

**Small-Scale Heterogeneity in Sediments: Experimental and  
Modelling Investigations**

**Anthony Stockdale MChem**

**August 2008**

**This Thesis is Submitted for the Degree of Doctor of  
Philosophy.**

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## List of papers

- I. Stockdale, A., Davison, W., Zhang, H., (Peer reviewed and revisions submitted). Micro-scale biogeochemical heterogeneity in sediments: A review of available techniques and observed evidence. *Earth-Science Reviews*.
- II. Stockdale, A., Davison, W., Zhang, H., 2008. High-resolution two-dimensional quantitative analysis of phosphorus, vanadium and arsenic, and qualitative analysis of sulfide, in a freshwater sediment. *Environmental Chemistry*, 5, 143-149. DOI: 10.1071/EN07096
- III. Stockdale, A., Davison, W., Zhang, H. Quantifying cobalt fractions associated with iron and manganese (oxyhydr)oxides in marine sediment using DGT.
- IV. Sochaczewski, Ł., Stockdale, A., Davison, W., Tych, W., Zhang, H., 2008. A three-dimensional reactive transport model for sediments, incorporating microniches. *Environmental Chemistry*, 5, 218-225. DOI:10.1071/EN08006
- V. Stockdale, A., Davison, W., Zhang, H. Sulphide evolution from faecal pellets and other microniches within sub oxic surface sediment: The effects on the geochemistry of iron and trace elements. Submitted to *Geochimica et Cosmochimica Acta*.

# **Small-Scale Heterogeneity in Sediments: Experimental and Modelling Investigations**

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## **Abstract**

This thesis consists of several studies relating to small-scale heterogeneity in sediments. The principal aim was to further our understanding of processes occurring at microniches. The individual studies consist of: 1) a critical review of previous studies of microniches that used probes with high spatial resolution and modelling approaches; 2) an experimental study of analysis of oxyanions in sediment at high resolution that applied a newly developed preparation method for a combined AgI/FeOOH binding phase, to investigating processes occurring at a sulphidic microniche within a freshwater sediment; 3) analysis of the relationship between trace metal (cobalt) and iron and manganese in a marine sediment using DGT, although this is not directly related to microniches, these data are useful in modelling the release of microniche trace metal from authigenic oxides; 4) the development and application of a three-dimensional diagenetic model to investigate conceptually the geochemical behaviour of microniches under different conditions, and to interpret modelled observations in terms of data from the literature and known trace element geochemistry. The key results/conclusions from both the laboratory and modelling studies are: 1) for a freshwater sediment, depletions in anions (of P, V, As) at a microniche of elevated sulphide were observed and the behaviour of phosphate at this niche was attributed to uptake associated with elevated activity of sulphate reducing bacteria; 2) modelled scenarios, with varying microniche properties, were shown to be relevant to experimental observations reported in the literature. The preferential deposition of FeS at the edge of microniches (with lifetimes of 2.5-5 days), forming 'crustal' deposits was demonstrated. The modelled data indicated that microniches may be significant in terms of the formation of some trace element sulphides. This thesis also contains an assessment of the significance of microniche processes and a discussion of priorities for future work.

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## **1 Introduction**

Thesis regulations state that the introductory chapter should cover ‘the whole of the background and context of the research.’ However, this thesis includes, as an independent chapter, a substantial critical literature review covering a large part of the background and context to this work (Paper I). In order to avoid unnecessary repetition, I have written the introduction so that it complements, rather than repeats, Paper I. The introduction includes those subjects that are absent from the review chapter. These topics are, a description of the characteristics of microniches and their location and a review of the modelling of microniches. Additional to the thesis requirements, an assessment of the wider significance of microniche processes is included, following the thesis conclusions.

### **1.1 Definitions of microenvironment and microniche**

Despite the fact that these terms are defined elsewhere in the thesis, it is important to define these from the outset. I define a microenvironment as a localized location within the 3-dimensional sediment matrix where the geochemistry is significantly different from the average for that depth. This may apply to a gas bubble, a burrow or feeding tube from a benthic organism, or a particle of reactive organic matter or other component that has biogeochemical reaction rates that are higher than the surrounding environment. The term microniche is reserved for microenvironments associated with localized reactive organic matter.

### **1.2 Description of thesis structure**

This thesis is composed of five papers related to trace metal and microniche geochemistry. A comprehensive critical literature review (Paper I), practical studies

(Papers II and III) and modelling studies (Papers IV and V) form the basis of this thesis. Descriptions of these papers are included in Section 3.

### 1.3 The characteristics of microniches and their surroundings

#### 1.3.1 Environmental conditions around microniches

The physical and chemical characteristics of a sediment will have a large effect on determining the significance of microniches in different deposition environments. Table 1 shows different sediment and microniche characteristics and their potential effect on sulphide production or long-term effects. As is evident from the scenarios in Table 1, size, rate and porosity have the greatest influence on the potential for niche sulphide evolution in the  $O_2/NO_3^-$  zones. Below these zones these characteristics exert less influence. For microniches to have any long-term effect on sediment geochemistry, such as the formation of trace element-sulphides, the relative reversibility of such formation is an important consideration. For a niche where trace element-sulphides have formed, to have any long-term effect on element accumulation, the effects must not be fully reversible. Cyclical processes such as re-suspension may negate microniche effects by stimulating reoxidation of reduced species within niches. Overturn by biota may have the greatest influence on long-term effects, as these processes are important in introducing niches to various depths. Conversely, it may also relocate degraded niches to a zone where they are subject to re-oxidation (resulting in an oscillating redox condition). The degree of reversibility of formation reactions will influence the degree to which this reoxidation process affects different elements. For example, ZnS is oxidised more slowly than FeS (e.g. Sukola et al, 2005), and the oxidation of tetrathiomolybdate to molybdate has a slow rate (Erickson and Helz, 2000). Tetrathiomolybdate is also more readily scavenged by

Table 1. Effect of microniche and sediment characteristics on sulphide production and/or long-term effects. Scenarios assume sulphate availability within the sediment.

Characteristic	Scenario and effect
<b>Microniche</b>	
Size (volume)	The larger the niches the greater the likelihood of sulphide production within the oxic and suboxic zones.
Organic matter reaction rates	The greater the rate the greater likelihood of sulphide production within the oxic and suboxic zones. Increased rates will tend to increase peak sulphide concentrations and decrease the life-span of the niche. The contrast between the OM reduction rates in the 'bulk' sediment and the microniche will be important in assessing the significance of the niche.
Authigenic oxide concentration	Authigenic oxides will provide an alternative electron acceptor and sulphide will not evolve until these oxides are below their limiting concentration. Authigenic oxides may yield significantly higher trace metal evolution than OM alone. The relative ratios of oxides to available niche organic matter will control if sulphate reduction occurs within a niche.
Porosity	Within the oxygen and nitrate decomposition zones a high porosity niche will tend to require either a large size, high OM degradation rates or a combination of both factors, before sulphate is consumed. The lower the porosity of the niche the greater the sulphate production (providing the rate constant is equal). If the niche porosity is different from the bulk value, diffusion coefficients will differ within each zone and this may have an effect on the rates of resupply required to maintain e.g. iron sulphide precipitation.
Diffusional barriers (e.g. peritrophic membranes or hard parts)	The presence of a peritrophic membrane or hard parts (such as a shell) may restrict diffusion into or from the niche. This may lead to a more rapid consumption of oxygen and nitrate, resulting in sulphate reduction. All oxidants may be consumed.
<b>Sediment</b>	
Redox oscillations	Where sediment overturn via bioturbation is significant, redox oscillations may occur. Any formation of trace element-sulphides at microniches may be fully reversed by oxidation. Whilst bioturbation is important in the formation and distribution of microniches, the extent to which this process reverses the formation of sulphides also needs to be considered.
Microniche depth	When present in the sulphate reducing zone, microniches will produce zones of elevated sulphide regardless of their size. If they contain authigenic oxides, localised formation of metal sulphides may be expected. Sulphidic niches within the manganese and iron oxide reducing zones may result in net diffusion of trace elements into the niche with subsequent localised precipitation of sulphides.
Redox conditions above sediment-water interface	Where overlying water is permanently anoxic, bioturbation may be limited. Microniche sources will be limited to settling material, and sulphate reduction is likely to proceed in the water column before the particle settles. In such an environment, redox conditions of the niche will not significantly differ from the surroundings and the long-term effect of localised zones may be minimal.
Oxygen and nitrate penetration depth	Niches within the oxic and $\text{NO}_3^-$ zones require either a large size, high OM degradation rates, limited diffusion (membranes) or a combination of such processes, before sulphate is consumed. Niches within the oxygen and nitrate zones may have discrete layers oxidised by different oxidants. Niches present below the nitrate penetration depth will require physical movement into oxic and $\text{NO}_3^-$ zones for reverse redox processes to occur.
Organic matter concentration	In pristine or low OM environments, oxygen will tend to be present at much greater depths than more productive sediments. In such environments any formation of trace-element sulphides will tend to be reversible as, after the niche is consumed, oxygen is readily available.
Cyclical processes	Numerous processes may apply to this category. Some examples are given. Productivity and thus microniche creation may vary with seasons. In marine tidal regions, cyclical processes such as, tidal forcing (advection) and sediment re-suspension may occur. In lakes, seasonal variations in stratification may have effects on the sediment redox conditions.



FeS<sub>2</sub> and FeS than molybdate, further slowing its oxidation (Bostick et al, 2003; Helz et al, 2004).

### 1.3.2 Properties and types of microniches

As the term microniche applies to any discrete site of reactive OM, this can encompass material from a range of different sources. Microniches can be attributed to decaying organisms (observed using a pH optode; Zhu et al, 2006), algal aggregates (added to sediment to study sulphidic microniches; Widerlund and Davison, 2007) and faecal pellets (photographed after resin embedding and thin sectioning of an intact core; Watling, 1988). Within vegetated sediments such as mangroves, root systems can also generate microniches (e.g. Alongi et al, 2004). Such niches will have a range of different properties. For example: algal aggregates will tend to have a high porosity and a low concentration of authigenic oxides; faecal pellets may possess a peritrophic membrane, be more compact than the ambient sediment (lower porosity) and in some cases have been shown to contain a greater distribution of fine mineral grains than the ambient sediment (Watling, 1988), potentially affecting tortuosity.

Jørgensen (1977) estimated a detrital particle scale range of one  $\mu\text{m}$  to several millimetres or centimetres. Johnson (1974) examined the particle components of a surface sediment, including the consideration of particles that may be potential sources of food and thus may potentially produce microniches. Potential food sources such as diatoms, algae and pollen/spores had sizes as low as 5-85  $\mu\text{m}$ , with the upper size range being  $\sim 1000 \mu\text{m}$  for diatom and algal chains. Faecal pellets ranged from 10 to 650  $\mu\text{m}$  diameter, the upper value being consistent with observations by Watling (1998), who observed cylindrical pellets with widths of approximately 200  $\mu\text{m}$  and

lengths ~500  $\mu\text{m}$ . Taghon et al (1984) observed faecal pellets from a tube dwelling marine polychaete (*Amphicteis scaphobranchiata*) with an approximate average size of six mm length and one mm width. For cylindrical faecal pellets, width will be the most important factor for the formation of microniches as the shortest diffusive path will be the controlling factor for the resupply of oxidative solutes to the centre of the niche.

For small particles, such as those observed by Johnson (1974), to form as microniches, specific conditions must be met: 1) they must occur below the depth where oxygen and nitrate are both below the concentration at which, less energetically favourable oxidants are utilised to degrade organic matter, 2) where they contain authigenic oxides (e.g. in the case of some faecal pellets) the concentration of these components must be limited compared to the available OM, and/or, 3) they must be present in the sulphate reducing zone. Widerlund and Davison (2007) used diffusive gradients in thin-films (DGT) and computer imaging densitometry (CID) to quantify microniche sulphide distributions in a sulphidic freshwater lake sediment. A majority of the observed niches (~62%) were in the size range of 0.8 to 1.6 mm diameter, assuming spherical geometry (actual modal circularity value was 0.9). Microniches with a diameter above 2.5 mm accounted for ~12% of the total number of niches. Despite their lower numbers compared to smaller niches such microniches can occupy a relatively large volume (e.g. a 2.5 mm diameter niche has a volume equal to 125 individual 0.5 mm niches, assuming spherical geometry).

In terms of depth distributions, Johnson (1974) found that non-algal plant fragments showed no significant difference in abundance between the surface (sediment-water

interface) and two centimetres depth sediment samples. Faecal pellet abundance was approximately one third less at two cm depth, with the most significant difference being in the abundance of micro-algae, which at two cm depth was ~16% of the surface abundance. When all potential food particles are considered as a single group (this includes organic-mineral aggregates), there was no significant difference in abundance between the surface and two cm depth samples.

### 1.3.3 Settling particle microniches (faecal pellets and marine snow)

Settling particles within the water column such as faecal pellets and aggregates (termed marine snow), have been identified as localized zones of heterotrophic activity within the water column. When these particles settle on the sediment surface and are introduced into the sediment by the actions of biota they may form microniches. In situ metal deposition may occur within settling particles during passage through the water column, via precipitation of metals within extracellular capsules of bacteria. This may have an impact on water column chemistry (Cowen and Silver, 1984) and provide increased levels of reactive metals if such particles ultimately form sediment microniches. Settling particles are, by their nature, more readily identifiable than sedimentary microniches and have been studied directly, providing evidence for the existence of reducing micro-zones, and the processes occurring within them. The particle sizes observed for marine snow vary greatly from <100  $\mu\text{m}$  to several decimetres in diameter (Hamner et al, 1975). Marine snow can have microbial communities with densities several orders of magnitude higher than in surrounding seawater (Alldredge et al, 1986). Zooplankton faecal pellets have been measured to sink at rates between 15 and 950 m per day (Cherry et al, 1978; Alldredge, 1979 and references therein).

The chemistry of both marine snow and faecal pellets has been investigated using microelectrodes. A faecal pellet attached to a particle of marine snow was shown to have a significantly larger number of bacteria per volume than a marine snow particle, with the same pellet undergoing a pH decline of up to 0.91 units, and complete oxygen depletion during dark conditions (Alldredge and Cohen, 1987). This study also observed oxygen depletions of up to ~46%, and a lowering of pH by 0.22 units (compared to surrounding water), in a marine snow particle of 4.1 mm diameter. For a microniche within a marine sediment Ploug et al (1997) observed oxygen depletion, and a lowering of the pH from 8.2 in the ambient sediment to 7.4, in the centre of an anoxic aggregate (1.4 mm diameter). Sulphide was not analysed in these studies.

The potential for marine snow to produce sulphide within a seawater with a low oxygen concentration was examined by Shanks and Reeder (1993). Using tetrazolium salts, and both artificial and field samples of marine snow, they showed that sulphide evolves in aggregates of 0.7 to 2.0 mm in diameter. Within pieces of detritus (such as diatom frustules), elevated concentrations of sulphide were detected. This was attributed to a reduced flux of O<sub>2</sub> into these zones, caused by the physical structure of the detritus. Within sediments larger examples of microniches within shell structures have been observed within the oxic and suboxic zones (e.g. Emery and Rittenberg, 1952).

In comparison to sedimentary microniches, settling particle microenvironments will tend to have higher ambient surrounding concentrations of oxygen, and advective flow of fluid around the particle as it sinks may aid solute transport (although, Alldredge and Cohen, 1987; observed that boundary layers hundreds of micrometers thick are

maintained despite this advection). Within sediments, because of reduced transport and higher bacterial populations, the conditions required for microniche formation are optimised compared to the water column. The extent to which sinking particles have an effect on microniche formation in sediments will depend upon whether they reach the sediment while they are still metabolically active.

