

NASA CR-165516  
SN-1020-A1-F

# THERMAL OXIDATIVE DEGRADATION REACTIONS OF PERFLUOROALKYLEETHERS

(NASA-CR-165516) THERMAL OXIDATIVE  
DEGRADATION REACTIONS OF  
PERFLUOROALKYLEETHERS Final Report, Sep.  
1980 - Sep. 1981 (Ultrasystems, Inc.,  
Irvine, Calif.) 46 p HC A03/MF A01 CSCI 07C G3/23

N82-12135

Unclas  
08316

Prepared by:

K. L. Paciorek, T. I. Ito, and R. H. Kratzer



ULTRASYSTEMS, INCORPORATED  
Irvine, California

Prepared for:

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

NASA Lewis Research Center  
Contract NAS3-22517

William R. Jones, Project Manager



1. Report No. NASA CR-165516	2. Government Accession No.	3. Recipient's Catalog No.	
4. Title and Subtitle Thermal Oxidative Degradation Reactions of Perfluoroalkylethers.		5. Report Date October 1981	6. Performing Organization Code
		8. Performing Organization Report No. SN-1020-A1-F	
7. Author(s) K. L. Paciorek, T. I. Ito, and R. H. Kratzer		10. Work Unit No.	
9. Performing Organization Name and Address Ultrasystems, Inc. 2400 Michelson Drive Irvine, CA 92715		11. Contract or Grant No. NAS3-22517	
		13. Type of Report and Period Covered Contractor Report September 1980 - September 1981	
12. Sponsoring Agency Name and Address National Aeronautics and Space Administration Washington, D.C. 20546		14. Sponsoring Agency Code	
		15. Supplementary Notes Project Manager, William R. Jones NASA Lewis Research Center Cleveland, OH 44135	
16. Abstract The objective of this contract was to investigate the mechanisms operative in thermal and thermal oxidative degradation of Fomblin Z and hexafluoropropene oxide derived fluids and the effect of alloys and additives upon these processes.  The nature of arrangements responsible for the inherent thermal oxidative instability of the Fomblin Z fluids has not been established. It was determined that this behavior was not associated with hydrogen end-groups or peroxy linkages. The degradation rate of these fluids at elevated temperatures in oxidizing atmospheres was found to be dependent on the surface/volume ratio. Once a limiting ratio was reached, a steady rate appeared to be attained. Based on elemental analysis and oxygen consumption data, $-CF_2OCF_2CF_2O-$ , not $-CF_2CF_2O-$ , is one of the major arrangements present. The action of the M-50 and Ti(4Al, 4Mn) alloys was found to be much more drastic in the case of Fomblin Z fluids than that observed for the hexafluoropropene oxide derived materials. The effectiveness of antioxidant/anticorrosion additives; P-3 and phospho-s-triazine, in the presence of metal alloys was very limited at 316°C; at 288°C the additives arrested almost completely the fluid degradation. The phospho-s-triazine appeared to be at least twice as effective as the P-3 compound; it also protected the coupon better. The Ti(4Al, 4Mn) alloy degraded the fluid mainly by chain scission processes; this took place to a much lesser degree with M-50.  The presence of a certain proportion of hydrogen-terminated chains in Krytox MLO-71-6 fluid was verified by NMR spectroscopy. These were eliminated on exposure of the fluid to oxygen at 343°C. In oxygen at 316°C, aluminum metal did not seem to promote chain scissions; a steady but low rate of degradation was observed for pure titanium metal.			
17. Key Words (Suggested by Author(s)) Perfluoroalkylethers, Degradation mechanisms, Fomblin Z, Krytox, Corrosion and Effect of Metal Alloys, Additives, Inhibitors		18. Distribution Statement	
19. Security Classif. (of this report) Unclassified	20. Security Classif. (of this page) Unclassified	21. No. of Pages 40 + v	22. Price*

\* For sale by the National Technical Information Service, Springfield, Virginia 22161

## FOREWORD

This annual report describes the work performed by Ultrasystems, Inc. during the period 3 September 1980 through 4 September 1981 under Contract NAS3-22517, "Thermal Oxidative Degradation Reactions of Perfluoroalkylethers". The investigations were carried out by T. I. Ito, R. H. Kratzer, and K. L. Paciorek, project manager, at the Chemicals and Materials Research Department, Irvine, California. The contract was administered by the NASA Lewis Research Center with Mr. William R. Jones as the project manager.

We would like to acknowledge the cooperation and assistance of Mr. C. E. Snyder of the Air Force Wright Aeronautical Laboratories, Fluids, Lubricants, and Elastomers Branch. We also would like to express our indebtedness to Dr. Paul R. Resnick of E. I. DuPont de Nemours and Company for the determination and interpretation of the NMR spectra of selected fluids.

## TABLE OF CONTENTS

ABSTRACT	i
FOREWORD	ii
TABLE OF CONTENTS	iii
LIST OF TABLES	iv
LIST OF FIGURES	v
1. SUMMARY	1
2. INTRODUCTION	3
3. RESULTS AND DISCUSSION	4
3.1 Degradation Studies , Fomblin Z Fluids	4
3.2 Mechanistic and Structural Considerations	8
3.3 Investigation of Polyperfluoroalkylethers Derived from Hexafluoropropene Oxide	11
4. EXPERIMENTAL DETAILS AND PROCEDURES	14
5. PRELIMINARY CONCLUSIONS	16
6. REFERENCES	17

## LIST OF TABLES

<u>Table No.</u>		<u>Page No.</u>
I	Thermal and Thermal Oxidative Investigations of Fomblin Z Fluid, Batch MLO-72-22	19
II	Thermal and Thermal Oxidative Investigations of Fomblin Z Fluid, Batch MLO-79-196	20
III	Effects of Metal Coupons and Additives on Thermal and Thermal Oxidative Behavior of Fomblin Z Fluid, Batch MLO-72-22	21
IV	Product Distribution, Thermooxidative Degradation of Fomblin Z Fluids	22
V	Elemental Analysis Considerations	23
VI	Influence of Metal Coupons Upon Ratios of Volatilized Fluid to Oxygen Consumed	24
VII	Effect of Metal Coupons on Thermal Oxidative Behavior of Polyhexafluoropropene Oxide Fluids	25

## LIST OF FIGURES

<u>Figure No.</u>		<u>Page No.</u>
1	$^{19}\text{F}$ NMR spectrum of Fomblin Z fluid MLO-72-22	26
2	$^{19}\text{F}$ NMR spectrum of Fomblin Z fluid MLO-72-22, expanded sections A, B, and C	27
3	$^{19}\text{F}$ NMR spectrum of Fomblin Z fluid MLO-72-22, expanded section B	28
4	$^{19}\text{F}$ NMR spectrum of Fomblin Z fluid MLO-72-22, from -200 to +100 ppm	29
5	$^{19}\text{F}$ NMR spectrum of Fomblin Z fluid MLO-72-22, integrated data	30
6	Proton NMR spectrum of Fomblin Z fluid (Residue Test No. 19)	31
7	Proton NMR spectrum of Fomblin Z fluid (Residue Test No. 21)	31
8	Proton NMR spectrum of Krytox MLO-71-6 fluid (as received)	32
9	Proton NMR spectrum of Freon E-2, $\text{C}_3\text{F}_7\text{OCF}(\text{CF}_3)\text{H}$	33
10	Proton NMR spectrum of Krytox MLO-71-6 fluid (recovered after Test 18/20)	34
11	$^{19}\text{F}$ NMR spectrum of Krytox MLO-71-6 fluid (as received)	35
12	$^{19}\text{F}$ NMR spectrum of Krytox MLO-71-6 fluid, expanded to 10 ppm sweep	36
13	Portion of $^{19}\text{F}$ NMR spectrum of Krytox MLO-71-6 fluid, expanded to 20 ppm	37
14	Decomposition tube and adapter	38
15	Metal specimen holder arrangement	39
16	Box furnace arrangement	40





## 1. SUMMARY

Investigations of the mechanisms operative in thermal and thermal oxidative degradation of Fomblin Z type fluids and the effect of alloys and additives upon these processes are reported. Included are limited studies carried out on hexafluoropropene oxide derived polyethers.

The inherent thermal oxidative instability of the Fomblin Z fluids is not associated with hydrogen termination of the chains. Present investigations point to complete absence of hydrogen in these compositions. After thermal pretreatment, the stability of the fluid to metal alloys in inert atmospheres indicates the absence of peroxide linkages; NMR data support these deductions. The degradation rate at elevated temperatures in oxidizing atmospheres is dependent on the fluid surface to volume ratio. Once a limiting ratio is reached, a steady rate appears to be attained. Based on elemental analysis and oxygen consumption data,  $-\text{CF}_2\text{OCF}_2\text{CF}_2\text{O}-$ , not  $-\text{CF}_2\text{CF}_2\text{O}-$ , is one major arrangement present. The action of the M-50 and Ti(4 Al, 4 Mn) alloys is much more drastic in the case of Fomblin Z fluids than that observed for the hexafluoropropene oxide derived materials. The effectiveness of anti-oxidation/anticorrosion additives, P-3 and phospho-s-triazine, in the presence of metal alloys is very limited at  $316^\circ\text{C}$ ; at  $288^\circ\text{C}$  the additives arrest almost completely the fluid degradation. The phospho-s-triazine appears to be at least twice as effective as the P-3 compound; it also protects the coupon better. The Ti(4 Al, 4 Mn) alloy degrades the fluid mainly by chain scission processes; this occurs to a much lesser degree with M-50.

The presence of a certain proportion of hydrogen-terminated chains in Krytox MLO-71-6 fluid was verified by NMR spectroscopy. Prolonged exposure of the fluid to oxygen at  $343^\circ\text{C}$  resulted in degradation of these chains and fluid stabilization. Limited studies of the effect of the pure

metals at elevated temperatures in oxygen upon the hexafluoropropene oxide derived fluid gave results not consistent with the alloy investigations. Aluminum metal did not seem to promote chain scissions at 316°C. A steady but low rate of degradation, under these conditions, was observed for the titanium metal.

## 2. INTRODUCTION

Perfluorinated polyethers such as those derived from the telomerization of hexafluoropropene oxide exhibit extremely high thermal stabilities with incipient decomposition temperatures in the vicinity of  $410^{\circ}\text{C}$  [ref. 1,2]. This stability is not diminished in an oxidizing environment as represented by air or pure oxygen, which is in contrast to the behavior of hydrocarbons. The investigations carried out to date on polyperfluoroalkylethers have been fairly extensive [ref. 1-13], however these were concentrated predominantly on the hexafluoropropene oxide derived materials containing pending side chains with only limited work performed on the linear, unbranched materials [ref. 10-13]. Based on these data, the linear polyperfluoroalkylethers exhibit significantly lower thermal and thermal oxidative stabilities than those shown by the hexafluoropropene oxide derived compositions. It has been suggested [ref. 3,4] that the lower-than-expected stability of commercial polyhexafluoropropene oxide fluids is due to the presence of some hydrogen-terminated chains. These apparently can be removed by oxidation at elevated temperatures. The reason for the low thermal stability of the linear ethers is unknown. In view of their low temperature viscosity characteristics and wide fluid ranges, the linear materials are of great potential utility for aircraft applications where extremes of temperature are encountered.

The present investigation was directed at elucidating the mechanisms of the thermal oxidative degradation of the linear materials and the effect of the additives and metals upon this process. The verification of the presence of hydrogen-terminated chains in the "untreated" polyhexafluoropropene oxide derived materials and the determination of the action of pure metals upon these fluids, as opposed to the alloys, constituted other aspects of this program.

### 3. RESULTS AND DISCUSSION

The present investigation involved two different classes of perfluoroalkylethers, namely linear and hexafluoropropene oxide derived materials. The latter are formed by oligomerization of hexafluoropropene oxide, whereas the linear perfluoroalkylethers are prepared from tetrafluoroethylene and oxygen under ultraviolet radiation [ref. 13]. The process as such introduces peroxide linkages which are then removed by subsequent heat treatment. The termination reaction used in the preparation of polyhexafluoropropene oxides is well documented [ref. 1,2] and theoretically should give only perfluoroalkyl end-groups. No such information is available for the linear materials, although it is published data [ref. 13] that the grouping is  $\text{CF}_2\text{H}$ . The nature of the end-groups and the presence of irregularities are the factors which limit the inherent stability of the perfluoroalkylether systems. Thus, any study of the thermal and thermal oxidative behavior must incorporate structural considerations. These, of course, will differ depending on the synthetic methods involved even when dealing with what should be identical arrangements. Thus, there is no direct comparison between the "tetrafluoroethylene oxide" and hexafluoropropene oxide derived materials.

To permit clarity of presentation, the investigations of the two fluids are discussed separately. The implications of these various aspects are evident by the results discussed in the sections which follow.

