1	Potable water reuse through advanced membrane technology
2	Chuyang Y. Tang ^{a,*} Zhe Yang ^a , Hao Guo ^a , Jason Wen ^b , Long D. Nghiem ^c , Emile
3	Cornelissen ^{d,e,f,*}
4	^a Haking Wong Building, Department of Civil Engineering, the University of Hong Kong, Pokfulam Road,
5	Hong Kong, China
6	^b Department of Water Resources, City of Lakewood, California, USA
7	^c Centre of Technology in Water and Wastewater, University of Technology Sydney, Sydney NSW 2007
8	^d KWR Watercycle Research Institute, 3433 PE Nieuwegein, Netherlands
9	^e Singapore Membrane Technology Centre, Nanyang Environment and Water Research Institute, Nanyang
10	Technological University, Singapore 637141, Singapore
11	^f Particle and Interfacial Technology Group, Ghent University, Coupure Links 653, B-9000 Ghent, Belgium
12	
13	* Corresponding Author. Tel: +852 2859 1976, Fax: +852 2559 5337, E-mail address: tangc@hku.hk
14	(CYT); Emile.Cornelissen@kwrwater.nl (EC)
15	

Abstract

Recycling water from municipal wastewater offers a reliable and sustainable solution to cities and regions facing shortage in conventional water supply. Places including California and Singapore have developed advanced water reuse programs as an integral part of their water management strategy. Membrane technology, particularly reverse osmosis, has been playing a key role in producing high quality recycled water. This feature paper highlights the historical development, current status and future perspectives of advanced membrane processes to meet both indirect and direct potable reuse. Recent advances in membrane materials and process configurations are presented and opportunities and challenges are identified in the context of water reuse.

INTRODUCTION

Potable water reuse has become an important indispensable component of the water infrastructure in many cities and regions around the world to address water scarcity. As a notable example, water supply of Southern California traditionally relied heavily (about two-thirds) on imported water, whose availability has shrunk significantly over the last four decades due to more upstream demand, stringent environmental regulations and multi-year droughts. Severe overdraft of groundwater since 1940s caused declining groundwater levels and seawater intrusion that contaminated freshwater aquifers. In the 1970s, Orange County Water District in Southern California started its Water Factory 21 (WF21), which employed advanced treatment processes to produce high quality recycled water for direct injection to the drinking water aquifers. Since 2008, a new Groundwater Replenishment System (GWRS) has replaced WF21 to produce 70 MGD of highly purified water using reverse osmosis (RO) technology. This world's largest advanced wastewater reclamation system for potable reuse has expanded its production to 100 MGD in 2015, with an ultimate capacity of 130 MGD to be completed by 2023.

Membrane technology, particularly RO, has played a key role in producing highly purified recycled water for potable reuse. Compared to alternative technologies such as activated carbon adsorption and soil aquifer treatment, RO provides better assurance for safe potable applications thanks to its ability to simultaneously remove a broader range of contaminants including total dissolved solids, pathogenic agents, and organic micropollutants [ref.]. Advancement in membrane technology in recent years has increased the number of water reuse projects worldwide (Figure 1). In California alone,

several additional major projects have been implemented or planned, including the 40-MGD Edward C. Little Water Recycling Facility, a potential 150-MGD Regional Recycled Water Program in Metropolitan Water District of Southern California,⁵ and a scheduled Groundwater Reliability Improvement Project (GRIP) ⁶ to produce recycled water in 2018. Water reuse has gone far beyond any single region or country, stretching from the United States, Singapore in the Far East, South and Western Europe to Australia in the southern hemisphere. In Singapore, the five NEWater plants provide a total of 170 MGD, or 40% of the nation's water supply. This number is scheduled to be increased to 55% by 2060. Other notable examples include: the 20 MGD Beenyup plant commissioned in Perth, Western Australia in 2016, which is the first RO plant in Australia for indirect potable reuse; ... In Belgium (Europe) the Intermunicipal Water Company of Veurne-Ambacht (IWVA) treats secondary wastewater effluent at the Torreele facility for indirect potable reuse via groundwater recharge in the dune water catchment of St. André. 8 This 2 MGD has been in operation since 2002 and has brackish water reverse osmosis at its core for high quality water production. In Australia, after a successful full scale trial over 5 years, in 2016, the Beenyup Advanced Water Recycling plant was officially opened in Perth as the first indirect potable reuse scheme in the country. In conjunction with aquifer storage and recovery, the Beenyup plant can produce 20 MGD of recycled water, which is enough to supply up to 100,000 households in Perth.

50

51

52

53

54

55

56

57

58

59

60

61

62

63

64

65

66

67

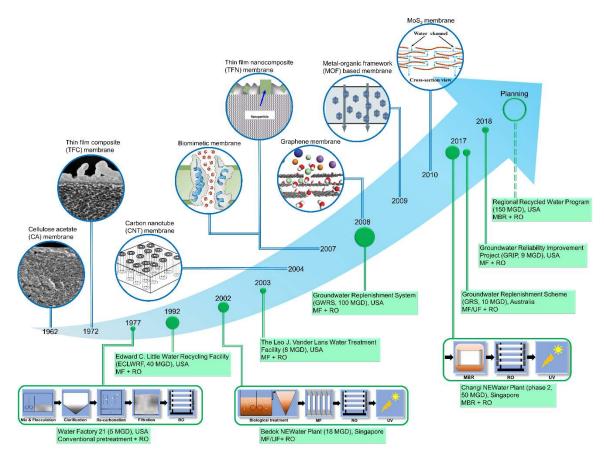


Figure 1. Historical developments of membrane-based wastewater reuse. The lower part of the figure shows notable examples of wastewater reuse plants together with their treatment schemes. The size of the sphere represents the relative size of a plant. The upper part of the figure presents the development of new desalting membranes. The respective years of first appearance of aquaporin, graphene, MOF and MoS₂ membranes are based on Refs ⁹⁻¹². The images of the membranes in the upper part of the figure are reprinted with copyright permissions: CA and TFC membranes from Ref. ¹³, CNT membrane from Ref. ¹⁴, biomimetic membrane from Ref. ¹⁵, TFN membrane from Ref. ¹⁶, graphene membrane from Ref. ¹⁷, MOF membrane from Ref. ¹⁸ and MoS₂ membrane from Ref. ¹⁹.

With water scarcity becoming an increasingly serious threat globally,²⁰ the thirst for water reuse is growing. This feature paper examines the evolution of membrane-based water reuse technology and highlights future opportunities and challenges in this field.

