



Article

Synthesis, Property and Mechanism Analysis of a Novel Polyhydroxy Organic Amine Shale Hydration Inhibitor

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Abstract: Based on the adsorption mechanism analysis of polyhydroxy organic compound on a shale surface, a novel polyhydroxy organic amine shale hydration inhibitor N, N, N', N'-tetrakis (2-hydroxyethyl) ethylenediamine (THEED) was synthesized via a nucleophilic reaction by using diethanolamine and dibromoethane as raw materials. Its structure was characterized by Fourier transform infrared spectrometry (FTIR), Hydrogen Nuclear Magnetic Resonance (¹H NMR) and Liquid Chromatography Mass Spectrometry (LCMS). The inhibition performance of THEED was studied by a shale rolling recovery experiment, a linear expansion experiment and the particle size distribution experiment. Results showed the shale rolling recovery rate in 2.0 wt % THEED solutions was up to 89.6% at the rolling condition of 100 °C × 16 h, and the linear expansion height of artificial shale core in 2.0 wt % THEED solutions was just 4.74 mm after 16 h. The average particle size of Na-bentonite (Na-MMT) in fresh water was 8.05 μm, and it was observed that the average particle size has been increased to 124 μm in 2.0 wt % THEED solutions. The shale hydration inhibition mechanism of the novel inhibitor THEED was analyzed by FTIR, Scanning Electron Microscopy (SEM) and X-ray diffractometry (XRD), we concluded that the nice shale hydration inhibition performance of THEED was achieved by means of intercalation and adsorption onto the surface of shale. The superior shale hydration inhibition property makes THEED promising in maintaining wellbore stability in drilling engineering.

Keywords: polyhydroxy; shale hydration inhibitor; shale gas; drilling fluids; clay; organic amine

1. Introduction

China's predicted shale gas reserves are about $10\sim 47 \times 10^{12} \text{ m}^3$, which accounts for 5.7% of the world total reserves [1]. However, the mineral compositions of shale reservoirs in China are complicated, and hydration dispersion clay minerals, such as montmorillonite (which itself accounts for something in the range from 0%–15% of clay minerals in shale gas reservoirs), are usually encountered in drilling engineering [1]. Shale formations are known for their chemical interactions with water-based drilling muds, which may result in swelling, bit balling, or even closure of the wellbore [2–4]. When there is bentonite-rich shale gas formation exposure in drilling fluids, the strength of the shale gas wellbore will be greatly reduced and borehole instability occurred.

Therefore, the drilling fluids must have excellent shale hydration inhibition ability, in order to ensure the smooth progress of drilling engineering [5,6]. Oil-based drilling fluids (OBDFs) are

always the best drilling fluids option for drilling shale gas. However, the increasing demands for environmental legislation and excessive costs restrict these OBDFs in drilling applications. Water-based drilling fluids (WBDFs) are simple in their composition, are inexpensive, and the drilling waste is easily accepted by the environment; therefore, the development of WBDFs become an inevitable trend in drilling engineering [7–9]. But, the relatively poor inhibition of WBDFs has limited its application in shale gas drilling [10].

For a long time, a variety of drilling fluids additives generally referred to as ‘shale hydration inhibitor’ or ‘clay stabilizer’ have been developed and utilized to ensure the wellbore stability in shale gas drilling [11]. There are two ways by which shale hydration swelling will be inhibited during the drilling engineering; (i) through the intercalation of small organic molecules into the interlayer space of shale, and (ii) through the shale package by high molecular weight polymers [12]. The efficiency testing of a shale inhibitor is as old as the drilling fluids industry itself, and shale-drilling fluids testing remains an active topic of interest for drilling fluids evaluation, as the hydration expansion of shale is mainly caused by the expansive Na-MMT in the shale composition, the evaluation of a shale inhibitor generally by using Na-MMT. When shale inhibitor started to be deliberately utilized for wellbore stability, the reaction of these additives with swelling clay-rich shale formations became immediately apparent, and the oilfield industry has been trying to make sense of it all ever since [13,14].

A recent review by Stephens et al. recommends that the conventional test for different shale inhibitors are atmospheric swelling tests (linear expansion experiment), dispersion tests (hot-rolling test), capillary suction tests, bulk hardness tests, an immersion test and fracture development tests [15,16]. However, considering the economic and practical situation, the hot rolling recovery experiment, linear expansion experiment and particle size distribution experiment are the three usual testing methods in the laboratory. The hot rolling experiments can be used to analyze the ability of a shale inhibitor to inhibit the shale hydration dispersion. A linear expansion experiment is utilized to study the performance to inhibit the shale hydration expansion of inhibitors. The particle size analysis experiment has the function of comprehensively studying the shale inhibitor to inhibit shale hydration expansion and dispersion.