The direct study of marine snow microniches has provided useful insights into the geochemistry of isolated reactive particles. However, this work has seldom been recognised by those investigating microniches. Changes in pH observed in 1D for marine snow using electrodes (Alldredge and Cohen, 1987; Ploug et al, 1997) have been confirmed for microniches in 2D using planar optodes (Zhu et al, 2006). Sulphide production within marine snow was identified in very small (0.7-2 mm) aggregates of reactive matter (Shanks and Reeder, 1993), before being reported in 2D at high resolution within sediments (Devries and Wang, 2003). From these studies we can conclude that there is some common geochemistry shared by the particles in the different environments. Direct analysis of marine snow particles is more easily achieved than direct study of microniches and this provides an opportunity to use the full range of electrode probes (listed in Paper I) to further our geochemical knowledge of microniches for a range of elements or species.

#### 1.4 Modelling of microniches

The modelling of microniches was pioneered by Jørgensen (1977), who investigated the conditions required for the presence of oxygen depletion within microniches in the oxic zone of the sediment. Adopting a 1D approach, the O<sub>2</sub> consumption was modelled, considering microniche size (diameter, spherical geometry was adopted)

and ambient O<sub>2</sub> concentrations. Jørgensen (1977) calculated that for anoxia to occur at the centre, a niche would have to be two millimetres in diameter when the O<sub>2</sub> concentrations were that of saturated seawater and the respiration rates within the niche was five times the sediment average (a very conservative estimate). At 1% O<sub>2</sub> saturation the minimum niche diameter required was 200 µm.

Jahnke (1985) recognised that microniches rich in organic matter may support large bacterial populations and have respiratory rates faster than the bulk sediment. He also concluded that smaller rapidly respiring particles are more likely to experience O<sub>2</sub> depletion at their centres than larger slower respiring niches. Ambient porosity of 0.9 with a microniche value of 0.7 (ml cm<sup>-3</sup>) was used. This gave an effective microniche diffusion coefficient within the niches of 61% of the porewater value. Jahnke (1985) stated that when modelling the effects of microniches on a whole system, the volume-integrated OM degradation rate (the overall rate accounting for processes at microniches as well as in the bulk sediment) must remain constant. This therefore exerts a control on the number of microniches and/or the OM degradation rates at the niches. In practice this means that if the degradation rate of microniches increases, then fewer microniches must exist per unit volume. Jahnke (1985) showed that the maximum respiratory rate (per unit volume of sediment) of one millimetre diameter microniches is inversely correlated to the number of particles, with a factor of ten decrease in the number of particles yielding a ten times increase in maximum niche respiratory rate.

There are two key limitations to both the Jørgensen (1977) and Jahnke (1985) modelling. Firstly, by not considering electron acceptors other than O<sub>2</sub> and nitrate, the

likelihood that localized oxygen penetration will be decreased by oxidation of localised elevated concentrations of reduced components (e.g.  $\text{NH}_4^+$ ,  $\sum\text{S}(-\text{II})$ ,  $\text{Fe}^{2+}$ ,  $\text{Mn}^{2+}$ ) is excluded. Secondly, by assuming homogeneous conditions around the microniches, the complex 3D distribution of solutes that occurs within the sediment is not considered. As both models considered niches within the oxic zone, it is likely that strong gradients will occur within the niches as well as within the surrounding sediment. This effect will be even more exacerbated where the ambient and niche porosities are different.

Brandes and Devol (1995) modelled microniches within a two-dimensional gridded domain (one square centimetre), to explain observations of simultaneous  $\text{O}_2$  and  $\text{NO}_3^-$  respiration obtained from whole core squeezing experiments. They suggest that, in addition to organic carbon microniches, mixing of reduced inorganic material into the oxic zone may also be important in creating micro-zones of oxidizable material that consumes oxygen. The gridded area contained a distribution of <20, 100  $\mu\text{m}$  diameter microniches, with high respiration rates. Their relative positions were adjusted (by eye) to obtain a best fit to the experimental data. With the assumed carbon concentration and  $\text{O}_2$  respiration rates, the estimated particle lifetime was 15 days. Given the niche lifetimes measured/estimated from other studies (e.g. 2.5 days, Alldredge and Cohen, 1987; <5 days, Zhu et al, 2006), the particle respiration rates may be underestimated. However, Brandes and Devol (1995) did suggest that if the system were modelled in 3D, for the same result it would require fewer particles with higher reaction rates and hence shorter lifetimes.

## **2 Aims and scope of the thesis**

The aims of this thesis were fourfold:

1. To critically review the literature of previous studies of microniches using high resolution probes and modelling approaches.
2. To develop a binding phase for the DGT technique, to enable analysis of oxyanions in sediment at high resolution, and to apply this technique to investigate processes occurring at a sulphidic microniche within a freshwater sediment.
3. To investigate the relationship between trace metal (cobalt) and iron and manganese in a marine sediment using DGT.
4. To apply a three-dimensional diagenetic model to investigate conceptually the geochemical behaviour of microniches under different conditions and to interpret these observations in terms of data from the literature and known trace element geochemistry.

## **3 Descriptions of individual papers**

### **3.1 Paper I**

Paper I is a critical review of the literature on the experimental evidence available on the existence of micro-heterogeneity in sediments, in essence forming an extended introduction to the thesis. The review covers the historical development of studies of micro-heterogeneity, current technologies used to elucidate their presence and suggests how future studies may be better focussed. Whilst the review covers the study of burrow microenvironments as well as microniches, each section is concluded with a description of the evidence for the existence of microniches. The rationale for the study of microniches is covered in this paper and is therefore excluded from the introduction.



### 3.2 Paper II

Paper II describes the methods for preparation, deployment and analysis for a combined silver iodide-ferrihydrite binding phase (within a hydrogel) for the diffusive gradients in thin-films (DGT) technique. The gel allows simultaneous analysis of phosphorus, sulphide, vanadium and arsenic. Results from laser ablation of the gel obtained at a sulphidic microniche in a freshwater sediment are discussed in terms of the potential geochemistry.

### 3.3 Paper III

Paper III presents observations revealed from multiple DGT deployments in a marine (Fleetwood Marina, UK) sediment. Aged sediments and fresh intact incubated cores yielded different relationships between Fe/Mn and cobalt. This study is not related directly to microniches. However, both understanding resupply to the DGT device and determining the relationships between trace metals and authigenic oxides are potentially important to the study of microniche geochemistry.

### 3.4 Paper IV

Paper IV presents the formulation and use of a diagenetic model designed specifically to investigate geochemistry at, or induced by, microniches. The complete framework of the model is described. The model is then applied to a hypothetical scenario, where microniches exist a few millimetres below the sediment water interface. The oxygen, nitrate and sulphide concentrations are discussed in terms of how they are affected by the niche.

### 3.5 Paper V

Paper V extends the microniche modelling undertaken in Paper IV by considering the effect of organic matter degradation rates and porosity on the life-span of a niche. Sulphide evolution in a niche below the nitrate penetration depth is discussed in terms of iron-sulphide formation. The potential trace metal diagenesis at microniches is discussed with reference to observations reported in the literature.



### **Addendum to electronic version**

**This version contains unchanged introductory material from the print version of the thesis. The final print version of the thesis contained various version of papers depending on the stage reached in the publication process at the time of submission. All of the papers are now published so the full citations are given below and the final version are not reproduced here. Paper 5 was changed substantially during the peer-review process, with the removal of a discussion of trace metals. For completeness the version submitted in the final thesis is included in this electronic version.**

**Pre-prints of all published papers are archived on the Lancaster University eprint archive at: <http://eprints.lancs.ac.uk>**

I. Stockdale, A., Davison, W., Zhang, H., 2009. Micro-scale biogeochemical heterogeneity in sediments: A review of available techniques and observed evidence. *Earth-Science Reviews*, 92, 81-97. <http://dx.doi.org/10.1016/j.earscirev.2008.11.003>

II. Stockdale, A., Davison, W., Zhang, H., 2008. High-resolution two-dimensional quantitative analysis of phosphorus, vanadium and arsenic, and qualitative analysis of sulfide, in a freshwater sediment. *Environmental Chemistry*, 5, 143-149. <http://dx.doi.org/10.1071/EN07096>

III. Stockdale, A., Davison, W., Zhang, H., Hamilton-Taylor, J., 2010. The association of cobalt with iron and manganese (oxyhydr)oxides in marine sediment. *Aquatic Geochemistry*. <http://dx.doi.org/10.1007/s10498-010-9092-1>

IV. Sochaczewski, Ł., Stockdale, A., Davison, W., Tych, W., Zhang, H., 2008. A three-dimensional reactive transport model for sediments, incorporating microniches. *Environmental Chemistry*, 5, 218-225. <http://dx.doi.org/10.1071/EN08006>

V. Stockdale, A., Davison, W., Zhang, H., 2010. Sulfide evolution from faecal pellets and other microniches within sub oxic surface sediment. *Geochimica et Cosmochimica Acta*. <http://dx.doi.org/10.1016/j.gca.2010.02.005>



# Sulphide evolution from faecal pellets and other microniches within sub oxic surface sediment: The effects on the geochemistry of iron and trace elements

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## Abstract

Direct introduction of particles within sediments, such as faecal pellets, as well as biotic translocation of surface deposited material to greater depths, can lead to heterogeneously distributed particles of localized highly reducible organic matter (microniches) being present at depth. Where  $O_2$ ,  $NO_3^-$ , and Fe/Mn oxyhydroxides become depleted within microniches or where they exist in zones of sulphate reduction, significant localized peaks in sulphide concentration can occur. These discrete zones of sulphide can cause specific localized diagenesis, affecting iron as well as trace elements. We have used a reaction-transport model developed specifically for investigating spherical microniches, and incorporating 3D diffusion, to investigate how the rate of organic matter (OM) degradation and the particle porosity affect sulphide and iron concentrations and the saturation index (SI) at such niches. For all of the modelled scenarios the SI for iron sulphide is positive, indicating conditions for FeS precipitation in all niches. Those simulations within the microniche lifetime (the time taken for the niche OM to reach 35% of its initial value,  $t_{35\%}$ ) range of 2.5 to 5 days gave comparable concentration ratios of sulphide to iron in solution within the niche to experimentally observed values. Decreasing porosity, lower  $t_{35\%}$  values and increasing OM degradation rates all tend to increase the likelihood that peak FeS precipitation will preferentially occur at the edges of the niche rather than uniformly throughout its volume. For trace elements forming sulphide precipitates, the saturation conditions evolve quickly (minutes) after the particle is introduced. Faecal pellets and other microniches may be important zones of FeS and trace metal sulphide formation in sediments and provide mechanism for metal removal within the oxic and suboxic zones, where formation of sulphides would not be predicted by analysis of the bulk sediment. These processes have implications for understanding the diagenesis of Fe and trace metals, and for our knowledge of the mechanisms for organic material preservation in the fossil record.

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## 1. INTRODUCTION

In stable sediment where oxygen is present at the sediment water interface, bioturbation influences the sediment structure. Due to burrow formation, irrigation, feeding and associated processes, this influence often extends some way into the zone of the sediment usually considered anoxic. These processes create distributions of localized geochemical features as a result of, active burrows (with surface connection), inactive and infilled burrows, and faecal pellets, as well as translocation of surface deposited material, such as marine snow, to greater depths. Here we consider that microniches are formed when discrete particles of reactive organic matter are introduced at depth in the sediment. These microniches can be attributed to decaying organisms (observed using a pH optode; Zhu et al, 2006), algal aggregates (added to

sediment to study sulphidic microniches; Widerlund and Davison, 2007) and faecal pellets (photographed after resin embedding and thin sectioning of an intact core; Watling, 1988). Within vegetated sediments such as mangroves, root systems can also generate microniches (e.g. Alongi et al, 2004). The diameter of these microniches can in principle vary from a few microns up to the centimetre scale. However, using high-resolution probes their diameter has generally been observed in the range of 400  $\mu m$  to  $\sim 1$  cm (Stockdale et al, 2008; and references therein).

Where microniches become depleted in  $O_2$ ,  $NO_3^-$ , and Fe/Mn oxyhydroxides or where they exist in zones of sulphate reduction, significant localized peaks in sulphide concentration can occur. Elevated sulphide within these microniches results in conditions where the formation of metal sulphides is optimised. Within the upper iron-dominated zone of marine sediments, localized pyrite is commonly associated with microniches (Raiswell, 1993). To

date, scant consideration has been given to how localized concentrations and microscale processes will affect, temporally and spatially, the formation of metal sulphides and favour particular reaction mechanisms in particles such as faecal pellets. It is difficult to do this by measurement as techniques that allow measurement on an appropriate scale are just being developed now. The stochastic nature of the processes means that it is likely to be many years before a true representative and comprehensive data set is available. In the absence of experimental data, modelling can be used to advance understanding in this field. Subsequent sections of the introduction examine previous modelling of microniches, evaluate the trace element/sulphide behaviour and niche geochemistry that is relevant to this work, and finally describe the aim and rationale of this work.

### 1.1. Trace Element/Sulphide Geochemistry

Several studies have compared reactive and pyrite bound fractions of trace metals, based on whether their proportion extracted with nitric acid (the final stage of a sequential leaching process) is more, less or similar to that of iron (Huerta-Diaz and Morse, 1990, 1992; Otero and Macias, 2003). The two parameters, degree of pyritization (DOP; Berner, 1970) and degree of trace metal pyritization (DTMP), are measures of the extent to which reactive iron is transformed into pyrite (DOP) and reactive trace metal is incorporated into pyrite (DTMP). These concepts were introduced to try to account for the quantities of metal present outside of a sulphide phase (influenced by e.g., adsorbing surfaces) where sulphide precipitation is favourable (Huerta-Diaz and Morse, 1992). Equations 1 and 2 show how these data are calculated.

$$\text{DOP}(\%) = \frac{\text{Pyrite-Fe}}{\text{Pyrite-Fe} + \text{Reactive-Fe}} \times 100 \quad (1)$$

$$\text{DTMP}(\%) = \frac{\text{Pyrite-TM}}{\text{Pyrite-TM} + \text{Reactive-TM}} \times 100 \quad (2)$$

Trace elements can be placed into three distinct groups based on the observed DTMP versus DOP (Figure 1). Morse and Luther (1999) assessed the early diagenetic geochemical processes that may affect the incorporation of trace elements into pyrite. Table 1 shows the phytoplankton element- carbon ratios reported in the literature and the early diagenetic processes that, according to Morse and Luther (1999), may affect the DTMP. These explanations for the observed behaviour indicate possible mechanisms of initial trace element reactions with sulphide and FeS, and the group within which an element falls may give an indication of how they behave within highly sulphidic microniches. For example, elements that exist as oxyanions will undergo reduction to yield species that are either more susceptible to scavenging as sulphides (e.g. Mo or As), or resistant to reaction with sulphides (e.g. Cr). Where ionic trace element sulphides are more susceptible to scavenging by FeS (e.g.  $\text{MoS}_4^{2-}$ ; Helz et al, 2004) they may be more likely to be incorporated into pyrite. Other

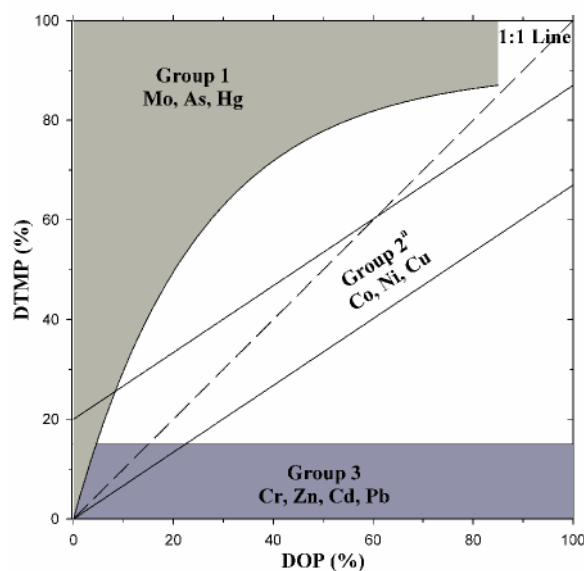


Figure 1. Degree of trace metal pyritization (DTMP) vs. degree of pyritization (DOP). Based on data in Huerta-Diaz and Morse, (1992) and Otero and Macias, (2003). A similar figure was presented in Burdige (2006).  $^{65}\text{Cu}$  is included in Group 2 for simplicity, however the data tend to follow the 1:1 line more closely than represented here.

metals (Zn, Cd, Pb) react at a faster rate with sulphide (relative to Fe) and may form metal sulphides independent of pyrite.