#### 3.1 Degradation Studies, Fomblin Z Fluids

Two different batches of Fomblin Z fluid were received from the U.S. Air Force Wright Aeronautical Laboratories (AFSC). The material found by the Air Force to be of higher stability, MLO-72-22, was obtained from Montecatini Edison in 1972. The less stable sample MLO-79-196 was a later (1979) received composition. It is noteworthy that both the Air Force and the Bray

Oil Co. concurred [ref. 14] that earlier Fomblin Z samples were thermally more stable; this was ascribed to the possible presence of residual peroxide linkages in more recent batches. The thermal and thermal oxidative investigations carried out on these two materials are summarized in Tables I and II, the tests involving metal coupons and additives are given in Table III, and the compositions of the volatiles are presented in Table IV.

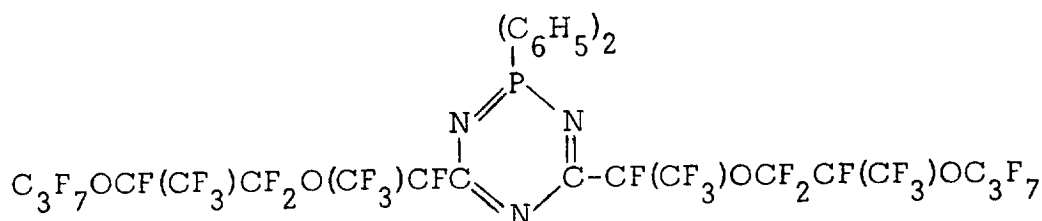
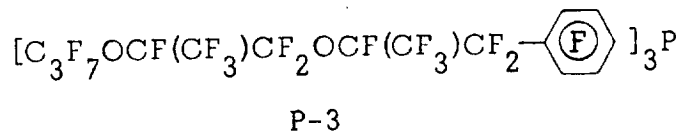
To determine the possible presence of heat "removable" unstable linkages, Test Nos. 1, 2, 3, and 7 were carried out. Based on the quantity of the volatile condensibles formed, it is evident that, at least up to 250°C, the fluid MLO-79-196 degrades more extensively. However, additional heat treatment (see Test No. 3, Table II) does not lead to further degradation showing that exposure of the fluid to 250°C in an inert atmosphere removes some unstable centers.

Concentrating on the MLO-72-22 fluid (see Table I), it is obvious that oxidizing atmospheres at elevated temperatures promote considerable degradation with initial exposure (see Test Nos. 5 and 6) resulting in significantly higher degradation than subsequent exposures to the same temperature. It would appear that the degradation rate at a given temperature, after the initial phase, proceeds at a relatively steady rate (see Test Nos. 6, 9, and 10). An increase in temperature of ~10°C between 332 and 343°C (Test Nos. 12 and 17) increases the rate by a factor of ~2 which is in very good agreement with Arrhenius' equation and shows clearly that the change in temperature does not alter the operative mechanism. The change in molecular weight is, however, considerable and there is also some change in the elemental composition (see Table V). Whether this is real is unknown. Ignoring the elemental composition variation, one is tempted to assume that the lowering in the molecular weight took place prior to the attainment of the steady rate, possibly at the stage of Test No. 6 (?).

On the basis of Test Nos. 17 and 19, it would appear that the degradation rate at 343°C is ~ 60-65 mg/g per 24 hr. This applies only to small quantities of fluid. When large quantities of fluid are employed, the rate with respect to the quantity of fluid employed drops considerably (see Test Nos. 21, 30, and 39). This drop is not due to oxygen depletion since in Test No. 21 only 5.4% of the available oxygen was consumed and it can be deduced that in Run No. 39 the value would be ~ 12%. Thus, it must be assumed that the degradation rate is governed by the solubility or diffusion of oxygen into the fluid. The larger the volume of the fluid, the lower the surface area of the fluid in contact with oxygen (all the tests were performed in the same type of a tube). Consequently, in the case of the large samples, the pretreatment in oxidizing atmospheres is not complete as shown by the comparison of Test Nos. 31 and 6. It is believed that the rate observed for the small quantities of fluid (~ 3 g) is the true rate, since it was unchanged by halving the quantity of the fluid (compare Test Nos. 17 and 19). It should be stressed that, in the case of the hexafluoropropene oxide derived fluids, variations of the ratios of surface area to volume had no effect upon the degradation extent [ref. 3,4].

The thermal oxidative behavior of the MLO-79-196 Fomblin Z fluid paralleled closely that of the MLO-72-22 material as evident by the compilation presented in Table II. The degradation rates at corresponding temperatures are fairly comparable, e.g., 16-17 mg/g for MLO-79-196 versus 19-22 mg/g for MLO-72-22 over a 24 hr period at 316°C. It is noteworthy that no decrease in molecular weight of the residual fluid was found to take place in the case of the MLO-79-196. On the other hand, the final molecular weights were comparable. The nature and relative concentration of the condensible volatiles formed by these two fluids are directly comparable.

The majority of the investigations were carried out on the MLO-72-22 fluid and this fluid only was evaluated in the presence of metal coupons and additives. This series of the tests is compiled in Table III. The metal alloys employed were M-50 and Ti(4 Al, 4 Mn); the additives were P-3 (MLO-80-279) and phospho-s-triazine. The structures of these are given below.



The presence of metal coupons was found to accelerate greatly the fluid's degradation. Exposure to oxygen at 316°C in the presence of M-50 for 24 hr resulted in complete liquid degradation (Test No. 32B, Table III). In 8 hr at 316°C more than half of the fluid was degraded. The additives (Test Nos. 34 and 35) were effective in arresting this process to a degree at 316°C, although the degradation rate was higher by more than a factor of 10 as compared to the tests carried out in the absence of the M-50 coupon. Based on the quantity of products formed, the phospho-s-triazine additive seems to be twice as effective as the P-3 compound.

The studies performed on hexafluoropropene oxide derived materials [ref. 3,4] showed that the additives arrest the fluid degradation in the absence of metal. The same was found to be the case in Fomblin Z fluids (Test No. 33). However, this action is only partially effective at 316°C in the presence of

metal (Test Nos. 34 and 35). Whether this is due to the accelerated consumption of the additive is unknown. At 288°C both of the additives were very effective in arresting degradation (Test Nos. 36 and 37) with the phospho-s-triazine exhibiting a stronger action (factor of 3 as measured by volatiles produced). The Ti(4 Al, 4 Mn) alloy was found to degrade the fluid more extensively at 288°C than the M-50 coupon as shown by comparison of Test Nos. 38 and 41. The P-3 additive was very effective in arresting this action. No parallel studies were performed with the phospho-s-triazine compound. In the absence of oxygen, both of the alloys failed to promote the fluid's degradation even at 316°C (Test Nos. 44 and 45).

The coupons recovered from Test Nos. 32A, 32B, 34, 35, and 38 were badly corroded and covered with flaky deposits. Unexpectedly, corrosion was evident on the coupons obtained after Runs 37, 42, and 45 where the degradation of fluid was very low; the coupons recovered from Test Nos. 36 and 44 were shiny. The surprising aspect is that P-3 additive did not seem to fully prevent the corrosion of M-50, whereas the phospho-s-triazine compound achieved it.

### 3.2 Mechanistic and Structural Considerations

The  $^{19}\text{F}$  and proton NMR spectra of the Fomblin Z fluid recovered after Test No. 19 are given in Figures 1-6. The proton NMR of the "lightly" thermally stressed fluid is given in Figure 7 (Test No. 21). From the  $^{19}\text{F}$  NMR the assignment is difficult; the polymer appears to contain  $\text{CF}_3\text{O}$ ,  $-\text{OCF}_2$ ,  $-\text{OCF}_2\text{CF}_2-$ , and  $\text{OCF}_2\text{CF}_2\text{CF}_2\text{CF}_2-$  groups arranged randomly. Area "A" may be assigned to  $\text{CF}_3\text{O}$ -,  $-\text{OCF}_2\text{O}-\text{CF}_2\text{O}$ -,  $-\text{OCF}_2\text{OCF}_2\text{CF}_2$ , etc.; areas "B" and "C" may be assigned to  $-\text{OCF}_2\text{CF}_2\text{O}$ -,  $-\text{OCF}_2\text{CF}_2\text{CF}_2\text{CF}_2-$  groups depending on what is attached to the oxygen, e.g.,  $-\text{OCF}_2\text{CF}_2\text{OCF}_2\text{O}$ - is different from  $-\text{OCF}_2\text{CF}_2\text{OCF}_2\text{CF}_2\text{O}$ -. Area "D" is due to a  $-\text{CF}_2-$  surrounded by other  $\text{CF}_2$  groups, e.g.,  $-\text{OCF}_2\text{CF}_2\text{CF}_2\text{CF}_2\text{O}$ -. It should be noted that



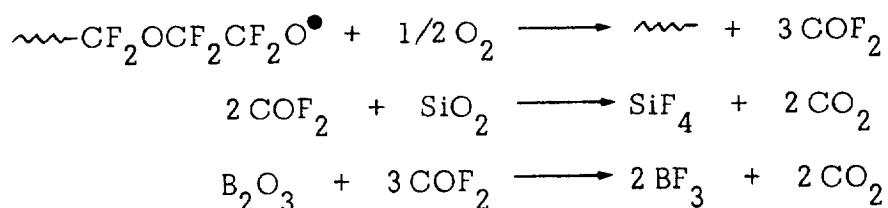
the integral of "D" is similar to that of "B" suggesting that the  $-CF_2O$  absorptions of "B" are related to the  $CF_2$  absorptions of "D". No peaks were found in the 0 to +100 ppm region showing absence of COF groups. The spectra are different from those reported by Sianesi, et al. [ref. 13]. Significantly, there are no doublets with 50-70 HZ splitting characteristic of  $-OCF_2H$  or  $-OCFH-$  or  $-CF_2H$  groups, etc.; in other words, the  $^{19}F$  NMR is consistent with the  $^1H$  NMR in suggesting the absence of protons, Figures 6,7.

The absence of protons is in agreement with the experimental data (discussed in Section 3.1) namely the lack of stabilization after exposure to oxidizing atmospheres for prolonged periods of time. The experimental data would thus indicate that either all the chains are hydrogen-terminated, which should be revealed by proton NMR, or such a termination is insignificantly low and is not responsible for the observed thermal oxidative behavior of the fluids. It is unlikely that residual peroxide linkages are causing the observed thermal oxidative instability since the rate of degradation failed to decrease after prolonged exposure to elevated temperatures. Metals in the absence of oxygen did not cause any fluid degradation supporting further that there are no residual peroxide linkages. Consequently, it must be concluded that the arrangement of the units in the chains or the end-groups are responsible for the observed behavior.

Elemental analyses of the fluid, both "lightly" thermally stressed and after extensive exposure to oxygen at elevated temperature, differ somewhat as evident from the tabulation given in Table V. On the other hand, the variation in carbon content is within acceptable limits and it has been usually found [ref. 15] that in these type of compositions fluorine values are generally low as compared to those actually present. Thus, it is unknown whether the calculated increased oxygen content in the residue of Test No. 19 is real. However, the C:O ratio which is lower for both of the samples than the 2:1 value calculated for  $(CF_2CF_2O)_x$

polymer is definitely real. Consequently, it would appear from these data that the ratio of  $\text{CF}_2\text{O}$  entities to  $\text{CF}_2\text{CF}_2\text{O}$  groups is in the vicinity of 1:1. This would further imply that the concentration of  $-\text{O}(\text{CF}_2)_x\text{O}-$  units wherein  $x$  is higher than 2 is low. All these stipulations do not contradict the NMR spectral findings; unfortunately the latter do not provide information regarding the concentration of specific groups, i.e.,  $-\text{OCF}_2\text{O}-$ ,  $-\text{O}(\text{CF}_2)_2\text{O}-$ ,  $-\text{O}(\text{CF}_2)_4\text{O}-$ , etc.

From the calculations of the ratios of fluid volatilized to oxygen atoms consumed (given in Table VI) for the different segments, it would appear that the content of  $-\text{OCF}_2\text{O}-$  units is higher than that denoted by  $-\text{CF}_2\text{OCF}_2\text{CF}_2\text{O}-$  arrangement. Test Nos. 16, 19, 21, and 31 were carried out in the absence of metal coupons. In these runs only traces of materials non-volatile at  $-78^\circ\text{C}$  were formed. Based on the nature of the collected volatiles, it can be deduced that  $\text{COF}_2$  was the initial product formed,  $\text{SiF}_4$ ,  $\text{CO}_2$ , and  $\text{BF}_3$  are the products of  $\text{COF}_2$  interactions with constituents of glass at the elevated temperatures:



Inasmuch as at least some  $\text{COF}_2$  survived the treatment, one would expect to see  $\text{CF}_3\text{COF}$  or related acid fluorides if there was substantial content of  $-\text{O}(\text{CF}_2)_x\text{O}-$  units where  $x$  is higher than 2. It should be noted that  $\text{CF}_3\text{COF}$  was found in the volatiles formed by hexafluoropropene oxide derived polyethers [ref. 3, 4], but none was detected in the Pomblin Z investigations.

