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Transformation of Hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX) by Permanganate

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Abstract

The chemical oxidant permanganate (MnO_4^-) has been shown to effectively transform hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX) at both the laboratory and field scales. We treated RDX with MnO_4^- with the objective of quantifying the effects of pH and temperature on destruction kinetics and determining reaction rates. A nitrogen mass balance and the distribution of reaction products were used to provide insight into reaction mechanisms. Kinetic experiments (at pH ~7, 25 °C) verified that RDX– MnO_4^- reaction was first-order with respect to MnO_4^- and initial RDX concentration (second-order rate: $4.2 \times 10^{-5} \text{ M}^{-1} \text{ s}^{-1}$). Batch experiments showed that choice of quenching agents (MnSO_4 , MnCO_3 , and H_2O_2) influenced sample pH and product distribution. When MnCO_3 was used as a quenching agent, the pH of the RDX– MnO_4^- solution was relatively unchanged and N_2O and NO_3^- constituted 94% of the N-containing products after 80% of the RDX was transformed. On the basis of the preponderance of N_2O produced under neutral pH (molar ratio $\text{N}_2\text{O}/\text{NO}_3^- \sim 5:1$), no strong pH effect on RDX– MnO_4^- reaction rates, a lower activation energy than the hydrolysis pathway, and previous literature on MnO_4^- oxidation of amines, we propose that RDX– MnO_4^- reaction involves direct oxidation of the methylene group (hydride abstraction), followed by hydrolysis of the resulting imides, and decarboxylation of the resulting carboxylic acids to form N_2O , CO_2 , and H_2O .

Introduction

Hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX) is a common groundwater contaminant at numerous military sites where munitions were either formulated, manufactured, or used in military exercises. Permanganate (MnO_4^-) is an oxidant commonly used with *in situ* chemical oxidation (ISCO) and has been widely accepted for treating chlorinated ethenes. Past research has shown that MnO_4^- preferentially attacks compounds with carbon–carbon double bonds, aldehyde groups, or hydroxyl groups and is attracted to the electron-rich region of chlorinated alkenes.(1) Although RDX possesses none of these characteristics, laboratory studies performed by Adam et al.(2) showed that MnO_4^- could effectively transform and mineralize RDX (i.e., ~87% recovered as $^{14}\text{CO}_2$). Moreover, a pilot-scale demonstration at the Nebraska Ordnance Plant further supported MnO_4^- as a possible *in situ* treatment for RDX-contaminated groundwater.(3) Despite demonstrating efficacy



in removing RDX from tainted waters, the reaction rates and mechanisms by which MnO_4^- transforms RDX (and other explosives) have not been thoroughly studied.(4) While a carbon mass balance of the RDX– MnO_4^- reaction has been observed,(2) a similar nitrogen mass balance for this reaction has not been reported.

One analytical challenge to identifying degradation products in a MnO_4^- matrix is that the solution is highly colored (i.e., purple), so colorimetric and UV detection techniques are not possible unless samples are quenched to remove MnO_4^- before analysis. However, the choice of quenching agent may influence pH or product distribution and further complicates understanding the RDX– MnO_4^- reaction mechanism.

The transformation of RDX by various treatments has revealed several possible reaction pathways. These include direct ring cleavage, nitro-group reduction, concerted decomposition, and N-denitration.(5–12) While intermediates produced by some of these pathways are fleeting and difficult to mea-

sure, the end products produced are often similar (N_2O , NO_2^- , NO_3^- , NH_4^+) but produced in different ratios depending on the reaction mechanisms. In this paper, we report results from laboratory investigations designed to describe the kinetics of the RDX– MnO_4^- interaction, quantify the effect of temperature on RDX destruction kinetics, and provide a nitrogen mass balance of the RDX– MnO_4^- reaction. On the basis of experimental results, possible mechanisms by which RDX is degraded by MnO_4^- are proposed.

Experimental Section

Details of the chemical standards, analytical instruments (e.g., HPLC, IC, GC/ECD, and UV spectrophotometer), analysis of N-containing gases, RDX purification procedures used for mass balance experiments, and experimental controls are provided in Supporting Information (SI-1, SI-2, SI-3).

Aliquot Sample Preparation. To accurately quantify RDX and degradation product concentrations during oxidation by MnO_4^- , samples were quenched to prevent further RDX transformation. To avoid interferences during RDX and degradation analyses, three different quenching agents were tested (MnSO_4 , MnCO_3 , and H_2O_2). The choice of quenching agent was found to influence pH and product distribution (see Supporting Information, SI-4). The two quenching agents we used most frequently included MnCO_3 (0.10 g per mL of sample unless otherwise stated) and $\text{MnSO}_4 \cdot \text{H}_2\text{O}$ [0.10 mL of a MnSO_4 solution (0.10 g/mL) per mL of sample]. The typical quenching procedure involved removing 1-mL aliquots from the RDX– MnO_4^- batch reactors, placing the aliquots in a 1.5-mL centrifuge tube, adding the quenching agent, and centrifuging at 14000 rpm for 10 min. When MnCO_3 was used, an additional 5 min of shaking on a vortex was performed before centrifuging. The supernatant was then transferred to an HPLC or an IC vial and stored at 4 °C until analysis.

RDX Kinetic Experiments. Kinetic experiments were performed under batch conditions by placing 150 mL of RDX solution in 250-mL Erlenmeyer flasks and agitating on an orbital shaker. Solution samples were taken every 2–3 d, quenched with MnSO_4 , and analyzed for RDX by HPLC. We initially prepared RDX solutions by spiking 150 mL of H_2O with 1.04 mL of RDX stock solutions prepared in acetone, but acetone was found to facilitate the decomposition of MnO_4^- at alkaline pH and prevent further degradation of RDX >10 d (see Supporting Information, SI-5). Consequently, all aqueous RDX solutions were prepared by dissolving purified crystalline RDX in water over several days.

To determine reaction rates, kinetic experiments fixed the initial RDX concentration at 0.09 mM and samples were treated with MnO_4^- in excess by varying concentrations between 4.20 and 84.03 mM. Likewise, using initial MnO_4^- concentrations at 33.61 mM, we treated varying concentrations of RDX (0.01–0.09 mM). Both experiments were conducted in neutral pH (~7) at room temperature (25 °C). Reaction rates were then determined by the initial rate method.⁽¹³⁾ The rate law describing a second-order reaction between RDX and MnO_4^- is presented in Supporting Information (SI-6).

RDX– MnO_4^- Temperature Experiment. To quantify the effect of temperature on the RDX– MnO_4^- reaction (i.e., second-order rate constant, k''), we performed experiments in 150-mL glass bottles containing 100 mL of RDX (0.02 mM). Treatment temperatures were 20, 35, 50, and 65 °C and held constant for 2–3 h prior to the start of the experiment.

The aqueous RDX solution was treated with 4.20 mM MnO_4^- . Aqueous RDX solutions without MnO_4^- ($n = 3$) were used as controls and monitored at each temperature. Samples were periodically collected and quenched with MnCO_3 as described and analyzed for RDX by HPLC.

4-NDAB Experiments. To determine the stability of 4-NDAB in the presence of MnO_4^- , we conducted batch experiments with 4-NDAB as the starting substrate. Batch experiments were performed in a 250-mL Erlenmeyer flask containing 100 mL of 4-NDAB (0.04 mM) covered with parafilm and agitated with an orbital shaker at ambient temperature (24 °C). 4-NDAB was treated with 4.20, 8.40, 16.81, and 33.61 mM of MnO_4^- . Samples were collected every 30 min and quenched with MnCO_3 as previously described. 4-NDAB was immediately analyzed by HPLC.

RDX Nitrogen Mass Balance Experiment. Aqueous RDX (0.10 mM) prepared from purified RDX was placed into a 10-mL serum vial (Wheaton, Millville, NJ). The vial was closed with a silicone septum with zero headspace and crimped with an aluminum cap. So that we could precisely calculate the nitrogen mass balance, each vial was weighed before and after introducing any chemicals. Once the vial was sealed, a 21G (i.e., needle gauge no. 21) needle and a 3-mL syringe were inserted through the septum. Helium gas was then added to the 21G needle to push out 2.5 mL of solution into the 3-mL syringe. The 21G needle was removed and another syringe was inserted into the He headspace where MnO_4^- stock solution was introduced to produce an initial concentration of 33.61 mM. Because the added MnO_4^- stock replaced a portion of the He headspace gas back into the 3-mL syringe, experimental treatments began at ambient pressure ($t = 0$ d). Vials were again weighed to determine the precise volume of solution and headspace in each replicate. To avoid possible gas losses through the needled-pierced septa, the septa were sealed with thermoplastic adhesive. Each vial was then covered with aluminum foil to prevent MnO_4^- photodegradation^(14, 15) before shaking on a reciprocal shaker until analysis.

Sacrificial sampling occurred at 0, 1, 2, 3, 6, 9, 15, 19, 23, and 28 d. Each replicate ($n = 4$) was used to analyze three different types of analytes. For N_2O gas production, 0.5 mL of headspace gas was removed and injected directly into GC/ECD. For changes in solution concentrations of RDX and $\text{NO}_3^-/\text{NO}_2^-$, 2.0 mL of sample were quenched with MnCO_3 . One aliquot (1.0 mL) was analyzed by HPLC while the other was used to quantify $\text{NO}_3^-/\text{NO}_2^-$ by IC. Each replicate solution was also analyzed for MnO_4^- with a UV spectrophotometer to ensure uniformity in MnO_4^- concentrations among replicates.

Results and Discussion

RDX Kinetics Experiments. Treating aqueous RDX with varied MnO_4^- concentrations resulted in a wide range of RDX destruction rates (i.e., pseudo-first-order rate, $k_{\text{obs}} = 0.02\text{--}0.37$ d⁻¹, Figure S11A). By plotting $\log[k_{\text{obs}}]$ versus $\log[\text{MnO}_4^-]_0$ (Figure 1A), the calculated slope (β) of this regression was 0.98 ± 0.06 ($r^2 = 0.99$) and indicates that reaction was first-order with respect to MnO_4^- . Likewise, kinetic experiments estimated the reaction order with respect to RDX (α). Upon treatment of varying RDX concentrations with 33.61 mM MnO_4^- , the initial reaction rates (r_0 ; based on Equation S8) were approximated from the tangent of the concentration-time curves (Figure S12). The log of the initial reaction rate ($\log[r_0]$) was plotted against initial RDX concentration to es-

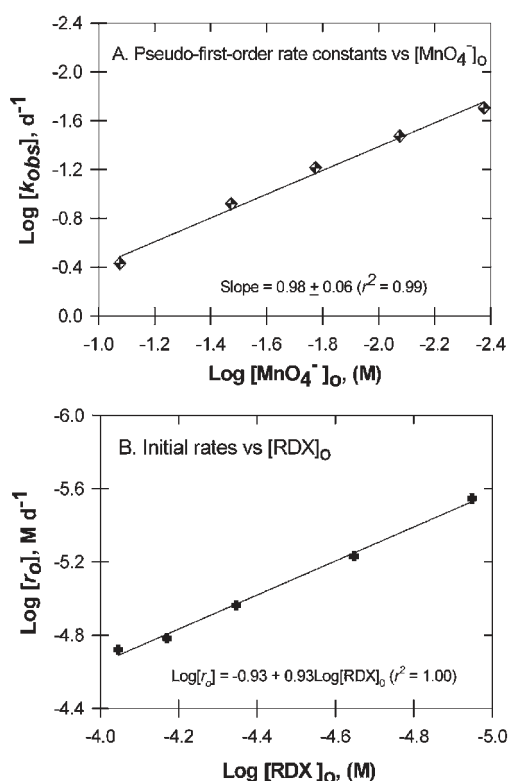


Figure 1. (A) Plot of pseudo-first-order rate constants for RDX degradation vs $[\text{MnO}_4^-]_0$. Aqueous RDX (0.09 mM) was treated with MnO_4^- ranging from 4.20 to 84.03 mM. (B) Plot of initial rates of RDX degradation vs $[\text{RDX}]_0$ ranging from 0.01 to 0.09 mM when treated with 33.61 mM MnO_4^- .

estimate reaction order for RDX (α). Results indicated α values very close to 1, also verifying the reaction is first-order with respect to RDX (Figure 1B).

