

This is the submitted version of the following article: Abu Yazid, N; Barrena. R. and Sánchez, A. *The immobilization of proteases produced by SSF onto functionalized magnetic nanoparticles: application in the hydrolysis of different protein sources* in Journal of molecular catalysis B: enzymatic (Ed. Elsevier), vol. 133, suppl. 1 (Nov. 2016), p. S230-S242, which has been published in final form at

DOI 10.1016/j.molcatb.2017.01.009

© 2016. This manuscript version is made available under the CC-BY-NC-ND 4.0 license <http://creativecommons.org/licenses/by-nc-nd/4.0/>

1           **The immobilisation of proteases produced by SSF onto functionalized magnetic**  
2           **nanoparticles: Application in the hydrolysis of different protein sources**

3  
4  
5                   Noraziah Abu Yazid, Raquel Barrena, and Antoni Sánchez\*

6  
7   Composting Research Group

8   Department of Chemical, Biological and Environmental Engineering

9   Escola d'Enginyeria

10   Universitat Autònoma de Barcelona

11   08193-Bellaterra (Barcelona, Spain)

12  
13   \*Corresponding author:

14   Tel.: +34 935811019

15   Fax: +34 935812013

16   Email address: antoni.sanchez@uab.cat  
17  
18  
19  
20  
21  
22  
23  
24  
25  
26  
27

28 **ABSTRACT**

29 Alkaline proteases produced from protein-rich waste (hair waste and soya residues)  
30 by solid state fermentation (SSF) were immobilised onto functionalized magnetic iron oxide  
31 nanoparticles (MNPs) using glutaraldehyde as a crosslinking agent. The covalent binding  
32 method had a better immobilisation yield compared to simple adsorption, retaining 93%-96%  
33 (459±106 U/mg nanoparticles, 319±34 U/mg nanoparticles) of hair waste and soya residues  
34 proteases, respectively after crosslinking with 5% glutaraldehyde for 6 h. However, the  
35 adsorption immobilisation yield was 47%-54% after 8 h for both proteases. MNPs and  
36 immobilised proteases were characterized using transmission electron microscopy (TEM),  
37 scanning electron microscopy (SEM), Fourier transform infrared spectroscopy (FT-IR) and  
38 electron diffraction. Our results indicated successful crosslinking between the proteases and  
39 amino-functionalized MNPs. **The operational stability (pH and temperature) and storage**  
40 **stability of free and immobilised enzyme were also analysed.** Despite the fact that the  
41 optimum pH of free and immobilised proteases was identical in the alkaline region, the  
42 immobilised proteases reached their optimum condition at higher temperatures (~~40°C–60°C~~  
43 **40 °C – 60 °C**). After 2 months of storage at ~~4°C~~ **4 °C**, the immobilised proteases showed  
44 good stability, retaining more than 85% of their initial activity. The high magnetic response  
45 of MNPs render an ease of separation and reusability, which contributes to the residual  
46 activity of both immobilised proteases on MNPs ~~remained retaining~~ more than 60% of their  
47 initial values after seven hydrolytic cycles. These results ~~resulted showed~~ the enhancement of  
48 the stability of the crosslinking interactions between the proteases and nanoparticles. The  
49 immobilised proteases were capable of hydrolysing ~~select selected~~ proteins (casein, oat bran  
50 protein isolate, and egg white albumin). However, differences in the degree of hydrolysis  
51 were observed, depending on the combination of the protease and type of substrate used.

52 *Keywords:* protease; protein-rich waste; solid state fermentation; hydrolysis; immobilisation

## 53 **1. Introduction**

54 Because of the proteolytic nature of alkaline proteases, they have been commercially  
55 utilised for industrial applications, explicitly in the food, pharmaceutical, textile, detergent,  
56 and leather industries [1,2]. Their specific role in protein hydrolysis has drawn worldwide  
57 attention regarding the versatility of these enzymes for biotechnological applications.  
58 Currently, the general cost of protease production is very high, considering the cost of  
59 substrates, commercial media and maintenance of cultures used for inoculation. For this  
60 reason, the need to develop novel processes with higher yields is highly recommended from a  
61 commercial point of view [3].

62 Different options have been considered to reduce the cost and increase the utilization of  
63 proteases. One of the most promising alternatives is solid state fermentation (SSF), which  
64 allows the procurement of value-added products using inexpensive waste as a solid substrate.  
65 SSF has been successfully applied in the production of proteases using protein-rich waste  
66 without the need to inoculate a specific microorganism [4,5]. In addition to recycling the  
67 abundant solid waste produced by industries as cheap substrates, SSF avoids the hassle of  
68 maintaining cultures since microorganism can develop mutations over time [6].  
69 Economically, no additional cost is required, as there is no restricted sterilized environment  
70 required to produce proteases through SSF since a specific microorganism for inoculation is  
71 not involved.

72 Apart from that, soluble proteases are susceptible to autolysis, which leads to their rapid  
73 inactivation. The instability and lack of flexibility, reusability and recovery make their use a  
74 challenge for commercialization. Therefore, the use of immobilisation enzymes offers an  
75 attractive method in which immobilised enzymes have enhanced stability that allows for their  
76 recyclability and simple recovery without contamination of the final product [7]. There are

77 five basic enzyme immobilisation methods, including simple adsorption, covalent binding,  
78 encapsulation, crosslinking, and entrapment [8].

79 ~~Of all the methods, covalent binding provides firm binding between the enzyme and~~  
80 ~~carrier and avoids enzyme, as it can be regulated by using specific functional groups (-NH<sub>2</sub>,~~  
81 ~~SH) to bind with the proteins. Of all the methods, covalent binding provides firm binding~~  
82 ~~between the enzyme and carrier, thus avoiding enzyme leakage as it can be regulated by~~  
83 ~~using specific functional groups (-NH<sub>2</sub>, -SH) [9]. This method of immobilisation provides an~~  
84 ~~efficient way to increase the stability and flexibility of enzyme reusability and recovery [10].~~  
85 Coupling agents, such as glutaraldehyde, maleic anhydride and genipin, have been widely  
86 used as their functional groups can interact with the functional groups of modified carriers  
87 and proteins [10,11]. Glutaraldehyde can be used either to alter enzymes after immobilisation  
88 or to activate the support for enzyme immobilisation. In addition, the use of glutaraldehyde  
89 can increase protein stability, thus avoiding protease autolysis [2,12].

90 In recent years, the immobilisation of enzymes onto nanomaterials, particularly iron oxide  
91 magnetic nanoparticles (MNPs), to form nanobiocatalysts has attracted much attention in  
92 some fields of research, including biolabeling, bioseparation, biosensors, biofuel cells, and  
93 environmental analysis [9,13]. The use of MNPs has been particularly attractive for  
94 immobilisation because of their special characteristics, such as their high surface area, simple  
95 manipulation and separation by the application of an external magnetic field,  
96 biocompatibility, biodegradability, and low toxicity [10,14]. ~~There are several studies~~  
97 ~~reporting the application of purified protease immobilised on magnetic supports [15–18];~~  
98 ~~however there are only a few studies that have exploited MNPs for crude protease~~  
99 ~~immobilisation and further use in protein hydrolysis and synthesis [19].~~

100 In this work, the use of relatively inexpensive enzyme preparative for immobilisation  
101 onto functionalized MNPs and crosslinking with glutaraldehyde was assessed. The goal was

102 to test the viability of using low-cost proteases derived from animal (hair waste) and  
103 vegetable (soy fibre residues) protein-rich waste that were produced by SSF after being  
104 immobilised onto functionalized MNPs in the hydrolysis of different type of proteins. The  
105 relative differences in terms of stability and reusability between the free and immobilised  
106 enzymes were significant, exhibiting the feasibility of the immobilised enzymes produced in  
107 this work. Also, the magnetic properties of the support render a convenient separation  
108 between the substrate and the enzymes within the catalytic system.

109

## 110 **2. Materials and Methods**

### 111 *2.1 Material and reagents*

112 Ferric chloride ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ), ferrous sulphate ( $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ ), (3-aminopropyl)-  
113 triethoxysilane (3-APTES, 97%), glutaraldehyde solution (50%), cetyl-trimethyl-ammonium  
114 bromide (CTAB), trichloroacetic acid (TCA), Folin-Ciocalteu reagent, casein from bovine  
115 milk, and egg white albumin were obtained from Sigma-Aldrich (Spain). Oat bran containing  
116 17.6% protein was purchased from a supermarket (Mercadona, Spain). Hair waste with a  
117 protein content of 75.6% was obtained from the local tanning industry located in Igualada,  
118 Barcelona, and soya fibre residues with a protein content of 25.1% were received from  
119 Natursoy, Spain.  $\beta$ -mercaptoethanol, tricine sample buffer, 10%-20% Mini-PROTEAN gels,  
120 and Coomassie 250 stain were purchased from Bio-Rad (Spain). All other chemicals were  
121 from commercial sources and were of analytical grade.

### 122 *2.2 Preparation of the protease enzyme concentrates from protein-rich waste using SSF*

123 Two different sources of alkaline proteases were produced from protein-rich waste, hair  
124 waste and soya fibre residues using solid state fermentation (SSF) as described elsewhere  
125 [4,5]. Briefly, hair waste and soya fibre residues were individually mixed with anaerobically

126 digested sludge at a weight ratio of 1:2, and then, the mixtures were added to a bulking agent  
127 (wood chips) at a volumetric ratio of 1:1. SSF was undertaken in triplicate using 10 L air-  
128 tight reactors for approximately 1 to 3 weeks. Later, the proteases, Phw from hair waste and  
129 Psr from soya fibre residues, were extracted from the reactors using Tris-HCl buffer (50 mM,  
130 pH 8.1). The times for extracting proteases for different substrates were specified for each  
131 case based on the maximum activity of the protease produced during SSF. Phw at day 14<sup>th</sup>  
132 yielded 787±124 U/g DW, and Psr at day 4<sup>th</sup> yielded 634±24 U/g DW. The extracts were  
133 ultrafiltrated through Amicon Ultra-15 centrifugal filter devices (Millipore, Ireland) with a  
134 10kDa molecular weight cut-off (MWCO) prior to lyophilisation. The initial activities after  
135 lyophilisation for Phw and Psr were 466 U/ml and 330 U/ml, respectively.

### 136 *2.3 Preparation of oat bran protein isolate (OBPI)*

137 The preparation of oat bran protein isolate (OBPI) was performed as described elsewhere  
138 [20] with slight modifications. Briefly, oat bran was added to 1.0 M NaCl at a ratio of 1:8  
139 (w/v), and the pH was adjusted to 9.5 using 1.0 M NaOH. The mixture was agitated for 30  
140 min at room temperature. Then, the supernatant was collected after centrifuged at 5,000 x g  
141 for 25 min at ~~4°C~~ 4 °C. The pH was adjusted to 4 with 1.0 M HCl prior to centrifugation at  
142 5,000 x g for 40 min at ~~4°C~~ 4 °C. The supernatant was then discarded, and the protein isolate  
143 was dissolved in Milli-Q water and adjusted to pH 7 with 0.1 M NaOH. The protein isolate  
144 was lyophilised and stored at ~~-20°C~~ -20 °C for future use.

### 145 *2.4 Synthesis of amino-functionalized Fe<sub>3</sub>O<sub>4</sub> magnetic nanoparticles (MNPs)*

146 Magnetic nanoparticles (MNPs) were synthesised by co-precipitation in water phase  
147 [21,22] with slight modifications. A mixture of 25 mM ferrous sulphate and 50 mM of ferric  
148 chloride were dissolved in 100 ml of Milli-Q water with the addition of 0.1% of CTAB as a  
149 stabiliser. The mixture was stirred at ~~40°C~~ 40 °C for 1 hour under ~~a-the~~ nitrogen atmosphere.

150 Then, 125 ml of deoxygenated NaOH (0.5 M) was added dropwise to the mixture, and the  
151 mixture was left for 1 hour at ~~40°C~~ 40 °C to let the solution chemically precipitate. The  
152 resultant MNPs were separated magnetically and washed five times with Milli-Q water. The  
153 recovered MNPs were dried overnight at ~~60°C~~ 60 °C.

154 The surface of the MNPs was modified using a silanization reaction. Approximately 0.61  
155 g of MNPs was dispersed in a solution containing 3.05 ml of APTES, 0.763 ml of Milli-Q  
156 water, and 45.75 ml of methanol. The mixture was ultrasonically agitated for 30 min. Then,  
157 10 ml of glycerol was added and heated at ~~90°C~~ 90 °C for 6 h, and the mixture was stirred  
158 until separation. The surface-modified MNPs were recovered by applying a magnet, and they  
159 were washed three times with Milli-Q water.

