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Role of ions in pool boiling heat transfer of pure and silica nanofluids

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Heat transfer in silica nanofluids at different acidity and base is measured for various ionic concentrations in a pool boiling experiment. Nanosilica suspension increases the critical heat flux 3 times compared to conventional fluids. The 10-nm particles possess a thicker double diffuse layer compared to 20-nm particles. The catalytic properties of nanofluids decrease in the presence of salts, allowing the particles to cluster and minimize the potential increase in heat transfer. Nanofluids in a strong electrolyte, i.e., in high ionic concentration, allow a higher critical heat flux than in buffer solutions because of the difference in surface area. The formation and surface structure of the deposition affect the thermal properties of the liquid. © 2005 American Institute of Physics.

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Several investigators¹⁻³ have reported a significant enhancement in critical heat flux when nanoparticles of sizes less than 50 nm are dispersed in pure water in a pool boiling environment. Such fluids with nanoparticle suspensions are called nanofluids. The anomalous thermal properties and the suspension characteristics make nanofluids promising for nanotechnology based heat transfer applications such as electronic cooling and heat exchangers.

Even at very low concentrations, these nanofluids possess high thermal conductivity. In the presence of nanoparticles, particle-particle and particle-molecule interactions play a major role in increasing the thermal conductivity of the nanofluids which enhances the heat transfer. A few possible factors to enhance the thermal conductivity are discussed in published literature, including the Brownian motion of nanoparticles, ordered arrangement of liquid molecules in the vicinity of nanoparticles, ballistic heat transfer mode in nanoparticles, and clustering of nanoparticles.⁴⁻⁶

In this letter, we show that the heat transfer characteristics are even more pronounced when the pool boiling experiment is performed in a strong electrolyte. The objective of this work is to systematically study the effect of the negatively charged silica nanoparticle suspension in boiling conditions in water for different particle size, particle concentration, and under various pH conditions and ionic concentration.

The experiments were done using a suspended nichrome (NiCr) wire immersed in water with varying pH. The wire of length 46 mm and 0.32 mm in diameter was horizontally suspended in a pool of water in a glass beaker and tightly attached to a copper lead wire, and then soldered. The data for the boiling curve was obtained by slowly increasing the current and recording the voltage. Depending on the chemical composition of the liquid, the wire could suddenly break or glow due to a jump in voltage. The boiling curve was generated by using a calibration curve from a known temperature-resistance relationship for NiCr (Ref. 7) and obtaining the heat flux from

$$q = I^2 R_w / \pi DL, \quad (1)$$

where q is the heat flux, R_w is the wire resistance, D is the wire diameter, and L is the wire length. The experiments were conducted with 250 ml of water completely immersing the wire. The boiling process evaporated about 5 ml of water during the experiment, i.e., <2%, which had no significant effect on the temperature or heat flux measurements. Silicon (IV) oxide is a commercial product of Alfa Aesar, and was acquired in a colloidal suspension. The weight percentage of 10 and 20 nm is 15% and 40%, respectively. Nanofluids used in the pool boiling experiment were prepared by stirring nanosilica in different acidity and salt content base liquids for about 30 min. Experiments were run after a good dispersion of nanoparticles was achieved.

The uncertainty in the resistance measurements from the multimeter is 0.459%. The soldering of the wires at both ends adds uncertainty to the length of the whole wire and attributes to the largest uncertainty in the heat flux, which is 5.8%. The uncertainty in the T - R curve fit for nichrome is estimated to be 30 °C.

Since particle suspensions are stable at different pH solutions depending on the particle characteristics, our initial investigation focused on the effect of pH in pure water. Pool boiling is a mode of heat transfer that occurs on a surface submerged in a pool of initially quiescent fluid with a change in phase from liquid to vapor. Referring to the boiling curve of water at different pH, photographs of pH7 are provided in Fig. 1 to illustrate the physical mechanisms taking place at various heat flux. The different pH solutions were prepared using either HCl or NaOH so that the initial ionic concentration of the H⁺ or the OH⁻ ions can be calculated. Initially, as the current is passed through the wire, the heat transfer mode changes from natural convection to the saturated boiling regime where bubbles begin to coalesce. As the heat flux is further raised beyond what is known as the critical heat flux (CHF), a sudden large increase in temperature occurs. With the wire being blanketed by mostly vapor, there is again a linear rise of wire temperature with an increase of heat flux, until a point is reached when the wire breaks. Near CHF, the heating surface is covered by rising vapor columns in the form of jets with countercurrent liquid jets flowing downward as shown in Fig. 1. Based on the fact that CHF is limited by the removal rate of bubbles which carry away the