Both sets of kinetic experiments (Figure 1) demonstrate that the initial reaction between RDX and MnO_4^- is second-order (i.e., $\alpha = \beta = 1$) with a rate constant (k'') of $4.16 \times 10^{-5} \text{ M}^{-1} \text{ s}^{-1}$ ($\pm 0.22 \times 10^{-5}$) (Equation S6). A compilation of destruction rates of various contaminants by MnO_4^- (4) revealed that a number of contaminants may react with MnO_4^- as fast as or faster than the chlorinated ethenes, the groundwater contaminants most commonly treated by MnO_4^- . One of those contaminants reported to have a second-order rate constant similar to that of the chlorinated ethenes was TNT.(4) Given that TNT and RDX are often cocontaminants in the field, a parallel set of kinetic experiments were performed with TNT (see Supporting Information, Figures S11B and S13). These experiments concluded that the TNT- MnO_4^- reaction is first-order with respect to TNT and MnO_4^- or second-order overall (Figure S14) with a k'' of $1.18 \times 10^{-3} \text{ M}^{-1} \text{ s}^{-1}$ ($\pm 0.02 \times 10^{-3}$). While the second-order rate constant observed for RDX in this study is similar to those reported,(2, 4) our k'' for TNT is lower than that reported by Waldemer and Tratnyek ($0.03 \text{ M}^{-1} \text{ s}^{-1}$ (4)) but still 28-fold higher than what we observed for RDX, indicating a large difference in reactivity between these two explosives. This observation is perhaps not surprising and undoubtedly related to differences in chemical classes (nitramine vs nitroaromatic).

Effect of Temperature on RDX- MnO_4^- Reaction. Albano et al.(3) previously reported that RDX transformation rates were slowed 3-fold under temperatures indicative of aquifer conditions (11.5 vs 23 °C). We treated aqueous

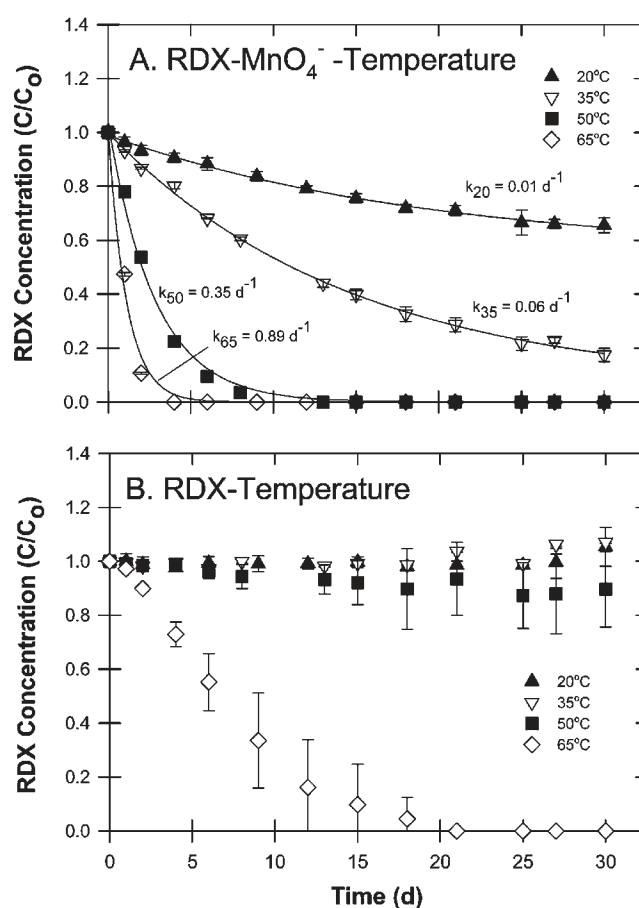


Figure 2. Temporal changes in RDX concentration in aqueous solution treated with 4.20 mM of MnO_4^- at 20, 35, 50, or 65 °C. Bars indicate sample standard deviations ($n = 3$).

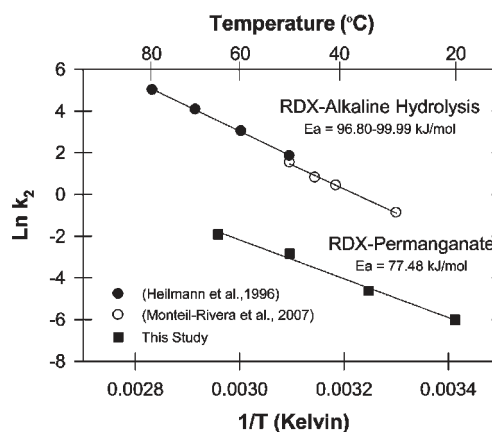


Figure 3. Arrhenius plot of second-order rate constants.

RDX with MnO_4^- at four temperatures to further elucidate the temperature dependency of the reaction at elevated temperatures. Results showed the RDX destruction rates were significantly increased with increasing temperature with pseudo-first-order rates ranging from 0.01 to 0.89 d^{-1} (Figure 2A). At 20 °C, RDX concentration was only reduced by 30% after 30 d ($k = 0.01 \text{ d}^{-1}$) while complete RDX transformation (100%) was achieved within 6 d at 65 °C ($k = 0.89 \text{ d}^{-1}$). A comparison of

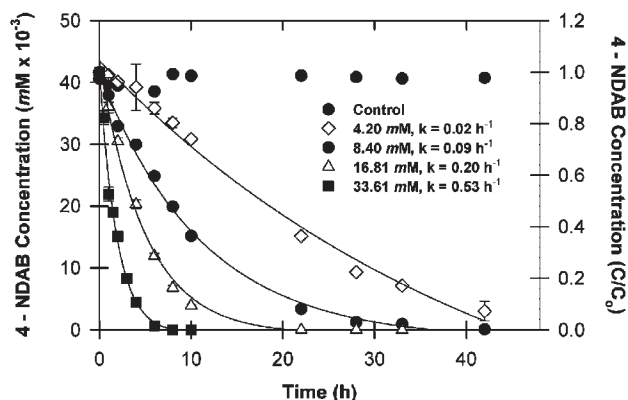


Figure 4. Loss of 4-NDAB concentration following treatment of 4-NDAB aqueous solution with various concentrations of MnO_4^- and quenching with 0.10 g MnCO_3 (per mL). Bars indicate sample standard deviations ($n = 3$).

controls (temperature only) showed that RDX was relatively stable at temperatures $\leq 50^\circ\text{C}$ but decreases in RDX concentrations were observed at 65°C , albeit at a slower rate than when MnO_4^- was also present (Figure 2B). A comparison of previously reported destruction rates shows that, in order to get the destruction rate we observed at 65°C with 4.20 mM MnO_4^- , Adam et al.(2) needed 168 mM MnO_4^- at room temperature (a 40-fold higher concentration).

Computed pseudo-first-order constants (k_{obs} , Figure 2A) were converted to second-order rate constants at $\beta = 1$ based on Equation S6 (see Supporting Information, SI-6, SI-7, and Table S2). The temperature dependency was further calculated by using an Arrhenius plot (Figure 3). The activation energy for the reaction between RDX and MnO_4^- in the temperature range $20\text{--}65^\circ\text{C}$ was 77.48 ± 5.13 kJ/mol (Figure 3) with an Arrhenius parameter (i.e., $\ln A$) of 25.77 ± 1.96 L/mol min. For comparison, the temperature dependency of RDX hydrolysis from previously published work is also plotted (Figure 3). Results show that the RDX- MnO_4^- reaction is less temperature sensitive than alkaline hydrolysis and second-order rate constants for RDX- MnO_4^- are considerably lower than the rate constants for alkaline hydrolysis observed under similar temperatures.

4-NDAB Experiments. Past research has shown that 4-NDAB is an RDX degradation product after ring cleavage for both abiotic and biological treatments,(8, 9, 16) such as aerobic biodegradation(16-19) and alkaline hydrolysis.(6) In aerobic degradation, 1 mol of RDX yields 1 mol of 4-NDAB and 2 mols of NO_2^- .(20) Adam et al.(2, 21) also separately reported observing 4-NDAB during treatment with MnO_4^- or ozone. While Adam et al.(2) also used peroxide to quench MnO_4^- , which would explain the detection of NDAB (Figure S6B), their experiments with ozone required no quenching agent.(21) A question surrounding 4-NDAB detection during RDX degradation is whether it is formed during the RDX- MnO_4^- reaction or if it is just a product of the quenching process (see Supporting Information, SI-4).

Because only a trace of 4-NDAB (Figure S6) was observed in the RDX- MnO_4^- reaction when MnCO_3 was used as a quenching agent, additional explanations for its lack of detection were pursued. In testing the stability of 4-NDAB under the different pH values, we found that 4-NDAB was relatively stable for the first 10 d (>90% remaining) (Figure S8). Therefore, the stability of NDAB was not influenced by the pH of our treatments.

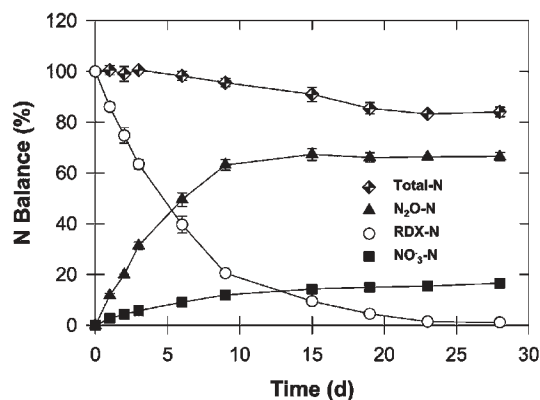


Figure 5. Nitrogen mass balance results from tracking loss of RDX and production of N_2O and NO_3^- . Bars indicate sample standard deviations ($n = 4$).

We also used 4-NDAB as the starting substrate by treating it with varying concentrations of MnO_4^- . Results showed that 4-NDAB is much more quickly transformed by MnO_4^- than RDX, with transformation occurring within hours (Figure 4) versus days for RDX (Figure S6A). 4-NDAB is likely oxidized faster than RDX because oxidation of the formamide group to a carbamic acid and the subsequent decarboxylation are known to be very fast reactions.(22-24) While 4-NDAB was found to be a dead-end product of RDX via photodenitration,(8) aerobic biodegradation,(5) and alkaline hydrolysis,(6) we showed that it was not stable in MnO_4^- (Figure 4). Treatment of 4-NDAB with MnO_4^- also produced N_2O . A separate N-mass balance attempt showed that >50% of the N in 4-NDAB was converted to N_2O . In contrast to what was observed with RDX (see below), NO_3^- was not formed in the 4-NDAB- MnO_4^- reaction.

Nitrogen Mass Balance Experiment. Using purified RDX, we prepared an aqueous solution and treated it with MnO_4^- . Initial experiments screened for a variety of N-containing products (NO_2^- , NO_3^- , N_2O , NH_4^+ , 4-NDAB, and MEDINA), but only NO_3^- and N_2O were found to be formed in significant quantities. Temporal tracking of RDX, N_2O , and NO_3^- revealed that, after approximately 25% of the RDX had been transformed, a 99% N balance was obtained (day 2, Figure 5). By day 9, roughly 80% of the RDX had been transformed and RDX, N_2O , and NO_3^- still constituted 95.6% of the N balance. During the time when most of the RDX was transformed (i.e., 0-9 d), roughly 5 times as much N_2O was produced than NO_3^- (molar basis). The production of N_2O declined after 9 d, and concentrations reached a plateau by day 15; NO_3^- production continued with a slow steady increase until 28 d, the time when RDX was no longer detectable (Figure 5). The nitrous oxide production was calculated by summing the direct headspace measurement plus the calculated dissolved liquid phase concentration in equilibrium with the measured gas phase concentration.(25) Possible reasons why N_2O production did not continue to mirror RDX loss after 15 d include the inability of our microcosms to retain the headspace gases, the relationship between dissolved (i.e., calculated) and headspace N_2O concentrations changing as headspace pressure (i.e., N_2O production) increased, or other nitrogen gases or dissolved species being produced.

