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## Reaction Mechanism and Kinetics for Ammonia Synthesis on the Fe(111) Surface

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#### **Abstract**

The Haber Bosch industrial process for synthesis of ammonia (NH<sub>3</sub>) from hydrogen (H<sub>2</sub>) and nitrogen (N<sub>2</sub>), produces the millions of tons of ammonia gas annually needed to produce nitrates for fertilizers required to feed the earth's growing populations. This process has been optimized extensively, but it still uses enormous amounts of energy (2% of the world's supply), making it essential to dramatically improve its efficiency. To provide guidelines to accelerate this improvement, we used quantum mechanics (QM) to predict reaction mechanisms and kinetics for NH<sub>3</sub> synthesis on Fe(111) – the best Fe single crystal surface for NH<sub>3</sub> synthesis. We predicted the free energies of all reaction barriers for all steps in the mechanism and built these results into a kinetic Monte Carlo model for predicting steady state catalytic rates to compare with single-crystal experiments at 673 °K and 20 atm. We find excellent agreement with a predicted turnover frequency (TOF) of 17.7 sec<sup>-1</sup> per 2x2 site (5.3 x  $10^{-9}$  moles/cm<sup>2</sup>/sec) compared to TOF= $10 \text{ sec}^{-1}$  per site from experiment.

Key words for indexing: Haber-Bosch; Density Functional Theory (DFT), PBE-D3 functional, reaction barriers, kinetic Monte Carlo.

#### 1. Introduction

The invention of the Haber-Bosch process for converting nitrogen gas (N<sub>2</sub>) and hydrogen gas (H<sub>2</sub>) into the ammonia (NH<sub>3</sub>) needed to generate the nitrates for the fertilizers underlying the agricultural revolution that feeds the world, is one of the greatest advances from scientific research. Millions of tons of NH<sub>3</sub> are produced each year<sup>1</sup> for agricultural and industrial purposes. Efficiency of up to 70%<sup>2</sup> has been achieved with commercially available iron based catalysts<sup>3</sup> and with ruthenium-based catalysts under lab settings<sup>4</sup>. Ruthenium-based catalysts are more active than iron-based ones<sup>5,6</sup>, and have been recently further developed.<sup>7,8</sup> However, ruthenium-based catalysts suffer from environmental problems due to ruthenium's scarce abundance in Earth's crust, high cost, together with its toxicity when in the form of compounds<sup>9</sup>, so that the industrial Haber-Bosch process is still based on iron catalysts. The industrial Haber-Bosch process requires drastic conditions of temperature (700°K-850°K) and pressure (50-200atm),

consuming 2% of the world's power, 3,5,10-12 which has motivated repeated attempts to improve the efficiency of Fe catalyst. 5

In order to provide a basis for making more rapid progress in such improvements, we want to use QM to determine the reaction mechanism and rates to help guide the search for improvements. In order to validate the QM predictions, we need to compare to experiments on well characterized surfaces. Fortunately, Somorjai et al<sup>13</sup> reported comprehensive investigations of the rates for NH<sub>3</sub> synthesis on Fe single crystals to which we can compare directly. Somorjai et al considered a pressure of 20 atm and temperatures in the range of 638 to 723°K, to determine the rates of ammonia formation. For 673°K they found relative rates of 418: 25: 1 for Fe(111), Fe(100), and Fe(110) surfaces, respectively. In another study<sup>14</sup>, they concluded that C7 sites (Fe atoms with seven nearest neighbors) are the most active in iron ammonia synthesis catalysts. Such sites involve the top three layers of Fe(111) exposed to the reactant gases, rationalizing the reactivity of Fe(111) > Fe(100) > Fe(110). Somorjai showed that small amounts of K promote the catalysis increasing the rates by a factor of two. However the location of the K in the catalyst is not known, so we will compare to Somorjai results for the most active Fe(111) bare surface without K or other promoters.

We report here QM calculations on the 26 surface adsorbate configurations important in the **full** reaction mechanism including the free energy barriers that determine the rates for the 17 steps that we find to play an important role in the catalysis under Somorjai conditions. Then we use these predicted rates in a self-consistent kinetic Monte Carlo (kMC) model to predict the steady state rates of all the reaction steps to obtain the turn over frequency (TOF) for the Somorjai single crystal conditions. At 673K and 20 atm pressure, we predict TOF=17.7 sec<sup>-1</sup> per 2x2 site (5.3 x 10<sup>-9</sup> moles/sec-cm<sup>2</sup>), which is in excellent agreement with the experimental TOF=9.7 sec<sup>-1</sup>. This validates our modeling results, providing the basis for using theory to help design improved catalytic systems.

#### 2. Methods

For these QM studies we use the Perdew-Burke-Ernzerhof (PBE) flavor of Density Functional theory (DFT). including the D3 (Becke Johnson)<sup>15</sup> empirical corrections for long range London dispersion (van der Waals attraction).<sup>16</sup> The reason is that this level of QM has been validated recently for several systems. Thus reference<sup>17</sup> carried out systematic studies for the oxygen reduction reaction (ORR,  $O_2$  + protons  $\rightarrow$   $H_2O$ ) on Pt(111) using the same PBE-D3 level as in this paper. Including 5 layers of explicit solvent in QM metadynamics on all reaction steps, comparisons could be made to experimental activation barriers for two values of the external potential. In both cases the calculated activation barriers were within 0.05 eV of the experiment.

For the CO reduction reaction on Cu(100) the same level of theory obtains an activation energy within 0.05 eV of experiment. This same level of theory has also led to similar accuracy for the oxygen evolution reaction on  $IrO_2^{22}$  and for onset potentials on Cu(111).

This is not a guarantee that PBE-D3 will work as well for Fe, where the presence of unpaired spins could cause problems, but it provides a reasonable starting point. Indeed, the accuracy compared to experiment seems to be comparable to these other cases.

Indeed, we carried out exactly the same set of calculations at the PBE level without D3 (results in the SI) and find TOF=89.3 compared to 17.7 for PBE-D3 and 9.7 experiment. This indicates that for this system PBE-D3 provides better accuracy than pure PBE.

All calculations were carried out with the  $VASP^{26}$  software package. We established that an energy cutoff of 400eV leads to converged forces. The K-point sampling was chosen to be 4 x 4 x 1. All calculations include spin-polarization.

#### 2.1 Small Gas Molecules

Calculations for the gas phase molecules used the PBE functional (as implemented in Jaguar) with the D3 empirical correction for London dispersion. Free energy corrections including enthalpy (H), entropy (S), and zero-point energy (ZPE) from Jaguar calculations are included in Supplemental Information (SI).

To obtain the total free energy, G=H-TS, for the gas molecules at temperature T, we add to the DFT electronic energy (E), the zero-point energy (ZPE) from the vibrational levels (described as simple harmonic oscillators), and the specific heat corrections in the enthalpy from 0 to T. The entropy (S), as a sum of vibrational, rotational and translational contributions, are evaluated from the same levels. To correct the free energy for pressure, we assume an ideal gas and add  $RT*ln(P_2/P_1)$  with a reference pressure of P=1 atm.

