 1988a]. Tower-based measurements have been implemented

as a means of more representative ground-based sampling [Ward *et al.*, 1992].

There are a number of advantages in studying biomass fires in the laboratory. They include burning under controlled conditions, where the chemical and physical properties of the fuel and environment may be known in detail, and capture of all the smoke for the entire course of the fire so that emission factors for any measurable airborne species can be determined accurately. The laboratory characterization of the products of biomass burning began with work to assess the contribution of forest fires in the southeastern United States to regional air pollution [Ryan and McMahon, 1976] and the emissions due to burning agricultural waste [Darley *et al.*, 1966] or wood for heat [Dasch, 1982]. This early work often distinguished between flaming and smoldering combustion, distillation and pyrolysis, and normally featured detection of  $\text{CO}_2$ , CO, and  $\text{NO}_x$ . Formic acid and acetic acid were later added to the range of products detected in laboratory fires [Talbot *et al.*, 1988]. The laboratory experimental fires of Lobert *et al.* [1991] were the first to characterize a wide variety of emission products of particular importance to atmospheric chemistry.

In addition to the challenges presented by the need to sample fires representatively, there is the additional challenge of

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identifying instrumental techniques that can cope with hot, reactive samples where the potential for chemical interference and the dynamic range of concentrations is very high. The companion work to the study described here was the first application of open-path FTIR spectroscopy to the analysis of smoke from biomass burning and focused on prescribed fires in sagebrush and forestry operations in the western United States [Griffith *et al.*, 1991]. This paper demonstrated the advantages of an FTIR-based study of biomass fires: (1) Simultaneous measurements can be made of a wide variety of species with good selectivity (i.e., resistance to interference) over a wide range of concentrations with detection limits in the low parts per billion range. (2) Measurements can be made pseudocontinuously in real time so that dynamic processes can be followed. (3) There is no need to take samples and no possibility of sampling- or storage-related artifacts so that reactive gases can be quantified. (4) The measurement is path integrated, averaging over small-scale local variations. It is thus relatively immune to spatial variation compared with point sampling.

This work extends the open-path FTIR field studies of Griffith *et al.* [1991] to controlled fires in a large-scale combustion laboratory at the Intermountain Fire Sciences Laboratory (IFSL). This paper describes a preliminary study in which measurements of smoke composition for up to 16 chemical species from 9 biomass fires were made in October 1989. The study demonstrates the potential of the open-path FTIR technique for laboratory fires and provides a sufficient body of data to yield significant insights into biomass fire emissions. The technique will be further developed and applied with a dedicated FTIR system recently installed in the IFSL combustion laboratory.

## Methods

### Fire and Fuel Types

Table 1 summarizes the fuels burnt in each of nine experimental fires. The fuels were selected for the fires with several objectives in mind. There were two fires each of brown ponderosa pine needles (fires 3 and 5) and freshly cut sagebrush (fires 8 and 12), which offered the opportunity to measure separately the products of important fuel components in western United States land management fires, to qualitatively investigate the natural variation in nominally identical fires and, especially from the pine needles, to investigate the temporal behavior of fire emissions in a relatively simple fuel bed.

Many important biomass fires burn in an inhomogeneous mixture of several fuels [Kauffman *et al.*, 1994; Seavoy, 1973]. We therefore included preliminary simulations of widely occurring natural and anthropogenic fire types. Two of the fuel beds (fires 9 and 10) contained litter and "duff" (partially decomposed organic matter) and represent attempts to simulate a typical forest-floor ground fire in a coniferous forest. A further common type of wildfire is the crown fire which, along with the ground fuels, consumes the foliage of live, mature trees. A low-intensity crown fire was simulated by fire 11, which featured vertically oriented green pine limbs over a base of litter, dry needles, and small woody fuel. Finally, the two main fire types used to dispose of "activity fuels" (logging waste or harvesting residues also termed "slash") were also simulated. Unpiled, scattered fuels were burned in fire 6, a broadcast burn simulation, and fire 7 simulated burning piled, woody logging waste.

Fuel contents were not systematically determined due to malfunction of the CHN analyzer. Where required in calcula-

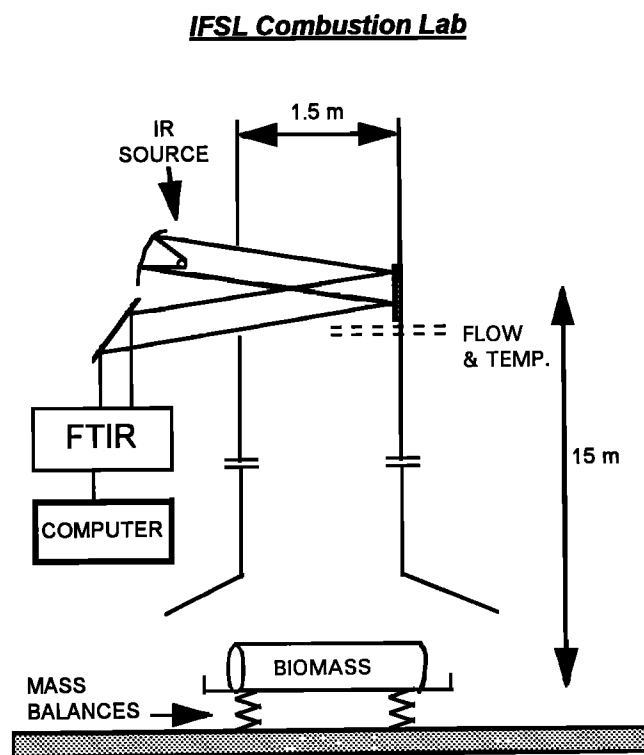
**Table 1.** Fuel Components and Amount Used for Fire-Type Simulations

Fire Type	Number	Fuel Bed Composition	Mass Percent	Comment
Pine needle 1	3	pine needles	100	pinus ponderosa
Pine needle 2	5	pine needles	100	pinus ponderosa
Sagebrush 1	8	sagebrush	100	artemisia tridentata
Sagebrush 2	12	sagebrush	100	artemisia tridentata
Broadcast	6	duff	44	
		pine needles	14	pinus ponderosa
		twigs	18	
		wood	24	
Slash	7	twigs and needles	10	pinus ponderosa
		small branches	90	
Ground 1	9	pine needles	27	pinus ponderosa
		pine needles and duff	73	
Ground 2	10	duff	39	
		twigs and needles	35	pinus contorta
		pine needles	26	pinus ponderosa
Crown	11	twigs and needles	26	pinus contorta
		wood < 30mm	19	pseudotsuga menziesii
		pine needles	19	
		green needles and twigs	36	pinus ponderosa

tions, carbon content is assumed to be the commonly accepted value of 45% of dry matter for all fuels except brown ponderosa pine needles. For this fuel, 51% was assumed based on *Klemmedson* [1975] and a small number of measurements of the composition of subsamples with a Perkin-Elmer 2400 CHN analyzer. The N:C ratio determined from these measurements was 0.6%.

### Experiment

The experimental configuration and FTIR spectrometer have been described previously [*Griffith et al.*, 1991] and are shown in Figure 1. The fuel is burned on an  $\sim 1 \times 2$  m continuously weighed fuel bed, and the smoke captured by a 1.5-m-diameter stack with a 3.6-m inverted funnel opening just above the fuel bed. A sampling platform surrounds the stack 15 m above the fuel bed. The IR light source was collimated and transmitted twice across the stack through the smoke for a total smoke absorption path of 3 m, then focused and recollimated into an EOCOM interferometer with a Ge/KBr beam splitter and InSb/MCT sandwich detector. Spectra were alternately recorded by the InSb ( $1800\text{--}3900\text{ cm}^{-1}$ ) and MCT ( $700\text{--}1900\text{ cm}^{-1}$ ) detectors throughout each fire. Resolution was  $0.12\text{ cm}^{-1}$ , which is approximately the pressure-broadened full width at half height of individual spectral lines. The spectra recorded before the fire were used to determine background levels of  $\text{H}_2\text{O}$ ,  $\text{CO}_2$ ,  $\text{CO}$ , and  $\text{CH}_4$  and to serve as reference spectra to create absorbance spectra from spectra collected during the fire where required. Normally 5-20 scans were coadded over 0.5 to 2 min for each spectrum, with higher time resolution used near the beginning of the fire. Fires typically burnt for about 1 hour, resulting in 25-40 individual spectra per fire.



**Figure 1.** Schematic of the experimental arrangement used to make the measurements.

Mass flow up the stack was measured by a hot wire mass flowmeter (Kurz, model 455). The absolute flowmeter calibration was uncertain, and the flowmeter malfunctioned for fires 9-12, as discussed in more detail below. Temperature was measured by a thermocouple gauge,  $\text{CO}$  and  $\text{CO}_2$  by NDIR (Horiba PIR-2000), and  $\text{NO}$  and  $\text{NO}_x$  by chemiluminescence (Thermolectron model 42). These measurements were logged every 5 s. Samples for auxiliary gas measurements were drawn from the center of the stack near the FTIR beam through  $\sim 30$  m of 0.25" Teflon tube. The fuel bed mass was recorded every 30 s for fires 8-12. The stack gas flow was driven by convection without additional fan forcing. Normal atmospheric pressure at the IFSL is 90.9 kPa. Temperatures in the stack gas absorption path 15 m above the fuel bed ranged from 300 to 420 K.