#### 160 *2.5 Immobilisation of alkaline proteases (Phw, Psr)*

161 ~~For immobilisation of surface modified MNPs, 1 ml of alkaline protease from hair waste~~  
162 ~~(Phw) with an initial activity 466 U/ml or alkaline protease from soya residue (Psr) with an~~  
163 ~~initial activity 330 U/ml was dispersed in 9 ml of Tris HCl buffer (pH 8.1) and mixed with~~  
164 ~~100 mg of amino functionalized MNPs. The activation of the NH<sub>2</sub> groups in the nanoparticles~~  
165 ~~was carried out by adding glutaraldehyde as a crosslinking agent at various concentrations~~  
166 ~~(1%, 2.5%, and 5% (v/v)). The mixture was gently agitated at 4°C 4 °C for 8 h. Subsequently,~~  
167 ~~the immobilised proteases were separated by a magnetic field, washed five times with Tris~~  
168 ~~buffer (50 mM, pH 8.1) to remove any unbound glutaraldehyde and finally resuspended in 1~~  
169 ~~ml of Tris buffer (50 mM, pH 8.1). The immobilised proteases were stored at 4°C 4 °C for~~  
170 ~~future use.~~

171 To begin with immobilisation of protease onto surface-modified MNPs, 1 ml of alkaline  
172 protease from hair waste (Phw) with an initial activity 466 U/ml and alkaline protease from  
173 soya residue (Psr) with an initial activity 330 U/ml, respectively, was dissolved in 9 ml of  
174 Tris-HCl buffer (pH 8.1). Then, 100 mg of amino-functionalized MNPs was dispersed into



175 the mixture. Afterwards, the activation of the NH<sub>2</sub> groups in the nanoparticles was carried out  
 176 by adding glutaraldehyde as a crosslinking agent at various concentrations (1%, 2.5%, and  
 177 5% (v/v)) in the mixtures, followed by gentle agitation at 4 °C for 8 h. Subsequently, the  
 178 MNPs with the immobilised proteases (MNPs-protease) were separated by a magnetic field  
 179 and washed five times with Tris buffer (50 mM, pH 8.1) to remove any unbound  
 180 glutaraldehyde and enzyme. Finally, the MNPs-protease were resuspended in 1 ml of Tris  
 181 buffer (50 mM, pH 8.1) and stored at 4 °C for further application.

182 For immobilisation via adsorption, approximately 100 mg of naked MNPs were dispersed  
 183 in 9 ml of the Tris buffer solution (50 mM, pH 8.1). Then, 1 ml of free alkaline protease from  
 184 hair waste (466 U/ml) or soya residue (330 U/ml) was added. The mixture was gently  
 185 agitated at 4°C 4 °C for 8 h. Later, the immobilised proteases were magnetically separated  
 186 and treated as previously described.

187 The immobilisation yield (%) and the amount of immobilised protease (Phw<sub>im</sub>, P<sub>sr</sub><sub>im</sub>)  
 188 loading on MNPs (U/mg) were calculated using following equations (Eqs. 1, 2) [15,23]:

$$189 \text{ Enzyme loading (U/mg)} = (U_i - U_{sp})/W \quad (1)$$

$$190 \text{ Immobilisation yield (\%)} = (U_i - U_{sp})/U_i \times 100 \quad (2)$$

191 Where U<sub>i</sub> is the initial enzyme activity (U), U<sub>f</sub> is the enzyme activity in the supernatant after  
 192 immobilisation (U), and W is the weight of MNPs used for immobilisation (mg).

193 Furthermore, the immobilisation efficiency (%) and activity recovery (%) were calculated as  
 194 follows (Eqs. 3, 4) [23]:

$$195 \text{ Efficiency (\%)} = (U_e/U_{imm}) \times 100 \quad (3)$$

$$196 \text{ Activity recovery (\%)} = (U_e/U_i) \times 100 \quad (4)$$

197 Where  $U_e$  is the activity of bound enzyme that is measured in the immobilisate (U),  $U_{imm}$  is  
198 the immobilised enzyme activity determined from subtracting the remaining enzyme activity  
199 in the supernatant from the initial activity (U).

## 200 *2.6 Characterization of the immobilised enzymes*

201 Functionalized MNPs before and after immobilisation were characterized using high  
202 resolution transmission electron microscopy (HRTEM, JEM-2011/JEOL) and scanning  
203 electron microscopy (SEM, Zeiss Merlin). The samples were prepared by placing a drop of  
204 the sonicated solutions on a copper grid, and then, the samples were allowed to dry. Samples  
205 with the immobilised enzyme were stained with uranyl acetate (2%) prior to analysis.  
206 Functionalized nanoparticle immobilisation was then confirmed using Fourier Transform  
207 Infrared spectroscopy (FT-IR, Bruker Tenser 27) within a range of 500-4,000  $\text{cm}^{-1}$ .

## 208 *2.7 Stability of immobilised protease*

209 The storage stability was determined by maintaining the immobilised enzymes via  
210 crosslinking and simple adsorption at ~~4°C~~ 4 °C for 60 days. The activity of the enzymes was  
211 measured at day 0<sup>th</sup> as the initial activity, while the activity for the 60<sup>th</sup> and 7<sup>th</sup> days were used  
212 as the final activity of the immobilised enzymes and free enzymes, respectively.

213 To study the operational stability, both immobilised and free enzymes were incubated for  
214 1 h at various pH and temperature values according to the response surface of the central  
215 composite design (CCD) performed using the Design-Expert software (version 6.0.6). The  
216 CCD consisted of 13 experimental points, including five replications at the central point and  
217 four star points ( $\alpha = 1$ ). The pH was adjusted using the following buffers: acetic acid-sodium  
218 acetate 1 M (pH 5), Tris-HCl 1 M (pH 8), and  $\text{Na}_2\text{HPO}_4$ -NaOH 0.05 M (pH 11). Analysis of  
219 variance (ANOVA) was conducted to determine the significance of the main effects.

220 ~~The residual activity of each factor tested was calculated by that assuming the initial~~  
221 ~~activity of the immobilised or free enzyme was 100%.~~ The residual activity of each factor  
222 was calculated by assuming that the initial activity of the immobilised or free enzyme is  
223 100%.

#### 224 *2.8 Reusability of immobilised protease*

225 The reusability of immobilised proteases from hair waste (Phw) and soya fibre residue  
226 (Psr) was tested on casein as a model protein. The initial activities of the immobilised  
227 enzymes were measured and compared with seven consecutive repeated uses of immobilised  
228 enzymes under the assay conditions. After each cycle, immobilised enzymes were  
229 magnetically separated and washed with Tris-HCl buffer (50 mM, pH 8.1). Then, they were  
230 resuspended in fresh medium and incubated at ~~50°C~~ 50 °C for 120 min. The activity of  
231 immobilised enzymes from the first batch was considered to be 100%.

#### 232 *2.9 Application of immobilised proteases in protein hydrolysis*

233 Prior to hydrolysis, 4% (w/v) suspension of selected proteins (casein from bovine milk,  
234 egg white albumin, and OBPI) in Tris-HCl buffer (50 mM, pH 8.1) were incubated at ~~50°C~~  
235 50 °C for 15 min. Then, the reaction was initiated by adding 1 ml of free enzymes (330-460  
236 U/ml) or 1 ml immobilised enzymes suspension (319-459 U/mg NP) into 9 ml of substrate.  
237 The mixture was incubated in a water bath at ~~50°C~~ 50 °C with mechanical agitation at 100  
238 rpm. An aliquot of ~~six~~ 6 ml was withdrawn at 0.5, 2, 4, 6, and 24 h. The free enzyme activity  
239 was deactivated by heating the samples in boiling water for 15 min. Then, the samples were  
240 cooled by placing the samples in a cold water bath for 15 min. Afterwards, the samples were  
241 centrifuged at 5,000 x g for 15 min to separate any impurities or enzyme from the  
242 hydrolysate. The immobilised enzyme was separated from the hydrolysate by a magnetic  
243 drive. The hydrolysate was kept frozen at ~~-80°C~~ -80 °C prior to lyophilisation.

## 244 2.10 Analytical methods

### 245 2.10.1 Protease assay

246 The proteolytic activity of the free and immobilised protease was determined using  
247 casein as a substrate according to method described by Alef and Nannipieri [24] with slight  
248 modifications. Briefly, 1 ml of the enzyme extract (free enzyme) or 0.1 g of immobilised  
249 protease in 0.9 ml of Tris buffer (pH 8.1) was added to 5 ml of a 2% (w/v) casein solution  
250 and incubated at ~~50°C~~ 50 °C and 100 rpm for 1 hour. The reaction was terminated by adding  
251 5 ml of 15% (w/v) TCA. The samples were centrifuged at 10,000 rpm for 10 min at ~~4°C~~ 4 °C.  
252 An aliquot of 0.5 ml of the supernatant was added to the alkaline reagent prior to the addition  
253 of 0.5 ml of 25% (v/v) Folin-Ciocalteu phenol reagent. The resulting solution was incubated  
254 at room temperature in the dark for 1 h. The absorbance was measured at 700 nm using a  
255 tyrosine standard. One unit of alkaline protease activity was defined as the liberation of 1 µg  
256 of tyrosine per minute under the assay conditions. All activity tests were performed in  
257 triplicate.

### 258 2.10.2 Total protein content determination

259 The total protein content was determined by the Lowry method [25] using bovine serum  
260 albumin (BSA) as a standard. The absorbance was analysed at 750 nm using an UV-visible  
261 spectrophotometer (Varian Cary 50).

### 262 2.10.3 Degree of hydrolysis

263 The degree of hydrolysis was determined by quantifying the soluble protein content after  
264 precipitation with TCA [19,26]. 1ml of protein hydrolysate was mixed with 1 ml of 10%  
265 (w/v) TCA and incubated at ~~37°C~~ 37 °C for 30 min to allow for precipitation. This was  
266 followed by centrifugation (10,000 x g, 10 min). Then, the soluble protein content in the

267 supernatant was determined by the Lowry method [25], and it was expressed in milligrams.

268 The degree of hydrolysis (DH) was determined using the following equation (Eq.1):

269

$$270 \quad \text{DH(\%)} = \frac{\text{soluble protein content in 10\% TCA}}{\text{total protein content}} \times 100 \quad (5)$$

271

#### 272 *2.10.4 Electrophoresis*

273 Tricine-SDS PAGE was used to observe the pattern of smaller proteins generated after  
274 the hydrolysis reaction. Electrophoresis was performed using 10-20% Mini-PROTEAN Tris-  
275 Tricine gels under denaturing and reducing conditions. The reduction was achieved by  
276 heating the sample at ~~90°C~~ 90 °C for 5 min in the presence of β-mercaptoethanol (2% v/v).  
277 The gel was fixed with methanol (40% v/v) and acetic acid (10% v/v) and subsequently  
278 stained with Coomassie Brilliant Blue R-250. Then, the gel was destained with a solution  
279 containing methanol, acetic acid, and water (20: 4: 26 v/v).

280

### 281 **3. Results and discussion**

#### 282 *3.1 Immobilisation of Phw and Psr onto magnetic nanoparticles*

283 The Phw and Psr enzymes from SSF were immobilised onto magnetic nanoparticles via  
284 simple adsorption and crosslinking with glutaraldehyde (GA). Both methods were carried out  
285 for 8 h with the aim of investigating the effect of time and crosslinker concentration on  
286 immobilisation (Fig. 1). **The simple adsorption yielded a maximum activity recovery of 28%**  
287 **with an activity loading of 87±22 U/mg NP for Phw and of 33% Psr (activity loading of**  
288 **70±17 U/mg NP) after 8 h of immobilisation (Fig. 1a, 1c). The immobilisation efficiency for**  
289 **both Phw and Psr in simple adsorption increased during 8 h with a maximum of 60-61%**  
290 **efficiency yield, while the maximum immobilisation yield in simple adsorption for both Phw**

291 and Psr were 47% and 54%, respectively (Fig. 1b, 1d). The surfaces of naked MNPs likely  
292 possess high reactivity, which makes them susceptible to degradation under particular  
293 environmental conditions. This fact could involve weaker binding forces that contribute to  
294 the poor stability of the protein attachment's to the surface [9,27].

295 Immobilisation via the crosslinker showed good results for both enzymes studied (Phw  
296 and Psr). The immobilisation yield increased according to the increase in the GA  
297 concentration from 1%-5% up to 6 h; then, it decreased abruptly for Phw (Fig. 1b). ~~Only~~  
298 ~~when 1% GA with Psr was used did the immobilisation yield continue to increase (Fig. 1b).~~  
299 Only when using Psr with 1% GA, the immobilisation yield continues increasing (Fig. 1d).  
300 Maximum activity recovery and immobilisation yields were obtained after 6 h of crosslinking  
301 time, 90% and 96% respectively, which is (equivalent to an activity load of  $459\pm 106$  U/mg  
302 NP) for Phw with 5% GA (Fig 1a, 1b). Similarly in Psr with 5% GA the maximum activity  
303 recovery and immobilisation yield were 92% and 93%, respectively (equivalent to activity  
304 loading of  $319\pm 34$  U/mg NP) (Fig. 1c, 1d). In addition, the immobilisation via crosslinker  
305 was superior to simple adsorption as both of the enzymes (Phw, Psr) showed good  
306 immobilisation efficiency in the range of 45% to 98% during 6 h of immobilisation time (Fig  
307 1b, 1d). This indicated that the crosslinking time and GA concentration play an important role  
308 during the immobilisation of enzymes in this study. As GA plays a role as a spacer arm for  
309 the carriers by providing aldehyde groups to couple to free amine groups from the enzymes,  
310 forming imines, it can also act as a denaturing agent [12]. Additionally, some studies  
311 obtained different crosslinking times (between 1 h to 4 h) and GA concentrations (from 1% to  
312 6%), implying good biocompatibility for these specific enzymes [12,21,28,29].

