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# Thermo Dynamic Analysis on MHD Casson Nano-Fluid Flow in a Vertical Porous Space with Stretching Walls

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# Thermo Dynamic Analysis on MHD Casson Nano-Fluid Flow in a Vertical Porous Space with Stretching Walls

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## I. INTRODUCTION

The problem of mixed convective flow in vertical channels with different wall temperatures has a number of important engineering applications such as microelectronic components cooling, in the design of compact heat exchangers, industrial furnaces, power engineering and so on. Also, convection flows with heat and mass transfer under the influence of a magnetic field, chemical reaction occurs in many branches of engineering applications and transport processes in industrial applications such as chemical industry, power and cooling industry for drying, chemical vapour deposition on surfaces, cooling of nuclear reactors and MHD power generators (See Refs. [1-10]). Moreover, MHD channel flows gained significant theoretical and practical importance owing to their applications in MHD generators, accelerators and blood flow measurements. In view of these applications, Srinivas et al. [7] have studied the effects of thermal-diffusion and diffusion-thermo effects in a two-dimensional viscous flow between slowly expanding or contracting walls with weak permeability.

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The effect of chemical reaction and thermal radiation on MHD flow over an inclined permeable stretching surface with non-uniform heat source was examined by Srinivas et al. [8]. Later, Muthuraj et al. [9] discussed the combined effects of thermal-diffusion and diffusion-thermo with space porosity on MHD mixed convective flow of micropolar fluid in a vertical channel. Immaculate et al. [10] have investigated the influence of thermophoretic particle deposition on fully developed MHD mixed convective flow in a vertical channel with thermal-diffusion and diffusion-thermo effects. More recently, effects of thermal diffusion and diffusion thermo on MHD Couette flow of Powell-Eyring fluid in an inclined porous space in the presence of chemical reaction was investigated by Muthuraj et al. [11].

In engineering applications, the flows of non-Newtonian fluid have been attracting researchers significantly during the past few decades. In particular, it occurs in the extrusion of polymer fluids, cooling of metallic plate in the bath, exotic lubricants, artificial gels, natural gels, colloidal and suspension solutions. The most important among these fluids is the Casson fluid. It can be defined as a shear thinning liquid which is assumed to have an infinite viscosity at zero rate of shear, a yield stress below which no flow occurs and a zero viscosity at an infinite rate of shear. Human blood can also be treated as a Casson fluid due to the blood cells' chain structure and the substances contained like protein, fibrinogen, rouleaux etc [16]. Hence the Casson fluid has its own importance in scientific as well as in engineering areas. Many researchers have used the Casson fluid model for mathematical modeling of blood flow in narrow arteries at low shear rates (See Refs.[12-18]). Nadeem et al. [15] examined MHD flow of a Casson fluid over an exponentially shrinking sheet. Sarojamma et al.[16] have investigated MHD Casson fluid flow with heat and mass transfer in a vertical channel with stretching walls. Arthur et al.[17] have analyzed of Casson fluid flow over a vertical porous surface with chemical reaction in the presence of magnetic field. More recently, the unsteady MHD free flow of a Casson fluid past an oscillating vertical plate with constant wall temperature was analyzed by Khalid et al.[18].

Nanoparticle research is currently an area of intense scientific interest due to a wide variety of potential applications in biomedical, optical and electronic fields. It is a microscopic particle with at least one dimension less than 100 nm. Many existing studies indicate that an enormous enhancement in the emission intensity, quantum yield, and lifetime of the molecular rectangles has been observed when the solvent medium is changed from organic to aqueous and it clearly exhibit enhanced thermal conductivity, which goes up with increasing volumetric fraction of nanoparticles[19-28]. The model of nanofluid was first developed by Choi [19]. Later, fully developed mixed convection flow between two paralleled vertical flat plates filled by a nanofluid with the Buongiorno mathematical model using HAM was analyzed by Xu et al. [25]. Nadeem et al. [26] presented the steady stagnation point flow of a Casson nanofluid in the presence of convective boundary conditions. Khan et al. [27] analyzed the fully-developed two-layer Eyring–Powell fluid in a vertical channel divided into two equal regions. One region is filled with the clear Eyring–Powell fluid and the other with the Eyring–Powell nanofluid. The problem of MHD laminar free convection flow of nanofluid past a vertical surface was analyzed by Freidoonimehr [28]. More recently, Immaculate et al. [29] examined the MHD unsteady flow of Williamson nanofluid in a vertical channel filled with a porous material and oscillating wall temperature using HAM. To the best of our knowledge MHD Casson nanofluid in a vertical channel with stretching walls has not been studied before. In this paper, we therefore propose to analyze the steady fully-developed mixed convection flow of MHD Casson nanofluid in a vertical porous space with stretching walls in the presence of chemical reaction. It is important to note that this type of analysis has direct applications to the study of blood flow in the cardiovascular system subject to external magnetic field. The reduced non-dimensional, highly non-linear,

coupled system of equations is solved by HAM [30-35]. The influence of significant parameters on heat and mass transfer characteristics of the flow is presented through graphs and discussed.

## II. FORMULATION OF THE PROBLEM

We consider MHD Casson nanofluid flow in a vertical porous space bounded by two stretching walls and are maintained at different temperatures, concentrations. The channel walls are at the positions  $y = -L$  and  $y = L$ , as shown in Fig.1. A constant magnetic field of strength  $B_0$  is applied perpendicular to the channel walls. The fluids in the region of the parallel walls are incompressible, non-Newtonian and their transport properties are assumed to be constant.

The constitutive equation for the Casson fluid can be written as [16]

$$\tau_{ij} = \begin{cases} 2 \left[ \mu_B + \frac{\tau_y}{\sqrt{2\pi}} \right] e_{ij}, & \pi > \pi_c \\ 2 \left[ \mu_B + \frac{\tau_y}{\sqrt{2\pi_c}} \right] e_{ij}, & \pi < \pi_c \end{cases} \quad (1)$$

where  $\mu_B$  is the plastic dynamic viscosity of the non-Newtonian fluid,  $\tau_y$  is the yield stress of the fluid,  $\pi$  is the product of the component of deformation rate with itself, namely,  $\pi = e_{ij}e_{ij}$ , and  $e_{ij}$  is the (i, j) th component of deformation rate, and  $\pi_c$  is critical value of this product based on non-Newtonian model. Under the above assumptions and usual Boussinesq approximation, the fluid flow is governed by the following equations (See Refs. [16, 25, 26])