### Spectrum Analysis

Three different procedures were followed to compute trace gas concentrations from spectra. For most gases, reference spectra were calculated from the HITRAN [*Rothman et al.*, 1992] molecular absorption line parameter database and fitted to the measured spectra using classical least squares (CLS) fitting in selected spectral regions. For species where this was not applicable, either interactive spectral subtraction or peak-height-based analyses using reference spectra were used. The three procedures are briefly described below.

**Synthetic Calibration/CLS-based retrievals.** The Multiple Atmospheric Layer Transmission (MALT)/CLS method is described in detail elsewhere [*Griffith*, 1996]. Briefly, a set of calibration spectra is calculated from the HITRAN database using the program MALT, such that the calculated spectra closely match real experimental spectra over a range of gas concentrations. These spectra are then used as a calibration set for conventional quantitative analysis using CLS methods [*Haaland*, 1990]. In CLS analysis, measured spectra are fitted by least squares with a linear combination of calibration spectra; all absorbing species are simultaneously fitted. For each trace gas species an optimum small spectral region is selected for the gas or gases of interest. The spectral regions used for each gas are listed in Table 2. For each region a set of calibration spectra, including all molecules absorbing in that region, was calculated at 10 K intervals from 290 to 420 K and the analyses of measured spectra were carried out using calibration spectra calculated at the temperature nearest the measured temperature at the time the spectrum was recorded. Figure 2a shows an example of a MALT/CLS fit to an experimental spectrum for  $\text{CO}/\text{CO}_2$  at  $2211\text{--}2243\text{ cm}^{-1}$ .

**Spectral subtraction and peak-height-retrievals.** For species for which spectral line parameters are not available, MALT/CLS cannot be used and more traditional methods are required. This was the case for  $\text{CH}_3\text{OH}$ ,  $\text{C}_2\text{H}_4$ ,  $\text{CH}_3\text{COOH}$ , and terpenes. For  $\text{CH}_3\text{OH}$  a prominent  $Q$ -branch feature appears near  $1033\text{ cm}^{-1}$ , overlapped by single lines of  $\text{NH}_3$ . A calibrated laboratory spectrum of 36.1 parts per million (ppm)  $\text{CH}_3\text{OH}$  in 90.9 kPa  $\text{N}_2$  was recorded in a 5.6-m White cell on a Bomem DA3 FTIR spectrometer at  $0.12\text{ cm}^{-1}$  resolution and used as a reference for interactive spectral subtraction. The absorption coefficient agreed with that derived from the spectrum of *Hanst and Hanst* [1994] within 10%. A MALT-calculated  $\text{NH}_3$  spectrum at the correct temperature was then interactively subtracted from the measured spectrum to remove the  $\text{NH}_3$  absorption lines, followed by interactive

**Table 2.** Spectral Regions Used to Retrieve Concentrations Reported in This Work

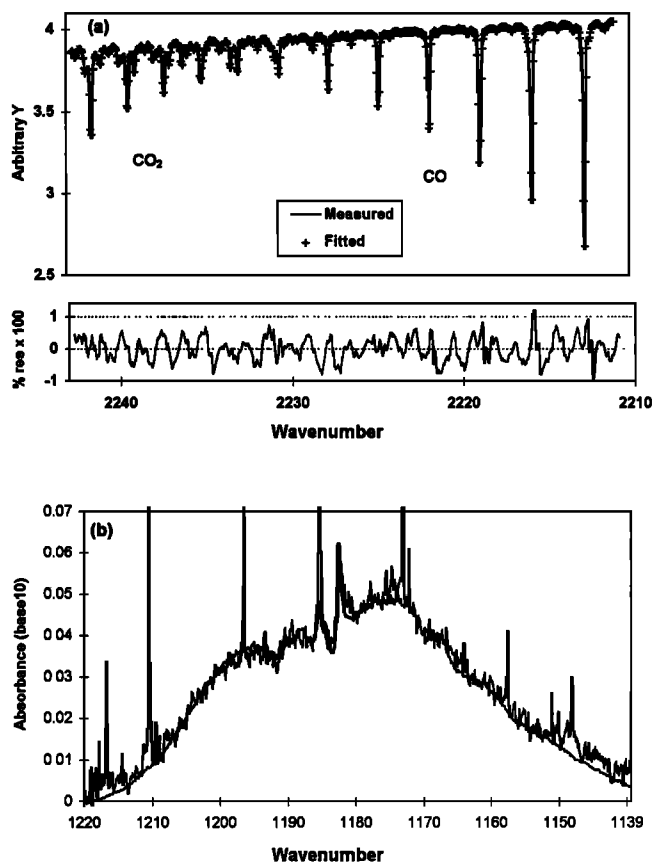
Molecule	Spectral Regions or Peaks	Molecule	Spectral Regions or Peaks
H <sub>2</sub> O	3020.0 - 3007.1	CH <sub>3</sub> COOH	1176 <sup>c</sup>
CO <sub>2</sub> and CO	2242.7 - 2210.9	CH <sub>3</sub> OH	1033.3 <sup>d</sup>
CO <sub>2</sub>	737.01 - 727.92	CH <sub>2</sub> O	2782.7 - 2777.3
CO <sub>2</sub>	2252.8 - 2239.9 <sup>a</sup>	HCOOH	1107.4 - 1102.7
CO	2055.8 - 2049.5 <sup>b</sup>	NO	1913.4 - 1911.0
<sup>13</sup> CO	2062.2 - 2061.7 <sup>b</sup>	NO	1907.1 - 1905.1
CO	2179.7, 2176.2, 2172.8 <sup>a</sup>	NO	1903.8 - 1902.3
CH <sub>4</sub>	3020.0 - 3007.1	NO	1901.1 - 1899.9
CH <sub>4</sub>	2997.3 - 2976.1	NO	1906.9 - 1899.5
CH <sub>4</sub>	1306.7 - 1299.0	NO <sub>2</sub>	1599.5 - 1597.7
C <sub>2</sub> H <sub>4</sub>	949.4 <sup>c</sup>	NH <sub>3</sub>	1047.3 - 1045.1
C <sub>2</sub> H <sub>6</sub>	2987.0 - 2985.7	NH <sub>3</sub>	968.7 - 961.7
C <sub>2</sub> H <sub>6</sub>	2984.7 - 2982.7	NH <sub>3</sub>	933.5 - 926.5
C <sub>2</sub> H <sub>2</sub>	3271.2 - 3254.7	HCN	3272.1 - 3270.7
C <sub>2</sub> H <sub>2</sub>	743.4 - 728.8	SO <sub>2</sub>	1348.5 - 1347.7
Monoterpenes	2930 <sup>c</sup>	OCS	2071.4 - 2069.9

<sup>a</sup>Stronger peaks used only to quantify background.

<sup>b</sup>Regions used only to spot check the precision.

<sup>c</sup>Analysis based on peak height.

<sup>d</sup>See text for details.



**Figure 2.** (a) Example of measured, fitted, and % residual (= (fitted-measured)\*100) spectra from Multiple Atmospheric Layer Transmission/classical least squares (MALT/CLS) analyses for CO and CO<sub>2</sub>. Lines from 2210 to 2235 cm<sup>-1</sup> are due to CO and lines from 2232 to 2245 cm<sup>-1</sup> to CO<sub>2</sub>. Mixing ratios determined from the spectra are 1558 ppm CO<sub>2</sub> and 175 ppm CO. (b) A smoke spectrum from fire 11 together with a scaled reference spectrum for acetic acid from *Hanst and Hanst* [1994]. The additional sharp lines in the smoke spectrum are due to water vapor. The scaling factor and density correction indicate 25.7 ppm acetic acid in the smoke.

subtraction of the reference CH<sub>3</sub>OH spectrum. The scaling factor of the CH<sub>3</sub>OH spectrum required to subtract the CH<sub>3</sub>OH feature from the measured spectrum provided the equivalent CH<sub>3</sub>OH concentration.

For C<sub>2</sub>H<sub>4</sub> and CH<sub>3</sub>COOH the concentrations were based on published reference spectra at appropriate resolution [*Hanst and Hanst*, 1994]. Peak absorption coefficients were determined from the published spectra and applied to peak heights in the measured spectra to retrieve concentrations according to the Beer-Lambert law. For CH<sub>3</sub>COOH and C<sub>2</sub>H<sub>4</sub> the spectral features are broad but not overlapped by other broad features, and their characteristic shapes and positions provide unambiguous identification. Figure 2b shows an example of a measured spectrum from fire 11 together with a reference spectrum for acetic acid taken from *Hanst and Hanst* [1994].

#### Auxiliary Data

The CO<sub>2</sub>, CO, NO, and NO<sub>x</sub> analyzers were calibrated by standard methods using National Institute of Standards and Technology (NIST)-traceable standards. The flowmeter and thermocouple gauge relied on manufacturer's calibrations. To enable comparisons, all data were reduced to a common 1-min time base using a cubic spline interpolation.