The Free energy changes ( $\delta G$ ) for the overall Haber Bosch reaction N<sub>2</sub>+3H<sub>2</sub> => 2NH<sub>3</sub> under various conditions are calculated as

```
\begin{split} \delta G &= 2*E(NH_3) + 2*ZPE(NH_3) + 2*H(NH_3) - 2T*S(NH_3) - \\ &[E(N_2) + 3*E(H_2) + ZPE(N_2) + 3*ZPE(H_2) + H(N_2) + 3*H(H_2) - T*S(N_2) - 3T*S(H_2)] \end{split}
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The pressure dependence is added using RT\*ln( $P_2/P_1$ ), 5atm and 15atm for  $N_2$  and  $H_2$  respectively. We calculate  $\delta G$  is -0.52 eV for the reaction under 673°K, and 20atm total pressure, which can be compared with  $\delta G$  =-0.02eV at 700°K and 5:15:1 atm  $N_2$ ,  $H_2$  and  $NH_3$ , respectively, from experiment. <sup>30</sup> We calculate  $\delta G$  is -1.22 eV for the reaction under 673°K, 5atm: 15atm: 1.5 torr for  $N_2$ ,  $H_2$ , and  $NH_3$  respectively.

#### 2.2 Surface Optimization

The PBE-D3(BJ) level of DFT leads to a calculated lattice parameter of a = 2.807 Å for the bulk Fe bcc structure at 0°K, slightly smaller than the experimental value 2.866 Å at 298°K. <sup>31</sup> This level of DFT predicts a magnetic moment for bulk Fe of 2.23  $\mu$ B in excellent agreement with the experimental value, 2.22  $\mu$ B. <sup>31</sup>

For calculating the surface chemistry, we selected the (111) surface which Somorjai showed to be the most active catalytically. For these DFT calculations we use a two-dimensional periodic slab with six layers of Fe atoms each of which consists of a (2 x 2) (6.912 Å x 8.276 Å) unit cell (4 surface Fe per cell). We include 15 Å of vacuum in the z direction to minimize possible interactions between the replicated cells. The top five layers are relaxed while the bottom layer is kept fixed at the optimum geometry calculated for bulk Fe.

The vibrational frequencies for free energy calculations are calculated by allowing the adsorbed molecules and the top 3 layers of Fe to relax, with the bottom two layers fixed. For these phonon calculations we used 10<sup>-6</sup> eV energy convergence threshold to obtain reliable phonon frequencies (no negative eigenvalues.) To obtain the Free energy, G=H-TS, for the various equilibrium

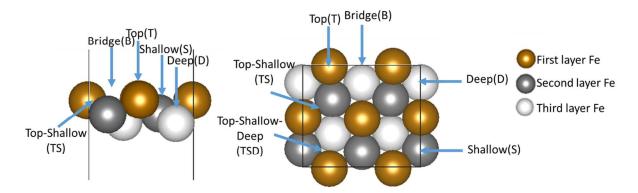
configurations, we used density functional perturbation theory (DFPT) to calculate the phonon density of states, which was used to calculate the ZPE, the temperature correction to the enthalpy, and the vibrational contributions to the entropy. An identical procedure was used for the transition states. We note that some of the frequencies correspond to hindered translational or rotational modes, for which the harmonic oscillator description is less accurate. In these cases, namely  $NH_3$  and  $N_2$  desorption calculations, we use ZPE corrections only<sup>32-34</sup>.

#### 2.3 Transition States

Transition state searches used the climbing image NEB method in the VASP-VTST code. <sup>35</sup> Here the initial and final states geometries were minimized first. Then three intermediate images were optimized, excluding initial and final images. An additional NEB climbing-image calculation was performed to obtain the final value of the barrier. The climbing NEB method generates a true transition state, as we confirmed by performing vibrational frequency calculations showing a single negative curvature in the Hessian. Dimer calculations <sup>36-37</sup> were performed whenever extra imaginary frequencies were found in the NEB transition state image.

#### 2.4 Surface sites

The adsorption sites for the various species H, N, NH, NH<sub>2</sub>, NH<sub>3</sub> calculated here are consistent with previous experimental<sup>38</sup> and DFT results<sup>39-41</sup>. The Fe(111) surface has four types of adsorption sites: top (T), bridge (B), 3-fold-shallow (S), and 3-fold-deep (D), with top/shallow (TS), and top-Shallow-deep (TSD) intermediate sites, as shown in Figure 1.



**Figure 1.** Structure of the Fe(111) surface with various surface adsorption sites noted. Bronze spheres represent the top layer, dark grey spheres represent the second layer, while white spheres are third layer Fe atoms. Multiple adsorption sites are labeled from both top and side views, including B, T, S, D, TS, and TSD sites. This figure shows only 3 of the 6 layers used in the calculations.

We find generally that

- H prefers the TS site between a top Fe and a 2<sup>nd</sup> layer Fe or the TSD site between Fe on all 3 layers
- N prefers the B site,
- NH prefers the BD site, with N sitting on the bridge(B) site, but NH pointing sideways toward the D site
- NH<sub>2</sub> prefers the TS site between a top Fe and a 2<sup>nd</sup> layer Fe.

• NH<sub>3</sub> prefers the T site.

but as shown below in Fig. 3 occupation of other sites sometimes shifts the minima.

## 3. Energy landscape. The most favorable pathways for converting $3H_2+N_2$ to $2NH_3$ , with illustrations for $T=673\,^{\circ}K$ and p=20atm

We carried out DFT calculations including various numbers of H, N, NH, NH<sub>2</sub>, NH<sub>3</sub> molecules bound to the various stable sites for a 2x2 supercell of the (111) surface. For each combination of sites, we calculated the vibrational frequencies to obtain the free energy at the operational temperature. Then we calculated the reaction barriers for the various reaction pathways. We then used these values to find reaction sequences with lowest overall free energy barrier for the full process of converting one N<sub>2</sub> and three H<sub>2</sub> to form two NH<sub>3</sub>.

For a total pressure P=20 atm under stoichiometric conditions and T=673°K, we find that the lowest free energy for an equilibrium in which no reactions are allowed is the 3N\_NH<sub>2</sub> configuration shown in Figure 2. Thus, prior to allowing reactions to proceed, the equilibrium condition on the Fe(111) surface in our 2x2 model would be predominantly the 3N\_NH<sub>2</sub> configuration. We take the free energy of this state as our reference point, with G=0. However, as discussed in section 4, the steady state kinetic process producing NH<sub>3</sub> leads to different distributions of states that depend on the NH<sub>3</sub> pressure assumed for the steady state.

We examined the barriers between all the states connecting though reactions of  $N_2$  and  $H_2$  at various sites, leading finally to the energy landscape in Figure 2, involving 26 intermediates and leading to the lowest maximum barriers. We include in Figure 2 the states that we found to be important for the steady state kinetics as described in section 5. We confined our calculations to the 2x2 supercell.