EVOLUTION OF MEMBRANE-BASED WATER REUSE

Reverse osmosis (RO) is a well-established technology that can be used in combination

with other complementary processes (for pretreatment to remove particulate matter and posttreatment to ensure the destruction of any remaining micropollutants ²¹⁻²⁴ and remineralization in the case of potable reuse) to produce high quality recycled water (Figure 1 and Figure 2). WF21 in Southern California introduced the first RO plant in the world in 1977 to purify reclaimed water to meet drinking water standards.² This 5 MGD RO plant was used to reduce the total dissolved solids of secondary effluent after pretreatment by conventional lime clarification, recarbonation, and multimedia filtration (Figure 2a). In modern potable reuse plants, conventional pretreatment is often replaced by a single microfiltration (MF) process (Figure 2b), which is more compact and efficient for the removal of particulates. In addition, downstream low pressure-high intensity ultraviolet light with hydrogen peroxide (UV/H₂O₂) is typically used to ensure adequate destruction of small molecular weight micropollutants such as N-nitrosodimethylamine (NDMA), N-nitrosodiethylamine (NDEA), and 1,4=Dioxane that cannot be completely removed by RO membranes.²⁵ This advanced MF-RO-UV/H₂O₂ treatment scheme has been widely adopted in many potable reuse plants, such as the grand-scale GWRS in Southern California³, the Bedok and Kranji NEWater plants in Singapore⁷, the Beenyup plant in Australia (ref?), and the Toreele Reuse plant in Belgium (ref?). A further significant improvement is the direct treatment of membrane bioreactor (MBR) effluent by RO (Figure 2c). In this new treatment scheme, the MBR achieves simultaneous roles of bioreactor, biomass separation, and RO pretreatment.^{26, 27} The elimination of further RO pretreatment using the particulate-free MBR effluent translates into additional savings of space, energy, and cost, which prompts Changi NEWater Plant in Singapore to adopt the MBR-RO-UV/H₂O₂ scheme.⁷

86

87

88

89

90

91

92

93

94

95

96

97

98

99

100

101

102

103

104

105

106

107

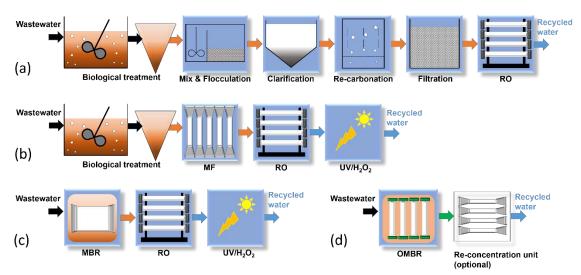


Figure 2. Evolution of membrane-based water reuse: (a) conventional pre-treatment of secondary effluent followed by RO; (b) MF pre-treatment of secondary effluent followed by RO, where an additional UV/H_2O_2 post-treatment may be used for the further removal of organic micropollutants; (c) MBR-RO treatment, where an additional UV/H_2O_2 post-treatment may be used for the further removal of organic micropollutants; and (d) OMBR with an optional draw solution re-concentration unit. Some OMBR applications (e.g., using fertilizer-based draw solution) do not require the re-concentration unit.

Alternative membrane processes such as forward osmosis (FO) ²⁸⁻³¹ have also been explored for water reuse. FO-based processes, in which water transports through a dense semi-permeable membrane using a high osmotic pressure draw solution, are interesting due to their better ability to deal with difficult-to-treat waste streams (e.g., with high organic loading).³² One key challenge for FO is the energy-intensive re-concentration of draw solution for clean water production.³¹ To overcome this issue, Shon and co-workers developed a fertilizer-drawn FO process, in which the FO permeate water can be reused for fertigation. Other applications that do not require draw solution re-concentration, such as osmotic dilution of seawater or brine with wastewater ^{34, 35}, are also gaining more attention. Nevertheless, economic benefits of water reuse through osmotic dilution are yet to be proven.²⁹

An osmotic membrane bioreactor (OMBR) patented in 2005 ³⁶ is an innovative MBR technique for the reclamation of wastewater, which combines activated sludge treatment and forward osmosis in a single unit process (Figure 2d).^{37, 38} Compared to the MBR-RO scheme, OMBR can be potentially more compact and less energy intensive for niche applications where draw solutions do not need to be re-concentrated (e.g., by using fertilizer draw solutions). Other potential for osmotic membrane bioreactors include the high rejection of micropollutants ³⁹ and the simultaneous recovery of water, mineral, and nutrient ^{40,41}. Recent extension to anaerobic OMBRs further allow the recovery of energy in the form of biomethane.⁴² Nevertheless, challenges of membrane fouling ⁴³, salinity accumulation in the bioreactor ⁴⁴, and membrane stability ⁴⁵ need to be further addressed to enable its full scale applications.

TOWARDS BETTER PERFORMANCE MEMBRANES

Membranes play a critical role in RO-based water reuse. The quest for high-permeability and high-selectivity RO membranes is summarized in Figure 1. The first-generation RO membranes are of cellulose acetate with an asymmetrical structure. With the development of more permeable and more selective thin film composite (TFC) polyamide membranes in the 1970s, existing commercial RO membranes are largely dominated by the latter. At typical TFC RO membrane consists of a polyamide rejection layer of several tens to hundreds of nanometers in thickness, which is formed by an interfacial polymerization reaction of an amine monomer (typically m-phenylenediamine or MPD) and an acyl chloride monomer (typically trimesoyl chloride) on an ultrafiltration support substrate. Commercial TFC polyamide membranes have a wide range of pH tolerance (pH 2-11),

excellent mechanical stability (up to several MPa of applied pressure), high salt rejection (e.g., NaCl rejection of up to 99.7%) and yet a moderate water permeability (e.g., 1-8 L/(m²h¹bar¹)).^{47, 48} Unlike seawater desalination whose energy consumption (~ 4 kWh/m³) is mainly dictated by the high osmotic pressure of seawater (~ 2.7 MPa), the energy consumption in RO-based water reuse (~ 1 kWh/m³ with approximately 0.555 kWh/m³ for RO³) is governed mostly by membrane resistance and fouling. Tripling membrane water permeability can potentially reduce the energy consumption for potable reuse by half.⁴⁹ Thus, developing low-pressure RO membranes with high permeability and good antifouling performance deserves to be a top research priority.

Nanocomposite membranes. A new type of RO membranes, known as thin film nanocomposite (TFN) membranes, were developed by Hoek and coworkers in 2007.¹⁶ In this novel approach, zeolite nanoparticles of defined pore size are included into the polyamide rejection layer during an interfacial polymerization (Figure 3a). The inclusion of porous zeolite nanoparticles enhances the resulting membrane permeability while maintaining its salt rejection. The ease of fabricating TFN membranes at relatively cheap cost allows its commercial scale up.⁵⁰ In the meantime, many other materials, such as nanoparticles of silver, silica, or zinc oxide, have been extensively studied for the synthesis of TFN membranes ^{51,52}, although the majority of the studies were performed at bench scale.