### 1.2. Geochemistry of Microniches

Localized elevated sulphide coupled with trace element supply, resulting for example, from the oxidation of organic matter or diffusion of trace elements into a microniche from the surrounding sediment, may result in environments where trace element sulphide formation is significantly higher than values observed from bulk measurements. For example measurements such as core slicing, where mixing of redox regimes may result in loss of observable sulphides via oxidation. If such sulphides are not subsequently re-oxidized, microniches may account for a significant proportion of trace element accumulation. Widerlund and Davison (2007) observed numerous 2D images of sulphidic microniches in a freshwater sediment using diffusive gradients in thin films (DGT). They calculated that the proportion of the probe area occupied by sulphidic microniches was approximately one to four percent of the total probe area, indicating that in some sedimentary environments, microniches (and their associated elevated degradation rates) are significant in terms of the fraction of organic matter reduced. High resolution DGT has also demonstrated that cationic trace metals can be released at sulphidic microniches (Motelica-Heino et al, 2003). Conversely, depletion of phosphate and oxyanions of trace elements at a microniche has been observed at a sulphidic niche using similar techniques (Stockdale et al, 2008a).

Table 1. Pyritization group, phytoplankton element/carbon (E:C) ratios, and geochemical reasons for pyritization behaviour, for a range of elements.

DTMP: DOP group	Element	E:C (mol mol <sup>-1</sup> (× 10 <sup>-6</sup> ))	Ref.	Reasons attributed to trace element pyritization behaviour (Morse and Luther, 1999)
0	Fe	49	(1)	
		61	(2)	
1	As <sup>a,b,c</sup>	2.7	(3)	Oxyanions, first reduced by sulphide, may subsequently react with sulphides resulting in incorporation into pyrite.
	Mo	0.24	(2)	
	Hg <sup>b</sup>	0.0065	(4)	
2	Co	1.5	(2)	Slower water exchange kinetics than Fe <sup>2+</sup> ; FeS phase precipitates and metals are subsequently incorporated into pyrite.
	Ni	2.7	(1)	
	Cu	2.7 3.1	(1) (2)	
3	Cr <sup>b,c</sup>	4.1	(5)	Oxyanion reduced to a form that is kinetically inert to reaction with sulphide.
	Zn	12.5	(1)	
		6.5	(2)	
	Cd	2.5	(1)	
		1.7	(2)	
	Pb <sup>b,c,d</sup>	1.1	(6)	Faster water exchange kinetics than Fe <sup>2+</sup> , (Zn, Cd, Pb)S phases precipitate prior to FeS, resulting in low fractions of pyritized metal.

(1) Bruland et al (1991) citing Martin and Knauer (1973) and Martin et al (1976), averaged values. (2) Ho et al, 2003. (3) Michel et al (1998). (4) Bargagli et al (1998). (5) Ebihara et al (2006). (6) Bu-Olayan et al (2001). <sup>a</sup>Estimated value. <sup>b</sup>Converted from µg/g(dw) by assuming 35g (dw) of phytoplankton contains 12g (one mole) of C. <sup>c</sup>Potential contamination sources near study sites. <sup>d</sup>Value from the site with the lowest Pb value for seawater.

### 1.3. Modelling of Microniches

Jørgensen (1977) pioneered modelling of microniches, investigating the conditions required for a niche to become anoxic within oxic sediment. This work and subsequent work by Jahnke (1985) considered scenarios where concentrations of possible reactants in the porewater surrounding the niche were homogeneous. Brandes and Devol (1995) extended the concepts to include multiple niches and associated gradients for O<sub>2</sub> and NO<sub>3</sub><sup>-</sup> in two-dimensions. Raiswell et al (1993) recognised that understanding localized iron-sulphide precipitation may be of value in paleoenvironmental studies and formulated a basic, 3D, three-component model (dissolved Fe and sulphide and a pyrite precipitate) relating diffusion and precipitation at the edge of spherical microniches of diameters 50 µm or more. The model assumed that sulphide diffuses away from the niche and reacts with dissolved iron to form precipitates. The modelling assumed that there is a constant (infinite) fixed pool for each of the solute components. The sulphide pool associated with the niche and the iron pool from the bulk surrounding sediment. Between these pools, at the edge of the niche, there is a reaction zone where diffusion and precipitation occur. The modelling showed that a greater niche diameter or higher sulphate reduction rate, required increasingly high dissolved iron concentrations to constrain pyrite precipitation to the niche edge (Raiswell et al, 1993). If the niche size is increased and the Fe is kept constant this would allow a greater proportion of the niche sulphide to diffuse further from the niche

before reacting with iron, leading to a lack of preservation of a pyrite imprint at the niche.

Multi component modelling in 3D has revealed further complexity in microniche geochemistry. Sochaczewski et al (2008), showed that within a single microniche near the sediment surface, there can be up to three discrete zones characterised by the dominance of different oxidants (O<sub>2</sub>, NO<sub>3</sub><sup>-</sup> and SO<sub>4</sub><sup>2-</sup>). It was assumed that there was no Fe or Mn oxides in the niche, which represents a parcel of organic matter. Sulphide is produced because O<sub>2</sub> and NO<sub>3</sub><sup>-</sup> are readily consumed in the small volume of the niche.

### 1.4. Aims and Rationale of this Work

In the absence of appropriate experimental techniques, modelling can be used to advance understanding of processes occurring at localized highly labile particles such as faecal pellets or algal aggregates. 3D modelling gives a truer result as it allows lateral diffusion around niches that is not accounted for in 1D simulations. Here we modelled, in 3D, an idealised spherical particle with different values applied to the variables porosity and organic matter degradation rate. The modelling was undertaken without use of any fitting parameters so that any correlations to experimentally observed data are on an a priori basis. There were two main aims of this study. Firstly, to examine how a range of porosities and OM degradation rates affect sulphide and iron concentrations within microniches and to discuss how the results are related to observations and hypotheses from previous studies. Secondly, to assess how the modelling results are applicable to trace element diagenesis.



## 2. MODELLING FRAMEWORK

### 2.1. Model Description

The sediment model 3D TREAD is a fully three-dimensional diagenetic model specifically designed to investigate diagenetic processes occurring at spherical microniches. A brief description of the model is given here, for a more comprehensive account see Sochaczewski et al (2008).

The complexity of any simulation in 3D TREAD is dependent upon the number of modelled components and reactions specified by the user. Rather than providing a rigid framework where components and reactions are fixed, the model lets users specify all required parameters. For each individual component the following conditions can be set: boundary conditions for the top and bottom of the domain; diffusion coefficients; microniche radius, coordinates and concentration; initial profiles (for  $t = 0$  s). Reactions and their rates are then specified for the listed components. Reactions can be specified as primary (i.e. organic matter decomposition) or secondary, with primary reactions requiring specification of a priority component (the OM oxidant) and a concentration threshold, below which the reaction with the next priority can begin to proceed. Secondary reactions can be specified as first order for each reactant (overall order based on the number of reactants) or first order for a single component only (overall order of one).

The domain parameters required include: domain size (x, y and z lengths), resolution (this controls the density of the 3D mesh), total simulation run time, the time step between each calculation, and the time step between each data save (this allows the output file size to be constrained and reduces output processing times). The porosity profile (and distinct values for each microniche) together with the equation for tortuosity (and associated variables) complete the parameterization of the model. As the model inputs are entered via a graphical user interface, parameters can be altered easily, allowing a range of scenarios to be tested.

### 2.2. Setup of Model Simulations

The reactions applied to the modelling are shown in Tables 2 and 3 (primary and secondary reactions respectively). Full model parameters (required inputs as described in section 2.1.) are provided in the supporting information as Table S1.

Table 2. Primary (organic matter) reactions included in the modelled simulations.  $H_2O$ ,  $H^+$  and  $\Sigma CO_2$  are include in the reactions for balancing but are excluded from the model simulations. The full equations including  $f$  and TE are used in the calculations for Tables 4 and 5 ( $f$  is the fraction of trace metal associated with the particular component and TE is the trace element).

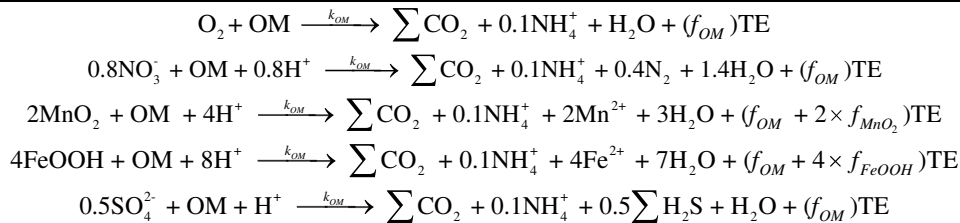
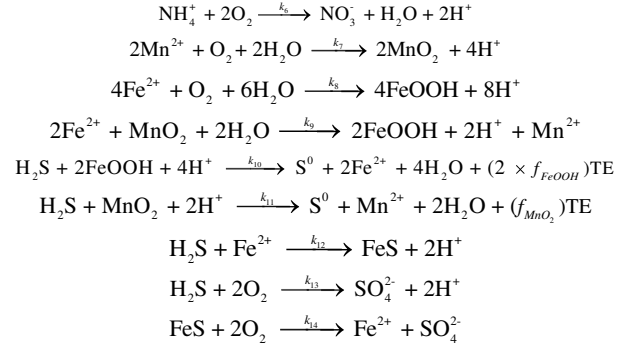


Table 3. Secondary reactions included in the modelled simulations.  $H_2O$ ,  $H^+$  and  $S^0$  are include in the reactions for balancing but are excluded from the model simulations. ( $f$  is the fraction of trace metal associated with the particular component and TE is the trace element).

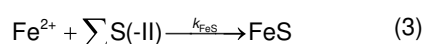


The environmental framework (i.e. the sediment chemistry and properties) is based on a comprehensive data set for a marine sediment by Fossing et al (2002; 2004). The modelling and associated parameters in this study are partly based upon previous studies (e.g. Froelich et al, 1979; Van Cappellen and Wang, 1996; Wang and Van Cappellen, 1996; Rysgaard et al, 1998). These data include all of the required inputs with the exception of the microniche specification. As we model a smaller domain, boundary conditions are derived from the 1D sediment profiles presented by Fossing et al (2002; 2004).

Sulphide removal mechanisms were via diffusion and reaction with  $Fe^{2+}$  (discussed below). The niche size (diameter) was set at three mm (metal release was measured at a similar sized sulphidic niche in a freshwater sediment by Motelica-Heino et al, 2003). Porosity outside the niche was set as 0.83, consistent with the data compilation used for the bulk values. Microniche porosity was varied to examine its effect. The range considered was from high porosity ( $\phi = 0.97, 0.9$ ) to niches denser ( $\phi = 0.8, 0.7$ ) than the ambient value. Niches are assumed to have negligible iron or manganese oxides available for OM oxidation. Where the niche surface contacts the bulk sediment these oxidants are assumed to be available. The limited consequences of the presence of authigenic oxides within microniches is briefly discussed in section 3.4.2.1.

### 2.3. Treatment of Iron-Sulphide Reactions

Iron sulphide precipitation/dissolution reactions are often modelled assuming reversible reactions, typically expressed as separate reactions for formation and dissolution. Whether or not the saturation conditions are met controls which of the two reactions can proceed (see, van Cappellen et al, 1993; Boudreau, 1996; Wang and van Cappellen, 1996 for details of this approach). This relationship is widely used in diagenetic models (e.g. Wijsman et al, 2002; Morse and Eldridge, 2007). However, in other modelling cases (e.g. Berg et al, 2002; Fossing et al, 2004) a simple unidirectional formation reaction has been applied (Eq. 3).



A significant advantage of using this approach is that the complexities of modelling pH changes within the model can be avoided. Furthermore, for our modelling this approach is appropriate, as saturation conditions are likely to apply throughout the small domain modelled. Thus the reverse process is negligible and can effectively be excluded.

### 3. RESULTS AND DISCUSSION

This section reports the results of the modelling and discusses them in terms of:

- trends in iron, sulphide and the related saturation index (SI) with changing porosity, OM degradation rate and niche lifespan.
- relating data from these trends to experimental observations

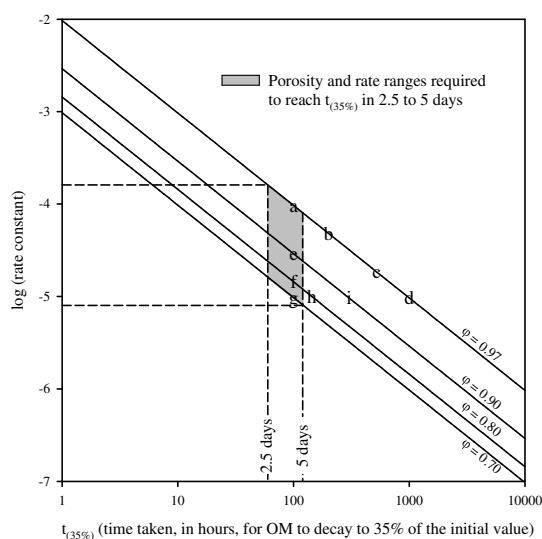


Figure 2. Relationship between the rate constant for the decomposition of organic matter (OM), porosity of the microniche, and the time taken (in hours) for the OM concentration to decay to 35% of the initial value. Letters represent individual data points used in model runs described in the text.

- assessing the optimum conditions for the formation of FeS crusts at microniches
- relating the modelled data to known behaviour of trace elements in terms of, trace element sources, reaction pathways, and solubility of trace element sulphides.

### 3.1. Description of Modelled Scenarios

Microniches with various properties were modelled. The effects of porosity and reaction rate of organic matter on the lifespan of a niche are shown to give a general overview, with specific examples considered in more detail to examine the generation of sulphide (and associated iron) profiles. The simulation conditions were devised to consider localized sulphide concentrations and the associated lifespan of the niches, while making comparisons with reported reaction rates and experimental observations of niche life-span. Modelling different porosities allow the results to be interpreted for a range of particle types, from high porosity niches such as algal aggregates to lower porosity particles such as faecal pellets.