The favorable path selected in Fig. 2 includes the following transitions (all energies in eV)

- 1.  $3N_NH_2 + 3H_2gas + N_2gas$ ; G=0 at T=673°K and p=20atm
- 2. =>3N NH<sub>2</sub> 2H (H<sub>2</sub>gas $\rightarrow$  H\* + H\*) G=0.57, where we expect a barrier of 0.57 eV.
- 3. =>3N NH<sub>3</sub> H (H\* + NH<sub>2</sub>\* $\rightarrow$  NH<sub>3</sub>\*) G=0.30 and G†= 1.47
- 4.  $\Rightarrow$  3N\_H (NH<sub>3</sub>\*to NH<sub>3</sub>gas) G= -0.26 and G†= 1.12
- 5. =>2N NH (H\*+N\* $\rightarrow$ NH\*) G= 0.22 and G†= 0.66
- 6. =>2N\_NH\_2H ( $H_2$ gas $\rightarrow$  H\* + H\*) G=0.30, we calculate a barrier of 0.57 eV.
- 7. =>2N\_NH<sub>2</sub>\_H (NH\*+H\* $\rightarrow$ NH<sub>2</sub>\*) G= -0.39 and G†= 0.56, described in detail in transition state section.
- 8. =>2N\_NH<sub>3</sub> (NH<sub>2</sub>\*+H\*→NH<sub>3</sub>\*) G=0.39 and G†= 1.36, however, there is an alternative path from 2N\_NH<sub>2</sub>\_2H to 2N\_NH<sub>3</sub>\_H, with a lower barrier of G†= 1.13, this will be further discussed in the kMC section. The resting state of this step is indeed 2N\_NH<sub>2</sub>\_H, with G = -0.39, together making this barrier 1.13+0.39 = 1.52 in kMC.
- 9. =>2N (NH<sub>3</sub>\*to NH<sub>3</sub>gas) G=0.11 and G†= 1.40 Similar with the previous step, there is an alternative path from 2N\_NH<sub>3</sub>\_H => 2N\_H, with a lower barrier of G†= 1.03. Similarly, the resting state is  $2N_NH_2_H$ , with G = -0.39, together making this barrier 0.39+1.03 = 1.42 in kMC. These alternative paths are shown in figure 2 using green color.

- 10. =>  $2N_N_2(N_2gas \rightarrow N2*triple bonded$ , top layer) G= 0.20. This step involves  $N_2$  adsorption (G†= 0.94) and its resting state is  $2N_2H$  (edge configuration, see the SI) with G = -0.63, together making this barrier 0.94+0.63=1.57 in kMC.
- 11. =>  $4N(N_2* \rightarrow N*+N*)$  G= -1.10 and G†= 0.64 is the highest barrier along  $N_2$  dissociation, see SI Fig. S4.
- 12. => 3N\_NH\_H (H\*+ N\* $\rightarrow$  NH\*) G= -0.65 and G†= -0.07
- 13. =>3N NH<sub>2</sub> (NH\*+H\* $\rightarrow$ NH<sub>2</sub>\* to complete the cycle).

The above states are described by a simple linear energy landscape in Figure 2, confined in a 2x2 cell. However, we have also included the most populated states involved in the steady state kMC calculations, such as 2N H and 2N 2H.

- 14.  $3N_NH_3 => 3N (NH_3*to NH_3gas)$ , G from 0.30 => 0.41, and G†= 1.34
- 15.  $2N_NH_2_2H => 2N_NH_3_H (NH_2* + H* \rightarrow NH_3*)$ , G from -0.27 => 0.01, and G†= 1.13
- 16. 2N NH<sub>3</sub> H => 2N H (NH<sub>3</sub>\*to NH<sub>3</sub>gas), G from 0.01 => -0.22, and G†= 1.03
- 17. 2N H  $\Rightarrow$  2N, G from  $-0.22 \Rightarrow 0.11$
- 18.  $2N \Rightarrow 2N$  2H, G from  $0.11 \Rightarrow -0.63$

In this simplified scheme we considered dissociative chemisorption of  $H_2$ gas to  $H^* + H^*$  explicitly only for the step  $2N + H_2$ gas to  $2N_2H$ . This step is closest to the dissociative chemisorption of  $N_2$ gas to  $N^* + N^*$  that in Section 5 we single out as the RDS in our kinetic model. We find that  $NH_3$  production rate changes from 17.7 sec<sup>-1</sup> per  $2x^2$  site to TOF 17.5 sec<sup>-1</sup> if we use the calculated barrier of 0.57 eV instead of setting the barrier to zero. For other steps we assume  $H_2$  dissociative chemisorption to have barrier that's small enough to not affect kinetics. And we form successive  $NH_x$  species by the Langmuir-Hinshelwood (LH) mechanisms:  $NH_x^* + H^* \rightarrow NH_{x+1}^*$  (for PBE\_D3, step 12 LH is small enough, and not rate determining. Thus, we don't consider ER further).

The highest-energy transition states in the free energy landscape are, in decreasing order:

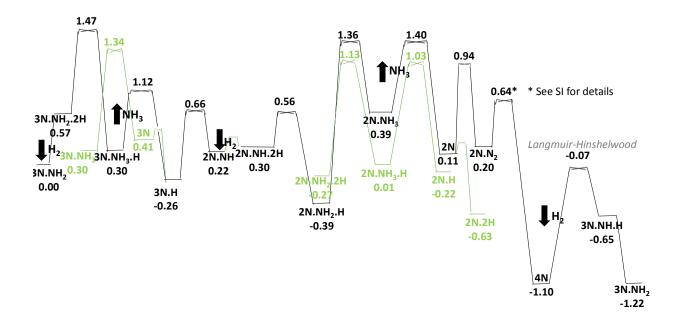
- TS3: step 3 with  $G^{\dagger}=1.47$  eV involves  $H^* + NH_2^* => NH_3^*$ , an LH mechanism. The detailed transition state structure is shown in Fig S3(b) of the SI.
- TS 8: step 8 with  $G^{\dagger}=1.13$  eV involves  $H^* + NH_2^* => NH_3^*$ , an LH mechanism. The detailed transition state structure is shown in Fig S3(a) of the SI.
- TS4: step 4 with  $G^{\dagger}=1.12$  eV involves  $NH_3^* => NH_3$  gas, just as in step 9. We used electronic adsorption energy of NH3 with ZPE correction as the desorption barrier.
- TS9: step 9 with G†=1.03 eV involves NH<sub>3</sub>\* => NH<sub>3</sub> gas, shown in the green path of figure 2. Here, we considered the alternative pathway of desorption NH<sub>3</sub> from 2N\_NH<sub>3</sub>\_H. We used electronic adsorption energy of NH<sub>3</sub> with ZPE correction as the desorption barrier.
- TS10: step 10 with G†=0.94 eV, we included N<sub>2</sub> adsorption into consideration, and used the electronic adsorption energy together with ZPE as the desorption barrier, and this leads to G†=0.94 eV.
- TS5: step 5 with G†=0.66 eV involves H\* + N\* => NH\*, an LH mechanism. The NEB energy and structures are shown in Fig. S2(a) of the SI. This is the lowest energy barrier for adding an H to NHx. We also examined  $3N_H + H_2(gas) => 2N_NH_2H$  in which gas phase

H<sub>2</sub> adds to N\* to form NH\* + H\*, This involves a high energy intermediate state with G= 1.78eV, so we will not consider this step further.

- TS 11: step 11 with  $G^{\dagger}=0.64$  eV. We took consideration of  $N_2$  dissociation.
  - a) the initial bonding of  $N_2$  retains the triple-bond while making a sigma bond to an on-top site on the first layer (denoted  $\sigma N \equiv N$ -T phase, where  $\equiv$  in the middle represents the bond order, and T represents adsorption on top layer, or Nørskov  $\gamma$ )
  - b) there is a barrier to moving to a sigma bond to an on-top site on the second layer (denoted  $\sigma N \equiv N-S$ , where S represents adsorption on second layer, or Nørskov  $\delta$ )
  - c) There is a barrier for one  $\pi$  bond of  $N_2$  to bind to two surface Fe atoms (denoted as  $\pi N=N-\eta_2$  or Nørskov  $\alpha$ )
  - d) There is a barrier for the  $2^{nd}$   $\pi$  bond of  $N_2$  to 4N, with the N-N bonding to three surface Fe atoms (denoted as  $2\pi N-N\eta_3$  or Nørskov  $\alpha$ ')
  - e) Finally, there is a barrier for the remaining N-N bond to dissociate with each N bonding to 4 surface atoms (denoted as Nørskov  $\beta$  phase), leading to the 4N state. The NEB energy and structures for  $N_2$  dissociation are shown in Fig. S4 of the SI.
- TS7: step 7 with G†=0.56 eV involves H\* + NH\*→ NH<sub>2</sub>\*, an LH mechanism. The NEB energy and structures are shown in Fig. S2(b) of the SI.