Metals definitely promoted scission of the chain bonds as shown by the increased ratio of the volatilized fluid to oxygen consumed and by the type of products formed. This is especially significant in the case of

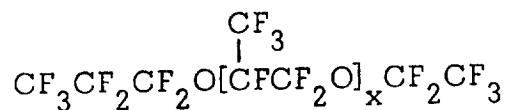
Ti(4 Al, 4 Mn) alloy wherein at 288°C almost half of the products were in the form of the relatively involatile -COF terminated chains as determined by infrared spectral analysis. Characterization of these compounds, after transformation to the corresponding methyl esters, by GC-MS analysis, should provide some information with respect to the type of units present in the fluid. This will be performed under the follow-on program.

### 3.3 Investigation of Polyperfluoroalkylethers Derived from Hexafluoropropene Oxide

The studies conducted under U.S. Air Force sponsorship [ref. 3,4] revealed that hexafluoropropene oxide derived fluids, produced by DuPont de Nemours Co. under the trade name of Krytox, exhibited thermal oxidative instability which could be eliminated by prolonged treatment in oxygen at 343°C (650°F). At that time it was speculated that this phenomenon was due to the presence of a certain proportion of hydrogen-terminated chains which were degraded and volatilized on exposure to oxygen at elevated temperatures leaving behind the stable perfluoroalkyl-terminated materials. NMR spectral analyses verify fully this theory.

The proton NMR of the fluid as received (see Figure 8) shows the presence of CF<sub>3</sub>CFHO- as a typical doublet at 5.9 ppm. This doublet is also exhibited by the fully characterized compound C<sub>3</sub>F<sub>7</sub>OCF(CF<sub>3</sub>)H in Figure 9. After the thermal oxidative exposure at 343°C, these peaks disappear entirely as attested by the 812 scans of this region in Figure 10.

The <sup>19</sup>F NMR spectra of Krytox MLO-71-6 are given in Figures 11-13. Based on the structure of the hydrogen-free fluid given below,



the assignment of the peaks is as follows:

$\begin{array}{c} \text{CF}_3 \\ | \\ -\text{OCF}- \end{array}$  and  $-\text{CF}_2\text{O}-$  complex peak at -80.3 ppm

$\text{CF}_3\text{CF}_2\text{CF}_2\text{O}$  spike at -82.2 ppm

$\text{CF}_3\text{CF}_2\text{O}$  spike at -87.7 ppm

$\text{CF}_3\text{CF}_2\text{CF}_2\text{O}$  spike at -130.0 ppm

$\begin{array}{c} \text{OCF} \\ | \\ \text{CF}_3 \end{array}$  peak at -144.3 ppm

If x is 30 then the integral ratio between the peaks at -130.0 and -144.3 ppm should be 1/15. It is difficult to measure this ratio accurately, but it seems to be approximately 1/18. This would make x=36 (see Figure 13) resulting in an average molecular weight of 6280. If one considers the accuracy involved, the agreement with the osmometrically measured value of 5500 [ref. 3,4] is very good.

Past studies have shown that even at 288°C (550°F) exposure of the as-received fluid (not pretreated in oxygen at 343°C) to Ti(4 Al, 4 Mn) alloy in oxygen resulted in extensive degradation. The rate of the degradation increased with time. It was postulated at that time that this behavior was due to the aluminum component of the alloy. Based on the results of Test Nos. 22 and 23 (see Table VII), this is not the case since even at 316°C (600°F) no increase, but rather a substantial decrease in degradation was noted on successive exposures of the fluid to temperature in the presence of the aluminum metal and oxygen. Fluid which had been pretreated in oxygen at 343°C was virtually inert to the aluminum coupon at 316°F (see Test No. 24).

The action of pure titanium metal on the as-received fluid, at least for the first 48 hr (see Test Nos. 25 and 26), was directly comparable to that of the aluminum metal. Yet, the extent of degradation observed with the pretreated fluid, as measured by the volatiles formed, was significantly

larger (compare Test Nos. 24 and 27). Interestingly, this rate of degradation was virtually unaffected whether the coupon was used previously or whether it was freshly polished. Successive exposures and different periods of exposure failed to change the rate from  $\sim 10$  mg/g/24 hr. This finding would indicate that the titanium metal promotes scissions of the bonds within a chain at a steady rate. This action would not seem to be caused by titanium fluoride since if this was the case, an increase in the rate with time would be expected. One would visualize that this type of action is surface area dependent. Thus, the presence of a larger coupon or multiple coupons should increase the rate. Due to funds limitation, this was not established. The results obtained from the investigations of the pure aluminum and titanium metals differ drastically from those found with the Ti(4 Al, 4 Mn) alloy. Whether these differences are due to the alloying process or the presence of manganese will be determined under the follow-on effort.

#### 4. EXPERIMENTAL DETAILS AND PROCEDURES

The perfluoroalkylether fluids employed in this study, namely Krytox, MLO-71-6 fluid (product of E. I. DuPont de Nemours and Co), and the Fomblin Z fluids, MLO-72-22 and MLO-79-129 (products of Montecatini Edison), and P-3 additive were obtained through the courtesy of Mr. C. E. Snyder, Air Force Wright Aeronautical Laboratories.

The degradation apparatus was a modified, scaled-down version of the AFML Micro-O-C-Test arrangement [ref. 6,7]. It was described in detail previously [ref. 3,4]. The schematics given in Figures 14 and 15 show the reaction tube configuration and the rod assembly for holding the metal coupon specimens. The metal coupons were 3/8" OD and 1/8" ID. These were obtained from Metaspec Company, San Antonio, Texas. For heating of sample tubes in a vertical position, a modified Lindberg Heavy-Duty box furnace, Type 51232 (see Figure 16) was utilized. In this arrangement, 180 mm of the 420 mm tube was at temperature; the fluid occupied at the most the lower 75 mm (see Figure 14), the extra gas reservoir was in the ambient environment.

In a typical experiment, the fluid was introduced into the degradation tube (see Figure 14) which was then evacuated and filled to a known pressure at a known temperature with a selected gas (air,  $N_2$ , or  $O_2$ ). Inasmuch as the apparatus was calibrated and the fluid volume measured accurately, the quantity of gas thus introduced was exactly known. The degradation tube was then inserted into the preheated box furnace and kept there for a specified period of time; throughout this exposure the temperature was continuously recorded. After removal from the furnace, the tube was allowed to cool to room temperature, attached to the high vacuum line, and opened. The liquid nitrogen noncondensibles were collected quantitatively, measured, and analyzed by mass spectrometry. The liquid nitrogen con-

densibles, which were volatile at room temperature, were measured, weighed, and analyzed by infrared spectroscopy and mass spectrometry. The fluid residue itself was weighed and subjected to infrared spectral analysis; in selected instances, molecular weight and NMR determinations were performed.

The metal coupons prior to testing were polished using first Norton No-Fil Durite finishing paper Type 4 220A. This was followed by open coat Silicon Carbide papers grades 400A and 500A, respectively. Subsequently, the coupons were washed with Freon 113, dried, weighed, and suspended in the test apparatus (see Figure 15). After the completion of a given experiment, the metal coupons were washed with Freon 113, dried inside an inert atmosphere chamber, then weighed and visually inspected. The used coupons were subsequently sealed in Mylar envelopes.

## 5. PRELIMINARY CONCLUSIONS

Summarized below are conclusions reached during the current investigations of thermal oxidative degradation reactions of perfluoroalkylethers.

1. Fomblin Z fluids were found to be inherently unstable when subjected to elevated temperatures,  $\sim 316^{\circ}\text{C}$  ( $600^{\circ}\text{F}$ ), in oxidizing atmospheres. This instability is not due to hydrogen termination or the presence of peroxy linkages, or oxidatively removable impurities.

2. Fomblin Z fluids do not have the structural arrangement derived from tetrafluoroethylene oxide, rather they represent a chain system of difluoroformyl and tetrafluoroethylene oxide units with the former predominating.

3. Fomblin Z fluids in oxidizing atmospheres at  $316^{\circ}\text{C}$  ( $600^{\circ}\text{F}$ ) degrade completely in the presence of M-50 and Ti(4 Al, 4 Mn) alloys. The effectiveness of additives under these conditions is minimal. The additives are effective in arresting the degradation process at  $288^{\circ}\text{C}$  ( $550^{\circ}\text{F}$ ). Metal alloy's action is due to polymer bond scissions. The alloys do not promote the fluids' degradation in inert atmospheres at  $316^{\circ}\text{C}$  ( $600^{\circ}\text{F}$ ).

4. The presence of hydrogen chain termination was established to be the cause of thermal oxidative instability exhibited by "untreated" poly(hexafluoropropene oxide) fluids.

5. Based on pure metal studies, it does not appear that aluminum and titanium metals are responsible for the observed action of Ti(4 Al, 4 Mn) alloy in the poly(hexafluoropropene oxide) fluids.



## 6. REFERENCES

1. W. H. Gumprecht, The Preparation and Thermal Behavior of Hexafluoropropylene Epoxide Polymers, paper presented at the Fourth International Symposium on Fluorine Chemistry, Estes Park, Colorado, July 1967.
2. W. H. Gumprecht, The Preparation, Chemistry, and some Properties of Hexafluoropropylene Epoxide Polymers, paper presented at the Gordon Fluorine Conference, New Hampshire, 1968.
3. K. L. Paciorek, R. H. Kratzer, J. Kaufman, and J. H. Nakahara, Determination of Fluorocarbon Ether Autoxidative Degradation Mechanism, AFML-TR-77-150, August 1977.
4. K. L. Paciorek, R. H. Kratzer, J. Kaufman, and J. H. Nakahara, Thermal Oxidative Studies of Poly(hexafluoropropene oxide) Fluids, *J. Appl. Polymer Sci.*, 24, 1397 (1979).
5. C. Tamborski and C. E. Snyder, Synthesis and Use of Perfluoroalkylarylphosphines in High Temperature Fluid Applications, paper presented at the Third Winter Fluorine Conference, St. Petersburg, Florida, January 1977.
6. C. E. Snyder and R. E. Dolle, Development of Polyperfluoroalkylethers as High Temperature Lubricants and Hydraulic Fluids, *ASLE Transactions*, 19 (3), 171 (1976).
7. R. E. Dolle and F. J. Harsacky, New High Temperature Additive Systems for PR-143 Fluids, AFML-TR-65-349, January 1966.
8. R. E. Dolle, High Temperature Corrosion Preventive Additives for Fluorocarbon Polyether Fluids, AFML-TR-67-210, September 1967.

9. G. J. Morris, Interaction Between Perfluoroalkyl Polyether Linear and Cyclic Derivative Fluids and High Temperature Bearing Steels in Oxidation Corrosion Environment, AFML-TR-73-175, November 1973.
10. C. E. Snyder, C. Tamborski, H. Gopol, and C. A. Svisco, Synthesis and Development of Improved High-Temperature Additives for Polyperfluoroalkylether Lubricants and Hydraulic Fluid, ASLE Preprint No. 78-AM-B-2.
11. C. E. Snyder, L. J. Gschwender, and C. Tamborski, Linear Polyperfluoroalkylether Based Wide-Liquid-Range High-Temperature Fluids and Lubricants, ASLE Preprint No. 80-AM-5C-3.
12. D. Sianesi, V. Zamboni, R. Fontanelli, and M. Binaghi, *Wear*, 18, 85 (1971).
13. D. Sianesi, A. Pasetti, and G. Belardinelli, U.S. Patent 3,715,378, February 6, 1973.
14. Private communications.
15. K. J. L. Paciorek, T. I. Ito, J. H. Nakahara, and R. H. Kratzer, work performed under U.S. Air Force Contract Nos. F44620-76-C-0065 and F49620-79-C-0037.