### 313 3.2 Characterization of the functionalized nanoparticles used for immobilisation

314 Transmission electronic microscopy (TEM) images of MNPs before and after  
315 modification with APTES and after the enzymes immobilisation onto the activated surface

316 were compared (Fig. 2). The average particle size of naked MNPs slightly increased from  
317 10.2 nm (Fig. 2a) to 16.1 nm (Fig. 2b) after surface modification with APTES. This effect has  
318 been observed previously in other studies [30,31]. After surface modification with APTES,  
319 fewer nanoparticle aggregates formed. As suggested previously [10], surface modifications of  
320 magnetic nanoparticles can improve their solubility and help avoid aggregation of particles.  
321 In Fig. 2c and Fig. 2d, a layer covering surface of MNPs upon immobilisation of the  
322 proteases (Phw and Psr) can be seen. The thickness of this layer covering the surface of  
323 MNPs was estimated to be approximately 5.1 nm for Psr and 8.4 nm for Phw, indicating an  
324 increase in the size of the particles.

325 Based on electron diffraction analysis (Fig. 3) of the TEM images, the crystalline  
326 structure of the particles was not affected by surface modifications. Fig. 3a shows a clear  
327 loop, confirming the crystalline structure of MNPs. After surface modification by APTES or  
328 CTAB as a stabilizer, the crystalline structure was not modified; however, the size of some  
329 nanoparticles was enlarged, as observed in Fig. 3b and Fig. 3c. Once protease immobilisation  
330 was performed, the structure of the nanoparticles became an amorphous structure, confirming  
331 that the enzyme covered the surface of the nanoparticles (Fig. 3d). **The surface of the naked**  
332 **MNPs and functionalized MNPs can be observed in SEM images (Fig. 4a and Fig. 4b). The**  
333 **small and spherical particles with well-defined edges are observed as in other studies [32].** In  
334 contrast, in Fig. 4c and Fig. 4d, the edge surface of nanoparticles is smooth because they are  
335 covered by the enzymes, indicating that the immobilisation of proteases onto functionalized  
336 MNPs was successful.

337 The surface modification and immobilisation of proteases (Phw and Psr) onto  
338 nanoparticles was confirmed by a comparison of the FT-IR spectra of naked MNPs,  
339 functionalized MNPs, and Phw and Psr immobilised onto functionalized MNPs. The FT-IR  
340 spectrum in Fig. 5A shows a strong absorption peak at  $584\text{ cm}^{-1}$ , which could corresponds to

341 Fe-O, as indicated in other studies [33,34]. It has been suggested that this strong peak could  
342 be due to the stretching vibration mode associated with metal-oxygen absorption. In this  
343 region, the stretching vibration peaks related to metal (ferrites in particular) in the octahedral  
344 and tetrahedral sites of the oxide structure were found [31]. In Fig. 5A, the peaks at  $1,662\text{ cm}^{-1}$   
345  $^1$  and  $3,444\text{ cm}^{-1}$  were due to the bending and stretching vibration of -OH, respectively [35].  
346 After grafting with APTES, the characteristic peak of the Fe-O bond shifted from  $584\text{ cm}^{-1}$  to  
347  $638\text{ cm}^{-1}$  and  $640\text{ cm}^{-1}$  because of the formation of the Fe-O-Si bond (Fig. 5B, 5C, 5D). The  
348 shifting of the absorption peaks to high wavenumbers is due to the greater electronegativity  
349 of -Si(O-) compared to H, which contributes to the bond forces for Fe-O bonds [36].  
350 Additional strong peaks at  $1,039\text{ cm}^{-1}$ ,  $1,035\text{ cm}^{-1}$ , and  $1,034\text{ cm}^{-1}$  correspond to the Fe-O-Si  
351 bending vibrations, indicating that alkyl silanes are successfully attached to functionalized  
352 MNPs (Fig. 5B, 5C, 5D). Additionally, the presence of silane groups was observed at  $995\text{ cm}^{-1}$   
353  $^1$ ,  $893\text{ cm}^{-1}$ , and  $896\text{ cm}^{-1}$  and were from the stretching vibrations of the Si-OH and Si-O-Si  
354 groups from APTES [35,36]. Characteristic peaks of the immobilised enzymes attached via  
355 the crosslinker (Fig. 5C, 5D) were observed at  $1,536\text{ cm}^{-1}$ ,  $1,544\text{ cm}^{-1}$  and  $1,630\text{ cm}^{-1}$  because  
356 of the C=N and C=O absorption from the glutaraldehyde and  $\text{NH}_2$  from the enzyme [29].  
357 Small shifts in intensity from  $2,928\text{ cm}^{-1}$  (Fig. 5B) to  $2,991\text{ cm}^{-1}$  (Fig. 5C) and  $2,984\text{ cm}^{-1}$   
358 (Fig. 5D) correspond to the C-H stretching vibration from the methyl group [37], which  
359 illustrated the effect before and after the immobilisation of the enzymes. Additionally, in Fig.  
360 5C and Fig. 5D, there were broad and strong peaks at  $3,325\text{ cm}^{-1}$  and  $3,344\text{ cm}^{-1}$ , which  
361 indicated the vibration modes of the O-H and -NH groups from enzymes that interact with  
362 nanoparticles, which has been suggested previously [19].

### 363 *3.3 Operational stability of immobilised Phw and Psr*

364 The operational stability in terms of temperature and pH is an important criterion in the  
365 application of immobilised enzymes [2,38]. To study this factor (Phw\_im, Psr\_im), various



366 pH values (5 – 11) and temperatures (30°C–70°C 30 °C – 70 °C) were tested, and the results  
 367 were compared with those of free enzymes (Phw\_free, Psr\_free). The results were analysed  
 368 using analysis of variance (ANOVA) to indicate the significant factor influencing the stability  
 369 of both enzymes. The ANOVA results in Table 1 show that the regression coefficients had a  
 370 high statistical significance ( $p < 0.05$ ) and show the values obtained for the coefficient of  
 371 determination for both Phw\_im and Psr\_im ( $R^2$  0.9730 and  $R^2$  0.9733) and Phw\_free and  
 372 Psr\_free ( $R^2$  0.9723 and  $R^2$  0.9712, respectively). The values indicated that the model of the  
 373 immobilised enzymes could not explain only 2.7% of the variables behaviour, while with the  
 374 free enzymes the value was 2.8-2.9%. For immobilised enzymes, the calculated F-value  
 375 ( $\alpha = 0.05$ ,  $DOF = 4,3$ ) was 9.12 for the regression. This value was higher than the tabulated F-  
 376 values (1.65, 1.85), indicating that the treatment differences were highly significant.  
 377 Similarly, in free enzymes, the obtained F-values (2.90, 3.94) were less than the critical F-  
 378 value ( $F_{0.05(4,5)} = 5.19$ ), reflecting the significance of the model. The following Equations (6 –  
 379 9) represent the second order polynomial model of the residual activity for the experimental  
 380 data:

$$381 \text{ Residual Phw\_im(\%)} = -407.2 + 56.5\text{pH} + 10.1\text{T} - 2.6\text{pH}^2 - 0.1\text{T}^2 - 0.16\text{pHT} \quad (6)$$

$$382 \text{ Residual Psr\_im(\%)} = -275.9 + 41.8\text{pH} + 6.3\text{T} - 1.8\text{pH}^2 - 0.05\text{T}^2 - 0.17\text{pHT} \quad (7)$$

$$383 \text{ Residual Phw\_free(\%)} = 22.2 + 2.5\text{pH} + 1.5\text{T} - 0.026\text{T}^2 \quad (8)$$

$$384 \text{ Residual Psr\_free(\%)} = 66.4 + 1.04\text{pH} + 0.54\text{T} - 0.021\text{T}^2 \quad (9)$$

385 For free enzymes, the models were reduced by removing the interaction between pH and  
 386 temperature, as it was not significant to the stability of the free enzymes.

387 Contour plots of the second order polynomial model were generated as a function of the  
 388 independent variables of pH and temperature for immobilised and free enzymes. The contour  
 389 plots of free Phw and Psr exhibited their stability under mesophilic conditions (30°C 30 °C to  
 390 40°C 40 °C). Free enzymes were stable over a broad range of pH values (Fig. 6b, 6d), with no

391 optimum condition obtained in the range tested (pH 5-11). However, both of the immobilised  
392 enzymes had improved the stability by achieving their optimum condition in the alkaline  
393 region (pH 8 to 11) with thermophilic temperature stability ranging from 40°C 40 °C to 60°C  
394 60 °C for immobilised Phw (Fig. 6a) and 40°C 40 °C to 55°C 55 °C for immobilised Psr (Fig.  
395 6c).

#### 396 *3.4 Storage stability of immobilised Phw and Psr*

397 Storage stability plays a crucial role in the use immobilised proteases, as the shelf life  
398 determines the viability of an immobilised enzyme over time [39]. The storage stabilities of  
399 enzymes immobilised via a crosslinker (Phw\_GA and Psr\_GA) and adsorption (Phw\_adsorp  
400 and Psr\_adsorp) were tested by dispersing the immobilised enzymes in Tris buffer and  
401 maintaining them at 4°C 4 °C for 60 days. Free enzymes (Phw\_free and Psr\_free) were used  
402 as controls to monitor the durability of enzyme activity. Phw\_free and Psr\_free were not  
403 stable in solution, as their activity decreased over time. This fact could be related to the  
404 behaviour of the proteases, as they tend to autolyse themselves by nucleophilic attack on the  
405 intermediate in a presence of water [1,40]. After 7 days of storage at 4°C 4 °C, the residual  
406 activity of Phw\_free and Psr\_free was less than 17% (Table 2). There was a significant  
407 decrease in the activity of the immobilised enzyme via adsorption over 60 days of storage,  
408 with a residual activity of less than 45%. The weak bonding between the enzyme and  
409 nanoparticles could induce partial desorption during the period of storage. Generally,  
410 immobilisation via adsorption involves relatively weak interactions, such as electrostatic  
411 interactions, hydrogen bonds, van der Waals forces and hydrophobic interactions, which tend  
412 to strip off enzymes from the carrier easily, thus leading to a loss of activity and  
413 contamination of the reaction media [9]. However, the enzymes immobilised via crosslinking  
414 (Phw\_GA and Psr\_GA) retained 91% and 86% of their residual activity, respectively, after

415 60 days of storage at 4°C (Table 2). These results show that enzymes immobilised created by  
416 crosslinking provide a distinctive advantage in stability over immobilised enzymes created by  
417 adsorption at a longer duration of storage.

### 418 *3.5 Reusability of immobilised Phw and Psr*

419 For the sake of the cost-effective use of enzymes, reusability is a critical factor to  
420 consider [41]. The reusability of immobilised Phw and Psr created using crosslinking was  
421 evaluated in a repeated batch process using fresh casein as a model protein in each batch  
422 cycle (Fig. 7). Both immobilised Phw and Psr retained 66% and 64% of their activity,  
423 respectively, after 7 cycles, indicating a significant enhancement of the stability of the  
424 crosslinking interaction between the proteases and nanoparticles. In this work, testing the  
425 reusability was feasible, as the immobilised enzymes were easily separated by a magnetic  
426 force.

### 427 *3.6 Application of immobilised Phw and Psr in the hydrolysis of proteins*

428 Casein has been used as a model protein to evaluate the degree of hydrolysis (DH) of  
429 immobilised enzymes created via crosslinking and free Phw or Psr. The results of the  
430 hydrolysis are shown in Fig. 8a. The DH of immobilised Phw (24%) was higher than that of  
431 free Phw (15%) during the first 30 min of reaction time (Fig. 8a). **The maximum DH was**  
432 **achieved after 24 h and was 80% for immobilised Phw and 40% for free Phw. Besides, the**  
433 **residual activity of both immobilised Phw and Psr were stable for 24 h whereas the residual**  
434 **activity of free Phw and Psr had decreased pronouncedly after 24 h at 50 °C indicating an**  
435 **improvement of process efficiency and thermal stability of the immobilised enzymes [19].**  
436 **The higher stability may be possibly due to the multipoint covalent binding of protease to the**  
437 **solid support that limit the flexibility and conformational mobility of the enzyme, hence**  
438 **inhibits unfolding or denaturation of the enzyme [42]. Likewise, the DH of immobilised Psr**

439 (12%) showed the same rate as that of free Psr (13%) and continued to increase over time  
440 with a similar profile, reaching the maximum DH 30% in free Psr and 50% in immobilised  
441 Psr after 24 h of reaction time. Thus, the immobilised enzymes in the present study could  
442 enhance the ability of free enzymes to hydrolyse protein, as shown by the model protein,  
443 reflecting that the active enzymes were successfully immobilised.

444 The effect of both proteases (Phw and Psr) was also evaluated in hydrolysis of the protein  
445 source from animals (egg white albumin) and vegetables (oat bran protein isolate). The  
446 hydrolysis of oat bran protein isolate (OBPI) corroborated the efficiency of immobilised Phw  
447 and Psr, as they had a higher DH compared to free Phw and Psr over a longer duration (Fig.  
448 8b). These results agree with those obtained using functionalized magnetite nanoparticles to  
449 hydrolyse soya protein isolates and whey protein isolates [29,43]. It seems that Psr exhibited  
450 a higher DH than (free and immobilised) Phw when using a vegetable protein source. In the  
451 hydrolysis of egg white albumin, immobilised Psr reached a maximum DH 60% after 24 h  
452 and free Psr achieved maximum DH 45% after 6 h, while Phw reached a maximum DH of  
453 70% and 51% for immobilised and free Phw, respectively (Fig. 8c). Hence, the different  
454 source of the proteases seems to be a distinct behaviour that depends on the substrate source;  
455 in fact, it could determine the choice of enzymes according to the application, as suggested  
456 by others [2].