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2)$$

$$\rho_f \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p}{\partial x} + \mu_f \left( 1 + \frac{1}{\beta} \right) \nabla^2 u - \sigma B_0^2 u - \frac{\mu_f \Phi^*}{k^*} u - \rho_f C_F u^2 + \rho_f g \beta_t (1 - C_0)(T - T_0) + g \beta_c (\rho_p - \rho_f)(C - C_0) \quad (3)$$

$$\rho_f \left( u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p}{\partial y} + \mu_f \left( 1 + \frac{1}{\beta} \right) \nabla^2 v - \frac{\mu_f \Phi^*}{k^*} v \quad (4)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha^* \nabla^2 T + \tau^* \left[ D_B \left( \frac{\partial C}{\partial x} \frac{\partial T}{\partial x} + \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} \right) + \frac{D_T}{T} \left\{ \left( \frac{\partial T}{\partial x} \right)^2 + \left( \frac{\partial T}{\partial y} \right)^2 \right\} \right] \quad (5)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D_B \nabla^2 C + \frac{D_T k_T}{T} \nabla^2 T - k_1 C \quad (6)$$

The boundary conditions of the problem are

$$u = bx, v = 0, T = T_1, C = C_1 \text{ at } y = -L \quad (7)$$

$$u = bx, v = 0, T = T_2, C = C_2 \text{ at } y = L \quad (8)$$

where  $u$  and  $v$  are the velocity components in  $x$  and  $y$  directions,  $T_1$  and  $T_2$  are the wall temperatures ( $T_2 > T_1$ ),  $C_1$  and  $C_2$  are the wall concentrations,  $\bar{T}$  is the mean value of  $T_1$  and  $T_2$ ,  $C_f$  is the inertial coefficient,  $C_p$  is the specific heat,  $B_0$  is the transverse magnetic field,  $D_B$  is the Brownian diffusion coefficient,  $D_T$  is the thermophoresis diffusion coefficient,  $g$  is the acceleration due to gravity,  $p$  is the pressure,  $T$  is the temperature,  $k^*$  is the permeability of the medium,  $K$  is the thermal conductivity of the fluid,  $\alpha^* = \frac{K}{(\rho C_p)_f}$  is the thermal

diffusivity of the fluid,  $\tau^* = \frac{(\rho C_p)_p}{(\rho C_p)_f}$ ,  $b > 0$  is the stretch

of the channel walls, respectively,  $\beta = \frac{\mu_B \sqrt{2\pi_c}}{\tau_y}$  is the

Casson parameter,  $\rho_f, \rho_p$  densities of the base fluid and nanoparticle, respectively,  $(\rho C_p)_f$  is the heat capacity of the fluid,  $(\rho C_p)_p$  gives the effective heat capacity of the nanoparticle material,  $\nu$  is the kinematic viscosity,  $\phi^*$  is the porosity of the medium,  $\mu_f$  is the dynamic viscosity of the fluid,  $\sigma$  is the coefficient of electric conductivity,  $\beta_t$  is the coefficient of thermal expansion,  $\beta_c$  is the coefficient of expansion with concentration and  $\nabla^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2}$ .

We introduce the similarity variables

$$u = bxf'(\eta); v = -Lbf(\eta); \eta = \frac{y}{L}; \theta = \frac{T - T_1}{T_2 - T_1}; \phi = \frac{C - C_1}{C_2 - C_1} \quad (9)$$

Invoking the above similarity variables to equations (3)-(6) and eliminating pressure gradient, we get

$$\left(1 + \frac{1}{\beta}\right) f^{iv} - R_e (f'f'' - ff''') - Hf'' - Iff'' + G_r\theta' + G_c\phi' = 0 \quad (10)$$

$$\theta'' + P_r [N_b\phi'\theta' + N_t(\theta')^2 + R_e f\theta'] = 0 \quad (11)$$

$$\phi'' + \frac{N_t}{N_b}\theta'' + L_e (R_e f\phi' - \gamma\phi + k_1^*) = 0 \quad (12)$$

The corresponding boundary conditions are:

$$f' = 1, f = 0, \theta = 0, \phi = 0 \text{ at } \eta = -1 \quad (13)$$

$$f' = 1, f = 0, \theta = 1, \phi = 1 \text{ at } \eta = 1 \quad (14)$$

Where  $H = M + \frac{1}{D_a}$ ,  $k_1^* = \frac{-k_1 C_1 L^2}{\nu_f (C_2 - C_1)}$ ,  $I = \frac{2C_f b x L^2}{\nu_f}$  is the inertia coefficient,

$R_e = \frac{L^2 b}{\nu_f}$  is the Reynolds number,  $M = \sqrt{\frac{\sigma B_0^2 L^2}{\mu_f}}$  is the Hartmann number,

$D_a = \frac{k^*}{\phi^* L^2}$  is the permeability parameter,

$N_b = \frac{\tau^* D_B (C_2 - C_1)}{v_f}$  is the Brownian motion

$G_r = \frac{g\beta_t(1-C_0)(T_2-T_1)L^2}{v_f b x}$  local temperature

parameter  $N_t = \frac{\tau^* D_T (T_2 - T_1)}{\bar{T} v_f}$  is the thermophoresis

Grashof number,  $G_c = \frac{g\beta_c(\rho_p - \rho_f)(C_2 - C_1)L^2}{\mu_f b x}$  is

parameter,  $\gamma = \frac{k_1 L^2}{v_f}$  is the chemical reaction parameter.

the local nano-particle Grashof number,  $P_r = \frac{v_f}{\alpha^*}$  is

The dimensionless volume flow rate  $\bar{Q}$  is given by

the Prandtl number,  $L_e = \frac{v_f}{D_B}$  is the Lewis number,

$$\bar{Q} = \int_{-1}^1 f' d\eta. \quad (15)$$

The skin friction coefficient, local heat rate transfer and the local mass diffusion rate at the walls are defined as

$$C_f = \frac{L\tau_w}{\mu_f b x}; \quad Nu = \frac{Lq_w}{K(T_2 - T_1)}; \quad Sh = \frac{Lm_w}{D_B(C_2 - C_1)}$$

$$\text{where } \tau_w = \mu_f \left(1 + \frac{1}{\beta}\right) \left(\frac{\partial u}{\partial y}\right); \quad q_w = -K \left(\frac{\partial T}{\partial y}\right); \quad m_w = -D_B \left(\frac{\partial C}{\partial y}\right) \quad (16)$$

Its non-dimensional form is given by

$$C_f = \left(1 + \frac{1}{\beta}\right) f''(\eta) \Big|_{\eta=\pm 1}; \quad Nu = -\theta'(\eta) \Big|_{\eta=\pm 1}; \quad Sh = -\phi'(\eta) \Big|_{\eta=\pm 1} \quad (17)$$