- TS12: step 12 with  $G^{\dagger}=-0.07$  eV is an LH mechanism in which  $H^*+N^*=> NH^*$
- State 13. This is the same as the state 1 but the G=-1.22 eV because we have produced two NH<sub>3</sub> from 3H<sub>2</sub> +N<sub>2</sub>. Similarly, state 11 has G=-1.10 because we already have produced two NH<sub>3</sub> along the pathway.

The energy landscape is plotted in Figure 2 for the Somorjai experimental conditions of  $673^{\circ}$ K and 20 atm of total pressure (H<sub>2</sub> and N<sub>2</sub> in stoichiometric ratio and NH<sub>3</sub> pressure = 1.5 torr)<sup>13</sup>. The lowest free energy state 3N NH<sub>2</sub> is taken as reference, setting G=0.

#### PBE\_D3, 673K, 20 atm



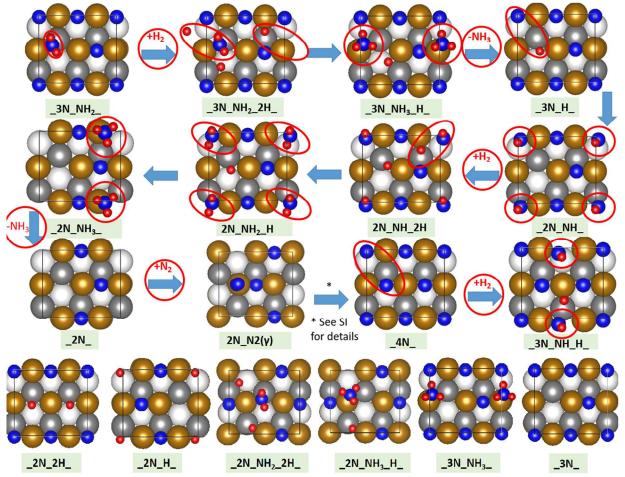
**Figure 2.** Energy landscape for NH<sub>3</sub> synthesis reactions under Somorjai condition, 673°K, 20atm. The lowest energy state 3N\_NH<sub>2</sub> is taken as reference, with a free energy of zero. We considered the linear pathway in black and proposed alternative pathway in green, in order to obtain the optimum barriers.

NH<sub>3</sub> production rate is dominated by 3 steps:

- 1). N<sub>2</sub> dissociation and desorption,
- 2). hydrogenation of NH<sub>2</sub>, and
- 3). NH<sub>3</sub> desorption.

This diagram considers the reaction of 3 H<sub>2</sub> plus 1 N<sub>2</sub> to form 2 NH<sub>3</sub>, so that the total free energy decreases by 1.22 eV as we go from 3N\_NH<sub>2</sub> on the left to 3N\_NH<sub>2</sub> on the right. The free energy diagram with same states calculated at PBE level can be found in SI fig. S1.

The simplified reaction pathway described above is illustrated pictorially in Figure 3 showing the surface structure step by step, to clarify the nature of each adsorption site and the interactions between these adsorbed species.



**Figure 3.** Surface structure for selected reaction steps in Fig. 2. Bronze spheres represent first layer Fe atoms, Dark gray represents second layer Fe atoms, and white represents third layer Fe

atoms. Nitrogen atoms are shown using navy blue spheres, and hydrogen atoms are shown using red spheres. Every intermediate structure is geometrically optimized with the results summarized in Fig (3) to illustrate the adsorption sites for various species, and interaction between these adsorbed species. Note that in cases where species are at the edges, we show all images that map onto the 2x2 cell. In cases where a circle is used to highlight the reactive species at an edge we show the other equivalent circles.

Transition state geometries are shown in SI Fig. S2-4. We considered five reactions:

- A. 3N  $H \Rightarrow 2N$  NH, migration of hydrogen and addition to N on the surface (LH);
- B. 2N NH 2H => 2N NH<sub>2</sub> H, hydrogen migration and addition to NH on the surface (LH);
- C. 3N NH<sub>2</sub> 2H  $\Rightarrow$  3N NH<sub>3</sub> H, hydrogen migration and addition to NH<sub>2</sub> on the surface (LH);
- D. 2N NH<sub>2</sub> 2H  $\Rightarrow$  2N NH<sub>3</sub> H, hydrogen migration and addition to NH<sub>2</sub> on the surface (LH);
- E.  $2N_{N_2} => 4N$ . This involves a complex pathway from triple-bonded  $N_2$  adsorbed on first layer ( $\sigma N \equiv N-T$  or  $\gamma$ ) => triple-bonded  $N_2$  adsorbed on second layer ( $\sigma N \equiv N-S$  or  $\delta$ ) => double-bonded  $N_2$  to a bridge site ( $\pi N = N\eta_2$  or  $\alpha$ ) => single-bonded  $N_2$  at a 3-fold site ( $2\pi N-N\eta_3$  or  $\alpha$ ') => the dissociated state  $4N(\beta)$ .

#### 4. Discussion of the wavefunctions

Since Fe is ferromagnetic, we analyzed the magnetic moments of the various atoms and the changes in the key steps of ammonia synthesis. Total magnetic moments for all the states along the pathway can be found in Table 1.

name	total mag(uB)	dMAG	covalent bond to Fe	ratio	#comment	#comment
111_surface_24Fe	64.76	0.00	0			2.70 per Fe
3N.NH <sub>2</sub>	57.10	-7.66	10	77%	3*3+1	
3N.NH <sub>2</sub> .2H	56.49	-8.26	12	69%	3*3+1+2	0.3 per H
TS_3N.NH <sub>2</sub> .2H	55.94	-8.82				
3N.NH₃.H	56.33	-8.43	10	84%	3*3+1	
3N.H+NH₃(g)	57.00	-7.75	10	78%	3*3+1	
TS_3N.H+NH₃(g)	57.54	-7.22				
2N.NH+NH₃(g)	58.17	-6.59	8	82%	3*2+2	
2N.NH.2H+NH <sub>3</sub> (g)	57.27	-7.48	10	75%	3*2+2+2	
TS_2N.2H.NH+NH <sub>3</sub> (g)	58.80	-5.96				
2N.NH2.H+NH <sub>3</sub> (g)	59.35	-5.40	8	68%	3*2+1+1	
TS_2N.H.NH2+NH <sub>3</sub> (g)	59.08	-5.67				
2N.NH <sub>3</sub> +NH <sub>3</sub> (g)	59.45	-5.30	6	88%	3*2	
2N_diagonal.NH₂.2H	58.32	-6.44	9	72%	2*3+1+2	
TS_2N_diagonal.NH <sub>2</sub> .2H	58.64	-6.12				
2N_diagonal.NH₃.H	59.08	-5.68	7	81%	2*3+1	2.84 per N
2N+2NH₃(g)	59.83	-4.93	6	82%	3*2	
$2N.N2(\sigma N \equiv N-T) + 2NH_3(g)$	58.83	-5.92	6	99%	3*2	No N2 to Fe
$TS(\sigma N \equiv N-T => \sigma N \equiv N-S)$	59.21	-5.54				

$2N.N2(\sigma N \equiv N-S) + 2NH_3(g)$	58.51	-5.54	6	92%	3*2	No N2 to Fe
$TS(\sigma N \equiv N-S \Rightarrow \pi N=N)$	58.37	-6.38				
2N.N2(πN=N)+2NH <sub>3</sub> (g)	58.65	-6.11	8	76%	3*2+2	2 new N-Fe
TS(πN=N=>2πN-N)	58.53	-6.23				
2N_N2(2πN-N)+2NH <sub>3</sub> (g)	58.17	-6.59	10	66%	3*2+4	4 new N-Fe
TS(2πN-N =>N+N)	57.36	-7.39			8	
4N+2NH <sub>3</sub> (g)	54.77	-9.98	12	83%	3*4	2.50 per N
4N.2H+2NH <sub>3</sub> (g)	54.32	-10.44	14	75%	3*4+2	
TS_4N.H2	55.40	-9.35				
3N.NH.H+2NH <sub>3</sub> (g)	55.92	-8.84	12	74%	3*3+2+1	
3N.NH <sub>2</sub> +2NH <sub>3</sub> (g)	57.10	-7.66	10	77%	3*3+1	
Average in covalent				77%		
character						

**Table 1.** Analysis of change in spin along the pathway. Total magnetic moment for each state and the change with respect to pure Fe are reported. Covalent bond calculated using simple VB theory is presented in covalent bond column, and we assume each adsorbed N, NH, NH<sub>2</sub>, NH<sub>3</sub>, H to decrease spin moment 3, 2, 1, 0, 1 respectively.

We observe non-negligible changes in these moments along the reaction pathways.

In earlier studies of hydrocarbon intermediates on the metals Ru, Rh, Pd, Os, Ir, Pt, Kua and Goddard proposed a Valence Bond (VB) model in which alkyl, alkylidene, and alkylidyne intermediates to a metal surface are considered to make 1, 2, or 3 valence bonds to the metal surface and showed that this correlates well with bond energies and other properties. <sup>42-45</sup> We propose a similar valence bond (VB) model to understand the spin changes in spin for Fig. 4(a) and SI table 2. We assume that each of the unpaired spins of N atom makes a covalent bond to an unpaired spin on the neighboring Fe atoms, reducing the spin by 3 units. Indeed, for the 4N state the spin of the cluster is reduced by 10.51 or 2.63 spins per N. We will also assume that the two unpaired spins of NH can make two bonds, which should reduce the Fe spin by 2 units and NH<sub>2</sub> can make one =bonds, which should reduce it by 1 unit as should H.