The shale hydration inhibitors which were used in the early stage of the oil industry are inorganic salts, such as potassium chloride, calcium chloride, ammonium chloride, etc. Relatively high amounts of inorganic shale hydration inhibitor are required, with amounts of potassium chloride ranging from 2–15 wt % typically being necessary to maintain wellbore stability. Some polymer inhibitors, such as asphalt, polymeric alcohols, ammonium salt polymers, zwitterionic polymers, nonionic polymers and cationic polymers have been successfully applied in the past years, and the concentrations of polymer typically being necessary ranging from 0.5 wt %–2 wt % [17]. These inhibitors alleviate the problem of wellbore instability to some extent for a period of time. However, present shale inhibitors still fail to fully meet the safe drilling needs of shale gas drilling at present [18].

Organic amine inhibitors have been proven show a certain shale hydration inhibition property by a large number of experiments [19]. Since the 1960s, small molecular organic amine inhibitors such as NH_4Cl , tetramethylammonium chloride, dimethyldiallylammonium chloride, amine derivative and polyamine have been applied in the past years. However, most organic amines have disadvantages, such as high level toxicity, poor temperature resistance and poor salt resistance performance, and these easily released the harmful gas NH_3 . The hydroxyl functional groups of molecules can form strong hydrogen bonds with the exposed OH (O) of shale, thus increasing the adsorption ability of the amine molecule onto the shale surface, which will provide more inspiration to the oil field researcher to design a shale inhibitor molecule [20–22].

What is more, results have shown that low molecular weight polyhydroxy organic amine can enter into the shale crystal layer, compressing the diffusion double layer and becoming strongly adsorbed onto the surface of the shale by the synergistic effect of a hydroxyl group and amine groups. However, few articles have reported the applications of polyhydroxy organic amine inhibitors in WBDFs [14,23].

Based on the adsorption mechanism analysis of polyhydroxy compounds on shale and the above review, a novel polyhydroxy organic amine shale hydration inhibitor N,N,N',N'-tetrakis (2-hydroxyethyl) ethylenediamine was synthesized via a nucleophilic reaction by using diethanolamine and dibromoethane as our raw materials. Its inhibition performance was evaluated by a shale hot rolling recovery experiment, a linear expansion experiment and particle size distribution experiment. Its shale inhibition mechanism was studied by means of FTIR, XRD and SEM in this paper.

2. Experimental

2.1. Materials

Diethanolamine, dibromoethane, ethanol, ethyl acetate, anhydrous magnesium sulfate (MgSO_4), anhydrous sodium carbonate (Na_2CO_3) and potassium chloride (KCl) were all analytically pure and purchased from Kelon Chemical Reagent Factory, Chengdu, China. NW-1 (a low molecule quaternary ammonium salt shale inhibitor) and mineral oil were provided by the Engineering Technology R&D Company limited, Beijing, China. Na-MMT was obtained from Xia Zijie Bentonite Technology Co., Ltd, and was used for inhibitor/Na-MMT preparation. The cation exchange capacity (CEC) of Na-Mt was 82 meq/100 g (0.82 mmol/g). The Na-MMT was suspended in distilled water, Na-saturated by repeated treatment with 1M Knack, and the $<2 \mu\text{m}$ fraction was collected. The excess of the Cl^- ions was removed by washing with distilled water. The sample (Na-Mt) was dried at 60°C and ground to pass a 0.2 mm sieve. The main compounds were of SiO_2 65.37%, Al_2O_3 20.23%, Fe_2O_3 3.07%, MgO 3.85%, Na_2O 2.65%, CaO 0.81% and K_2O 1.02%. The shale samples were obtained from Fuling Chongqing, and the mineral compositions were illustrated in Table 1.

Table 1. The mineral compositions of shale samples.

Mineral Compositions	Kaolinite	Chlorite	Illite	Sodium Bentonite	Illite/Sodium Bentonite
Content/%	0.0	26.3	65.1	8.6	10.0

2.2. Synthesis and Characterization of THEED

The prepared steps of N, N, N', N'-tetrakis (2-hydroxyethyl) ethylenediamine (THEED) are as follows: 0.2 mol diethanolamine, 0.1 mol dibromoethane and 75 mL ethanol were placed in a round-bottom flask equipped with a reflux condenser and refluxed for 12 h with magnetic stirring at 45°C . Then, 0.2 mol Na_2CO_3 was added and the reaction was continued for another 4 h. When reaction was finished, insoluble material was removed by filtration, and the ethanol was evaporated by a rotary distillation apparatus. The crude product was extracted with deionized water and ether, and the ether layer was dried with MgSO_4 to obtain the viscous product. After removing diethanolamine and ether from the product by vacuum distillation at the condition of $135\text{--}137^\circ\text{C}/0.1 \text{ mm Hg}$, a transparent, yellow final product THEED was obtained with a yield of 75.6%. The synthesis route of THEED is shown in Figure 1.