### III. SOLUTION BY HOMOTOPY ANALYSIS METHOD (HAM)

For HAM solutions, we can choose the initial guesses and auxiliary linear operators in the following form:

$$f_0(\eta) = \frac{\eta^3 - \eta}{2}; \quad \theta_0(\eta) = \frac{1 + \eta}{2}; \quad \phi_0(\eta) = \frac{1 + \eta}{2} \quad (18)$$

$$L_1(f) = f^{iv} \quad L_2(\theta) = \theta'' \quad L_3(\phi) = \phi'' \quad (19)$$

$$(1 - \wp)L_1[\hat{f}(\eta, \wp) - f_0(\eta)] = \wp h N_1[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)] \quad \hat{f}(-1, \wp) = 0, \hat{f}(1, \wp) = 0 \quad (20)$$

$$(1 - \wp)L_2[\hat{\theta}(\eta, \wp) - \theta_0(\eta)] = \wp h N_2[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)], \quad \hat{\theta}(-1, \wp) = 0, \hat{\theta}(1, \wp) = 1 \quad (21)$$

$$(1 - \wp)L_3[\hat{\phi}(\eta, \wp) - \phi_0(\eta)] = \wp h N_3[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)], \quad \hat{\phi}(-1, \wp) = 0, \hat{\phi}(1, \wp) = 1 \quad (22)$$

where,

$$N_1[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)] =$$

$$\left(1 + \frac{1}{\beta}\right) f^{iv}(\eta, \wp) - R_e \left(\hat{f}'(\eta, \wp) \hat{f}''(\eta, \wp) - \hat{f}(\eta, \wp) \hat{f}'''(\eta, \wp)\right) - H \hat{f}''(\eta, \wp) - I \hat{f}'(\eta, \wp) \hat{f}''(\eta, \wp) + G_r \hat{\theta}'(\eta, \wp) + G_c \hat{\phi}'(\eta, \wp)$$

$$\mathbf{N}_2[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)] = \hat{\theta}''(\eta, \wp) + P_r[N_b \hat{\phi}'(\eta, \wp) \hat{\theta}'(\eta, \wp) + N_t (\hat{\theta}'(\eta, \wp))^2 + R_e \hat{f}(\eta, \wp) \hat{\theta}'(\eta, \wp)]$$

$$\mathbf{N}_3[\hat{f}(\eta, \wp), \hat{\theta}(\eta, \wp), \hat{\phi}(\eta, \wp)] = \hat{\phi}''(\eta, \wp) + \frac{N_t}{N_b} \hat{\theta}''(\eta, \wp) + L_e (R_e \hat{f}(\eta, \wp) \hat{\phi}'(\eta, \wp) - \gamma \hat{\phi}(\eta, \wp) + k_1^*)$$

For  $\wp = 0$  and  $\wp = 1$ , we have

$$\hat{f}(\eta, 0) = f_0(\eta) \quad \hat{f}(\eta, 1) = f(\eta) \quad (23)$$

$$\hat{\theta}(\eta, 0) = \theta_0(\eta) \quad \hat{\theta}(\eta, 1) = \theta(\eta) \quad (24)$$

$$\hat{\phi}(\eta, 0) = \phi_0(\eta) \quad \hat{\phi}(\eta, 1) = \phi(\eta) \quad (25)$$

when  $\wp$  increases from 0 to 1, then  $\hat{f}(\eta, \wp)$ ,  $\hat{\theta}(\eta, \wp)$ ,  $\hat{\phi}(\eta, \wp)$  vary from initial guess  $f_0(\eta)$ ,  $\theta_0(\eta)$ ,

$\phi_0(\eta)$  to the approximate analytical solution  $f(\eta)$ ,  $\theta(\eta)$ ,  $\phi(\eta)$ . By Taylor's theorem the series  $\hat{f}(\eta, \wp)$ ,  $\hat{\theta}(\eta, \wp)$ ,  $\hat{\phi}(\eta, \wp)$  can be expressed as a power series of  $\wp$  as follows,

$$\hat{f}(\eta, \wp) = f_0(\eta) + \sum_{m=1}^{\infty} f_m(\eta) \wp^m, \quad f_m(\eta) = \frac{1}{m!} \left. \frac{\partial^m \hat{f}(\eta, \wp)}{\partial \wp^m} \right|_{\wp=0} \quad (26)$$

$$\hat{\theta}(\eta, \wp) = \theta_0(\eta) + \sum_{m=1}^{\infty} \theta_m(\eta) \wp^m, \quad \theta_m(\eta) = \frac{1}{m!} \left. \frac{\partial^m \hat{\theta}(\eta, \wp)}{\partial \wp^m} \right|_{\wp=0} \quad (27)$$

$$\hat{\phi}(\eta, \wp) = \phi_0(\eta) + \sum_{m=1}^{\infty} \phi_m(\eta) \wp^m, \quad \phi_m(\eta) = \frac{1}{m!} \left. \frac{\partial^m \hat{\phi}(\eta, \wp)}{\partial \wp^m} \right|_{\wp=0} \quad (28)$$

In which 'h' is chosen in such a way that these series are convergent at  $\wp = 1$ , therefore we have

$$f(\eta) = f_0(\eta) + \sum_{m=1}^{\infty} f_m(\eta), \quad \theta(\eta) = \theta_0(\eta) + \sum_{m=1}^{\infty} \theta_m(\eta), \quad \phi(\eta) = \phi_0(\eta) + \sum_{m=1}^{\infty} \phi_m(\eta) \quad (29)$$

b) *The m-th order deformation equations*

Differentiating the zero-order deformation Eqns. (20) - (22)  $m$ -times with respect to  $\wp$  and then dividing them by  $m!$  and finally setting  $\wp = 0$ , we obtain the following  $m$ -th order deformation equations:

$$L_1[f_m(\eta) - \chi_m f_{m-1}(\eta)] = hR_m^f(\eta) \quad (30)$$

$$L_2[\theta_m(\eta) - \chi_m \theta_{m-1}(\eta)] = hR_m^\theta(\eta) \quad (31)$$

where,

$$R_m^f(\eta) = \left(1 + \frac{1}{\beta}\right) f_{m-1}^{iv} - R_e \sum_{k=0}^{m-1} (f_{m-k-1}' f_k'' - f_{m-k-1} f_k''') - H f_{m-1}'' - I \sum_{k=0}^{m-1} f_{m-k-1}' f_k'' + G_r \theta_{m-1}' + G_c \phi_{m-1}'$$

$$R_m^\theta(\eta) = \theta_{m-1}'' + P_r \left( \sum_{k=0}^{m-1} [N_b \phi_{m-k-1}' \theta_k' + N_t \theta_{m-k-1}' \phi_k'] + R_e f_{m-k-1}' \theta_k' \right)$$

$$L_3[\phi_m(\eta) - \chi_m \phi_{m-1}(\eta)] = hR_m^\phi(\eta) \quad (32)$$

together with condition

$$f_m(-1) = 0 \quad f_m(1) = 0 \quad (33)$$

$$\theta_m(-1) = 0 \quad \theta_m(1) = 0 \quad (34)$$

$$\phi_m(-1) = 0 \quad \phi_m(1) = 0 \quad (35)$$

$$R_m^\phi(\eta) = \phi_{m-1}'' + \frac{N_t}{N_b} \theta_{m-1}'' + L_e \left( R_e \sum_{k=0}^{m-1} f_{m-k-1} \phi_k' - \gamma \phi_{m-1} + k_1^* (1 - \chi_m) \right)$$

where,

$$\chi_m = \begin{cases} 0 & \text{for } m = 1 \\ 1 & \text{for } m \neq 1 \end{cases}$$

where  $E_1, E_2$  and  $E_3$  are the residual error at  $m$ -th order of HAM approximation for  $f, \theta$  and  $\phi$  respectively. The average square residual error is given by:

$$\Delta_m = \frac{1}{3} \sum_{i=1}^3 \int_{\eta=-1}^{\eta=1} E_i^2 d\eta \quad (39)$$