The possibility of other N-containing gases (NO , NO_2 , N_2) forming from the RDX- MnO_4^- reaction was investigated using ^{15}N -RDX but could not be confirmed [see Supporting In-

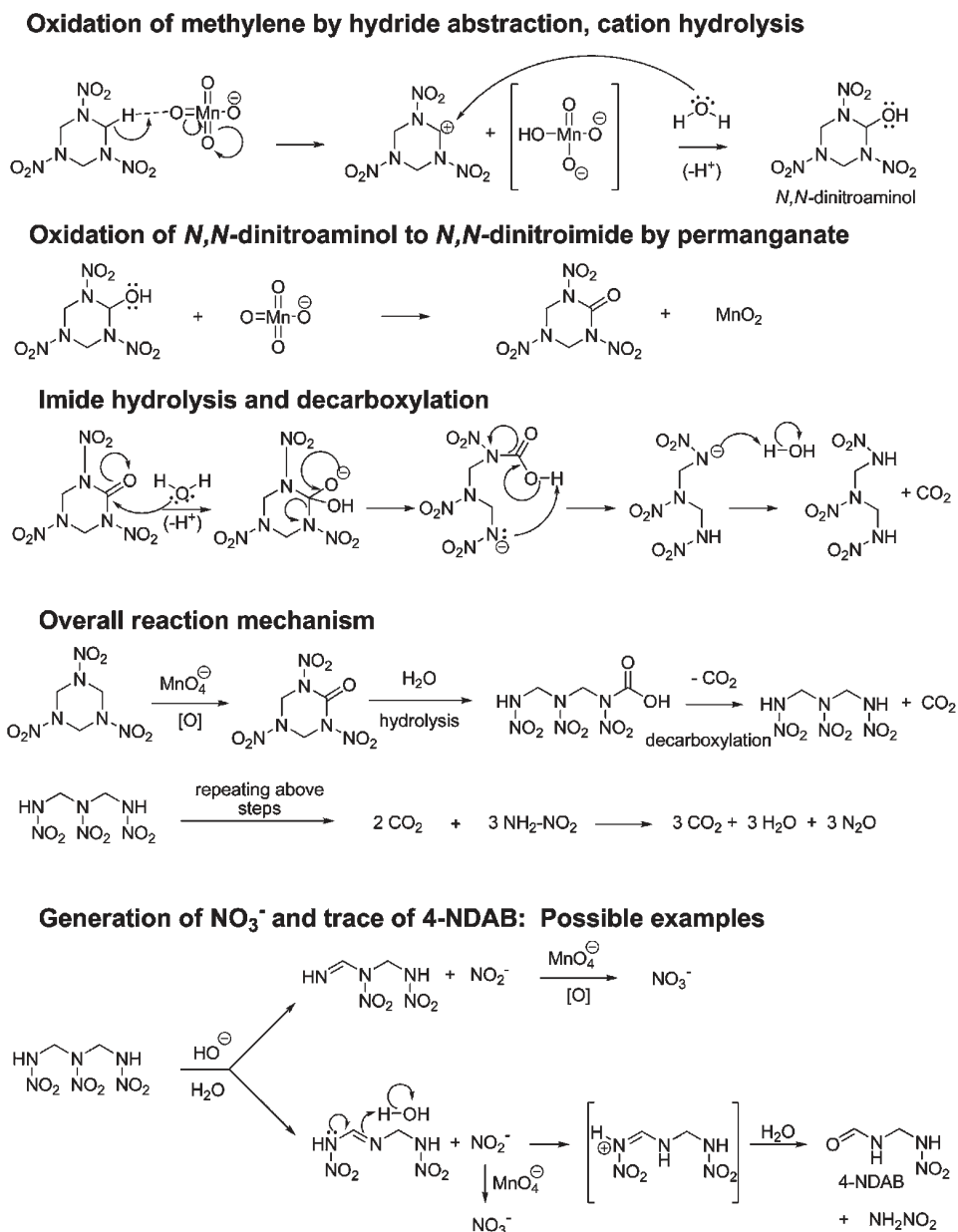


Figure 6. Proposed RDX degradation pathway of RDX- MnO_4^- reaction under neutral pH.

formation, SI-1 (analysis of N-containing gas)]. Previous attempts to obtain a nitrogen balance during treatment of RDX have had mixed results. When 4-NDAB is a significant product, good N-balances have been obtained. For instance, Balakrishnan et al.(6) studied alkaline hydrolysis of RDX (pH 10–12.3) and found 90.7% of nitrogen mass balance [i.e., NO_2^- (16.2%), N_2O (25.6%), $\text{NH}_3/\text{NH}_4^+$ (1.3%), and 4-NDAB (47.6%)]. When reductive treatments to RDX have been imposed, N-balances have generally been low (e.g., References 26 and 27).

RDX Degradation Mechanism. RDX is known to be degraded within days (~15 d) by base hydrolysis (pH 10) at ambient temperature(6) and within hours to minutes at elevated temperatures.(28, 29) We show that RDX was degraded by MnO_4^- at neutral pH over several days at room temperature (Figure S6A) and that increasing temperature increased destruction rates (Figures 2 and 3). On the basis of results obtained from the various experiments (quenching agents, pH,

temperatures, and activation energies), and the lack of readily identifiable carbon-containing intermediates (other than a trace of 4-NDAB), the initial step in the RDX- MnO_4^- reaction is likely rate-limiting. On the basis of the various experimental treatments imposed, we believe this initial step can be described in one of two ways. When solution pH was alkaline, either as an artifact of the quenching agent (Figure S6B) or purposely increased (Figure S6C), then it is probable that the first step in the RDX- MnO_4^- reaction is similar to the previously reported hydrolysis pathway (N-denitration;(6) see Supporting Information, SI-9, Figure S18). This mechanism would produce 4-NDAB, which was observed. And although 4-NDAB is a relatively stable intermediate during alkaline hydrolysis,(28) we show that 4-NDAB reacts with MnO_4^- at a much faster rate than RDX (Figures 2, 4, and S6A). Under alkaline pH then, 4-NDAB was apparently produced by hydrolysis faster than it is oxidized by MnO_4^- (Figures S6B and S6C), which allowed it to be detected.

Under neutral pH, which is more indicative of treating aqueous RDX with MnO_4^- (pH 7.2 observed), we believe the initial step is an oxidation mechanism that begins with abstraction of a hydride from the methylene carbon by MnO_4^- causing a carbocation to form (Figure 6). This proposed step is supported by past research on MnO_4^- -amine reactions.(30-32) Permanganate oxidation of amines has been shown to proceed in one of two ways, namely single electron transfer (SET) from the amine nitrogen and hydride or hydrogen atom abstraction from the carbon. A detailed consideration of both possible first steps (SET vs hydride loss) for RDX oxidation is presented in Supporting Information (SI-8, Figure S17). In brief, theoretical explanations and experimental observations indicate that SET will dominate the reactivities of tertiary amines with MnO_4^- but hydrogen abstraction becomes more prominent in secondary and primary amines.(31, 32) Second-order rate constants have also been shown to significantly decrease when the mechanism shifts from SET to hydrogen atom loss.(31) Moreover, when the initial intermediate can be stabilized with resonance as previously shown for benzylamine, the rate determining step proceeds by loss of hydride (or hydrogen atom) rather than SET.(30) Given that the initial carbocation intermediate proposed for RDX (Figure 6) would be more stable than the intermediate formed by SET (Figure S17), we believe the hydride loss mechanism would be operative.

Following through with the proposed mechanism (Figure 6), the carbocation intermediate would react with water by hydrolysis to form a C–O bond (alcohol) and the resulting *N,N*-dinitroaminol with MnO_4^- itself to form an imide. It is well established that MnO_4^- oxidizes alcohols to carbonyl compounds.(33) but the mechanisms have been shown to change completely as pH, reagent, and structure are varied.(34-37) To our knowledge an oxidation mechanism for the proposed *N,N*-dinitroaminol has not been studied, so no specific mechanism for this conversion (aminol to imide) is presented. Once formed, however, water would attack the imide carbon (hydrolysis) to open the ring and lead to a carbamic acid/amide anion. The carbamic acid/amide ion would then undergo decarboxylation and liberation of CO_2 . The accelerated rate of *N,N*-dinitroimide hydrolysis and decarboxylation has been previously observed in *N*-nitrourea chemistry.(38-40) This same three-step cycle of oxidation, hydrolysis, and decarboxylation would continue leading to the production of CO_2 and H_2NNO_2 (nitramide), which would rapidly be converted to N_2O (6) and water (Figure 6).

While the proposed mechanisms are presented separately (Figures 6 and S18) and in a stepwise fashion, it is possible that several of these steps occur simultaneously. The dominant mechanism, however, can be inferred by the distribution of nitrogen-containing degradation products observed. RDX hydrolysis is reported to produce N_2O , NO_2^- , NH_3 , and N_2 in the proportions 3.2:4.7:2.6:1, respectively.(28) The hydride removal mechanism predicts that if RDX is exclusively degraded by oxidation, only N_2O would be produced; any nitrate observed would have to result from hydrolysis of postoxidation intermediates (Figure 6). Restated, if the solution chemistry is dominated by oxidation, we should observe ratios of $\text{N}_2\text{O}/\text{NO}_3^-$ which strongly favor N_2O . If the process is mainly hydrolysis followed by oxidation, the same ratio would strongly favor NO_3^- . Our experiments indicate that RDX- MnO_4^- reaction produces N_2O and NO_3^- in a molar ratio of about 5:1, leading us to conclude that oxidation processes are dominant under the conditions we report.

Supporting Information, providing details of experimental procedures and further explanation of results, is presented following the References.

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Supporting information follows.

Supporting Information for:

Transformation of Hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX) by Permanganate

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SI-1. Additional Experimental Section

Chemical Standards. Commercial-grade RDX (~90% purity) was obtained from the Fort Detrick U.S. Biomedical Research and Development Laboratory (Frederick, MD). 4-nitro-2,4-diazabutanal, (4-NDAB, >99% purity) was custom synthesized by SRI International (Menlo Park, CA). Sodium permanganate (NaMnO_4 , 40% by weight) and potassium permanganate (KMnO_4) were obtained from Fisher Scientific (Pittsburgh, PA). Reagent grade hydrogen peroxide (H_2O_2 , 30% v/v), methanol, manganous sulfate ($\text{MnSO}_4 \cdot \text{H}_2\text{O}$) (J.T.Baker, Phillipsburgh, NJ), and manganous carbonate (MnCO_3 , 99.9%, metals basis) (Alfa Aesar, Ward Hill, MA) were used as purchased. All solvents used in this research were HPLC grade (Fisher Scientific, Springfield, NJ). An analytical RDX standard (100 $\mu\text{g}/\text{mL}$) in a 50:50 acetonitrile-methanol matrix was purchased from AccuStandard (New Haven, CT). Nitrate (NO_3^-), Ammonium (NH_4^+) (1000 mg/L, GFS Chemicals, Columbus, OH) and nitrite (NO_2^-) (1000 mg/L, Absolute Standards Inc., Hamden, CT) standards were used as purchased. Nitrous oxide (N_2O) standards were prepared from the 2% stock gases (mole basis) obtained from Scott Specialty Gases (Plumsteadville, PA).

High-Performance Liquid Chromatography (HPLC). Temporal changes in RDX and degradate concentrations were quantified at a 220 nm by HPLC equipped with a photodiode array detector (Shimadzu Scientific Instruments, Columbia, MD). Peak separations were performed by injecting 20 μL of sample into a Supelcosil LC-8, 250 x 4.6 mm, (Supelco, Sigma-Aldrich Corporation, PA) or a Fluophase PFP perfluorinated column, 250 x 4.6 mm, coupled with a guard column (Thermo Scientific, MA). A variety of mobile phases and flow rates (0.50-1.50 mL/min) were tested to separate peaks but the typical mobile phase was an isocratic mixture of methanol and H_2O (30:70), or acetonitrile and H_2O (50:50) at a flow rate of 0.75 mL/min.

Ion Chromatography (IC). Analysis of $\text{NO}_2^-/\text{NO}_3^-$ and NH_4^+ were performed with a Dionex DX-120 Ion Chromatograph (Sunnyvale, CA) with suppressed conductivity detection (conductivity detector, CDM-3). For anion analysis, separation was performed with an AS-15 IonPac column, 250 x 4.0 mm, using an eluent of 38 mM NaOH at a flow rate of 1 mL/min. For cation analysis, separation was performed with a CS12A IonPac column, 250 x 4.0 mm, using an isocratic eluent of 5.5 mM H_2SO_4 at a flow rate of 1.2 mL/min. The injection volume for both analyses was 25 μL . To effectively analyze samples by IC, RDX samples treated with MnO_4^- were quenched with MnCO_3 .

Gas Chromatography/Electron Capture Detector (GC/ECD). Nitrous oxide (N_2O) emitted from the RDX- MnO_4^- reaction was measured by direct injection into a Hewlett-Packard (Palo Alto, CA) 6890 GC operated with a HP-Plot column (Molecular sieve 5A) 30 m/0.53 mm (50 μm film thickness) and electron capture detector (ECD). A P-5 gas (a mixture gas of 95% Argon and 5% CH_4) was used as a carrier gas for the GC system. The GC oven was equilibrated at least two hours at 225 $^\circ\text{C}$ before analysis.

UV-Spectrophotometer. Changes in MnO_4^- concentrations were monitored by diluting solution with Ultra Pure water in 20-mL vials and quantifying concentrations with a HACH Spectrophotometer DR2800 (HACH Company, Loveland, CO) at a wavelength of 525 nm. A test of whether colloidal MnO_2 interfered with quantification of MnO_4^- is presented in SI-3.

Analysis of N-containing gases.