Figure 1. Synthesis route of N, N, N', N'-tetrakis (2-hydroxyethyl) ethylenediamine (THEED).

The infrared spectra were collected using the WQF-520 Fourier Transform Infrared (FTIR) spectrometer in the wavenumber range of $4000\text{--}400 \text{ cm}^{-1}$. Hydrogen Nuclear Magnetic Resonance (^1H NMR) spectra were carried out by using a Bruker AV-400 nuclear magnetic resonance spectrometer with chemical shift values in ppm downfield from TMS using D_2O as solvents. The Liquid Chromatography Mass Spectrometry (LCMS) test was acquired on a Shimadzu LCMS-2020 instrument,

the ion source was ESI, scanning range was m/z 90~900, nebulizing gas flow was 1.5 L/min, dry gas flow was 15.0 L/min. The column was Ascentis Express C18, its length was 50 mm, the internal diameter was 3.0 mm, and description was 2.7 μm . Scanning electron microscopy (SEM) characterization of 2 wt % THEED solution was obtained with a FEI Quanta 450 instrument, in the magnifying multiple ranges from 500 \times to 10000 \times .

2.3. Tests by Using Shale Samples

The hot-rolling tests are carried out with shale samples to study the inhibitive ability of THEED, and the retention percentage will be measured after hot-rolling the samples for a specific amount of time at the set temperature. In the experiments, we selected the most representative shale inhibitors KCl, mineral oil and NW-1 (a low molecular quaternary ammonium salt shale inhibitor), respectively, and compared the inhibition performance of THEED. The merits of the test consist of the fact that actual shale cuttings can be tested [15,16]. In this work, the obtained (50 ± 0.01 g) 40-mesh shale samples were dried at 105 $^{\circ}\text{C}$ for 24 h, and rolling the shale samples in high-temperature aging tanks filled with 350 ml (fresh water, 2.0 wt % inhibitor and mineral oil) solutions. The hot-rolling tests were carried out at 100 $^{\circ}\text{C}$ for 16 h. When these experiments were completed, the shale samples were carefully rinsed and filtered by a 100-mesh sieve, then dried to constant weight at 100 $^{\circ}\text{C}$, weighed, and from this we calculated the hot rolling recovery rate by Equation (1):

$$V_H = \frac{R_t}{50} \times 100\% \quad (1)$$

where R_t is the recycling mass, V_H is the rolling recovery rate.

2.4. Tests by Using Na-MMT

Linear swelling tests were carried out in the laboratory by using CPZ-2 swelling apparatus (Dongying, China). The advantages of the linear swelling test are ease to evaluate the efficiency of an inhibitor to inhibit shale swelling and low cost, and the linear swelling test is a very popular method in the laboratory [15,16]. The select principles of KCl, mineral oil and NW-1 have been explained in the "Tests by using shale samples" section. The artificial core was made by using 10 ± 0.01 g, 40-mesh Na-MMT powder, which was pressed tightly into a sample tube via a hydraulic compactor under 10 MPa for 5 min. The linear swelling rates over the whole experimental time at an atmospheric pressure condition were obtained.

2.5. Particle Size Analysis Tests

THEED with certain concentrations was added into WBDFs and stirred for 2 h. Then, particle size analysis was measured with a laser diffraction technique (HORIBA, Kyoto, Japan). The operating temperature was 25 $^{\circ}\text{C}$, the circulation speed was 2000 r/min., the repeatability error was less than 3%, the accuracy error less than 3%, the ultrasonic system was 40 Hz, 70 W, and the stirring speed was 100–475 rpm.

2.6. Inhibition Mechanism Study

2.6.1. FT-IR Analysis

1 g THEED was added into 100 mL WBDFs and stirred for 2 h, then centrifuged for 30 min and then we collected the precipitations. The precipitate was dried in a vacuum oven to constant weight at 50 $^{\circ}\text{C}$ for 24 h, and samples (pure THEED, pure Na-MMT and THEED/Na-MMT complex) were analyzed in the wavenumber range of 4000–400 cm^{-1} . The parameters of the infrared spectrometer were as follows: the spectral resolution was higher than 0.5 cm^{-1} and the wavelength accuracy was 0.1 cm^{-1} .

2.6.2. XRD Analysis

Samples were prepared as described in the “FTIR analysis” section, both the dry and wet precipitations were performed on an X Pert PRO MPD diffractometer (PANalytical B.V., Amsterdam, the Netherlands), the test angle was from 3° to 10° , and the angle accuracy was 0.0001.

2.6.3. SEM Analysis

SEM was investigated with the FEI Quanta 450 instrument (Thermo Fisher Scientific, Waltham, MA, USA), the range of the magnifying multiple was from 500 to 5000, the samples were trimmed from the bottom of the filter cake, and the images were obtained at 120–500 Pa. The acceleration voltage of FEI Quanta 450 was 0.02–30 kV, the Probe current was 12 pA–20 nA, and the stability ability was better than 0.2%/h.