#### IV. CONVERGENCE AND THE RESIDUAL ERROR

The convergence and rate of approximation for the HAM solution depends on auxiliary parameter 'h' (See Refs. [29-34]), for this purpose, we have plotted h-curves in Fig.2 with fixing the values of involved parameters  $G_r = 5, G_c = 5, R_e = 1, l = 1, N_t = 0.45, N_b = 0.45, L_e = 10, M = 2, P_r = 2.5, D_a = 0.5, K_1 = 1, \gamma = 0.5, \beta = 0.6$ . As a result, we can choose proper value of 'h' and also we obtain the optimal values of the auxiliary parameter 'h' by minimizing the average square residual error for the equations (10) to (12). We define the residual error for above mentioned equations as:

$$E_1 = \left( 1 + \frac{1}{\beta} \right) f^{iv} - R_e (f'f'' - ff''') - Hf'' - I f'f'' + G_r \theta' + G_c \phi' \quad (36)$$

$$E_2 = \theta'' + P_r [N_b \phi' \theta' + N_t (\theta')^2 + R_e f \theta'] \quad (37)$$

$$E_3 = \phi'' + \frac{N_t}{N_b} \theta'' + L_e (R_e f \phi' - \gamma \phi + k_1^*) \quad (38)$$

Further, we have tabulated the minimum average square residual errors for 10<sup>th</sup>, 15<sup>th</sup>, 20<sup>th</sup>, 25<sup>th</sup> order of HAM approximation for different values of parameters with optimal 'h' in Table 1. It is noted that the number of HAM approximation increases the corresponding minimum square residual error decreases significantly and hence it leads to more accurate solutions. Further, it is important to note that our present HAM solution is good agreement with Numerical solution which is obtained by NDSolve scheme of Mathematica (See Fig.9).

*Table 1:* The average square residual error for the optimal value of 'h' for different order of approximations

Optimal h		$\Delta_m$			
		10 <sup>th</sup> order	15 <sup>th</sup> order	20 <sup>th</sup> order	25 <sup>th</sup> order
-0.50	$M = 5$	$4.48300 \times 10^{-1}$	$2.17722 \times 10^{-2}$	$8.560151 \times 10^{-3}$	$6.293116 \times 10^{-3}$
-0.46	$\beta = 0.4$	$9.61660 \times 10^{-1}$	$4.76619 \times 10^{-2}$	$1.085990 \times 10^{-2}$	$7.63834 \times 10^{-3}$
-0.28	$\gamma = 1.5$	$2.41549 \times 10^{-1}$	$6.41384 \times 10^{-2}$	$1.741480 \times 10^{-2}$	$7.771010 \times 10^{-3}$
-0.46	$P_r = 1$	$3.23985 \times 10^{-3}$	$8.82479 \times 10^{-4}$	$1.155850 \times 10^{-6}$	$1.230240 \times 10^{-8}$
-0.51	$N_t = 0.5$	$5.53236 \times 10^{-1}$	$2.67400 \times 10^{-2}$	$1.01741 \times 10^{-2}$	$6.737690 \times 10^{-3}$
-0.49	$N_b = 0.2$	$7.79008 \times 10^{-3}$	$7.15877 \times 10^{-3}$	$6.053300 \times 10^{-3}$	$6.032410 \times 10^{-3}$
-0.58	$L_e = 5$	$1.341560 \times 10^{-1}$	$1.15096 \times 10^{-2}$	$7.017850 \times 10^{-3}$	$6.73713 \times 10^{-3}$

#### V. RESULTS AND DISCUSSIONS

To study the behavior of solutions, numerical calculations for different values of magnetic parameter (M), Permeability parameter ( $D_a$ ), Casson fluid parameter ( $\beta$ ), thermophoresis parameter ( $N_t$ ),

Brownian motion parameter ( $N_b$ ), Lewis number ( $L_e$ ), Chemical reaction parameter ( $\gamma$ ) and Prandtl number ( $P_r$ ) have been carried out. Throughout the computations we employ  $G_r = 5, G_c = 5, R_e = 1, l = 1, N_t = 0.45, N_b = 0.45, L_e = 10, M = 2, P_r = 2.5,$

$D_a = 0.5$ ,  $K_1 = 1$ ,  $\gamma = 0.5$ ,  $\beta = 0.6$  unless otherwise stated. Fig. 3a is prepared to see the influence of the Casson fluid parameter with two different values of magnetic parameter 'M' with fixed values of all other parameters. It is observed that magnitude of velocity is a decreasing function with increasing Casson fluid parameter and also we noted that increasing 'M' is lead to decelerate the velocity. Physically it means that the application of transverse magnetic field produces a resistive type force (Lorentz force) similar to drag force which tends to resist the fluid flow and thus reducing its velocity (as noted in [18]). The effect of permeability parameter  $D_a$  on the velocity is displayed in Fig. 3b. It depicts that the effect of increasing the value of  $D_a$  is to increase the velocity, which means that the drag force is reduced by increasing the value of the permeability parameter. Fig. 3c illustrates the influence of thermophoresis parameter  $N_t$  on velocity. It shows that increasing  $N_t$  is not shown much influence on velocity distribution. The quite similar effect can be noticed by varying Brownian motion parameter  $N_b$  on the velocity (See Fig.3d).

Fig. 4a is graphed to see the effect of Lewis number on temperature distribution. It is seen that temperature field is an increasing function in the left half of the channel whereas the behavior is reversed in the other region. Fig. 4b describes that, increasing chemical reaction parameter gives opposite behavior that of Fig.4a. Fig. 4c is plotted to see the influence of Brownian motion parameter on temperature distribution. It is evident that increasing  $N_b$  is to increase the fluid temperature significantly. The similar effect can be noticed with increasing  $N_t$  and  $P_r$ , which are shown in Figs.4d and 4e. Physically speaking, increasing thermal parameters is to increase momentum diffusivity, which leads to enhance the fluid temperature. Further, it is noted that  $N_t$ ,  $P_r$  shows the significant influence on temperature field than other parameters. Fig. 5a shows the variation in concentration field with different values of Lewis number  $L_e$ . It depicts that increasing  $L_e$  lead to enhance species concentration significantly. Also, it is observed that when increasing  $L_e$  from 0 to 5 there is nearly 45% increase in concentration whereas increasing  $L_e$  from 5 to 10 there is only 20% (approx) decrease in the same, which means that low values of  $L_e$  dominates on concentration field. The opposite trend can be seen if  $L_e$  is replaced by chemical reaction parameter. (See Fig. 5b). Fig. 5c is prepared to

see the effect of  $N_b$  on concentration. It is observed that concentration enhances with an increase of  $N_b$  whereas increasing thermal parameters  $N_t$  and  $P_r$  leads to suppress the concentration gradually (See Figs. 5d and 5e).

