## **Supporting Information**

## Sources, Fate & Transport of Perfluorocarboxylates

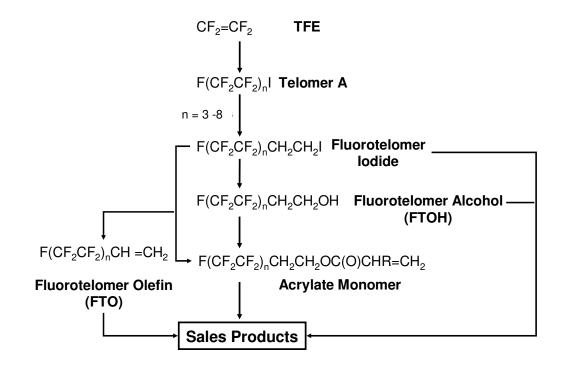
| 3  | Konstantinos Prevedouros <sup>1</sup> , Ian Cousins <sup>*1</sup> , Robert C. Buck <sup>2</sup> , Stephen H. Korzeniowski <sup>2</sup> |
|----|--|
| 4  | * Corresponding author phone: (+46) (0) 8 164012; fax: (+46) (0) 8 6747638; email:   |
| 5  | ian.cousins@itm.su.se  |
| 6  | <sup>1</sup> Department of Applied Environmental Science (ITM), Stockholm University, SE-10691 Stockholm,                              |
| 7  | Sweden   |
| 8  | <sup>2</sup> E. I duPont de Nemours & Co., Inc., P.O. Box 80023, Wilmington, Delaware, U.S.A. 19880-0023                               |
| 9  |  |
| 10 | The supporting information provides additional details describing the basis and computations for the direct and indirect               |
| 11 | source emissions as well as environmental inventories and sinks.   |

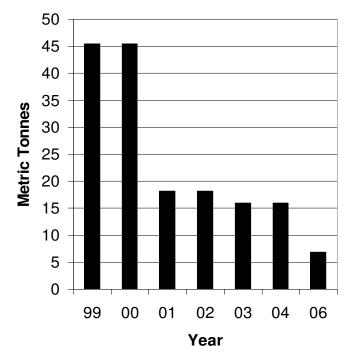
1

```
FIGURE S1. Industrial Processes for Synthesis of PFCAs
1
2
     Equation 1 Electrochemical Fluorination (ECF)
3
     H(CH_2)_7COF + HF + e \rightarrow F(CF_2)_7COF \rightarrow F(CF_2)_7CO_2NH_4
4
                                                            APFO
5
     Equation 2 Fluorotelomer lodide Oxidation
6
7
     F(CF<sub>2</sub>)<sub>8</sub>I
                           [O] \rightarrow F(CF_2)_7COOH \rightarrow F(CF_2)_7CO_2NH_4
                     +
     Perfluorooctyl lodide
                                                           APFO
8
     Equation 3 Fluorotelomer Olefin Oxidation
9
     F(CF_2)_8CH=CH_2 + [O] \rightarrow F(CF_2)_8COOH \rightarrow F(CF_2)_8CO_2NH_4
10
     Fluorotelomer 8-2 Olefin
                                                             APFN
11
12
     Equation 4 Fluorotelomer lodide Carboxylation
     F(CF<sub>2</sub>)<sub>8</sub>I
                    +
                           [CO_2] \rightarrow F(CF_2)_8COOH \rightarrow F(CF_2)_8CO_2NH_4
13
      Perfluorooctyl lodide
                                                                APFN
14
15
     Products in Eq. 1 and 3 are actually carbon chain length mixtures.
16
```

17 The ECF process produces 20-30 weight percent branched perfluorocarbon chain isomers.

### 1 Figure S2. Fluorotelomer-Based Product Manufacture Schematic





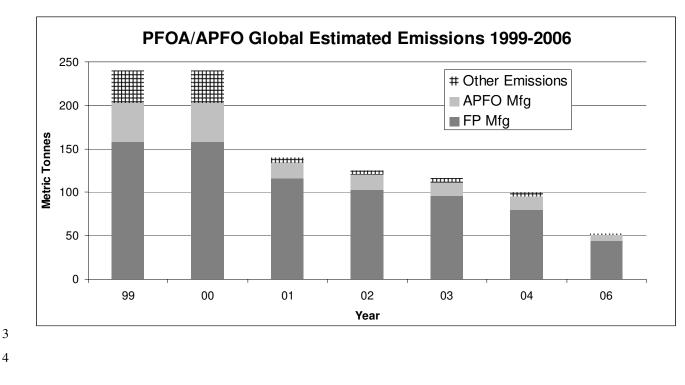
1 Figure S3. Global Industry-Wide Emissions from APFO Manufacture 1999-2006



This graph shows the recent historical trend of APFO emissions from its manufacture as an industrial chemical. Data for 1999-2004 are based on reported information (references 1,2,3,4). Data for 2006 are projected.

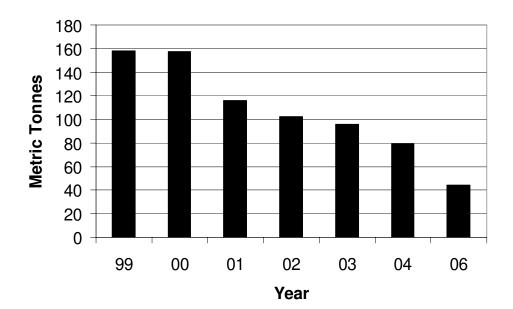
6 See also Table S3.

FIGURE S4. Estimated Global PFO/APFO Emissions from All Sources 1999-2006.



- 5 This graph shows the recent historical trend of PFO/APFO emissions from all sources from
- 6 1999-2006. The data for 2006 are projected. See also Figures S3, S5 and S6.

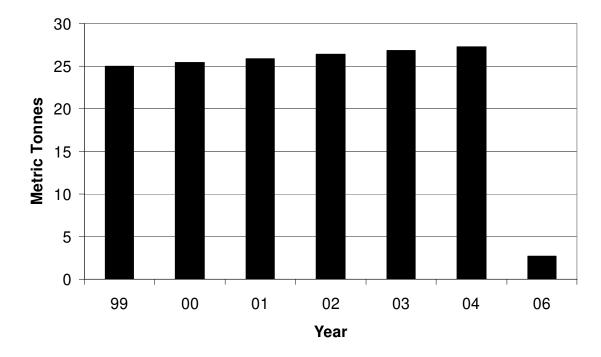
1 2



## 1Figure S5. Global Industry-Wide APFO Emissions from Fluoropolymer2Manufacture 1999-2006

4 This graph shows the recent historical trend of APFO emissions from its use in fluoropolymer 5 manufacturing. Data for 1999-2004 are based on reported information (refs. 1,2,3,4,5). Data for 2006 6 are projected. See also data in Table S5.