### 3.2. Iron and Sulphide at Microniches

#### 3.2.1. Trends Related to Porosity and Rate

Typically observed values for the rate of decomposition of OM, porosity and microniche size were used in the simulations, to ensure that the outputs can be related to realistic environmental scenarios. Figure 2 shows the relationship between reaction rate and microniche lifetime for niches with a range of porosities. Lifetime is operationally defined as the time taken for a niche to be degraded to 35% of the starting value ( $t_{35\%}$ ). The lettered data points in Figure 2 represent three groups of data where one of the parameters is constant. Group A (a, b, c, d) has constant porosity, with the decreasing rate constant resulting in an increase in  $t_{35\%}$  across the series. Group B (a, e, f, g) was obtained by setting a series of decreasing porosity and adjusting rate constants to give equal values for  $t_{35\%}$  (100 hours). For Group C (g, h, i, d) the rate constant was maintained and  $t_{35\%}$  calculated for the range of porosities. Fossing et al (2002; 2004), in modelling a marine sediment in 1D, used a multi-G approach to organic matter degradation (e.g. Westrich and Berner, 1984). They used a ratio for the rate constants of degradation of the fast and slowly degrading pools of OM of 800 ( $k_{om-f} : k_{om-s}$ ). This  $k_{om-f}$  rate constant was applied to the scenarios modelled in Group C. Within Group A, ratios of 800, 1600, 4000 and 8000 were used to generate outputs for d, c, b and a respectively. The  $t_{35\%}$  values for Group B lay within the range of microniche lifetimes observed by Alldredge and Cohen (1987) and Zhu et al (2006).

Figure 3 shows, for each of the lettered groups, the sulphide and  $\text{Fe}^{2+}$  concentrations at the centre of the modelled microniches, and the saturation index (SI), which is related to the solubility

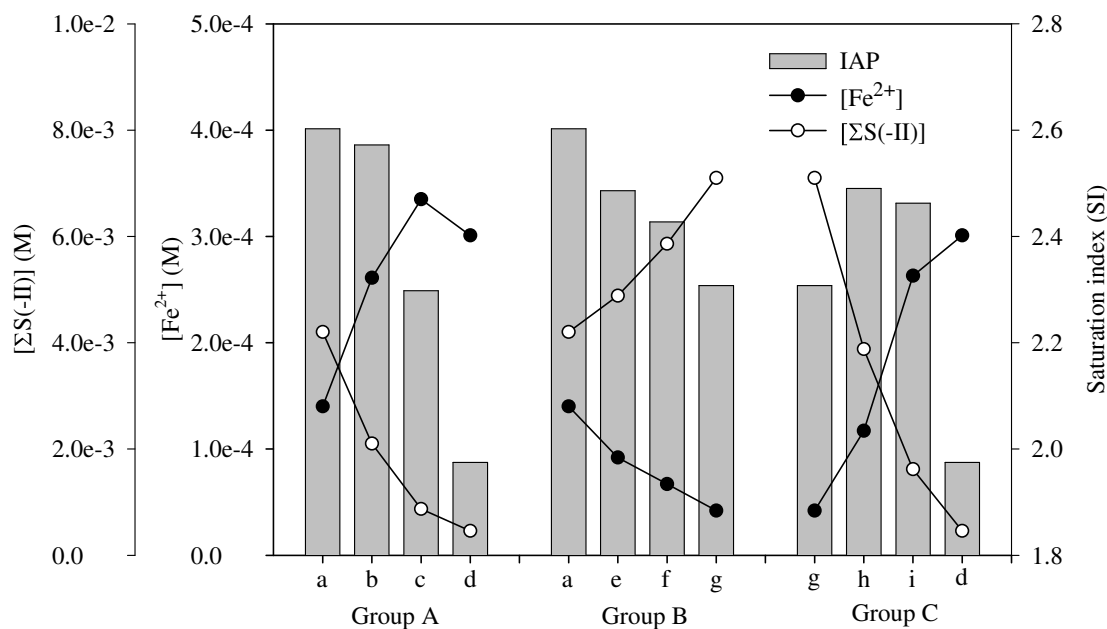


Figure 3. Predicted concentrations of sulphide and iron and the related saturation index (SI) after 2.3 hours of the simulations at the centre of a microniche. The letters represent the data points in Figure 2, where each group of letters has one variable set as a constant. Group A has constant porosity, Group B has conditions where  $t_{35\%}$  is constant, Group C has a constant OM degradation rate. Note that the axis for the SI values does not start at zero.

product of FeS ( $K_{sp}$ ) and the ion activity products (IAP; Eqs. 4 and 5).

$$\text{IAP} = \{\text{Fe}^{2+}\}\{\text{HS}^{-}\}/\{\text{H}^{+}\} \quad (4)$$

$$\text{SI} = \log(\text{IAP}/K_{sp}) \quad (5)$$

IAP was calculated assuming a pH of 7 (consistent with marine porewater values that are typically lower than the overlying water (e.g. Ben-Yaakov, 1973; Zhu et al, 2006) and ionic strength of 0.7 M, with activity coefficients of,  $\gamma_{\text{Fe}^{2+}} = 0.255$ ,  $\gamma_{\text{HS}^{-}} = 0.410$ ,  $\gamma_{\text{H}^{+}} = 0.958$ , (values for  $\text{Fe}^{2+}$  and  $\text{H}^{+}$  were calculated using the Pitzer equation and associated variables as reported in Millero and Schreiber, 1982; bisulphide value is that reported in Davison, 1980).

Decreasing the rate constant and maintaining a fixed porosity (Group A) results in decreasing peak sulphide values, due to lower generation of sulphide fluxes within the niche. The Fe(II) concentration at the centre of the niche is determined by several opposing factors. As sulphide produced in the niche diffuses out, it reduces FeOOH in the surrounding sediment and the resulting Fe(II) diffuses in. Fe(II) is also supplied to the system as FeOOH is used as an electron acceptor at the niche edge. For scenarios with shorter life-spans, the FeOOH is depleted more rapidly, affecting the potential Fe(II) supply from this source. However, Fe(II) is also continuously removed at all locations by reaction with  $\text{HS}^{-}$  to form FeS. The peaked distribution for Fe can be ascribed to changes in the relative dominance of these three processes. The SI is strongly dependent on sulphide in this case.

Where OM degradation rate constants are adjusted for different porosity microniches to give equal lifetimes for all niches (Group B), diffusion and reaction with sulphide controls the peak values of Fe(II) and diffusion and the rate constant controls peak sulphide. As the porosity decreases, both diffusion and reaction rates lowered, decreasing both the inward iron flux and the outward flux of sulphide. In this marine system the sulphate removal rate is not high enough to cause this electron acceptor to become limited in any of the modelled scenarios. Iron tends to exert the main control on the SI within this group.

Where porosity ( $\phi$ ) is increased at a constant OM degradation rate constant (Group C) sulphide decreases due to a reduced flux caused by the lower physical amount of reactive OM within the niche (accounted for in the model calculation by a  $(1-\phi)$  function). Across this group the peak concentration of Fe(II) increases as diffusion is faster and removal by sulphide is lower. The highest values for the SI are observed at intermediate porosities. SI in this group is not controlled exclusively by one species. Within the lowest porosity niche it is constrained by limited diffusion of Fe(II) into the niche, while within the highest porosity niche it is constrained by lower sulphide concentrations caused by a reduced sulphide flux. These processes are represented visually in Figure 4, which shows 2D profiles of  $\Sigma\text{S}(-\text{II})$ , Fe(II) and FeS after 24 hours for scenario g. Part d of this figure shows a schematic of how FeS may preferentially form at the edges of niche, which is shown by the modelled data in part c of the figure.

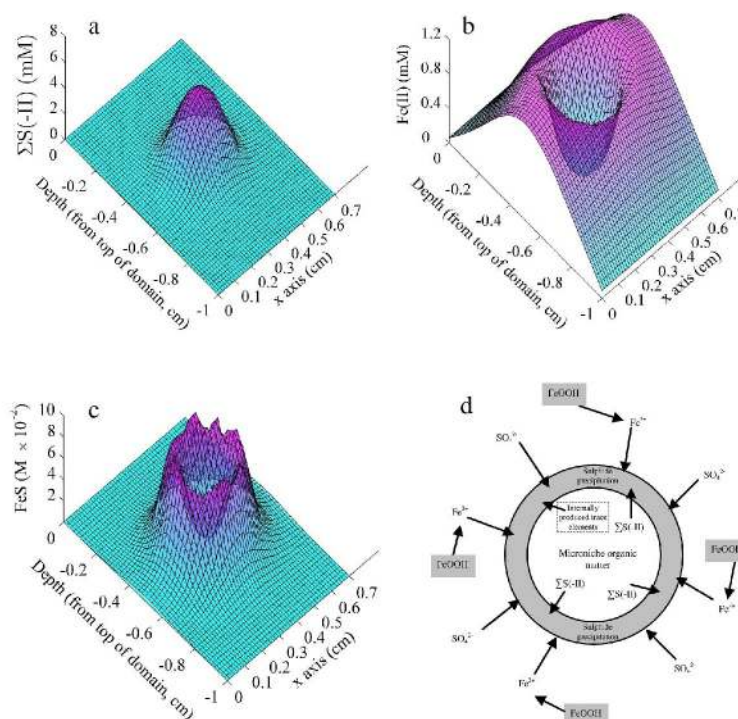


Figure 4.  $\Sigma S(-II)$  (a),  $Fe(II)$  (b) and  $FeS$  (c) concentration across the x axis of the modelled domain after 24 hours (y coordinate was the centre of the microniche). The microniche had a porosity of 0.7, an OM concentration of 5 M, and an OM degradation rate of  $9.6 \times 10^{-6} \text{ s}^{-1}$  (scenario g in Figure 2). Part d, shows a schematic for the sulphide precipitation and solute fluxes into and from the microniche, modified from Berner (1980, p131).

### 3.2.2. Relating General Trends from the Modelled Data to Experimental Observations

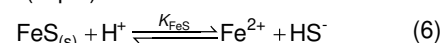
Peak sulphide concentrations for the microniches are high when compared to bulk porewater values from electrode studies. For example, Sell and Morse (2006) reported a value of  $\sim 3 \times 10^{-5} \text{ M}$  for a marine sediment, approximately 2 cm below the oxygen penetration depth. If this value is representative of a background measurement, in the modelled microniche, peak concentrations are between  $\sim 15$  and 240 times the background value. Using DGT to measure sulphide in a freshwater sediment, Motelica-Heino et al (2003), reported a sulphidic microniche with concentrations approximately 30 times the average background value. Sagemann et al (1999) set up laboratory experiments to determine conditions that may result in mineral formation at the soft tissue of benthic organisms (via precipitation of carbonates and phosphates as well as sulphides). They measured sulphide concentrations at the edge of a decomposing shrimp carcass of  $\sim 5.6 \text{ mM}$ . This value fits into the range of values modelled here (0.46-7.1 mM).

The ratios of the total-sulphide to iron concentrations calculated from the data in Figure 3 fall in the range 1.6 to 169. When the lifetimes greater than 7 days are excluded (Figure 2, points b, c, d and i) are excluded, the lowest ratio is 30. For microniches within a freshwater lake sediment, sulphide concentrations have been observed to be over 40 times higher than those of  $Fe^{2+}$  (Motelica-

Heino et al, 2003). These agreements between measurement and modelling further supports the assertion that niche lifetimes of less than one week are the most representative of natural conditions.

### 3.3. Iron Sulphide at Microniches

The solubility of freshly formed iron sulphide in circumneutral sediment tends to be controlled by the solubility product related to the bisulphide concentration (Eq. 6).



We calculated the distribution of sulphide species in simple sulphide solutions with a pH of 6, 7 and 8, an ionic strength of 0.7 and assuming  $[S^{2-}]$  is negligible (activity coefficients were,  $\gamma_{H^+} = 0.96$ ,  $\gamma_{HS^-} = 0.41$  and  $\gamma_{H_2S} = 1.0$ ). At pH 6, 7 and 8 approximately 19%, 70% and 96% respectively, of the total sulphide will be present as bisulphide. Within marine sediments pH has been observed over this range. Zhu et al (2006) using planar optodes, measured pH at a dead decaying organism (which can be considered a microniche) and reported pH at or below the lower detection limit of 5.9. Average pH between 1-6 cm below the sediment water interface, in the same sediment without the microniche but with burrowing activity, was  $\sim 6.8$  with maxima of  $\sim \text{pH } 8$  and minima of  $\text{pH } \leq 6.2$ . Using the SI data from Figure 3 (calculated at pH 7), the degree of saturation of  $FeS$  can be calculated. The lowest and highest values for SI are 1.97 and 2.6, equivalent to

a degree of saturation of 94 and 400 respectively. It is possible that levels of saturation will not reach these values due to the formation of other mineral phases.

Berner (1980) suggested that concretions of pyrite may be formed by heterogeneous reduction of sulphate at clots of organic matter. The sulphide reacts with Fe(II) diffusing towards the niche from the surrounding sediment to form iron sulphides that eventually transform to pyrite. The amount of FeS or pyrite formed is limited by the amount of decomposable organic matter in the niche and the resupply of Fe(II). Berner (1980) proposed that a crust of pyrite will form adjacent to the organic matter. When viewed in 2D as a cross section through the niche, the iron sulphide precipitate appears as a halo shape (Figure 4, part c). In modelling the lettered scenarios in Figure 2, we have determined the distribution of iron sulphide after 24 hours of each of the model runs. Figure 5 shows the vertical FeS profiles through the centre of each niche from these simulations and identifies the profile shape for each of the modelled scenarios. Simulations with  $t_{35\%}$  values higher than seven days (b, c, d, and i) tend to have either undefined or poorly defined FeS peaks at the niche edges. Where the  $t_{35\%}$  value lies within the 2.5-5 day range, peak FeS values are centred on the edges of the niche and peak values do not differ significantly (a, e, f and g). The greater the porosity of the niche, the lower the ratio of FeS at the edge of the niche compared to the centre of the niche. Scenario g shows the most significant halo effect and this is illustrated in 2D in Figure 4, part c.

The modelling has shown, a priori, that the concept described by Berner (1980) can be explained quantitatively by the microniche model, and that the niche life-times of 2.5-5 days give the best results in terms of the definition of the crustal nature of these iron sulphide deposits.

### 3.3.1. Relevance of 'Crustal' Deposition to Paleoenvironmental Studies

Although not the main focus of this study it is important to recognise the significance of the observed precipitation behaviour to the study of the preservation of microniches in the paleo record. Much work has focused on the processes involved in the preservation of soft-matter in the fossil record (e.g. Briggs et al, 1991; 1996; Raiswell et al, 1993; 2008). The conclusion that niche lifetimes of 2.5-5 days give better defined crustal deposition is supported by the work of Sagemann et al (1999). They concluded that: 1) Mineralization will be dominated by dysaerobic and anaerobic reactions, even in oxic sediments. 2) The most extensive mineral formation of soft tissues occurred under anoxic conditions. 3) Steep chemical gradients during the decay process lead to mineral formation. 4) Exceptional preservation of soft tissue is favoured by elevated microbial activity. 5) These critical controls that determine the balance between decay and mineral formation (points 1-4) must operate at an early stage following the death of an organism and mineral formation (leading ultimately to fossilisation) of soft tissue must be a rapid process

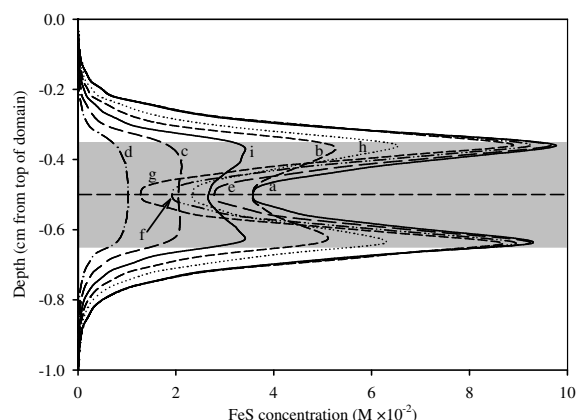


Figure 5. FeS concentrations after a 24 hour model simulation for each of the lettered scenarios in Figure 2. The shaded area represents the locations where the niche is present.