The variation of pressure gradient  $\frac{dp}{dx}$  with M and  $G_r$  is plotted in Fig.6a. It is observed that increasing both the parameters lead to enhance the pressure gradient whereas in the absence of magnetic field pressure gradient is negative with increasing  $G_r$ , it means that high pressure gradient is need to promote the flow in the presence of magnetic field. The influence of inertia coefficient and material parameter on  $\frac{dp}{dx}$  is graphed in Fig. 6b. It illustrates that pressure gradient is decreasing function with increasing I and  $\beta$  whereas very high pressure gradient exist for lower value of material parameter ( $\beta < 0.5$ ). It indicates that more driving force is required for non-Newtonian fluid than Newtonian fluid. The variations on wall heat transfer rate (Nu) and wall mass transfer rate (Sh) with different values of  $N_b$ ,  $N_t$ ,  $L_e$  and  $\gamma$  are presented in Figs. 7 and 8 respectively. Influence of  $N_b$  and  $N_t$  on 'Nu' at both the walls is displayed in Fig 7. At the wall  $\eta = -1$ , 'Nu' is a decreasing function with increasing  $N_b$ ,  $N_t$  whereas at the other wall there is no much influence with increasing  $N_b$ . Also, a sharp increment occurs in 'Nu' with increasing  $N_t$ . Variation on 'Sh' with different values of  $L_e$  and  $\gamma$  at both the walls is displayed in Fig 8. It depicts that, 'Sh' is a decreasing function with increasing  $L_e$  while increasing  $\gamma$  is not shown much influence at the wall  $\eta = -1$ . At the other wall, the opposite trend is noticed with increasing  $L_e$ .

## VI. CONCLUSIONS

This article looks at flow, heat and mass transfer characteristics of a MHD Casson nanofluid in a vertical porous space with stretching walls in the presence of chemical reaction. HAM is adopted to obtain analytical solutions of the reduced set of ordinary differential equations. The results are presented through graphs for various values of the pertinent parameters and the salient features of the solutions are discussed graphically. This type of investigations is very important for mathematical modeling of blood flow in narrow arteries at low shear



rates. It is found that magnitude of velocity is a decreasing function with the Casson fluid parameter and Hartmann number whereas increasing permeability parameter  $D_a$ . Increasing  $N_b$ ,  $N_t$  and  $P_r$  are tends to promote the fluid temperature significantly. Concentration field significantly enhances

with increasing  $L_e$  while increasing  $N_t$  and  $P_r$  suppresses the fluid concentration. Nusselt number distribution is a decreasing function with increasing  $N_b$ ,  $N_t$  at the wall  $\eta = -1$  while the parameter  $N_t$  tends to enhance at the other wall  $\eta = 1$ .

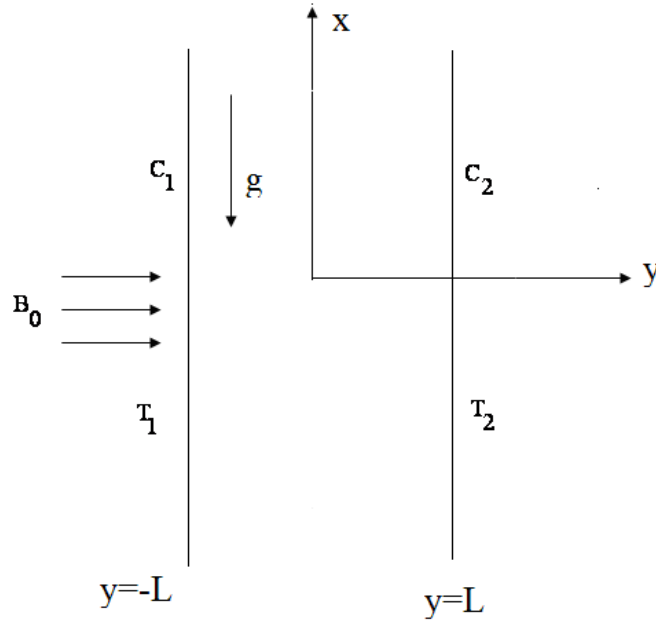
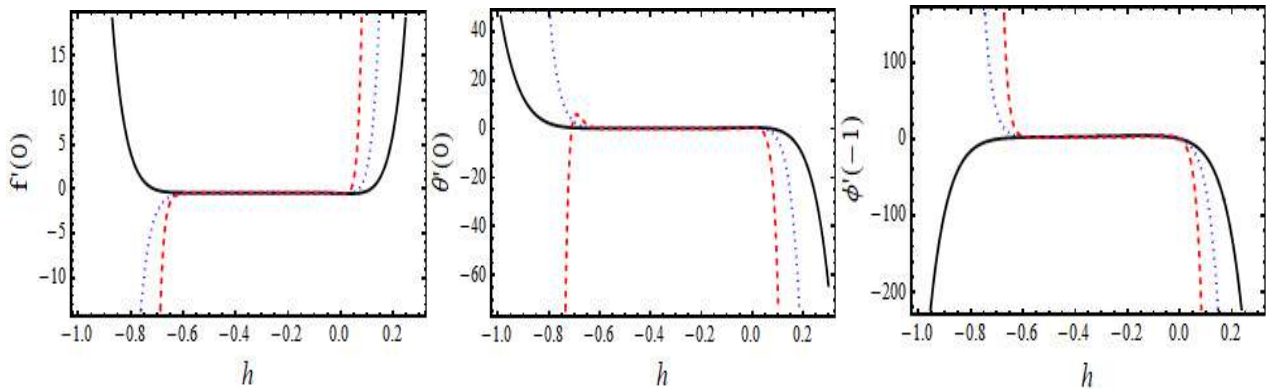
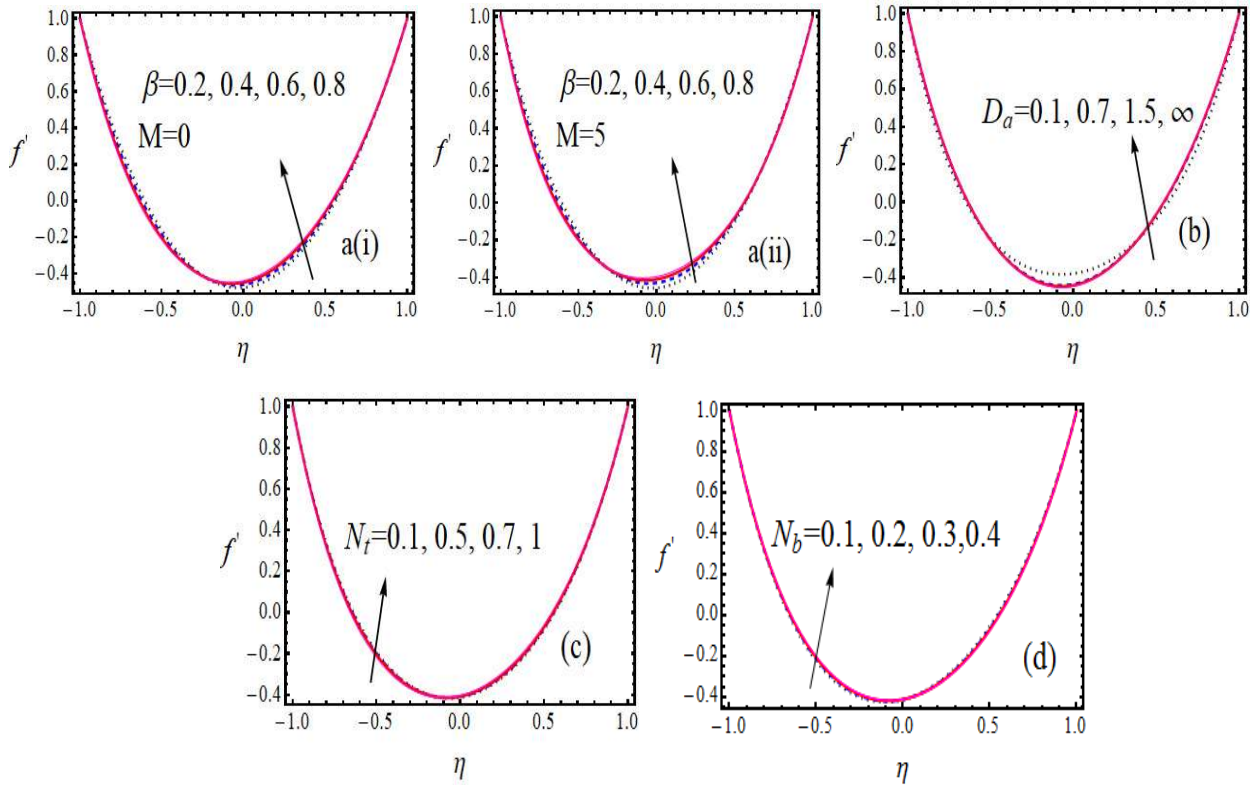