## 1 Figure S6. Global Industry-Wide APFO Emissions from Fluoropolymer Dispersion



#### 2 **Processing**



This graph shows the recent historical trend of APFO emissions from the processing of fluoropolymer
dispersions. Data for 1999-2004 are based on reported information (ref. 6). Data for 2006 are projected
based upon recent commitments to reduce these emissions. See also data in Table S6 and S7.

## Table S1. Chemical Abbreviations, Names & Formulas

| Chemical     | Chemical                               | Chemical                             |
|--------------|--|--------------------------------------|
| Abbreviation | Name                                   | Formula                              |
| PFCA(s)      | Perfluorocarboxylate(s)                | F(CF <sub>2</sub> )nCOO <sup>-</sup> |
| PFHx         | Perfluorohexanoate                     | F(CF2)5COO <sup>-</sup>              |
| PFHxA        | Perfluorohexanoic Acid                 | F(CF2)5COOH                          |
| PFHp         | Perfluorohepanoate                     | F(CF2)6COO <sup>-</sup>              |
| PFHpA        | Perfluoroheptanoic Acid                | F(CF2)6COOH                          |
| PFO          | Perfluorooctanoate                     | F(CF2)7COO <sup>-</sup>              |
| PFOA         | Perfluorooctanoic Acid                 | F(CF2)7COOH                          |
| APFO         | Ammonium Perfluorooctanoate            | F(CF2)7COONH4                        |
| PFN          | Perfluorononanoate                     | F(CF2)7COO <sup>-</sup>              |
| PFNA         | Perfluorononanoic Acid                 | F(CF2)8COOH                          |
| APFN         | Ammonium Perfluorononanoate            | F(CF2)8COONH4                        |
| PFD          | Perfluorodecanoate                     | F(CF2)8COO <sup>-</sup>              |
| PFDA         | Perfluorodecanoic Acid                 | F(CF2)9COOH                          |
| PFU          | Perfluoroundecanoate                   | F(CF2)10COO <sup>-</sup>             |
| PFUA         | Perfluoroundecanoic Acid               | F(CF2)10COOH                         |
| PFDD         | Perfluorododecanoate                   | F(CF2)11COO <sup>-</sup>             |
| PFDDA        | Perfluorododecdanoic Acid              | F(CF2)11COOH                         |
| PFTD         | Perfluorotridecanoate                  | F(CF2)12COO <sup>-</sup>             |
| PFTDA        | Perfluorotridecanoic Acid              | F(CF2)12COOH                         |
| PFAS         | Perfluoroalkylsulfonyl products        | F(CF2)nSO2-R                         |
| POSF         | Perfluorooctylsulfonyl fluoride        | F(CF2)8SO2F                          |
| PFOS         | Perfluorooctane sulfonate              | F(CF2)8SO3-                          |
| N-Et FOSE    | N-ethyl fluorooctylsulfonamidoethanol  | F(CF2)8SO2N(Et)CH2CH2OH              |
| N-Me FOSE    | N-methyl fluorooctylsulfonamidoethanol | F(CF2)8SO2N(Me)CH2CH2OH              |
| FTOH         | Fluorotelomer Alcohol                  | F(CF2CF2)nCH2CH2OH                   |
| FTO          | Fluorotelomer Olefin                   | F(CF2CF2)nCH=CH2                     |

## 1 TABLE S2. Commercial PFCA Products Characterization

2 3 4

#### Weight % By Carbon Chain Length

| Product<br>Identification   | Figure<br>S1<br>Process | %<br>Branched<br>Isomers | 8<br>PFO | 9<br>PFN | 10<br>PFD       | 11<br>PFU  | 12<br>PFDD                     | 13<br>PFTD |
|-----------------------------|-------------------------|--------------------------|----------|----------|-----------------|--|--------------------------------|------------|
| Fluorad <sup>®</sup> FC-143 | 1                       | 15                       | 99       | 0.22     | <u>&lt;</u> LOQ | nm   | <loq< td=""><td>nm</td></loq<> | nm         |
| Surflon <sup>®</sup> S-111  | 3                       | 0                        | 0.78     | 74       | 0.37            | 20   | 0.1                            | 5          |
| APFO - DuPont               | 2                       | 0                        | 99       | nd       | <u>&lt;</u> LOQ | <loq< td=""><td><loq< td=""><td>nm</td></loq<></td></loq<> | <loq< td=""><td>nm</td></loq<> | nm         |

5

6 These are representative commercial PFCA products used as processing aids in the manufacture of

7 fluoropolymers.

8  $F(CF_2)_nCOO^-NH_4^+$  Commercial Product Analyses conducted by LC/MS/MS;

9 nd = not detected; nm = not measured.

 $10 \quad \text{<LOQ} = \text{less than the limit of quantification, detectable but not quantifiable (<0.01);}$ 

11  $\leq$ LOQ = Detectable, close to 0.01;.

### 1 Table S3. Estimated Industry-Wide Global Historic PFO Emissions from APFO

- Manufacture (ref. 2)
- 2 3

| Time<br>Period | # of<br>Years | Estimated Average<br>Annual APFO<br>Production (t/yr) | Est Average Annual<br>PFO Emissions (t/yr) | Estimated<br>Total PFO<br>Emissions <sup>§</sup> (t) |
|----------------|---------------|---|--|--|
| 1995-2002      | 8             | 200 - 300   | 20 – 40 (see Fig. S3)                      | 160 - 320  |
| 1980-1994      | 15            | 100 - 150   | 10 - 15                                    | 150 - 225  |
| 1965-1979      | 15            | 30 - 50   | 3 - 5                                      | 45 - 75  |
| 1951-1964      | 14            | 5 - 25  | 0.5 – 2.5                                  | 7 – 35   |
|                |               | Total Global Historic                                 | Emissions (tonnes)                         | 400 – 700*   |

- 4 \* Rounded to the nearest 100 t = metric tonnes
- 5 § Value is total emissions for the given time period
- 6