TABLE I  
THERMAL AND THERMAL OXIDATIVE INVESTIGATIONS OF  
FOMBLIN Z FLUID, BATCH MLO-72-22

Test No. <sup>a</sup>	Amt Used, g	Atm	Temp °C	Duration hr	MW	Condensable Products			Oxygen Consumed			CO Produced		
						mg	mg/g <sup>b</sup>	mg	mg/g <sup>c</sup>	mg/mg <sup>d</sup>	% <sup>e</sup>	mg	mg/mg <sup>f</sup>	
1	26.33	N <sub>2</sub>	150	3				-	-	-	-	-	-	-
			200	2				-	-	-	-	-	-	-
			250	2	15500 <sup>g</sup>	0.2	0.01	-	-	-	-	-	-	-
4 <sup>h</sup>	3.46	Air	150	3		1.0	0.29	-	-	-	-	-	-	-
			200	3		1.3	0.38	-	-	-	-	-	-	-
			250	3		1.1	0.32	-	-	-	-	-	-	-
			288	3		1.2	0.35	-	-	-	-	-	-	-
			316	3		2.6	0.75	n.d. <sup>1</sup>	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
5 <sup>h</sup>	3.44	Air	316	24		165.0	47.97	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
6 <sup>h</sup>	3.26	O <sub>2</sub>	316	24		72.7	22.30	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
9 <sup>h</sup>	3.16	O <sub>2</sub>	316	24		90.3	28.58	1.59	0.50	0.02	0.5	2.7	0.03	n.d.
10 <sup>h</sup>	3.07	O <sub>2</sub>	316	48		118.9	38.73	4.27	1.39	0.04	1.4	4.7	0.04	n.d.
12 <sup>h</sup>	3.02	O <sub>2</sub>	332	24		81.4	26.95	1.69	0.53	0.02	0.5	2.7	0.03	n.d.
17 <sup>h</sup>	2.95	O <sub>2</sub>	343	100		792.2	268.54	23.81	8.07	0.03	7.8	6.2	0.01	n.d.
19 <sup>h</sup>	1.76	O <sub>2</sub>	343	48	8600	216.1	122.78	7.46	4.23	0.03	2.4	4.7	0.01	n.d.
21 <sup>j</sup>	19.51	O <sub>2</sub>	343	24	15100	422.5	21.65	15.86	0.81	0.03	5.4	6.9	0.02	n.d.
30	24.15	O <sub>2</sub>	343	24	14100	435.3	18.02	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
31 <sup>k</sup>	4.27	O <sub>2</sub>	316	24		278.5	65.22	11.21	2.62	0.04	3.7	2.7	0.01	n.d.
39	54.54	O <sub>2</sub>	343	24		942.0	17.27	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
40 <sup>k</sup>	3.74	O <sub>2</sub>	288	24		92.0	24.60	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

a) Test Nos. 1 and 4 were conducted on a vacuum line; the remainder of the tests were carried out in a 428 ml straight tube apparatus (ref. 3).

b) Products in mg per g of fluid employed.

c) Oxygen consumed in mg per g of fluid employed.

d) Oxygen consumed in mg per mg of products formed.

e) Percent of oxygen available.

f) Mg of carbon monoxide formed per mg of products liberated.

g) Molecular weight of as received MLO-72-22 was found to be 13100.

h) Fluid used for this test was the involatile residue of the preceding test.

i) Not determined.

j) Fluid used for this test was the residue of Test No. 1.

k) Fluid used was the combined residues of Test Nos. 21 and 30.

TABLE II  
 THERMAL AND THERMAL OXIDATIVE INVESTIGATIONS OF  
 FOMBLIN Z FLUID, BATCH MLO-79-196

Test No. <sup>a</sup>	Amt Used, g	Atm	Temp °C	Duration hr	MW	Condensible Products		Oxygen Consumed			CO Produced <sup>f</sup>		
						mg	mg/g <sup>b</sup>	mg	mg/g <sup>c</sup>	mg/mg <sup>d</sup>	% <sup>e</sup>	mg	mg/mg
2	35.29	N <sub>2</sub>	150	3									
3 <sup>h</sup>	32.71	N <sub>2</sub>	200	2	7100 <sup>g</sup>	16.9	0.48						
7 <sup>h</sup>	5.03	N <sub>2</sub>	250	6.6		0.8	0.02						
		N <sub>2</sub>	288	6		0.5	0.10						
8 <sup>h</sup>	5.03	Air	316	6		0.8	0.16						
11 <sup>h</sup>	3.90	Air	288	3	6500	0.2	0.04	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
13 <sup>h</sup>	3.82	O <sub>2</sub>	316	24		62.7	16.08	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
14 <sup>h</sup>	3.77	O <sub>2</sub>	316	24		60.6	15.86	5.42	1.42	0.09	2.7	0.04	0.04
15 <sup>h</sup>	3.71	O <sub>2</sub>	316	24		63.6	16.87	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
16 <sup>h</sup>	3.46	O <sub>2</sub>	332	48	6000	246.9	66.55	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
		O <sub>2</sub>	332	48		271.5	78.46	8.48	2.45	0.03	4.2	0.02	0.02

a) Test Nos. 2, 3, and 7 were conducted on a vacuum line; the remainder of the tests were carried out in a 428 ml straight tube apparatus (ref. 3).

b) Products in mg per g of fluid employed.

c) Oxygen consumed in mg per g of fluid employed.

d) Oxygen consumed in mg per mg of products formed.

e) Percent of oxygen available.

f) Mg of carbon monoxide formed per mg of products liberated.

g) Molecular weight of as received MLO-79-196 was found to be 6400.

h) Fluid used for this test was the involatile residue of the preceding test.

i) Not determined.

TABLE III  
EFFECTS OF METAL COUPONS AND ADDITIVES ON THERMAL AND  
THERMAL OXIDATIVE BEHAVIOR OF FOMBLIN Z FLUID, BATCH MEO-72-22

Test No.	Amt Used, g	Atm	Temp °C	Duration hr	Coupon	Additive	Condensable Products		mg	mg/g <sup>b</sup>	mg	Oxygen Consumed		CO Produced	
							mg	mg/g				mg/g <sup>c</sup>	% <sup>e</sup>	mg	mg/g
31	4.27	O <sub>2</sub>	316	24	None	None	278.5	65.22	11.21	2.62	0.04	3.7	2.7	0.01	
32A	4.24	O <sub>2</sub>	316	24	M-50	None	?	?	n.d. <sup>g</sup>	n.d.	n.d.	n.d.	n.d.	n.d.	
32B	4.17	O <sub>2</sub>	316	8	M-50	None	2666.0	639.33	104.69	25.10	0.04	35.0	2.5	0.00	
33	3.84	O <sub>2</sub>	316	24	None	1% P-3 <sup>h</sup>	11.3	2.94	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	
34	4.08	O <sub>2</sub>	316	24	M-50	1% P-3	1176.2	286.28	27.51	6.74	0.02	9.2	11.7	0.01	
35	3.39	O <sub>2</sub>	316	24	M-50	1% C <sub>2</sub> PN <sub>3</sub> <sup>i</sup>	535.1	157.85	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	
36	3.34	O <sub>2</sub>	288	24	M-50	1% C <sub>2</sub> PN <sub>3</sub>	1.1	0.33	-	-	-	-	-	-	
37	3.57	O <sub>2</sub>	288	24	M-50	P-3	3.4	0.95	-	-	-	-	-	-	
38	3.34	O <sub>2</sub>	288	15	M-50	None	1117.1	421.55	40.42	12.10	0.04	13.57	1.3	0.00	
40	3.74	O <sub>2</sub>	288	24	None	None	92.0	24.60	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	
41	3.84	O <sub>2</sub>	288	8	Ti (4 Al, 4 Mn)	None	2235.0	582.03	51.14	13.31	0.02	17.24	4.2	0.00	
42	3.67	O <sub>2</sub>	288	24	Ti (4 Al, 4 Mn)	1% P-3	4.1	1.12	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	
43	3.65	N <sub>2</sub>	316	24	None	None	8.1	2.22	-	-	-	-	-	-	
44	3.96	N <sub>2</sub>	316	24	M-50	None	9.0	2.27	-	-	-	-	-	-	
45	3.87	N <sub>2</sub>	316	24	Ti (4 Al, 4 Mn)	None	9.2	2.38	-	-	-	-	-	-	

a) All the fluids used were pretreated at 343°C for 24 hr.

b) Products in mg per g of fluid employed.

c) Oxygen consumed in mg per g of fluid employed.

d) Oxygen consumed in mg per mg of products formed.

e) Percent of oxygen available.

f) Mg of carbon monoxide formed per mg of products liberated.

g) Not determined.

h) MLO-80-279.

i) [C<sub>3</sub>F<sub>7</sub>OCF(CF<sub>3</sub>)CF<sub>2</sub>OCF(CF<sub>3</sub>)CN]<sub>2</sub>[(C<sub>6</sub>H<sub>5</sub>)<sub>2</sub>PN], monophospho-s-triazine.

TABLE IV  
 PRODUCT DISTRIBUTION, THERMOOXIDATIVE DEGRADATION  
 OF FOMBLIN Z FLUIDS<sup>a</sup>

Test No.	O <sub>2</sub> consmd. mmol	Volatile Products			CO <sub>2</sub>	Type, %		
		mmol	MW found	MW calcd.		COF <sub>2</sub>	SIF <sub>4</sub>	BF <sub>3</sub>
5	n.d. <sup>b</sup>	2.576	64	60	65	3.1	22	9.5
6	0.387	1.137	64	62	60	3.7	26	9.8
9	0.050	1.353	67	63	63	2.2	26	9.8
10	0.134	1.887	63	64	60	2.0	28	9.9
12	0.050	1.294	63	60	66	2.2	22	10.3
13	0.169	0.943	64	57	68	5.2	16	10.6
14	n.d.	0.977	65	54	73	4.0	11	12.0
15	0.499	3.796	65	70	53	0.9	41	5.0
16	0.265	4.406	62	74	46	1.3	46	6.8
17	0.729	10.888	73	69	52	0.4	36	11.7
19	0.233	3.056	71	67	55	1.5	34	9.0
21	0.496	6.727	63	62	66	0.4	27	6.6
31	0.351	4.149	64	62	61	6.6	25	7.0
32B	3.272	31.299	78	62	54	19.7	21	5.2
33	0.025	0.152	74	76	47	0.9	52	0.5
34	0.860	15.358	70	66	49	13.6	30	6.9
38	1.263	13.905	63	56	67	13.9	13	5.8
40	0.246	1.116	66	54	70	14.9	9	6.4
41	2.169	17.574	67	56	64	23.3	11	2.0

a) The quantities of CO<sub>2</sub>, COF<sub>2</sub>, and BF<sub>3</sub> were determined by infrared spectral analysis; the proportion of SIF<sub>4</sub> was obtained by difference.

b) Not determined.

TABLE V  
ELEMENTAL ANALYSIS CONSIDERATIONS

Material	C %	F %	C : F : O
MLO-72-22 (Test 21)	20.03	61.21	2.85 : 5.50 : 2
MLO-72-2 (Test 19)	19.63	60.09	2.57 : 4.99 : 2 3.86 : 7.48 : 3
$(CF_2CF_2O)_x$	20.69	65.52	2 : 4 : 1
$(CF_2OCF_2OCF_2CF_2O)_x$	19.37	61.29	4 : 8 : 3
$(CF_2OCF_2CF_2O)_x$	19.80	62.64	3 : 6 : 2

TABLE VI  
 INFLUENCE OF METAL COUPONS UPON RATIOS OF  
 VOLATILIZED FLUID TO OXYGEN CONSUMED

Test No.	Atm	Temp °C	Coupon	Products mg	Ratio mmol fluid lost to O atoms consmd	
					Segm, 116 <sup>a</sup>	Segm, 182 <sup>b</sup>
16	O <sub>2</sub>	332	None	272	2.1 : 1	1.3 : 1
19	O <sub>2</sub>	343	None	216	2.6 : 1	1.5 : 1
21	O <sub>2</sub>	343	None	426	2.1 : 1	1.3 : 1
31	O <sub>2</sub>	316	None	279 (4) <sup>c</sup>	2.0 : 1	1.2 : 1
32B	O <sub>2</sub>	316	M-50	2666 (10)	2.6 : 1	1.7 : 1
38	O <sub>2</sub>	288	M-50	1117 (22)	3.7 : 1	2.3 : 1
41	O <sub>2</sub>	288	Ti (4 Al, 4 Mn)	2235 (47)	4.6 : 1	2.9 : 1

a) Segment -CF<sub>2</sub>CF<sub>2</sub>O-.

b) Segment -CF<sub>2</sub>OCF<sub>2</sub>CF<sub>2</sub>O-.

c) Values in brackets correspond to the percentage of products which were involatile at -78°C.



TABLE VII  
EFFECT OF METAL COUPONS ON THERMAL OXIDATIVE BEHAVIOR  
OF POLYHEXAFLUOROPROPENE OXIDE FLUIDS

Test No. <sup>b</sup>	Metal	Amt Used	Temp °C	Duration hr	Total Products <sup>c</sup>	
					mg	mg/g <sup>d</sup>
18/20	-	28.22	343	194	1950	69.1
22	Al	4.52	316	24	201.1	44.5
23 <sup>e</sup>	Al	4.32	316	24	52.6	12.2
24 <sup>f</sup>	Al	4.52	316	24	1.8	0.4
25	Ti	4.34	316	24	224.1	51.6
26 <sup>g</sup>	Ti	4.12	316	24	51.6	12.5
27 <sup>f</sup>	Ti	4.38	316	24	24.9	8.0
28 <sup>h</sup>	Ti	3.48	316	24	39.9	11.5
29 <sup>i</sup>	Ti	3.44	316	64	97.1	28.2

- a) In all tests, Krytox MLO-71-6 was employed in an oxygen atmosphere.  
b) All tests were carried out in a 418 ml sealed ampoule.  
c) These are room temperature volatiles condensable at -196°C.  
d) Products formed in mg/g of material employed.  
e) The residue of Test No. 22 was utilized in this experiment.  
f) A portion of the involatile residue of Test No. 20 was used in this experiment.  
g) The residue of Test No. 25 was used in this experiment.  
h) The residue of Test No. 27 was used in this experiment with a fresh Ti metal coupon.  
i) The residue of Test No. 28 was used in this experiment, the coupon was not changed.

