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Ultrastable Particle-Stabilized Foams

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Experimental Section

The colloidal particles used in this study were acquired from the following suppliers: δ -Al₂O₃, $d_{50} \sim 70$ nm, Nanophase Technologies Co. (Romeoville, IL, USA); α -Al₂O₃, $d_{50} \sim 200$ nm (grade Ceralox HPA-0.5), Sasol North America Inc. (Tucson, AZ, USA); α -Al₂O₃, $d_{50} \sim 2000$ nm (grade CL 2500 SG), Alcoa Co. (Ludwigshafen, Germany); ZrO₂, $d_{50} \sim 50$ nm (grade TZ-3Y-E), Tosoh Corporation (Tokyo, Japan); β -Ca₃PO₄, $d_{50} \sim 50$ nm, Flame Powders AG (Schlieren, Switzerland); SiO₂, $d_{50} \sim 80$ nm (grade Snowtex ZL), Nissan Chemical (Houston, TX, USA). All other chemicals were purchased from Fluka AG (Buchs, Switzerland). Prior to foaming, colloidal suspensions were prepared by adding the dry powders to the liquid solvent upon steady mixing. The suspension solids concentration varied between 15 and 45 vol%, depending on the powder, solvent and short amphiphiles

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used. Surface lyophobization of initially hydrophilic particles was carried out by first de-agglomerating the powder through a standard ball-milling process, followed by the gradual addition of aqueous solutions containing the short amphiphiles. Concentrated 2M HCl or 1M NaOH solutions (Titrisol, Fluka AG, Buchs, Switzerland) were used for pH adjustments. The adsorption of amphiphiles on the particle surface was indirectly determined by measuring the concentration of amphiphiles left in the bulk liquid media after 2 h mixing of the powder with the amphiphile. The bulk concentration was determined by removing the particles in a two-step centrifugation process (Z513K, Hermle Labortechnik GmbH, 4,500 rpm, 1h; 5417R, Eppendorf AG, 15,000 rpm, 20 min) and subsequently measuring the amphiphilic concentration in the supernatant solutions by potentiometric titration (DT-1200, Dispersion Technology, Inc., Mount Kisco, NY, USA). The suspension surface tension was assessed with the pendant drop method (PAT1, Sinterface Technologies GmbH, Berlin, Germany) [1], using 15-35 mm³ suspension droplets pending in air. Foams were produced by thoroughly mixing the concentrated suspensions with a planetary mixer (Major Classic, Kenwood Ltd, Havant, UK) for 3 minutes at full speed. The whipped cream and egg white foams used for comparison were also prepared by mechanical frothing for 3 minutes. The shaving foam (Gillette Foam, Regular, Gillette Co, London) was taken directly from the product container and was not submitted to any further processing. The foamability was measured from the weight and volume of the foam obtained. Transmitted light microscopy (Polyvar MET, Reichert-Jung, Austria) was used to investigate foam stability by monitoring the bubble size distribution of wet foams over time. Fluorescent silica particles and hexyl amine was used for the confocal laser scanning microscopy images. The labeled silica particles ($d_{50} \sim 500$ nm) were synthesized following the procedure described in reference [2] and consisted of a

silica core (~ 400 nm), a fluorescent layer around the core (~ 10 nm) and an outer silica rim (~ 100 nm). Concentrated silica foams (15 vol%) were prepared with a hand-mixer at pH 10.2 with 30 mM of hexyl amine. Hollow colloidosomes were obtained by diluting (20×) the concentrated foams and were subsequently harvested for imaging in the confocal microscope.

Foams with different materials

Particle-stabilized foams with several different materials were prepared using the method described in the article. Table S1 depicts the exact conditions required for surface lyophobization of various types of colloidal particles and the resulting features of the foams produced by mechanical shearing. Foams exhibiting high air content and small mean bubble sizes were achieved by appropriately selecting the anchoring group and tail length of the amphiphile molecule according to the surface chemistry of the colloidal particles used (Table S1).

Role of free amphiphiles:

The reduction in surface tension required for foaming was shown to be due to the combined effect of modified particles and non-adsorbed free amphiphiles (see Figure 3 of the article). However, it is important to note that even though the non-adsorbed amphiphiles also decrease the suspension surface tension (Figure 3), no stable foams were obtained upon mechanical shearing of aqueous solutions containing solely the amphiphilic molecules. Bubbles created during mixing

promptly disappeared when mechanical shearing was stopped. Additional foaming experiments were carried out to confirm that the foams obtained do not result from the adsorption of free amphiphiles at the air-water interface in combination with an increase of the viscosity of the foam lamella due to the presence of particles. These experiments were performed with suspensions containing the amphiphile butyl amine and a high concentration of alumina particles (35 vol%) in water at pH 4.75. Since amines do not adsorb at the alumina surface at acidic pHs, the amphiphiles present in this suspension are free to adsorb at the air-water interface, while the completely hydrophilic alumina particles remain within the suspension liquid medium. No stable foam was produced by mechanical shearing these amine-containing alumina suspensions, confirming the major role of the interface-adsorbed lyophobized particles on the preparation of highly-stable foams.