7

8

9

10

- 1951 was the starting year for the computations because it was the first year APFO was manufactured and used in the commercial manufacture of fluoropolymers by DuPont. The amount of APFO was determined based on the annual production of fluoropolymers from 1951 to present.
- Production in earlier time periods was estimated to be 50% of the amount manufactured in 1995-2004 for the period 1980-1994; 30% of the amount manufactured in 1980-1994 for the period 1965-1979; and 10% of the amount manufactured in 1965-1979 for the period 1951-14
- 15

#### 16 **Example Calculations**

- $(40t \times 8yrs) + (15t \times 15yrs) + (5t \times 15yrs) + (2.5t \times 14yrs) = 320+225+75+35 = 655$  rounded to
- 18 nearest 100 is **700 tonnes**.
- $(20t \times 8yrs) + (10t \times 15yrs) + (3t \times 15yrs) + (0.5t \times 14yrs) = 160+150+45+7 = 362$  rounded to
- 20 nearest 100 is **400 tonnes**.
- The upper bound of annual emissions (40) for 1995-2002 was estimated by the following
  computation : [6 years (1992-2000) x 45 t/yr.] + [2 years (2001-2002) x 18 t/yr] = 306 tonnes
  over eight years. (306 ÷ 8 years) = 38; rounded to the nearest 10 the upper bound is 40. See
  also Figure S3.
  - ES0512475 .doc

1 **Table S4. Estimated Global Historic PFN Emissions from APFN Manufacture** 

| Time Period | # of<br>Years | Estimated Average<br>Annual APFN<br>Production (t/yr) | Est Average Annual<br>APFN Emissions (t/yr) | Est. Total<br>APFN<br>Emissions <sup>§</sup> (t) |
|-------------|---------------|---|---|--|
| 1995 – 2004 | 10            | 15 - 75   | 2 – 7.5                                     | 20 -75   |
| 1985 – 1994 | 10            | 20 - 100  | 2 - 10                                      | 20 - 100   |
| 1975 – 1984 | 10            | 25 - 50   | 2.5 - 5                                     | 25 – 50  |
|             |               | Total Global Historic Emissions (tonnes)              |   | 70 - 200*  |

4 \* Rounded to nearest one significant figure. t = metric tonnes

5 § Value is total emissions for the given time period

6

The time periods and annual production are estimates assuming growth since APFN was first
patented for use in making fluoropolymers (ref. 7, also see p. 15).

9 • Manufacturing emissions have been estimated to be 10% of amount of APFN manufactured,

10 comparable in percentage to the amount cited in the main manuscript for APFO.

• APFN is manufactured as a mixture of perfluorocarboxylates (See Table S2).

• See also the description of the PVDF process that follows for more details on how the annual

13 APFN production amounts were estimated.

#### 14 **Example Calculations**

# (8t x 10yrs)+ (10t x 10yrs) + (5t x 10yrs) = 75+100+50 = 225 rounded to nearest 100 is 200 tonnes.

• 
$$(3t \times 10yrs) + (2t \times 10yrs) + (2.5t \times 10yrs) = 30+20+25 = 75$$
 rounded to nearest 10 is 80 tonnes.

ES0512475 .doc

## Table S5.Estimated Industry-Wide Global Historic APFO Emissions from<br/>Fluoropolymer Manufacture

| Time Period | # of                            | Est Average Annual APFO | Estimated Total                 |
|-------------|---------------------------------|-------------------------|---------------------------------|
| Time Period | Years                           | Emissions (t/yr)        | APFO Emissions <sup>§</sup> (t) |
| 1995 – 2004 | 10                              | 100 - 200               | 1,000 – 2,000                   |
| 1980 - 1994 | 15                              | 50 - 100                | 750 – 1,500                     |
| 1965 – 1979 | 15                              | 20 - 30                 | 300 - 450                       |
| 1951 - 1964 | 14                              | 3 - 15                  | 42 - 210                        |
|             | Total Global Historic Emissions |                         | 2,000 - 4,000*                  |

| 5  | * Rounded to the nearest one thousand. $t = metric tonnes$  |
|----|---|
| 6  | § Value is total emissions for the given time period  |
| 7  | • 60% of APFO used in the manufacture of fluoropolymers is emitted to land and water.   |
| 8  | • 1951 was the starting year for the computations because it was the first year of commercial   |
| 9  | fluoropolymer manufacture by DuPont. Recent references provided sufficient information to   |
| 10 | estimate emissions from 1995-2004 $(3,4,5)$ .   |
| 11 | • APFO use in earlier time periods was estimated to be 50% of the amount used in 1995-2004 for  |
| 12 | the period 1980-1994; 30% of the amount used in 1980-1994 for the period 1965-1979; and   |
| 13 | 10% of the amount used in 1965-1979 for the period 1951-1964.   |
| 14 | Example Calculations  |
| 15 | • $(200t \times 10yrs) + (100t \times 15 years) + (30t \times 15 years) + (15t \times 14 years) = 4,160 \text{ or } 4,000 \text{ tonnes}$ |
| 16 | rounded to the nearest 1000.  |
| 17 | • $(100t \times 10yrs)$ + $(50t \times 15 years)$ + $(20t \times 15 years)$ + $(3t \times 14 years)$ = 2,092 or <b>2,000</b> tonnes       |
| 18 | rounded to the nearest 1000.  |

## Table S6. Aqueous Fluoropolymer Dispersion APFO Emissions Mass Balance(ref.6)

| APFO Destinations                   | Wt% of Input APFO in Aqueous<br>Fluoropolymer Dispersions |
|-------------------------------------|---|
| Decomposed in Dispersion Processing | 62%   |
| Air Emission                        | 16%   |
| Wastewater Emission                 | 5%  |
| Solid Waste Emission                | 5%  |
| Undetermined                        | 12%   |
| Total                               | 100%  |

The historic amount of PFCAs in fluoropolymer dispersions can be estimated starting from the
 average annual production of APFO in Table S3. Assuming that 90% of APFO production was
 used for fluoropolymer manufacture then multiplying by 16% to assign the appropriate amount
 of PFCAs to fluoropolymer dispersion products followed by multiplying by 40% for
 environmental emissions from dispersion processing the annual and total environmental
 releases can be estimated. These values are given in Table S7.