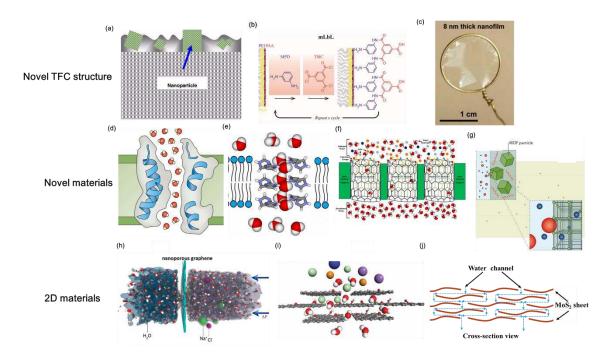


Figure 3. Novel RO membranes. Polyamide membranes include (a) a thin-film nanocomposite membrane with nanomaterials embedded into polyamide rejection layer, ¹⁶ (b) a molecular layer-by-layer (mLBL) membrane fabricated by repeated cycles of interfacial polymerization of MPD with TMC, ⁵³ and (c) a sub-10-nm-thick polyamide rejection layer fabricated by performing interfacial polymerization reaction on a sacrificial nanostrand interlayer. ⁵⁴ Examples of emerging materials for high performance membranes include: (d) aquaporins, ¹⁵ (e) artificial water channel, ⁵⁵ (f) carbon nanotubes, ⁵⁶ (g) metal-organic frameworks, ¹⁸ (h) nanoporous graphene monolayers, ⁵⁷ (i) graphene oxide frameworks, ¹⁷ and molybdenum disulfide (MoS₂) frameworks. ¹⁹ All figures are reprinted with copyright permissions from the respective references.

Ultrathin membranes. Another effective way to increase the membrane permeability is by reducing the thickness of the polyamide rejection layer. Gu and co-workers introduced a molecular layer-by-layer (mLBL) membrane.⁵³ In their approach, an ultrathin polyamide rejection layer was prepared by alternative soaking of a substrate in low-concentration MPD and TMC solutions for repeated cycles (Figure 3b). A mLBL membrane of 20-25 nm in thickness was prepared, which show 75% improvement in water permeability and similar NaCl rejection compared to a control TFC membrane prepared by conventional interfacial polymerization with rejection layer thickness of 110 nm. Livingston and co-workers ⁵⁴ prepared an ultrathin polyamide membrane by

performing interfacial polymerization reaction on a sacrificial layer of nanostrands. The presence of nanostrand layer significantly reduced the diffusion of MPD monomers, which resulted in an ultra-thin and smooth polyamide rejection layer of less than 10 nm in thickness (Figure 3c). Though the resultant membrane had excellent water permeability of more than two orders of magnitude higher than a commercial benchmark and similar selectivity, this method is unfortunately difficult to scale up. By electrospraying MPD and TMC monomer solutions into microdroplets for subsequent interfacial polymerization, Tang and co-workers demonstrated finely controlled growth of a polyamide rejection film at 1 nm/min.⁵⁸ This electrospray-assisted additive interfacial polymerization approach, a method that can be more easily scaled up, was able to prepare uniform ultrathin polyamide membranes of four to a few tens of nm in thickness.

Next generation desalting materials and membranes. In recent years, novel materials have emerged as potential candidates for preparation of high performance RO membranes. ^{15, 59} One type of promising material is aquaporins (Figure 3d), or water channel proteins, that are found in cellular membranes for delivering water across biological cells with permeabilities of 2-3 orders of magnitude higher than the best commercially available RO membranes and with nearly complete rejection of solutes including H⁺. ⁶⁰⁻⁶² Synthetic channels and porous materials have also been investigated for their use in synthesizing ultra-permeable membranes; some of the most notable examples include self-assembled artificial water channels ⁵⁵, carbon nanotubes (CNTs) ^{10, 14, 56}, microporous metal-organic frameworks (MOFs) ^{50, 63, 64}, and graphene ⁵⁷, graphene oxide ⁶⁵⁻⁶⁷, and MoS₂ ^{68, 69} (Figure 3e-j). Their intrinsic ultra-fast water transport rates can

potentially half the energy consumption for water reuse. We exertheless, a recent review highlights the challenges of defects prevention (for achieving high rejection) and scaling up (for commercial scale production). Indeed, most of the reported membranes prepared by these novel desalting materials have NaCl rejections of only \sim or < 90%, which are significantly below commercial benchmarks. A compromise approach is to incorporate these materials in a thin film nanocomposite structure, which can effectively maintain salt rejection at the expense of water permeability.

Antifouling membranes. Developing membranes that are resistant to fouling, particularly biofouling, is a priority research area in the context of membrane-based water reuse. Various strategies have been developed to enhance antifouling performance of membranes, which often involves surface coating, grafting, and immobilization of anti-adhesion and/or biocidal agents.⁷⁰ These approaches are generally designed to modify a membrane's hydrophilicity, surface charge, and/or roughness, or to impart antimicrobial moieties. Some notable examples of anti-fouling enhancement include polyvinyl alcohol grafting ⁷¹, polydopamine coating ⁷², zwitterionic grafting ⁷³ and silver/copper nanoparticles immobilization ⁷⁴⁻⁷⁶.

DEALING WITH ORGANIC MICROPOLLUTANTS

The presence of micropollutants in wastewater is a significant issue for membrane-based water reuse. NDMA is a notorious disinfectant byproduct and a human carcinogen that is frequently detected in RO permeate.^{25, 77} California has set a Public Health Goal of 3 ng/L and a notification level of 10 ng/L for this suspected carcinogen.⁷⁸ NDMA rejection by

RO membranes is in the range from 20 to 80%.^{77, 79, 80} Post-treatment by advanced oxidation processes, such as UV treatment, is effective in destructing NDMA. Nevertheless, it generally requires a very high UV intensity (e.g., 1000 mJ/cm²), a dosage of an order of magnitude higher than that used for UV disinfection.⁷⁷ Besides NDMA, other micropollutants of concern include endocrine disruptors and pharmaceutically active compounds.⁸¹⁻⁸³. Recent issues in the Netherlands with discharge of perfluorpolymers and pyrazole in surface water bodies challenged Dutch drinking water facilities. While perflourpolymer rejection by RO membranes is very high (>95%)⁸⁴, the pyrazole rejection is low (approximately 35%)⁸⁵ depending on the type of RO membrane resulting in the need of a post UV/peroxide treatment.