#### Accuracy and Precision of Results

In good quality laboratory spectra (S:N > 1000), absolute accuracy using the MALT/CLS method is normally better than 2% [*Griffith*, 1996], whereas for the spectra here the S:N is typically around 100. Analyses of several species was possible from two or more independent spectral regions (e.g., CO<sub>2</sub>, CH<sub>4</sub>, NH<sub>3</sub>, and C<sub>2</sub>H<sub>2</sub>). The agreement in replicate measurements of the same species in different spectral regions for most species is better than 5% at concentrations well above the detection limit and this is taken as a general estimate of the accuracy of the MALT/CLS retrievals (including accuracy of the HITRAN absorption cross sections). In addition, there is a typical sensitivity of ~ 1% K<sup>-1</sup> to assumed temperature. Thus rounding of the analysis temperature to the nearest 10 K (and variation in temperature across the stack of the same order) introduces an additional maximum error of ~ 5%. We

allow a further 4% error for variations in pathlength and background absorption outside the stack due to smoke leakage through the viewing port. In summary, a general estimate of total error in single gas concentration measurements is  $\sim 8\%$  ( $1\sigma$ ) or 1 ppmv, whichever is higher. This implies an accuracy of 11% ( $1\sigma$ ) for emission ratios of compounds due to the same combustion process.

For the specific case of  $H_2O$ , a significant part ( $\sim 20\%$ ) of the total absorption is due to  $H_2O$  at room temperature in the 3-m optical path outside the stack. To avoid large errors due to temperature dependence of the absorption line strengths, for the water analysis we used lines in the spectral window near  $3010\text{ cm}^{-1}$  which were found to be only weakly temperature dependent.

For some species, comparisons are possible with simultaneous measurements by other instruments. Comparisons of FTIR and non-dispersive infrared (NDIR) measurements of CO and  $CO_2$  show excellent relative agreement but with FTIR measurements systematically  $\sim 7\%$  higher than NDIR. Similar comparison of NO by FTIR and chemiluminescence show agreement within 10%. For consistency the NDIR and chemiluminescence measurements have not been used in calculating emission ratios or other derived quantities.

Measurement of total mass flow in the stack by the hot wire flowmeter is subject to error due to the inhomogeneous flow profile and the absolute flowmeter calibration. The errors in fuel bed mass and temperature measurement are assumed to be negligible relative to those in concentrations and flow.

### Derived Quantities

The raw data from each fire consist of time series of concentrations, fuel mass, temperature, and stack gas flow. Concentrations are converted to equivalent mixing ratios at the temperature and pressure of the sample. A number of derived quantities are of use in discussing the following results:

Emission ratio is the ratio of (molar) concentrations of two species, normally as the excess concentrations above background.

Emission factor is the ratio of the amount of a species emitted to the amount of fuel burned in grams per kilogram or moles per kilogram.

Molar emission factor is the ratio of the amount of a particular element in a species emitted to the amount of that element in the fuel burnt, in units of mole per mole. Emission factors are integrated over time and may be defined for the whole fire or for separate fire processes such as flaming and smoldering. Calculation of emission factors from the experimental data is described below.

Combustion efficiency (CE) is the molar ratio of  $CO_2$  emitted to the carbon burned and should be 1.0 for complete combustion. For practical purposes we use modified combustion efficiency (MCE) as the ratio of measured emitted  $CO_2$  to the sum of emitted  $CO_2 + CO$ :

$$MCE = [CO_2] / [CO_2 + CO] \quad (1)$$

on the grounds that  $[CO_2 + CO]$  correlates well with the total carbon burnt [Ward and Radke, 1993]. MCE can be calculated on an instantaneous or time-integrated basis.

### Calculation of Emission Factors

The molar emission factor for species x relative to fuel carbon is determined as the molar flow of x up the stack ( $flow(x)$ ) divided by the molar flow of C in all carbon-containing species up the stack ( $flow(C)$ ):

$$\text{molar EF}(x) = flow(x) / flow(C) \quad (2)$$

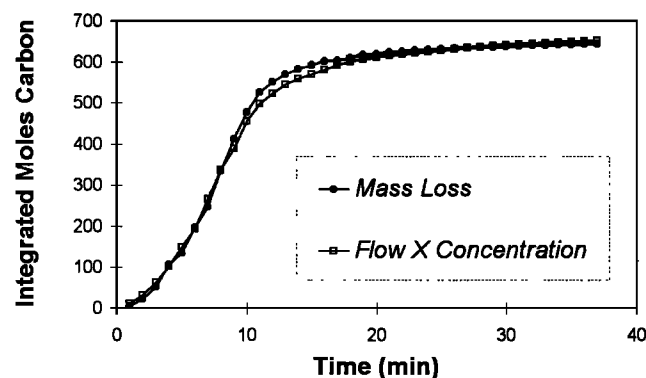
The molar emission factor relative to fuel mass (grams dry matter),  $EF(x)$ , requires the fuel carbon mass fraction,  $C(\text{fuel})$ :

$$EF(x) = \text{molar EF}(x) \times C(\text{fuel}) / 12 \quad (3)$$

$Flow(x)$  is the product of the total molar flow (determined by the flowmeter) times the mixing ratio of x (determined by FTIR). For  $flow(C)$  we take the sum of flows of all measured C-containing species as a close approximation to total C. The molar emission factor for species x times the molecular weight of species x gives the emission factor on a mass ratio basis. This method provides the most reliable emission factors because absolute errors in the flow measurement cancel. It is only important that the relative shape of the flow versus time profile be correct to ensure the correct weightings in calculating time-averaged emission factors.

For fires 9-12 the flowmeter malfunctioned and an independent measurement of flow was required. In principle, the stack flow can also be determined from the measured total fuel mass loss if the fuel composition is known and it is assumed that all smoke is collected by the stack. For fire 8 (sagebrush fuel) both the mass loss and the stack flow were measured and allow an intercalibration of the two methods. Figure 3 shows plots of the integrated carbon loss for fire 8 against time as calculated from both stack flow and from the mass loss, assuming fuel composition of 45% C and 6% H. The flowmeter measurements were scaled by 0.76 to force agreement of the two methods, which provided the effective calibration factor for the flowmeter. The absolute calibration factor so determined may be in error by up to 10% due to the assumption of 45% fuel carbon in the sagebrush fuel. The calibration factor has recently been remeasured in our laboratory to be 0.75 in an independent calibration.

For consistent treatment of all fires, emission factors have therefore been determined from stack flows calculated as follows: For fires 3-7, for which no fuel bed mass data were collected, the measured flow data were used scaled by a calibration factor of 0.76. For fire 8, for which flow and mass



**Figure 3.** Integrated carbon flow up the stack as calculated from the mass loss record and the concentration times flow data (see text for details).

**Table 3.** Emission Factors for Flaming and Smoldering Combustion and for the Total Fire (mole/kg dm (x 100)); Relative Production, Modified Combustion Efficiency, and Fuel Consumption by Smoldering Process for Each Fire