457 SDS-PAGE of the hydrolysates from selected proteins (casein, OBPI, egg white albumin)  
458 is shown in Fig. 9. The presence of several smaller peptides with low molecular weights  
459 support the idea that proteins were hydrolysed by immobilised protease derived from an  
460 animal source (Phw) and vegetable source (Psr). Similar profiles were obtained for both  
461 immobilised enzymes (Phw and Psr), showing their ability to perform the reaction after being  
462 grafted on nanoparticle surfaces created by crosslinking with glutaraldehyde.

463

#### 464 **4. Conclusion**

465 Low-cost proteases obtained through the SSF of protein-rich wastes (hair waste and soya  
466 fibre residues) were successfully immobilised onto functionalized MNPs over a relatively  
467 short time. The ease of the separation and reusability of these enzymes in comparison with  
468 free enzymes could be considered an advantage of their use in industrial processes.  
469 Additionally, stability was enhanced from mesophilic to thermophilic conditions under  
470 alkaline conditions, preventing autolysis of the enzymes and maintaining their initial  
471 activities for 2 months with only 9%-14% activity loss. Immobilised Phw and Psr were able  
472 to hydrolyse some proteins derived from plant and animal sources with a high degree of  
473 hydrolysis, indicating that they are promising for immobilised enzyme applications in a wide  
474 range of industrial processes.

475

#### 476 **Acknowledgements**

477 The authors thank the Spanish Ministerio de Economía y Competitividad (Project  
478 CTM2015-69513-R) for their financial support. N.A. Yazid thanks the Government of  
479 Malaysia and University Malaysia Pahang for their financial support. Raquel Barrena is  
480 grateful to TECNIOspring fellowship programme (no. TECSPR15-1-0051) co-financed by  
481 the European Union through the Marie Curie Actions and ACCIÓ (Generalitat de Catalunya).

482

#### 483 **References**

- 484 [1] M.B. Rao, A.M. Tanksale, M.S. Ghatge, V. V. Deshpande, Molecular and  
485 biotechnological aspects of microbial proteases., *Microbiol. Mol. Biol. Rev.* 62 (1998)  
486 597–635.
- 487 [2] O.L. Tavano, Protein hydrolysis using proteases: An important tool for food  
488 biotechnology, *J. Mol. Catal. B Enzym.* 90 (2013) 1–11.

- 489 [3] A.K. Mukherjee, H. Adhikari, S.K. Rai, Production of alkaline protease by a  
490 thermophilic *Bacillus subtilis* under solid-state fermentation (SSF) condition using  
491 Imperata cylindrica grass and potato peel as low-cost medium: Characterization and  
492 application of enzyme in detergent formulation, *Biochem. Eng. J.* 39 (2008) 353–361.
- 493 [4] J. Abraham, T. Gea, A. Sánchez, Potential of the solid-state fermentation of soy fibre  
494 residues by native microbial populations for bench-scale alkaline protease production,  
495 *Biochem. Eng. J.* 74 (2013) 15–19.
- 496 [5] N.A. Yazid, R. Barrena, A. Sánchez, Assessment of protease activity in hydrolysed  
497 extracts from SSF of hair waste by and indigenous consortium of microorganisms,  
498 *Waste Manag.* 49 (2016) 420–426.
- 499 [6] S.S. Kim, H.S. Lee, Y.S. Cho, Y.S. Lee, C.S. Bhang, H.S. Chae, S.W. Han, I.S.  
500 Chung, D.H. Park, The effect of the repeated subcultures of *Helicobacter pylori* on  
501 adhesion, motility, cytotoxicity, and gastric inflammation., *J. Korean Med. Sci.* 17  
502 (2002) 302–306.
- 503 [7] C. Mateo, J.M. Palomo, G. Fernandez-Lorente, J.M. Guisan, R. Fernandez-Lafuente,  
504 Improvement of enzyme activity, stability and selectivity via immobilization  
505 techniques, *Enzyme Microb. Technol.* 40 (2007) 1451–1463.
- 506 [8] M. Asgher, M. Shahid, S. Kamal, H.M.N. Iqbal, Recent trends and valorization of  
507 immobilization strategies and ligninolytic enzymes by industrial biotechnology, *J.*  
508 *Mol. Catal. B Enzym.* 101 (2014) 56–66.
- 509 [9] J. Xu, J. Sun, Y. Wang, J. Sheng, F. Wang, M. Sun, Application of iron magnetic  
510 nanoparticles in protein immobilization, *Molecules.* 19 (2014) 11465–11486.
- 511 [10] X. Jin, J.F. Li, P.Y. Huang, X.Y. Dong, L.L. Guo, L. Yang, Y.C. Cao, F. Wei, Y. Di  
512 Zhao, H. Chen, Immobilized protease on the magnetic nanoparticles used for the  
513 hydrolysis of rapeseed meals, *J. Magn. Magn. Mater.* 322 (2010) 2031–2037.
- 514 [11] I.A. Cavello, J.C. Contreras-Esquivel, S.F. Cavalitto, Immobilization of a keratinolytic  
515 protease from *Purpureocillium lilacinum* on genipin activated-chitosan beads, *Process*  
516 *Biochem.* 49 (2014) 1332–1336.
- 517 [12] H.J. Chae, M.J. In, E.Y. Kim, Optimization of protease immobilization by covalent  
518 binding using glutaraldehyde., *Appl. Biochem. Biotechnol.* 73 (1998) 195–204.
- 519 [13] S.A. Ansari, Q. Husain, Potential applications of enzymes immobilized on/in nano  
520 materials: A review, *Biotechnol. Adv.* 30 (2012) 512–523.
- 521 [14] P. Xu, G.M. Zeng, D.L. Huang, C.L. Feng, S. Hu, M.H. Zhao, C. Lai, Z. Wei, C.  
522 Huang, G.X. Xie, Z.F. Liu, Use of iron oxide nanomaterials in wastewater treatment:  
523 A review, *Sci. Total Environ.* 424 (2012) 1–10.
- 524 [15] A. Sahu, P.S. Badhe, R. Adivarekar, M.R. Ladole, A.B. Pandit, Synthesis of  
525 glycinamides using protease immobilized magnetic nanoparticles, *Biotechnol. Reports.*  
526 12 (2016) 13–25.

- 527 [16] S.-L. Cao, X.-H. Li, W.-Y. Lou, M.-H. Zong, Preparation of a novel magnetic  
528 cellulose nanocrystal and its efficient use for enzyme immobilization, *J. Mater. Chem.*  
529 *B.* 2 (2014) 5522–5530.
- 530 [17] S. Cao, H. Xu, X. Li, W. Lou, M. Zong, Papain@magnetic nanocrystalline cellulose  
531 nanobiocatalyst: a highly efficient biocatalyst for dipeptide biosynthesis in deep  
532 eutectic solvents, *ACS Sustain. Chem. Eng.* 3 (2015) 1589–1599.
- 533 [18] S. Cao, Y. Huang, X. Li, P. Xu, H. Wu, N. Li, W. Lou, Preparation and  
534 Characterization of Immobilized Lipase from *Pseudomonas Cepacia* onto Magnetic  
535 Cellulose Nanocrystals, *Sci. Rep.* 6 (2016) 1–12.
- 536 [19] R. Sinha, S.K. Khare, Immobilization of halophilic *Bacillus* sp. EMB9 protease on  
537 functionalized silica nanoparticles and application in whey protein hydrolysis,  
538 *Bioprocess Biosyst. Eng.* 38 (2015) 739–748.
- 539 [20] S. Jodayree, Antioxidant activity of oat bran hydrolyzed proteins in vitro and in vivo,  
540 Doctoral Thesis, Ottawa, Ontario, 2014.
- 541 [21] T.G. Hu, J.H. Cheng, B.B. Zhang, W.Y. Lou, M.H. Zong, Immobilization of alkaline  
542 protease on amino-functionalized magnetic nanoparticles and its efficient use for  
543 preparation of oat polypeptides, *Ind. Eng. Chem. Res.* 54 (2015) 4689–4698.
- 544 [22] A. Abo Markeb, A. Alonso, A.D.A.D. Dorado, A. Sánchez, X. Font, Phosphate  
545 removal and recovery from water using nanocomposite of immobilized magnetite  
546 nanoparticles on cationic polymer, *Environ. Technol.* 3330 (2016) 1–14.
- 547 [23] R.A. Sheldon, S. Van Pelt, Enzyme immobilisation in biocatalysis: why, what and  
548 how, *Chem. Soc. Rev.* 42 (2013) 6223–6235.
- 549 [24] K. Alef, P. Nannipieri, Methods in applied soil microbiology and biochemistry -  
550 Enzyme activities, Academic Press, San Diego, 1995.
- 551 [25] O.H. Lowry, N.J. Rosebrough, A.L. Farr, R.J. Randall, Protein measurement with the  
552 Folin phenol reagent., *J. Biol. Chem.* 193 (1951) 265–275.
- 553 [26] M.P.C. Silvestre, H.A. Morais, V.D.M. Silva, M.R. Silva, Degree of hydrolysis and  
554 peptide profile of whey proteins using pancreatin, *Brazilian Soc. Food Nutr.* 38 (2013)  
555 278–290.
- 556 [27] D.A. Cowan, R. Fernandez-Lafuente, Enhancing the functional properties of  
557 thermophilic enzymes by chemical modification and immobilization, *Enzyme Microb.*  
558 *Technol.* 49 (2011) 326–346.
- 559 [28] S. Prasertkittikul, Y. Chisti, N. Hansupalak, Deproteinization of natural rubber using  
560 protease immobilized on epichlorohydrin cross-linked chitosan beads, *Ind. Eng. Chem.*  
561 *Res.* 52 (2013) 11723–11731.
- 562 [29] S.N. Wang, C.R. Zhang, B.K. Qi, X.N. Sui, L.Z. Jiang, Y. Li, Z.J. Wang, H.X. Feng,  
563 R. Wang, Q.Z. Zhang, Immobilized alcalase alkaline protease on the magnetic chitosan

- 564 nanoparticles used for soy protein isolate hydrolysis, *Eur. Food Res. Technol.* 239  
565 (2014) 1051–1059.
- 566 [30] H. Quanguo, Z. Lei, W. Wei, H. Rong, H. Jingke, Preparation and Magnetic  
567 Comparison of Silane-Functionalized Magnetite Nanoparticles, 22 (2010) 285–295.
- 568 [31] J.A. Lopez, F. González, F.A. Bonilla, G. Zambrano, M.E. Gómez, Synthesis and  
569 characterization of Fe<sub>3</sub>O<sub>4</sub> magnetic nanofluid, *Rev. Latinoam. Metal. Y Mater.* 30  
570 (2010) 60–66.
- 571 [32] M.R. Ladole, A.B. Muley, I.D. Patil, M.I. Talib, R. Parate, Immobilization of  
572 tropizyme-P on amino-functionalized magnetic nanoparticles for fruit juice  
573 clarification, *J. Biochem. Tech.* 5 (2014) 838–845.
- 574 [33] I.J. Bruce, T. Sen, Surface modification of magnetic nanoparticles with alkoxysilanes  
575 and their application in magnetic bioseparations, *Langmuir.* 21 (2005) 7029–7035.
- 576 [34] M. Yamaura, R.L. Camilo, L.C. Sampaio, M.A. Macedo, M. Nakamura, H.E. Toma,  
577 Preparation and characterization of (3-aminopropyl)triethoxysilane-coated magnetite  
578 nanoparticles, *J. Magn. Magn. Mater.* 279 (2004) 210–217.
- 579 [35] D.L. Pavia, G.M. Lampman, G.S. Kriz, J.A. Vyvyan, eds., Introduction to  
580 spectroscopy, 5th ed., Cengage Learning, United State of America, 2015.
- 581 [36] R.A. Bini, R.F.C. Marques, F.J. Santos, J.A. Chaker, M. Jafelicci, Synthesis and  
582 functionalization of magnetite nanoparticles with different amino-functional  
583 alkoxysilanes, *J. Magn. Magn. Mater.* 324 (2012) 534–539.
- 584 [37] P.E.G. Casillas, C.A.R. Gonzalez, C.A.M. Pérez, Infrared Spectroscopy of  
585 Functionalized Magnetic Nanoparticles, in: T. Theophile (Ed.), *Infrared Spectrosc. -*  
586 *Mater. Sci. Eng. Technol.*, InTech, 2012: pp. 405–420.
- 587 [38] R.J.S. De Castro, H.H. Sato, Production and biochemical characterization of protease  
588 from *Aspergillus oryzae*: An evaluation of the physical-chemical parameters using  
589 agroindustrial wastes as supports, *Biocatal. Agric. Biotechnol.* 3 (2014) 20–25.
- 590 [39] A.G. Kumar, S. Swarnalatha, P. Kamatchi, G. Sekaran, Immobilization of high  
591 catalytic acid protease on functionalized mesoporous activated carbon particles,  
592 *Biochem. Eng. J.* 43 (2009) 185–190.
- 593 [40] R. Beynon, J.S. Bond, eds., *Proteolytic enzymes: a practical approach*, 3rd ed., Oxford  
594 University Press, 2001.
- 595 [41] T. Chen, W. Yang, Y. Guo, R. Yuan, L. Xu, Y. Yan, Enhancing catalytic performance  
596 of  $\beta$ -glucosidase via immobilization on metal ions chelated magnetic nanoparticles,  
597 *Enzyme Microb. Technol.* 63 (2014) 50–57.
- 598 [42] R.K. Singh, Y.W. Zhang, N.P.T. Nguyen, M. Jeya, J.K. Lee, Covalent immobilization  
599 of beta-1,4-glucosidase from *Agaricus arvensis* onto functionalized silicon oxide  
600 nanoparticles, *Appl. Microbiol. Biotechnol.* 89 (2011) 337–344.