From table 1, we see that the net spin changes observed in the 14 states that are not TS, average 77% of the expected value for this model, supporting this simple Valence Bond view of bonding. Of course a more complete analysis should consider the ligand field splitting to these unpaired spins and the orbital requirements to form a covalent bond from the Fe d-orbitals to the N porbitals, but we think that the simple VB view accounts for the major spin coupling effects.

These changes in magnetic moment suggests an important role for spin in the reactions, which suggests that engineering the spin of surface atom may provide a new way to increase Haber Bosch reaction efficiency. This suggests designing new catalysts that have different spin character, e.g., Co, Ni, Mn, or Cr all of which can exhibit localized spins, or Ru or Os which should not have large spins. Also the changes in the oxidation state of the atoms reported in Figure 4(b) are noteworthy and analogously suggest an important concomitant effect of charge transfer effects.

#### 5. Kinetic modelling results with illustrations for T=673°K and p=20atm

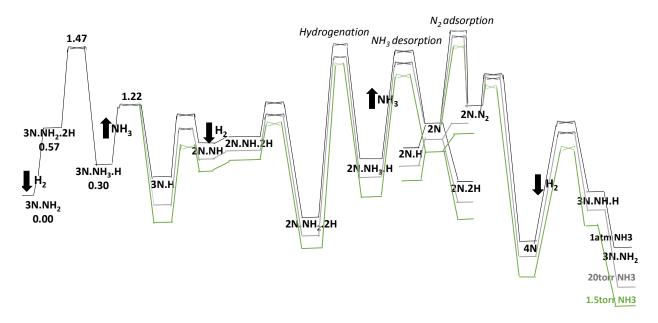
#### **5a. Kinetic Monte Carlo Simulations**

The free energies in Fig. 2 provide a crude estimate for the rate. Here we might estimate the rate from transition state theory (TST) as  $k=(k_BT/h)\exp[-1.57/k_BT]=24 \text{ sec}^{-1}$ , leading (after multiplication by a factor of 2 due to the presence of 2 reaction sites in the unit cell) to a TOF of 48 NH<sub>3</sub> molecules per second per (2x2) unit cell.

However, for such a complex mechanism, it is necessary to go beyond this rough estimate with simulations that include all distributions of the states involved and the rates between them in a full kMC model, allowing the system to achieve steady state. We evaluated each rate using transition state theory as  $(k_BT/h)\exp(-\Delta G^{\dagger}/k_BT)$ , where  $\Delta G^{\dagger}$  is the difference in free energy between the starting state and the saddle point. In the case of ER reactions involving gas-phase species turning into adsorbates, we again use transition state theory, but for the reverse LH process, and then we invoke microscopic reversibility principle to calculate the rate of the direct process.

This system is not in equilibrium. To consider the kinetics of the system in steady state, we carried out kMC calculations as discussed below. In this case we find that the state  $2N_2H$  has the lowest  $\Delta G$  under steady-state conditions at  $P(H_2)=15$  atm,  $P(N_2)=5$  atm,  $P(N_3)=1.5$  torr, T=673 °K, and the free-energy difference between this state and the highest point  $\Delta G^{\dagger}$  along the reaction path is 1.57 eV. Taking into consideration the states important in the kMC calculations and varying  $NH_3$  pressure leads to the diagram in Figure 4.

#### PBE D3 Effect of NH3 Pressure



**Figure 4.** Illustration of how the equilibrium energy landscape from Figure 2 becomes modified for steady state kinetics of forming NH<sub>3</sub> at different pressures from 15 atm of H<sub>2</sub> and 5 atm of N<sub>2</sub> at 673°K (Somorjai conditions). We show the results for three pressures of NH<sub>3</sub> product: 1.5 torr, 20 torr, and 1 atm. Barriers in green are assumed to be fast and assigned rates of  $10^{11}$  s<sup>-1</sup>. The populations are shown in Table 2. We see here that NH<sub>3</sub> acts as a poison, decreasing the TOF from 17.7 at 1.5 torr, to 16.5 at 20 torr, to 2.8 at 1 atm.

In the Somorjai et al<sup>13</sup> papers, the measured ammonia production at 673 °K and 15 atm  $H_2$ , 5 atm  $N_2$ , extrapolated to zero ammonia pressure is 2.8 x  $10^9$  NH<sub>3</sub> moles/cm<sup>2</sup>/sec which corresponds to 9.7 NH<sub>3</sub> molecules produced per second on a (2x2) unit cell.

We conducted kMC simulations at T = 673 °K and pressures:  $pH_2=15atm$ ,  $pN_2=5atm$  and  $pNH_3=1.5$  torr. We used 20 independent replicas and 2 x  $10^9$  kMC steps each (checking that the results converged within 5% with respect to a test case using 100 replicas and 2 x  $10^{10}$  kMC steps) for a total simulated time of 2733 sec. This leads to production of 48482 NH<sub>3</sub> molecules produced by our (2x2) unit cell, corresponding to a **predicted TOF= 17.7 NH<sub>3</sub> molecules per second per (2x2) site, in good agreement with the experimentally measured TOF of 9.7** (our predicted rate should be higher than experiment since our surface is perfect). We should caution here that the final TOF is very sensitive to the key barriers at the RDS. Thus to change the 17.7 to 9.7 we need only increase the free energy of the transition state for the 10th step from 0.94 eV to 0.98 eV.

As shown in the SI, exactly the same set of calculations at the PBE level without D3 find TOF=89.3 compared to 17.7 for PBE-D3 and 9.7 experiment. This indicates that for this system PBE-D3 provides better accuracy than pure PBE. However, the rate for the PBE level would match experiment by changing the barrier for the 3rd step from 1.47 eV to 1.64 eV. Of course the real accuracy depends on that for quite a number of individual steps.

The steady-state apparent  $\Delta G$  (i.e., the logarithm of the relative populations) for the most important states are reported in Table 2, which shows that the processes before and after the ammonia desorption are not far from equilibrium. That is, the populations are not far from those expected on the basis of their equilibrium  $\Delta G$  according to the Boltzmann distribution (the percent of residence times is also shown), except for the irreversible ammonia desorption steps.

If instead of  $NH_3=1.5$  torr, we use  $NH_3=1$  atm, shown in Figure 5, the total rate from the kMC is 2.8  $NH_3$  molecules per second per (2x2) site. Thus  $NH_3$  is a poison. Somorjai et al does not report the dependence of TOF on  $NH_3$  pressure for the (111), but they do report it for Fe(100)<sup>14</sup>:

- for 20 torr pressure of NH<sub>3</sub>, TOF=0.21 NH<sub>3</sub>-molecules/sec/(2x2)
- for 1.5 torr pressure of NH<sub>3</sub>, TOF=1.1 NH<sub>3</sub>-molecules/sec/(2x2)
- extrapolating to zero NH<sub>3</sub> pressure, leads to TOF= 1.5 NH<sub>3</sub>-molecules/sec/(2x2).