Fire Number/ Type	Combustion Type	$\Delta$ Gas Flaming	Smoldering							Pyrolysis/Distillation							Smoldering			PM2.5 g/kg	
			H <sub>2</sub> O	CO <sub>2</sub>	NO	NO <sub>2</sub>	SO <sub>2</sub>	CO	CH <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	NH <sub>3</sub>	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>2</sub>	HAc <sup>a</sup>	MeOH	H <sub>2</sub> CO	HFo	HCN	MCE		Process
3/ Pine needles	F <sup>a</sup>	5933	4173	10.6	1.14	2.70	40.36	4.64	0.58	0.09	0.56	0.96	0.41	0.11	1.25	bdl <sup>b</sup>	bdl	0.990	22.6	24.2	nd <sup>c</sup>
	S	3570	3334	0.84	bdl	bdl	656.8	126	17.9	12.8	10.8	2.96	17.1	6.69	3.63	bdl	bdl	0.835			
	T	5384	3986	8.33	0.55	1.55	181.4	29.9	4.07	2.94	2.54	1.45	3.95	1.68	1.80	bdl	bdl	0.956			
5/ Pine needles	R	1	2	5	14	12	3	4	6	8	9	13	7	11	10						
	F	5291	4172	8.94	1.33	4.0	42.40	4.62	0.74	0.41	0.87	0.67	0.14	0.22	0.49	bdl	bdl	0.990	18.3	24.5	30.4
	S	5487	3275	0.95	0.08	bdl	702.1	137	22.5	13.6	11.1	5.74	12.1	3.26	4.75	bdl	bdl	0.823			
T	5474	4002	7.87	1.22	2.7	166.4	28.2	4.35	2.84	2.64	1.60	4.14	2.03	0.98	bdl	bdl	0.960				
6/ Broadleaf	R	1	2	5	13	9	3	4	6	8	10	12	7	11	14						
	F	5684	3701	6.56	1.89	0.68	41.45	2.90	0.56	0.60	1.02	0.88	0.02	0.32	1.43	bdl	bdl	0.989	25.1	45.8	5.93
	S	2109	3215	1.67	0.19	0.09	463.1	44.3	6.08	10.6	4.85	1.55	2.19	3.01	2.91	bdl	bdl	0.874			
T	4722	3577	5.02	1.73	0.67	146.8	15.1	1.93	3.38	2.21	1.15	0.72	0.93	2.25	bdl	bdl	0.961				
7/ Slash	R	1	2	5	10	14	3	4	9	6	8	11	13	12	7						
	F	6209	3724	3.82	1.52	1.87	22.59	1.49	0.09	nd	nd	0.68	nd	nd	0.43	nd	bdl	0.994	15.6	23.6	1.48
	S	2977	3170	0.21	0.10	4.95	523.4	38.3	5.01	nd	nd	1.86	nd	nd	4.37	nd	bdl	0.858			
T	5439	3637	2.93	1.31	1.84	100.5	7.70	0.78	nd	nd	0.86	nd	nd	1.17	nd	bdl	0.973				
8/ Sagebrush	R	1	2	5	7	6	3	4	10	8	9	11	9	11	8						
	F	6827	3654	9.44	2.15	2.60	82.54	4.62	0.28	0.73	1.48	1.66	bdl	bdl	1.46	bdl	bdl	0.978	18.1	70.0	2.32
	S	1320	3267	7.79	0.17	bdl	450.8	18.2	1.74	5.62	2.50	1.26	bdl	bdl	2.47	bdl	bdl	0.879			
T	5737	3585	9.25	1.66	1.85	149.6	6.67	0.47	1.62	1.61	1.49	bdl	bdl	1.55	bdl	bdl	0.960				
9/ Ground	R	1	2	4	7	6	3	5	12	8	9	11	9	11	10						
	F	4720	3229	4.07	3.12	4.08	403.8	39.9	6.48	8.67	7.29	3.39	12.3	10.6	9.28	bdl	bdl	0.889	na <sup>d</sup>	na	nd
	R	1	2	12	14	11	3	4	10	8	9	13	5	6	7						
10/ Ground	F	5514	3476	5.61	3.12	2.60	212.4	23.4	3.58	7.29	4.09	2.12	4.57	2.51	5.96	bdl	bdl	0.942	na	na	nd
	S	1	2	7	11	12	3	4	10	5	9	14	8	13	6						
	T	6404	3279	5.14	1.43	2.16	324.5	56.0	6.64	6.53	11.3	4.96	11.5	9.93	9.18	2.38	1.42	0.910	na	na	nd
11/ Crown	R	1	2	11	15	14	3	4	9	10	6	12	5	7	8						
	F	6151	3671	10.6	2.00	3.11	69.06	3.33	0.28	0.71	1.09	1.19	bdl	bdl	1.64	bdl	bdl	0.982	10.9	20.0	nd
	S	860.0	3219	4.85	0.31	bdl	513.4	9.40	0.63	4.40	0.59	2.56	bdl	bdl	0.46	bdl	bdl	0.862			
T	5416	3622	9.81	1.76	2.65	117.2	4.38	0.30	1.13	1.09	1.27	bdl	bdl	1.39	bdl	bdl	0.969				
12/ Sagebrush	R	1	2	4	7	6	3	5	12	10	11	9	11	9	8						
	F	6151	3671	10.6	2.00	3.11	69.06	3.33	0.28	0.71	1.09	1.19	bdl	bdl	1.64	bdl	bdl	0.982	10.9	20.0	nd
	S	860.0	3219	4.85	0.31	bdl	513.4	9.40	0.63	4.40	0.59	2.56	bdl	bdl	0.46	bdl	bdl	0.862			
T	5416	3622	9.81	1.76	2.65	117.2	4.38	0.30	1.13	1.09	1.27	bdl	bdl	1.39	bdl	bdl	0.969				

Each gas is listed with the process that dominates in its formation.

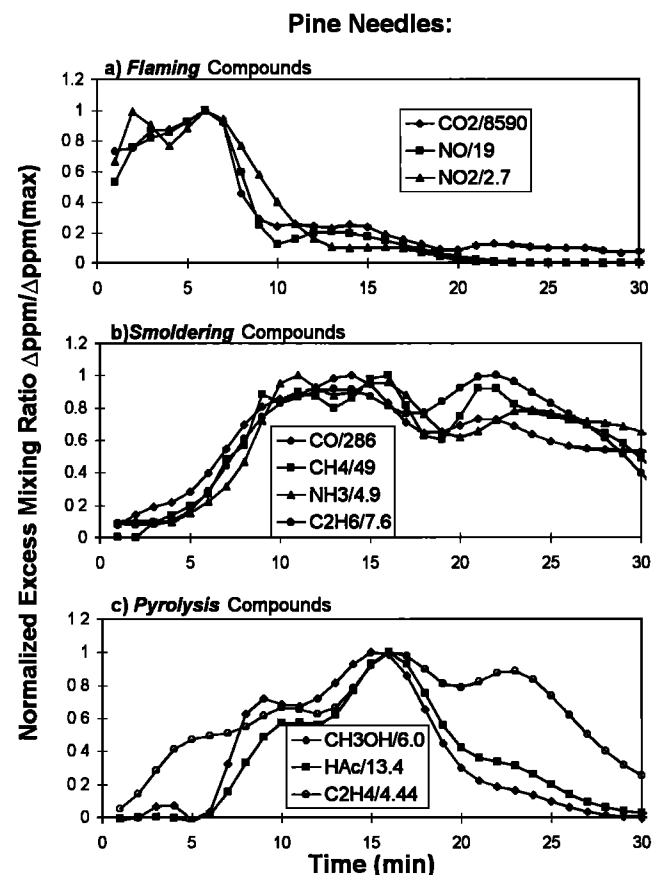
<sup>a</sup>F, flaming; S, smoldering; T, total (fire integrated); R, rank (order of production).<sup>b</sup>bdl, below detection limit.<sup>c</sup>nd, no data.<sup>d</sup>na, not applicable.<sup>e</sup>HAc, acetic acid; MeOH, methanol; HFo, formic acid.

loss data were forced to agree, flow data scaled by 0.76 were also used. For fires 9-12 the flows implied by the measured fuel mass loss were calculated, assuming 45%C and 6%H, and were used in place of actual flow measurements.

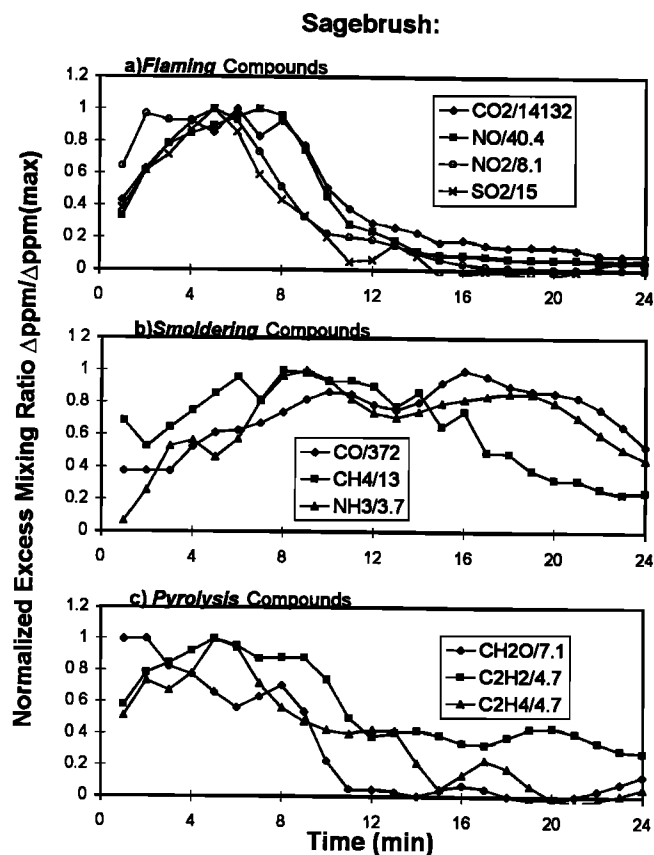
We estimate that the relative weighting of compounds due to the flow profile used in determining fire-averaged emission factors is accurate to 10% ( $1\sigma$ ). We estimate the probable error due to assuming the %C as  $< 10\%$  and that due to unmeasured carbon species as  $< 2\%$ . In summary the data are presented in compact form as emission factors in Table 3 with an estimated accuracy of 16% ( $1\sigma$ ).

## Results and Discussion

Time series of concentrations of 14 species could be determined simultaneously for most of each fire. These species were carbon dioxide, carbon monoxide, methane, ethane, ethene, ethyne, formaldehyde, methanol, acetic acid, volatile higher hydrocarbons (terpenes), water, nitric oxide, nitrogen dioxide, ammonia, and sulfur dioxide. Three others, formic acid, hydrogen cyanide, and carbonyl sulfide, were measurable only during periods of peak emissions for some fires. Emission factors and modified combustion efficiency for each fire are summarized in Table 3, which includes these quantities for the whole fire as well as by fire process as described in the ensuing discussion.



**Figure 4.** Examples of time evolution of compounds emitted from a fire in a fuel bed of pine needles (fire 5), separated by (a) flaming, (b) smoldering, and (c) pyrolysis/distillation combustion process.