601 [43] E.M. Lamas, R.M. Barros, V.M. Balcao, F.X. Malcata, Hydrolysis of whey proteins by  
602 proteases extracted from *Cynara cardunculus* and immobilized onto highly activated  
603 supports, *Enzyme Microb. Technol.* 28 (2001) 642–652.

604

605

606

607

608

609

610

611

612

613

614

615

616

617

618

619

620

621 **Tables**

622 **Table 1** Analysis of variance (ANOVA) for the response surface quadratic model for  
 623 immobilised (Phw\_im and Psr\_im) and free (Phw\_free and Psr\_free) enzymes.

Protease	Source of variation	Sums of square	Degree of freedom	Mean square	F-value	Prob>F
Phw_im	Regression	12107.4	5	2421.5	50.47	<0.0001
	Residual	335.9	7	47.98		
	Pure error	150	4	37.5		
	Lack of fit	185.9	3	61.95	1.65	
	Total	12443.2	12			
Psr_im	Regression	5108.7	5	1021.7	50.99	<0.0001
	Residual	140.3	7	20		
	Pure error	58.8	4	14.7		
	Lack of fit	81.5	3	27.2	1.85	
	Total	5248.9	12			
Phw_free	Regression	3382.4	3	1127.5	105.4	<0.0001
	Residual	96.3	9	10.7		
	Pure error	20.8	4	5.2		
	Lack of fit	75.5	5	15.1	2.9	
	Total	3478.7	12			
Psr_free	Regression	6452.3	3	2150.8	101.1	<0.0001
	Residual	191.5	9	21.3		
	Pure error	32.3	4	8.1		
	Lack of fit	159.2	5	31.8	3.94	
	Total	6643.8	12			

624 Phw\_im: R<sup>2</sup> 0.9730, adj R<sup>2</sup> 0.9537, pred R<sup>2</sup> 0.8519

625 Psr\_im: R<sup>2</sup> 0.9733, adj R<sup>2</sup> 0.9542, pred R<sup>2</sup> 0.8260

626 Phw\_free: R<sup>2</sup> 0.9723, adj R<sup>2</sup> 0.9631, pred R<sup>2</sup> 0.9315

627 Psr\_free: R<sup>2</sup> 0.9712, adj R<sup>2</sup> 0.9616, pred R<sup>2</sup> 0.9224

628  
 629  
 630  
 631  
 632  
 633  
 634  
 635  
 636  
 637  
 638  
 639  
 640  
 641  
 642  
 643  
 644

645 **Table 2** The storage stability of free and immobilised enzymes created via crosslinking with  
 646 glutaraldehyde (GA) and via adsorption (adsorp) during 60 days of storage.  
 647

Enzymes	Initial activity (U/ml)	Final activity (U/ml)	Residual activity (%)
Phw_GA	501±72	458±51	91
Psr_GA	346±69	297±84	86
Phw_adsorp	190±15	77±9	41
Psr_adsorp	152±9	46±5	30
Phw_free	537±26	91±21 <sup>a</sup>	17
Psr_free	358±29	42±3 <sup>a</sup>	12

648 <sup>a</sup> The final activity was determined after 7 days of storage.  
 649 The standard deviation was calculated from 3 replicates.

650  
 651  
 652  
 653

654

655

656

657

658

659

660

661

662

663

664

665

666

667

668

669 **Figure captions**

670 **Fig. 1** The effect of the glutaraldehyde (GA) concentration and crosslinking time on the  
 671 activity recovery of (a) Phw and (c) Psr with 0% GA (simple adsorption) (■), 1% GA (▨),  
 672 2.5% GA (▩), and 5% GA (▧); enzyme loading per carrier of (a) Phw and (c) Psr with 0%  
 673 GA (simple adsorption) (—●—), 1% GA (—○—), 2.5% GA (—▼—), and 5% GA (—△—);  
 674 immobilisation yield of (b) Phw and (d) Psr with 0% GA (simple adsorption) (■), 1% GA (▨),  
 675 2.5% GA (▩), and 5% GA (▧); immobilisation efficiency of (b) Phw and (d) Psr  
 676 with 0% GA (simple adsorption) (—●—), 1% GA (—○—), 2.5% GA (—▼—), and 5% GA (—△—)  
 677 —△—) onto amino-functionalized MNPs.

678 **Fig. 2** TEM images at a magnification of 30,000x of (a) naked MNPs, (b) amino-  
 679 functionalized MNPs, (c) amino-functionalized MNPs after being immobilised with Phw, and  
 680 (d) amino-functionalized MNPs after being immobilised with Psr.

681 **Fig. 3** The electron diffraction images of (a) naked MNPs, (b) MNPs after the addition of  
 682 CTAB, (c) MNPs after surface modification with APTES, and (d) MNPs after the  
 683 immobilisation of the enzymes Phw and Psr.

684 **Fig. 4** The SEM images at 50.00 KX magnification of (a) naked MNPs, (b) amino-  
 685 functionalized MNPs, (c) amino-functionalized MNPs after being immobilised with Phw, and  
 686 (d) amino-functionalized MNPs after being immobilised with Psr.

687 **Fig. 5** The FT-IR spectra of (A) naked MNPs, (B) amino-functionalized MNPs, (C) amino-  
 688 functionalized MNPs after immobilisation of Phw, and (D) amino-functionalized MNPs after  
 689 immobilisation of Psr.

690 **Fig. 6** Contour plots of the residual activity (%) of the enzymes in terms of their operation  
 691 stability as a function of pH and temperature of (a) immobilised Phw, (b) free Phw, (c)  
 692 immobilised Psr, and (d) free Psr

693 **Fig. 7** The reusability of immobilised Phw (■) and immobilised Psr (□) onto amino-  
694 functionalized MNPs using casein as a model substrate for the hydrolysis reaction

695 **Fig. 8** The degree of hydrolysis of the selected protein hydrolysates obtained from the  
696 hydrolysis of immobilised Phw (—○—), free Phw (—●—), immobilised Psr (—△—), and free Psr  
697 (—▽—) with (a) casein; (b) oat bran protein isolate (OBPI); and (c) egg white albumin. The  
698 residual activity of immobilised Phw (—□—), free Phw (—■—), immobilised Psr (—◇—) and  
699 free Psr (—◆—) in 50 °C during 24h.

700 **Fig. 9** SDS-PAGE of the hydrolysates after reduction using 2-mercaptoethanol for selected  
701 proteins before and after treatment with the immobilised proteases; (1) Molecular mass  
702 marker; (2) casein; (3) egg white albumin; (4) hydrolysate from casein after treated with  
703 immobilised Phw; (5) hydrolysate from egg white albumin after treatment with immobilised  
704 Phw; (6) hydrolysate from OBPI after treatment with immobilised Phw; (7) hydrolysate from  
705 casein after treatment with immobilised Psr; (8) hydrolysate from egg white albumin after  
706 treatment with immobilised Psr; (9) hydrolysate from OBPI after treatment with Psr.