3. Results and Discussion

3.1. Characterizations of THEED

FTIR, ^1H NMR and LCMS were utilized to determine the structure of THEED. Figure 2 shows the FTIR spectrum of THEED.

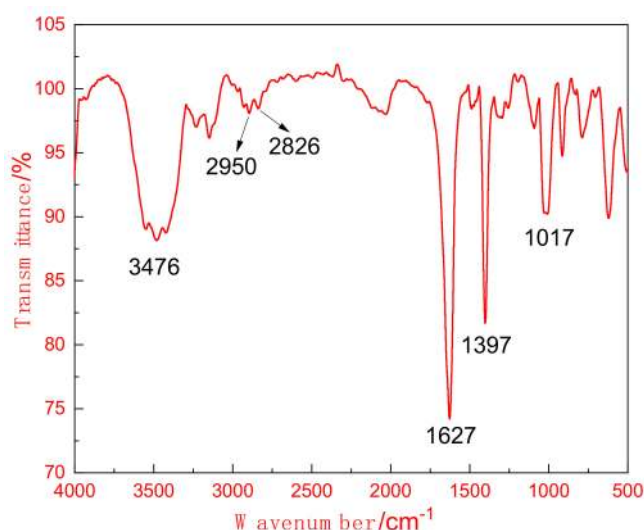


Figure 2. Fourier transform infrared spectrometry (FTIR) spectrum of THEED.

As shown in Figure 2, the peak at 3476 cm^{-1} was due to the $-\text{OH}$ stretching of THEED. Peaks at approximately 2950 cm^{-1} and 2826 cm^{-1} were assigned to the stretching vibration bands $-\text{CH}_3$ and $-\text{CH}_2$, respectively. The recorded strong peak at 1627 cm^{-1} was assigned to the bending vibration of NH groups. The peaks at 1397 cm^{-1} and 1017 cm^{-1} were attributed to the characteristic absorption bands of the CH groups. The FTIR characterization spectrum contains all characteristic functional group absorption peaks of the target product, initially indicating the successful preparation of THEED.

^1H NMR and LCMS were further used to confirm the structure and purity of the target product, and the results are shown in Figures 3 and 4, respectively. As shown in Figure 3, the chemical shifts of H are: 4.67 (m, 4H), $\text{C}-\text{O}-\text{H}$; 3.58 (s, 8H), $\text{N}-\text{C}-\text{CH}_2-\text{O}$; 2.66 (t, 8H), $\text{N}-\text{CH}_2-\text{C}$; 2.63 (t, 4H), $\text{N}-\text{CH}_2-\text{CH}_2-\text{N}$. In the LCMS spectrum as displayed in Figure 4, the purity of THEED was as high as 99.7%. The FTIR, ^1H NMR and MS results all indicated that THEED has been successfully prepared.

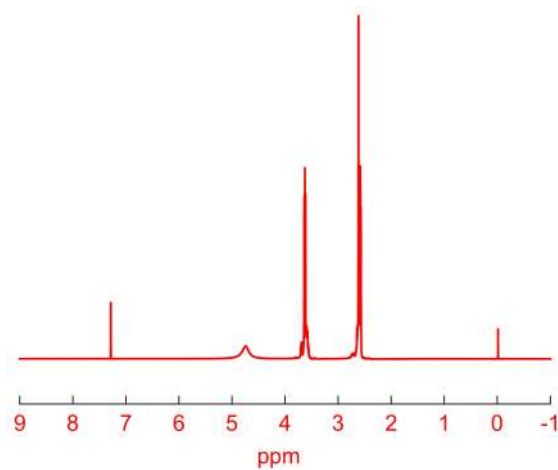


Figure 3. Hydrogen nuclear magnetic resonance (¹H NMR) spectrum of THEED.

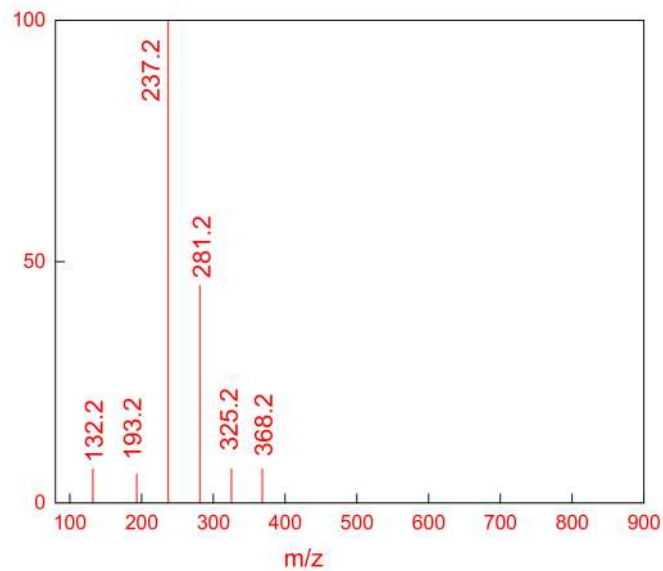


Figure 4. Mass Spectrometry (MS) spectrum of THEED.