Due to their historical roots in desalination, commercial thin film composite polyamide RO membranes have been highly optimized for salt rejection and water permeability, yet they are often not adequate for the removal of micropollutants, particularly small polar organic compounds. In recent years, researchers have started to realize the need for designing membranes specifically for micropollutants removal. Tailoring membrane surface properties by surface coating/grafting show some promising results. Re-89 For instance, a hydrophilic polydopamine coating can effectively half the passage of hydrophobic EDCs through a polyamide membrane. To reduce the adverse effect on water permeability, materials of high selectivity to micropollutants are needed. In this regard, some of the novel desalting materials such as aquaporins and MOFs are of great interest due to their highly defined pore structure and high specificity for water. Recent studies on aquaporin-embedded polyamide membranes showed improved rejection rates

to a wide range of micropollutants.^{91, 92} Graphene oxide sheets that are capable of forming highly hydrophilic water channels have also demonstrated great potential for micropollutants removal.⁹³⁻⁹⁵

BRIDGING THE GAP

The challenge of implementing water reuse is not confined solely to the technical domain. Public acceptance is a complex and thorny issue, one that has derailed a number of water reuse projects in the past. 96, 97 A particular high profile case is that of Toowoomba in Australia, where intense debate about a proposed indirect potable reuse scheme led to a referendum. 98 As the result of the referendum, in which 60% of the participants opposed the scheme, it was abandoned. Toowoomba has been seen as the trigger point for the Queensland government in Australia to abandon the Western Corridor Recycled Water project, which was completed in 2009 but has never been used as intended. The fallout from Toowoomba underscores the need to fully understand the connection between public perception about water reuse and technological innovation.

Public acceptance. Since Toowoomba, significant efforts often by collaborations between social scientists and engineers, and practitioners in the water sector have been made to positively influence public perception about water reuse. These efforts have resulted in better awareness by the public about the reliability and efficiency of membrane separation and other technologies used for water reclamation, and hence, a gradual shift in public acceptance and a growing number of successful water reuse schemes in recent years. For examples, the City of San Diego reported an increase in

public support of potable water reuse from 26% in 2004 to 73% in 2012 after sustained investment in research and public engagement activities.⁹⁶

The legitimacy of potable reuse. Recent socio-psychological studies have also added considerable depth to our understanding of the complex interactions amongst factors that can influence public acceptance of water reuse. Through an experiment with 1000 Australian correspondents, Dolnicar et al. 100 conclusively observed that providing information about the treatment processes significantly increased public acceptance of water reuse. Proactively working with the media is also an important component of public engagement activities. Ormerod and Silvia analysed 158 newspaper articles about potable water reuse in the Orange County Water District from 2000 to 2016 and did not identify any negative coverage. While some of these articles were positive, the majority was neutral and uncommitted about potable water reuse. These results echo previous findings from Hurlimann and Dolnicar 101 who observe concluded that the media coverage of potable water reuse can often be characterized by lack of inclusion of views, a low level of support statements with scientific evidence, a low level of impartiality, and a high level of hedging language. The implicit uncertainty about the reported information in newspaper coverage highlights the need for better engagement between key stakeholders of potable water reuse and the.

304

305

306

307

308

286

287

288

289

290

291

292

293

294

295

296

297

298

299

300

301

302

303

Improving public knowledge alone may not be sufficient to change public perception. In the context of water reuse, there is a pre-cognitive and irrational perception that prevents many people from separating the final product (clean water) and its contaminated source (human excreta).⁹⁶ This is despite the fact that no traces of the original contamination

exists and that no incident on human health due to water reuse has ever been reported albeit the many intentionally and unintentionally (unplanned) potable water reuse schemes that have been in operation, in some cases, for several decades. One effective strategy to overcome the challenge of irrational public perception provide experiential activities such as field visits, tasting opportunities, using reused water for public swimming pools and water splash pads. As a notable example, strong public support to water reuse in Singapore can be attributed, at least in part, to a very concerted and systematic public engagement program that includes the attractive NEWater Visitor Centre at the Bedok plant. The centre has effectively become a tourist attraction, where the public can book a tour for free to learn about how Singapore copes with their water supply problem and be given a bottle of NEWater (reused water) as souvenir or for tasting. Effort to garner public support to potable reuse has evolved beyond simple marketing activities. Harris-Lovett et al., have recently proposed a framework based on societal legitimacy for engaging the public on issues of potable water reuse. On the same vein, Binz et al., point out that technological innovation is incongruous with established social rules. Thus, given the perceived unprecedented nature of potable water reuse, it is often confronted with strong skepticism and a lack of societal legitimacy. Harris-Lovett et al., argued that establishing legitimacy for potable water reuse involves embedding RO, advanced oxidation, and other new technologies in the shared social belief system, moral standards and cultural conventions through a set of strategies that go beyond traditional public relations and educational outreach.

309

310

311

312

313

314

315

316

317

318

319

320

321

322

323

324

325

326

327

328

329

330

331

Public trust and technical reliability. A key component of the legitimacy framework

proposed by Herris-Lovett et al., is reliable risk management procedures. A promising strategy is to make key innovation in potable water reuse namely membrane separation and other advanced technologies more understandable by relating to standards and procedures that have already gained legitimacy in other established sectors. Online monitoring is essential not only for establishing a safety record but also effective risk management. Indeed, while acknowledging the central role of technology innovation, Lee and Tan accredited Singapore's success in supplying NEWater for potable use to an extensive data acquisition program to demonstrate the safety record of potable water reuse. Prior to the NEWater, the Singapore Public Utility Board collected some 20,000 test results from different sampling locations in a demonstration plant, covering about 190 physical, chemical and microbiological parameters. The results were benchmarked again the WHO and USEPA drinking water standards to demonstrate the credibility of potable water reuse.

With a focus on public safety, real-time monitoring has been a crucial strategy for assurance and risk management of potable water reuse. Real-time monitoring offers an opportunity to engage with the public as well as quickly detect and rectify failure. Given the central role of RO in potable water reuse, several highly sensitive sensors have been developed to monitor chemical and microbial contaminants on a real-time or near real-time basis for membrane integrity assurance. In addition to traditional surrogate parameters such as conductivity, total organic carbon, and sulfate which can be readily monitored online, several new surrogates specific to potable water reuse have been added in recent years. They include UV254 or fluorescence for monitoring organic micropollutants and multi-able light scattering or measurement of adenosine triphosphate for monitoring microbial contaminants.

Of a particular note, Fujioka et al., have successfully developed an analytical technique consisting of high-performance liquid chromatography followed by photochemical reaction and chemiluminescence detection (HPLC PR-CL) for online monitoring of N-nitrosodimethylamine (NDMA) and several other N-nitrosamines in secondary treated effluent and RO permeate. The detection limit of their technique (0.3 – 2.7 ng/L) is comparable to the regulated concentrations of these organic micropollutants in most potable water reuse guidelines or standards. The HPLC PR-CL developed by Fujioka et al., marks a significant milestone as this is the first time target organic micropollutants can be monitored in near real-time. Further development in online monitoring of RO performance can be expected and will help to bridge the gap between technology innovation and public confidence in potable water reuse.