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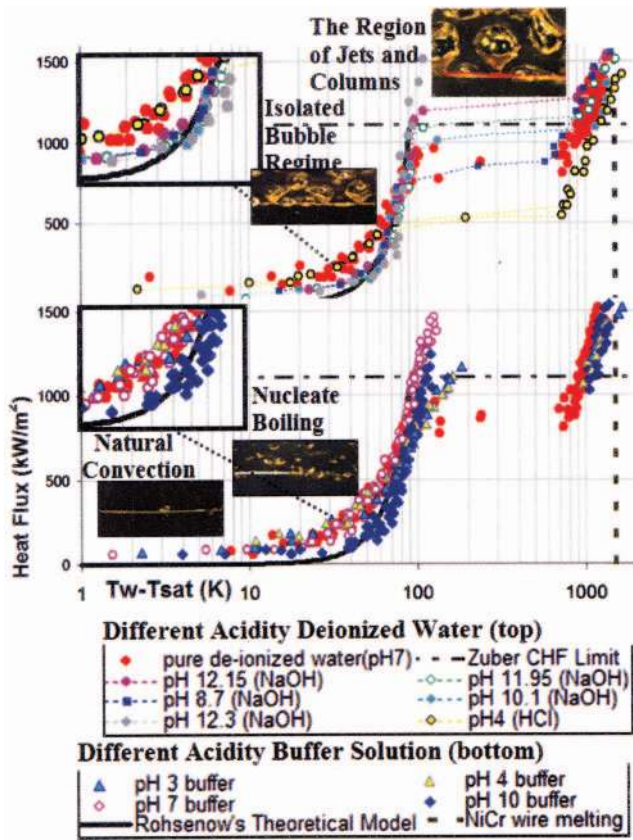


FIG. 1. (Color) Heat flux vs wire superheat at different pH. The photographs at different heat flux show different boiling regimes.

heat in the form of heat of vaporization, Zuber⁸ obtained CHF for pure water as

$$q''_{max} = 0.131 h_{fg} \rho_v^{1/2} (g \sigma \Delta \rho)^{1/4}, \quad (2)$$

where h_{fg} , σ , and $\Delta \rho$ are the heat of vaporization, surface tension, and the density difference between the phases, respectively. The data obtained in this paper compare well with the CHF given in Eq. (2) as well as with the saturated boiling regime preceding CHF as given by Rohsenow's⁹ well-established correlation

$$q_{flux\ Ros}(\Delta T) := \mu_f h_{fg} \left[\frac{\sigma}{g_1(\Delta \rho)} \right]^{-0.5} \left(\frac{1}{C_{sf}} \right)^{1/0.33} \times Pr^{-1.7/0.33} \left[\frac{c_{pl}(\Delta T)}{h_{fg}} \right]^{1/0.33}, \quad (3)$$

where μ_f is the fluid viscosity, ΔT is the temperature superheat, Pr is the Prandtl number, and C_{sf} is taken to be 0.045.

As seen in Fig. 1, for different pH, the heat flux where the horizontal curve appears (this happens due to a sudden jump in the wire resistance) decreases with increasing acidity. This is the point where the wire begins to glow. The nichrome wire dipped in an acidic solution begins to melt at a much earlier stage compared to a basic solution. Metal glowing usually occurs at high temperatures (above 800 °C). The flow of electrons from the positive electrode (anode) in the system to the negative one (cathode) seems to be vital in determining the vapor phase behavior during the process of electrolysis. The positively charged hydrogen ion goes to the anode which has a negatively charged surface, takes an electron (oxidation), and becomes a neutrally charged hydrogen atom (H). Hydrogen atoms combine to form a hydrogen gas

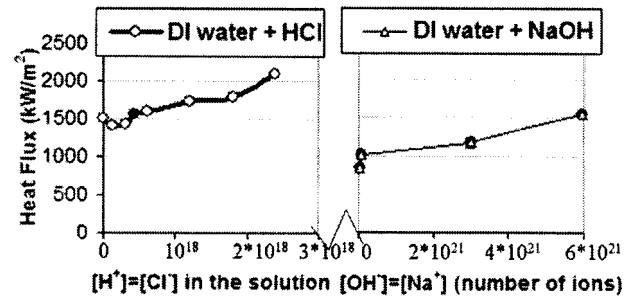


FIG. 2. CHF as a function of the number of dissociated ions (a) H⁺ and Cl⁻ and (b) Na⁺ and OH⁻ in deionized water.

(H₂) which bubbles up from the anode and the wire. A similar phenomenon was seen as in Ref. 10. When the amount of HCl is increased, no jump in temperature is noticed, and the CHF value starts to increase; however, the wire breaks before glowing.