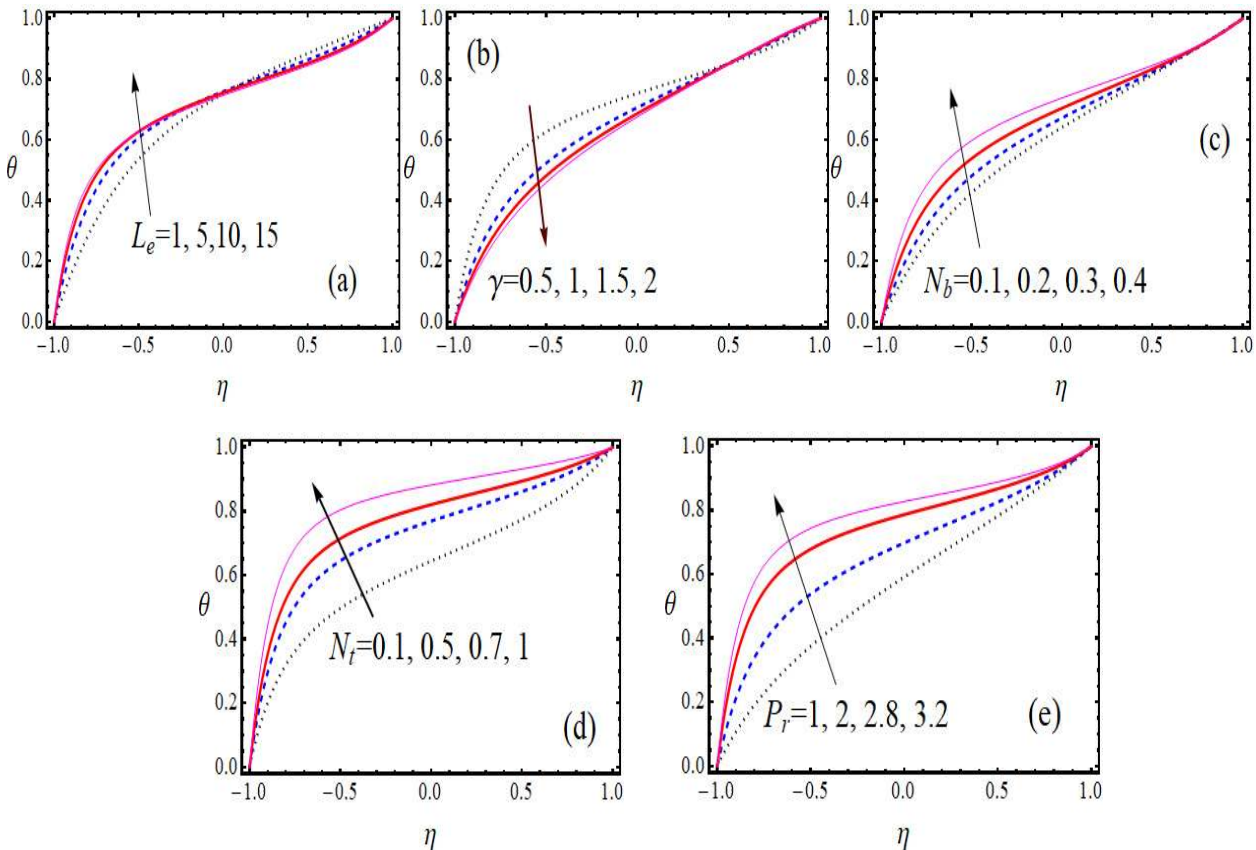
Fig. 1: Schematic diagram of the problem