Nitrogen Gas (N_2) To determine if N_2 gas was a product of the RDX- MnO_4^- reaction, experiments were conducted under vacuum in a Rittenburg tube, a two-legged Y-shaped tube (Fig. S1), containing crystalline RDX (both ^{14}N -RDX and ^{15}N -RDX) in one side and concentrated MnO_4^- solution in the other. Uniformly labeled, $[\text{U-}^{15}\text{N}]\text{RDX}$, (^{15}N abundance of 97 atom%) was purchased from PerkinElmer (Waltham, MA). Prior to starting the reaction (i.e., mixing), all gases were evacuated through a vacuum line

while the MnO_4^- solution was simultaneously frozen. Once the frozen solution melted, we mixed it with the crystalline RDX in the other side. The tube was then immersed in water ($\sim 20^\circ\text{C}$) to confirm no leakage and avoid atmospheric gas contamination. We also mirrored this experiment without vacuuming so as to monitor the RDX concentration by HPLC. When RDX was completely degraded, gas emission was drawn by a vacuum system passing through a cold trap to freeze all gases but N_2 gas (Fig. S2; (1)). Gas samples were then collected in sample bulb and cryogenically transferred to an Optima Dual Inlet mass spectrometer (VG Isotech, Colchester, VT).

Results indicated that no increase in gas pressure was observed during the sample transfer and full scan measurement showed that, very little, if any N_2 gas ($m/z = 28, 29, 30$) formed during treatment. The primary reaction gas formed, N_2O , was trapped in the preparation line but was not analyzed on the instrument.



Figure S1: (Left) The Rittenburg tube containing MnO_4^- solution was frozen in liquid nitrogen while all gases were being vacuumed. (Right) thawed RDX- MnO_4^- solution after mixing.



Figure S2: Experimental system for trapping of N_2 gas. When RDX was completely degraded, all gases were evacuated from the Rittenburg tube (Lower Circle) and trapped in the vacuum system except N_2 gas which was forced to the gas-tight sampling tube (Upper Circle).

NO_x gases (i.e., NO_2 and NO) Besides the N_2 and N_2O gases, we also investigated the production of NO_x gases (i.e., NO_2 (nitrogen dioxide) and NO (nitric oxide)) to determine if they were released during the $RDX-MnO_4^-$ reaction. NO_2 is known to produce from the reaction of concentrated nitric acid and copper and is a toxic brownish gas with a pungent acid odor. However, in the diluted solution of nitric acid and copper, water molecules cause the reaction to produce NO instead. Although we did not observe a distinct brownish color of NO_2 during the $RDX-MnO_4^-$ reaction, we attempted to identify NO_2 and other possible transformation products by treating 5 mL of

saturated RDX (12.1 mg ^{15}N -labeled and 0.4 mg non-labeled RDX) with 168.067 mM of MnO_4^- in a 12-mL vial with a gastight septum. Each vial was degassed for 5 min and purged with Helium for 5 min by the acid injector (3.2 psi, Gilson, Middleton, WI) at a flow rate of 20.5 mL min^{-1} . NaMnO_4 (0.2 mL of 40% by weight) was injected into a vial by a gastight syringe. The temperature was controlled in a Precision 180 Series water bath at 60°C (Precision Scientific Co., Baltimore, MD) to increase RDX destruction rate. At 11 d, a $10 \mu\text{L}$ gas sample was removed from the vial and injected directly into a Hewlett-Packard 5890 GC (Palo Alto, CA) an Agilent 5972 quadrupole mass spectrometer. The N gases were separated on a 30 m/0.32 mm PLOT Moleseive column (J&W Scientific, Folsom, CA). The instrument was calibrated using Helium reference gas.

Results indicated that NO_2 and NO were not detectable during the RDX-MnO_4^- reaction. A complicating factor, however, is that if NO_x gasses (i.e., NO or NO_2) are liberated during the treatment of RDX with MnO_4^- , it will be difficult to quantify because MnO_4^- provides an excellent means of removing NO by oxidizing it to NO_2^- and NO_3^- , depending on pH (2-4). Alkaline or acidic MnO_4^- has also been shown to be capable of trapping NO_x gas emission from soils (5-8).

SI-2. RDX Purification

The commercial grade RDX contains ~90% RDX and ~10% HMX (octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine). To remove interferences and degradation artifacts associated with HMX, we removed the HMX by preparing a concentrated RDX solution (in acetonitrile) and purified to ≥99% RDX by using a Waters 2695 HPLC (Waters Corp., Milford, MA) with a temperature-controlled (30 °C) Kromasil C18 column, 250 x 4.6 mm, (Thermo Scientific, MA) and Photodiode Array Detector (Waters 2996, Waters Corp., Milford, MA). The flow rate for this purification procedure was 1.5 mL/min with a repeated injection volume of 25 μL. A mobile phase of methanol (in H₂O) was used with the following gradient: 60:40 for 9 min followed by 90:10 for 3.5 min and 60:40 for the remainder of the run (~7.5 min). A Spectrum CF-2 fraction collector was used to isolate the RDX peak eluting from the column. The RDX fractions were combined and concentrated by the RapidVap evaporation system (Labconco, Kansas city, MO) in which a cylindrical receptacle was swirled and blown by N₂ gas at 50 °C until dry.

SI-3. Experimental Controls

A series of experiments were performed under batch conditions to verify that RDX destruction rates by MnO_4^- were similar when the initial pH was controlled or allowed to drift as the reaction proceeded (Fig. S3), the use of MnCO_3 as a quenching agent did not significantly influence sample pH or temperature (Table S1), RDX concentrations after quenching with MnCO_3 were stable and not subject to hydrolysis (Fig. S4), and that quantification of MnO_4^- concentrations were not influenced by colloidal MnO_2 (Fig. S5).

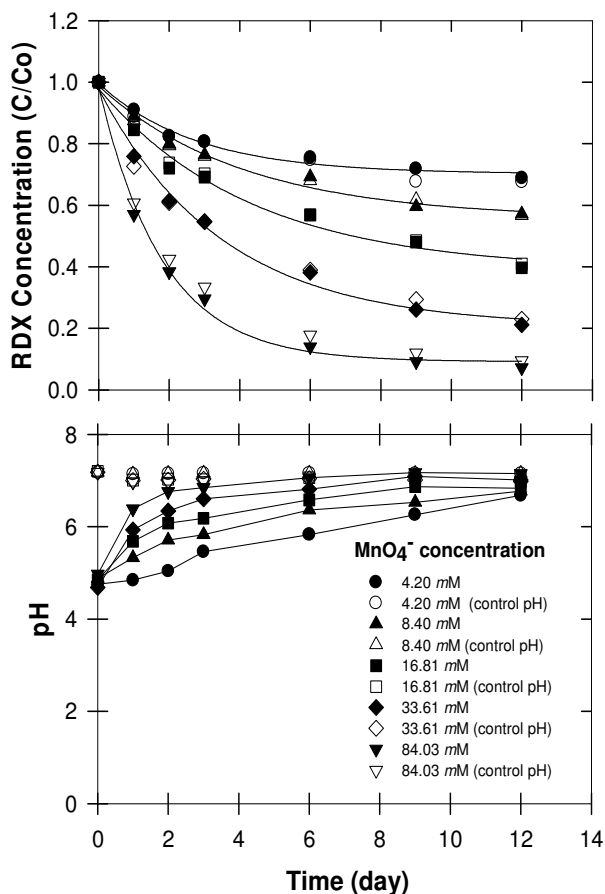


Figure S3. Changes in RDX concentration and pH by various concentrations of MnO_4^- under controlled and unbuffered pH.

Table S1. Changes in pH and temperature of RDX-MnO₄⁻ solution following quenching with various mass of MnCO₃.

MnCO ₃ (g per mL of sample)	pH before quenching	pH after quenching	Temp before quenching (°C)	Temp after quenching (°C)
0.00 g	5.88		25	
0.03 g	5.82	6.15	25	24
0.04 g	5.81	6.02	25	23
0.05 g	5.85	6.02	25	23
0.06 g	5.80	5.93	25	23
0.07 g	5.74	5.86	25	22.5

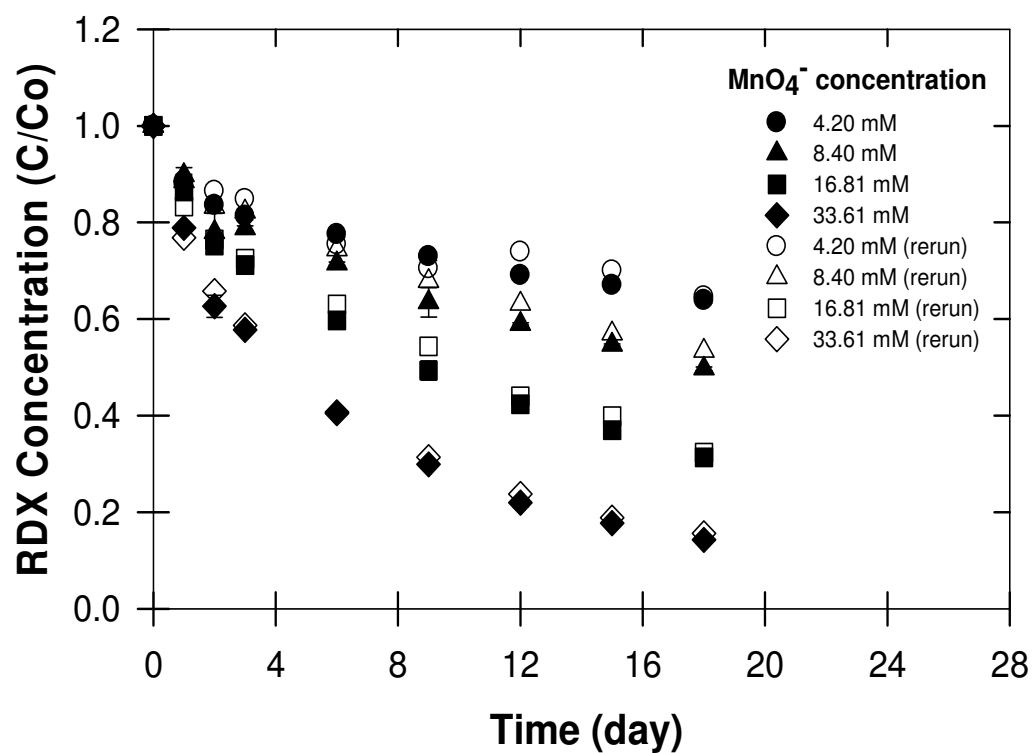


Figure S4. Temporal changes in RDX concentrations following treatment with varying MnO_4^- concentrations. Solid symbols signify concentrations of samples analyzed immediately, open symbols are the same samples analyzed 9 d later.

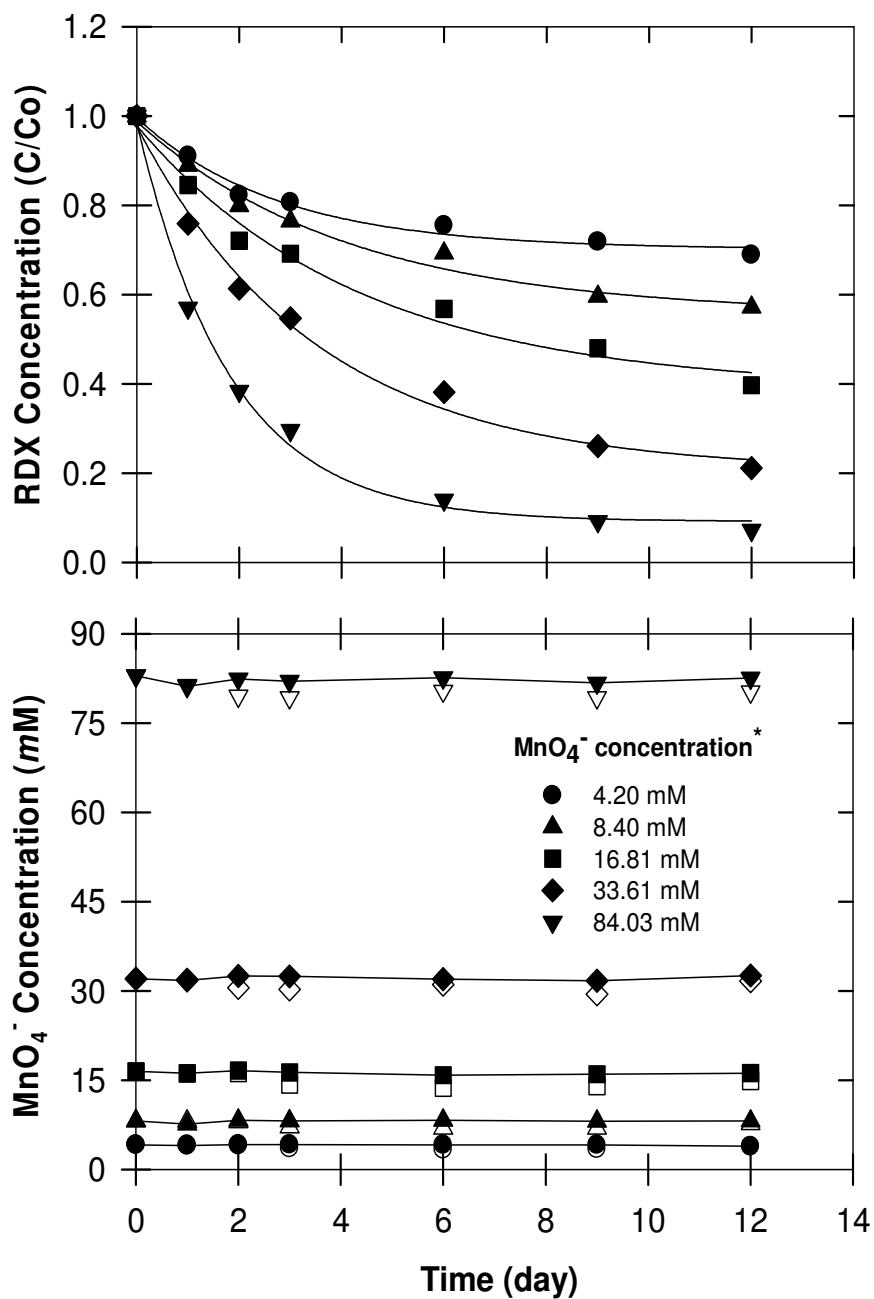


Figure S5. Changes in RDX and MnO_4^- concentrations following treatment with varying MnO_4^- concentrations. Solid symbols indicate MnO_4^- concentrations determined without filtration, open symbols with filtration (0.45 μm glasswool filter).