369 AUTHOR INFORMATION 370 **Corresponding Author** *Phone: (+852) 2859 1976; e-mail: tangc@hku.hk 371 372 Notes 373 The authors declare no completing financial interest. 374 375 ACKNOWLEDGMENTS 376 The study receives financial support from the General Research Fund of the Research 377 Grants Council (Project # 17207514) of Hong Kong. The partial funding support from Seed Fund for Strategic Interdisciplinary Research at the University of Hong Kong is also 378 379 appreciated. 380

- 382 1. Zektser, S.; Loáiciga, H. A.; Wolf, J. T., Environmental impacts of groundwater
- overdraft: selected case studies in the southwestern United States. *Environ. Geol.* **2005**,
- 384 47, (3), 396-404.
- 385 2. Orange County Water District (OCWD); Water Factory 21.
- 386 https://www.ocwd.com/media/2451/water-factory-21-brochure.pdf
- 387 3. Orange County Water District (OCWD); Groundwater Replenishment System
- 388 (GWRS). https://www.ocwd.com/gwrs/
- 389 4. West Basin Municipal Water District; Edward C. Little Water Recycling Facility.
- 390 http://www.westbasin.org/water-supplies-recycled-water/facilities
- 391 5. Metropolitan Water District of Southern California; Regional Recycled Water
- 392 Program. http://www.mwdh2o.com/DocSvcsPubs/rrwp/index.html#home
- 393 6. Water Replenishment District of Southern California (WRD); Groudwater Reliability
- 394 Improvement Project (GRIP)
- 395 http://www.wrd.org/content/groundwater-reliability-improvement-project-grip
- 396 7. Public Utilities Board (PUB). www.pub.gov.sg/
- 397 8. Van Houtte, E., Verbauwhede, J., Long-time membrane experience at Torreele's
- water re-use facility in Belgium. Desalination and Water Treatment 2013, 51, (22-24),
- 399 4253-4262.
- 400 9. Kumar, M.; Grzelakowski, M.; Zilles, J.; Clark, M.; Meier, W., Highly permeable
- 401 polymeric membranes based on the incorporation of the functional water channel protein
- 402 Aquaporin Z. Proc. Natl. Acad. Sci. 2007, 104, (52), 20719-20724.
- 403 10. Manawi, Y.; Kochkodan, V.; Hussein, M. A.; Khaleel, M. A.; Khraisheh, M.; Hilal,
- 404 N., Can carbon-based nanomaterials revolutionize membrane fabrication for water
- 405 treatment and desalination? *Desalination* **2016**, *391*, 69-88.
- 406 11. Qiu, S.; Xue, M.; Zhu, G., Metal-organic framework membranes: from synthesis to
- 407 separation application. *Chem. Soc. Rev.* **2014,** *43*, (16), 6116-6140.
- 408 12. Splendiani, A.; Sun, L.; Zhang, Y.; Li, T.; Kim, J.; Chim, C.-Y.; Galli, G.; Wang, F.,
- Emerging photoluminescence in monolayer MoS2. Nano lett. 2010, 10, (4), 1271-1275.
- 410 13. Gerstandt, K.; Peinemann, K.-V.; Skilhagen, S. E.; Thorsen, T.; Holt, T., Membrane
- 411 processes in energy supply for an osmotic power plant. Desalination 2008, 224, (1-3),
- 412 64-70.
- 413 14. Hinds, B. J.; Chopra, N.; Rantell, T.; Andrews, R.; Gavalas, V.; Bachas, L. G.,
- Aligned multiwalled carbon nanotube membranes. *Science* **2004**, *303*, (5654), 62-65.
- 415 15. Werber, J. R.; Osuji, C. O.; Elimelech, M., Materials for next-generation desalination
- and water purification membranes. *Nat. Rev. Mater.* **2016,** *1*, 16018.
- 417 16. Jeong, B.-H.; Hoek, E. M.; Yan, Y.; Subramani, A.; Huang, X.; Hurwitz, G.; Ghosh,
- 418 A. K.; Jawor, A., Interfacial polymerization of thin film nanocomposites: a new concept
- 419 for reverse osmosis membranes. *J. Membr. Sci.* **2007**, *294*, (1), 1-7.
- 420 17. You, Y.; Sahajwalla, V.; Yoshimura, M.; Joshi, R. K., Graphene and graphene oxide
- 421 for desalination. *Nanoscale* **2016**, 8, (1), 117-119.
- 422 18. Denny Jr, M. S.; Moreton, J. C.; Benz, L.; Cohen, S. M., Metal-organic frameworks
- for membrane-based separations. Nat. Rev. Mater. 2016, 1, 16078.
- 424 19. Sun, L.; Huang, H.; Peng, X., Laminar MoS 2 membranes for molecule separation.
- 425 Chem. Commun. **2013**, 49, (91), 10718-10720.

- 426 20. United Nations Department of Economic and Social Affaires
- 427 http://www.un.org/waterforlifedecade/scarcity.shtml
- 428 21. Drewes, J. E.; Reinhard, M.; Fox, P., Comparing microfiltration-reverse osmosis and
- soil-aquifer treatment for indirect potable reuse of water. Water Research 2003, 37, (15),
- 430 3612.
- 431 22. Côté, P.; Masini, M.; Mourato, D., Comparison of membrane options for water reuse
- 432 and reclamation. *Desalination* **2004**, *167*, (1-3), 1-11.
- 433 23. Wintgens, T.; Melin, T.; Schäfer, A.; Khan, S.; Muston, M.; Bixio, D.; Thoeye, C.,
- 434 The role of membrane processes in municipal wastewater reclamation and reuse.
- 435 Desalination **2005**, 178, (1-3 SPEC. ISS.), 1-11.
- 436 24. Bennett, A., Potable water: New technology enables use of alternative water sources.
- 437 Filtration + Separation **2011**, 48, (2), 24-27.
- 438 25. Fujioka, T.; Khan, S. J.; Poussade, Y.; Drewes, J. E.; Nghiem, L. D., N-nitrosamine
- removal by reverse osmosis for indirect potable water reuse A critical review based on
- observations from laboratory-, pilot- and full-scale studies. Separation and Purification
- 441 *Technology* **2012**, *98*, 503-515.
- 442 26. Lay, W. C. L.; Lim, C.; Lee, Y.; Kwok, B. H.; Tao, G.; Lee, K. S.; Chua, S. C.; Wah,
- 443 Y. L.; Ghani, Y. A.; Seah, H., From R&D to application: Membrane bioreactor
- 444 technology for water reclamation. Water Practice and Technology 2017, 12, (1), 12-24.
- 27. Qin, J.-J.; Kekre, K. A.; Tao, G.; Oo, M. H.; Wai, M. N.; Lee, T. C.; Viswanath, B.;
- 446 Seah, H., New option of MBR-RO process for production of NEWater from domestic
- sewage. *Journal of Membrane Science* **2006,** 272, (1), 70-77.
- 448 28. Cath, T. Y.; Childress, A. E.; Elimelech, M., Forward osmosis: Principles,
- applications, and recent developments. Journal of Membrane Science 2006, 281, (1-2),
- 450 70-87.
- 451 29. Shaffer, D. L.; Werber, J. R.; Jaramillo, H.; Lin, S.; Elimelech, M., Forward osmosis:
- 452 Where are we now? *Desalination* **2015,** *356*, 271-284.
- 453 30. Zhao, S.; Zou, L.; Tang, C. Y.; Mulcahy, D., Recent developments in forward
- osmosis: Opportunities and challenges. *Journal of Membrane Science* **2012**, *396*, 1-21.
- 455 31. Lutchmiah, K.; Verliefde, A. R. D.; Roest, K.; Rietveld, L. C.; Cornelissen, E. R.,
- Forward osmosis for application in wastewater treatment: A review. Water Research 2014,
- *457 58*, 179-197.
- 458 32. Li, X. M.; Chen, G.; Shon, H. K.; He, T., Treatment of high salinity waste water from
- shale gas exploitation by forward osmosis processes. In Forward Osmosis: Fundamentals
- 460 and Applications, 2015; pp 339-362.
- 461 33. Phuntsho, S.; Shon, H. K.; Hong, S.; Lee, S.; Vigneswaran, S., A novel low energy
- 462 fertilizer driven forward osmosis desalination for direct fertigation: Evaluating the
- performance of fertilizer draw solutions. *Journal of Membrane Science* **2011**, 375, (1-2),
- 464 172-181.
- 465 34. Boo, C.; Elimelech, M.; Hong, S., Fouling control in a forward osmosis process
- 466 integrating seawater desalination and wastewater reclamation. Journal of Membrane
- 467 Science **2013**, 444, 148-156.
- 468 35. Valladares Linares, R.; Li, Z.; Sarp, S.; Bucs, S.; Amy, G.; Vrouwenvelder, J. S.,
- 469 Forward osmosis niches in seawater desalination and wastewater reuse. Water Research
- 470 **2014,** *66*, 122-139.
- 471 36. Wessels, L. P.; Cornelissen, E. R. Operation and apparatus for treating waste water of