707

708

709

710

711

712

713

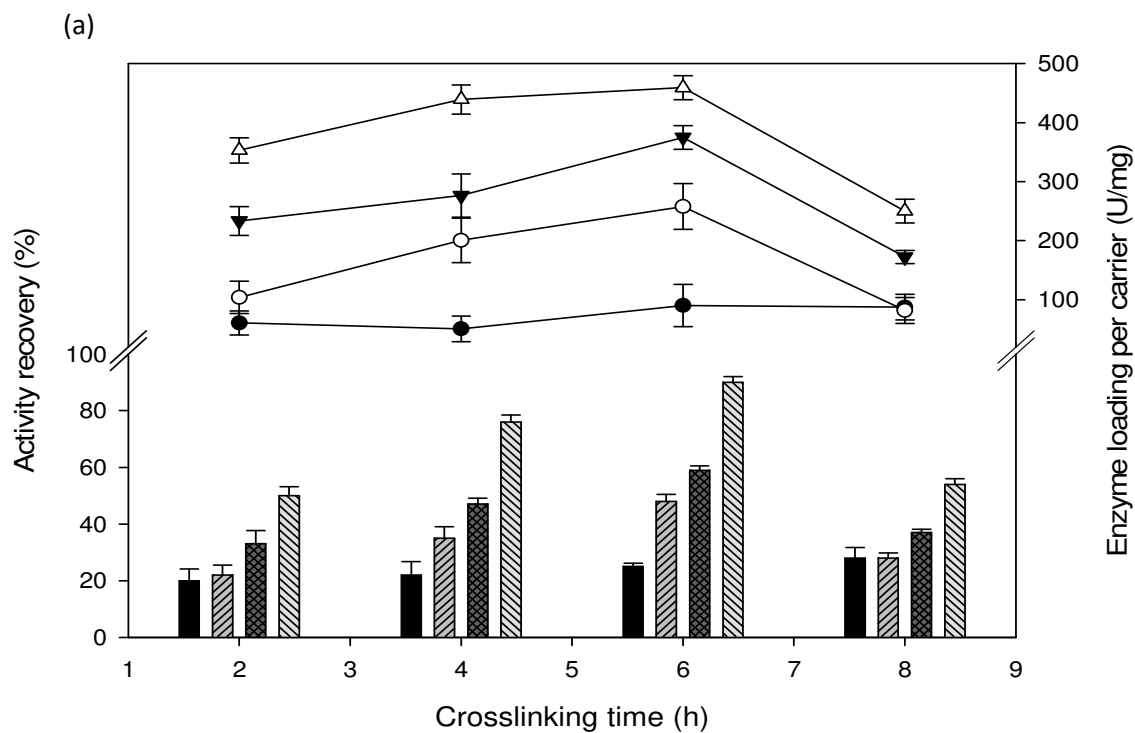
714

715

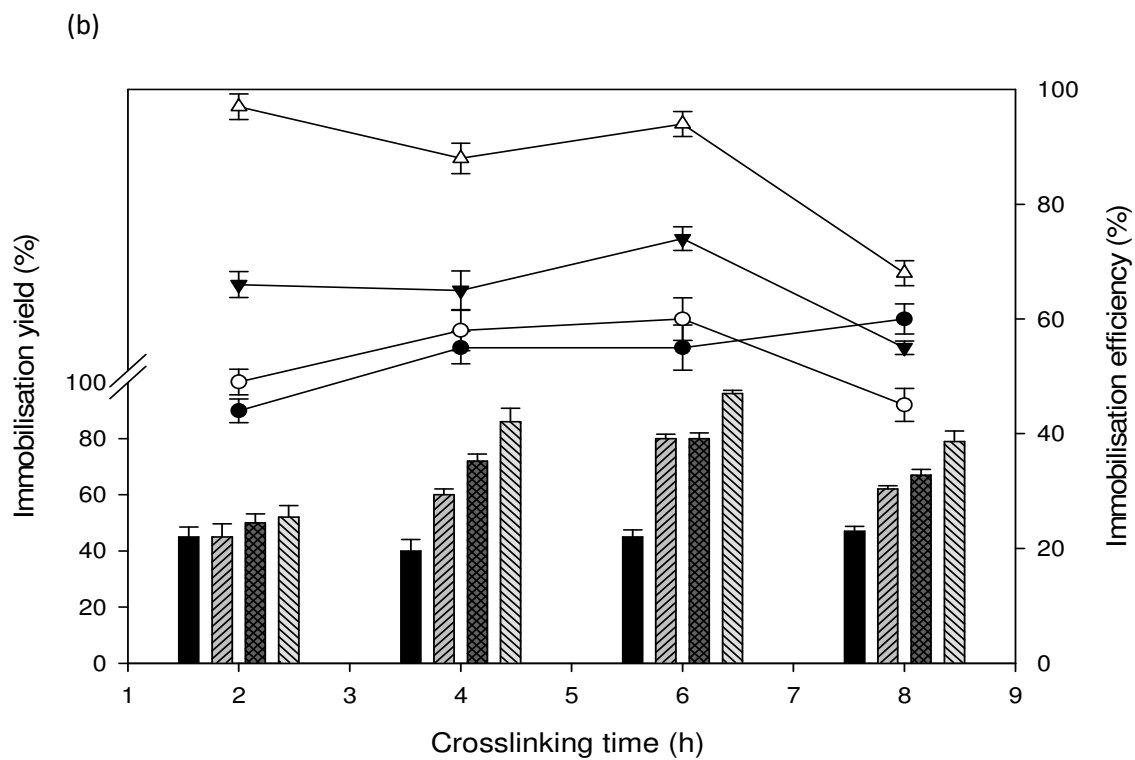
716

717

718 **Fig. 1**

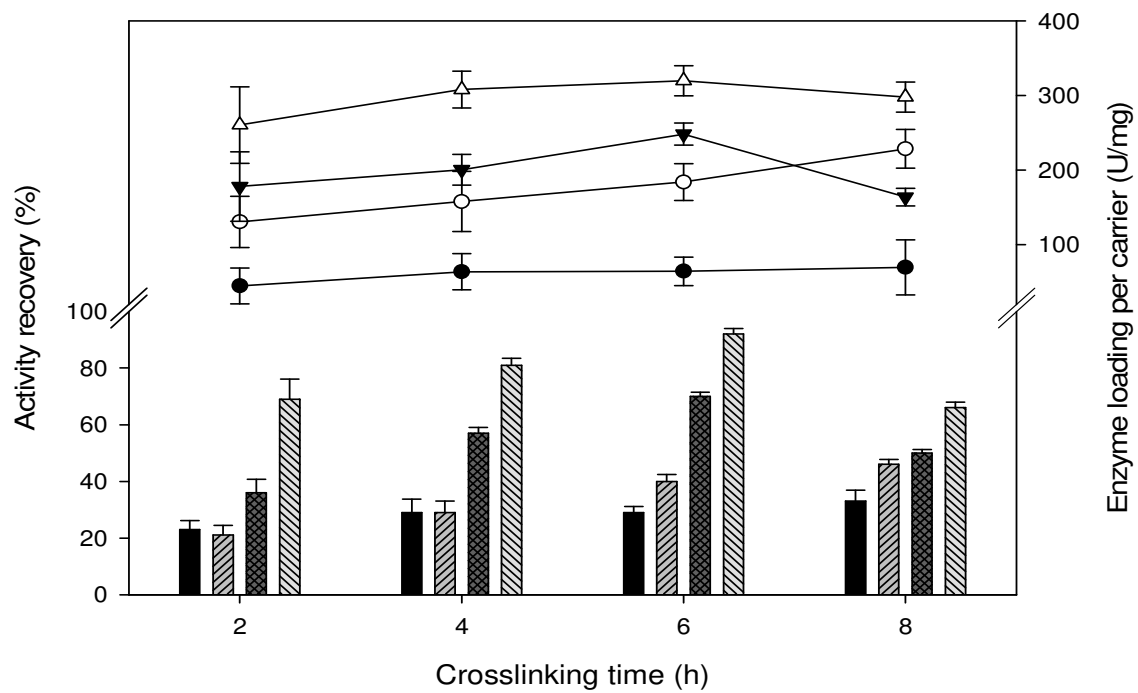


719



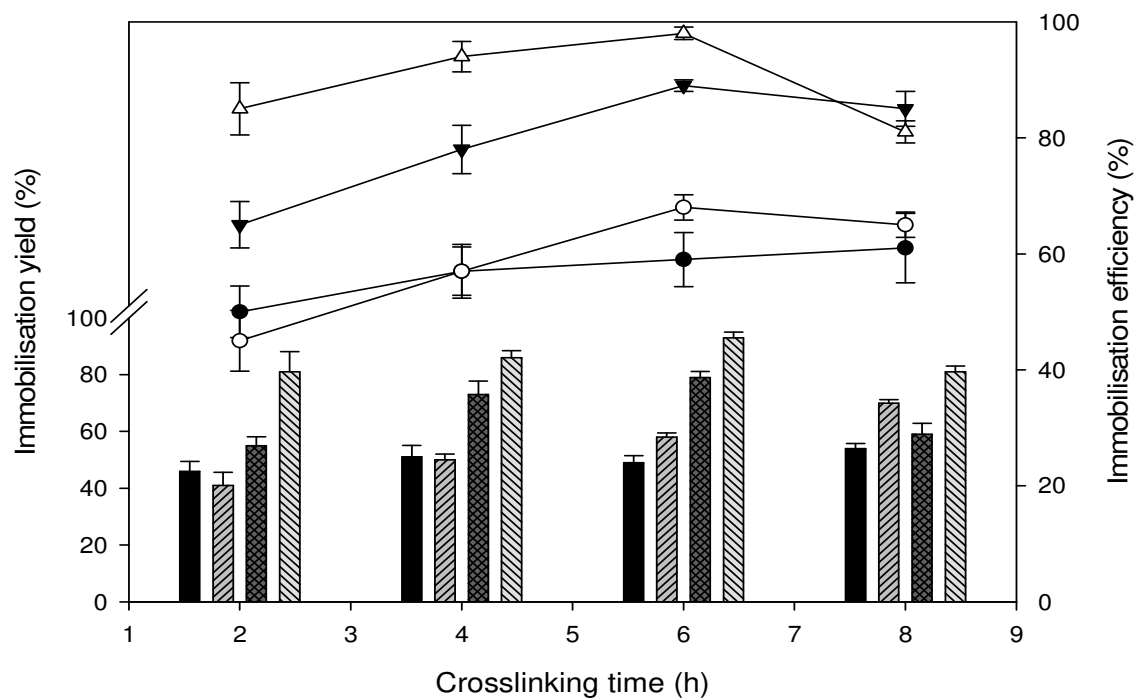
720

(c)



721

(d)