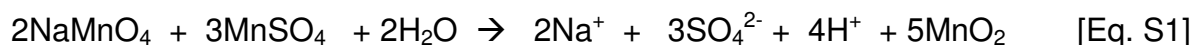
SI-4. Effect of quenching agents on RDX degradation products

To determine the effect of quenching agents on RDX degradation products, aqueous solutions of RDX (0.07 mM) were treated with 33.61 mM of MnO_4^- . We initially prepared RDX solutions by spiking 150 mL H_2O with 1.04 mL of RDX stock solutions prepared in acetone but the acetone- MnO_4^- reaction resulted in autocatalysis of MnO_4^- at alkaline pH and prevented further degradation of RDX >10 d (see Supporting Information; SI-5). Consequently, all aqueous RDX solutions were prepared by dissolving purified crystalline RDX in water over several days. Once MnO_4^- was added to RDX solutions to initiate the reaction, samples were periodically collected and quenched with MnCO_3 or H_2O_2 . Quenching with MnCO_3 (pH = 6.7) was performed as described in the main manuscript. When quenched with 30% H_2O_2 (0.04 mL per mL of sample), samples were required to mix continuously to control H_2O_2 consumption. The pH of samples quenched with H_2O_2 were found to increase significantly (pH = 11.5). To elucidate this pH effect, one set of batch samples were quenched with MnCO_3 , and we increased the pH to that observed with the H_2O_2 by adding NaOH. Temporal changes in RDX, 4-nitro-2,4-diazabutanal (4-NDAB), NO_3^- , and NO_2^- concentration were monitored by using HPLC and IC.

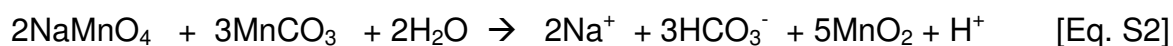
Results indicated that an RDX solution treated with MnO_4^- led to complete RDX transformation within 15 d (Fig. S6A). To quantify temporal changes in RDX concentrations, samples were removed from the batch reactors every 2 to 3 d and chemically quenched to remove MnO_4^- and prevent further RDX oxidation. While MnSO_4 is commonly used as a quenching agent (9-13) and does not interfere in HPLC analysis of RDX (12-13), the sulfate liberated interferes with NO_2^- and NO_3^- analyses by ion chromatography (IC). By using MnCO_3 , we avoided this interference during IC analysis. However, the disadvantage of using MnCO_3 is that, at the concentrations of

quenching agents used, MnCO_3 takes longer than MnSO_4 to quench the MnO_4^- . Given the typical time course of the batch experiments (15 d), we compared RDX destruction rates from the same batch experiment and observed similar RDX destruction rates (Fig. S7).

Another consideration is that the quenching agent can alter the pH of the sample and possibly influence product formation or stability. When samples were quenched with MnSO_4 , solution pH decreased from ~ 7.2 (before quenching) to pH 2.6 after quenching as predicted by the following reaction (Eq. S1).

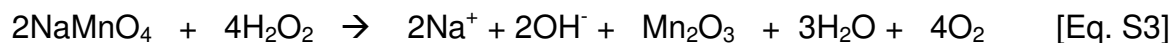


When RDX- MnO_4^- solutions were quenched with MnCO_3 (Eq. S2), sample pH (after quenching) remained near 6.7, which is closer to the pH of the unquenched RDX- MnO_4^- solution.



Product analysis during the RDX- MnO_4^- reaction showed that when MnCO_3 was used as a quenching agent, we observed NO_3^- production in the reaction but no NO_2^- and only a trace of 4-NDAB (~ 0.004 mM) (Fig. S6A).

Peroxide was also used as a quenching agent. Here, peroxide reacts with MnO_4^- by the following reaction (Eq. S3):



Because OH^- is liberated, the pH of samples quenched with H_2O_2 increased (pH

~11.5) and we observed NO_2^- , NO_3^- , and 4-NDAB (Fig. S6B). Although the magnitude of NO_3^- generated was similar to what we observed when MnCO_3 was used as a quenching agent (Fig. S6A, S6B), RDX destruction kinetics were much faster ($k = 1.83 \text{ d}^{-1}$). Because we suspected excess peroxide may have contributed to RDX destruction, we conducted an experiment where RDX solution was treated with H_2O_2 in the same ratio as used in quenching process (0.04 mL of 30% H_2O_2 to 1 mL RDX or 1.2% (v/v) H_2O_2 ; no MnO_4^-). Results showed that RDX concentration was not significantly affected, pH remained constant, and RDX degradation products (NO_2^- , NO_3^- , and 4-NDAB) were not observed.

The peroxide concentration used in this control experiment (RDX + H_2O_2 only) was higher than what the quenched RDX- MnO_4^- samples would have experienced because most, if not all, of the H_2O_2 would have reacted with the MnO_4^- . Therefore, the increased RDX destruction kinetics observed (Fig. S6B) does not appear to be directly related to the presence of excess peroxide. Rather, catalytic decomposition of H_2O_2 into various radicals (i.e., superoxide anion (O_2^-), hydroperoxide radical (HO_2^\bullet), and hydroxyl radical ($^\bullet\text{OH}$)) may have played a role in the enhanced degradation of RDX (Fig. S6B). Although MnO_2 surfaces can enhance oxidation reactions (14), this precipitate, which forms during RDX- MnO_4^- reaction (12), is also a catalyst for decomposition of H_2O_2 and both O_2^- and HO_2^\bullet are favored at high pH (15-16). O_2^- itself is known to be capable of degrading RDX (17). Furthermore, during the quenching process, Mn_2O_3 is liberated (Eq. S3) and can simultaneously act as a catalyst for degradation of organic compounds in the presence of H_2O_2 (15, 18). Another possibility is that the alkaline pH created during the quenching process (Eq. S3) facilitated H_2O_2 decomposition into $^\bullet\text{OH}$ which contributed to RDX degradation. Moreover, Gates-Anderson et al. (19) observed that in strongly basic solutions (pH > 9) $^\bullet\text{OH}$ can also be generated from MnO_4^- and directly oxidize organic contaminants. These explanations support a seven-fold increase of

RDX destruction kinetics (Figs. S6A, S6B).

Finally, an elevated temperature may also have been responsible for greater RDX destruction in the H₂O₂ quenched samples. Heilmann et al. (20) showed that alkaline hydrolysis rates of RDX in aqueous solution dramatically increased at high temperature (50°C). We observed that using H₂O₂ as a quenching agent caused a rapid 9°C increase in sample temperatures. Because H₂O₂-MnO₄⁻ reaction is exothermic, it is reasonable that the combination of alkaline pH and heat may have contributed to RDX degradation (See also *Effect of Temperature on RDX-MnO₄⁻ Reaction* in the main manuscript).

Given that the treatment of RDX with peroxide alone did not cause an increase in pH or the production of NO₂⁻ and 4-NDAB, the alkaline pH created by the H₂O₂-MnO₄⁻ reaction was likely responsible for the degradation products observed. To test this further, we again used MnCO₃ as a quenching agent and artificially raised the pH of the samples before and after quenching to pH 11.5 (similar to what was observed with H₂O₂ as a quenching agent). Results showed RDX degradation was slower than when peroxide was used to quench the MnO₄⁻ and closer to the results obtained when MnCO₃ was used without pH adjustment (Fig. S6A, $k = 0.26 \text{ d}^{-1}$; Fig. S6C, $k = 0.33 \text{ d}^{-1}$). This observation lends credence to the possibility that peroxide radicals may have been involved during the quenching of MnO₄⁻ with H₂O₂ (Fig. S6B). Using MnCO₃ + alkaline pH also produced NO₂⁻ and 4-NDAB as reaction products (Fig. S6C). Two known RDX degradation schemes involve the removal of one nitro group (denitration) with the intermediate methylenedinitramine (MEDINA) or two nitro groups and the formation of 4-NDAB (e.g. (21)). Thus, the detection of nitrite during the RDX-MnO₄⁻ reaction (with H₂O₂ quenching agent or MnCO₃ + alkaline pH) is likely a result of the alkalinity stabilizing NO₂⁻ and preventing further transformation. Numerous reports have shown

that nitrite is more persistent at alkaline pH (22-23). Balakrishnan et al. (24) also found NO_2^- as an endproduct of RDX hydrolysis.

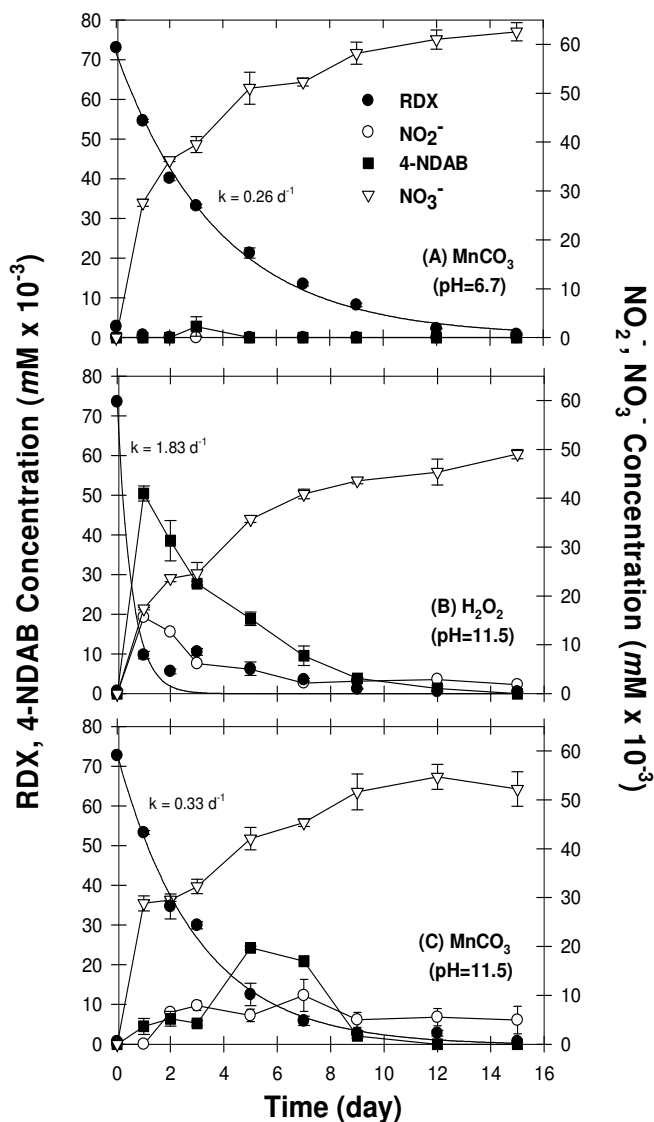


Figure S6: Changes in RDX concentration and production of degradation products (4-NDAB, NO_2^- , and NO_3^-) when quenched with; (A) 0.10 g MnCO_3 (per mL); (B) 0.04 ml 30% H_2O_2 (per mL, pH ~ 11.5); and (C) 0.10 g MnCO_3 (per mL) in which sample solutions pH was raised to 11.5 before and after quenching. Bars indicate sample standard deviations (n = 3).