# Table S7. Estimated Industry-Wide Global Historic APFO Emissions fromAqueousFluoropolymer Dispersion Processing

2 3 4

1

| Time Period | # of Years                      | Est Average Annual APFO<br>Emissions (t/yr) | Estimated Total<br>APFO Emissions <sup>§</sup> (t) |
|-------------|---------------------------------|---|--|
| 1995 – 2002 | 8                               | 12 - 17                                     | 100 – 140  |
| 1980 - 1994 | 15                              | 6 – 9                                       | 90 – 140   |
| 1965 – 1979 | 15                              | 2 – 3                                       | 30 – 45  |
| 1951 - 1964 | 14                              | 0.3 – 1                                     | 3 – 14   |
|             | Total Global Historic Emissions |   | 200 – 300*   |

5

6 \* Rounded to nearest hundred t = metric tonnes

7 § Value is total emissions for the given time period

- Begin with values from Table S3, Column 3; 90% of APFO production is used in manufacture of Fluoropolymers (multiply by 0.9); 16% of Fluoropolymers manufactured with APFO are Dispersion Products (multiply by 0.16); As high as 40% of APFO present in Dispersion Products is emitted to the environment (multiply by 0.4)
  <u>Example Calculations</u>
  The lower bound estimate for 1995-2002 : 200 x 0.9 x 0.16 x 0.4) = 12. 12 x 8 years = 96,
- rounded to the nearest 10 equals 100.
- The upper bound estimate for 1995-2002 : 300 x 0.9 x 0.16 x 0.4 = 17. 17 x 8 years = 136,
   rounded to the nearest 10 equals 140.

- **Polyvinylidene Fluoride (PVDF) Polymerization** 1 2 The following patent citations were used as a basis for setting the range for the percent APFN 3 surfactant on weight of vinylidene fluoride (VF) monomer which is used in Tables S9 and S10. In 4 addition, private communication from J. Franklin (see pages 17-18) was also considered. 5 6 7 **PVDF Emulsion Polymerization Patent Citations** all cite PFCA salts of varying chain lengths as suitable for use 8 9 Weight Percent 10 **PFCA Surfactant** 11 **US 3,475,396** (ref. 8) 12 Column 2, Line 66 0.5 - 3.013 Claim 4 2 - 614 0.5 - 3.015 Claim 7 **US 3.640.985** (ref. 9) 16 Col 3. Lines 10-35 0.05 - 5.0; usually 0.05 - 2.017 18 **US 3,708,463** (ref. 10) Col 3-4 Lines 60-75, 1-17 0.1 - 1.5; 0.5 - 1.0 preferred 19 **US 4,569,978** (ref. 11) 20 21 Col. 2. Lines 33-37 0.05 - 0.5; 0.1- 0.2 preferred 22 23 These patents cite the use of perfluorocarboxylates (PFCAs) as a surfactant in the emulsion polymerization of vinylidene fluoride to make polyvinylidene fluoride (PVDF). 24 25 Current PVDF manufacturers have confirmed that APFN is the surfactant that is and has been used commercially since the mid 1970s. 26 Based on 15,000 tonnes of PVDF manufactured in 2002 by emulsion polymerization and a range 27 • of use of 0.1 to 0.5 weight percent, the amount of AFFN used in 2002 ranges between 15 to 75 28 29 tonnes. 30 • Note: PFCA surfactants are not used in the suspension polymerization process for manufacturing PVDF. 31 • For the Purpose of this Assessment, the following ranges of surfactant use and PVDF production 32
- 33 were used:
- 34

1 Table S8. Estimated Historic Use of APFN in PVDF Production

| Time Period | Estimated<br>PVDF Production<br>(tonnes) | Estimated Weight<br>Percent APFN<br>Surfactant Used | Estimated<br>APFN Production<br>(tonnes per year) |
|-------------|--|---|---|
| 1995 - 2004 | 15,000                                   | 0.1 – 0.5   | 15 – 75   |
| 1985 - 1994 | 10,000                                   | 0.2 – 1.0   | 20 – 100  |
| 1975 - 1984 | 5,000                                    | 0.5 – 1.0   | 25 – 50   |

4

• The use range for 1995-2005 reflects the information provided on the next pages to establish a

6 lower bound and the patent information cited on the prior page which indicates that APFN use may

7 be greater to establish the estimated upper bound of 0.5 wt%.

• Higher APFN use in earlier years is used for the periods before 1995 as the patents indicate this.

9 Estimated surfactant use is reduced over time to reflect industry improvements in process

10 efficiency.

| 1        | 28 September 2005   |
|----------|---|
| 2        | James Franklin  |
| 3        | CLF-Chem Consulting SPRL  |
| 4        | Brussels, Belgium   |
| 5        |   |
| 6        |   |
| 7        |   |
| 8        | CONSUMPTION OF APFN IN THE MANUFACTURE OF PVDF  |
| 9        |   |
| 10<br>11 |   |
| 11       | Specific consumption of fluorinated surfactant  |
| 12       | Specific consumption of indomnated surfactant   |
| 14       | The production of polyvinylidene fluoride (PVDF) by emulsion (dispersion) polymerization in the presence of a     |
| 15       | long-chain fluorinated surfactant was first commercialized by the Pennwalt Corporation in the 1970s, on the       |
| 16       | basis of a process developed by Diamond Shamrock (US Patent 3,475,396).   |
| 17       |   |
| 18       | US Patent 4,569,978 filed by Pennwalt on 17 April 1985 describes the use of fluorinated surfactants including     |
| 19       | Surflon S111 (the main component of which is APFN). Surfactant levels of 0.05 to 0.5 weight percent, based on     |
| 20       | the weight of monomer used, are claimed in Claim 1. As is usual in the patent literature, the first claim is very |
| 21       | broad and one of its objectives is to prevent potential competitors from even approaching the preferred           |
| 22       | operating conditions, which are more closely defined in further claims. Thus, in the case of US Patent            |
| 23       | 4,569,978, the "preferred" range of surfactant levels is given as 0.1-0.2 % (Claim 15).                           |

According to informed industry sources, this range is consistent with current industrial practice. In the case of coating-grade PVDF, for which latex particle size is of paramount importance, surfactant concentrations higher than 0.2% would yield a too low particle diameter, while using less than 0.1% would result in an unstable latex.