- a bioreactor in a membrane filtration unit (NL1028484). 8-3-2005, 2005.
- 473 37. Achilli, A.; Cath, T. Y.; Marchand, E. A.; Childress, A. E., The forward osmosis
- 474 membrane bioreactor: A low fouling alternative to MBR processes. *Desalination* 2009,
- 475 *238*, (1-3), 10-21.
- 476 38. Cornelissen, E. R.; Harmsen, D.; de Korte, K. F.; Ruiken, C. J.; Qin, J. J.; Oo, H.;
- 477 Wessels, L. P., Membrane fouling and process performance of forward osmosis
- 478 membranes on activated sludge. *Journal of Membrane Science* **2008**, *319*, (1-2), 158-168.
- 479 39. Alturki, A.; McDonald, J.; Khan, S. J.; Hai, F. I.; Price, W. E.; Nghiem, L. D.,
- 480 Performance of a novel osmotic membrane bioreactor (OMBR) system: Flux stability and
- removal of trace organics. *Bioresource Technology* **2012**, *113*, 201-206.
- 482 40. Wang, X.; Chang, V. W. C.; Tang, C. Y., Osmotic membrane bioreactor (OMBR)
- 483 technology for wastewater treatment and reclamation: Advances, challenges, and
- prospects for the future. *Journal of Membrane Science* **2016**, *504*, 113-132.
- 485 41. Holloway, R. W.; Achilli, A.; Cath, T. Y., The osmotic membrane bioreactor: A
- 486 critical review. Environmental Science: Water Research and Technology 2015, 1, (5),
- 487 581-605.
- 488 42. Chen, L.; Gu, Y.; Cao, C.; Zhang, J.; Ng, J.-W.; Tang, C., Performance of a
- 489 submerged anaerobic membrane bioreactor with forward osmosis membrane for
- low-strength wastewater treatment. Water Research 2014, 50, (0), 114-123.
- 491 43. Qin, J. J.; Kekre, K. A.; Oo, M. H.; Tao, G.; Lay, C. L.; Lew, C. H.; Cornelissen, E.
- 492 R.; Ruiken, C. J., Preliminary study of osmotic membrane bioreactor: Effects of draw
- solution on water flux and air scouring on fouling. Water Science and Technology 2010,
- 494 *62*, (6), 1353-1360.
- 495 44. Qiu, G.; Ting, Y. P., Osmotic membrane bioreactor for wastewater treatment and the
- 496 effect of salt accumulation on system performance and microbial community dynamics.
- 497 *Bioresource Technology* **2013,** *150*, 287-297.
- 498 45. Luo, W.; Xie, M.; Hai, F. I.; Price, W. E.; Nghiem, L. D., Biodegradation of cellulose
- 499 triacetate and polyamide forward osmosis membranes in an activated sludge bioreactor:
- 500 Observations and implications. *Journal of Membrane Science* **2016**, *510*, 284-292.
- 501 46. Petersen, R. J., Composite reverse-osmosis and nanofiltration membranes. *Journal of*
- 502 *Membrane Science* **1993**, *83*, (1), 81-150.
- 503 47. Li, D.; Wang, H., Recent developments in reverse osmosis desalination membranes.
- 504 J. Mater. Chem. **2010**, 20, (22), 4551-4566.
- 505 48. Tang, C. Y.; Kwon, Y.-N.; Leckie, J. O., Effect of membrane chemistry and coating
- 506 layer on physiochemical properties of thin film composite polyamide RO and NF
- membranes II. Membrane physiochemical properties and their dependence on polyamide
- and coating layers. *Desalination* **2009**, *242*, (1-3), 168-182.
- 509 49. Cohen-Tanugi, D.; McGovern, R. K.; Dave, S. H.; Lienhard, J. H.; Grossman, J. C.,
- Quantifying the potential of ultra-permeable membranes for water desalination. *Energy &*
- 511 Environmental Science **2014**, 7, (3), 1134-1141.
- 512 50. Pendergast, M. M.; Hoek, E. M., A review of water treatment membrane
- 513 nanotechnologies. *Energy Environ Sci.* **2011**, *4*, (6), 1946-1971.
- 514 51. Yin, J.; Deng, B., Polymer-matrix nanocomposite membranes for water treatment. J.
- 515 *Membr. Sci.* **2015**, *479*, 256-275.
- 516 52. Lau, W.; Gray, S.; Matsuura, T.; Emadzadeh, D.; Chen, J. P.; Ismail, A., A review on
- 517 polyamide thin film nanocomposite (TFN) membranes: History, applications, challenges