The SEM characterization of 2.0 wt % THEED solutions is shown in Figure 5. The SEM image shown in Figure 5 reveals that an obvious gel-network microstructure was formed in 2.0 wt % THEED solution, indicating there was a pulling behavior with each other between THEED molecules, and thus the result of this study was similar to those reported in the literature [24,25].

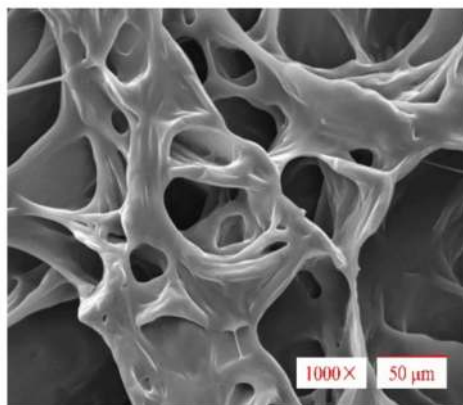


Figure 5. Scanning electron microscopy (SEM) image of THEED.

Cross-linking effects were formed depending on the hydrogen bonds formed between the THEED molecules, and then present a three-dimensional network structure in THEED solutions, where the literature [26–28] interprets this pulling behavior as “self-assembly”.

3.2. Inhibition Property Evaluation

3.2.1. Hot-Rolling Recovery Tests

The hot-rolling recovery tests were carried out at 100 °C for 16 h, as shown in Figure 6.

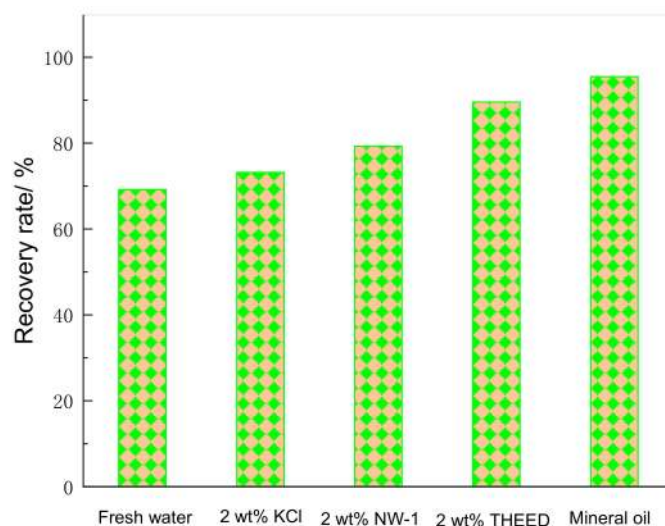


Figure 6. Hot-rolling recovery tests.

The hot-rolling recovery rate of the shale sample in fresh water was 69.2%, indicating the comparatively high dispersion degree of this shale sample. With the addition of a different shale inhibitor, the rolling recovery rates have been improved to some extent. As there were very small amounts of expansive clay minerals in shale sample, it was difficult for KCl to enter into the crystal layers, and the recovery rate of shale in 2 wt % KCl solutions increased slightly [29]. After adding quaternary ammonium salt NW-1, the rolling recovery rate increased to 79.3%, indicating that NW-1 could play a certain role in inhibiting shale dispersion. THEED contains a large number of adsorptive hydroxyl functional groups, which can be firmly adsorbed on the surface of shale through hydrogen bonds and electrostatic forces [30,31], and could compress the shale diffusive electric double layer and replacing the interlayer water of shale. The hot-rolling recovery rate of the shale sample in 2 wt% THEED solutions was 89.6%, and the recovery rate reached up to 95.5% in mineral oil, where there was the absence of water in mineral oil.

3.2.2. Linear Swelling Tests

In this part, linear swelling tests of the artificial shale core made by Na-MMT exposed to fresh water and different shale inhibitor solutions at room temperature and room pressure were studied, as shown in Figure 7.