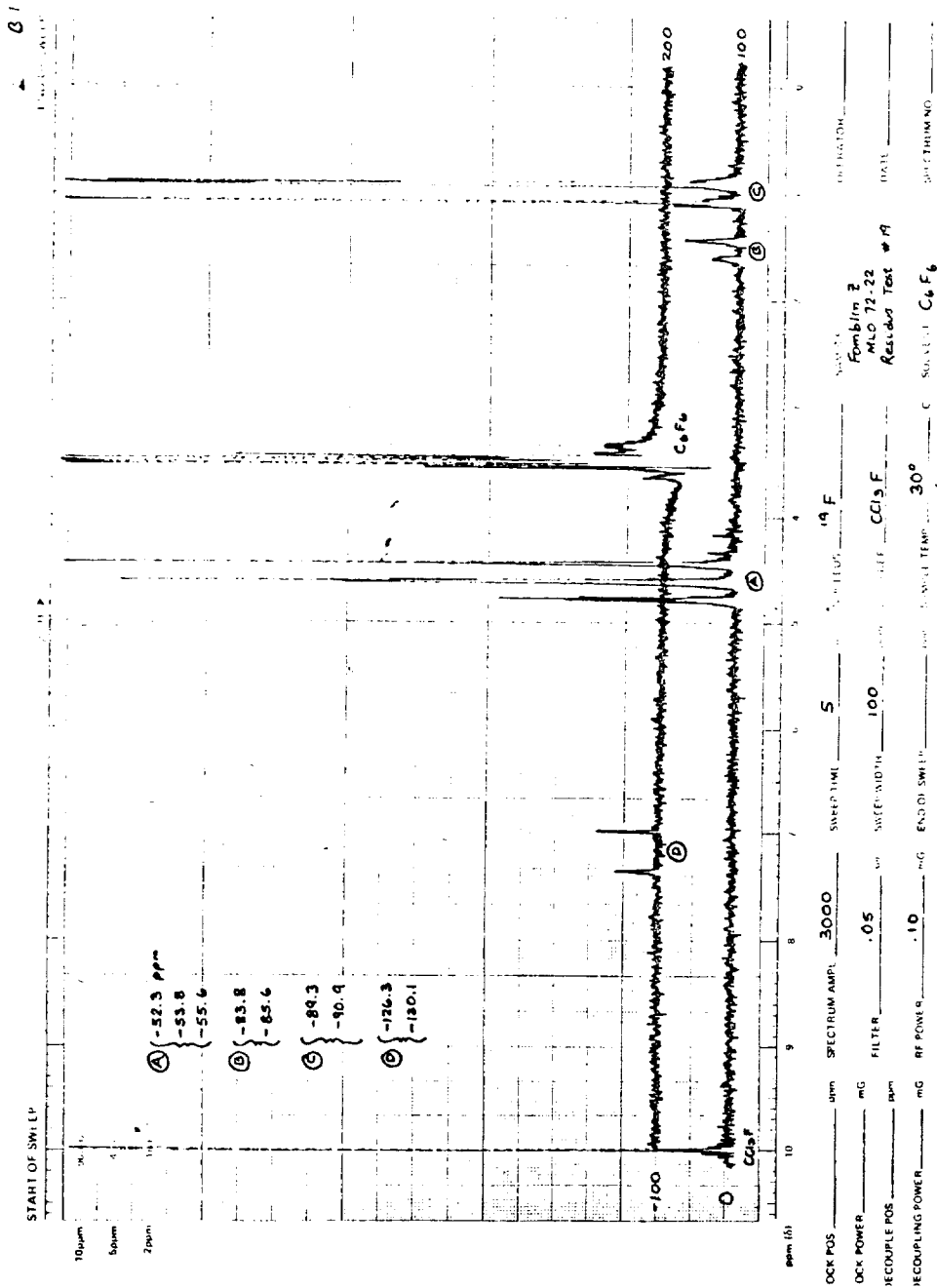


Figure 1: <sup>19</sup>F NMR spectrum of Fomblin Z fluid MLO-72-22

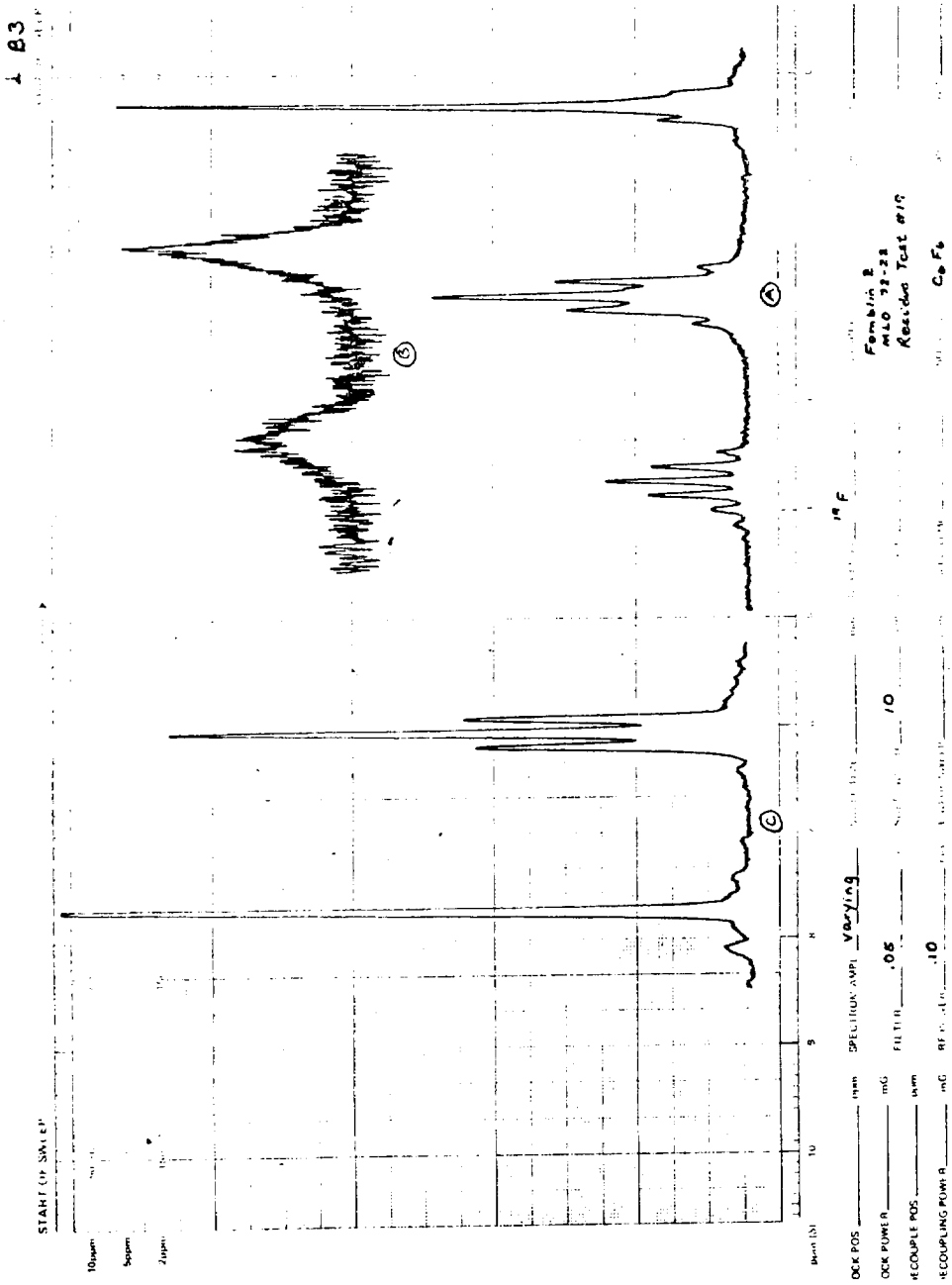


Figure 2:  $^{19}\text{F}$  NMR spectrum of Fomblin Z fluid MLO-72-22, expanded sections A, B, and C

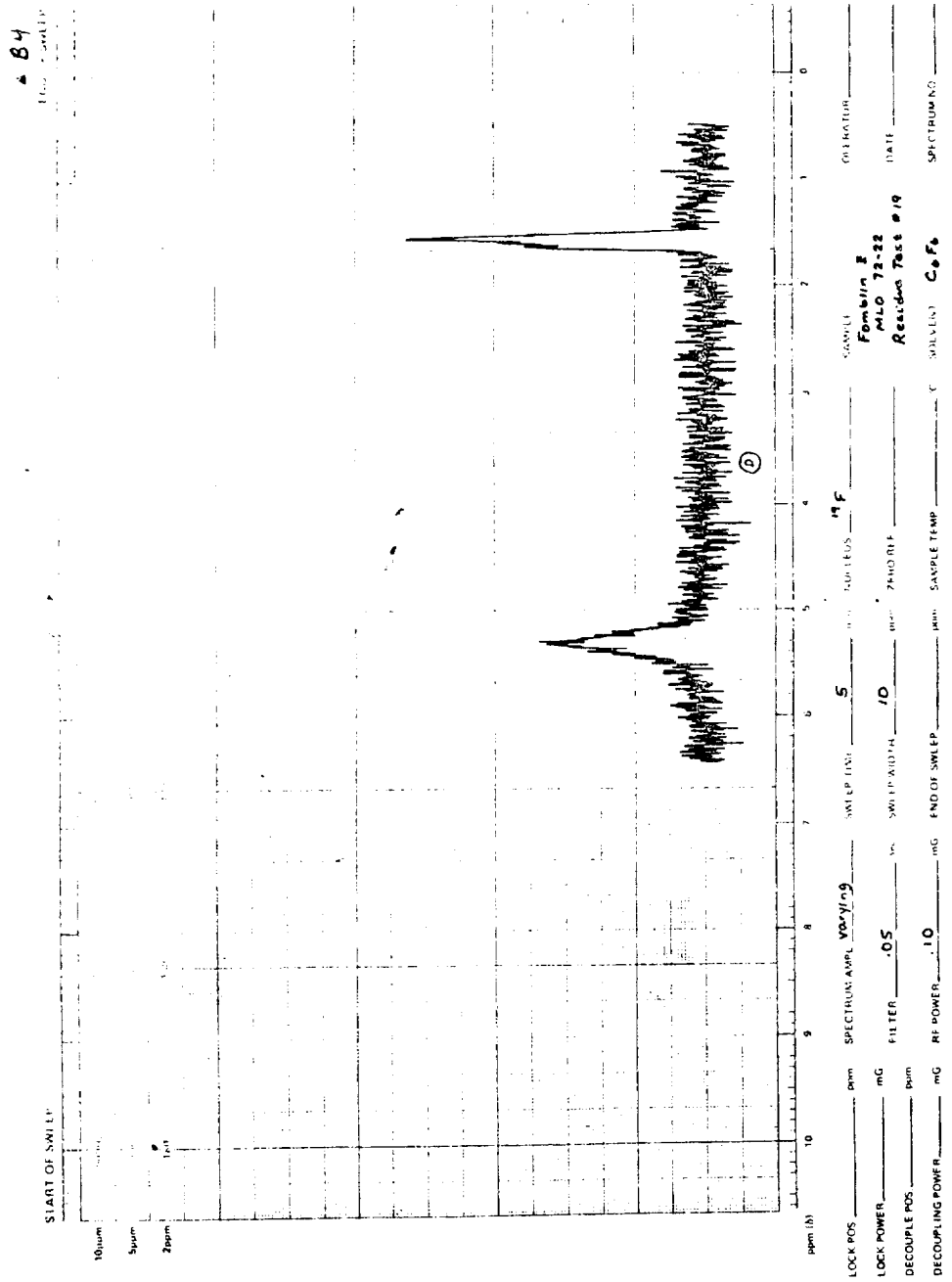


Figure 3: <sup>19</sup>F NMR spectrum of Fomblin Z fluid MLO-72-22, expanded section B