28 29

## Global production of PVDF by the emulsion process

The 2002 production capacities for PVDF in the major industrial regions, taken from Ring *et al* (2002), are given in the table below:

33

| Producer                  | Location              | Process     | Capacity,<br>ktonne/year |
|---------------------------|-----------------------|-------------|--------------------------|
| Atofina (now Arkema)      | Calvert City, KY, USA | Emulsion    | 8.4                      |
| Ausimont (now Solvay Sole | Thorofare, NJ, USA    | Emulsion    | 7.7                      |
| Solvay (now Dyneon)       | Decatur, AL, USA      | Suspension  | 2.3                      |
| Atofina (now Arkema)      | Pierre Bénite, France | Emulsion    | 2.2                      |
| Solvay                    | Tavaux, France        | Suspension  | 5.0                      |
| Central Glass             | Ube, Japan            | Emulsion?   | 0.3                      |
| Daikin                    | Settsu, Japan         | Suspension? | 0.1                      |
| Kureha                    | Iwaki, Japan          | Suspension  | 1.2                      |
| TOTAL                     |                       |             | 27.2                     |

34

The installed capacity for manufacture of PVDF by the emulsion process is thus about 18.6 ktonne/year, or 68 % of overall PVDF capacity. The suspension process does not use any fluorinated surfactants.

37

Actual production and consumption of PVDF is lower than installed capacity. Ring *et al* (2002) estimate overall production in the US, Western Europe and Japan at 14.2 ktonne (only 52 % of estimated 2002 installed capacity for the combined emulsion and suspension processes). On the other hand, there is limited production in China, Russia and possibly other countries. For the purpose of estimating APFN consumption in the manufacture of PVDF, we will conservatively assume production by the emulsion process to be 75 % of 18.6

43 ktonne/year, i.e., about 14 ktonne/year in 2002.

#### Consumption of APFN in the production of PVDF by the emulsion process

We will conservatively assume that all the PVDF produced by the emulsion process uses pure APFN as a surfactant. Multiplying the production of emulsion-grade PVDF (14 ktonne/year) by the specific consumption of APFN (0.1-0.2 %), we estimate the annual consumption of APFN for this purpose to be 14-28 tonne/year. This is the estimated range for year 2002. Consumption would have been smaller in earlier years when PVDF production was lower.

#### 9 10 **Reference**

10 **Refer** 11

12 Ring, K-L, Kälin T, Kishi A, 2002. Fluoropolymers. SRI International, CEH Marketing Research Report

## 1Table S9. Estimated Industry-Wide Global Historic APFN Emissions from PVDF2Fluoropolymer Manufacture

3

| Time period | # years | Estimated Annual APFN Use in<br>PVDF Production<br>(t / yr.) | Estimated APFN<br>Emissions<br>(t / yr.) | Estimated Total<br>APFN Emissions <sup>§</sup> (t) |
|-------------|---------|--|--|--|
| 1995-2004   | 10      | 15 -75   | 9 - 45                                   | 90 - 450   |
| 1985-1994   | 10      | 20 – 100   | 12 - 60                                  | 120 - 600  |
| 1975-1984   | 10      | 25 - 50  | 15 - 30                                  | 150 - 300  |
|             |         |  | Total Global<br>Historic Emissions       | 400 – 1,400*                                       |

4

<sup>5</sup> \* Rounded to nearest hundred.; t = metric tonnes; § Value is total emissions for the given time period

• 60% of APFN is estimated to be emitted during PVDF manufacturing, the same emissions

7 value as for APFO use in fluoropolymer manufacture.

#### 8 **Example Calculations**

- The upper bound estimation for 1995 2004: (75 t./yr. x 60%) = 45 t ; 45 t x 10 yrs = 450
- 10 tonnes.
- The lower bound estimation for 1995 2004 : (15 t/yr. x 60%) = 9 t ; 9 t x 10 yrs. = 90 tonnes.

## Table S10. Estimated Industry-Wide Global Historic APFN Emissions from PVDFFluoropolymer Industrial Processing

| Time Period | # of Years                               | Annual APFN emissions (t) | Estimated Total<br>APFN Emissions <sup>§</sup> (t) |
|-------------|--|---------------------------|--|
| 1995 – 2004 | 10                                       | 0.6 -1.2                  | 6 - 12   |
| 1985 – 1994 | 10                                       | 0.4 – 0.8                 | 4 – 8  |
| 1975 – 1984 | 10                                       | 0.2 - 0.4                 | 2 - 4  |
|             | Total Global Historic Emissions (tonnes) |                           | 10 - 20*   |

4

- 5 \* Rounded to nearest one significant figure; t = metric tonnes;
- 6 § Value is total emissions for the given time period

|    | Б |   |
|----|---|---|
| 11 |   | processing.(ref. 6)   |
| 10 |   | from the published valued for the disposition of APFO during fluoropolymer dispersion         |
| 9  |   | and 40% is emitted, most likely to air. These 60% and 40% values are best estimates derived   |
| 8  |   | polymerization and that when it is processed by industrial users 60% of the APFN is destroyed |
| 7  | • | It is estimated that between 100-200 ppm of APFN remains in all PVDF made by emulsion         |

- 12 **Example Calculation**
- The upper bound estimate for 1995-2004: (15,000 tonnes PVDF produced x 200ppm x 40%) =
   1.2 tonnes.
- The lower bound estimate for 1995-2004: (15,000 tonnes PVDF produced x 100ppm x 40%) =

16 0.6 tonnes.

ES0512475 .doc

20

- 1 Table S11. PFCA Impurities in POSF-Based Products
- 2

| Time Period | # of Years                      | Annual Global POSF | Estimated Total            |  |  |
|-------------|---------------------------------|--------------------|----------------------------|--|--|
|             |                                 | Production (t)     | PFCA Emissions $^{\$}$ (t) |  |  |
| 2002        | 1                               | 200                | 0.04 – 0.3                 |  |  |
| 2001        | 1                               | 1,400              | 0.3 – 2                    |  |  |
| 1995 – 2000 | 6                               | 4,500              | 5 – 43                     |  |  |
| 1980 – 1994 | 15                              | 3,000              | 9 – 72                     |  |  |
| 1960 – 1979 | 20                              | 450                | 2 – 14                     |  |  |
|             | Total Global Historic Emissions |                    | 20 – 130*                  |  |  |

- 4 \* Rounded to nearest ten t = metric tonnes
- § Value is total emissions for the given time period 5 6 • Data from the major global producer represents 80-90% of global production. • Use the range of 200 – 1,600 ppm (ref.12) as the PFCAs impurity level in POSF-Based 7 Products. 8 According to the source of these values (ref. 13), they represent the PFCAs impurity level on a 9 • 10 100% active ingredient basis, not on a sales product basis as stated in reference 12. Hence, we have used POSF production as the 100% active ingredient basis for our estimation. 11 12 **Example Calculation** 13 14 The upper bound estimate for 1995-2000 : (4,500 tonnes x 6yrs x 1600ppm) = 43 tonnes.•
- The lower bound estimate for 1995-2000 : (4,500 tonnes x 6yrs x 200ppm) = 5 tonnes.