(days to weeks) as it would not occur at the normal bulk efficiency of OM degradation in marine sediments.

## 3.4. Relating Modelled Observations to Trace Element Diagenesis at Microniches

### 3.4.1. Modelling of Trace Element-Sulphide Reactions

Whilst modelling of general trace metal-sulphide interactions is limited, several studies have attempted to model zinc-sulphide reactions (Druschel et al, 2002; Choi et al, 2006; Canavan et al, 2007). These approaches (which are described and reviewed in more detail in the supporting information) tend to apply FeS formation rates to ZnS, which may not be accurate. More experimental evidence for reaction rates and determination of the significance of the different processes, is needed before such reactions can be modelled with any certainty. For this reason we considered that rather than attempting to model directly trace element behaviour at microniches, it was more appropriate to discuss the modelled observations for Fe and  $\Sigma S(-II)$  in terms of known trace element data such as sulphide solubility, trace element sources and known reaction pathways.

### 3.4.2. Trace Element Sources

The fractions of trace elements associated with phytoplankton organic matter (Table 1) are used to inform discussion of metal diagenesis at microniches. The majority of the data are taken from reported Redfield stoichiometries (Bruland et al, 1991; Ho et al, 2003). We recognise that there is likely to be large natural variability in different particles in the marine environment. Where microniches are formed from marine snow, the particles may undergo both loss and accumulation of some elements during settling (e.g. Fisher et al, 1991). Trace elements within faecal pellets from both pelagic and benthic organisms may be amended by digestion processes (e.g. Lee and Fisher, 1992 and references therein). Phytoplankton are the primary food source for many organisms and can be aggregated to form microniches, therefore, the trace

element ratio data are a suitable proxy for a range of niche types.

Table S2 is included in the supporting information to show the data used for trace metal concentrations (fractions) associated with authigenic oxides. Individual values for trace element fractions associated with both Fe and Mn authigenic oxides in Tessier et al (1996) are for freshwater sediments. Douglas and Adeney (2000) measured trace metals associated with Fe/Mn oxyhydroxides in marine sediments, but did not cite individual values for Fe and Mn oxides. Based on the high Fe:Mn ratio and assuming the values are just for authigenic Fe oxides, the concentrations in the mixed oxyhydroxide are ~2.5 times lower than the Tessier et al (1996) values. Therefore, the values used for authigenic Fe and Mn oxides are estimated as the Tessier et al (1996) values divided by 2.5. Using these data, Table 4 shows estimated trace element fluxes per mole of organic carbon (OC) per second for a niche with the same rate and porosity properties as scenario g. Each column of data in the table assumes that there is only one dominant electron acceptor degrading the OC. Where authigenic oxides are the dominant electron acceptor trace metal release at microniches may be significant. However, the extent to which these oxide concentrations are sustained within microniches is limited (discussed in the following section).

**3.4.2.1. Microniches containing authigenic oxides.** Degradation of OC involving authigenic oxides releases trace metal concentrations greatly in excess of the release attributed to organic matter alone (Table 4). It is unlikely that the supply of authigenic oxides will be sufficient to sustain element release from this source during a significant proportion of the niche lifetime, but it could be responsible for a pulse of metals from a localized source. To demonstrate this we modelled a scenario where the oxide concentrations at the nitrate penetration depth (0.67 cm; from the 1D profiles in Fossing et al, 2002; 2004) were applied to the niche, resulting in niches with oxide concentrations slightly elevated compared to the ambient sediment. The niche was assumed to have the same degradation rate regardless of the oxidant. Even for this situation favouring the presence of Fe/Mn oxides, they were consumed within the first 2-3 hrs of the model simulation. This effect was observed regardless of the whether limiting concentration thresholds, allowing successive electron acceptors, were set at the bulk values or 2% of this value. Additionally, loss of oxides by oxidation of the OM within the niche was much more significant than loss caused by chemical oxidation of sulphide (this work, unpublished results).

Elevated cationic metal concentrations observed at sulphidic microniches using DGT (for Co, Ni and Cu; Motelica-Heino, 2003) were attributed to concomitant release of sulphide and metal from the degrading niche. The observed elevated concentrations were 2-3 times the baseline concentrations observed outside the niche. It is possible that elevated trace metal may alternatively be attributed to an initial fast release

Table 4. Estimated maximum trace metal release (in mol per mol of organic carbon per second) resulting from different organic matter oxidation pathways. Assumes conditions the same as scenario g in Figure 2 (i.e.  $\phi = 0.7$ , and rate =  $9.6 \times 10^{-6} \text{ s}^{-1}$ ). See Tables 1 and S2 for the element fractions data and Table 2 for the equations used. Elements are grouped according to their DTMP group (see Figure 1).

Element	Electron acceptor		
	O <sub>2</sub> , NO <sub>3</sub> <sup>-</sup> , SO <sub>4</sub> <sup>2-</sup> (mol (mol OM) <sup>-1</sup> s <sup>-1</sup> ( $\times 10^{12}$ ))	MnO <sub>2</sub> (mol (mol OM) <sup>-1</sup> s <sup>-1</sup> ( $\times 10^9$ ))	FeOOH (mol (mol OM) <sup>-1</sup> s <sup>-1</sup> ( $\times 10^9$ ))
As	7.78	-	-
Mo	0.69	-	-
Hg	0.019	-	-
Co	4.32	-	-
Ni	7.78	318	70.5
Cu	8.35	25.4	25.4
Cr	11.81	-	-
Zn	27.36	24.2	23.1
Cd	6.05	0.301	0.163
Pb	3.17	0.648	2.31

from microniche authigenic oxide sources rather than a gradual release from organic matter as it is oxidised by sulphate. The proportionally greater enrichment of observed Fe and Mn over their background values, than the trace metals (Motelica-Heino et al, 2003), gives further emphasis to this possible mechanism. If essential elements are taken up by the mediating bacteria, localized depletions in trace element concentrations may be expected. Localized low concentrations of phosphate and vanadium associated with sulphidic microniches were attributed to potential uptake by microniche bacteria (Stockdale et al, 2008a). Interpretation of DGT observed data should include an assessment of the potential effects induced by the device in its immediate vicinity (i.e. within 1-2 mm of its surface). For example, less sulphide will diffuse into the surrounding sediment from a microniche if it is adjacent to a DGT device, which removes some of the sulphide. Consequently there will be less sulphide available for chemical oxidation by authigenic oxides in the ambient sediment, which may result in lower trace metal release from these sources. Under unperturbed conditions, chemical reduction of ambient authigenic oxides by sulphide may promote a net diffusion of trace elements towards the niche, increasing their significance in terms of trace metal sulphide formation.

### 3.4.3. Trace Element Reaction Pathways

Studies of molybdenum sulphide reactions provide examples of how the concentration of sulphide may affect the initial processes that act as a precursor to pyritization, such as chemical reactions with sulphide and adsorption of sulphidic forms. Zheng et al (2000) found that a threshold sulphide concentration of  $\sim 10^{-7} \text{ M}$  had to be exceeded before Mo co-precipitates with Fe-S. Direct Mo precipitation (as Mo-S or particle bound Mo) required a sulphide

Table 5. Trace metal sulphide solubility products<sup>a</sup> for the least crystalline sulphide of each metal. Metal released from a microniche over 60 seconds<sup>b</sup> and trace metal saturation thresholds<sup>c</sup>.

Metal sulphide	$K_{sp}$	Activity coefficients <sup>d</sup> ( $\gamma_{Me^{2+}}$ )	Metal release at microniche (M)	Saturation threshold (M)
FeS(am)	$1.12 \times 10^{-3}$	0.255	-	$7.34 \times 10^{-7}$
CoS( $\alpha$ )	$3.98 \times 10^{-8}$	0.260	$1.3 \times 10^{-9}$	$2.56 \times 10^{-11}$
NiS( $\alpha$ )	$3.16 \times 10^{-6}$	0.268	$2.3 \times 10^{-9}$	$1.97 \times 10^{-9}$
CuS	$5.37 \times 10^{-23}$	0.220	$2.5 \times 10^{-9}$	$4.08 \times 10^{-26}$
ZnS(am)	$9.55 \times 10^{-10}$	0.266	$8.2 \times 10^{-9}$	$7.06 \times 10^{-13}$
CdS(am)	$1.00 \times 10^{-13}$	0.641	$1.8 \times 10^{-9}$	$2.61 \times 10^{-17}$
HgS	$3.16 \times 10^{-39}$	0.250	$5.7 \times 10^{-12}$	$2.11 \times 10^{-42}$
PbS(galena)	$5.62 \times 10^{-13}$	0.312	$9.5 \times 10^{-9}$	$3.01 \times 10^{-16}$

<sup>a</sup>Solubility products for the reaction  $MS_{(s)} + H^+ \leftrightarrow M^{2+} + HS^-$ .  $K_{sp}$  values from Huerta-Diaz et al (1998, and references therein), except HgS, from Di Toro et al (1992, and references therein). <sup>b</sup>Assuming niche has an OM concentration of 5 M and applying values for non-metal oxide electron acceptors from Table 4. <sup>c</sup>Trace metal saturation thresholds are the minimum metal concentrations required for saturation conditions to be met. These calculations assume a pH of 7, a peak total sulphide concentration of  $2 \times 10^{-3}$  M (met by all simulations except c, d and i; additional activity coefficients used were,  $\gamma_{H^+} = 0.958$  and  $\gamma_{HS^-} = 0.410$ ). <sup>d</sup>Activity coefficients were calculated from the Pitzer equation and variables reported in Millero and Schreiber (1982), except Hg which is an assumed value.

concentration exceeding  $\sim 10^{-4}$  M. A study by Erickson and Helz (2000) on Mo speciation in sulphidic waters (Black Sea) suggested that at a sulphide concentration of  $\sim 1.1 \times 10^{-5}$  M, molybdate ( $MoO_4^{2-}$ ) is converted to tetrathiomolybdate ( $MoS_4^{2-}$ ) without yielding significant concentrations of intermediates. Tetrathiomolybdate has been shown to adsorb more strongly than molybdate to pyrite in anoxic sediments (Bostick et al, 2003). Helz et al (2004), suggested that potential diffusion of Mo into sulphidic microenvironments and subsequent fixation could be misinterpreted as fixation at low ambient sulphide concentration.

All of the scenarios we have modelled result in sulphide peaks (at the niche centre) greater than  $10^{-3}$  M. This suggests that Mo within, or diffusing to, microniches will precipitate directly rather than co-precipitate with FeS. Analogous thio intermediates to Mo have been identified for arsenic (Wallschläger and Stacey, 2007) indicating that the sulphide reaction mechanisms may also be analogous. This is also suggested by the reported similarity in their DTMP versus DOP data (Figure 1). Microniches may therefore also have a similar impact on arsenic diagenesis. The summary of the metal sulphide reaction mechanisms suggested in Morse and Luther (1999) shown in Table 1, indicates that several different pathways exist for trace element reactions with sulphide. In addition to these mechanisms Di Toro et al (1990; 1992), have shown that Cd can undergo a displacement reaction with FeS to form a cadmium sulphide precipitate. They propose that similar reactions operate for other metals with lower sulphide solubility products than FeS (i.e. for Hg, Pb, Zn and Ni). At microniches, sulphide reactions of these trace elements as they diffuse into the niche from the ambient sediment may be more likely to be controlled by the displacement mechanism, as once established the FeS peak will be encountered before the sulphide peak in most of the modelled scenarios (as shown by the 2D images in Figure 4). Metal concentrations within the niche may be controlled by a balance between the relevant reactions and a combination of removal by direct sulphide

precipitation and the displacement mechanism, depending upon the niche lifetime and therefore the FeS concentration.

#### 3.4.4. Trace Element Sulphide Solubility

Table 5 shows the solubility products and saturation thresholds of several trace metal sulphides for the reaction of the metal with bisulphide. The saturation thresholds represent the concentration of metal that needs to be exceeded for supersaturation conditions to exist at the centre of the niche (where the sulphide peak is observed). These values were calculated assuming a pH of 7 and a peak sulphide concentration of  $2 \times 10^{-3}$  M, which is met in all of the modelled scenarios except c, d and i (where peak total sulphide concentrations are  $4.6 \times 10^{-4}$ ,  $8.7 \times 10^{-4}$  and  $1.6 \times 10^{-3}$  M respectively). The low solubility of many of these sulphides coupled with the very high peak sulphide concentrations, results in threshold concentrations of metals below  $2 \times 10^{-9}$  M for all sulphides except iron. When comparing these thresholds with the potential release of trace metals from OM (Table 5; assuming a OM concentration of 5 M and a 60 second time period), it is tempting to suggest that the release from organic matter within the microniche may be sufficient to buffer the element concentrations above the threshold values. However, this will depend on the reaction rates between trace elements and sulphide, the removal rate to other sinks (e.g. adsorption) and the extent to which trace elements in the OM are utilised by the bacteria facilitating the decomposition. Given the high sulphide concentration and the continuous release of trace elements, it is possible that there will be continuous trace metal sulphide formation throughout the lifetime of the niche. Where a niche exists in a zone of ambient authigenic oxide degradation, additional trace metal may be supplied to the niche. Trace element release from the authigenic oxides reduced during OM oxidation in the bulk sediment will be approximately a thousand times less than those values quoted for degradation at microniches in Table 4 (Based on the Multi-G rates from Fossing et

al, 2002). Despite this, the supply of some elements from this external source will still far exceed the microniche-OM supply due to the high concentrations associated with the oxides. This is particularly the case for Ni.

Sulphide evolution in particles above 1 mm in diameter within the oxygen and nitrate reduction zones has also been predicted (Sochaczewski et al, 2008). Faecal pellets and other microniche may be important zones of FeS and trace metal sulphide formation in sediments and provide mechanism for metal removal within the oxic and suboxic zones, where formation of sulphides would not be predicted by analysis of the bulk sediment.

### 3.5. Other Considerations

#### 3.5.1. Explaining the Fe(II) Profiles

Exclusion from our model of typical parameters, such as those that account for bioirrigation and biodiffusivity, is appropriate given the nature of our modelling. It may be reasonable to expect that in a real system there will be small zones where these parameters have no or little effect, at least over time scales of a few days. In our simulations the concentration of Fe(II) can build up to levels much higher than if these parameters were included (Figure 4b). The presence of fixed boundaries at the top and bottom of the domain result in an imposed flux out of the domain. In a heterogeneous system with bioturbation, there are likely to be localized zones where solutes diffuse toward secondary interfaces, such as burrows. We accept that our modelled scenarios may be simplistic in the treatment of such behaviour. However, the small-scale modelling we have attempted is not open to the treatment of bioturbation and irrigation as averaged processes. In using diagenetic data from a combined experimental and modelling study we have excluded any fitting parameters for bioturbation processes in order to give results that reflect what may occur at and around microniches.