- and approaches. *Water Res.* **2015**, *80*, 306-324.
- 519 53. Gu, J. E.; Lee, S.; Stafford, C. M.; Lee, J. S.; Choi, W.; Kim, B. Y.; Baek, K. Y.; Chan,
- 520 E. P.; Chung, J. Y.; Bang, J.; Lee, J. H., Molecular layer-by-layer assembled thin-film
- 521 composite membranes for water desalination. Adv. Mater. 2013, 25, (34), 4778-82.
- 522 54. Karan, S.; Jiang, Z.; Livingston, A. G., Sub-10 nm polyamide nanofilms with
- 523 ultrafast solvent transport for molecular separation. Science 2015, 348, (6241),
- 524 1347-1351.
- 525 55. Barboiu, M.; Gilles, A., From natural to bioassisted and biomimetic artificial water
- 526 channel systems. Acc. Chem. Res. 2013, 46, (12), 2814-2823.
- 527 56. Das, R.; Ali, M. E.; Hamid, S. B. A.; Ramakrishna, S.; Chowdhury, Z. Z., Carbon
- 528 nanotube membranes for water purification: a bright future in water desalination.
- 529 Desalination **2014**, *336*, 97-109.
- 530 57. Cohen-Tanugi, D.; Grossman, J. C., Water desalination across nanoporous graphene.
- 531 *Nano Lett* **2012,** *12*, (7), 3602-8.
- 532 58. Ma, X.-H.; Yang, Z.; Yao, Z.-K.; Guo, H.; Xu, Z.-L.; Tang, C. Y., Interfacial
- 533 Polymerization with Electrosprayed Microdroplets: Toward Controllable and Ultrathin
- Polyamide Membranes. Environmental Science & Technology Letters 2018, DOI:
- 535 *10.1021/acs.estlett.7b00566*.
- 536 59. Yang, Z.; Ma, X.-H.; Tang, C. Y., Recent development of novel membranes for
- 537 desalination. *Desalination* **2018**.
- 538 60. Tang, C.; Wang, Z.; Petrinić, I.; Fane, A. G.; Hélix-Nielsen, C., Biomimetic
- aguaporin membranes coming of age. *Desalination* **2015**, *368*, 89-105.
- 540 61. Tang, C.; Zhao, Y.; Wang, R.; Hélix-Nielsen, C.; Fane, A., Desalination by
- 541 biomimetic aquaporin membranes: Review of status and prospects. Desalination 2013,
- *308*, 34-40.
- 543 62. Shen, Y.-x.; Saboe, P. O.; Sines, I. T.; Erbakan, M.; Kumar, M., Biomimetic
- 544 membranes: A review. *J. Membr. Sci* **2014,** *454*, 359-381.
- 545 63. Sorribas, S.; Gorgojo, P.; Téllez, C.; Coronas, J.; Livingston, A. G., High flux thin
- 546 film nanocomposite membranes based on metal-organic frameworks for organic solvent
- 547 nanofiltration. J. Am. Chem. Soc. **2013**, 135, (40), 15201-15208.
- 548 64. Liu, X.; Demir, N. K.; Wu, Z.; Li, K., Highly water-stable zirconium metal-organic
- framework UiO-66 membranes supported on alumina hollow fibers for desalination. J.
- 550 Am. Chem. Soc. **2015**, 137, (22), 6999-7002.
- 551 65. Hu, M.; Mi, B., Enabling graphene oxide nanosheets as water separation membranes.
- 552 Environ. Sci. Technol. **2013**, 47, (8), 3715-3723.
- 553 66. Nair, R.; Wu, H.; Jayaram, P.; Grigorieva, I.; Geim, A., Unimpeded permeation of
- water through helium-leak-tight graphene-based membranes. Science 2012, 335, (6067),
- 555 442-444.
- 556 67. Hegab, H. M.; Zou, L. D., Graphene oxide-assisted membranes: Fabrication and
- potential applications in desalination and water purification. J. Membr. Sci. 2015, 484,
- 558 95-106.
- 559 68. Xu, G.-R.; Xu, J.-M.; Su, H.-C.; Liu, X.-Y.; Zhao, H.-L.; Feng, H.-J.; Das, R.,
- 560 Two-dimensional (2D) nanoporous membranes with sub-nanopores in reverse osmosis
- desalination: Latest developments and future directions. *Desalination* **2017**.
- 562 69. Hirunpinyopas, W.; Prestat, E.; Worrall, S. D.; Haigh, S. J.; Dryfe, R. A.; Bissett, M.
- A., Desalination and Nanofiltration through Functionalized Laminar MoS2 Membranes.

- 564 *ACS Nano* **2017**.
- 70. Lee, K. P.; Arnot, T. C.; Mattia, D., A review of reverse osmosis membrane materials
- for desalination—development to date and future potential. J. Membr. Sci. 2011, 370, (1),
- 567 1-22.
- 568 71. Hu, Y.; Lu, K.; Yan, F.; Shi, Y.; Yu, P.; Yu, S.; Li, S.; Gao, C., Enhancing the
- 569 performance of aromatic polyamide reverse osmosis membrane by surface modification
- via covalent attachment of polyvinyl alcohol (PVA). J. Membr. Sci. 2015, 501, 209-219.
- 571 72. Kasemset, S.; Lee, A.; Miller, D. J.; Freeman, B. D.; Sharma, M. M., Effect of
- 572 polydopamine deposition conditions on fouling resistance, physical properties, and
- 573 permeation properties of reverse osmosis membranes in oil/water separation. J. Membr.
- 574 *Sci.* **2013**, *425-426*, 208-216.
- 575 73. Mi, Y.-F.; Zhao, Q.; Ji, Y.-L.; An, Q.-F.; Gao, C.-J., A novel route for surface
- 576 zwitterionic functionalization of polyamide nanofiltration membranes with improved
- 577 performance. J. Membr. Sci. **2015**, 490, 311-320.
- 578 74. Yin, J.; Yang, Y.; Hu, Z.; Deng, B., Attachment of silver nanoparticles (AgNPs) onto
- 579 thin-film composite (TFC) membranes through covalent bonding to reduce membrane
- 580 biofouling. J. Membr. Sci. 2013, 441, (Supplement C), 73-82.
- 75. Ben-Sasson, M.; Lu, X.; Bar-Zeev, E.; Zodrow, K. R.; Nejati, S.; Qi, G.; Giannelis, E.
- P.; Elimelech, M., In situ formation of silver nanoparticles on thin-film composite reverse
- osmosis membranes for biofouling mitigation. Water Res. 2014, 62, 260-70.
- 584 76. Zhang, A.; Zhang, Y.; Pan, G.; Xu, J.; Yan, H.; Liu, Y., In situ formation of copper
- 585 nanoparticles in carboxylated chitosan layer: Preparation and characterization of surface
- 586 modified TFC membrane with protein fouling resistance and long-lasting antibacterial
- 587 properties. Sep. Purif. Technol. 2017, 176, 164-172.
- 588 77. Mitch, W. A.; Sharp, J. O.; Trussell, R. R.; Valentine, R. L.; Alvarez-Cohen, L.;
- 589 Sedlak, D. L., N-Nitrosodimethylamine (NDMA) as a Drinking Water Contaminant: A
- Review. *Environmental Engineering Science* **2003**, *20*, (5), 389-404.
- 591 78. State Water Resources Control Board of California
- 592 https://www.waterboards.ca.gov/drinking_water/certlic/drinkingwater/NDMAhistory.sht
- 593 ml
- 594 79. Steinle-Darling, E.; Zedda, M.; Plumlee, M. H.; Ridgway, H. F.; Reinhard, M.,
- 595 Evaluating the impacts of membrane type, coating, fouling, chemical properties and
- 596 water chemistry on reverse osmosis rejection of seven nitrosoalklyamines, including
- 597 NDMA. Water Research **2007**, 41, (17), 3959.
- 598 80. Fujioka, T.; Khan, S. J.; McDonald, J. A.; Roux, A.; Poussade, Y.; Drewes, J. E.;
- Nghiem, L. D., N-nitrosamine rejection by nanofiltration and reverse osmosis membranes:
- The importance of membrane characteristics. *Desalination* **2013**, *316*, 67-75.
- 81. Levine, A. D.; Asano, T., Peer reviewed: recovering sustainable water from
- 602 wastewater. *Environ. Sci. Technol.* **2004,** *38,* (11), 201A-208A.
- 82. Schwarzenbach, R. P.; Escher, B. I.; Fenner, K.; Hofstetter, T. B.; Johnson, C. A.; Von
- 604 Gunten, U.; Wehrli, B., The challenge of micropollutants in aquatic systems. Science
- 605 **2006,** *313*, (5790), 1072-1077.
- 606 83. Luo, Y.; Guo, W.; Ngo, H. H.; Nghiem, L. D.; Hai, F. I.; Zhang, J.; Liang, S.; Wang,
- K. C., A review on the occurrence of micropollutants in the aquatic environment and their
- fate and removal during wastewater treatment. Sci. Total Environ. 2014, 473, 619-641.
- 84. Loi-Brügger, A., Panglisch, S., Hoffmann, G., Buchta, P., Gimbel, R., Nacke, C.-J.,