Thus the experimental poisoning effect of NH<sub>3</sub> on (100) is similar to what we predict for (111).

Analogous kMC simulations at T = 730 °K and pressures:  $pH_2=15$ atm,  $pN_2=5$ atm and  $pNH_3=1.5$  torr give a TOF = 83.3 NH<sub>3</sub> molecules per second per (2x2) site which is still in reasonable agreement with the experimentally measured TOF of 22.8 from Figure 13 of Ref. <sup>13</sup> In conclusion, we find that hydrogenation of NH<sub>2</sub>, NH<sub>3</sub> desorption, H<sub>2</sub> poisoning, and N<sub>2</sub> desorption can be rate determining depending on the reaction conditions, while previous work on Fe-catalysts emphasized on N<sub>2</sub> dissociation being the sole rate determining step. <sup>12</sup>

### 5b. Rates for typical Haber Bosch conditions: T=723°K and p=200atm

The Haber-Bosch (HB) industrial process is conducted under a range of temperatures and pressures, with typical temperatures in the range 450-550 °C and total pressure around ~200 atm with a stoichiometric ratio of  $N_2$  and  $H_2$ . To compare our predictions with industrial conditions,

we choose T = 730 °K and two sets of pressures: (pH<sub>2</sub>=150 atm, pN<sub>2</sub>=50 atm, pNH<sub>3</sub>= 1 atm), and (pH<sub>2</sub>=120 atm, pN<sub>2</sub>=40 atm, pNH<sub>3</sub>= 20 atm), corresponding approximately to conditions holding at the beginning and the end of the HB process. For comparison, we also add that at pNH<sub>3</sub>= 1.5 torr Figure 2 becomes Figure S6 of the SI leading to a naïve TOF= 258 (or 516 after multiplying by a factor of 2), which is about 5 times what we predict for Somorjai conditions using the same rough formula.

Running kMC simulations under these two conditions leads to NH<sub>3</sub> production rates of 93.7 NH<sub>3</sub>-molecules/sec/(2x2) at pNH<sub>3</sub>= 1 atm, and 18.5 NH<sub>3</sub>-molecules/sec/(2x2) at pNH<sub>3</sub>= 20 atm, respectively. Free energy differences due to populations and thermodynamic free energy differences for various states are shown in Table 2.

	T=673, pH <sub>2</sub> =15, pN <sub>2</sub> =5, pNH <sub>3</sub> =1.5/760			T=730, pH <sub>2</sub> =150, pN <sub>2</sub> =50, pNH <sub>3</sub> = 1			T=730, pH <sub>2</sub> =120, pN <sub>2</sub> =40, pNH <sub>3</sub> =20		
configuration	t <sub>i</sub> (%)	$-ln(P_i/P_0)$	ΔG	t <sub>i</sub> (%)	$-\ln(P_i/P_0)$	ΔG	t <sub>i</sub> (%)	$-ln(P_i/P_0)$	ΔG
3N NH <sub>2</sub>	6.5	0.00	0.00	1.4	0.00	0.00	7.2	0.00	0.00
3N NH <sub>2</sub> 2H	3E-4	0.57	0.57	5E-4	0.50	0.49	2E-3	0.51	0.51
3N_NH <sub>3</sub> _H	6E-4	0.54	0.30	0.003	0.38	0.21	0.19	0.23	0.23
3N_H	1.1	0.10	-0.26	0.32	0.09	-0.08	1.2	0.11	0.11
2N_NH	6E-4	0.54	0.22	3E-4	0.52	0.39	1E-3	0.54	0.59
2N_NH_2H	1E-4	0.63	0.30	3E-4	0.53	0.36	8E-4	0.57	0.61
2N_NH <sub>2</sub> _H	20.	-0.07	-0.39	21.7	-0.17	-0.31	64.5	-0.14	-0.09
2N_NH <sub>3</sub>	5E-5	0.69	0.39	8E-5	0.61	0.47	4E-4	0.61	0.68
2N	2E-4	0.61	0.11	1E-3	0.62	0.47	2E-5	0.82	0.88
4N	0.22	0.20	-1.10	2E-2	0.28	-0.80	0.092	0.27	-0.80
3N_NH_H	4E-3	0.57	-0.65	1E-4	0.57	-0.43	8E-4	0.57	-0.41
2N_2H_lin	53.6	-0.12	-0.63	61.1	-0.24	-0.41	11.4	-0.03	0.02
2N_2H	16.9	-0.06	-0.56	10.4	-0.13	-0.24	1.96	0.08	0.19
2N_NH <sub>3</sub> _H	3E-3	0.45	0.24	5E-2	0.21	0.05	0.19	0.23	0.26
2N_H	5E-2	0.29	-0.22	2E-2	0.25	0.10	5E-3	0.46	0.52
2N_NH2_2H	1.6	0.08	-0.30	5.0	-0.08	-0.22	13.2	-0.04	0.03
kMC theory NH <sub>3</sub> mol/s/(2x2)	17.7		93.7			18.6			
Experiment <sup>13</sup> NH <sub>3</sub> mol/s/(2x2)	9.7			N/A			N/A		
total NH <sub>3</sub> mol	48482			33764			2529		
$3N_NH_3_H$ $\leftrightarrow 3N_H$	24262			16801			1284		
$\begin{array}{c} 2N\_NH_3\_H \\ \leftrightarrow 2N\_H \end{array}$	24220			16963			1245		

**Table 2.** Top rows – Per cent of populations (i.e., residence times) =  $t_i$ (%), apparent free energy differences [evaluated as minus the logarithm of ratio of populations =  $P_i/P_0$ , where  $P_0 = P_{3N\_NH2}$ ], and thermodynamic free energy differences ( $\Delta G$ ) for selected configurations in a Fe(111)-(2x2) unit cell under steady-state of ammonia synthesis as predicted by kMC simulations at different temperatures (673 and 730 K), and different  $H_2$ ,  $H_2$ ,  $H_3$  pressures using data from DFT/PBE-

D3. All configurations are assumed in the zig-zag arrangement, except for "2N\_2H\_lin" which is linear (see SI for details). Temperature in Kelvin, pressure in atmospheres, free energy differences in eV. Bottom rows – NH<sub>3</sub> molecules produced per second per (2x2) unit cell under the given conditions [NH<sub>3</sub>mol/s/(2x2) : the conversion factor to moles per second per cm<sup>2</sup> in ref<sup>13</sup> is 3 x 10<sup>-10</sup>], total number of NH<sub>3</sub> molecules produced in the kMC runs (total NH<sub>3</sub>mol), further partitioned into the 2 main steps involving NH<sub>3</sub> adsorption/desorption: 3N\_NH<sub>3</sub>\_H  $\leftrightarrow$  3N\_H; 2N NH<sub>3</sub> H  $\leftrightarrow$  2N H.

#### 6. Comparison with previous literature

#### 6.1 Comparison with experiment

In the above discussions we compared our predicted TOF with the single crystal experimental values (Somorjai), finding excellent agreement.

Another comparison in with experiment is to Temperature Programmed Desorption (TPD) in which a monolayer (ML) of NH<sub>3</sub> at low temperature is heated at a uniform rate dT/dt and the products measured with a mass spectrometer. Here the temperature for the peak desorption rate, TPD peak, combined with dT/dt in the Redhead equation gives a crude estimate of the binding energy. Our predicted binding energies are consistent with available experimental literature. Thus, Figure 9 of Strongin et al<sup>13</sup> reports TPD experiments on Fe(111) with a very broad desorption peak centered at about 300 °K for a heating rate of 8 °K/sec, which corresponds to an activation barrier for desorption of 0.82 eV. This compares well with the values of 0.89 to 1.00 eV we calculate for the NH<sub>3</sub> desorption barrier.