The number of ions was calculated by multiplying the number of moles (mass/molarity) by Avogadro number. Since the anode is the positive lead wire and its surface is negatively charged by electrons, there is a point at which oxidation and formation of hydrogen gas is no longer possible due to a high concentration of positive ions, which leads to a depletion of e⁻. In Fig. 2, this transition appears when the number of ions exceeds 5 × 10¹⁷. Beyond this point, the H⁺ ions remain free and carry part of the applied current, bypassing the wire and giving it “longer life,” hence, the wire is able to carry more current, increasing CHF.

In the case of increasing NaOH base [Fig. 2(b)], cations give off their excess electrons (the process of reduction), and when they become neutral, oxygen gas O₂ is formed. Thus, the hydrogen and oxygen gases determine the different stages of the boiling curve and the extent of the glowing or the absence of it. Additional insight can be obtained by conducting the heat transfer experiments using buffer solutions. In the case of a weak electrolyte, pure buffer solutions at different pH exhibit a jump in resistance and subsequent glowing at all pH except 7.0 (Fig. 1) Buffers are weak electrolytes and give off free ions at a very controlled rate, therefore, it is reasonable to expect wire melting when a temperature of ~800 °C is reached. That means the sudden jump in temperature always occurs at about 1100 kW/m², which is the Zuber CHF limit for pure solutions. In the case of the pH7 buffer solution, there is a balance of dissociated positive and negative ions and the wire does not glow. The boiling characteristics are different for pH7 deionized (DI) water in that the dissociated oxygen atoms allow the wire to glow.

Silica nanofluid is basically colloidal silica, i.e., fine particles dispersed in water, a state between bulk and molecular dispersed systems. The surface of silicon dioxide is negatively charged by the hydroxyl groups which occupy the space between the oxygen atoms during its manufacturing to achieve mutual repulsion and stability.

It has been already established by Vassallo *et al.*³ that in silica nanosuspensions, the critical heat flux can be increased by over 100%. In Figs. 3 and 4, it is shown that it can be improved to 300% depending on the particle size and the pH level.

It is important to investigate the process of polymerization (Fig. 3) and dispersion (Fig. 4) for the heat transfer analysis because polymerization (as in the buffer solution in Fig. 3) leads to lower surface area to volume ratio and, con-

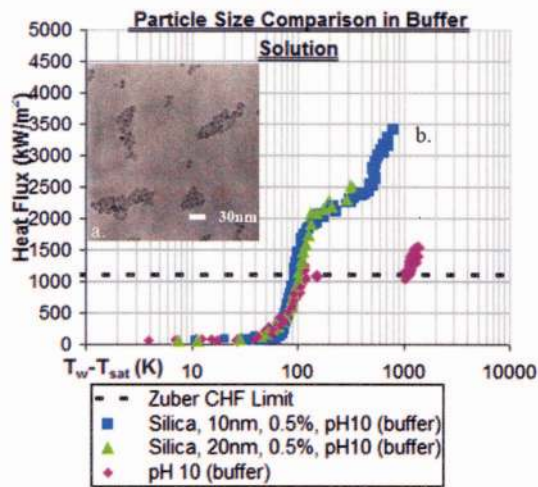


FIG. 3. (Color) (a) Agglomeration characteristics as seen in TEM of silica in buffer pH 10. (b) Pool boiling CHF for 10 and 20 nm particles in pH10 solution.

sequently, to lower heat flux. According to the general theory of polymerization,¹¹ in the presence of salts (pH7-10) aggregation and gelling occur due to a decrease in mutual repulsion. This effect is noticed in the TEM image in Fig. 3. In the absence of salts for pH7-10, as shown in the TEM image in Fig. 4, the repulsive barriers are strong enough to guarantee particle growth without aggregation.

The double diffuse layer surrounding the particle is calculated using a theoretical model by Gouy–Chapman¹² at 25 °C as follows:

$$k = 2.32 \times 10^9 (\sum c_i z_i^2)^{1/2}, \quad (4)$$

where $1/k$ is the double-layer thickness, c_i is the ion concentration, and z_i determines the extent of counterion charge in the solution. The final particle sizes are calculated to be 22 and 27 nm, for 10 and 20 nm respectively, which agrees with experimental results.