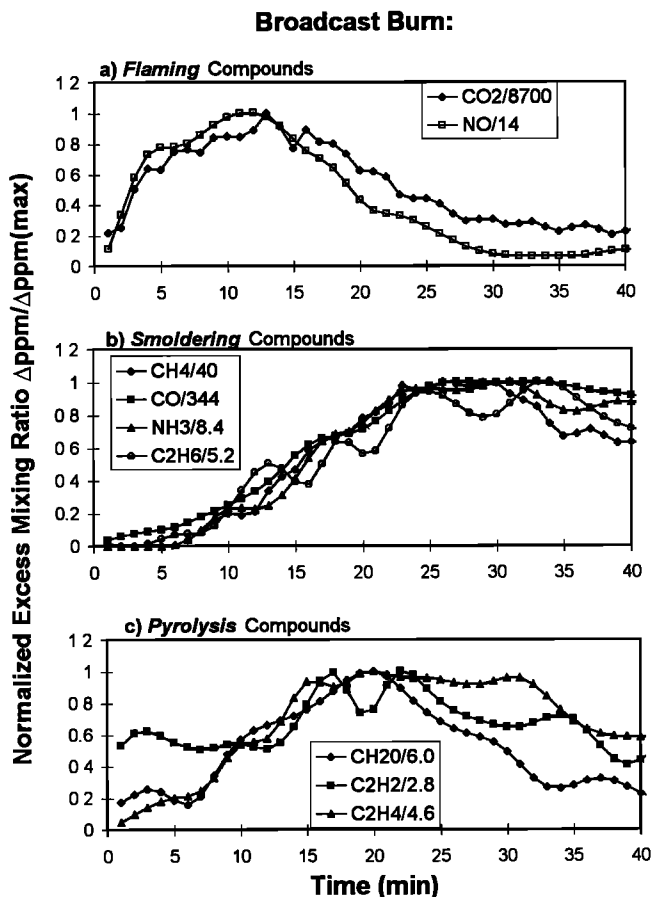
**Figure 5.** As for Figure 4 except for whole sagebrush fuel (fire 12).

### Temporal Behavior of Fire Emissions

Earlier laboratory studies of *Loberet et al.* [1991] were carried out in homogeneous, well-characterized fuels. That work demonstrated that some compounds can be attributed to flaming or smoldering combustion based on a linear correlation with  $\text{CO}_2$  or  $\text{CO}$ , similarity of the normalized temporal profile with  $\text{CO}_2$  or  $\text{CO}$ , and degree of oxidation. Our results confirm some of these observations. The normalized temporal profiles for selected flaming and smoldering compounds can be seen in Figures 4-6 (part a and b) for fires burning in dry brown pine needles (fire 5), sagebrush (fire 12), and a homogeneous mixture of forest residues (fire 6).

We also measure significant amounts of compounds that do not correlate linearly with either  $\text{CO}_2$  or  $\text{CO}$  and show markedly different normalized temporal profiles. The temporal profiles for some of these compounds can be seen in Figures 4-6 (part c). These compounds are principally unburnt pyrolysis products originating from heating of the primary fuel [Shafizadeh *et al.*, 1976; Overend *et al.*, 1985; Evans *et al.*, 1986; DeGroot *et al.*, 1988; Cofer *et al.*, 1989]. Pyrolysis products that we measure are acetic and formic acid, methanol, formaldehyde, and light unsaturated hydrocarbons. In studies limited to the emissions from smoldering combustion, the entrainment of unoxidized pyrolysis compounds in the smoke naturally falls within the definition of smoldering combustion [McKenzie *et al.*, 1995]. However, in this work these compounds also occur in the emissions during times dominated by flaming combustion. (See Figures 4 - 6.) Therefore because production of these compounds exhibits poor tempo-





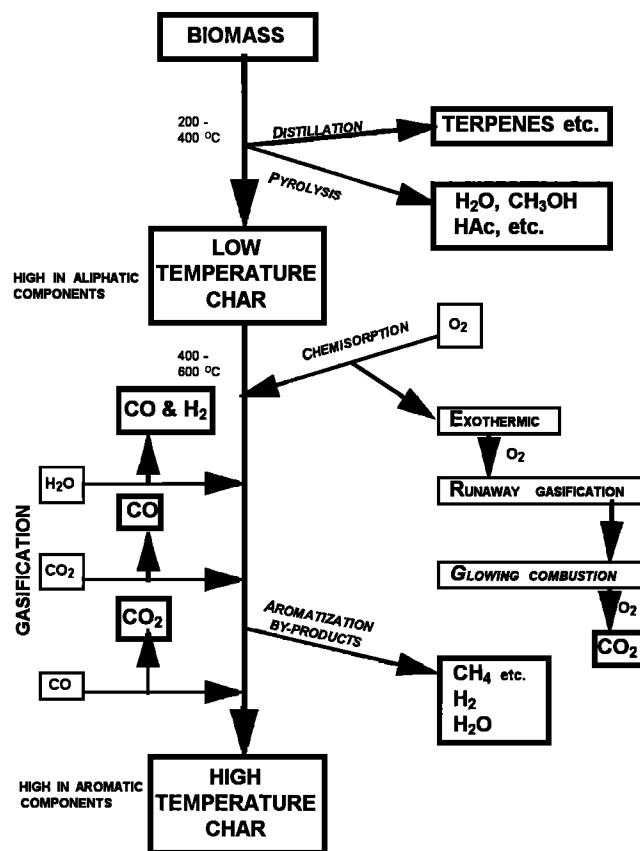
**Figure 6.** As for Figure 4 except for a simulated broadcast burn (fire 6).

ral correlation with both CO and CO<sub>2</sub> and because they may primarily be formed by thermal "cracking" of biomass without the reaction of an atmospheric oxidant with the fuel, we adopt an operational definition of smoldering combustion that excludes these compounds and invoke one further category of compounds: the "distillation and pyrolysis" category. We recognize that the construct of a category or class of compounds is a simplification and that there may be some overlap. For example, most of the CO<sub>2</sub> is produced by flaming combustion, but CO<sub>2</sub> is also the major product of smoldering combustion. Smoldering compounds correlate well with CO, which can be produced by direct, thermal decarbonylation of biomass, by gasification of char, or by incomplete oxidation of other emissions in flames. Formation of methane is a high-temperature pyrolysis process, and formaldehyde can be formed pyrolytically or from the partial oxidation of methanol or methane. Examples of fire processes which generate emissions but do not involve flames are diagrammed in Figure 7 [Lephardt and Fenner, 1980; Overend et al., 1985; Jakab et al., 1993]. These processes create the emissions in our smoldering and pyrolysis/distillation categories and also create the fuel that drives the turbulent diffusion flames that produce the bulk of the emissions.

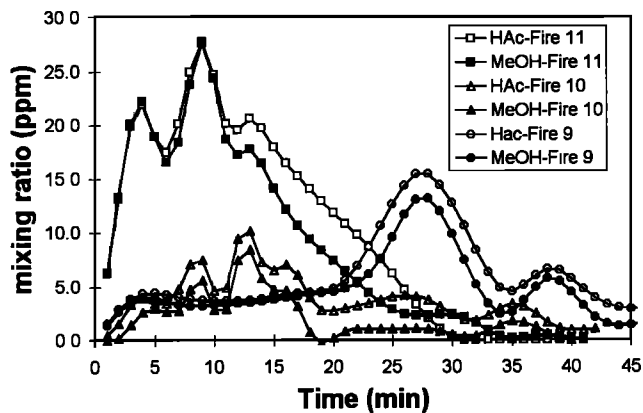
The pyrolysis compounds do not always track with each other or with any single tracer species because they often originate from different precursors or in different thermal or moisture regimes and because heat production and combustion efficiency vary throughout a fire. On the other hand,

correlations among pyrolysis compounds may identify common precursors or thermal regimes. An example is shown in Figure 8 where two pyrolysis compounds, methanol and acetic acid, are highly temporally correlated in nearly a 1:1 molar ratio for three different fires. The 1:1 production is in contrast to the 1:2 production observed for brown pine needles (Figure 4c). Consideration of the temporal profiles and production ratios suggests that methanol and acetic acid may be produced from biomass in similar thermal regimes (relatively low temperature, as shown in Figure 7) but from different precursors.

**Interpretative model.** From the perspective of being able to monitor total fire emissions for many species continuously, we find that the concept of fire stages or phases separated in time is less useful than the more general concept of fire processes, which may coexist in time. These processes are summarized in the following paragraphs. Figure 9 presents plots of modified combustion efficiency versus time for fires 3 (pine needles) and 6 (broadcast simulation) which is useful in interpreting the different processes.



**Figure 7.** Some of the important nonflaming processes in biomass combustion are summarized pictorially. Initially, heating of biomass releases distillation products such as terpenes and oxygenated pyrolysis products such as water and acetic acid. This contributes to the formation of low temperature char. Continued heating at increased temperatures releases hydrocarbons forming high temperature char. The high temperature char participates in gasification and glowing combustion producing the indicated emissions. The emissions shown here can form a flammable mixture. The rate of heat transfer from the flames and surface oxidation to the solid fuel controls the rate of production of the gaseous fuel for the flames.



**Figure 8.** Temporal profiles for the concentration of acetic acid and methanol in parts per million from a selection of fires.