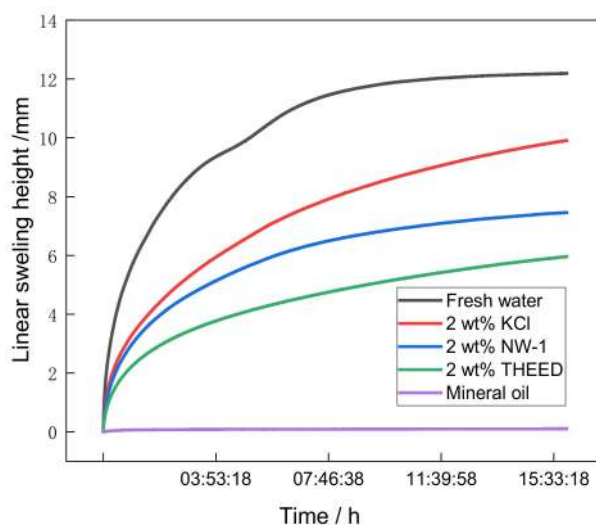


Figure 7. Linear swelling tests in different solution.

For all cases, the artificial shale core swelling height increased fast within the first 100 min, and followed by a relatively slight increase within the rest test time. Within the whole experimental time, the swelling height in fresh water (base height) was significantly higher (12.19 mm) than other inhibitor solutions. K^+ is well known to be the preferred inorganic inhibitor in WBSFs, and the widely held belief is that the low hydration energy and small ionic radius ensure the embedding of K^+ into clay [29], as shown in Figure 8. NW-1 and THEED could enter the layer of the tetrahedral crystal of shale and compress the diffusion electric double layer of shale due to the small volume of both of them. Linear expansion height of shale core sample in 2.0 wt % THEED solution was just 4.74 mm after 16 h, which was much lower than other cases in the study, except in mineral oil.

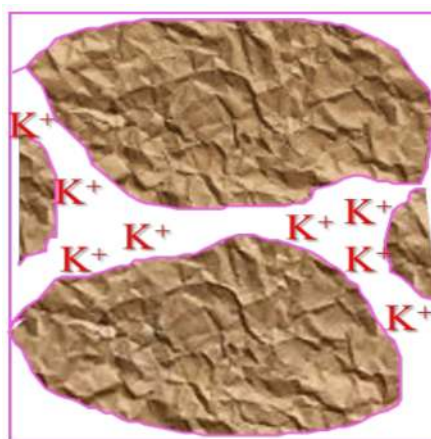


Figure 8. The clay inhibition mechanism of K^+ .

3.2.3. Particle Distribution Tests

It is well known that the negative charge surface of the shale is trendy to be neutralized by the positive charge of cations, and flocculation will occur when organic amine was added to the WBSFs. The shale particle disintegration test describes the hydration and disintegration of a shale sample when immersed in drilling fluid [32]. The inhibition performance was further evaluated by particle distribution tests.

As shown in Figure 9 for the case in fresh water, Na-MMT illustrated a tiny average particle size at 8.05 μm . In this work, the particle size of Na-MMT has been increased to 124 μm in 2.0 wt % THEED solutions. The reasons may be as follows: THEED and Na-MMT are adsorbed together by hydrogen

bonding and the Van der Waals force, resulting in the negative charge on the surface of Na-MMT being neutralized by THEED, so the diffusive electric double layer was being compressed, and resulting in the aggregation of Na-MMT.

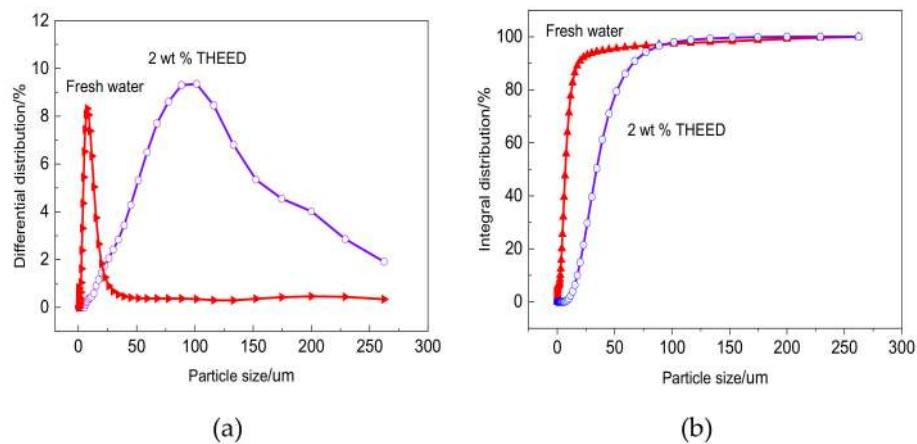


Figure 9. Particle distribution tests of THEED. (a) Differential distribution of samples. (b) Integral distribution of samples.

3.3. Inhibition Mechanism Analysis

The clay mineral composition of shale is very complicate, and the shale hydration expansion is just mainly caused by the swelling clay mineral (Na-MMT) in shale. In this work, we selected the highly expansive Na-MMT as the research object to analyze the inhibition mechanism of THEED.

3.3.1. FT-IR Analysis

FTIR is a sensitive technique to analyze the interaction type, configuration and local environment of Na-MMT modified by an intercalating agent. The inhibition mechanism has been analyzed by FTIR, as shown in Figure 10.