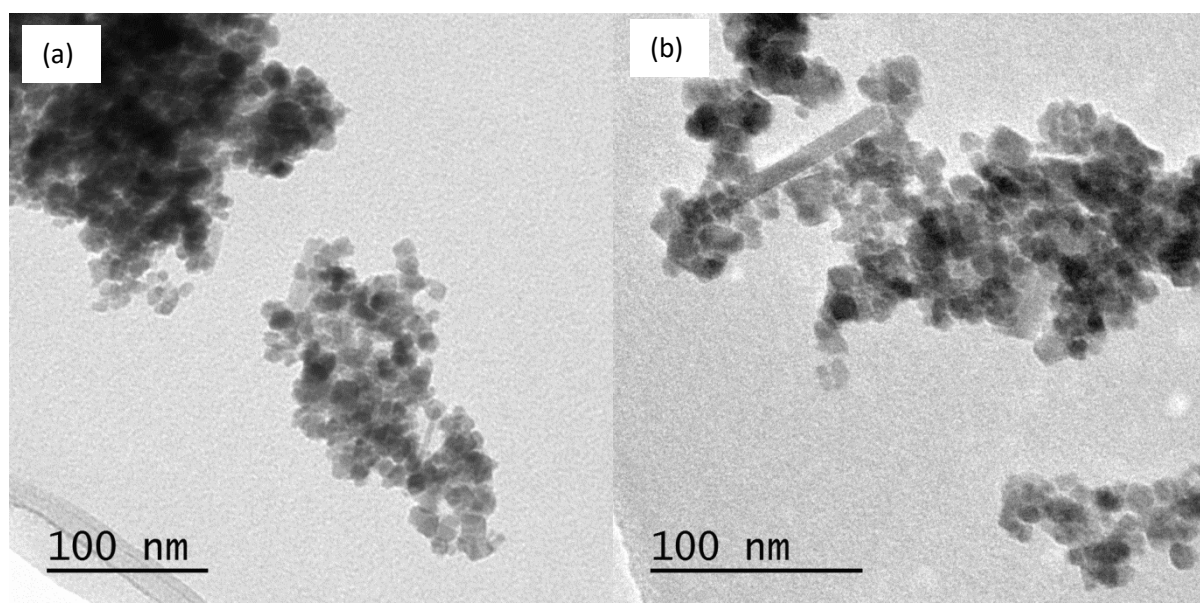
722

723

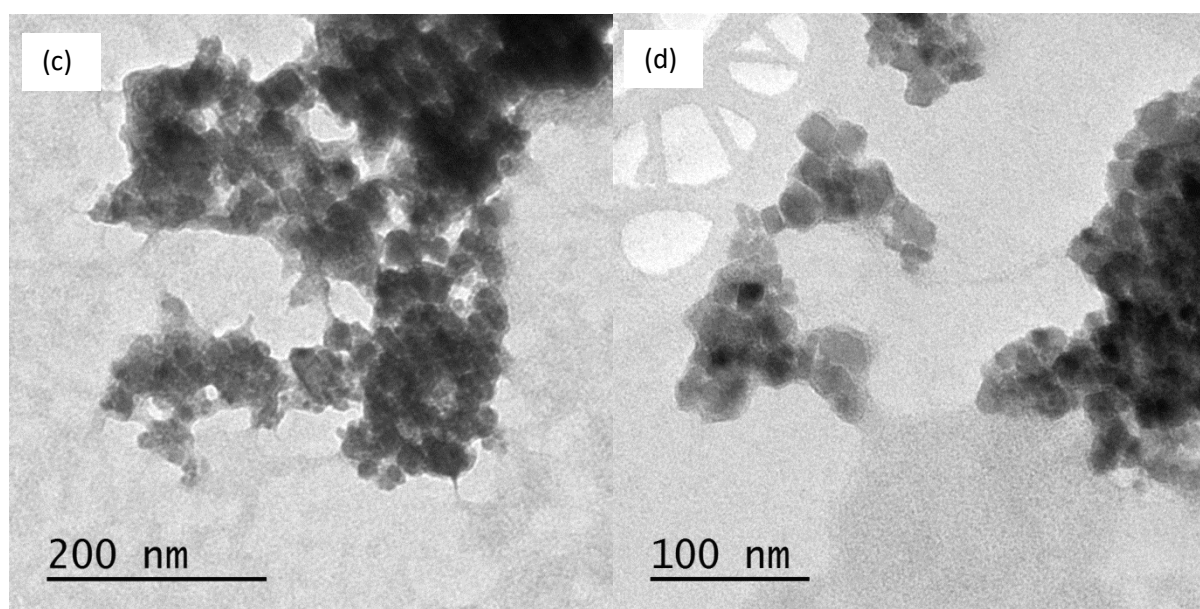
724

725

726

727 **Fig. 2**

728



729

730

731

732

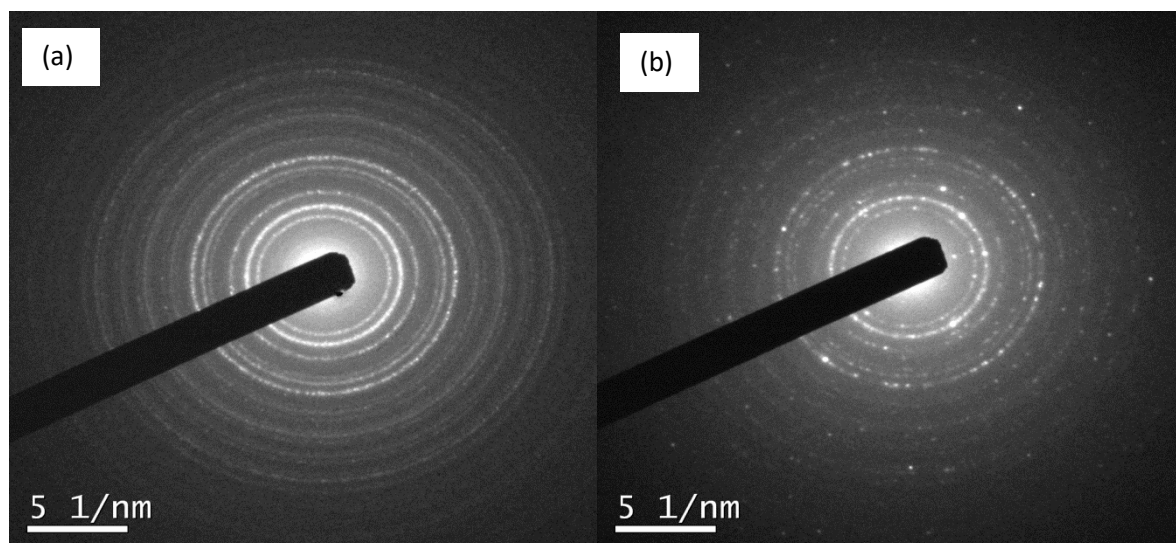
733

734

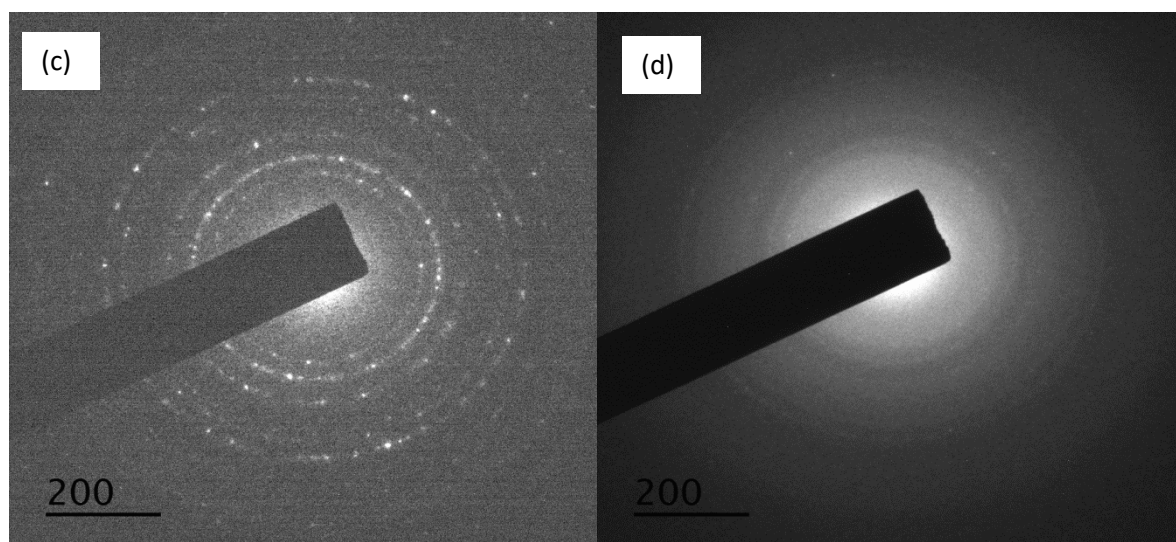
735

736



737 **Fig. 3**

738



739

740

741

742

743

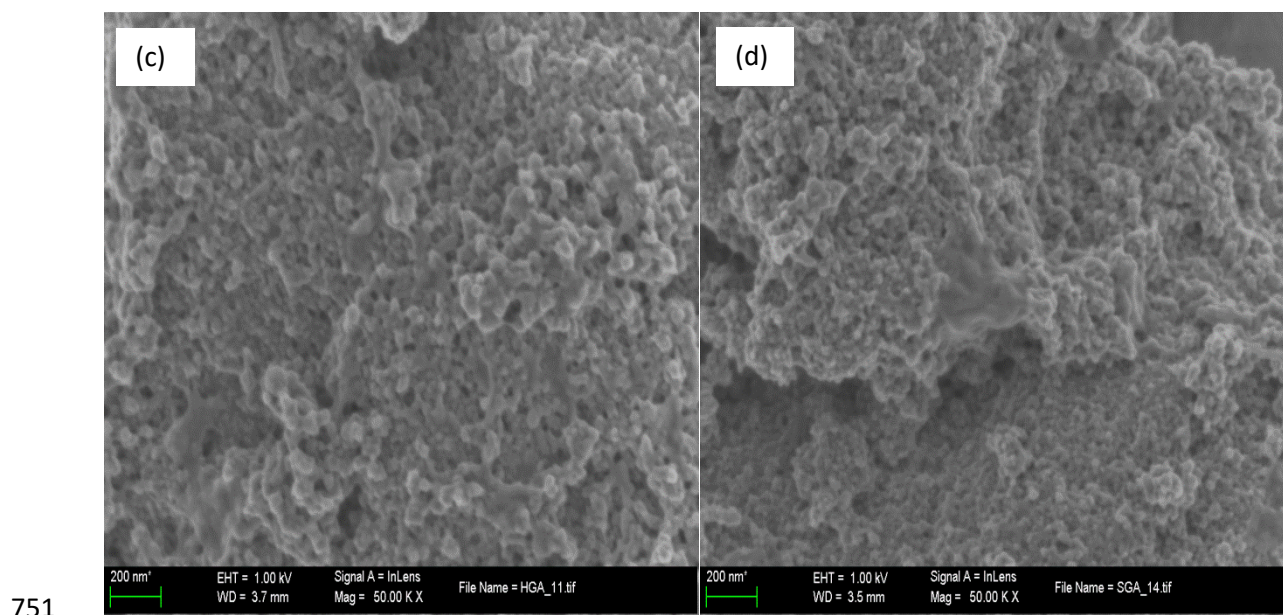
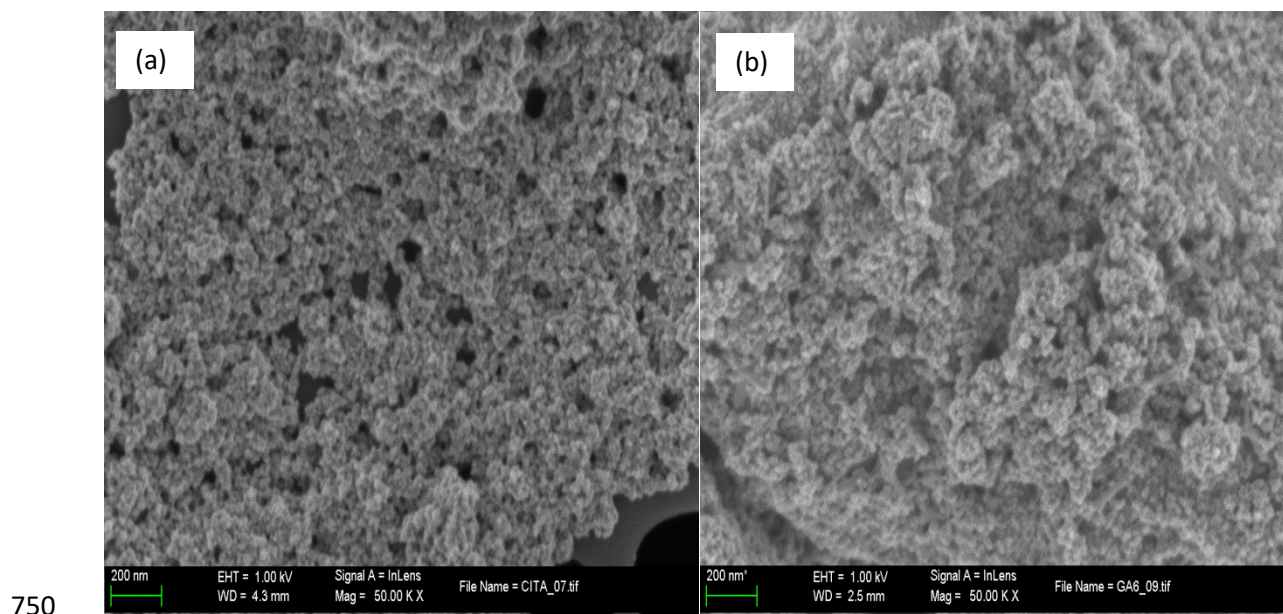
744