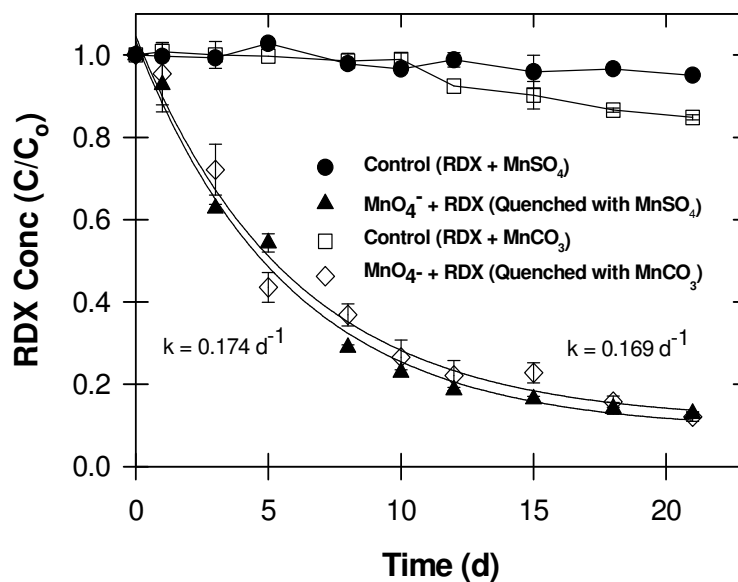


Figure S7: Comparison of RDX degradation kinetic rates when quenched with MnSO_4 or MnCO_3 . Bars indicate sample standard deviations ($n = 3$).

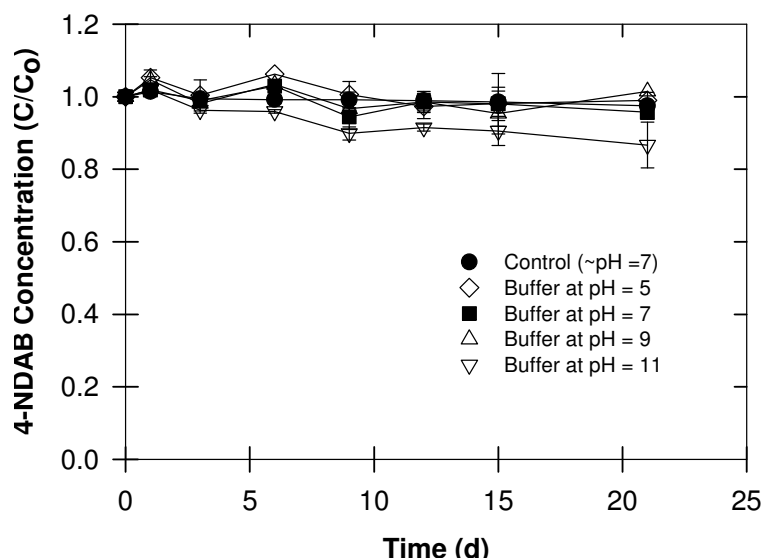


Figure S8: The effect of pH on 4-NDAB stability. Bars indicate sample standard deviations ($n = 3$).

SI-5. RDX Batch Experiments (Facilitated Decomposition of permanganate)

To evaluate the effects of initial MnO_4^- concentration on RDX destruction rates, we conducted the batch experiment by treating 150 mL of aqueous ^{14}C -RDX (0.02 mM, 30000 dpm mL^{-1} , uniformly ring-labeled) and varying MnO_4^- concentration from 8.40 mM to 168.07 mM. Each MnO_4^- concentration was replicated three times. Temporal samples were periodically collected and quenched with MnSO_4 as described in analytical section and monitored for the loss of RDX by HPLC and ^{14}C -activity by Liquid Scintillation Counter (LSC).

Results indicated that treating aqueous (i.e., distilled water) RDX with 168.067 mM of MnO_4^- reduced RDX concentrations to zero within 10 d ($k = 0.49 \text{ d}^{-1}$) (Fig. S9A). Lower MnO_4^- concentrations (8.40-42.02 mM) reduced RDX destruction rates and overall removal. For instance, when RDX was treated with 8.40 mM of MnO_4^- destruction rates decreased ~70% ($k = 0.14 \text{ d}^{-1}$) and only 29% of the initial RDX was removed within 10 d (25). These results are similar to those reported by Adam et al. (12) but differ in that temporal decrease in both RDX and ^{14}C concentrations (Fig. S9B) reached a plateau after ~10 d. The reasons MnO_4^- failed to continually transform and mineralize RDX beyond 10 d was investigated by monitoring temporal changes in pH and MnO_4^- concentrations.

By repeating the experiment with 84.03 mM of MnO_4^- and monitoring MnO_4^- and pH (Fig. S10A, S10B, S10C), we observed an increase in pH from 6.5 to > 8. Using higher MnO_4^- concentrations (126.05, 168.07 mM) also produced similar changes in pH. This increase in pH coincided with a significant decrease in MnO_4^- concentration (Fig. S10B). By contrast, when a pH-stat (Metrohm Titrino 718S; Brinkman Instruments, Westbury) maintained the pH at 7, RDX concentrations did not plateau but continued to decrease and very little consumption of MnO_4^- was observed (Fig. S10A, S10B). It is clear that in the unbuffered treatment, the rapid decrease in MnO_4^- concentration

coincided with the lack of further RDX destruction beyond 7 d (i.e., plateau). We believe the loss of MnO_4^- was likely caused by a facilitated decomposition of permanganate at alkaline pH. But alkaline pH alone was not solely responsible for the loss of MnO_4^- . Adam et al. (12) evaluated the effect of pH on RDX destruction kinetics and reported no pH effect in the range 4.1 to 11.3. A comparison of procedures used by Adam et al. (12) and our protocol revealed that a higher percentage of acetone was used in our batch reactors. This occurred by using RDX stock solutions prepared in acetone (both unlabeled and ^{14}C -labeled) to spike the aqueous solutions with RDX. Although the volume of acetone spiked into the aqueous batch reactors was relatively low (1.04 mL acetone/150 mL H_2O), when this same concentration of acetone was added to 84.03 mM of MnO_4^- without RDX, a similar decrease in MnO_4^- was observed (Fig. S10D, S10E, S10F); similarly, when aqueous RDX solutions were prepared without acetone, the pH remained constant (Fig. S10F) and MnO_4^- consumption was negligible (Fig. S10E). The plateau in RDX loss observed (Figs. S9, S10) resulted from the reaction of acetone with MnO_4^- and likely included the oxidation of acetone to oxalic acid and the reaction of oxalic acid with MnO_4^- to form Mn^{2+} , which is known to facilitate the decomposition of MnO_4^- .

While the accelerated removal of MnO_4^- was traced back to the use of acetone and subsequent formation of carboxylic acids in our batch reactors (Fig. S10), the implications of this observation may be more than just an experimental anomaly. Oxalic acid is a product of the TCE- MnO_4^- reaction (26). Li et al. (27) also showed that oxalate was a primary oxidation product of the explosive TNT (2,4,6-trinitrotoluene) during treatment with Fe^{2+} and H_2O_2 (i.e., Fenton oxidation). Thus, situations may arise where oxalate (or other carboxylic acids) are present and cause excessive MnO_4^- decomposition if the pH is not monitored and prevented from becoming alkaline.

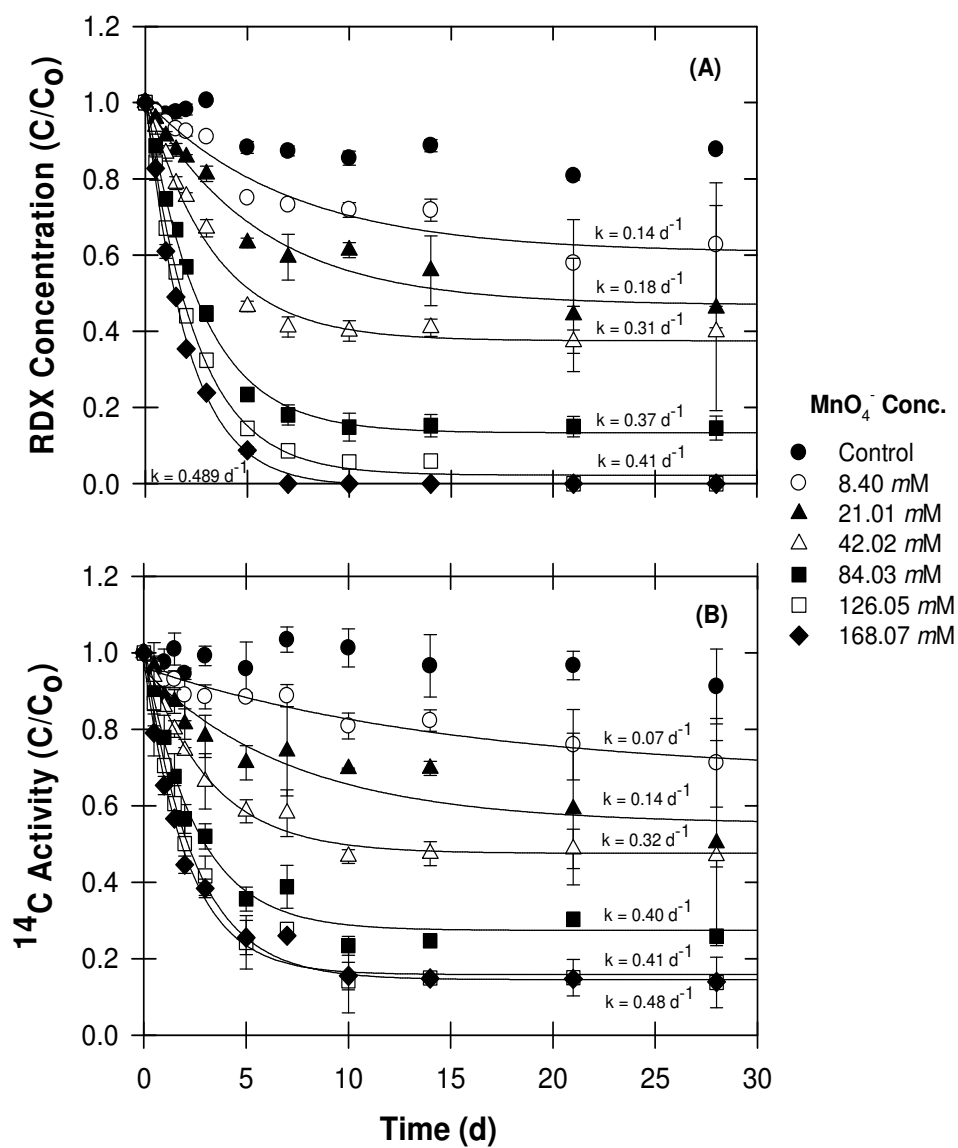


Figure S9: Loss of RDX and ^{14}C -activity in aqueous solution treated with various concentrations of MnO_4^- . Solution samples were quenched with MnSO_4 . Bars indicate sample standard deviations ($n = 3$).