For a homogeneous or well-mixed fuel bed a typical fire behaves as follows:

1. Following ignition at one end of the fuel bed, the flames and an associated pyrolysis/distillation zone begin to expand across and down through the fuel bed. After a few minutes the entire bed gives rise to 1- to 3-m flames for several minutes and the emissions are dominated by the products of flaming combustion with a comparably minor contribution from unmodified pyrolysis products. During this time the fire burns with high (typically 99%) combustion efficiency. This behavior corresponds to the first 10 min in the simulated broadcast burn (Figure 9a) and the first 5 min of the pine needle fire (Figure 9b).

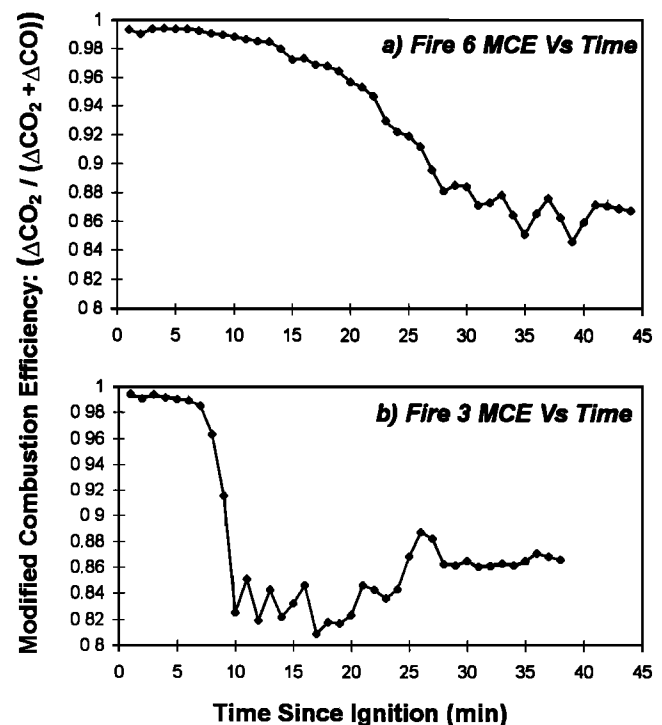
2. At the ignited end, the flaming zone starts to shift toward intermittent pockets of smaller flames mixed with "smoldering" combustion. Chemisorption of  $O_2$  on char is exothermic and drives glowing combustion which provides heat to pyrolyze and "distill" adjacent fuel which, in turn, contributes to more char formation.  $CO_2$ ,  $CO$ , and hydrocarbons are released from the char. With less flaming, a larger fraction of distilled and pyrolytically formed compounds can be entrained in the smoke unoxidized. As the shift toward smoldering and pyrolysis propagates across the fuel bed the combustion efficiency drops with time. This behavior is illustrated in the midsection of Figure 9a. Especially during this transition period of the fire, the emissions are the products of all three processes.

3. After the flames have ceased over the entire fuel bed the products are dominated by smoldering but still with an important contribution to emissions from pyrolysis. During this time the combustion efficiency is observed to range from 80 to 88% until the fire ceases to burn. This second sustained level of combustion efficiency is seen at the end of both fires in Figure 9.

Emissions from flaming and smoldering peak with the maxima in flaming and smoldering combustion, but peaks in the production of pyrolysis products are more variable. The high heat release rate associated with flaming combustion may pyrolyze more fuel and there is often a peak in the measured pyrolysis products either before, during, or shortly after the peak in flaming products. However, the majority of the initial pyrolysis products would normally be oxidized in the presence of vigorous flaming. During smoldering combustion

the pyrolysis products may be made at a lower absolute rate, but they have a higher probability of escaping the flames to be detected in the smoke. Therefore in all fires the quantity of pyrolysis products detected per unit fuel consumption is always higher during times dominated by smoldering combustion. For a specific, homogeneous fuel the flaming and smoldering processes tend to produce smoke that is approximately of fixed relative composition, so that the ratio of highly oxidized compounds to  $CO_2$  is more or less constant from flaming combustion, and the ratio of certain incompletely oxidized compounds to  $CO$  is roughly constant for smoldering combustion for a specific fire type. (See Figures 4 - 6 (part a and b).) This is the basis for the observation of "tracking," in which the normalized concentration profiles for flaming or smoldering compounds show a high degree of correlation with the other compounds in the same class [Lobert *et al.*, 1991]. In fires that exhibit tracking it is meaningful to report the ratio of the concentrations, obtained from a spot measurement and for two compounds from the same class, as an approximate emission ratio for the fire as a whole. This is useful because it allows reliance on data which are not fire-integrated to derive emission ratios. Thus in such fires the emission ratio for two compounds that are either both from flaming or both from smoldering can be measured at nearly any time. However, even for a homogeneous fuel bed, where tracking occurs for flaming and smoldering compounds, the pyrolysis products do not all track a single tracer species well. This implies that an integrated sample or (preferably) real-time, continuous sampling of the emissions and the smoke velocity is necessary to obtain good emission factors for these compounds.

When spotty or layered (inhomogeneous) fuel beds are burned, tracking is not observed even for flaming or smolder-



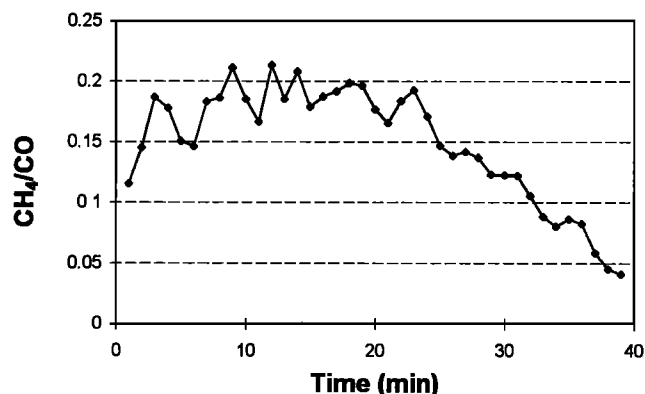
**Figure 9.** Modified combustion efficiency versus time for (a) fire 6 (broadcast simulation) and (b) fire 3 (pine needles), illustrating two different trajectories important in land management fires.

ing compounds. As different fuels dominate fuel consumption during the course of the fire, the tracking may go away. An example of this type of temporal behavior is shown in Figure 10 which shows the ratio of  $\text{CH}_4/\text{CO}$  during fire 11. During this fire the ratio changes by a factor of 5 from an initial value of 0.2, which is characteristic of pine needles which burn early in the fire, to a value of 0.04 which is characteristic of woody material. In practice, virtually all real fires run in such complex fuel beds, the one possible exception being pure grassland fires. A general approach to quantifying fire emissions is thus preferred, in which time-resolved concentrations and flow are measured and integrated to obtain total emissions.

**Relative fuel consumption by various combustion processes.** Because the three major fire processes produce different products, it is of use to be able to estimate the fuel consumption by process. Flaming and smoldering would normally account for most emissions by mass, but pyrolysis is important from an emissions standpoint because the sum of its products is similar to total methane emission. Essentially 90-99% of the fuel carbon is converted to either  $\text{CO}_2$  or CO from flaming and smoldering. Therefore for the purposes of estimating fuel consumption by process, we make the arithmetic approximation that all the fuel consumption is due to flaming or smoldering combustion. During the initial stages of a fire, emissions are dominated by flaming combustion and we may measure the emissions of nearly pure flaming combustion. For many fires it is also true that near the end of the fire the emissions are dominated by smoldering combustion and we can measure the products of this process. For each fire that featured time periods dominated by pure flaming or smoldering combustion we have computed the emissions per unit amount of fuel for those pure processes. By also quantifying the average emissions per unit amount of fuel for the whole fire, we can then determine the relative importance of each process in consuming fuel in an accurate manner following *Ward and Radke* [1993]. For smoldering

$$\%S = \frac{[\text{EF}(\text{flame}) - \text{EF}(\text{total})] * 100}{[\text{EF}(\text{flame}) - \text{EF}(\text{smolder})]} \quad (4)$$

We can calculate the percentage fuel consumption by smoldering combustion (%S) for each species individually. For  $\text{CO}_2$  and CO, which are measured with excellent S/N



**Figure 10.** Data from fire 11, illustrating smoldering compounds appearing in a nonconstant ratio over the course of a burn in a heterogeneous fuel bed.