745

746

747

748

749 **Fig. 4**

752

753

754

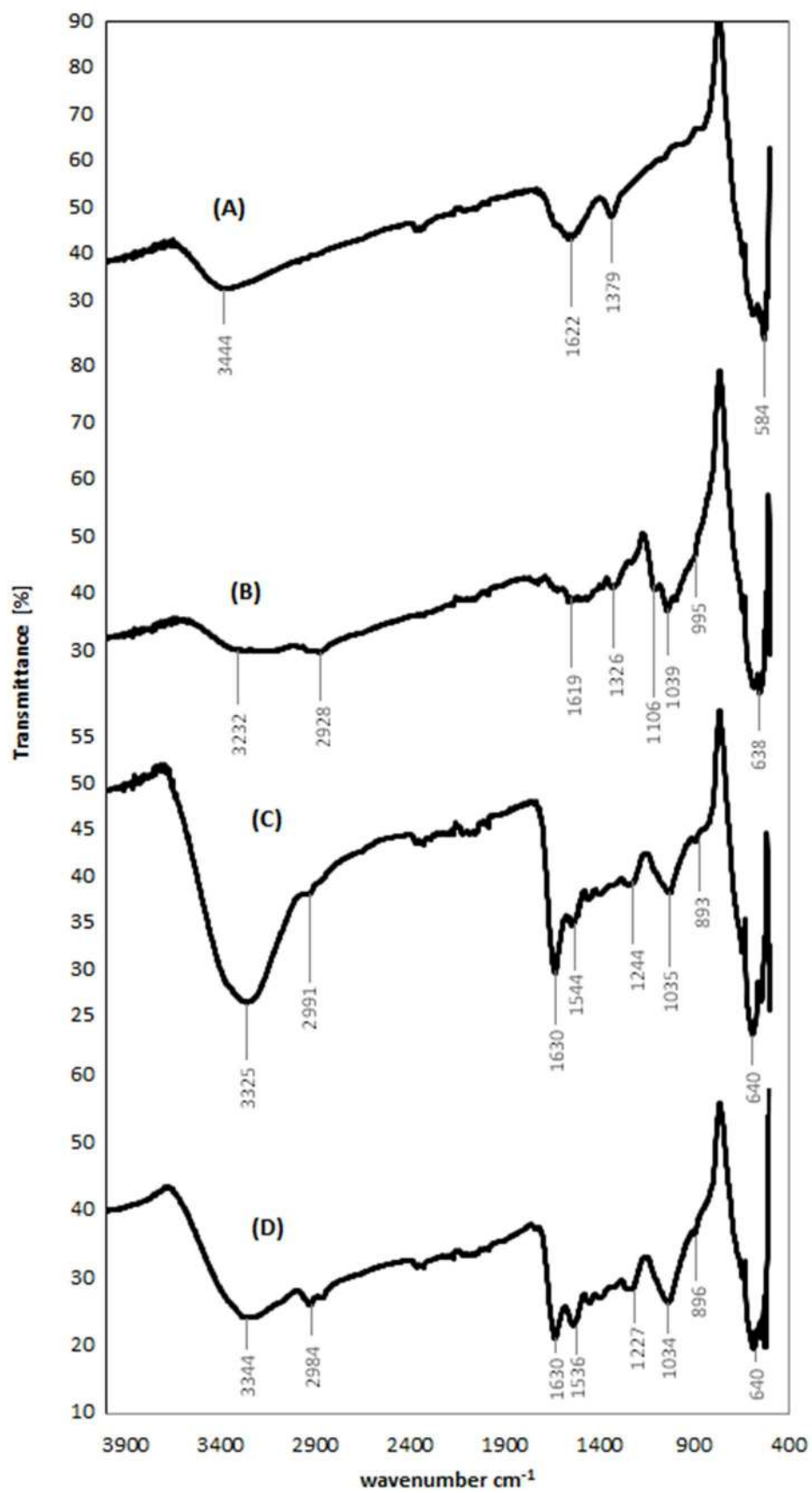
755

756

757

758

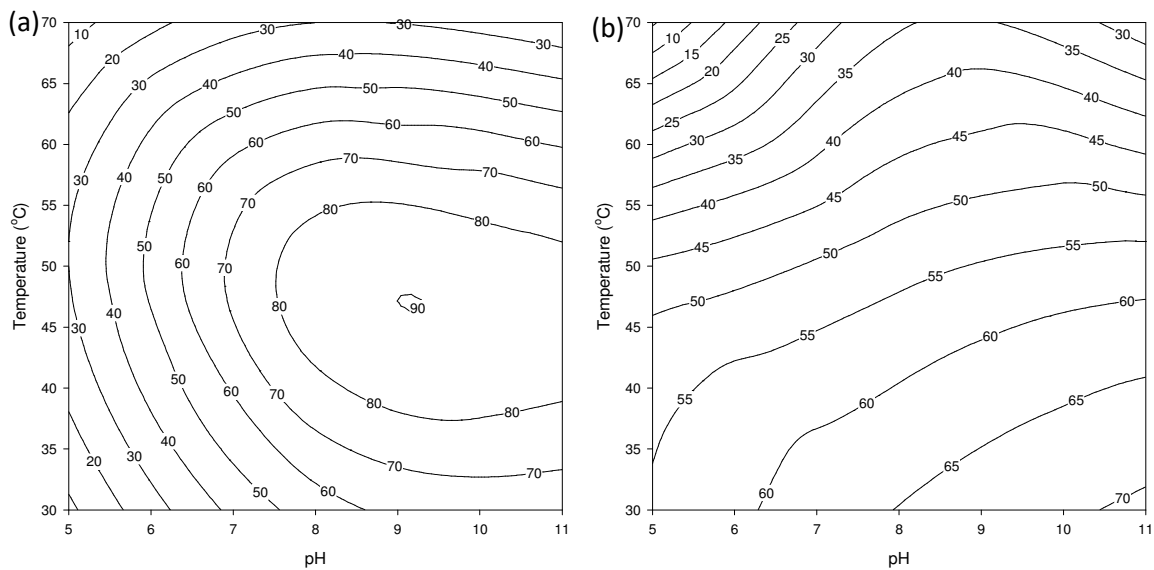
759 Fig. 5



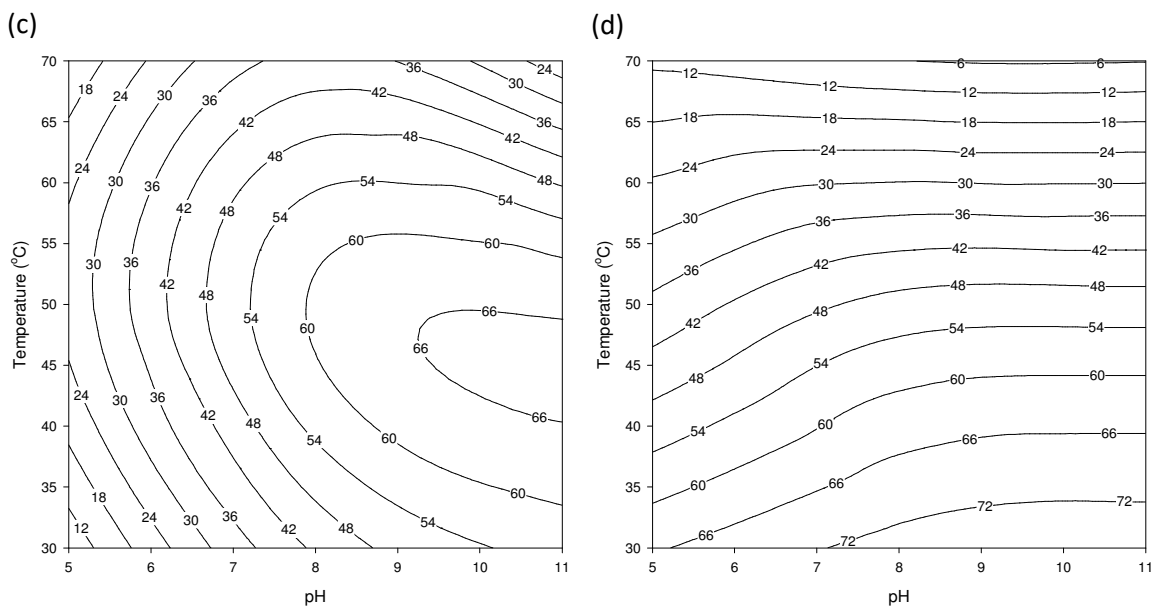
760

761

762 **Fig. 6**



763



764

765

766

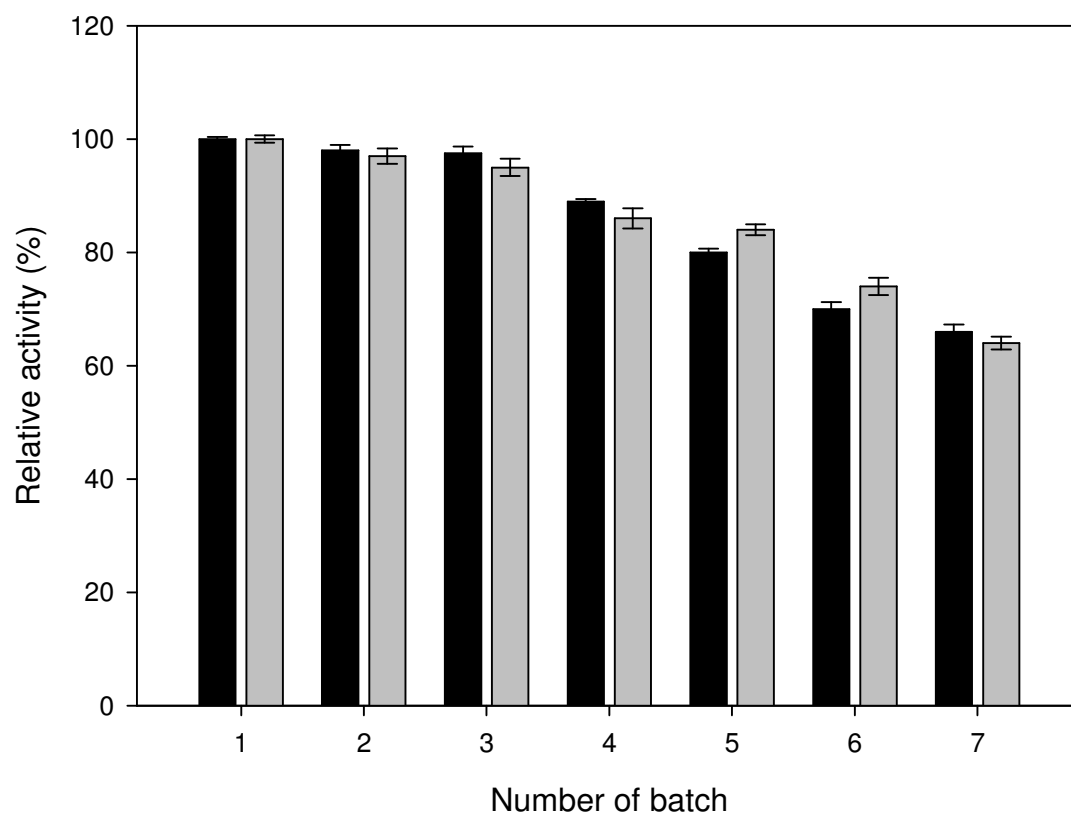
767

768

769

770

771

772 **Fig. 7**

773

774

775

776

777

778

779

780

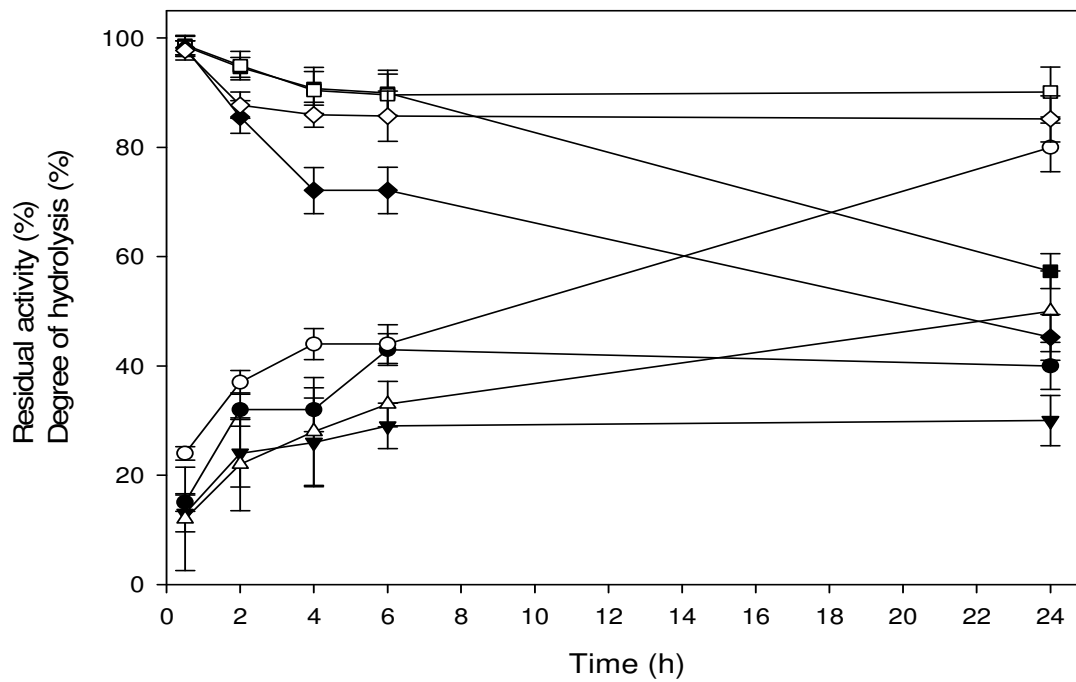
781

782

783

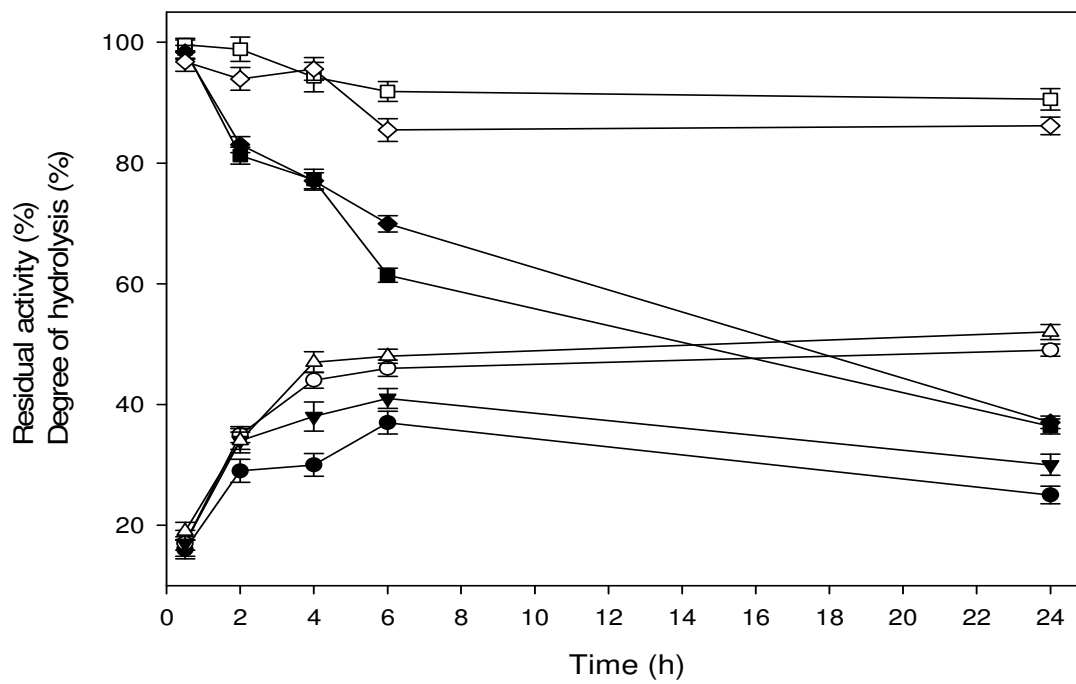
784 **Fig. 8**

(a)



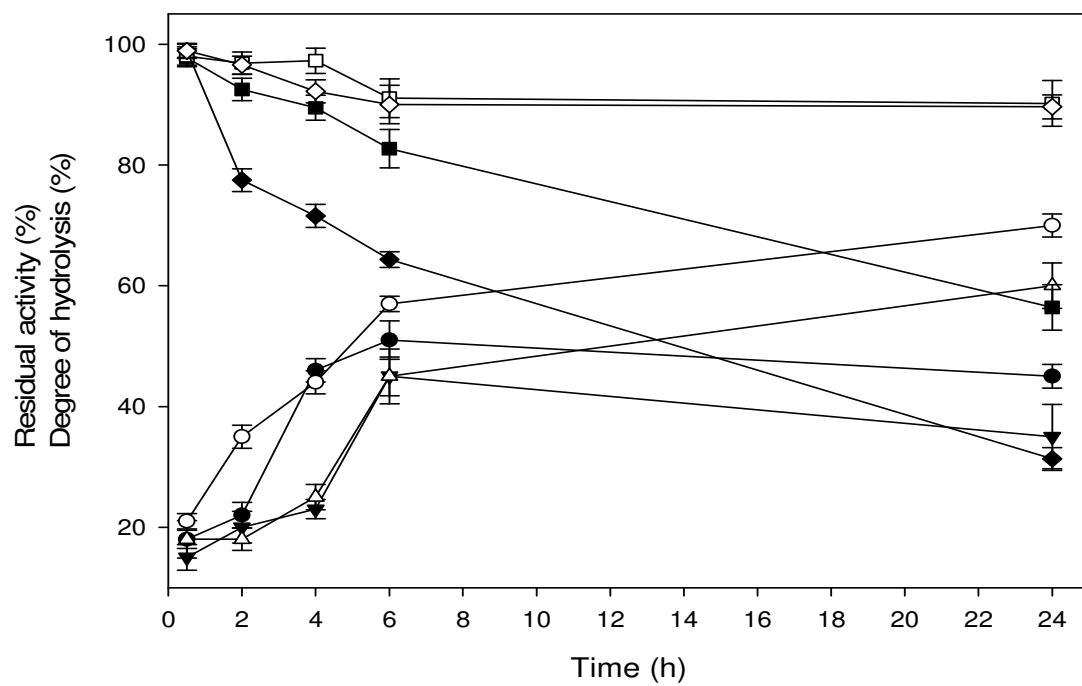
785

(b)



786

(c)



787

788

789

790

791

792

793

794

795

796

797

798

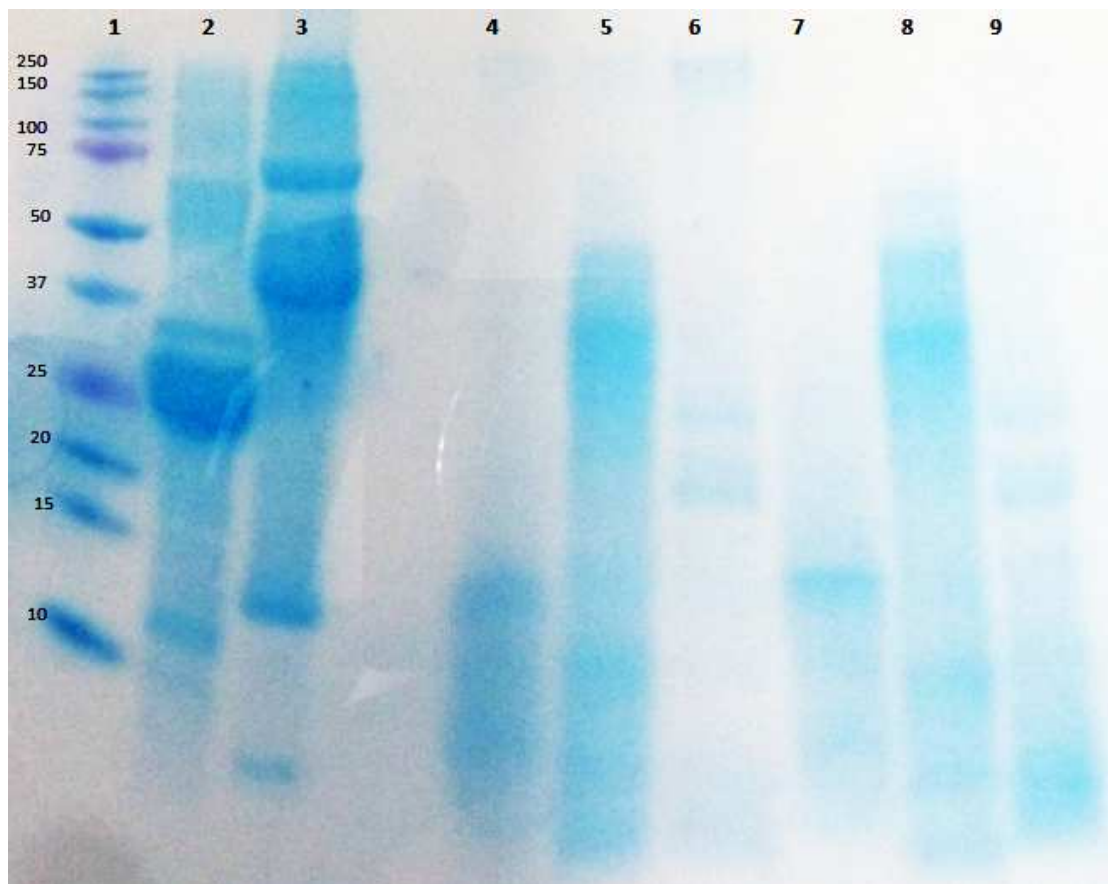
799

800

801

802 **Fig. 9**

803



804