Our results are also consistent with experiments conducted on polycrystalline Fe wires by Ertl and Huber  $^{46-47}$  At T = 673 °K our barriers for NHx dehydrogenation mechanisms (NHx  $\rightarrow$ NHx-1 + H) range from 0.53 to 0.63 eV which are lower than the barrier for NH<sub>3</sub> desorption (0.76 to 0.87 eV) which in turn are lower than the barrier for both N<sub>2</sub> dissociation (1.27 eV) and for N-adatom recombination (2.04 eV). Our predicted NH<sub>3</sub> sticking coefficient at 673 °K and a NH<sub>3</sub> pressure of 5 x 10<sup>-6</sup> torr is about 5 times larger than the N-adatom recombination rate (the kinetic constant corresponding to our 2.04 eV barrier is 0.03 sec-1), which should be contrasted with a near equality at T > 640 °K in previous study. However, the Ertl experiments were on Fe polycrystalline wires in which the presence of (100) and (110) facets may increase the ratio of N-adatom recombination over the NH<sub>3</sub> dissociative sticking rate. Indeed the experimentally derived value of 45±5 kcal/mol for the activation free energy of N-adatom recombination in literature. Indeed the experimentally derived value of 45±5 kcal/mol for the activation free energy of N-adatom recombination in literature. Indeed the experimentally derived value of 45±6 kcal/mol for the activation free energy of N-adatom recombination in literature. Indeed the experimentally derived value of 45±6 kcal/mol for the activation free energy of N-adatom recombination in literature.

Another TPD experiment on industrial catalysts <sup>49</sup> observed a  $N_2$  desorption peak at 644 °K, with an estimated N-adatom recombination rate of 1-2 x  $10^9$  x exp(- 146 kJ/mol/RT). This rate corresponds to an apparent free energy barrier at 644 °K of  $\Delta G = 2.00$  to 2.04 eV, which is very close to our predicted barrier of 2.04 eV at T = 673 °K, especially considering that the industrial catalyst is K-promoted and hence is expected to exhibit a smaller barrier. In the same work, the N-adatom coverage under Haber-Bosch reaction conditions was estimated to be 0.4 of the maximum N-adatom coverage under  $N_2+3H_2$  conditions, a value close to our predicted value of 0.5 for the 2N.xH configurations predominant on the (2x2) unit cell.

#### **6.2** Comparison with theory

#### 6.2a Nørskov studies

The pioneering QM study for Haber Bosch chemistry on Fe(111) was reported in 1999 by Nørskov et al<sup>50</sup>. They investigated in detail several states with  $N_2$  molecularly adsorbed and/or dissociated and considered simplified pathways for dissociation. Their qualitative picture considers  $N_2$  dissociation as the RDS, which we have shown to be correct with our detailed reaction kinetics based on QM free energies and reaction barriers. However, there are significant quantitative differences because **we calculated reaction barriers**, **whereas they examined only stable species.** Instead they made estimates using the Ulitsky-Elber approximation to find minimum energy paths. In contrast we used fully relaxed NEB techniques. In addition Nørskov et.al<sup>50</sup> used the rev-PBE xc-functional without dispersion corrections (dispersion corrections increase adsorption energies by  $\sim 10$  %). They used a slab with 7 layers apparently relaxed without constraints (compared to 6 in ours), but with a very small (1x1) unit cell or sometimes sqrt(3) x sqrt(3), rather than the 2x2 used in our studies. Also entropic corrections to free energies were not included in their calculations.

Nørskov et al.<sup>50</sup> considered dissociatively chemisorbed binding energies for  $N_2$  and described several states labeled as  $\alpha$ ,  $\alpha$ ',  $\delta$ ,  $\beta$ ,  $\gamma$ . We used PBE-D3 to calculate the binding energies for these states with the results in table S1 of the SI. We found much stronger binding for both horizontally and vertically chemisorbed  $N_2$  states  $\alpha$ ,  $\alpha$ ',  $\delta$ ,  $\beta$ , due to a better description of dispersion correction. We also found that  $N_2$  adsorption states have a very sensitive adsorption energy dependence with respect to the surface's N atom coverage. State  $\alpha$  is better in electronic energy of  $\sim$ 0.2 eV than  $\alpha$ ' on bare surface, however, with 2N present on the surface, the result is reversed and state  $\alpha$ ' is better in energy than  $\alpha$  by  $\sim$ 0.2 eV. We arrived at similar result for dissociated N atom.

However, despite some differences in the specific numbers, we confirmed the Nørskov overall pathway for dissociate chemisorption of N2. Triple-bonded N<sub>2</sub> adsorbed on first layer ( $\gamma$ ) => triple-bonded N<sub>2</sub> adsorbed on second layer ( $\delta$ ) => double-bonded N<sub>2</sub> bonded to a bridging site ( $\alpha$ ) => single-bonded N<sub>2</sub> bonded to a three-fold site ( $\alpha$ ') => dissociated N atoms ( $\beta$ ). The biggest difference is that our calculations have two other N already bonded to 4-fold sites, which changes the overall energetics and barriers.

### 6.2b Lin studies

A more recent QM study on adsorption and dissociation of  $NH_3$  molecule on Fe(111) by Lin et.al<sup>41</sup> provided comprehensive adsorption energy data for several species, including N, H, NH, NH<sub>2</sub>, and NH<sub>3</sub>. They used a revised Perdew-Burke-Ernzerhof (GGA-rPBE) exchange correlation functional, without dispersion corrections. They used a (3x3) unit cell, compared to our (2x2) cell. They calculated QM barriers but did not calculate the activation free energies for reactions. The influence of coverage on adsorption energy was not considered, nor were entropic corrections to free energies calculated. Their results in kcal/mol, are converted to eV in table S1 of the SI. This study by Lin et.al<sup>41</sup> leads to better agreement for binding of N, NH, NH<sub>2</sub> (after correcting for the difference in surface coverage). It is expected that their adsorption energies would be  $\sim 30$  % too weak due to the lack of D3 dispersion corrections.

#### 7. Summary and conclusions

We report here the first comprehensive study of the mechanisms underlying NH<sub>3</sub> synthesis by Fe based catalysts including the reaction barriers for all 17 steps involved and considering both Langmuir-Hinshelwood (surface species reacting with surface species) and Eley-Rideal (gas phase species reacting with surface species) processes.

The QM was at the level of PBE including D3 London dispersion (van der Waals attraction) corrections that was previously applied successfully to the oxygen reduction reaction ( $O_2$  + protons  $\rightarrow$   $H_2O$ ) on Pt and the  $CO_2$  and CO reduction reactions on Cu surfaces. <sup>17–21,23–25</sup>

Correcting the DFT for phonons to get free energies at experimental reaction conditions, and carrying out extensive kinetic Monte Carlo calculations to obtain the steady state populations at the conditions of the single crystal experiments (673°K, 15 atm  $H_2$ , 5 atm  $N_2$ , and 1.5 torr  $NH_3$ ) leads to a **predicted TOF=17.7 sec-1** per 2x2 Fe(111) surface site, in excellent agreement with the single crystal **experimental rate of TOF= 9.7 sec-1 per site**. This suggests that the accuracy of PBE-D3 for the critical barriers may be of the order of 0.04 eV.