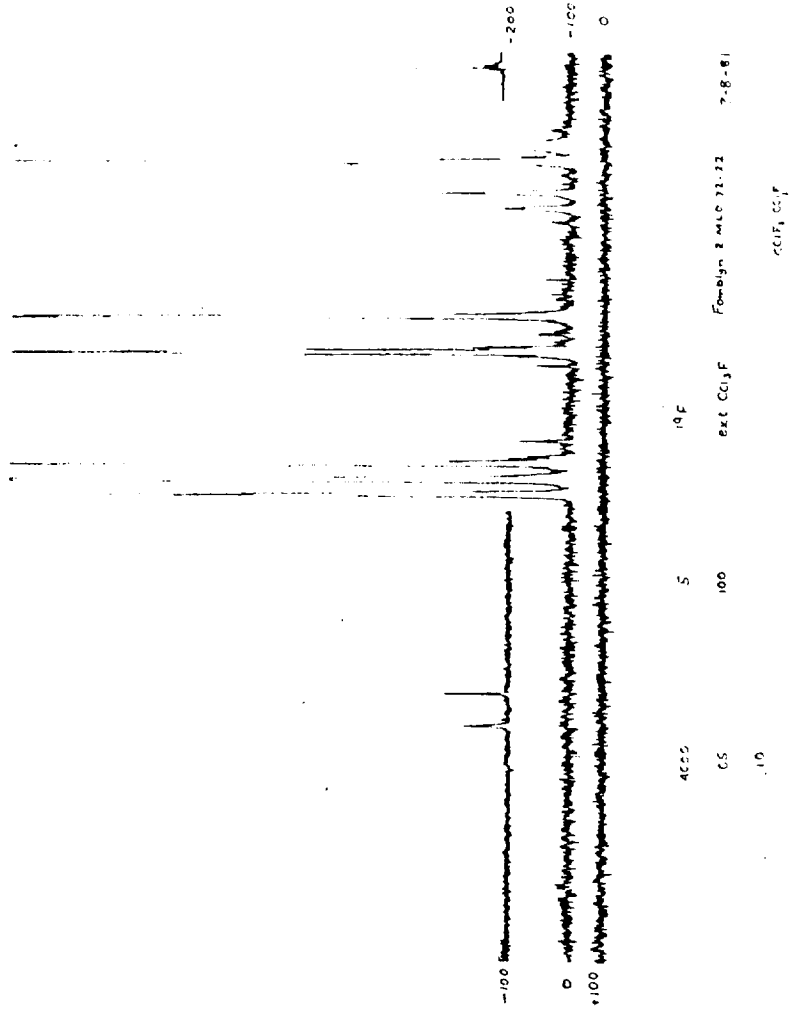


Figure 4: <sup>19</sup>F NMR spectrum of Fomblin Z fluid MLO-72-22, from -200 to +100 ppm

22

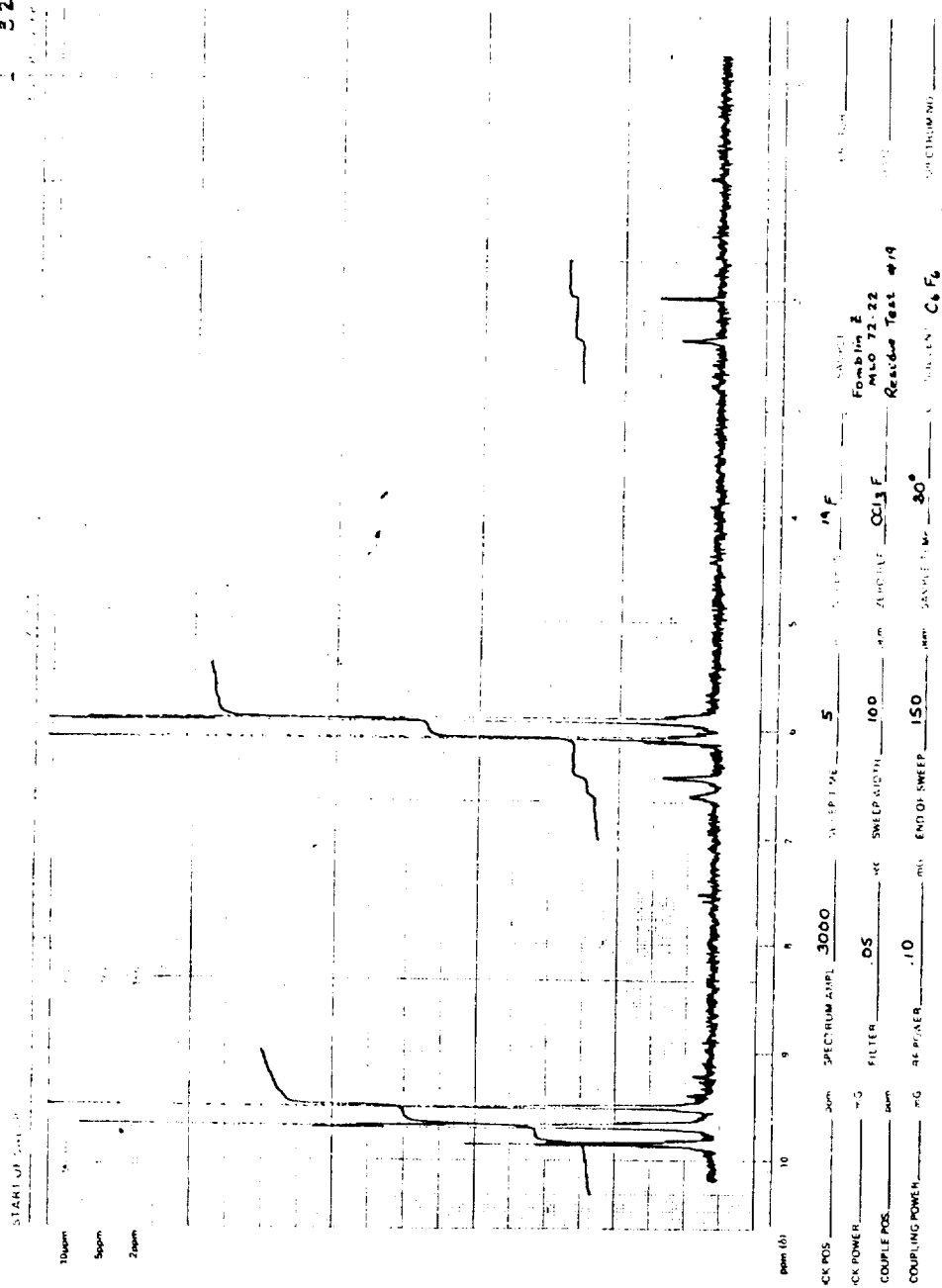


Figure 5: <sup>19</sup>F NMR spectrum of Fomblin Z fluid MLO-72-22, integrated data

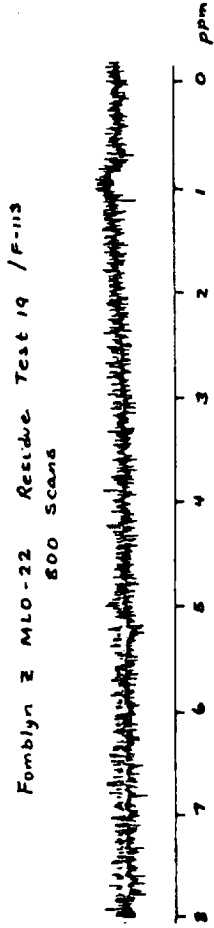


Figure 6: Proton NMR spectrum of Fomblin Z fluid  
(Residue Test No. 19)

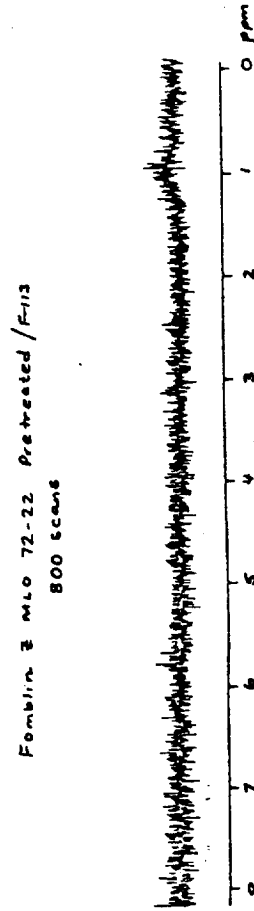


Figure 7: Proton NMR spectrum of Fomblin Z fluid  
(Residue Test No. 21)

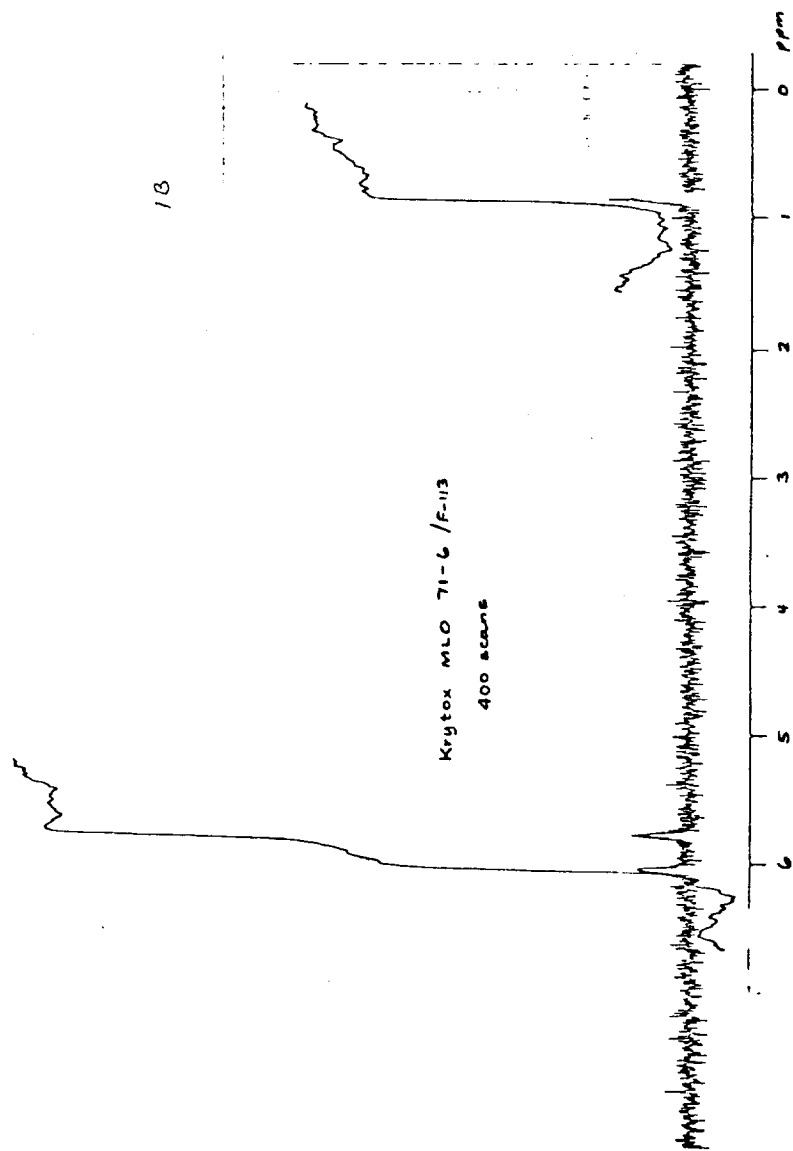


Figure 8: Proton NMR spectrum of Krytox MLO-71-6 fluid (as received)