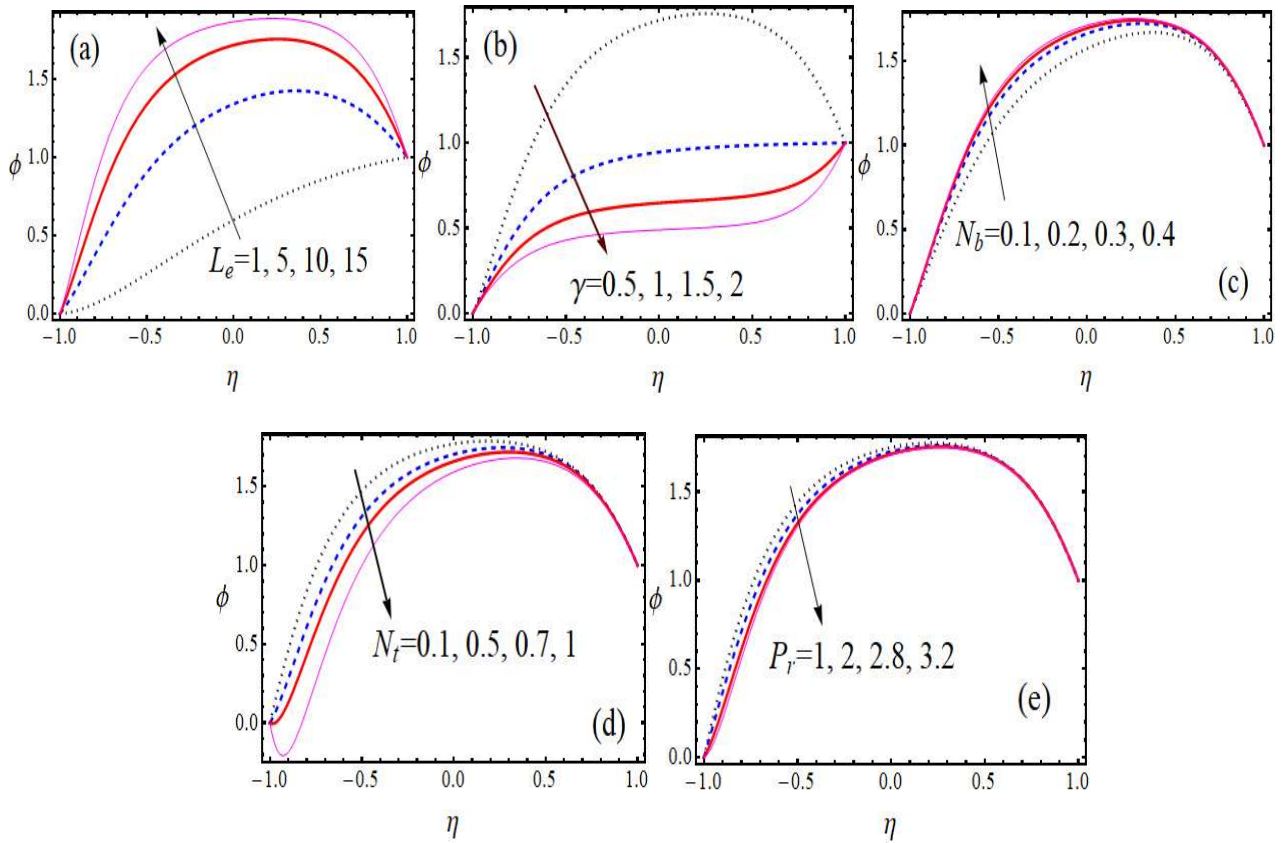
2: h-curves for velocity, temperature and concentration distribution (— 10<sup>th</sup>, .... 15<sup>th</sup>, - - - 25<sup>th</sup> orders of approximation)



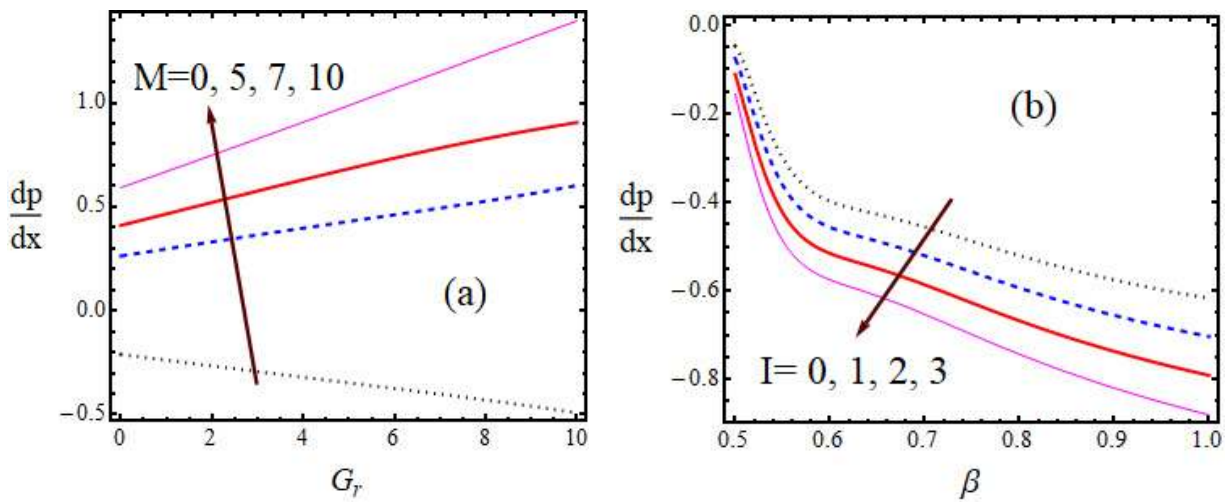
3: Effects of  $M$ ,  $\beta$ ,  $D_a$ ,  $N_t$  and  $N_b$  on Velocity distribution



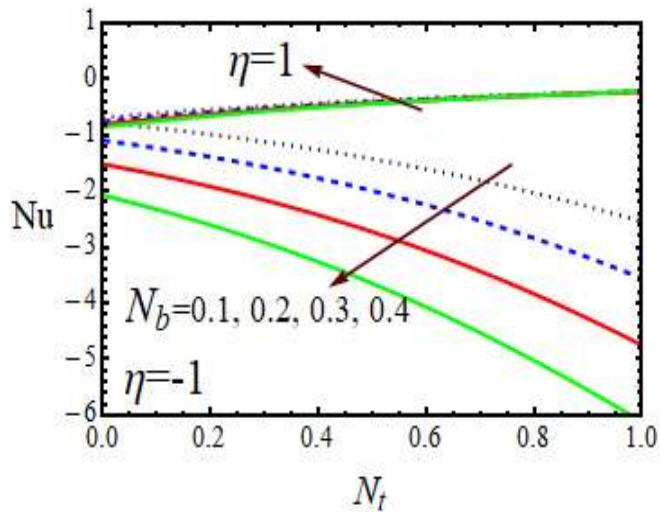
4: Effects of  $L_e$ ,  $\gamma$ ,  $N_b$ ,  $N_t$  and  $P_r$  on Temperature distribution



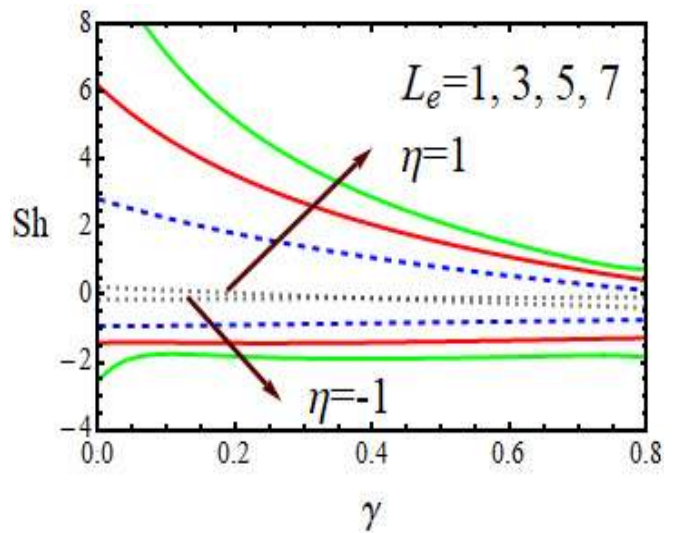
Effects of  $L_e$ ,  $\gamma$ ,  $N_b$ ,  $N_t$  and  $P_r$  on Concentration distribution