It has been suggested that for microniches greater than 100  $\mu\text{m}$  diameter formed from rapidly metabolising soft tissue, the greater the production of sulphide (from either larger niches or higher sulphate reduction rates), the higher the concentrations of porewater iron required in order to confine FeS precipitation to the decay site (Raiswell, 1993; Raiswell et al, 1993; 2008). Thus the complexity of the effect of the iron concentration is governed not only by the bulk concentration, but also by the local concentration, the OM microniche radius, and the OM degradation rates for both the niche (affecting sulphide production) and the bulk sediment (affecting porewater Fe in sediment zones where iron (oxyhydr)oxides are the dominant electron acceptor). The effect of lower iron concentrations on pyrite precipitation at microniches has been investigated experimentally (Allen, 2002).

#### 3.5.2. Influence of Microniche pH

For simplicity we have assumed a microniche pH of 7 for all calculations in this work. However, complex distributions of pH may occur at microniches, Zhu et al (2006) observed pH at a dead decaying organism of  $\leq 5.9$ , where the ambient pH

was  $\sim 6.6$ . Diffusion of protons away from the niche results in a concentration gradient extending from the niche. As pH becomes lower IAP's are reduced by two contributing factors. Firstly, the pH term in the denominator of the equation, and secondly the equilibrium of sulphide species is shifted towards the  $\text{H}_2\text{S}$  species. The result will be to reduce the formation rate for sulphides at the centre of the niche. As the proton concentration gradient extends from the niche, this effect may enhance FeS formation at the niche edges and result in more contrast in the halo effect.

#### 3.5.3. Potential Influence of Diffusive Barriers Around Microniches

In the modelling reported here we have assumed that solute transport into and from the niche is controlled exclusively by diffusion (accounting also for the changes to diffusion coefficients induced by porosity changes). Microniches in nature (including faecal pellets and decaying organisms) will have a range of diffusional barriers which will retard or prevent diffusion across the niche edge. Faecal pellets may possess peritrophic membranes, dead tube dwelling organisms may have a mucus membrane lining the burrow wall at its edge, soft parts of shelled organisms will only have limited exposure to the bulk sediment, and decaying organisms with hard-parts may have complex structures that affect diffusion (see also Stockdale et al, 2008). Where precipitates form surrounding a niche, it is possible that this will create a barrier to diffusion. How diffusive restrictions affect the formation of sulphide precipitates will largely depend upon the resupply of sulphate to the niche interior. In a scenario where diffusion is restricted yet sufficient to resupply sulphate, restriction in the efflux of sulphide will reduce the porewater Fe concentrations that is required for precipitation at the niche edge, consistent with the conclusions of Raiswell et al (1993) discussed in section 1.3.

## 4. CONCLUSIONS

We have modelled the behaviour of sulphide and iron within microniches with a range of OM degradation rates and porosities. For all of the modelled scenarios the ion activity product for iron sulphide far exceeds the solubility product, indicating conditions for FeS precipitation in all niches. Those simulations within the  $t_{35\%}$  range of 2.5 to 5 days gave comparable concentration ratios of sulphide to iron in solution within the particles to experimentally observed values.

Whilst it was not the aim of this work to specifically investigate processes occurring at microniches in terms of the preservation of OM in the paleo record, it is evident that the modelled data can inform such studies. The model can predict the conditions that result in preferential deposition of precipitates at the edge of microniches. Decreasing porosity, lower  $t_{35\%}$  values and increasing OM degradation rates all tend to increase the likelihood that peak iron sulphide precipitation will preferentially occur at the edges of the niche rather than uniformly throughout its volume.



It is likely that both the elevated sulphide and localized zones of FeS will have a significant effect on the diagenesis of trace metals. If microniches comprise a small but significant volume of the oxic and suboxic sediment they may exert an influence on the whole system that would not be predicted if only the bulk sediment was considered. The peak sulphide concentrations modelled here are significantly in excess of all of the critical reaction concentrations observed for molybdenum (these reactions include: co-precipitation with FeS, direct Mo precipitation and direct conversion of molybdate to tetrathiomolybdate). Trace metals available for reaction with sulphide can be supplied by: 1) generation within the particle by release from the degrading OM, 2) inward diffusion from the surrounding sediment, particularly where the Fe/Mn oxides in ambient sediment are the electron acceptors for OM oxidation, or 3) a combination of the two processes. For elements forming sulphide precipitates, the conditions required will evolve quickly (minutes) after the niche is introduced. Over time (hours) the FeS concentration will increase, allowing those elements that can undergo displacement reactions to do so in increasing proportions. As the FeS occurs at most microniches as a halo, the displacement reactions will occur preferentially within this zone.

#### ACKNOWLEDGEMENTS

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#### Supporting information

Additional tables and material, as referred to in the text, are available online at <http://www.sciencedirect.com>

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**Sulphide evolution from faecal pellets and other microniches within sub oxic surface sediment: The effects on the geochemistry of iron and trace elements**

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**Supporting Information**

## Additional tables

Table S1. Model parameters.

Parameter	Value	Reference	
Domain	x,y,z: 0.7, 0.7, 1.0 cm		
Resolution <sup>a</sup>	0.052		
Bulk porosity (entered as finite values in the 3d model)	$\phi = 0.832$	(1)	
Tortuosity option	Iversen- Jørgensen. $n = 2.79$		
Diffusion coefficients at 10°C	$\text{NH}_4^+$	$13.7 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$	(1)
	$\text{SO}_4^{2-}$	$7.22 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$	(1)
	$\Sigma\text{H}_2\text{S}$	$11.8 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$	(1)
	Mn	$4.57 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$	(2)
	Fe	$4.48 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$	(2)
Boundary conditions <sup>b</sup>			
U = Upper (0.67 cm below SWI)			
L = Lower (1.67 cm below SWI)			
	$[\text{O}_2]$	U & L 0 $\mu\text{M}$	(1)
	$[\text{NO}_3^-]$	U & L 0 $\mu\text{M}$	(1)
	$[\text{NH}_4^+]$	U 36 $\mu\text{M}$ ; L 83 $\mu\text{M}$	(1)
	$[\text{Fe}^{2+}]$	U 56 $\mu\text{M}$ ; L 91 $\mu\text{M}$	(1)
	$[\text{Mn}^{2+}]$	U 70 $\mu\text{M}$ ; L 60 $\mu\text{M}$	(1)
	$[\text{SO}_4^{2-}]$	U & L 2000 $\mu\text{M}$	(1)
	$[\Sigma\text{H}_2\text{S}]$	U & L 0 $\mu\text{M}$	(1)
Limiting concentrations (Niche = 2% of bulk value)			
	$[\text{MnO}_2]$	Bulk $1.02 \times 10^5 \mu\text{M}$ Niche $2.04 \times 10^3 \mu\text{M}$	(1)
	$[\text{FeOOH}]$	Bulk $2.04 \times 10^5 \mu\text{M}$ Niche $4.08 \times 10^3 \mu\text{M}$	(1)
Rate constants	$k_{\text{OM-s}}$	$1.2 \times 10^{-8} \text{ s}^{-1}$	(1)
	$k_{\text{OM-f}}$	See Figure 2	
	$k_6$	$2.5 \times 10^{-6} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_7$	$1.5 \times 10^{-5} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_8$	$5.0 \times 10^{-4} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_9$	$1.7 \times 10^{-8} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_{10}$	$2.0 \times 10^{-8} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_{11}$	$3.0 \times 10^{-9} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_{12}$	$7.5 \times 10^{-7} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_{13}$	$6.0 \times 10^{-7} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)
	$k_{14}$	$5.0 \times 10^{-5} \mu\text{M}^{-1} \text{ s}^{-1}$	(1)

(1) Fossing et al (2002, 2004). (2) Li and Gregory (1974). <sup>a</sup>See Sochaczewski et al (2008) for a full description of the resolution and mesh density. <sup>b</sup>Boundaries are based on the 1D profiles from (1).

Table S2. Trace metal fractions associated with Fe and Mn oxides used in calculations for Table 4 (values are the Tessier et al, 1992, values divided by 2.5. See main manuscript for explanation of this adjustment.

Metal	MnO <sub>2</sub>	FeOOH
	(mol mol <sup>-1</sup> )	
Ni	$5.52 \times 10^{-2}$	$6.12 \times 10^{-3}$
Cu	$4.40 \times 10^{-3}$	$2.20 \times 10^{-3}$
Zn	$4.20 \times 10^{-3}$	$2.00 \times 10^{-3}$
Cd	$5.12 \times 10^{-5}$	$1.36 \times 10^{-5}$
Pb	$1.12 \times 10^{-4}$	$2.00 \times 10^{-4}$

### Zinc-sulphide modelling

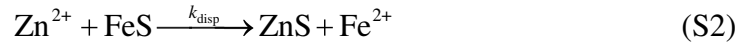
Whilst modelling of general trace metal-sulphide interactions is limited, several studies have attempted to model zinc-sulphide reactions. Druschel et al (2002) modelled zinc sulphide (ZnS) formation (precipitation) in sulphate reducing biofilms within flooded mine tunnels under conditions where the biofilm is exposed to a continuous flow of water containing high dissolved zinc concentrations (~1.4 ppm). Under these conditions it is suggested that, provided Zn<sup>2+</sup> is introduced faster than sulphide is generated, ZnS precipitation should occur to the exclusion of FeS. Such conditions will not exist at sedimentary microniches where Fe<sup>2+</sup> concentrations will be orders of magnitude higher than Zn<sup>2+</sup> and where sulphide concentrations have been observed to be over 40 times higher than those of Fe<sup>2+</sup> (Motelica-Heino et al, 2003).

Canavan et al (2007) modelled (and measured) trace metal behaviour in a freshwater sediment using a two reaction approach to ZnS formation. The first was a precipitation reaction (Eq. S1), where  $k_{\text{ZnS-precip}}$  is a rate constant ( $3.17 \times 10^{-18} \text{ mol g}^{-1} \text{ s}^{-1}$ ) and  $K_{\text{ZnS(sp)}}$  is the equilibrium constant ( $10^{-9.02}$ ). Both constants were used as model fitting parameters and this reaction was not allowed to proceed when ZnS was

undersaturated. This reaction is analogous to the iron sulphide precipitation/dissolution reactions used by van Cappellen et al (1993).

$$\text{ZnS}_{\text{precip}} = k_{\text{ZnS-precip}} \left( \frac{[\text{Zn}^{2+}][\text{HS}^-]}{[\text{H}^+]} K_{\text{ZnS(sp)}} - 1 \right) \quad (\text{S1})$$

Secondly a displacement reaction is used (Eq. S2).



Canavan et al (2007) assumed the rate constant for Equation S2 had first order kinetics (first order for  $\text{Zn}^{2+}$ ) and this value was also used as a fitting parameter. Experimental evidence for reactions that displace iron has been reported (Di Toro et al, 1992; and references therein).

Choi et al (2006) modelled sulphur dynamics in a vegetated wetland sediment and assumed Equation S2 was the only ZnS formation mechanism. They used a second order rate constant for  $k_{\text{disp}}$ . The rate constant was assumed to be equal to the constant for the formation of FeS from  $\text{Fe}^{2+}$  and  $\Sigma\text{S(II)}$ . Using this single reaction approach may not be appropriate for modelling zinc/sulphide reactions at fresh microniches, as it requires FeS to form prior to ZnS, which contradicts the reported faster water exchange kinetics of  $\text{Zn}^{2+}$  compared to  $\text{Fe}^{2+}$  (Morse and Luther, 1999). These modelling examples indicate the complexity of modelling trace metal dynamics in sulphidic sediments.

### **Additional references**

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#### **4 Conclusions**

The principal aim of this thesis was to further our understanding of processes occurring at microniches. The objective was carried out by experimental work using DGT to measure concentrations of anions at a sulphidic niche in sediments and by modelling the sulphide evolution and associated geochemistry at an idealised spherical niche within sediment, using a comprehensive data set.

A review of previous microniche research has shown that our understanding of sedimentary diagenesis has been somewhat oversimplified by analysis at a larger, spatially averaged, scale and that the lack of congruent analysis makes it difficult to interpret these data in terms of specific geochemical processes. Using a new binding phase that allows co-analysis of sulphide, phosphate and the trace anions, arsenate and vanadate, has shown that depletions in anions occur at a microniche of elevated sulphide. Phosphate uptake associated with elevated activity of sulphate reducing bacteria has been demonstrated. Further work is required to determine if bacterial uptake, use by bacteria as an electron acceptor, reduction by sulphide and subsequent scavenging, or other processes are responsible for the observed depletions associated with sulphide production.

Using a three-dimensional diagenetic model, simulation of the hypothetical cases of microniches in the near surface sediment showed that, for the conditions selected, sulphide was readily generated, provided the microniche diameter was greater than 1 mm. In scenarios that were shown to be relevant to experimental observations reported in the literature, the behaviour of sulphide and iron within microniches with a range of degradation rates and porosities was modelled. For all of the modelled



scenarios, the ion activity product for iron sulphide far exceed the solubility product, indicating conditions for FeS precipitation in all niches. Decreasing porosity, lowering niche life-times and increasing OM degradation rates all tend to increase the likelihood that peak iron sulphide precipitation will preferentially occur at the edges of the niche rather than uniformly throughout its volume. It is likely that both the elevated sulphide and localized zones of FeS will have a significant effect on the diagenesis of trace metals. For elements that can form sulphide precipitates, the conditions required will evolve quickly (minutes) after the niche is introduced. Over time (hours) the FeS concentration will increase and those elements that can undergo displacement reactions will do so increasingly, as the rate of displacement is related to the FeS concentration.

## **5 The wider significance of microniche processes and future priorities**

Research into the geochemistry and significance of microniches has, to date, been very piecemeal, with a tendency to have single unrelated research papers, often separated by several years and covering different sedimentary environments. This thesis has reviewed much of this body of work and includes three research papers dedicated to microniche geochemistry. Given that this information is collated into one volume here, it is worthwhile additionally providing an opinion on the possible rationales for this research, and suggestions for the key areas of future studies. As this synthesis includes speculative assessments of numerous studies, it is included at the end of all investigative material to avoid any conflict with the thesis conclusions.

Firstly it is important to stress again that bioturbation is likely to be an important prerequisite for microniche formation, as it accounts for their distribution. In non-

bioturbated environments, such as in euxinic sediment with varve deposits, clear horizontally homogeneous patterns exist that can be explained by considering the system in one-dimension. One of the key questions when considering the significance of microniches on other aspects of geochemistry is: are they important to long-term processes such as mineral formation, particularly trace element sulphides, and do we need to consider this when assessing paleoredox proxies? Clearly, in microniches where no sulphide evolution exists, changes will occur to local profiles of oxidants and OM degradation products, such as  $\text{NH}_4^+$  and  $\text{CO}_2$ . However, trace element release under these circumstances is unlikely to be under conditions where they are irreversibly immobilised locally or permanently converted to the mineral phase.

Table 1 highlights the characteristics of both sediments and microniches that may affect the ultimate significance of microniche processes. Of these characteristics, the most important in terms of trace metal sulphide formation will be those that allow for sulphide evolution within the niche, together with those that control the potential reversibility of the metal sulphide formation reactions.

Once a niche is no longer generating sulphide internally, and where ambient conditions are not sulphidic, the localized system will become substantially undersaturated for metal sulphides. The loss of precipitated trace elements (e.g. ZnS) and bound anionic sulphide species (e.g.  $\equiv\text{MoS}_4$ ) from a niche will be controlled by a number of factors. 1) The rate constant of the dissolution reaction. 2) Factors that may inhibit reverse reactions such as interactions with other solid phases. 3) The duration of the undersaturation event (i.e. translocation of the microniche by the actions of biota).