Table S12. Degradation of POSF-Based Raw Materials to PFCAs (ref.14)

| Time Period | # of Years  | Annual POSF                   | Estimated Total<br>PFCA Emissions <sup>§</sup> (t)* |  |  |
|-------------|-------------|-------------------------------|---|--|--|
|             |             | Production (t)                |   |  |  |
| 2002        | 1           | 200                           | 0.001 – 0.06  |  |  |
| 2001        | 1           | 1,400                         | 0.007 – 0.4   |  |  |
| 1995 – 2000 | 6           | 4,500                         | 0.1 – 8   |  |  |
| 1980 – 1994 | 15          | 3,000                         | 0.2 – 14  |  |  |
| 1960 – 1979 | 20          | 450                           | 0.05 – 3  |  |  |
|             | Total Globa | I Historic Emissions (tonnes) | 1 – 30*   |  |  |

4 \* Rounded to nearest integer and hundred t = metric tonnes

5 § Value is total emissions for the given time period

• Using 0.1 to 3 wt% POSF Raw materials and 0.5 to 1% POSF raw materials degradation to PFCAs

7 • 1% was recommended as the upper bound for degradation to PFCAs by the authors of the

8 degradation study. (refs.13)

9 • Should future degradation research results reveal greater or less degradation, the values computed

10 in this table will need to be recomputed.

#### 11 Example Calculation

- The upper bound estimate for  $1995-2000 : (4,500 \times 6yrs \times 3\% \times 1\%) = 8$  tonnes.
- The lower bound estimate for  $1995-2000 : (4,500 \times 6yrs \times 0.1\% \times 0.5\%) = 0.1$  tonnes.

ES0512475 .doc

1 Table S13. POSF-Based Aqueous Fire-Fighting Foam (AFFF)

|           |       |                                     |                    | Estimated Total             |
|-----------|-------|-------------------------------------|--------------------|-----------------------------|
| Time      | # of  | Annual POSF                         | POSF-based Product | PFCA Emissions <sup>§</sup> |
| Period    | Years | <b>Production</b> <sup>15</sup> (t) | for AFFF           | (t)                         |
| 2002      | 1     | 200                                 | 10                 | 0.01 – 0.1                  |
| 2001      | 1     | 1400                                | 70                 | 0.07 – 0.7                  |
| 1995-2000 | 6     | 3700                                | 1100               | 1 - 10                      |
| 1980-1994 | 15    | 1800                                | 1400               | 1 - 14                      |
| 1970-1979 | 10    | 450                                 | 200                | 0.2 - 2                     |
|           | -     | Total Global Historic               |                    |                             |
|           |       | Emissions (tonnes)                  |                    | 3 – 30*                     |

2

4 \* Rounded to one significant figure. t = metric tonnes

5 § Value is total emissions for the given time period

AFFF product is estimated to be 5% of the Total POSF Production per year of the major POSF
 manufacturer who is known to have been the major producer of AFFF products based on POSF

8 chemistry. This is why the values in column 3 are not the same as in Tables S11 and S12.

9 Additional AFFF use information is available in references 16 and 17.

• Example Calculation: (3700 x 0.05) x 6yrs = 1100 (rounded to nearest hundred)

- \* Range is for AFFF Product composition containing between 0.1 and 1.0 weight % PFCAs
- 12
- 13 **Example Calculation**
- 14  $(1100 \ge 0.01) = 10; (1100 \ge 0.001) = 1$  tonne.

ES0512475 .doc

1 **Table S14.** 

## 2 Estimated Industry-Wide PFCA Impurities in Fluorotelomer-Based Products

- 3 (ref.18)
- 4

| Time      | # of    | Average Annual                               | Estimated Total                 |
|-----------|---------|--|---------------------------------|
| Period    | Years   | Fluorotelomer A Production <sup>19</sup> (t) | PFCA Emissions <sup>§</sup> (t) |
| 1995-2004 | 10      | 4,000  | 0.2 – 20                        |
| 1980-1994 | 15      | 1,500  | 0.1 – 10                        |
| 1974-1979 | 5       | 500  | 0.01 – 1                        |
|           | Total G | obal Historic Emissions (tonnes)             | 0.3 – 30*                       |

#### 5

- 6 \* Rounded to one significant figure t = metric tonnes
- 7 § Value is total emissions for the given time period

| 8  | • | 1-100 ppm PFCAs as Impurity in Fluorotelomer-based Products (refs. 18,19). The amount of      |
|----|---|---|
| 9  |   | fluorotelomer-based products in a given year is estimated to be 5 times the amount of Telomer |
| 10 |   | A production, hence multiplication by 5 to compute the estimate. This factor of 5 is based on |
| 11 |   | the known "average" composition of a fluorotelomer-based product and the amount of Telomer    |
| 12 |   | A required to produce such and average product, roughly one part Telomer A produces 5 times   |
| 13 |   | the amount as product.  |
| 14 | • | All estimated emissions values rounded to one significant figure.                             |
| 15 |   |   |

10

### 16 **Example Calculations**

- The upper bound estimate for 1995-2004: (4000 tonnes x 10yrs x 100ppm x 5) = 20 tonnes
- 18
  - The lower bound estimate for 1995-2004: (4000 tonnes x 10yrs x 1ppm x 5) = 0.2 tonnes

# Table S15. Estimated Industry-Wide Releases of PFCAs from Degradation of Fluorotelomer-Based Raw Materials to PFCAs

| Time Period | # of Years | Average Annual<br>Fluorotelomer A Production (t) | Estimated Total<br>PFCA Emissions <sup>§</sup> (t) |
|-------------|------------|--|--|
| 1995-2004   | 10         | 4,000  | 4 - 80   |
| 1980-1994   | 15         | 1,500  | 2 – 45   |
| 1974-1979   | 5          | 500  | 0.3 – 5  |
|             | Tota       | al Global Historic Emissions (tonnes)            | 6 – 130*   |

4

- 5 \* Rounded to one significant figure t = metric tonnes
- 6 § Value is total emissions for the given time period
- Using 1.0 to 2.0 wt% based on Fluorotelomer A and 1–10% degradation to PFCAs.