- Removal of trace organic substances from river bank filtrate Performance study of RO
- and NF membranes. Water Science and Technology: Water Supply, 2008, 8, (1), 85-92.
- 85. Bertelkamp, C.; Hijnen, W.; Siegers, W.; Hofman-Caris, R.; Leer, R. v. d.
- 613 Verwijdering van Pyrazool in drinkwaterzuiveringsprocessen, H2O; 2016.
- 86. Kim, J.-H.; Park, P.-K.; Lee, C.-H.; Kwon, H.-H., Surface modification of
- nanofiltration membranes to improve the removal of organic micro-pollutants (EDCs and
- PhACs) in drinking water treatment: graft polymerization and cross-linking followed by
- 617 functional group substitution. *J. Membr. Sci.* **2008,** *321*, (2), 190-198.
- 87. Ben-David, A.; Bernstein, R.; Oren, Y.; Belfer, S.; Dosoretz, C.; Freger, V., Facile
- 619 surface modification of nanofiltration membranes to target the removal of
- 620 endocrine-disrupting compounds. *J. Membr. Sci.* **2010,** 357, (1), 152-159.
- 88. Guo, H.; Deng, Y.; Tao, Z.; Yao, Z.; Wang, J.; Lin, C.; Zhang, T.; Zhu, B.; Tang, C. Y.,
- Does Hydrophilic Polydopamine Coating Enhance Membrane Rejection of Hydrophobic
- Endocrine-Disrupting Compounds? *Environmental Science & Technology Letters* **2016,** *3*,
- 624 (9), 332-338.
- 625 89. Guo, H.; Yao, Z.; Yang, Z.; Ma, X.; Wang, J.; Tang, C. Y., A one-step rapid assembly
- of thin film coating using green coordination complexes for enhanced removal of trace
- organic contaminants by membranes. Environmental Science & Technology 2017, 51,
- 628 (21), 12638-12643.
- 629 90. Park, H. B.; Kamcev, J.; Robeson, L. M.; Elimelech, M.; Freeman, B. D.,
- Maximizing the right stuff: The trade-off between membrane permeability and selectivity.
- 631 Science **2017**, 356, (6343), eaab0530.
- 91. Madsen, H. T.; Bajraktari, N.; Hélix-Nielsen, C.; Van der Bruggen, B.; Søgaard, E.
- 633 G., Use of biomimetic forward osmosis membrane for trace organics removal. *J. Membr.*
- 634 *Sci.* **2015,** *476*, 469-474.
- 92. Xie, M.; Luo, W.; Guo, H.; Nghiem, L. D.; Tang, C. Y.; Gray, S. R., Trace organic
- 636 contaminant rejection by aquaporin forward osmosis membrane: Transport mechanisms
- and membrane stability. *Water Res.* **2017**.
- 638 93. Zhang, Y.; Zhang, S.; Chung, T.-S., Nanometric graphene oxide framework
- 639 membranes with enhanced heavy metal removal via nanofiltration. Environ. Sci. Technol.
- **2015,** *49*, (16), 10235-10242.
- 641 94. Jiang, Y.; Wang, W.-N.; Liu, D.; Nie, Y.; Li, W.; Wu, J.; Zhang, F.; Biswas, P.; Fortner,
- J. D., Engineered crumpled graphene oxide nanocomposite membrane assemblies for
- advanced water treatment processes. *Environ. Sci. Technol.* **2015**, *49*, (11), 6846-6854.
- 95. Oh, Y.; Armstrong, D. L.; Finnerty, C.; Zheng, S.; Hu, M.; Torrents, A.; Mi, B.,
- Understanding the pH-responsive behavior of graphene oxide membrane in removing
- ions and organic micropollulants. J. Membr. Sci. 2017, 541, 235-243.
- 96. Smith, H. M.; Brouwer, S.; Jeffrey, P.; Frijns, J., Public responses to water reuse –
- Understanding the evidence. *Journal of Environmental Management* **2018**, 207, 43-50.
- 649 97. Kelly S. Fielding, S. D. a. T. S., Public acceptance of recycled water: state-of-the-art
- 650 review. International Journal of Water Resources Development in press.
- 98. Hurlimann, A.; Dolnicar, S., When public opposition defeats alternative water
- projects The case of Toowoomba Australia. Water Research 2010, 44, (1), 287-297.
- 653 99. Hartley, T. W., Public perception and participation in water reuse. *Desalination* **2006**,
- 654 187, (1-3), 115-126.
- 655 100. Dolnicar, S.; Hurlimann, A.; Nghiem, L. D., The effect of information on public

- 656 acceptance The case of water from alternative sources. Journal of Environmental
- 657 *Management* **2010**, *91*, (6), 1288-1293.

662

- 658 101. Hurlimann, A.; Dolnicar, S., Newspaper coverage of water issues in Australia.
- 659 Water Research **2012**, 46, (19), 6497-6507.
- 660 102. Dolnicar, S.; Hurlimann, A.; Grün, B., What affects public acceptance of
- recycled and desalinated water? Water Research 2011, 45, (2), 933-943.

■ TOC