For many trace element sulphides it is unlikely that the reactions are fully reversible, as conditions 1) to 3) will not always be favourable.

### 5.1 Improving model predictions and use of organic matter degradation rates

Modelling of sediment systems in 1D generally utilises a Multi-G approach. By allowing the specification of a near-surface, fast reacting pool of OM imposed onto a more evenly distributed slow reacting pool, more accurate model results have been achieved for solute distributions. However, the fast reacting pool is considered as horizontally homogeneous and thus a universal rate constant is applied. Consider a situation where this pool consists entirely of microniches, with a depth distribution of decreasing particle density away from the sediment water interface. It would be reasonable to expect some of the niches to exist below the  $O_2$  and  $NO_3^-$  penetration depths, and that some particles within these upper redox zones will have conditions whereby these oxidants become limiting. This may result in the following effects. Firstly, sulphide will be produced in zones where it is not expected. Often models use fixed constants for biological processes such as biodiffusion or irrigation to explain such observations. The existence of microniches requires an additional consideration. Secondly, 1D models do not take into account that some of the fast reacting OM may be oxidised by electron acceptors other than  $O_2$  and  $NO_3^-$ . For the profiles of  $O_2$  and  $NO_3^-$  measured in 1D, to be comparable to those modelled in 3D environment, requires that either, the pool size of fast reacting OM is increased, or that the reaction rate of OM (within these redox zones) is increased. These adjustments are required in order to balance the  $O_2$  and  $NO_3^-$  consumption rates and therefore to maintain their vertical profiles.

## 5.2 Priorities for future work

In order to gain a better understanding of microniche process and their significance in terms of trace element sulphide sinks, there are, in my view, three key questions to be addressed.

1. The distribution and translocation of microniches needs to be investigated. Use of planar probes such as DGT and planar optodes may encourage preferential burrowing adjacent to the device. This can be an advantage when studying the actual geochemical processes. However, it cannot give accurate quantitative data for the entire volume of sediment due to this effect. Other techniques need to be employed to determine actual distributions of niches. Gridded deployment of needle electrodes for analysis of solutes such as sulphide, may yield some useful information. Although, the limitations of these types of probes, as discussed in Paper I, will apply.

2. In sulphate reducing microniches the effect of the pH decrease within the niche needs to be quantified. The change in pH will reduce the degree of saturation of the trace element sulphides and thus the rate at which precipitation occurs. In microniches at locations where sulphide does not evolve, e.g. in the oxic zone, this pH effect may influence other mineral phases such as carbonates.

3. The relative reversibility of trace element sulphide formation is an important consideration when assessing the significance of microniches, and good progress has been made in understanding how these processes are controlled for molybdenum. Further data is required for other trace elements and additional effects of processes such as surface adsorption or formation of organic coatings need to be investigated.

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## **Appendix A**

### **Description of characteristic response time in relation to DGT and the DIFS models, and the derivation of the related equations.**

DGT (diffusive gradients in thin-films) has been used for the measurement of Fe, Mn and trace metals in both freshwater (Motelica-Heino et al, 2003) and marine sediments (Fones et al, 2004). DGT measured concentration is only representative of porewater concentration when there is sufficient resupply from the solid phase to replenish the depleted porewater. A more typical scenario during DGT deployment is that there is a partial resupply from the solid phase. In these situations DGT measurement is best treated as an assessment of the solute that can be supplied locally in response to a perturbation. Cases of insufficient resupply have been considered previously for sediment DGT analysis (Zhang et al, 2002).

The DIFS (DGT induced fluxes in sediments) models were developed to yield numerical solutions to these dynamic systems. Two models have been developed using one-dimensional (Harper et al, 2000) and two-dimensional (Sochaczewski et al, 2007) diffusion. The DIFS models use a single pool of trace metal linearly distributed between the aqueous and sorbed phases (with distribution coefficient  $K_d$ ). The kinetics are accounted for by adsorption and desorption rate constants ( $k_f$  and  $k_b$ ) with transport within the system controlled by diffusion. DIFS has been used to assess resupply in saturated soils (e.g. Ernstberger et al, 2002; 2005) and recent work has applied DIFS to contaminated freshwater reservoir sediments (Roulier et al, 2008).

## Theory

For an equilibrium reaction of the form shown in Equation 1 the change in concentration of B over time can be expressed as a differential equation (Eq. 2).



$$\frac{d[B]_t}{dt} = k_f [A]_t - k_b [B]_t \quad (4)$$

Solving this equation gives the following result.

$$[B]_t = \frac{k_f P}{(k_f + k_b)} (1 - e^{-(k_f + k_b)t}) + [B]_i e^{-(k_f + k_b)t} \quad (5)$$

Where  $P$  is the sum of the initial concentrations of A and B,  $[B]_i$  represents the initial concentration of B and  $[B]_t$  is the concentration of B after time,  $t$ . As the pool size ( $P$ ) and the rate constants ( $k_f$  and  $k_b$ ) are unchanged throughout the reaction, the equation can be simplified (Eq. 4).

$$[B]_t = x(1 - e^{-(k_f + k_b)t}) + [B]_i e^{-(k_f + k_b)t} \quad (6)$$

If at time zero,  $[B]$  is zero, the equation can be further simplified (Eq. 5).

$$[B]_t = x(1 - e^{-(k_f + k_b)t}) \quad (7)$$

As  $t$  approaches  $\infty$ , the exponential term approaches zero and  $[B]$  approaches equilibrium (i.e. the maximum value). When the sum of  $k_f$  and  $k_b$  equals the reciprocal of  $t$  (Eq. 6), the exponential term becomes  $e^{-1}$  and the concentration of B is 63% ( $1 - e^{-1}$ ) of the equilibrium value.

$$k_f + k_b = t_c^{-1} \quad (8)$$

Thus, the relationship in Eq. 6 can be seen as a characteristic response time of the system to approach equilibrium. If  $k_f \gg k_b$  then Eq. 6 simplifies to Eq. 7.

$$k_f = t_c^{-1} \quad (9)$$



The distribution coefficient  $K_d$  can be directly related to the partitioned concentrations and the sorption/desorption rate constants (Eq. 8). Where  $p_c$  is the particle concentration.

$$K_d = \frac{C_{sorbed}}{C_{solution}} = \frac{k_f}{k_b p_c} \quad (10)$$

Combining Equations 7 and 8 gives the relationship between the characteristic response time, the desorption rate constant and the partition coefficient (Eq. 9).

$$t_c = \frac{1}{K_d k_b p_c} \quad (11)$$

These relationships defined above allow the sorption/desorption rate constants to be calculated from the DIFS fitted  $t_c$  and  $K_d$  values.

## Full step-wise derivations

Solving the equilibrium value of a zero order reaction of the form:



Let:  $[A]_i$  represent the initial value

$[B]_t$  represent the value at time t

$P$  represent the concentration of the entire pool of A and B, i.e.

$$P = [A]_i + [B]_i \quad (A2)$$

The changes in concentration of the components can be expressed as:

$$-\frac{d[A]}{dt} = \frac{d[B]}{dt} = k_f[A]_t - k_b[B]_t \quad (A3)$$

The concentration of A at time t can be expressed as:

$$[A]_t = [B]_i - [B]_t + [A]_i \quad (A4)$$

The concentration of A being proportional to the initial value of A minus any loss due to formation of B (i.e. initial B minus B at time t)

Substituting Equation A4 into A3 gives:

$$\frac{d[B]}{dt} = k_f([B]_i - [B]_t + [A]_i) - k_b[B]_t \quad (A5)$$

$$= k_f[B]_i - k_f[B]_t + k_f[A]_i - k_b[B]_t \quad (A6)$$

rearranging A2 and substituting for  $[A]_i$  gives:

$$= k_f[B]_i - k_f[B]_t + k_f(P - [B]_i) - k_b[B]_t \quad (A7)$$

$$= k_f[B]_i - k_f[B]_t + k_fP - k_f[B]_i - k_b[B]_t \quad (A8)$$

Which simplifies to:

$$= k_fP - (k_f + k_b)[B]_t \quad (A9)$$

Multiplying the first expression by Equation A10:

$$\frac{(k_f + k_b)}{(k_f + k_b)} (=1) \quad (\text{A10})$$

gives:

$$\frac{d[\text{B}]}{dt} = \frac{k_f P(k_f + k_b)}{(k_f + k_b)} - (k_f + k_b)[\text{B}]_t \quad (\text{A11})$$

$$= (k_f + k_b) \left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_t \right) \quad (\text{A12})$$

$$\frac{d[\text{B}]}{\frac{k_f P}{(k_f + k_b)} - [\text{B}]_t} = (k_f + k_b) dt \quad (\text{A13})$$

Integration of:

$$\int_t^i \frac{d[\text{B}]}{\frac{k_f P}{(k_f + k_b)} - [\text{B}]_t} = (k_f + k_b) \int_t^0 dt \quad (\text{A14})$$

Gives:

$$-\left[ \ln \left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_t \right) - \ln \left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_i \right) \right] = (k_f + k_b)t \quad (\text{A15})$$

$$-\left[ \ln \left( \frac{\left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_t \right)}{\left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_i \right)} \right) \right] = (k_f + k_b)t \quad (\text{A16})$$

$$\frac{\left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_t \right)}{\left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_i \right)} = e^{-(k_f + k_b)t} \quad (\text{A17})$$

$$\frac{k_f P}{(k_f + k_b)} - [\text{B}]_t = \left( \frac{k_f P}{(k_f + k_b)} - [\text{B}]_i \right) e^{-(k_f + k_b)t} \quad (\text{A18})$$

$$\frac{k_f P}{(k_f + k_b)} - [B]_t = \frac{k_f P}{(k_f + k_b)} e^{-(k_f + k_b)t} - [B]_i e^{-(k_f + k_b)t} \quad (\text{A19})$$

$$[B]_t = \frac{k_f P}{(k_f + k_b)} - \frac{k_f P}{(k_f + k_b)} e^{-(k_f + k_b)t} + [B]_i e^{-(k_f + k_b)t} \quad (\text{A20})$$

Giving the final solution:

$$[B]_t = \frac{k_f P}{(k_f + k_b)} (1 - e^{-(k_f + k_b)t}) + [B]_i e^{-(k_f + k_b)t} \quad (\text{A21})$$

As the total pool size and the rate constants are the same at any point in the reaction the expression containing these can be substituted for a constant:

$$[B]_t = x(1 - e^{-(k_f + k_b)t}) + [B]_i e^{-(k_f + k_b)t} \quad (\text{A22})$$

### Special cases

Case 1.  $[B]_{t=0} = 0$

Equation A21 is simplified to:

$$[B]_t = x(1 - e^{-(k_f + k_b)t}) \quad (\text{A23})$$

Case 2.  $t \rightarrow \infty$

Allowing  $t \rightarrow \infty$  gives the maximum (or equilibrium) value, as the exponential function tends towards zero. i.e.  $[B] = x$

Case 3.  $k_f + k_b = t^{-1}$

Using Equation A23

The exponential function becomes  $e^{-1}$  giving the equation:

$$[B]_t = x(1 - 0.37) = 0.63x \quad (\text{A24})$$

As  $x$  represents the equilibrium concentration the 63% equilibrium response time can be calculated from the reciprocal of the sum of the forward and reverse rate constants.

*Using Equation A22*

If the system is not starting from a zero concentration of B then the initial concentration must be considered. This equation allows the time required to reach intermediate levels of equilibrium recovery to be calculated. For example if a system was at 80% at  $t = 0$  and 90% at  $t = y$  the elapsed time can be calculated.  $k_f + k_b = t^{-1}$  can also be shown to be the 63% recovery between the two equilibrium values.

## Appendix B

### 3D Sediment Model for Microniches (3D TREAD): A Practical User Guide

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#### *Contents:*

- |                                    |   |
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| 1. What is 3D TREAD?               | 6. Running a simulation                         |
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| 3. Installing and running 3D TREAD | 8. Creating new input files from existing files |
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| 5.3. Reaction input                |   |
- 

#### ***1. What is 3D TREAD?***

3D TREAD is a dynamic numerical diagenetic model for sediments, allowing specification of spherical zones with different geochemistry from the surrounding matrix (microniches). The flexible specification of components and reactions allows the user to define any required components. The full numerical framework and an example of the model application are described in the original paper presenting this model (Sochaczewski et al, 2008. Environmental Chemistry, 5, 218-225. (<http://dx.doi.org/10.1017/EN08006>)).

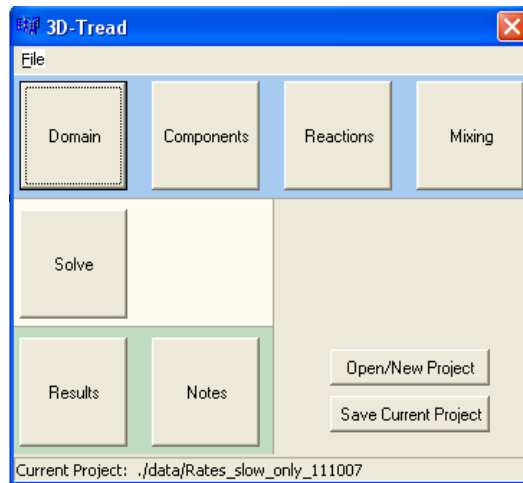
#### ***2. Requirements***

3D TREAD is a 32 bit application designed to run on Windows XP and Vista systems. Required disk space will vary depending on model inputs, a minimum of 500 MB free disk space is recommended. 3D TREAD has no other specific hardware requirements. However, a fast processor (at least 1.5GHz) and a minimum of 1GB of RAM is

recommended. The MathWorks programme Matlab is required for extracting output data.

### ***3. Installing and running 3D TREAD***

All required files are included in a zip file (downloadable from <http://www.es.lancs.ac.uk/wdgroup/index.htm>). Once the files are extracted the model can be run directly using the executable file 'sediment3d.exe'. This executable opens the graphical user interface (GUI) main menu, shown in Figure 1, which controls the input parameters.



**Figure 1.** The main menu – graphical user interface (GUI) for the 3D-TREAD model.

### ***4. Loading the GUI***

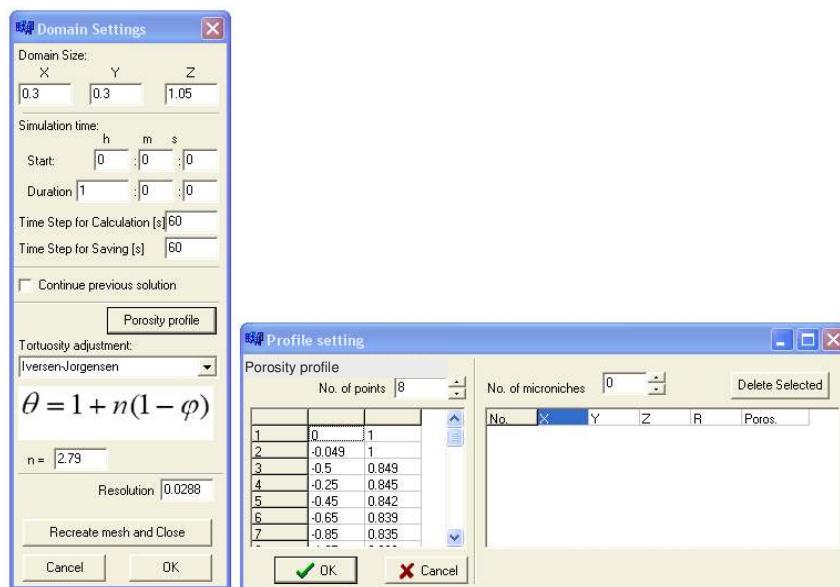
To start using the model run the executable file (sediment3d.exe). A folders/files dialogue box will appear whenever the model is started, allowing loading of a saved model. The path to the data folder will need to be set at the first use of the model ((place installed)/3DTREAD/data). Whenever the model is executed either, a previous file can be loaded, or a filename for a new model can be entered. Filenames must not contain any spaces. Once the name is set, or a saved model is selected, only the main menu will be shown. The active projects filename is shown at the base of this menu.