This overall agreement in the predicted TOF with experiment indicates that the QM combined with kMC provides a new detailed understanding of the reaction mechanism underlying NH<sub>3</sub> synthesis. This should provide a basis for considering how to modify the catalyst to improved performance. In particular, the changes in the spins and charges in the TS provides hints, as discussed above of considering alloying with metals having localized spins, such as Cr, Mn, Co, or Ni, or with metals not expected to have localized spins such as Ru or Os.

Despite the excellent agreement, we should caution that the experiments might have been affected by impurities such as O that might affect the rates. Also the QM calculations using the phonons to predict free energies at reaction conditions might miss dynamical and anharmonic effects that would require quantum based reaction dynamics. Moreover, the limitation to a 2x2 unit cell may eliminate some reactions that could require larger unit cells. In addition, replacing the PBE level of DFT might be important for a system such as this with localized spins and the origin of the D3 corrections for London dispersion is suspect.

#### Associated content

Supporting Information. Energy landscape and kinetic Monte Carlo results for Haber Bosch reaction at PBE level; transition state geometry and potential energy curves for key processes; pictorial illustration of "linear" and "zig-zag" configurations; detailed instructions on the use of the excel file with full numerical data (PDF). Numerical data of electronic energies and free energies for surface configurations using PBE-D3 and PBE xc-functionals at 673 °K and 730 °K, thermodynamic data for gas-phase molecules, and reaction energy barriers for key processes, reported in a 4-sheet excel file (XLSX).

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#### References

- (1) Erisman, J. W.; Sutton, M. A.; Galloway, J.; Klimont, Z.; Winiwarter, W. *Nat. Geosci.* **2008**, *1*, 636–639.
- (2) Schlögl, R. Angew. Chem. Int. Ed. 2003, 42, 2004–2008.
- (3) Mittasch, A.; Frankenburg, W. Adv. Catal. 1950, 2, 81–104.
- (4) Hara, M.; Kitano, M.; Hosono, H. ACS Catal. 2017, 7, 2313–2324.
- (5) Nielsen, A. Ammonia: Catalysis and Manufacture; Springer: Heidelberg, 1995.
- (6) Hellman, A.; Honkala, K.; Remediakis, I. N.; Logadóttir, Á.; Carlsson, A.; Dahl, S.; Christensen, C. H.; Nørskov, J. K. *Surf. Sci.* **2009**, *603*, 1731–1739.
- (7) Kitano, M.; Kanbara, S.; Inoue, Y.; Kuganathan, N.; Sushko, P. V.; Yokoyama, T.; Hara, M.; Hosono, H. *Nat. Commun.* **2015**, *6*.
- (8) Rossetti, I.; Pernicone, N.; Forni, L. Appl. Catal. Gen. 2001, 208, 271–278.
- (9) Akinfieva, T. A. Gig. Tr. Prof. Zabol. **1981**, No. 1, 46–47.
- (10) Jennings, J. R., Ed. Catalytic Ammonia Synthesis; Plenum: New York, 2013.
- (11) Norton P. R. *The Chemical Physics of Solid Surfaces and Heterogeneous Catalysis*; King, D. A., Woodruff, D. P., Eds.; Elsevier: Amsterdam, 1982; Vol. 4.
- (12) Ertl, G.; Knoezinger, H. *Handbook of Heterogeneous Catalysis*, 5 Volume Set; Wiley-VCH: Weinheim, Germany, 2008
- (13) Somorjai, G. A.; Materer, N. Top. Catal. 1994, 1, 215–231.
- (14) Strongin, D. R.; Carrazza, J.; Bare, S. R.; Somorjai, G. A. *J. Catal.* **1987**, *103*, 213–215.
- (15) Johnson, E. R.; Becke, A. D. J. Chem. Phys. 2006, 124, 174104.
- (16) Grimme, S.; Antony, J.; Ehrlich, S.; Krieg, H. J. Chem. Phys. **2010**, 132, 154104.
- (17) Cheng, T.; Goddard, W. A.; An, Q.; Xiao, H.; Merinov, B.; Morozov, S. *Phys. Chem. Chem. Phys.* **2017**, *19*, 2666–2673.
- (18) Cheng, T.; Xiao, H.; Goddard, W. A. Proc. Natl. Acad. Sci. U. S. A. 2017, 114, 1795–1800.
- (19) Cheng, T.; Xiao, H.; Goddard, W. A. J. Phys. Chem. Lett. 2015, 6, 4767–4773.
- (20) Cheng, T.; Xiao, H.; Goddard, W. A. J. Am. Chem. Soc. 2016, 138, 13802–13805.
- (21) Cheng, T.; Xiao, H.; Goddard, W. A. J. Am. Chem. Soc. 2017, 139, 11642–11645.
- (22) Ping, Y.; Nielsen, R. J.; Goddard, W. A. J. Am. Chem. Soc. 2017, 139, 149–155.
- (23) Xiao, H.; Cheng, T.; Goddard, W. A. J. Am. Chem. Soc. **2017**, 139, 130–136.
- (24) Xiao, H.; Cheng, T.; Goddard, W. A.; Sundararaman, R. J. Am. Chem. Soc. 2016, 138, 483–486.
- (25) Xiao, H.; Goddard, W. A.; Cheng, T.; Liu, Y. Proc. Natl. Acad. Sci. U. S. A. 2017, 114, 6685–6688.
- (26) Kresse, G.; Furthmüller, J. Phys. Rev. B 1996, 54, 11169–11186.
- (27) Perdew, J. P.; Burke, K.; Ernzerhof, M. Phys. Rev. Lett. 1996, 77, 3865–3868.
- (28) Perdew, J. P.; Burke, K.; Ernzerhof, M. Phys. Rev. Lett.. 1997, 78, 1396–1396.
- (29) Stephens, P. J.; Devlin, F. J.; Chabalowski, Cf.; Frisch, M. J. J. Phys. Chem. 1994, 98, 11623–11627.
- (30) Malcolm, W., Chase, J., Eds.; NIST-JANAF Thermochemical Tables, 4th ed. *J. Phys. Chem. Ref. Data* **1998.**
- (31) Kittel, C. *Introduction to Solid State Physics*; Wiley: New York, 1996.
- (32) McClurg, R. B.; Flagan, R. C.; Goddard III, W. A. J. Chem. Phys. 1997, 106, 6675–6680.
- (33) Campbell, C. T.; Sprowl, L. H.; Árnadóttir, L. J. Phys. Chem. C 2016, 120, 10283–10297.
- (34) Redondo, A.; Zeiri, Y.; Goddard III, W. A. *Phys. Rev. Lett.* **1982**, *49*, 1847.
- (35) Henkelman, G.; Uberuaga, B. P.; Jónsson, H. J. Chem. Phys. 2000, 113, 9901–9904.
- (36) Henkelman, G.; Jónsson, H. J. Chem. Phys. 1999, 111, 7010–7022.
- (37) Heyden, A.; Bell, A. T.; Keil, F. J. J. Chem. Phys. 2005, 123, 224101(.
- (38) Grunze, M.; Bozso, F.; Ertl, G.; Weiss, M. Appl. Surf. Sci. 1978, 1, 241–265.
- (39) Hsiao, M.-K.; Su, C.-H.; Liu, C.-Y.; Chen, H.-L. *Phys. Chem. Chem. Phys.* **2015**, *17*, 30598–30605.

- (40) Satoh, S.; Fujimoto, H.; Kobayashi, H. J. Phys. Chem. B **2006**, 110, 4846–4852.
- (41) Lin, R.-J.; Li, F.-Y.; Chen, H.-L. J. Phys. Chem. C 2010, 115, 521–528.
- (42) Kua, J.; Goddard, W. A. J. Phys. Chem. B 1998, 102, 9481–9491.
- (43) Kua, J.; Goddard, W. A. J. Phys. Chem. B **1998**, 102, 9492–9500.
- (44) Kua, J.; Faglioni, F.; Goddard, W. A. J. Am. Chem. Soc. 2000, 122, 2309–2321.
- (45) Kua, J.; Goddard, W. A. J. Am. Chem. Soc. 1999, 121, 10928–10941.
- (46) Ertl, G.; Huber, M. J. Catal. **1980**, *61*, 537–539.
- (47) Ertl, G.; Huber, M.; Lee, S. B.; Paal, Z.; Weiss, M. Appl. Surf. Sci. 1981, 8, 373–386.
- (48) Bozso, F.; Ertl, G.; Grunze, M.; Weiss, M. J. Catal. 1977, 49, 18–41.
- (49) Muhler, M.; Rosowski, F.; Ertl, G. Catal. Lett. **1994**, 24, 317–331.
- (50) Mortensen, J. J.; Hansen, L. B.; Hammer, B.; Nørskov, J. K. J. Catal. 1999, 182, 479–488.

## Table of Contents figure