8 • In biodegradation studies, 8-2 fluorotelomer alcohol degradation to PFOA reported values are

9 between 3 - 7% (refs.20,21,22), with the most recent data between 3-6%.(refs.21,22) In gas-phase

10 atmospheric studies, the conversion of 8-2 fluorotelomer alcohol to PFOA was estimated to be

between 1 - 10%. (ref. 23) From these studies, we selected the smallest and largest values of 1 and

12 10% as the lower and upper bounds for biodegradation.

Should future degradation research results reveal greater or less degradation, the values computed
 in this table will need to be recomputed.

#### 15 **Example Calculations**

#### • For the period 1995-2004, the upper bound estimate: $(4,000 \text{ tonnes } x \ 10\text{yrs } x \ 2\% \ x \ 10\%) = 80$

- 17 tonnes
- For the period 1995-2004, the lower bound estimate: (4,000 tonnes x 10yrs x 1% x 1%) = 4
   tonnes

20

### **Table S16. Analysis of PFCAs in Consumer Spray Application Products**

- 2 LC/MS/MS Assay of Spray Application Consumer Products purchased at retail prior to withdrawal
- 3 by the major manufacturer of POSF-based products.

| Consumer Product Sample           | PFHx | PFHp | PFO | PFN | PFOS |
|-----------------------------------|------|------|-----|-----|------|
| Fabric Protector                  | 60   | 5    | 5   | 7   | n.d. |
| Protector for Leather             | 100  | 100  | 78  | 10  | n.d. |
| Cleaner for Rugs & Carpets        | 100  | 11   | 9   | 9   | 500  |
| Cleaner for Fabric and Upholstery | 100  | 5    | 5   | 10  | 454  |

- Table Values are in *parts per million*. Rounded to nearest whole number.
- Single point determination to estimate analyte concentration for all analytes other than PFO.
- Quantitative analysis using 9 point calibration run in duplicate with spike recovery for PFO determination.
- 8 n/d = not detected
  - No perfluorocarboxylic acids with greater than nine carbons were detected.
- 9 10

4

5

6

7

## 11 Analytical Method Summary (See also ref. 24)

- 12 Sample Preparation
- The foam sample was sprayed into a 20 mL scintillation vial and capped.
- The vial was placed in the dark at room temperature until the sample was in a liquid state (e.g., 3 hours)
- The liquid sample was weighed and diluted with methanol (e.g., 10 mg diluted with 10 mL of methanol). An additional sample was weighed and spiked with analog.
- The sample was pipetted into a HPLC vial with an internal standard.
- 19 The sample concentration was determined using LC/MS/MS
- 20

### 21 Analytical Method LC/MS/MS

- 22 Mobile phase A: 2 mM ammonium acetate with 5% methanol; Mobile phase B: Methanol
- Column: Spherisorb ODS  $C_{18}$  2.1 x 200 mm 5  $\mu$  temp: 65 °C; 45 Minute Gradient
- Initial conditions: 15 % B; Linear gradient for 41 minutes to 67 %B; Initial conditions at 41.01 minutes; Initial conditions for 4 minutes.
- 26 <u>LC/MS/MS instrumentation</u>
- 27 Waters Quattro fitted with an Agilent 1100 operated in the negative ion electrospray. The following
- transitions were monitored: 313>269, 363>319, 413>369, 499>80, 463>419, 513>469, 563>519, 613>569
- 30 A six point calibration which was run twice at the beginning and end of the analysis with an R > 0.99.
- Samples were quantitated using the eight carbon analog. Spike recovery for the samples ranged 99-104%.
- 33

| 2                         |                         |                        |             |                        |                |          |
|---------------------------|-------------------------|------------------------|-------------|------------------------|----------------|----------|
|                           | Concentration           | Surface Area           | Depth       | Amount                 | Amount         |          |
| INVENTORIES               | (g/m <sup>3</sup> )     | (m <sup>2</sup> )      | (m)         | (g)                    | (tonnes)       |          |
| Min. Ocean Inventory      | 1.50 x 10 <sup>-8</sup> | 1.5 x 10 <sup>14</sup> | 50          | 1.13 x 10 <sup>8</sup> | 113            |          |
| Max. Ocean Inventory      | 4.39 x10 <sup>-7</sup>  | 1.5 x 10 <sup>14</sup> | 150         | 9.88 x 10 <sup>9</sup> | 9878           |          |
| Min. Freshwater Inventory | 5.0 x 10 <sup>-8</sup>  | 4.0 x 10 <sup>12</sup> | 20          | 4.00 x 10 <sup>6</sup> | 4              |          |
| Max. Freshwater Inventory | 1.0 x 10 <sup>-5</sup>  | 4.0 x 10 <sup>12</sup> | 20          | 8.00 x 10 <sup>8</sup> | 800            |          |
|                           | Concentration           | Surface Area           | Depth       | Density                | (1 – Porocity) | Amount   |
|                           | (g/g)                   | (cm <sup>2</sup> )     | (cm)        | (g/cm <sup>3</sup> )   |                | (tonnes) |
| Min. Sediment Inventory   | 2.0 x 10 <sup>-11</sup> | 4.0 x 10 <sup>16</sup> | 5           | 2.4                    | 0.3            | 3        |
| Max. Sediment Inventory   | 5.0 x 10 <sup>-10</sup> | 4.0 x 10 <sup>16</sup> | 5           | 2.4                    | 0.3            | 343      |
|                           | Inventory               | Sed. Rate              | Depth       | Loss                   |                |          |
| SINKS                     | (tonnes)                | (cm/yr)                | (cm)        | (tonnes/yr)            |                |          |
| Min. Sediment Burial      | 3                       | 0.1                    | 5           | 0.06                   | -              |          |
| Max. Sediment Burial      | 343                     | 0.3                    | 5           | 21                     |                |          |
|                           | Inventory               | Res. Time              | Loss        |                        | <b>_</b>       |          |
|                           | (tonnes)                | (yr)                   | (tonnes/yr) |                        |                |          |
| Min. Deep Sea Transport   | 113                     | 500                    | 0.22        | 1                      |                |          |
| Max. Deep Sea Transport   | 9878                    | 300                    | 33          |                        |                |          |

### Table S17. Environmental Inventory and Sink Calculations

3

4

1

• References for the values in the above table are given in the manuscript.

Ocean and freshwater inventories are calculated by multiplying ocean water concentration (g/m<sup>3</sup>)
 by surface area (m<sup>2</sup>) and depth (m).