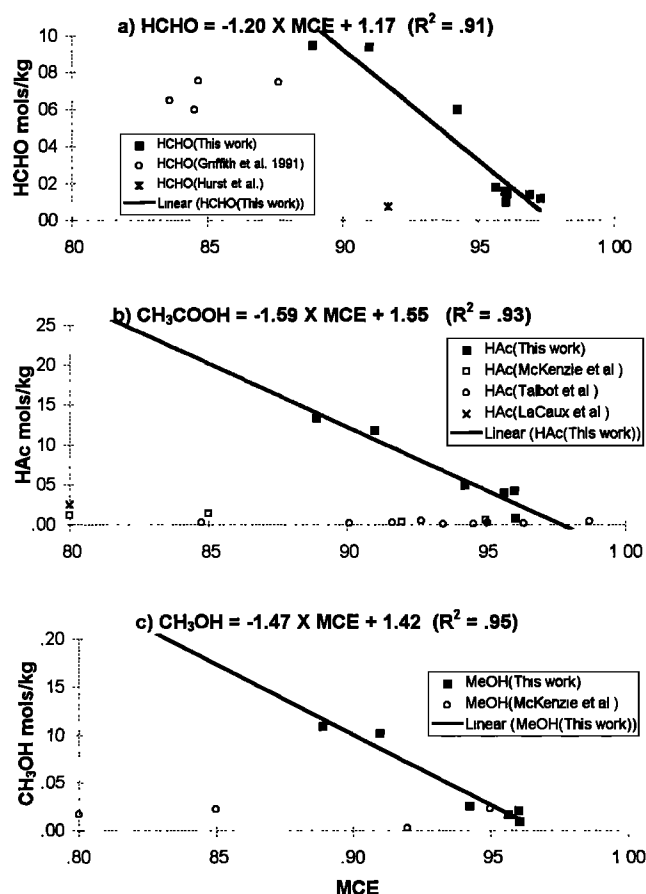
throughout the entire fire, the agreement is usually within 1%. For other flaming or smoldering emissions there is also normally good agreement. However, if the emitted species is a distillation or pyrolysis product, for example, methanol, formaldehyde, acetic or formic acid, good agreement is not normally found using such an analysis based on only flaming and smoldering.

Emission factors and combustion efficiencies for examples of nearly pure flaming and smoldering processes, and the percent fuel consumption by smoldering combustion determined as above, are included in Table 3 for all applicable fires. For the compounds listed as in the pyrolysis/distillation category the total emission factors are more accurate than the process emission factors.

We can contrast our process approach to that of *Lobert et al.* [1991] which distinguishes flaming and smoldering phases in time. In *Lobert's* work, CO is considered a tracer for smoldering combustion and the time of maximum rate of increase of CO emission is taken as the beginning of the smoldering stage. The results from the two approaches are compared for each fire as entries in Table 3. We find that the calculated fuel consumption for a "smoldering phase" is larger than the calculated fuel consumption by a smoldering process. The agreement between the two approaches is best when the fire makes a rapid transition between periods dominated by the two types of combustion, as in fire 3 (see Figure 9b). The difference between these approaches is more significant to understanding the combustion chemistry than it is in emission estimates. In emission estimates the fuel consumption by a smoldering "phase" may be overestimated, but in these cases, the emission factor for a smoldering "phase" will be underestimated and the resulting emission estimate should be nearly the same.

### Production of Oxygenated Organic Compounds

The oxygenated organic compounds measured in this work are formaldehyde, methanol, and acetic acid, with appreciable amounts of formic acid in one fire. Our data are included in Table 3 and plotted as emission factors versus modified combustion efficiency in Figure 11. To date, relatively little information has been available on the direct fire emissions of these difficult to measure compounds, but it is possible to make a limited comparison between our measurements and results obtained earlier. *Cooper* [1980] reports molar emission factors in the range  $1 - 5 \times 10^{-4}$  moles total aldehyde production per mole C burnt from residential firewood combustion with formaldehyde accounting for most of this. In our six most comparable fires (3,5,6,7,8,12), in which most of the fuel consumption was due to flaming combustion, we report a median molar emission factor of  $4.0 \times 10^{-4}$  for formaldehyde. *Hurst et al.* [1994a] sampled Australian savanna fires from aircraft followed by laboratory matrix isolation-FTIR analysis and report average molar emission factors of  $(2.0 \pm 1.2) \times 10^{-4}$  for formaldehyde and  $(5.5 \pm 3.4) \times 10^{-4}$  for acetaldehyde. The field study of *Griffith et al.* [1991] reports much higher levels of formaldehyde with an emission ratio  $\Delta\text{CH}_2\text{O}/\Delta\text{CO}_2$  of  $2.2 \times 10^{-3}$ , corresponding to an emission factor of  $\sim 1.9 \times 10^{-3}$ . The field study probed mainly smoldering combustion. The present laboratory study featured two ground fire simulations dominated by smoldering combustion (fires 9 and 10) and for these fires our average molar emission factor for formaldehyde was comparable at  $2.0 \times 10^{-3}$ . In summary, there is broad



**Figure 11.** Fire-integrated emission factors as a function of fire-integrated modified combustion efficiency for (a) formaldehyde, (b) acetic acid, and (c) methanol. The regression equations are fit to the results of this study. The results of *Hurst et al.*, *Talbot et al.*, and *Lacaux et al.* are from different (hardwood) fuel types.

agreement, but detailed comparisons are limited by the lack of data on fuel composition and combustion efficiencies from other studies. There are significantly higher quantities of  $\text{CH}_2\text{O}$  emitted from smoldering fires.

For the other oxygenated organics, methanol, acetic acid, and formic acid, few comparisons with other work are possible. *McKenzie et al.* [1995] measured methanol and acetic acid from laboratory fires with coniferous fuels by cryotrapping and gas chromatography/mass spectral (GC/MS) analysis, while three other studies used the mist chamber technique [*Cofer et al.*, 1985] for organic acids: *Talbot et al.* [1988] from brush and hardwood fuels in laboratory studies, *Dinh et al.* [1991] from African savannah fires, and *Lacaux et al.* [1994] from African charcoal-making kilns. In summary our data consistently show good internal consistency with strong correlations of emission factors with combustion efficiency (Figures 11b and 11c) while all other measurements show much lower emission factors and little or no correlation with combustion efficiency. Where sufficient auxiliary data are provided from other studies to estimate combustion efficiencies, these other data are also included in Figure 11. However, the comparison must be treated with caution because in the estimates of (fire averaged) combustion efficiency from other studies there were sometimes insufficient data to

weight the flaming and smoldering processes correctly. Correction for this may increase the combustion efficiencies from some other work by  $\sim 4\%$ .

It is notable that in our sagebrush fires, acetic acid was below the detection limit, which is more consistent with other studies. We measure formic acid in only one fire (the crown fire simulation) at levels 2 orders of magnitude higher than those measured by *Talbot et al.* [1988]. In all studies, acetic acid is emitted at 3-10 times the rate of formic acid. Qualitatively, the oxygenated organic compounds shown in Figure 11 are each emitted at levels about 20 to 25% that of methane and taking into account unmeasured higher homologues, the sum of oxygenated organic emissions may be of the same order as methane emissions.

The discrepancies between studies may be due to the different fuels burned, to the different sampling methods, and to different data analysis methods as discussed above. Direct intercomparisons are required to elucidate these differences. In particular, the present FTIR method is nonintrusive with no risk of losses during sampling. Clearly, our results imply potential for much higher emissions of oxygenated organic species than all previous work. The emissions of these compounds and their effects on regional atmospheric chemistry will be important and should be better understood.

The production of oxygenated organic compounds in fires is of potential atmospheric significance for several reasons: (1) Many of these compounds are reactive. (2) Organic acids contribute significantly to rain and cloud water acidity in remote regions [*Keene and Galloway*, 1984a, b]. (3) Oxygenated organics such as  $\text{CH}_2\text{O}$  may serve as precursors for organic acids such as formic acid and for oxidants such as  $\text{HO}_2$  and OH radicals. The atmospheric chemistry of oxygenated organics has been summarized elsewhere [*Finlayson-Pitts and Pitts*, 1986]. We note that oxidation of methanol can be a formaldehyde source, that oxidation dominates photolysis as a formaldehyde sink in "moderately polluted conditions," and that oxidation of formaldehyde can produce formic acid. Thus we speculate, as have *Andreae et al.* [1988], that some emitted oxygenated organics may contribute to a secondary gas phase formic acid source. In addition to this, a further secondary source of formic acid could be the oxidation of the emitted alkenes [*Arnts and Gay*, 1979; *Finlayson-Pitts and Pitts*, 1986]. Alkenes detected in this work are ethene and possibly monoterpenes [*Yokelson et al.*, 1995]. *Helas et al.* [1992] suggested that volatilized biogenic compounds from biomass burning may be a source of formic acid.

#### Production of Reactive Nitrogen-Containing Compounds

The dominant measured nitrogen-containing species emitted are  $\text{NO}$  and  $\text{NO}_2$  from flaming and  $\text{NH}_3$  from smoldering combustion (see Figures 4-6). If the N:C ratio of the fuel is known, a nitrogen mass balance can be calculated. This was measured only for some subsamples of brown pine needles, with a value of 0.6% as described earlier. For fires 3 and 5 in pine needles, the emission factors for  $\text{NO}$ ,  $\text{NO}_2$ , and  $\text{NH}_3$  average 0.081, 0.0089, and 0.029 mole  $\text{kg}^{-1}$  accounting for 38%, 4%, and 13% of the fuel nitrogen, respectively, a total of 55%. Emitted  $\text{N}_2\text{O}$  and  $\text{CH}_3\text{CN}$  were below detection limits, and other nitrogenous compounds such as HCN were observed only in the crown fire simulation. Accepting the value of *Kuhlbusch et al.* [1991] of  $36 \pm 13\%$  for  $\text{N}_2$  emission and a value of 10% for ash nitrogen [*Hurst et al.*, 1994b; *Crutzen*

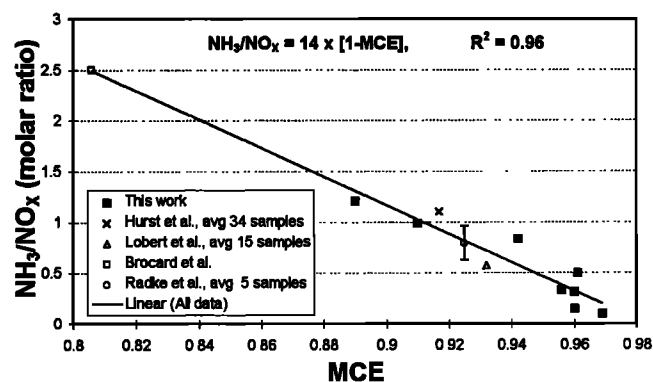
and Andreae, 1990], these emission factors account for all the fuel nitrogen within the experimental uncertainties. These findings are in general agreement with Hurst *et al.* [1994a, b] who report high levels of for NO, NO<sub>2</sub>, and NH<sub>3</sub> and that N<sub>2</sub>O, HCN, and CH<sub>3</sub>CN each account for less than 1% of the fuel nitrogen.