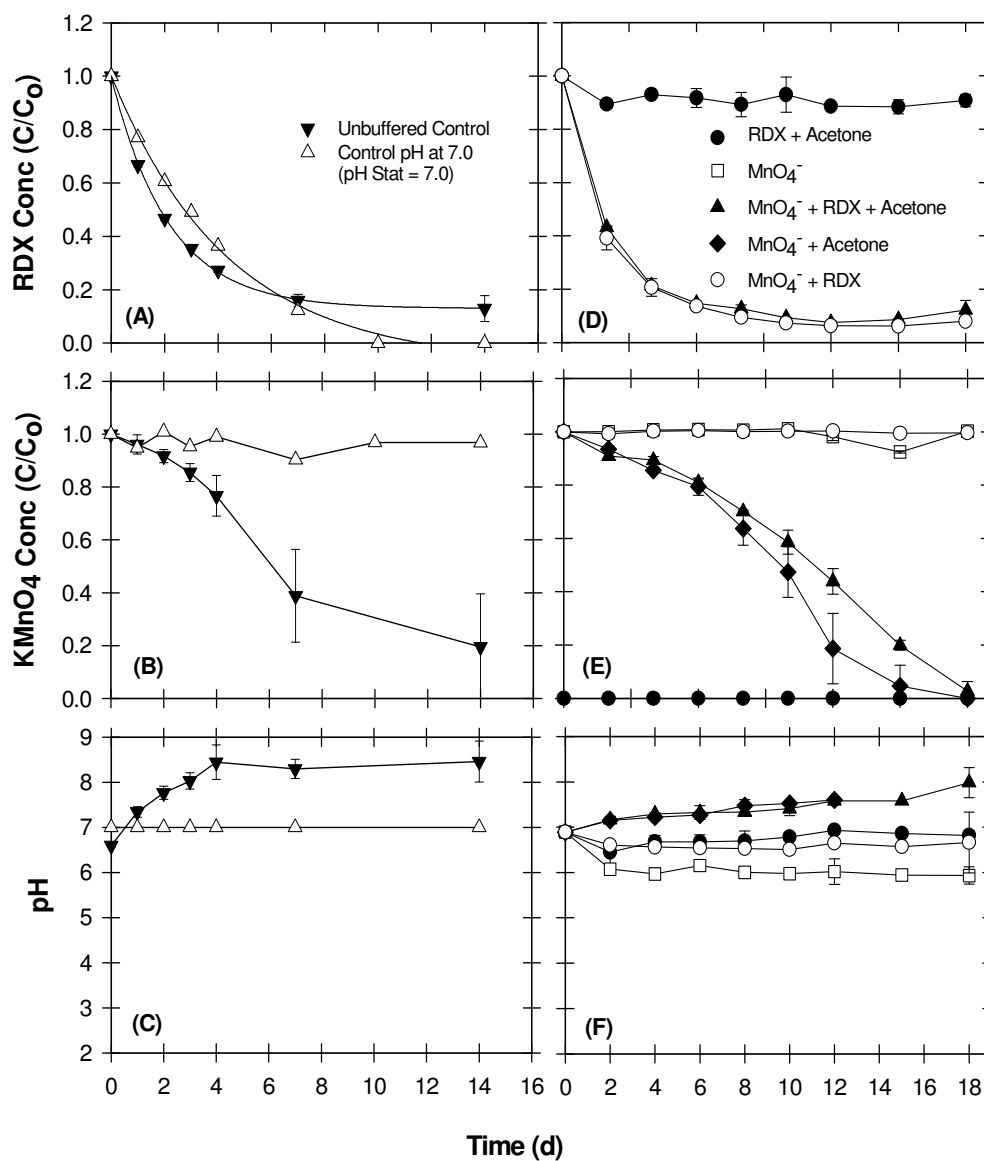


Figure S10: (A-C) Changes in RDX, MnO_4^- concentration, and pH in the presence of acetone following treatment with 84.03 mM of MnO_4^- (i.e., Unbuffered control, and control pH at 7). (D-F) Changes in RDX, MnO_4^- concentration, and pH with/without acetone. Solution samples were quenched with MnSO_4 . Bars indicate sample standard deviations ($n = 3$).

SI-6. Kinetic Models

While second-order expressions are commonly used to describe contaminant destruction rates by MnO_4^- (28-32), if MnO_4^- is in excess, the reaction can also be described by a pseudo first-order expression (12, 33). Like many other second-order reactions between contaminant and MnO_4^- , the general rate equation can be written as:

$$r = -\frac{1}{\alpha} \frac{d[\text{RDX}]}{dt} = k [\text{RDX}]^\alpha [\text{MnO}_4^-]^\beta \quad [\text{Eq. S4}]$$

$$r = k_{\text{obs}} [\text{RDX}]^\alpha \quad [\text{Eq. S5}]$$

$$k_{\text{obs}} = k [\text{MnO}_4^-]^\beta \quad [\text{Eq. S6}]$$

Where α is a reaction order with respect to RDX, β is a reaction order with respect to MnO_4^- , r is a reaction rate, k is a second-order rate constant, and k_{obs} is a pseudo-order rate constant. By varying the initial concentration of MnO_4^- and measuring k_{obs} by fitting the results into a pseudo first-order equation by regression analysis using computer software SigmaPlot Version 10.0 (34), the value of β with respect to MnO_4^- can be obtained by a log-log form of Eq. S6:

$$\log k_{\text{obs}} = \log k + \beta \log [\text{MnO}_4^-]_0 \quad [\text{Eq. S7}]$$

Likewise, by varying the initial concentration of RDX and measuring the reaction rate, the value of α with respect to RDX can be determined by a log-log form of Eq. S5. To evaluate for the reaction rates, we used the initial reaction rate (r_0) by approximating the tangent to the concentration time-curve (35); therefore, Eq. S5 can then be expressed as:

$$\log r_0 = \log k_{\text{obs}} + \alpha \log [\text{RDX}]_0 \quad [\text{Eq. S8}]$$

Second-order rates (k) were then derived from pseudo first-order rates (k_{obs}) by the relationship in Eq. S6.

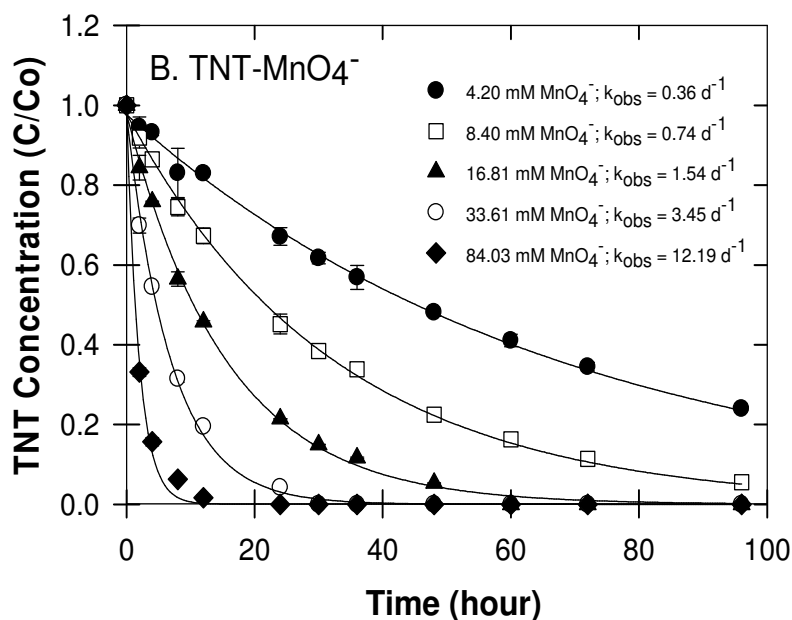
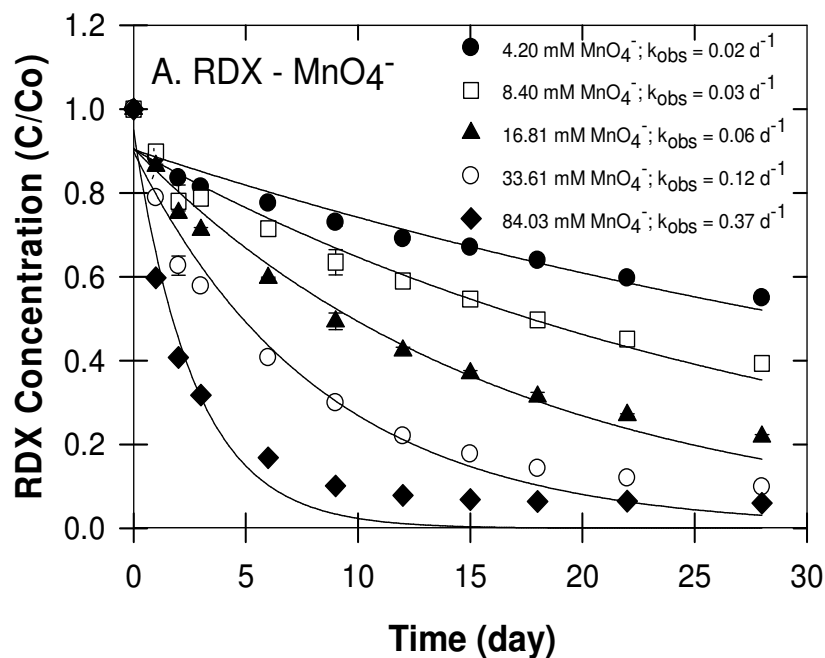


Figure S11: Loss of RDX (A) and TNT (B) when treated with various concentrations of MnO_4^- . Note differences in time scales. Bars indicate sample standard deviations (n = 3).

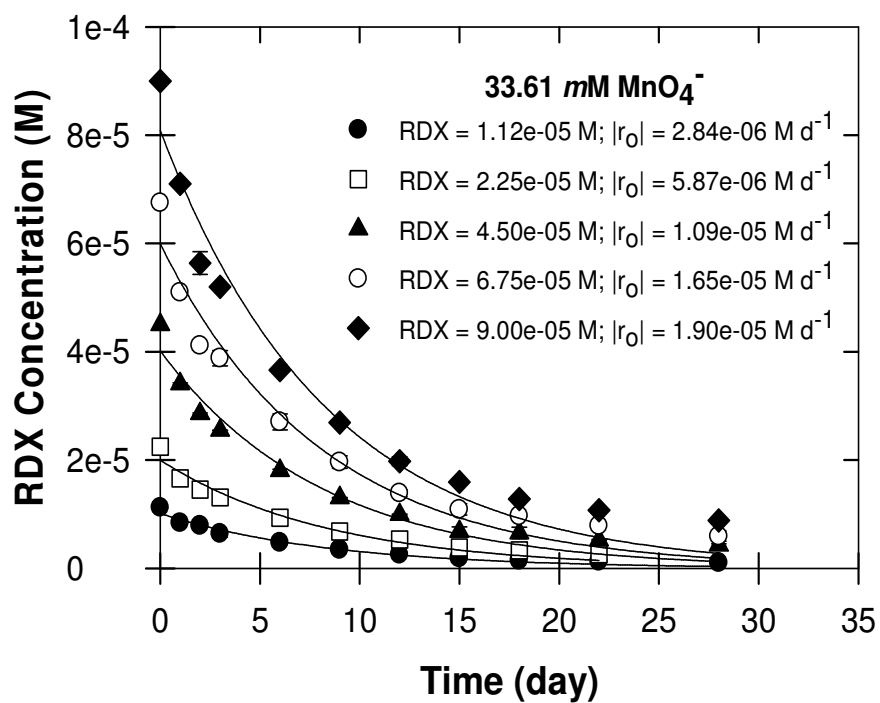


Figure S12: Loss of RDX (initial concentrations ranging from 0.01 to 0.09 mM) when treated with MnO₄⁻ at 33.61 mM. Bars indicate sample standard deviations (n = 3).

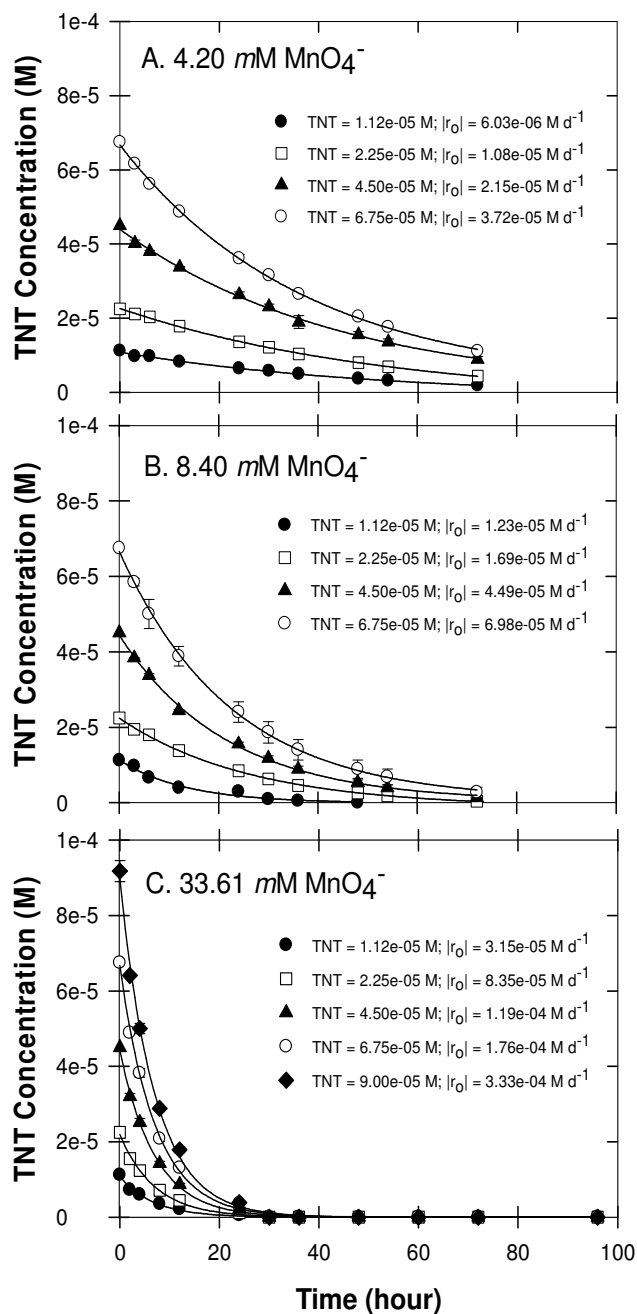


Figure S13: Loss of TNT (initial concentrations ranging from 0.01 to 0.09 *mM*) when treated with MnO₄⁻ at 4.20 (A), 8.40 (B), or 33.61 *mM* (C). Bars indicate sample standard deviations (*n* = 3).