- The sediment inventory is calculated by multiplying the sediment concentration (g/g) by the
  surface area (cm<sup>2</sup>), mixing depth (cm), density (g/cm<sup>3</sup>) and 1 porosity.
- For all inventories, grams are converted to metric tonnes by dividing by  $10^6$ .

The sediment burial loss is calculated by first calculated a sediment residence time (yr) by dividing
 the mixing depth (cm) by the sedimentation rate (cm/yr).

The annual loss from sediment burial (tonnes/yr) is calculated by dividing the sediment inventory
 (tonnes) by this residence time (yr).

• The annual loss by deep-sea transport (tonnes/yr) is calculated by dividing the surface ocean inventory (tonnes) by the residence time of deep ocean water (yr).

#### 1 Literature Cited

- 1 DuPont Company, "*DuPont Global PFOA Strategy*," U.S. EPA Administrative Record AR226-1914. U.S. Environmental Protection Agency, Washington, D. C., **2005**.
- 2 3M Company, "Voluntary Use and Exposure Information Profile Perfluorooctanic Acid and Salts" U.S. EPA Administrative Record AR226-0595. U.S. Environmental Protection Agency, Washington, D. C., **2000**. 3M Company, "Environmental, Health and Safety Measures Relating to Perfluorooctanoic Acid and its Salts (PFOA)" U.S. EPA EDocket OPPTS2003-0012-0007. U.S. Environmental Protection Agency, Washington, D. C., **2003**.
- 3 Ring, K.-L.; Kalin, T.; Kishi, A.; "Fluoropolymers," CEH Marketing Research Report, 2002.
- 4 Paustenbach, D. J.; Panko, S. M.; Scott, P.; Unice, K. Retrospective Modeling of potential residential exposure for perfluorooctanoic Acid (PFOA) releases from a manufacturing facility, manuscript submitted for publication.
- 5 Fluoropolymer Manufacturing Group, "Fluoropolymer Manufacturers Group Presentation Slides." U.S. EPA Administrative Record AR226-1094. U.S. Environmental Protection Agency, Washington, D. C., **2002**.
- 6 Fluoropolymer Manufacturing Group, "*Dispersion Processors Mass Balance Report*," U.S. EPA EDocket OPPT2003-0012-0900, -0901, -0902, -0903, -0904. U.S. Environmental Protection Agency, Washington, D. C., **2005**.
- 7 Asahi Glass Co., "Processing for producing perfluorocarboxylic acid." British Patent 1473807, **1975.**
- 8 Diamond Shamrock "*Process for Polymerizing Vinylidene Fluoride*" US Patent 3,475,395, **1969**.
- 9 PPG industries "Polymerization of Fluorine-Containing Ethenically Unsaturated Monomers in the presence of a Beta-Hydroxy-Alkyl Tertiary-Butyl Peroxide" US Patent 3,640,985, **1972**.
- 10 Diamond Shamrock "*Process for Preparing Vinylidene Fluoride Polymers for Coating Applications*" US patent 3,708,463, **1973**.
- 11 Pennwalt Corporation "*Emulsion Polymerization of Vinylidene Fluoride in the presence of Trichloromethane as Chain Transfer Agent*" US Patent 4,569,978, **1986**.
- 12 3M Company, "Environmental, Health and Safety Measures Relating to Perfluorooctanoic Acid and its Salts (PFOA)" U.S. EPA EDocket OPPTS2003-0012-0007. U.S. Environmental Protection Agency, Washington, D. C., **2003**.
- 13 Private communication, 3M Corporation.
- 14 Lange, C.C. "The aerobic biodegradation of N-EtFOSE alcohol by the microbial activity present in municipal wastewater treatment sludge. Biodegradation study report." 3M Project ID: LIMS E00-2252, **2000**.
- 15 3M Company, "*Phase-out Plan for POSF-Based Products*." U.S. EPA Administrative Record AR226-0588. U.S. Environmental Protection Agency, Washington, D. C., **2000**.
- 16 Fire Fighting Foam Coalition, "*Estimated Quantities of Aqueous Film Forming Foam* (*AFFF*) in the United States." U.S. EPA Administrative Record 226-1807. U.S. Environmental Protection Agency, Washington, D. C., **2004**.
- 17 U.K. Dept. of the Environment, Food & Rural Affairs (DEFRA) "*Risk Reduction Strategy* & *Analysis of the Advantages & Drawbacks for PFOS, Stage 4 Final Report,*" prepared by Risk & Policy Analysis, Norfolk, Loddon, U.K. March **2004**

- 18 Telomer Research Program, "*Letter of Intent*." U.S. EPA EDocket OPPTS-2003-0012-0013. U.S. Environmental Protection Agency, Washington, D. C., **2003**.
- 19 Telomer Research Program, "*Telomer Research Program Update-Presented to the USEPA OPPT, November 25, 2002.*" U.S. EPA Administrative Record 226-1141. U.S. Environmental Protection Agency, Washington, D. C., **2002**.
- 20 3M Environmental Laboratory "*Biodegradation Screen for Fluorotelomer Alcohols*." U.S. EPA Administrative Record 226-0555. U.S. Environmental Protection Agency, Washington, D. C., **2002**.
- 21 Wang, N.; Szostek, B.; Folsom, P. W.; Sulecki, L. M.; Capka, V.; Buck, R. C.; Berti, W. R.; Gannon, J. T. Aerobic Biotransformation of <sup>14</sup>C-labeled 8-2 Telomer B Alcohol by Activated Sludge from a Domestic Sewage Treatment Plant. *Environ. Sci. Technol.* 2005, 39, 531-538.
- 22 Dinglasan, M. J. A.; Ye, Y.; Edwards, E. A.; Mabury, S. A. Fluorotelomer Alcohol Biodegradation Yields Poly- and Perfluorinated Acids. *Environ. Sci. Technol.* **2004**, 38, 2857-2864.
- 23 Ellis, D. A.; Martin, J.W.; De Silva, A. O.; Mabury, S. A.; Hurley, M. D.; Sulbaek Andersen, M. P.; Wallington, T. J. Degradation of Fluorotelomer Alcohols: A Likely Atmospheric Source of Perfluorinated Carboxylic Acids. *Environ. Sci. Technol.* 2004, 38, 3316-3321.
- 24 Boulanger, B.; Vargo, J. D.; Schnoor, J. L.; Hornbuckle, K. C. Evaluation of Perfluorooctane Surfactants in a Wastewater Treatment System and in a Commercial Surface Protection Product *Environ. Sci Technol.* **2005**, 39, 5524-5530.