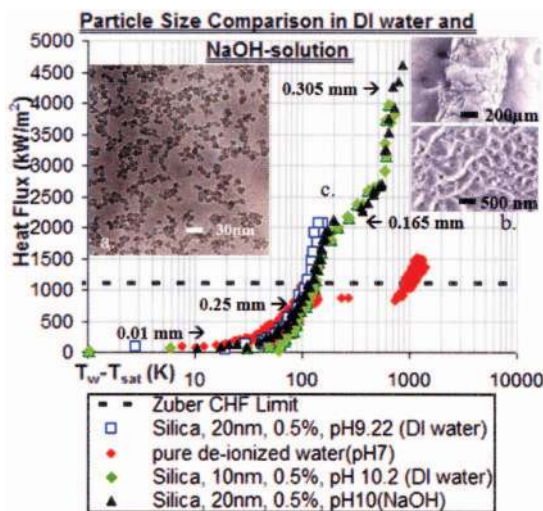


FIG. 4. (Color) (a) Colloidal behavior of silica in deionized water as seen in TEM; (b) TEM and SEM pictures of the Nichrome wire after deposition of silica; (c) Pool boiling CHF for 10 and 20 nm particles in deionized water with no additives and NaOH. Different levels of deposition on the wire are shown in mm at different stages of boiling.

Two characteristics of silica nanoparticles are explored: one is the role of the salts and the other is the effect of particle size on critical heat flux. In the presence of salts (such as in the buffer solution), due to van der Waals attractive forces, silica tends to form polymers, i.e., a chain of silicate layers, representing clusters and films. Since buffer solutions are weak electrolytes, they do dissociate at a very low rate when current is passed. Even so, they can release some sodium and potassium ions which could bond to the silica clusters and act as ion conductors. Thus, they form a solid hybrid polymer, with Na⁺ ion being more probable to bond because of its smaller size. Both 10 and 20 nm particles become neutrally charged. Although CHF is still significantly increased compared to pure fluids, the clustered particles result in a detrimental performance compared to silica suspended in deionized water, as noted in Fig. 3.

In Fig. 4, with no salts present (i.e., SiO₂+deionized water and NaOH solution), there are no significant agglomerations. The electrolytes present in the solution are responsible for carrying part of the applied current. The charged silica particle in suspension experiences “hydration” of the surface of the particles, i.e., a layer of water molecules are hydrogen bonded to SiOH groups. The corresponding zeta potential values for the two particle sizes are in the neighborhood of –20 mV, as shown in another study, hence negative charge barriers exist. The 10- and 20-nm particles grow to 19 and 22 nm, respectively, in DI water.

The CHF for 20 nm in a strong electrolyte solution (NaOH) goes up to 4600 kW/m² (Fig. 4) with an increase in the size of the particle which is negatively charged. Having an overall negative charge and a thin double layer, particles bond to a limited amount of free ions, leaving the majority in the solution. Therefore, it is reasonable to expect high potential transport through the liquid and diversion of a significant amount of current from the NiCr wire, giving it extended life. The double diffuse layer on the particle gets distorted and attracted to the wire, resulting in significant deposition. This surface porosity is also responsible for increasing the heat transfer. Heat transfer results were obtained for 0.2% with no additives. An increase of 10–15 % in CHF was observed for 0.5% solution compared to 0.2%.

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¹J. A. Eastman, S. U. S. Choi, S. Li, W. Yu, and L. J. Thompson, *Appl. Phys. Lett.* **78**, 718 (2001).

²S. P. Jang and S. U. S. Choi, *Appl. Phys. Lett.* **84**, 4316 (2004).

³P. Vassallo, R. Kumar, and S. W. D’Amico, *Int. J. Heat Mass Transfer* **47**, 407 (2004).

⁴P. Bhattacharya, S. K. Saha, A. Yadav, P. E. Phelan, and R. S. Prasher, *J. Appl. Phys.* **95**, 6492 (2004).

⁵P. Keblinski, S. R. Phillpot, S. U. S. Choi, and J. A. Eastman, *Int. J. Heat Mass Transfer* **45**, 855 (2002).

⁶N. R. Jana, Y. Chen, and X. Peng, *Chem. Mater.* **16**, 3931 (2004).

⁷www.resistancewire.com.

⁸N. Zuber, *Int. J. Heat Mass Transfer* **6**, 53 (1963).

⁹W. M. Rohsenow, *Trans. ASME, Ser. C: J. Heat Transfer* **84**, 969 (1962).

¹⁰http://www.rrc.state.tx.us/divisions/afred/education/lessonpdf/3_3electrolysis.pdf.

¹¹R. K. Iler, *Surface and Colloid Science*, edited by E. Matijevic (Wiley, New York, 1973), Vol. 6.

¹²M. Elimelech, J. Gregory, X. Jia, and R. A. Williams, *Particle Deposition and Aggregation* (Butterworth and Heinemann, Wooburn, MA, 1995).