Stabilization mechanism:

Among the several mechanisms leading to foam destabilization ^[3], bubble disproportionation had so far been particularly difficult to avoid in liquid foams due to the ever-present difference in Laplace pressure between bubbles of distinct sizes, which ultimately results in a steady diffusion of gas molecules from smaller to larger bubbles over time. ^[3] The remarkable resistance of our particle-stabilized foams against coalescence and disproportionation is most likely imparted by the strong attachment of particles at the air-water interface (Figure 4 in the article) and by the formation of an attractive particle network at the interface and throughout the foam lamella. ^[4, 5]

Particles attached to the air-water interface can reduce the overall foam free energy by thousands of kTs, if a considerable amount of interfacial area is replaced upon adsorption. [6, 7] Such a reduction in free energy makes the interfacial adsorption of partially lyophobic particles an irreversible process, as opposed to the continuous adsorption and desorption of conventional surfactant molecules at the air-water interface (Gibbs-Marangoni effect). Particles strongly adsorbed at the interface may resist the shrinkage of small bubbles during disproportionation by forming a percolating interfacial armor that mechanically withstands the low pressures resulting from gas diffusion outwards the bubble. [8] The fact that the air bubbles are highly confined throughout the foam volume may also contribute to the enhanced stability by restricting the movement of particles attached to the interface. In this case, the immobile attached particles would hinder the mobility of the airwater interface in a similar way to the well-known pinning effect of particles in grain boundaries of polycrystalline materials. This effect arises when a moving interface is constrained by an interface-adsorbed particle due to local equilibrium along the triple-phase junction. [9]

The attractive network of particles formed at the air-water interface and within the foam lamella is also expected to withstand the overpressure created in larger bubbles and prevent their expansion during disproportionation. The attractive particle network was formed either due to the screening effect of the adsorbed amphiphile (in the case of carboxylates and amines) or due to the high concentration of counter-ions in solution (in the case of gallates). Such conditions lead to a decrease of the electrical double layer thickness around particles, favoring their coagulation by van der Waals and hydrophobic attractive forces. The formation of such attractive colloidal network in particle-stabilized foams was confirmed by confocal microcopy images of concentrated foams. The fact that the foam stability

was enhanced by the addition of screening salt ions strongly indicates the important role of this attractive network. [5]

Comparison with flotation additives:

The lyophobization approach used in our method resembles that applied for the separation of micron- to millimeter-sized ore particles in flotation processes. However, the hydrophobic tail of the amphiphiles used in the flotation of oxides is considerably longer (typically > 10 carbons) than that of the short-chain molecules used in this work. [10-14] Shorter molecules such as xanthates exhibiting usually 3 to 5 carbons are also used in flotation, but have been predominantly applied for the separation of electrically conductive sulfide ores [15] and are usually inefficient in the recovery of oxide particles. [16] It should also be emphasized that the flotation process relies on the phase separation (creaming) of bubbles in order to purify the mineral ore, as opposed to our approach where no creaming effect is desired.

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FIGURE AND TABLE CAPTIONS

Table S1 Particle-stabilized foams produced from a variety of metal oxide colloidal particles using the approaches outlined in Figure 1 of the article.

Figure S1: Outstanding stability of particle-stabilized foams in comparison to state-of-the-art food and cosmetic foams. No drainage, creaming and disproportionation was observed in all particle-stabilized foams prepared with partially lyophobic particles (exemplified in d for alumina and valeric acid), as compared to the considerable destabilization that takes place in well-established cosmetic (a, shaving foam) and food foams (b, whipped cream; c, egg white foam). Images shown on the left-hand side were taken 5 minutes after foaming, whereas those on the right-hand side were taken after 4, 69, 67 and 100 hours for the shaving (a), whipped cream (b), egg white (c) and particle-stabilized foams (d), respectively (scale bar: 50 μm). Due to their remarkable stability, particle-stabilized foams can be used to produce bulk macroporous materials (> 500 cm³) upon drying and sintering, as exemplified by the inset image in (d) for alumina (scale bar: 50 μm).

TABLE

Table S1: Particle-stabilized foams produced from a variety of metal oxide colloidal particles using the approaches outlined in Figure 1 of the article.

Particle		Amphiphile		_	Solids	Foamability	Mean
Туре	Size, d_{50} (nm)	Type	Conc. (mol/L)	Solvent	content (vol%)	(% air)	bubble size (μm)
δ-Al ₂ O ₃	70	Valeric acid	0.011	Water, pH 4.75	5	88	130
δ-Al ₂ O ₃	70		0.050		20	90	47
α -Al ₂ O ₃	200		0.030		35	80	26
α -Al ₂ O ₃	2000		0.020		25	66	40
α-Al ₂ O ₃	200	Propyl gallate	0.100	Water, pH 9.9	35	83	30
ZrO ₂	50		0.080	Water, pH 9.9	22	79	70
Ca ₃ PO ₄	50	Butyl gallate	0.040	Water, pH 9.9	17	86	45
SiO ₂	80	Hexyl amine	0.065	Water, pH 10.6	35	82	30

FIGURES

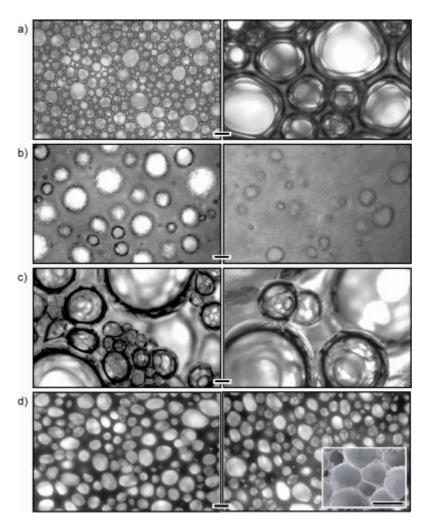


Figure S1