Our data confirm the earlier observation of Griffith *et al.* [1991] that NO<sub>x</sub> dominates the measurable nitrogen release during flaming combustion and that NH<sub>3</sub> is the dominant measured N product in smoldering combustion. Early estimates of NH<sub>3</sub> production from biomass burning project NH<sub>3</sub> production be about one third of NO<sub>x</sub> production [Crutzen and Andreae, 1990]. The laboratory studies of Lobert *et al.* [1991] yielded an average value for NH<sub>3</sub>/NO<sub>x</sub> of 0.57. Figure 12 shows the fire-integrated NH<sub>3</sub>/NO<sub>x</sub> ratio from several studies as a function of modified combustion efficiency. At combustion efficiencies below about 0.91 the molar ratio of NH<sub>3</sub>/NO<sub>x</sub> exceeds unity. The field measurements of Griffith *et al.* [1991], which were biased to smoldering combustion, yield a high average NH<sub>3</sub>/NO<sub>x</sub> ratio of 3.7. The data of Hurst *et al.* [1994a, b], from aircraft sampling of Australian savanna fires, give a NH<sub>3</sub>/NO<sub>x</sub> value near 1.1. Taken together, these results suggest that biomass burning may be a more significant source of atmospheric ammonia than has been generally recognized.

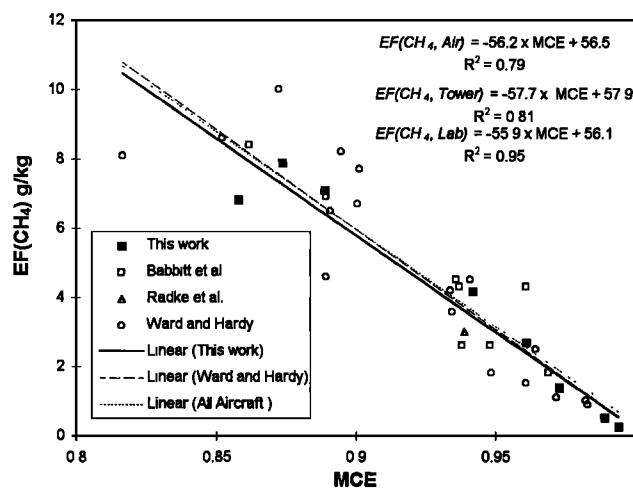
Over 50% of the fuel nitrogen is emitted as NO<sub>x</sub> or NH<sub>3</sub>. The atmospheric chemistry of ammonia is poorly understood, but it is important as the only common water-soluble base in the atmosphere and could potentially neutralize organic and inorganic acids in the plume in the liquid or gas phase. There are indications that a significant fraction of the emitted ammonia may be converted to ammonium ion [Andreae *et al.*, 1988a], but only a small fraction of the formic and acetic acid present in plumes appears to be converted to formate or acetate [Talbot *et al.*, 1988; Andreae *et al.*, 1988b]. NO and NO<sub>2</sub> are catalysts for regional ozone production and precursors for nitric acid production.

#### Comparison of Laboratory and Field Data

Comparison with FTIR field data from our earlier study [Griffith *et al.*, 1991] is illustrated for formaldehyde above.



**Figure 12.** Fire-integrated NH<sub>3</sub>/NO<sub>x</sub> molar ratios as a function of modified combustion efficiency for all fires in this work compared with other studies. Radke *et al.* [1990] report a mass of NO<sub>x</sub>, which is represented as a 50:50 mixture of NO and NO<sub>2</sub> and the error bar shows the range of possible values due to changing this ratio.



**Figure 13.** Laboratory results from this work coplotted with comparable field measurements of methane emission factors versus modified combustion efficiency. The comparison is limited to similar pine-dominated coniferous fuels. For the purposes of this figure, the emission factors from this work were calculated assuming 50% C (instead of 45%) as was done in the other three studies.

However, detailed comparison is difficult because of differences and uncertainties in fuel burned and in the relative amounts of different combustion products (i.e., flaming, smoldering, and pyrolysis) sampled. Tower-based sampling which is integrated over the duration of a fire in the field and accompanied by vertical velocity measurements, or aircraft sampling which effectively integrates combustion products from all fire processes in a mixed plume, should provide better comparisons. Figure 13 compares CH<sub>4</sub> emission factors versus MCE from this study of simulated field fires in mixed coniferous fuels (fires 6, 7, 9, and 10) with canister data sampled from aircraft [Radke *et al.*, 1991; Babbitt *et al.*, 1995] and towers [Ward and Hardy, 1991] in all cases for mixed coniferous fuels. The agreement is excellent within the limitations imposed by the different sampling and analysis methods.

#### Emission of Sulfur Compounds

We consistently observe SO<sub>2</sub> emitted from flaming combustion with a mean SO<sub>2</sub>/CO<sub>2</sub> ratio of  $(7.3 \pm 3.0) \times 10^{-4}$  (1 $\sigma$ ). Comparison with other measurements is made difficult by the wide possible ranges of fuel sulfur contents (S:C ratios from 0.023 to 0.9%) [e.g., Cook, 1993; Bowen, 1979] and the fraction of fuel sulfur volatilized (35-85%) [Ward *et al.*, 1982; Cook, 1993; Delmas, 1982]. These ranges suggest total sulfur/CO<sub>2</sub> emission ratios from  $8 \times 10^{-5}$  to  $8 \times 10^{-3}$ , and published measurements all fall in this range [e.g., Hurst *et al.*, 1994; Crutzen and Andreae, 1990; Andreae *et al.*, 1988; Delmas, 1982]. We observed OCS only at low levels (<1 ppm) in one fire, consistent with other findings that OCS accounts for only a very small fraction of fuel sulfur [Crutzen *et al.*, 1979, 1985; Crutzen and Andreae, 1990; Ward *et al.*, 1982]. There are probably other significant sulfur-containing emissions that were undetected. Consideration of sulfur phytochemistry [Richmond, 1973] suggests that hydrogen sulfide, methyl mercaptan, and dimethyl sulfide are likely to be in this class, but they are very weak absorbers of IR radiation.

## Conclusions

This work establishes the open-path FTIR technique as a valuable diagnostic tool for continuous, real-time analyses of many gases in smoke, providing an improved understanding of smoke composition and chemistry, fire behavior, carbon and nitrogen cycles, and biomass burning impacts on atmospheric chemistry. The observations in this study with the most relevance to projecting impacts on atmospheric chemistry are summarized as follows:

1. The concept of dividing a large fire into two stages separated in time is insufficient to categorize the temporal behavior of the emissions. There are at least three "processes" that should be considered, namely flaming, smoldering, and pyrolysis/distillation. One consequence of this is that a representative sample cannot always be taken at any arbitrary time during a fire. To measure, for example, oxygenated organics or any compound from heterogeneous fuels requires continuous sampling along with flow measurements or isokinetic integrated sampling to weight the relative contributions of the different combustion processes correctly. Only for simple, homogeneous fuels do many compounds "track" one another throughout a fire and allow representative single samples to be collected.

2. Although a lot is known about the combustion chemistry of light alkanes, the gaseous fuel that supplies flaming combustion of biomass is likely to contain large amounts of volatile plant constituents and oxygenated organics. The combustion chemistry of these materials is less well understood and will influence the emissions. The simplest example of this is that the smoke from biomass fires may contain levels of unburnt oxygenated organics and volatilized biogenic compounds that are high enough to have a significant impact on local and regional atmospheric chemistry. The emission levels and their impacts deserve more attention than they have received to date.

3. There is increasing evidence that the fate of nearly all the fuel nitrogen may be accounted for by NO, NO<sub>2</sub>, NH<sub>3</sub>, N<sub>2</sub>, and ash and that of these quantities the amount of NH<sub>3</sub> is likely to be more significant than previously assumed, especially for fires with low combustion efficiency.

4. Determination of integrated emissions from real fires in the field by application of emission factors determined from laboratory studies depends on determining the relative importance of the flaming, smoldering, pyrolysis, and distillation combustion processes (or at least the combustion efficiency) in the real fire.

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