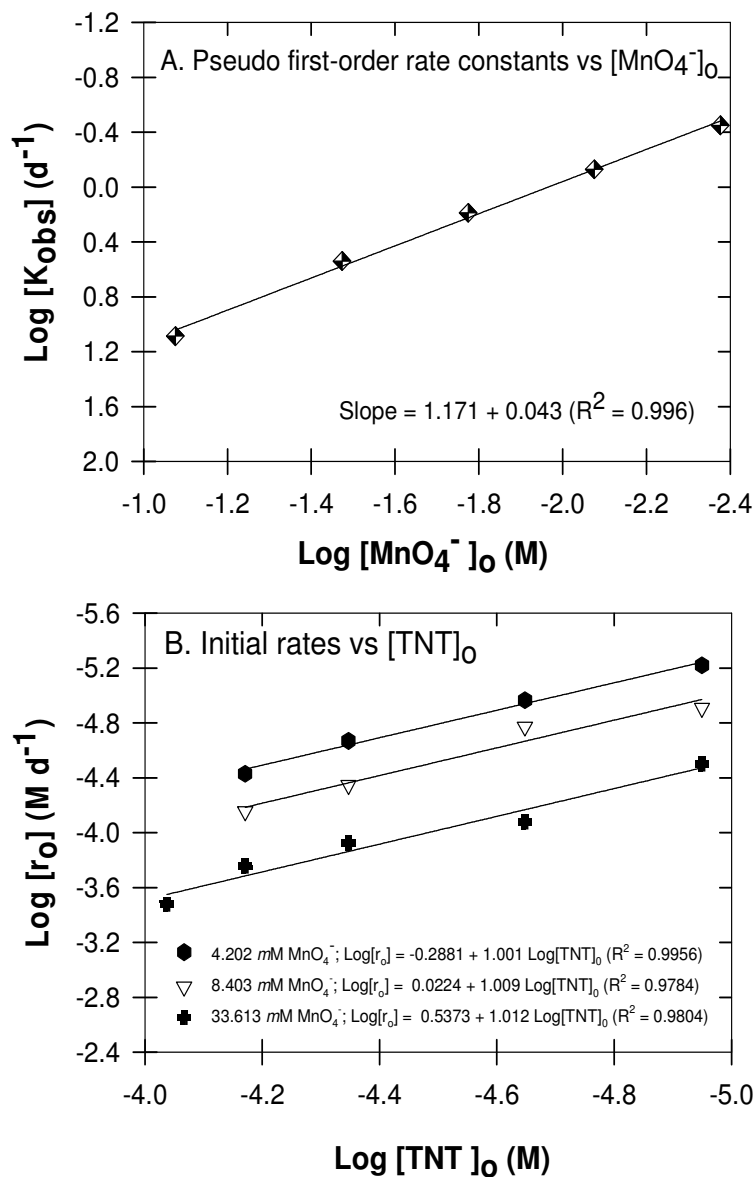


Figure S14: (A) Plot of pseudo first-order rate constants for TNT degradation vs $[\text{MnO}_4^-]$. Aqueous TNT (0.09 mM) was treated with MnO_4^- ranging from 4.20 to 84.03 mM . (B) Plot of initial rates of TNT degradation vs. $[\text{TNT}]_0$ ranging from 0.01 to 0.09 mM when treated with 4.20 , 8.40 , or 33.61 mM MnO_4^- .

SI-7. Temperature dependency

In RDX-MnO₄⁻ temperature experiment, the pseudo first-order rates were evaluated at four different temperatures. The activation energy, E , can be determined using a plot of the Arrhenius equation, as follows:

$$\ln k (T) = \ln A - \frac{E}{RT} \quad [\text{Eq. S9}]$$

Where A is the empirical Arrhenius factor or pre-exponential factor; R is gas constant (8.314 J/K·mol); and T is the absolute temperature (K). The logarithm of the second-order rate constants (k) are plotted against the reciprocal temperature ($1/T$) to determine the Arrhenius factor A and the E/R value from its linear least-squares fit (20, 36-37).

Table S2. Temperature Dependency of Kinetic Rates for Treatment of 0.02 mM RDX with 4.20 mM MnO₄⁻

T (°C)	k _{RDX1} ^a (d ⁻¹)	k _{RDX2} ^{a, b} (L mol ⁻¹ d ⁻¹)	k _{RDX2} ^a (L mol ⁻¹ min ⁻¹)	Ln k _{RDX2} ^a	1/T (1/K)
20	0.02 (0.00)	3.52 (0.13)	0.00 (0.00)	-6.01 (0.04)	0.0034
35	0.06 (0.00)	14.22 (0.21)	0.01 (0.00)	-4.62 (0.01)	0.0032
50	0.35 (0.01)	84.21 (2.22)	0.06 (0.00)	-2.84 (0.03)	0.0031
65	0.89 (0.03)	212.65 (7.16)	0.15 (0.01)	-1.91 (0.03)	0.0030

a Parenthetic values represent standard error of estimates. *b* k_{RDX2} = k_{RDX1}/C_{MnO4-}

SI-8. Single electron transfer versus hydride (or hydrogen atom) removal

Based on supporting literature (38-40), two key ideas emerge:

- 1) Two different mechanisms are observed in amino oxidations
 - a) single-electron transfer (SET) at the amine nitrogen and
 - b) hydride (or hydrogen) abstraction from the carbon;
- 2) The electron density on the amine nitrogen determines the operative mechanism.

Specifically, electron-poor amines or those with resonance stabilized intermediates tend to be oxidized by hydride abstraction. When these specific principles and the principles of organic oxidation chemistry are applied to RDX, the problem simplifies somewhat. For instance, there are only four distinct sites for oxidation of RDX: an oxygen atom, a nitro nitrogen atom, an amine nitrogen atom, or a carbon. This is illustrated below.

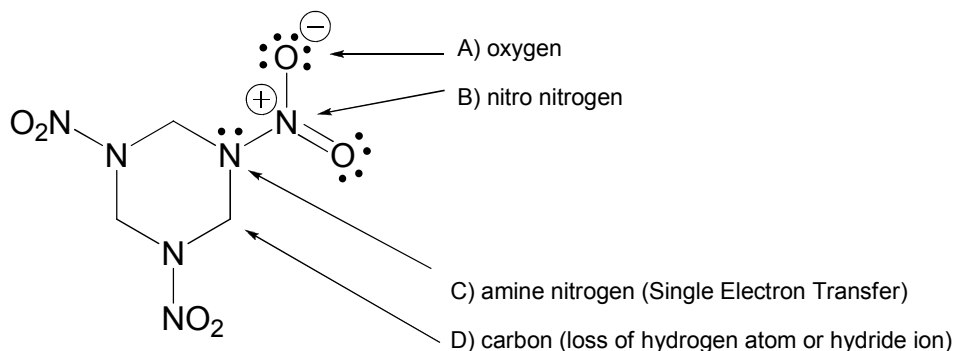


Figure S15: Possible sites for oxidation of RDX.

Oxidation at the oxygen atom or a nitro nitrogen atom would give extremely unstable intermediates since they place positive charge on electronegative oxygen or

an already electron deficient nitro group nitrogen, respectively. The only two reasonable sites for oxidation of RDX remaining are the exact two options carefully studied by the cited authors (38-40). That is, oxidation at the amine nitrogen (by SET) or oxidation at the carbon (by hydride abstraction, see S16, S17 below).

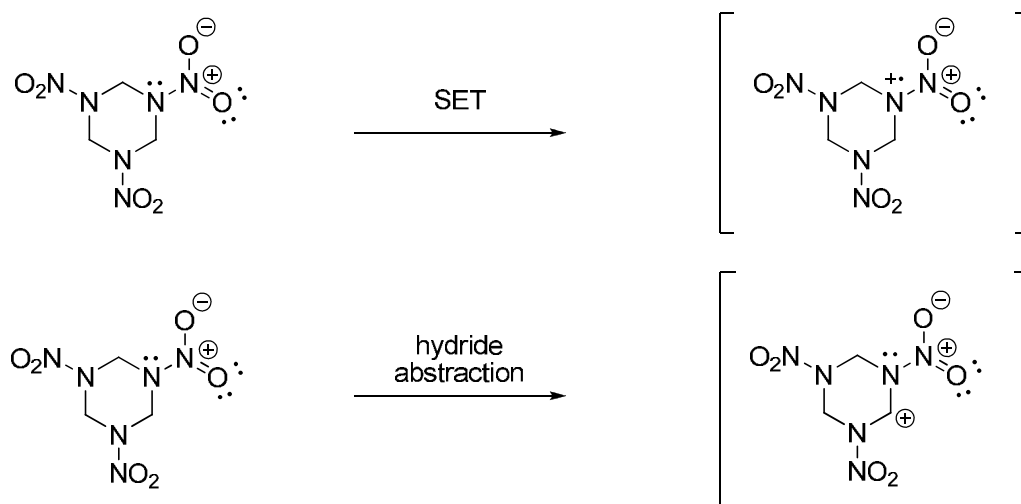


Figure S16: Overall comparison of SET versus hydride abstraction of RDX.

Because the amino nitrogens in RDX are extremely electron-poor, the hydride loss will tend to dominate the reaction. This is probably because the intermediate resulting from an initial single-electron transfer would produce an intermediate having two positive charges on the adjacent nitrogen atoms, as shown above. Such an intermediate would be much less stable than the proposed carbocation which maximizes the distance of the two positive charges from each other, and places one of them on the more electropositive carbon atom.

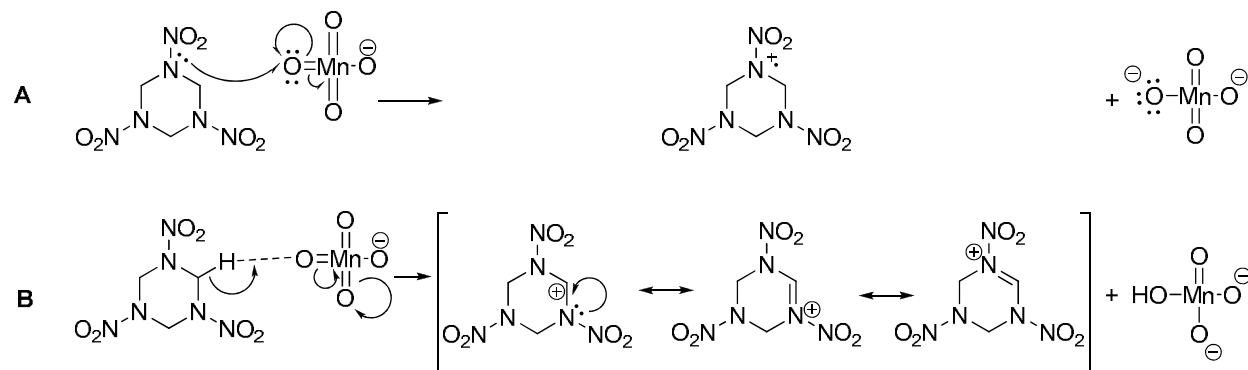


Figure S17: A comparison of initial first steps via single electron transfer (A) versus hydride removal (B).

When we considered both possible first-steps in the RDX- MnO_4^- reaction (SET vs. Hydride loss, Fig. S15), we believe the strongly electron-withdrawing nitro groups would tend to destabilize any cation intermediate. This destabilizing effect, however, would be minimized for the carbocation intermediate formed via hydride abstraction (Fig S17B) compared to the aminium ion formed by SET (Fig. S17A) because: 1) the carbocation is further from the nitro group than the aminium ion and is therefore less destabilized by inductive effects, 2) carbon is more electropositive than nitrogen, and thus less destabilized by the cation, 3) resonance stabilization for the carbocation can occur but is completely absent for the aminium intermediate. These theoretical explanations are supported by the experimental observations that 1°, 2° and 3° alkylamines having all their electron density isolated on the nitrogen tend to be oxidized by SET (38-39), while amines with resonance distributed electron density like benzylamine clearly undergo loss of hydride (or hydrogen atom) (40). Thus, theory and experiment indicate that the carbocation intermediate will be more stable and therefore formed more quickly than the aminium cation intermediate in RDX.

SI-10. References

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