## 5. Input parameters

Each button along the top line of boxes in the main menu, opens up additional interface boxes for entering of specific parameters (domain, components, or reactions; the mixing functionality is currently under development and is not explained here).

### 5.1. Domain and porosity inputs

Figure 2 show the graphical interface for these input parameters, which can be opened by pressing the ‘Domain’ button in the main menu. The porosity profile setting box can be opened by pressing the ‘Porosity profile’ box in the ‘Domain’ box.



**Figure 2.** Domain and porosity input interfaces.

X, Y and Z, are the domain dimensions in cm. Typically, to obtain optimum results in minimal time a ‘pencil’ type approach to the domain shape has been used (e.g. x and y = 0.3, z = 1 cm). Duration is the length of time over which the simulation is required, numbers should be entered here as integers (start time has no effect on the simulation and can be ignored). ‘Time Step for Calculation’ allows specification of the interval



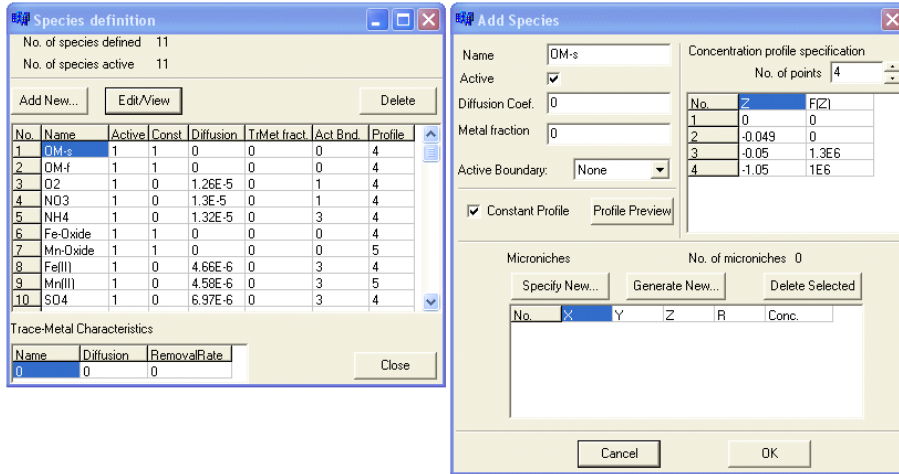
between each calculation (in s). ‘Time Step for Saving’ (s) allows the user to specify how often the output from the stepwise calculations are written to the output file. The value must be equal or greater than the calculation time step. It is crucial that these values are set to ensure that the last calculation of the model run is saved to the output files (e.g. specifying a 55 s runtime but a 10 s calculation time will result in the output being unreadable due to the lack of final values).

Several pre-set options are available for the specification of tortuosity-porosity relationships, including allowing user setting of the equation variables. For further details see Sochaczewski et al (2008) or the sources used; Boudreau (1997), and Boudreau and Meysman (2006). Porosity is entered as finite values in 3D TREAD not as equations. The user can specify any number of depth coordinates and the associated porosities as a list. For microniches the porosity should be specified as a single value, along with the coordinates and radius.

Resolution controls the density of the 3D mesh and thus the spatial resolution of the simulations. Lower resolutions will tend to result in niches with shallower concentration gradients at the niche edge. Setting too high a resolution will result in several problems: the node limitations of the software may be exceeded and the model will not run; the output file may become too large for Matlab to extract the data; or the simulation run-time will be greatly extended. As a rule of the thumb the maximum resolution can be set at: approximately the cube root of the domain volume ( $\sqrt[3]{(x \times y \times z)}$ ) divided by 15. Actual achievable resolution will depend upon the processing power of the computer and this estimate is only a guide.

## 5.2. Components input

Figure 3 shows the input interfaces for the modelled components.



**Figure 3.** Component input interface boxes.

By selecting the ‘Add New...’ button the ‘Add Species’ box is opened. Using this interface all of the component properties can be entered. The species name should not contain spaces. Diffusion coefficients should be entered in  $\text{cm}^2 \text{s}^{-1}$ . The 1D profiles for the component outside of the niche are entered by specifying a chosen number of points, and associated concentrations, throughout the z domain (depth coordinates should be specified as negative values and this rule applies to any depth specification throughout the model parameterisation). For microniches, the coordinates, radius and the concentration are required (microniche values are applied independently in the mesh specification and therefore zones of lower or higher concentration can be modelled for microniches). Boundaries can be specified as: only upper or lower, both, or no active boundary. Where boundaries are specified these are assumed to be fixed concentration (Dirichlet) boundaries and values are taken from the user specified concentration profiles. Where no boundaries are specified they are assumed to have a zero concentration gradient.

If an assumption of steady state is required to be applied to a component concentration, the ‘Constant Profile’ option can be selected. Using this option the concentrations are reset as the user specified initial conditions after each calculation time-step. (The ‘Trace-Metal Characteristics,’ ‘Active’ and ‘Metal fraction’ inputs are remnants of earlier versions and can be ignored). Once the species have been added, diffusion coefficients can be edited directly from the ‘Species definition’ interface, all other parameters can be edited using the ‘Edit/View’ button.

### 5.3. Reactions input

Figure 4 shows the input interface for specifying reaction stoichiometry and associated data for the modelled components.

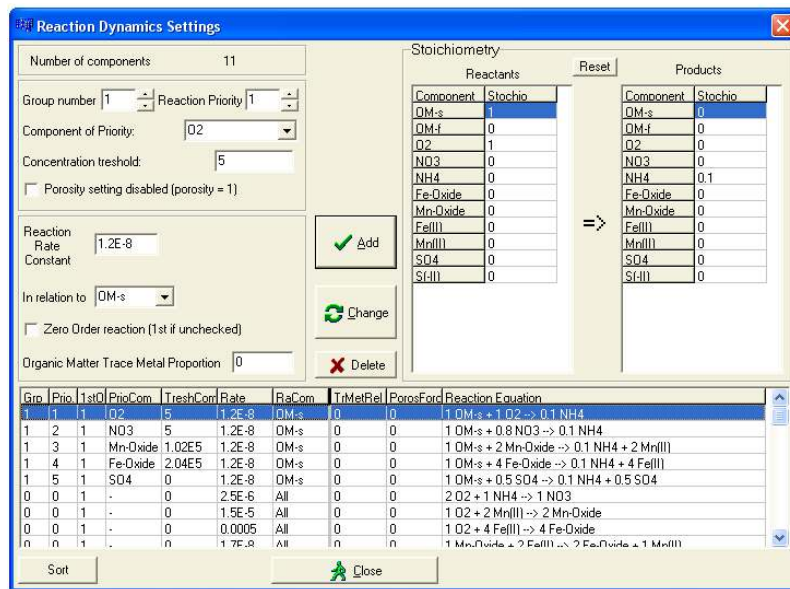


Figure 4. Reactions input interface boxes.

All the reactive species can participate in reactions that each have a set of user-specified values.

- Priority group number and reaction priority within this group. Organic matter fractions are typically given group numbers of 1, 2, etc., with the ‘Reaction

Priority' set according to the order of utilisation of the electron acceptors ( $O_2 = 1$ ,  $NO_3^- = 2$  etc.). Secondary reactions are typically given a group and priority of 0.

- For OM reactions reference component (oxidant) and the associated concentration threshold should be specified. (The 'Organic Matter Trace Metal Proportion' function is not active and can be ignored).
- Reaction rate constants for all reactions, with specification to which reactant it is related – i.e. OM in case of OM decomposition reactions, or all components for secondary reactions.
- Type of reaction kinetics (zero or first order).
- Chemical equation of the reaction (stoichiometric values).

Once all of the values for an individual reaction have been entered they can be saved by clicking the 'Add' button. To edit a reaction, highlight it in the list, make the required changes and save by clicking the 'Change' button. To create a new reaction similar to one that has been saved, select that reaction, make the required changes then click the 'Add' button.

## ***6. Running a simulation***

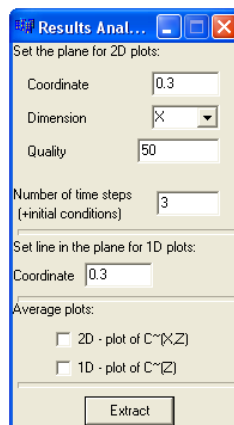
If the model is not to be run immediately the data can be saved manually by clicking the 'Save Current Project' button on the main menu. Otherwise, once all of the input and domain data have been entered clicking the 'Solve' button will automatically save all of the parameters to the appropriate files, hide the menu, and open a 'DOS – type' screen showing the progress of the model run. Once the run is complete the main menu will reappear and the results can be extracted. If an error message 'Solver Crash!!! Check Parameters' displays soon after clicking the 'Solve' button there may be parameters missing or the mesh density may be too high.

### *Continuing a previous solution*

If a model run requires a longer simulation than initially programmed it is not necessary to rerun the entire simulation. In the ‘Domain’ interface the ‘Continue previous solution’ box can be checked and the final solution concentration values for the previous solution will be applied as the initial model values. The run time (‘Duration’) can be altered before running the model. The mesh must be consistent, therefore the X, Y, Z and resolution parameters must not be changed. Once ‘Solve’ is pressed the previous results file will be overwritten. Therefore, all result extraction from the initial run must be performed before using this procedure.

### **7. The output file and extracting data**

Before using the ‘Results’ interface it is necessary to run Matlab and change the ‘Current Directory’ pathway to the 3D TREAD folder. Figure 5 shows the interface for selection of results for output and display. Plots can be set for either the x or y planes (versus depth – z).



**Figure 5.** Interface for selection of required output.

The coordinate set for the 2D plot will determine the location of the 2D plane. Combined with the 2D value, the coordinate for the 1D plot gives the x, y location of

the line plot. 'Quality' sets the number of coordinate plotted for each axis (maximum value of 256). For example if z is 1 cm long and the 'Quality' is set at 51 then the 1D plot will have data points at 0.2 mm intervals. The initial conditions are automatically plotted; the user can select how many, if any, intermediate time-steps are plotted (selecting a value of 1 for the 'Number of time steps' will only plot the final values; values greater than one will result in plots for values at intermediate time-steps). The 'Average plots' functions can be ignored. Once the values have been set, press the 'Extract' button. Then in Matlab run the 'plotresults.m' file (right click, then select 'run'). Matlab will generate a figure for each specified components. Each figure will contain both the 1D and 2D plots. As well as the figures, Matlab will also create a CSV file of all of the 1D plots for each component based upon the 'Quality' and 'Number of time steps' values. This file will be saved to the 'data' folder with the same filename as specified for the model run. If results are required for several coordinates for the same model run it is necessary to change the name of this file after each run, as otherwise it will be overwritten each time the results are extracted for a given model run.

### ***8. Creating new input files from existing files***

Instruction on how to create a new input file from an existing file. 1) Run the .exe file and open the existing file. 2) Click the 'Open/New Project' button. 3) Enter the required new filename. 4) Click 'Save' 5) Click 'Save Current Project'. 6) Open the 'Domain' box and click the 'Recreate mesh and Close' button (this creates a correctly named mesh file). The new file is ready and can be altered as required. If species need to be removed it is best to create a brand new file rather than using this procedure, this avoids problem with the species changing within specified reactions.

## 9. Supplementary information

### *Known issues*

After successful completion of some model runs (often for simulations with short runtimes, or where coarse mesh domains are used) an error message is shown. This message contains the text ‘The exception unknown software exception (0xc0000005) occurred in the application at location 0x00448e7e.’ Once this error box has been closed, a second error will be displayed ‘Solver Crash!!! Check Parameters.’ However, the model will have completed successfully in this case and the results can be extracted as normal.

### *File extensions*

Several files are created by the model to specify input parameters and output data. Table 1 shows the file extensions used by 3D TREAD for saving model input and output data. In addition to these files the file ‘setup.d’ contains the results interface parameters for only the most recently used file.

**Table 1.** File extensions used by 3D TREAD for model input and output data.

File extension	Stored values
domain.m	Mesh specification
.prj	All inputs entered in the ‘domain inputs’ box
micro.par	Programme remnant, necessary for model to run but contains no input data
rates.par	All reaction dynamics settings (stoichiometry, rates, etc..)
spec.par	A list file names for all specified components
spec_NAME.par	Name and parameters specified for each component (where NAME is the component name specified by the user)
!results.out	Model output for each component at each saved time step for the entire mesh
!results.out.cont	Component concentrations for the entire mesh for the end of the simulation only, allows these conditions to be applied to a continued model run
!results_plots.csv	Created by Matlab when the results are plotted, contains 1D data for each component and time-step based on user specified output requirements
stats.txt	Records the model runtime after the simulation is complete

## 10. Future Updates

The following updates are planned or underway:

- Removal of non-essential (legacy) functions

- A function allowing specification of precipitation reactions for e.g. sulphides
- Defining high mesh resolution at microniche edges
- Plotting of data across the z axis
- Addition of a function allowing exponential growth for reaction rates
- A built in plotting function, removing the need for Matlab

### ***11. Further information***

For additional information, including copies of the 3D TREAD manuscript(s), contact

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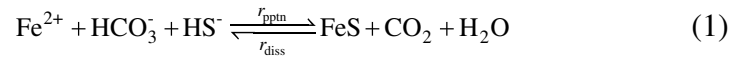
E-mail: [w.davison@lancaster.ac.uk](mailto:w.davison@lancaster.ac.uk)  
Fax: +44 (0)1524 593985



## Appendix C

### Typical treatment of iron – sulphide reactions

Typically, modelled iron sulphide precipitation/dissolution reactions are assumed to follow Equation 1 (e.g. Boudreau, 1996; also often shown in a simplified form where bicarbonate and carbon dioxide are excluded).



The empirical rate laws stated in Wang and van Cappellen (1996) are shown as Equations 2, 3 and 4. [FeS] is a proxy for the surface area and is excluded from Equation 2, as there may be no initial solid phase (see van Cappellen et al, 1993).

$$r_{\text{pptn}} = k_{\text{pptn}} \delta_{\text{pptn}} (\Omega_{\text{FeS}} - 1) \quad (2)$$

$$r_{\text{diss}} = k_{\text{diss}} \delta_{\text{diss}} [\text{FeS}] (1 - \Omega_{\text{FeS}}) \quad (3)$$

where:

$$\Omega_{\text{FeS}} = \frac{[\text{Fe}^{2+}][\text{HS}^-]}{\{\text{H}^+\} K'_{\text{FeS}}} \begin{cases} > 1: \delta_{\text{pptn}} = 1 & \delta_{\text{diss}} = 0 \\ \leq 1: \delta_{\text{pptn}} = 0 & \delta_{\text{diss}} = 1 \end{cases} \quad (4)$$

This relationship is widely used in diagenetic models (e.g. Wijsman et al, 2002; Morse and Eldridge, 2007). In applying this approach  $\delta$  acts as a simple switch that only allows either the forward or reverse reaction to proceed.