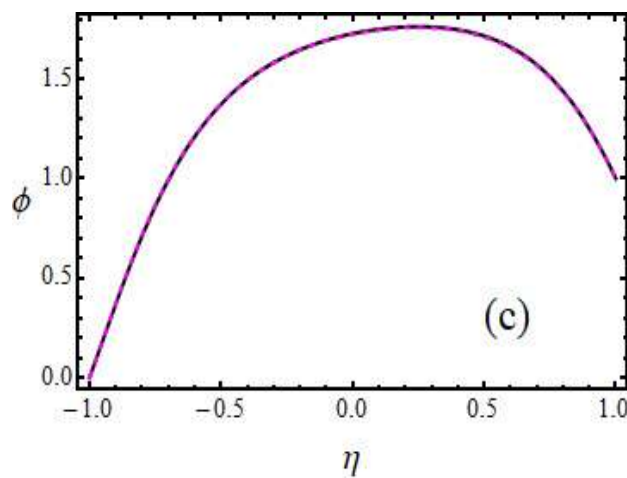
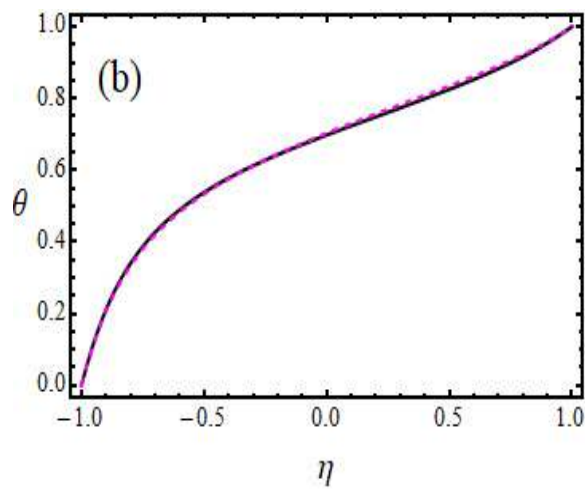
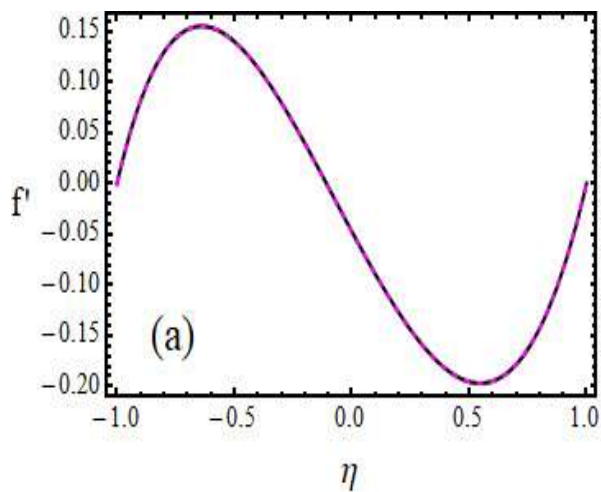
6: Effects of  $M$  and  $I$  on Pressure gradient distribution



7: Effect of  $N_t$  on Nusselt number distribution



8: Effect of  $\gamma$  on Sherwood number distribution



9: Comparison between \_\_\_\_HAM Solution and ----Numerical Solution

( $G_r = 5$ ,  $G_c = 5$ ,  $R_e = 1$ ,  $l = 1$ ,  $N_t = 0.45$ ,  $N_b = 0.45$ ,  $M = 2$ ,  
 $P_r = 2$ ,  $D_a = 0.5$ ,  $K_1 = 1$ ,  $\gamma = 0.5$ ,  $\beta = 0.6$ )



**NOMENCLATURE**

$B_0$  Transverse magnetic field  
 $b > 0$  Stretch of the channel walls(m)  
 $C$  Dimensional concentration(  $Kg / m^3$  )  
 $C_1, C_2$  Wall concentrations (  $Kg / m^3$  )  
 $C_0$  Initial concentration (  $Kg / m^3$  )  
 $C_F$  Inertial coefficient  
 $C_p$  Specific heat  
 $D_a$  Permeability parameter  
 $D_B$  Brownian diffusion coefficient (  $m^2 / s$  )  
 $D_T$  Thermophoresis diffusion coefficient (  $m^2 / s$  )  
 $e_{ij}$  (i, j)<sup>th</sup> component of deformation rate  
 $f$  Dimensionless stream function  
 $f'$  Dimensionless velocity  
 $g$  Acceleration due to gravity(  $m / sec^2$  )  
 $G_r$  Local temperature Grashof number  
 $G_c$  Local nano-particle Grashof number  
 $I$  Inertia coefficient  
 $k^*$  Permeability of the medium(  $m^2$  )  
 $K$  Thermal conductivity of the fluid (  $W / m K$  )  
 $L_e$  Lewis number  
 $M$  Hartmann number  
 $N_b$  Brownian motion parameter  
 $N_t$  Thermophoresis parameter  
 $p$  Pressure(  $N / m^2$  )  
 $P_r$  Prandtl number  
 $Re$  Reynolds number  
 $T$  Dimensional temperature  
 $T_1, T_2$  Wall temperatures (K)  
 $\bar{T}$  Mean value of  $T_1$  and  $T_2$  (K)  
 $T_0$  Inlet temperature (K)  
 $u, v$  Dimensional velocity components in x and y directions (m/s)

**Greek Symbols**

$\alpha^*$  Thermal diffusivity of the fluid (  $m / s^2$  )  
 $\beta$  Casson parameter  
 $\theta$  Dimensionless temperature  
 $\beta_t$  Coefficient of thermal expansion(  $K^{-1}$  )

$\beta_c$  Coefficient of expansion with concentration(  $K^{-1}$  )  
 $\mu_B$  Plastic dynamic viscosity of the non-Newtonian fluid (  $N s / m^2$  )  
 $\mu_f$  Dynamic viscosity of the fluid (  $N sec / m^2$  )  
 $\gamma$  Chemical reaction parameter  
 $\nu$  Kinematic viscosity(  $m^2 / sec$  )  
 $\rho_f, \rho_p$  Densities of the base fluid and nano-particle (  $Kg / m^3$  )  
 $(\rho C_p)_f$  Heat capacity of the fluid(J/K)  
 $(\rho C_p)_p$  Effective heat capacity of the nanoparticle Material (J/K)  
 $\phi^*$  Porosity of the medium  
 $\phi$  Dimensionless fluid concentration  
 $\sigma$  Coefficient of electric conductivity(S/m)  
 $\tau_y$  Yield stress of the fluid (  $N / m^2$  )  
 $\pi$  Product of the component of deformation rate

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