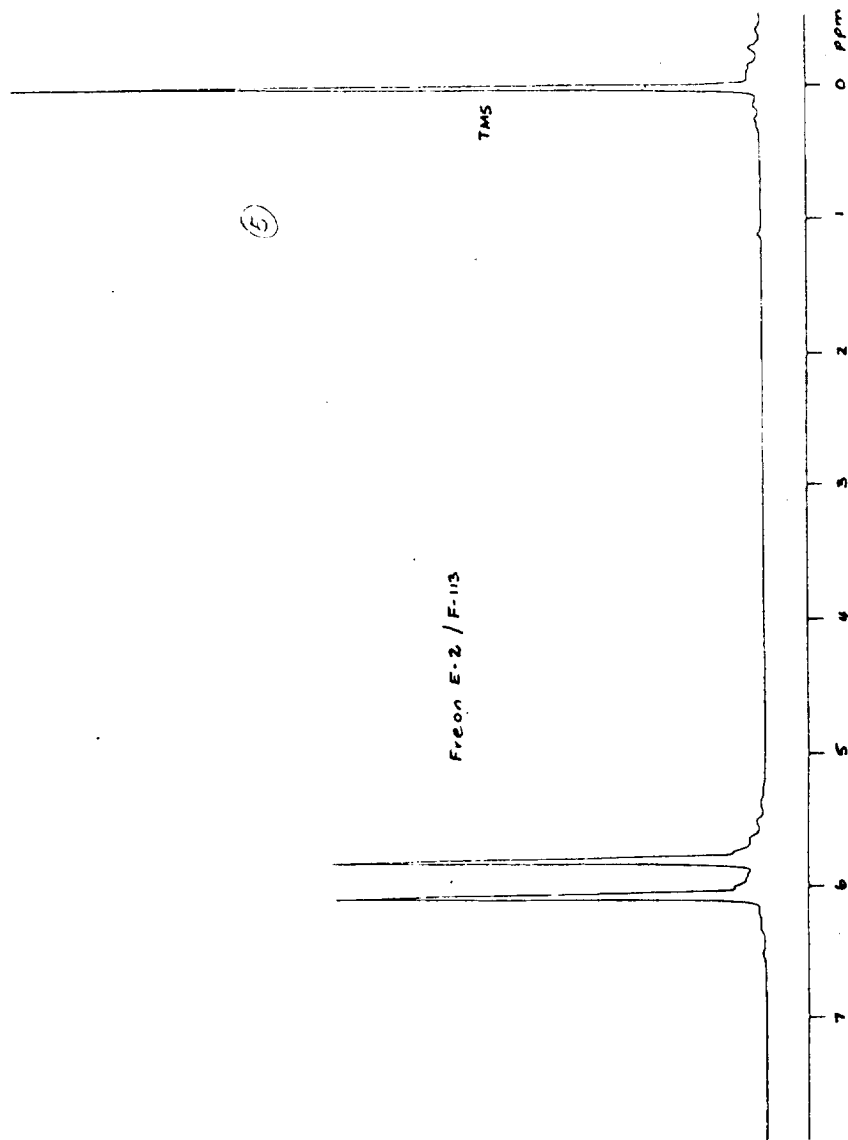


Figure 9: Proton NMR spectrum of Freon E-2,  $C_3F_7OCF(CF_3)H$

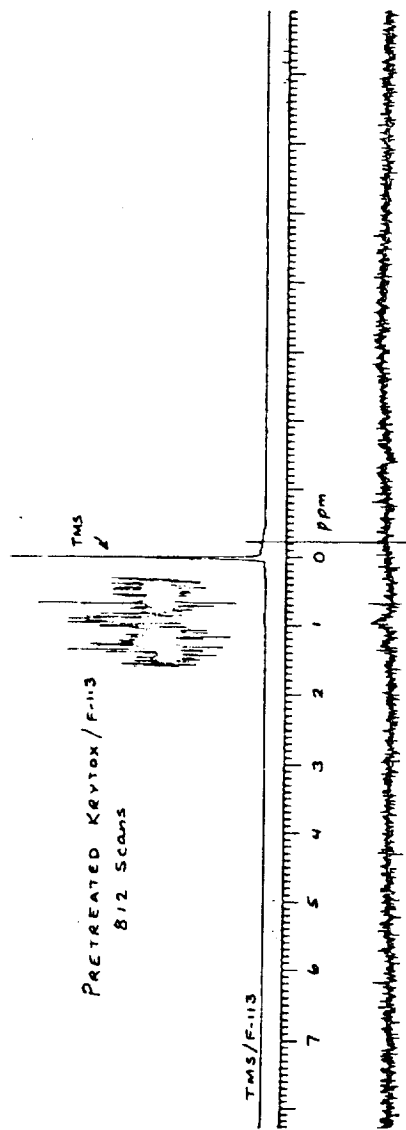


Figure 10: Proton NMR spectrum of Krytox MLO-71-6 fluid (recovered after Test 18/20)

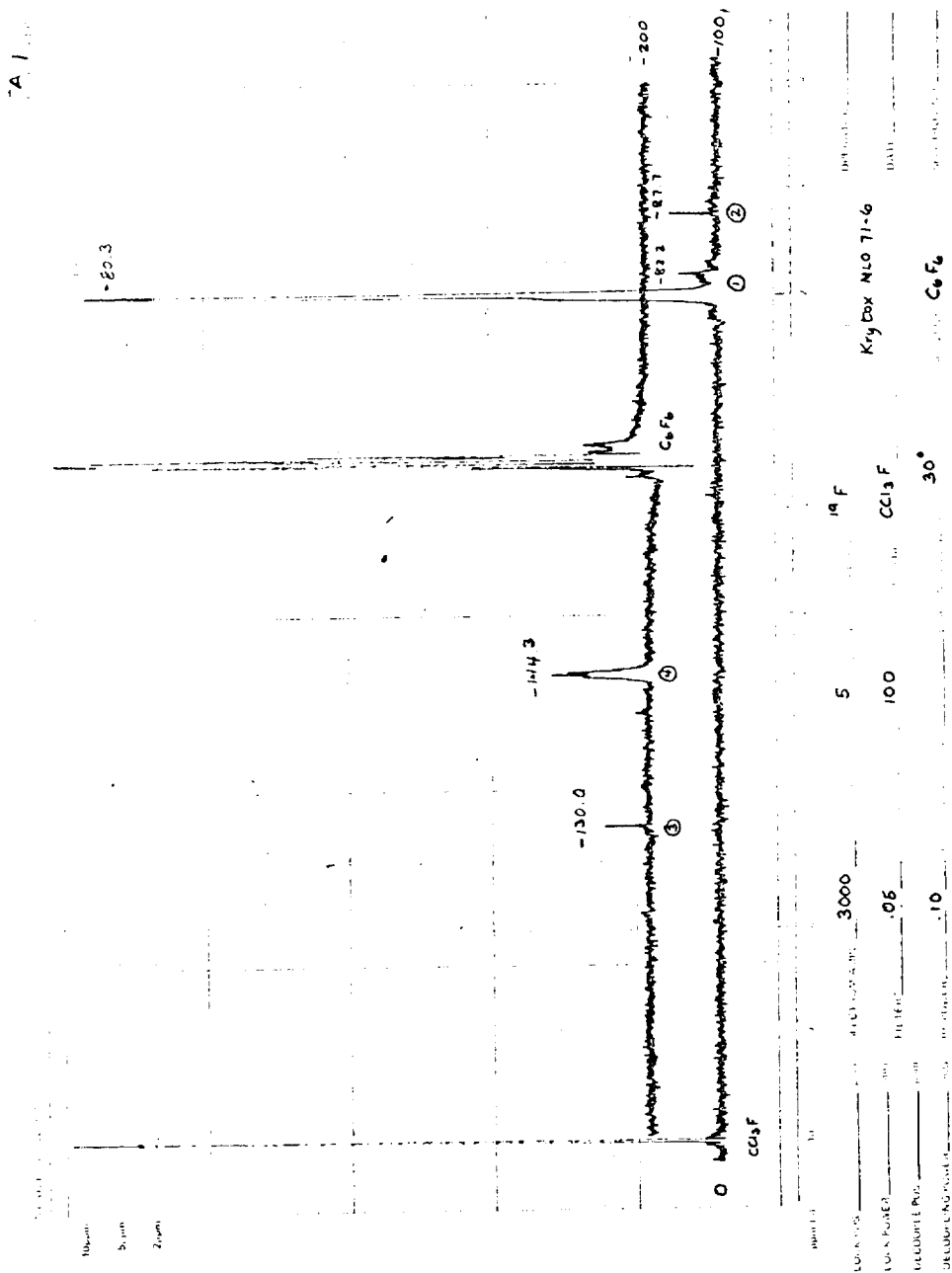


Figure 11: <sup>19</sup>F NMR spectrum of Krytox MLO-71-6 fluid (as received)

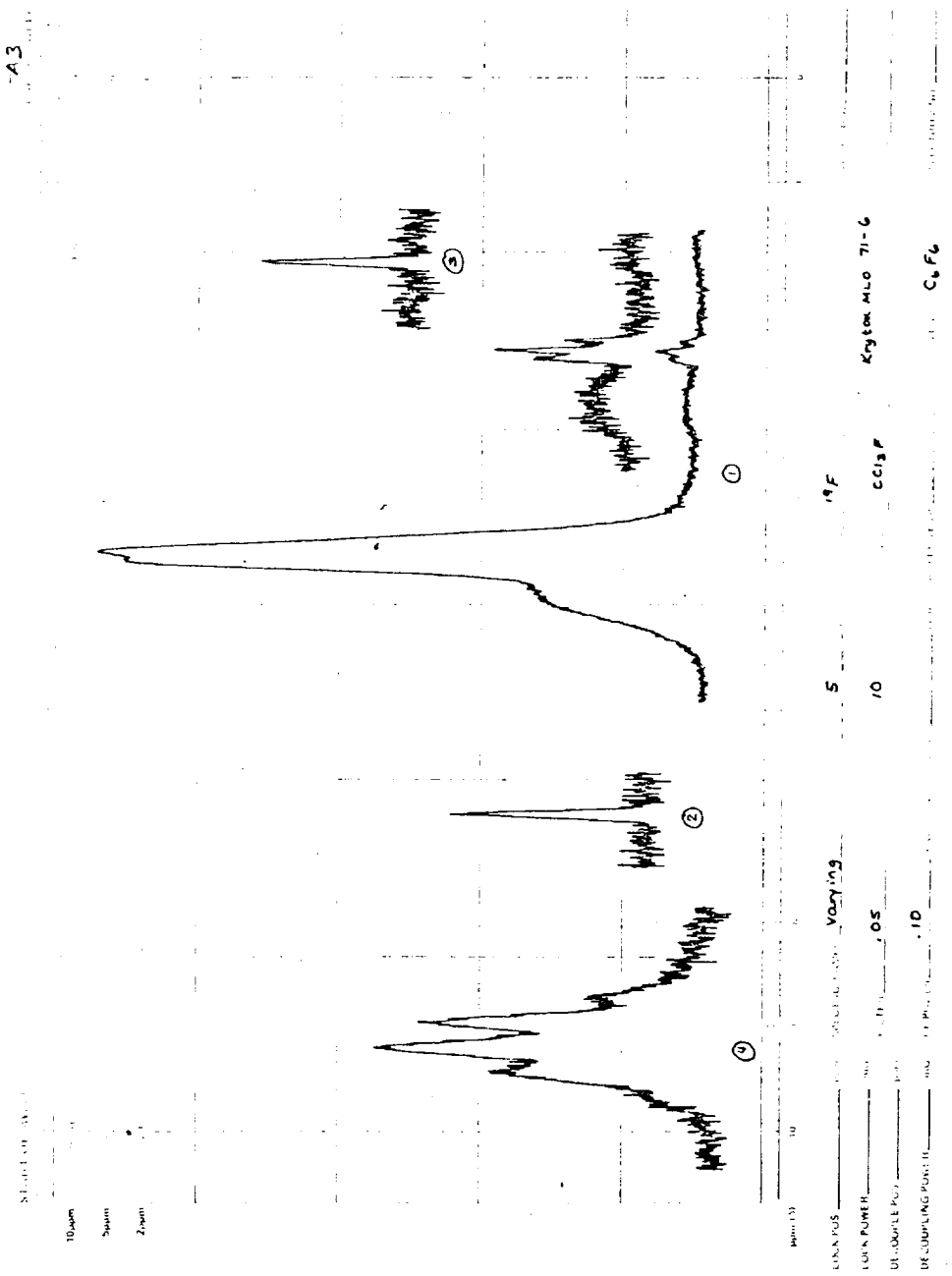


Figure 12: <sup>19</sup>F NMR spectrum of Krytox MLO-71-6 fluid, expanded to 10 ppm sweep

A4

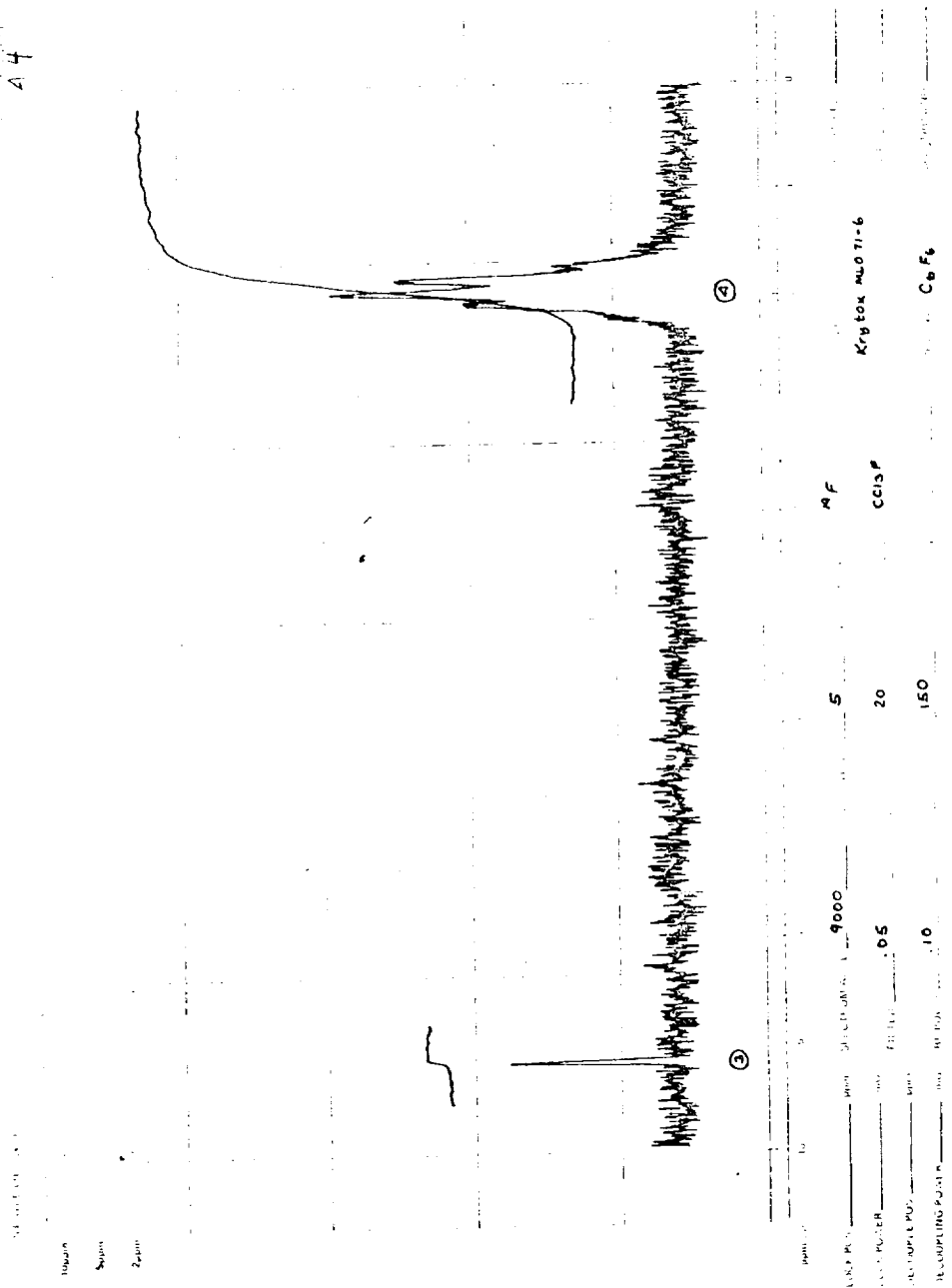


Figure 13: Portion of <sup>19</sup>F NMR spectrum of Krytox MLO-71-6 fluid, expanded to 20 ppm