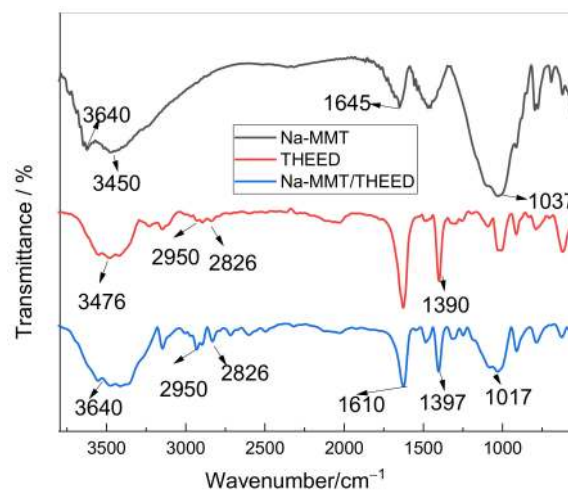


Figure 10. Inhibition mechanism analysis of THEED by FTIR.

The stretching vibrations of the structural OH groups occur at 3640 cm⁻¹, while the AlAlOH and AlMgOH bending bands are observed at 921 cm⁻¹ and 848 cm⁻¹, respectively. The bands at 3450 cm⁻¹ and 1645 cm⁻¹ correspond to the OH stretching and bending vibrations of water molecules present in the montmorillonite [33–35].

A strong complex band at 1037 cm^{-1} is attributed to the stretching vibration of the Si–O groups of the tetrahedral sheets and the absorption bands at 525 cm^{-1} and 467 cm^{-1} belong to Si–O–Al and Si–O–Si bending vibrations, respectively. Some peaks belong to THEED, such as 3476 cm^{-1} , 2950 cm^{-1} , 2826 cm^{-1} , 1627 cm^{-1} , 1397 cm^{-1} and 1017 cm^{-1} , which were observed in the spectrum of the Na-MMT/THEED composite material, which indicated the successful adsorption of Na-MMT onto THEED. Adsorption bands at 1610 cm^{-1} corresponding to the adsorbed water was weaker when compared to the pure Na-MMT at 1645 cm^{-1} , showing the significant decrease of adsorbed water in Na-MMT. This phenomenon is similar to that reported in the literature [35,36]. Decreased intensity was observed near the vibration band of Si–O at 1037 cm^{-1} in Na-MMT, indicating that THEED could react with part of Si–O in Na-MMT.

3.3.2. XRD Analysis

Clay layers, mainly of the value of the basal spacing $d_{(001)}$, were affected by water molecules, cationic compounds, adsorbents, intercalating agents, etc. [33]. The inhibition mechanism of THEED was further analyzed by X-ray diffractometry (XRD), and these results are shown in Figure 11.

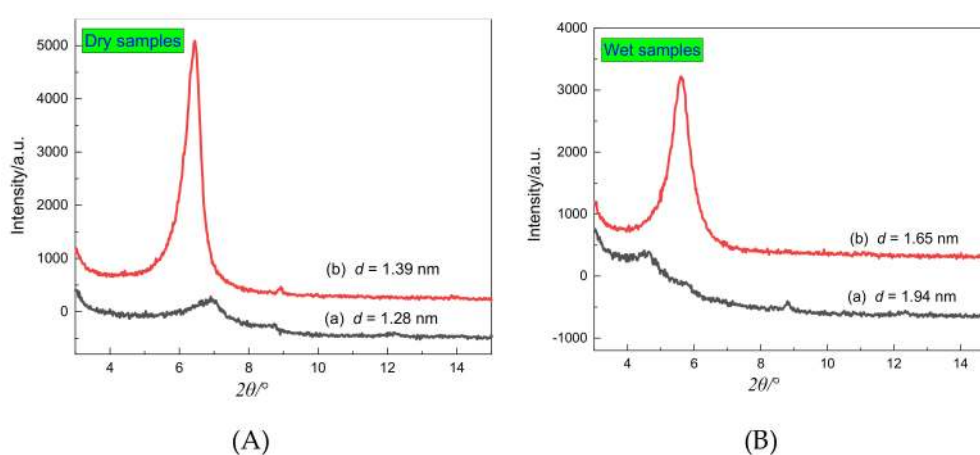


Figure 11. X-ray diffraction (XRD) patterns of samples: a pure Na-MMT; b Na-MMT/2 wt % THEED. (A) XRD curves of dry samples. (B) XRD curves of wet samples.

Figure 11 shows X-ray diffraction patterns of both dry and wet samples for the basal spacing $d_{(001)}$ diffraction peaks of Na-MMT and Na-MMT/THEED. As displayed, it can be seen that the interlayer spacing of dry Na-MMT is 1.28 nm, and the interlayer spacing has increased to 1.39 nm after the intercalation with 2 wt % THEED, which indicated that THEED had successfully entered and strongly adsorbed onto the interlayer of Na-MMT by the adsorption groups of THEED. In the wet cases, the interlayer spacing of Na-MMT in fresh water was 1.94 nm, while 2.0 wt % THEED could reduce the interlayer spacing to 1.65 nm. From the above results, we concluded that the amino group and hydroxyl groups of THEED can form hydrogen bonds with the Na-MMT surface, and replaced part of adsorbed water in the interlayer layer of Na-MMT and effectively inhibited the hydration expansion of Na-MMT.

3.3.3. SEM Analysis

SEM is a convenient technology to observe the morphological changes of Na-MMT composites. The obtained SEM images are demonstrated in Figure 12.

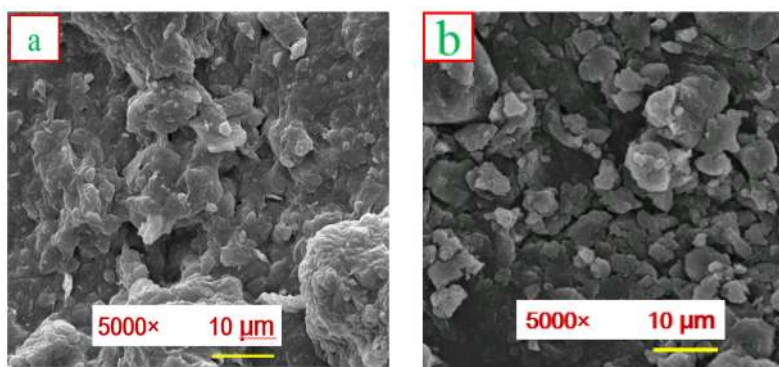


Figure 12. SEM analysis of samples. (a) The basic drilling fluids cake; (b) the Na-MMT/THEED cake.

Noticeable morphologic differences were observed in the different cake. The SEM image of basic drilling fluids cake showed the distinct wave-like, rough and homogeneously fluffy-shaped particles, as shown in Figure 12a. After treatment with 2 wt % THEED, the surface has become smooth and compact, the rough particles were stacked together in an excursive pattern to form slightly curled and crumpled edges (Figure 12b), which indicated the adsorptive reaction between THEED with Na-MMT. In addition, we also observed the appearance of micro-voids in the surface, which was probable due to the force decrease between Na-MMT sheets [37,38]. The bigger particle size has indicated that the intercalation happened between THEED and Na-MMT.

Through the inhibition property evaluation of THEED by a range of methods, and with reference to inhibition mechanism analysis in this work and in other work [39], we have proposed the inhibition mechanism of THEED on shale, as shown in Figure 13. With there being hydroxyl and amine functional groups in THEED, the polyhydroxy organic amine can enter into the shale crystal layer, compress the diffusion double layer of clay, pull the crystal layer together and prevent the hydration expansion and dispersion of shale.

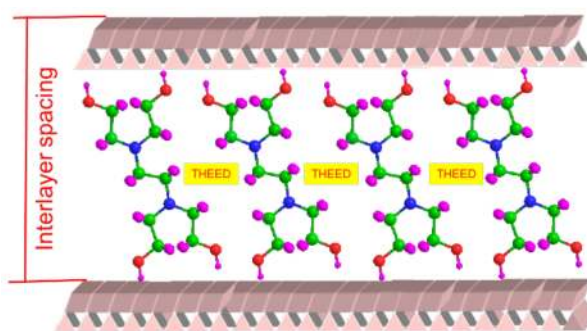


Figure 13. Inhibition mechanism analysis of THEED.

4. Conclusions

In conclusion, a novel polyhydroxy organic amine shale hydration inhibitor THEED was successfully synthesized in this work. Its structure was confirmed by FTIR, ^1H NMR and LCMS. Its inhibition performance was studied by several evaluation experiments, and results showed the outstanding shale hydration inhibition performance of THEED. We also utilized FTIR, XRD and SEM to study its inhibition mechanism, and it was found that THEED can be firmly adsorbed on the shale surface and enter into the interlayer of shale. In addition, THEED can change the appearance of Na-MMT by physical and chemical interaction with Na-MMT, and in that way achieve a good inhibition result. In summary, THEED shows excellent shale inhibition performance, and is expected to be applied in WBDFs.

Author Contributions: Conceptualization, W.D. and X.W.; Formal Analysis, M.S.; Investigation, G.C.; Writing—Original Draft Preparation, J.Z.; Writing—Review & Editing, M.S.; Supervision, W.D. and M.S.; Project Administration, W.D.; Funding Acquisition, W.D.; and all authors wrote the paper. All authors have read and agreed to the published version of the manuscript.

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Conflicts of Interest: The authors declare no conflict of interest.

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