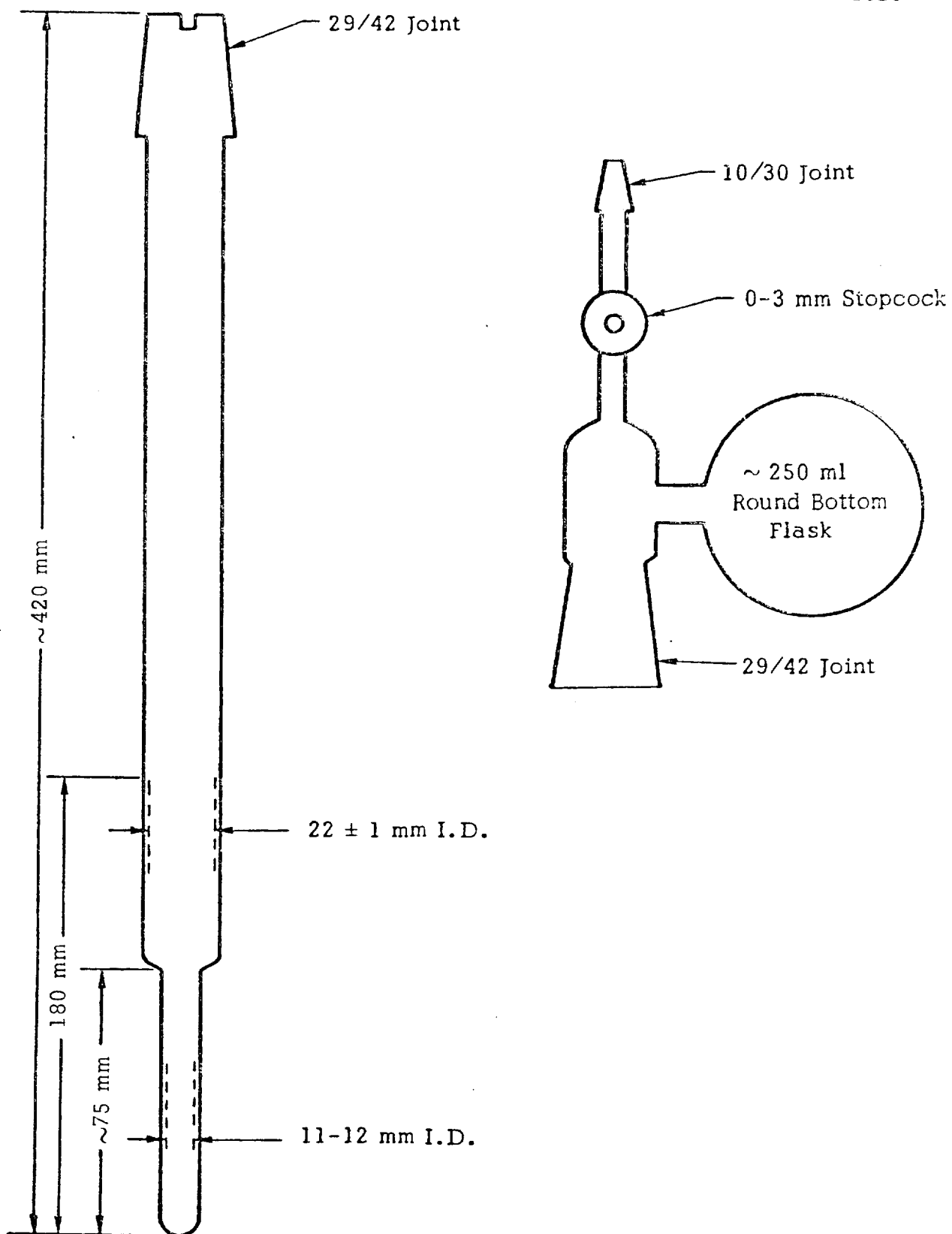


Figure 14: Decomposition tube and adapter

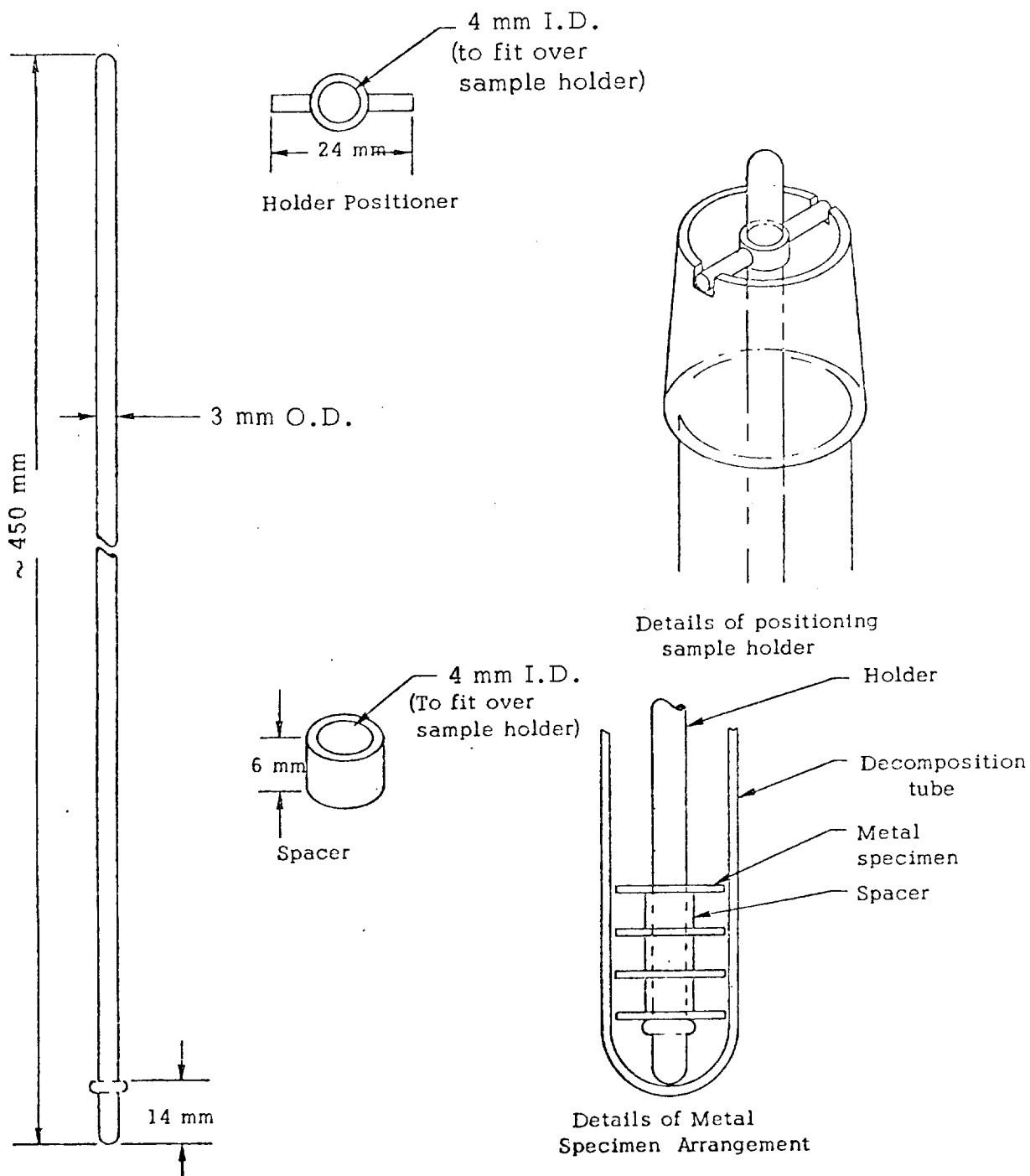


Figure 15: Metal specimen holder arrangement

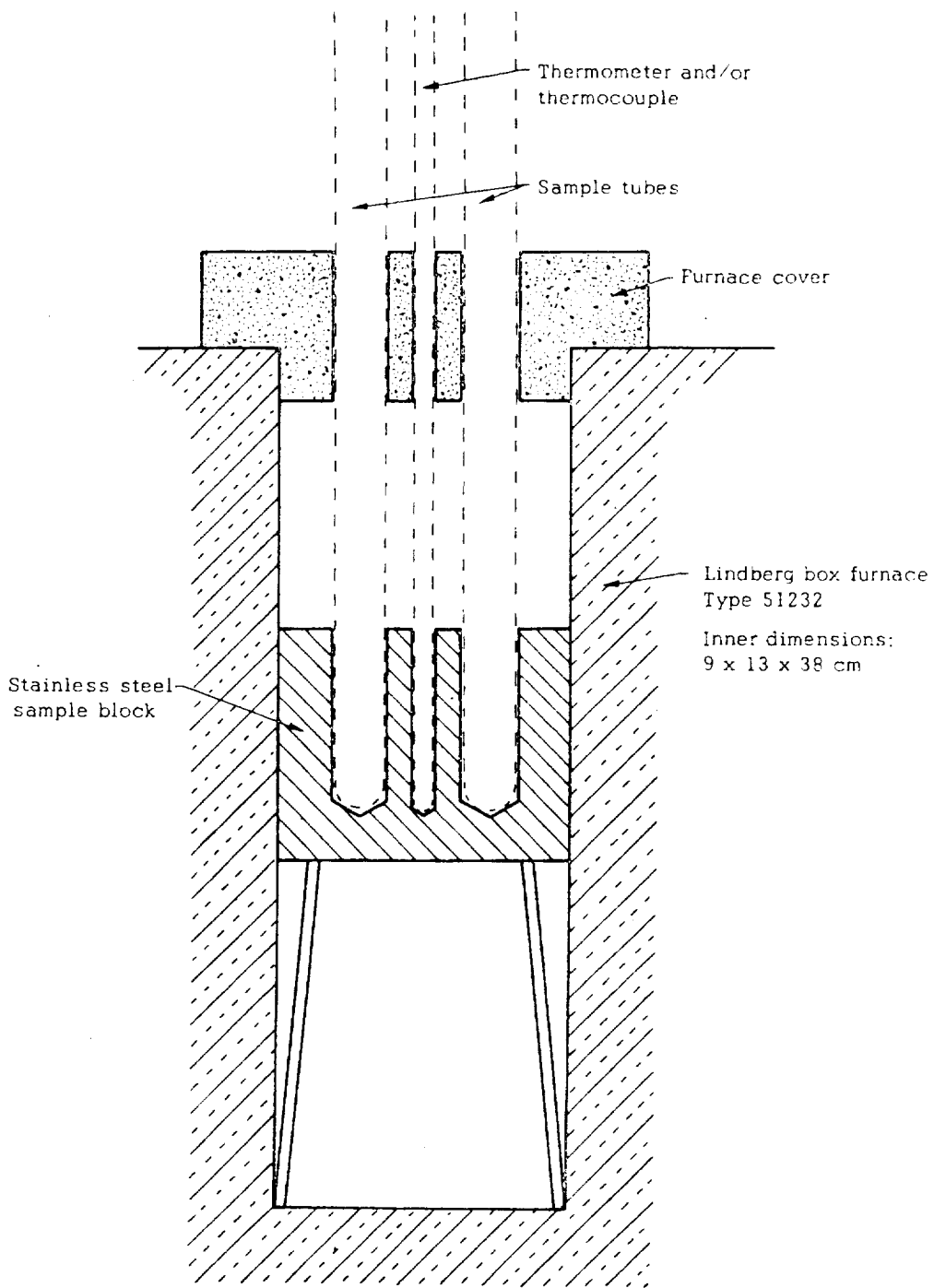


Figure 16: Box furnace arrangement